# **SPECTRA** Computer Code Manuals

## Volume 2 - User's Guide

# Version 24-02

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Arnhem, February 2024

K6223/24.277594 MSt-2402

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### Abstract

SPECTRA (Sophisticated Plant Evaluation Code for Thermal-hydraulic Response Assessment) is a fully integrated system analysis code, that models thermal-hydraulic behavior of Nuclear Power Plants, including reactor cooling system, emergency and control systems, containment, reactor building, etc. of various reactor types, like BWR, PWR, HTR. It can also be used to assess thermal-hydraulic response of non-nuclear plants, for example cooling systems of chemical reactors.

The full documentation of SPECTRA consists of the following four volumes:

- Volume 1: Program Description
- Volume 2: User's Guide
- Volume 3: Verification and Validation
- Volume 4: Code Structure, Development, Hardware and Software Requirements

This report presents Volume 2 of the SPECTRA Code Manuals - User's Guide. A detailed description of input data is provided in this volume. Examples of input files are shown. This volume presents also a description of the output files. The variables printed in the main SPECTRA output data file are shown and shortly described. Examples of output files are presented. Finally, a description of the plot file, and the procedure to make plots using the SPECTRA post-processor is given.

The SPECTRA Manuals are freely available in internet and are also supplied together with the SPECTRA code. The Volume 2 of the Code Manuals is provided in the file **Spectra-Vol2.pdf**.

# Explanation of names and abbreviations

CF	Control Function
CV	Control Volume
DIA	Diagnostics file
ICF	Initial Condition File
IT	Isotope Transformation
JN	Junction
MP	Material Properties
OUT	Output file
OX	Material Oxidation
PLT	Plot file
RK	Reactor Kinetics
RT	Radioactive Particle Transport
SC	1-D Solid Heat Conductor
SPECTRA	Sophisticated Plant Evaluation Code for Thermal-hydraulic Response
	Assessment
TC	2-D Solid Heat Conductor
TF	Tabular Function
TFD	Tabular Function Data file
TR	Thermal Radiation

### 1 Introduction

SPECTRA (Sophisticated Plant Evaluation Code for Thermal-hydraulic Response Assessment) is a fully integrated system analysis code, that models the thermal-hydraulic behavior of Nuclear Power Plants, including reactor cooling system, emergency and control systems, containment, reactor building, etc. of various reactor types, like BWR, PWR, HTR. It can also be used to assess thermal-hydraulic response of non-nuclear plants, for example cooling systems of chemical reactors. The structure of SPECTRA is shown in Figure 1-1.

The SPECTRA Code Manuals consists of the following four volumes:

- Volume 1: Program Description
- Volume 2: User's Guide
- Volume 3: Verification and Validation
- Volume 4: Code Structure, Development, Hardware and Software Requirements

This report presents Volume 2 of the SPECTRA Code Manuals (SCM) - User's Guide. The full description of the input data needed to run the program as well as the output data is given.



Figure 1-1 SPECTRA code structure.

Chapter 2 gives a detailed description of input data. Examples of input files are shown.

Chapter 3 presents a description of the output files. The variables printed in the main SPECTRA output data file are shown and shortly described. Examples of output are presented. This chapter provides also the description of the plot file and the procedure to make plots using the SPECTRA post-processor, use of the stop file to terminate calculations, use of the ICF file to provide the initial conditions, use of the TFD file for interactive Tabular Function definitions.

Chapter 4 presents an installation guide. Hardware and software requirements are specified. Installation and execution of the code are described. A verification test case is presented.

Several appendices are included, showing example cases and explaining the effect of using certain input parameters. The appendices show the influence of the user-defined parameters on the maps of pumps/compressors and turbines, as well as the influence of the user-defined parameters on valve loss factors.

## 2 Description of Input Data

SPECTRA input file must have an extension ".SPE". The name must not be longer than 510 characters or shorter than 5 characters, including extension, i.e. there must be at least one character and no more than 506 characters before the extension. The input file consists of a sequence of input records. Five different record types may be distinguished:

- title record,
- comment records,
- data records,
- requests for file attachments,
- terminator record.

The **title record** is optional and need not to be entered, but it is recommended to enter title for each problem, to have easy way to identify the problem. A title record is identified by an equal sign (=) in the first column. The title is printed in the output and the diagnostics file. If more than one title record is entered, the last one is used.

A **comment record** has an asterisk sign (\*) as the leftmost non-blank character. All characters to the right of an asterisk are interpreted as comments. Completely blank lines are interpreted as comments.

A **data record** may contain an arbitrary number of data words that may be integer (I), real (R), or alphanumeric (A), and, optionally, a comment preceded by an asterisk sign. Up to 512 characters are read by the program so the data words cannot be written on fields further to the right. The leftmost word of a data record is interpreted as the record identifier, the remaining words as the data words. Every data record must have a valid identifier.

If less data is entered than is expected in a given record, zeroes are assumed for the remaining words and a warning message is printed to the diagnostics file. If more data is entered than is expected, the remaining values are omitted and a warning message is printed to the diagnostics file.

The User's Guide gives a detailed description of every input entry (Word). Most of the input entries have an acceptable range and a default value. The acceptable ranges and default values are listed in the Chapter 2, describing the input data records. If the value for a given parameter is not entered <u>or it is entered as zero</u> then the default value (if exists) is assumed. In the cases when a non-zero value is the default value and zero is a valid input value, an instruction is given how to set the value to zero. If the input value is outside the acceptable range an error message is printed to the diagnostics file and the run is terminated at the end of the input processing phase.

Files may be attached to the input file using requests for file attachment, which has the form:

#### ATTACH FILENAME

The word ATTACH has to be written from the first column of a record. The input file can have as many attachments as desired, however no multiple level attachments are allowed. That means, an attached file cannot contain the ATTACH statement. Attaching files is convenient when a (large) model has to be used for calculations of multiple accidents. In such cases the base input deck remains the same, only small accident specific changes need to be made. The base deck can be stored and, when needed, attached at the top of input file, followed by the accident scenario inputs, which will replace the data in the base deck.

The input deck is terminated by the **terminator record**. The terminator record is identified by a period sign (.) in the first column. The terminator record is optional. If there is no terminator record in the data file, all records in the file are read, if the terminator record is present then all the following records are treated as comments.

### 2.1 Control Volume Input Data

### 2.1.1 Records: 100000, Control Volume Main Data - Global

Using this record one may specify the parameters described in record 100XXX for all Control Volumes in the model - see description of record 100XXX below.

### 2.1.2 Records: 100XXX, Control Volume Main Data - Individual

W-1 (I) :	ITYPCV	Control volume typ	be, (-).
		ITYPCV = 0:	normal (active) volume, transient conditions are
			calculated from mass and energy balance, unless the
			CV solution is switched off by the Solver option
			IOPSL - see record 900XXX, Word 6.
		ITYPCV $> 0$ :	user-defined conditions. This CV type is typically
			used to supply boundary conditions. The CV
			parameters (such as pressure, temperature, etc.) are
			either constant and equal to their initial values (for
			example pressure and temperature are entered in
			record 120XXX, section 2.1.9), or time-dependent,
			defined by Tabular or Control Functions specified
		$\mathbf{ITVDCV} < 0.$	In record 125AAA (section 2.1.14).
		$\prod IPCV < 0$	user-defined conditions for $l < 0.0$ s. At $l = 0.0$ s it
			to specify boundary conditions at the initial (for
			example steady state) phase of calculations. In that
			case the start time for the steady state calculations
			should be defined as negative.
		ITYPCV > 1000:	user-defined conditions if the value of the Tabular
			Function TF-YYY is greater than 0.0, where YYY
			= ITYPCV-1000, normal (active) CV otherwise.
			Similar to ITYPCV < 0, but in this case CV may be
			activated and deactivated many times during
			calculations.
		Acceptable range:	any integer<1000, must be a valid reference number
			of a Tabular Function, if $> 1000$ .
		Default value:	0 if no values are set in the record 125XXX, 1
			otherwise

**IDSPCV** W-2(I): Pointer to a Tabular or Control Function that defines the atmosphere Density Stratification Parameter (DSP) for this volume, (-). If the number is positive, then DSP will be defined by a Tabular Function with the reference number: IDSPCV. If the number is negative, then DSP will be defined by a Control Function with the reference number: IDSPCV . At any given time of the transient DSP will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, DSP will be set to 0.0. If it is larger than 1.0, DSP will be set to 1.0. If no value is entered, or the entered value is equal to zero, the DSP will be equal to 0.0 (perfect mixing) throughout the whole transient. Note that the actual value of DSP may be different from that specified

by the Tabular or Control Function. The code internally calculates the minimum and maximum value of DSP based on thermodynamic conditions and thermal stratification. If the value defined by Tabular or Control Function is greater than the maximum limit calculated by the code then the maximum limit is used. If the value defined by Tabular or Control Function is smaller than the minimum limit calculated by the code then the minimum limit is used.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.

Default value:

W-3(I): **ITSPCV** Pointer to a Tabular or Control Function that defines the atmosphere Thermal Stratification Parameter (TSP) for this volume, (-). If the number is positive, then TSP will be defined by a Tabular Function with the reference number: ITSPCV. If the number is negative, then TSP will be defined by a Control Function with the reference number: ITSPCV . If the current value of the Tabular or Control Function is smaller than 0.0, TSP will be set to 0.0. If it is larger than 1.0, TSP will be set to 1.0. If no value is entered, or the entered value is equal to zero, then TSP will be equal to 0.0 (perfect mixing) throughout the whole transient. Note that the value of TSP is restricted further by the minimum and maximum temperatures, determined by the words 4 and 5 below. Thus the actual value of TSP may differ from the value defined by the Tabular or Control Function.

Acceptable range: must be a valid reference number of a Tabular or a Control Function. if non-zero.

Default value:

W-4(I): ITMNCV Pointer to a Tabular or Control Function that defines the minimum atmosphere temperature (at the bottom of atmosphere part of CV) in case when the stratification model is applied (ITSPCV is non-zero). If the number is positive, then the minimum temperature will be defined by a Tabular Function with the reference number: ITMNCV. If the number is negative, then the minimum temperature will be defined by a Control Function with the reference number: | ITMNCV |. If the number is zero the minimum temperature is calculated internally by the code (recommended).

0.

		Acceptable range: Default value:	must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-5 (I) :	ITMXCV	Pointer to a Tabul temperature (at the stratification mode positive, then the r Function with the regative, then the r the maximum ter (recommended). <i>Acceptable range:</i> <i>Default value:</i>	lar or Control Function that defines the maximum top of the atmosphere part of CV). in case when the el is applied (ITSPCV is non-zero). If the number is maximum temperature will be defined by a Tabular e reference number: ITMXCV. If the number is maximum temperature will be defined by a Control eference number: ITMXCV  . If the number is zero mperature is calculated internally by the code must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-6 (I) :	IPSPCV	Pointer to a Tabula Stratification Parati positive, then PSF reference number: defined by a Contra If the current value 0.0, PSP will be se If no value is entered be equal to 0.0 (pet that the value of PSF temperatures, deter value of PSP may de Function. Acceptable range: Default value:	ar or Control Function that defines the Pool (thermal) meter (PSP) for this volume, (-). If the number is P will be defined by a Tabular Function with the IPSPCV. If the number is negative, then PSP will be ol Function with the reference number:  IPSPCV . e of the Tabular or Control Function is smaller than t to 0.0. If it is larger than 1.0, PSP will be set to 1.0. ed, or the entered value is equal to zero, then PSP will erfect mixing) throughout the whole transient. Note SP is restricted further by the minimum and maximum rmined by the words 7 and 8 below. Thus the actual liffer from the value defined by the Tabular or Control must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-7 (I) :	IPMNCV	Pointer to a Tabula temperature (at the is applied (IPSPC) minimum temperat reference number: minimum temperat reference number: temperature is calc <i>Acceptable range:</i> <i>Default value:</i>	ar or Control Function that defines the minimum pool bottom of pool) in case when the stratification model V is non-zero). If the number is positive, then the ture will be defined by a Tabular Function with the IPMNCV. If the number is negative, then the ture will be defined by a Control Function with the IPMNCV  . If the number is zero the minimum ulated internally by the code (recommended). must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-8 (I) :	IPMXCV	Pointer to a Tabula temperature (at the applied (IPSPCV maximum tempera reference number:	r or Control Function that defines the maximum pool top of pool) in case when the stratification model is is non-zero). If the number is positive, then the ture will be defined by a Tabular Function with the IPMXCV. If the number is negative, then the

0.

maximum temperature will be defined by a Control Function with the reference number: |IPMXCV|. If the number is zero the maximum temperature is calculated internally by the code (recommended).

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero.

Default value:

W-9(I): DTSPCV Maximum value of the ratio DSP/TSP. This parameter may be used to limit the atmosphere density stratification, DSP, based on the atmosphere thermal stratification, TSP. Usually TSP is easier to estimate than DSP, and this limit prevents from obtaining unrealistically large DSP. This word does not affect the TSP. If a negative value is entered then DSP is independent of TSP, but the saturation limit is used. The saturation limit is applied to prevent, as much as possible, the local steam partial pressure to increase above the saturation pressure. The saturation limit is used if DTSPCV > -99. If DTSPCV  $\leq -99$  then the saturation limit is not used, and DSP is given directly by the Tabular or Control Function. For Best Estimate analysis the default value is recommended. If the user wishes the force the desired density stratification, for example for conservative or sensitivity calculations, then the DTSPCV should be set to  $\leq -99$ .

Acceptable range:DTSPCV  $\leq 1000$ .Default value:-1.0 if ITSPCV=0 (Word 3 above),+3.0 otherwise.

W-10 (R): DSPCV Initial value

Initial value of Density Stratification Parameter, DSP, (-). DSP is defined as follows (see Volume 1):

$$\frac{dx_i(z)}{dz} = \tan\left(\frac{\pi}{2}DSP\right)$$

where  $x_i(z)$  is the molar concentration of gas *i* (the lightest gas) at the relative elevation z in the atmosphere. The value of z is equal to zero at the pool surface elevation (at the bottom of the CV if pool is not present), and equal to one at the top of CV.

For example, suppose that the hydrogen concentration at the bottom of the CV is 0.2% (0.002), while the concentration at the top of the CV is 5% (0.05). The value of DSP is obtained from:

 $((0.05 - 0.002) / 1.0) = \tan(\pi/2 \cdot DSP)$ , or: DSP =  $2/\pi \cdot \tan((0.05 - 0.002) / 1.0) = 0.0305$ Acceptable range:  $0.0 \le DSPCV \le 1.0$ . Default value: 0.0.

W-11 (R): TSPCV Initial value of Thermal Stratification Parameter, TSP, (-). TSP is defined as follows (see Volume 1):

$$TSP = \frac{T_{top}^{atms} - T_{bot}^{atms}}{T_{ave}^{atms}}$$

where  $T^{atms}$  is the atmosphere temperature, and the subscripts refer to the top, bottom, and average values.

For example, suppose that the initial atmosphere temperature is equal to 300 K at the pool surface elevation (at the bottom of CV if pool is not present), and is equal to 340 K at the top of CV. Average temperature is thus 320 K (this value needs to be entered in record 120XXX - see section 2.1.9 below). The value of TSP is equal to: TSP = (340 - 300) / (340 - 300)320 = 0.125.

Acceptable range:  $0.0 \le \text{TSPCV} \le 1.0$ . Default value: 0.0.

W-12 (R): **PSPCV** Initial value of Pool Stratification Parameter, PSP, (-). PSP is defined as follows (see Volume 1):

$$PSP = \frac{T_{top}^{pool} - T_{bot}^{pool}}{T_{ave}^{pool}}$$

where T<sup>pool</sup> is the pool temperature, and the subscripts refer to the top, bottom, and average values.

For example, suppose that the initial pool temperature is equal to 280 K at the pool bottom and 300 K at the pool surface elevation. The average temperature is thus 290 K (this value needs to be entered in record 120XXX - see section 2.1.9 below). The value of PSP is equal to: PSP = (300 - 280) / 290 = 0.069. Acceptable range:  $0.0 \le \text{TSPCV} \le 1.0$ .

```
Default value:
                   0.0.
```

- Maximum value of the rate of change of DSP, d(DSP)/dt, (1/s). W-13 (R): DDDTCV Acceptable range:  $10^{-5} \le \text{DTSPCV} \le 1.0$ . Default value:  $3.3 \cdot 10^{-3}$  with this value it takes at least 5 min (300 s) to remix a perfectly stratified layer,
- W-14 (I): **IRSBCV** Indicator determining whether eventual stratification should be removed during hydrogen burns.
  - stratification is removed during slow deflagrations, fast = 1: deflagrations and detonations,
  - = 2: stratification is removed during fast deflagrations and detonations,
  - = 3: stratification is removed during detonations,
  - > 3: stratification is not removed during hydrogen burns.
  - Acceptable range: IRSBCV > 0.

*Default value:* 1.

#### W-15 (I): Interpretation of the initial pool level definition (input parameter ILEVCV ZPLSCV, record 120XXX). = 0: ZPLSCV is the pool level (m), relative to the bottom of CV = 1: ZPLSCV is the relative pool level (-), $0.0 \le ZPLSCV \le 1.0$ *Acceptable range:* ILEVCV = 0 or 1 0

Default value:

### 2.1.3 Records: 101000, Control Volume Groups - General Data

- W-1 (I):KGRPCVDefault CV group number. CV groups are introduced for editing; at the<br/>end of input processing an altitude-volume table is printed for each CV<br/>group. CV groups may be used to check the fluid volumes for primary<br/>system, secondary system, etc. Additionally, RK/RT Packages may use<br/>a CV group to define primary system (IDSORK, record 748000).<br/>Acceptable range:  $1 \leq \text{KGRPCV} \leq 20$ <br/>Default value: 1
- W-2 (I):NAVTCVNumber of data points in the altitude-volume table, printed for each CV<br/>group at the end of input processing.<br/>Acceptable range:  $10 \le \text{NAVTCV} \le 100$ <br/>Default value: 50

### 2.1.4 Records: 101XXX, Control Volume Groups- Individual Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (I):IGRPCVCV group number. CV groups are introduced for editing; at the end of<br/>input processing an altitude-volume table is printed for each CV group.<br/>CV groups may be used to check the fluid volumes for primary system,<br/>secondary system, etc. Additionally, RK/RT Packages may use a CV<br/>group to define primary system (IDSORK, record 748000).<br/>Acceptable range:  $1 \leq IGRPCV \leq 20$ <br/>Default value:KGRPCV (defined in record 101000)

### 2.1.5 Records: 102XXX, Multiplicity of the Control Volume

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (R):XMLTCVMultiplicity of the Control Volume. This is the number of Control<br/>Volumes that are identical to the Control Volume XXX. If the number<br/>is not equal to 1.0, then the segment flow areas, the average flow areas,<br/>the segment volumes, and total volume of this Control Volume, entered<br/>in the input deck, are multiplied by this number.<br/>
Acceptable range:  $0.0 < XMLTCV < 10^{10}$ <br/>
Default value: 1.0

### 2.1.6 Records: 105XXX, Control Volume Name

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

 W-1 (A) NAMECV User defined name, length up to 50 characters. The name is read as a 50-character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.
 Acceptable range: any string of up to 50 characters. Default value: 50 "underline" characters: "\_".

### 2.1.7 Records: 11YXXX, Control Volume Segment Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version). Y is the option indicator, equal to 0, 5, 6, or 7. Any CV may be divided in vertical direction into a number of segments, each with a constant horizontal cross section area. The number of segments for volume XXX is equal to the number of records with this number. The total number of segments (NSEGCV) for a Control Volume may not exceed 10. Use of multiple segments with different cross section areas should be avoided in volumes that may contain bubbles or droplets (see Volume 3 and section 2.1.19, de-entrainment calculation option).

W-1 (R) :	HSEGCV(I)Height of the segment I, (m)			if $Y = 0$ or 5
	ZSEGCV(I	ZSEGCV(I) Top elevation of the segment I, (m)		
		If both height and	top elevation are entered, they mu	st be consistent:
		ZSEGCV(I) = ZSE	EGCV(I-1) + HSEGCV(I)	
		Acceptable range:	0.0 < HSEGCV(I) <	10 <sup>10</sup>
			ZSEGCV(I-1) < ZSEGCV(I) <	10 <sup>10</sup>
		Default value:	none.	
W-2 (R) :	ASEGCV(1	DHorizontal cross se	ection area of the segment I, $(m^2)$	if Y=0 or 6
	VSEGCV(I	VSEGCV(I)Volume of the segment I. $(m^3)$		
	~	If both volume and	l area are entered, they must be co	nsistent:
		VSEGCV(I) = AS	$EGCV(I) \times ZSEGCV(I)$	
		Acceptable range:	$0.0 < ASEGCV(I) < 10^{10}$ ,	
		1 0	$0.0 < VSEGCV(I) < 10^{90}$	
		Default value:	none.	
W-3 (I) :	Ι	Segment number. are read sequentia containing the first number of segmen <i>Acceptable range:</i>	If no value, or zero is entered, the ally - the first record in the input t (lower) segment data (I=1), then ts is denoted in the program as NS I = 1, 2,, 10	In the segment data at is interpreted as $I=2$ , etc. The total SEGCV.
		Default value:	none	

Summarizing, there are four optional inputs in this record:

•	110XXX	Height (m)	Horizontal area (m <sup>2</sup> )
•	115XXX	Height (m)	Volume (m <sup>3</sup> )
•	116XXX	Top elevation (m)	Horizontal area (m <sup>2</sup> )
•	117XXX	Top elevation (m)	Volume (m <sup>3</sup> )

Note that the last option corresponds to the MELCOR input of altitude/volume (with a negative volume entry, which in MELCOR signifies the segment volume rather than the cumulative volume). The total volume, VOLTCV, and total height, HEIGCV, of CV are calculated from:

$$VOLTCV = \sum_{j=1}^{N_{SEG}} HSEGCV_{j} \cdot ASEGCV_{j}$$
$$HEIGCV = \sum_{j=1}^{N_{SEG}} HSEGCV_{j}$$

### 2.1.8 Records: 111XXX, Control Volume Geometry Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (R) :	ELVBCV	Elevation of bottom of Control Volume, (m). ELVBCV gives the difference between the bottom of CV and a reference elevation. The choice of the reference elevation is arbitrary, but all CV must use the same reference elevation. <i>Acceptable range:</i> any real number. <i>Default value:</i> 0.0.
W-2 (R) :	AHORCV	Representative horizontal flow area of Control Volume, (m <sup>2</sup> ). Used to calculate vertical velocities. <b>It is recommended to use the flow area for the main flow direction for both AHORCV and AVERCV</b> (below) - see Volume 3, test runs for pipes with different inclinations. <i>Acceptable range:</i> >0, >max. area of all connected JN, if ICVAJN=1 <i>Default value:</i> Maximum value of the horizontal cross sections of the segments, ASEGCV
W-3 (R) :	AVERCV	Representative vertical flow area of Control Volume, (m²). Used to calculate horizontal velocities. It is recommended to use the flow area for the main flow direction for both AVERCV and AHORCV (above) - see Volume 3, test runs for pipes with different inclinations Acceptable range: >0, >max. area of all connected JN, if ICVAJN=1 Default value:Default value:>0, >max. area of the horizontal cross sections of the segments, ASEGCV
W-4 (R) :	DIPSCV	Characteristic dimension for pool surface interphase heat and mass transfer calculations. If a positive value is entered then the characteristic

dimension will always be equal to DIPSCV. If a negative value is

entered then the characteristic dimension will be proportional to the square root of the current pool surface area:

$$D_{pool} = /DIPSCV / \sqrt{A_{pool} / ASEGCV_1}$$

where  $A_{pool}$  is the pool surface area at given time and ASEGCV<sub>1</sub> is the horizontal cross section area at the bottom of CV. In such case the absolute value of the DIPSCV should correspond to the characteristic dimension for the bottom segment. If the pool level increases to higher segments, then the characteristic dimension will be scaled by the square root of the ratio of the current segment area and the bottom segment area. If zero or no value is entered the characteristic dimension will always be equal to the square root of the current pool surface area.

$$D_{pool} = \sqrt{A_{pool}}$$

Acceptable range:all reals .Default value:0.0 .

W-5 (R) :DHYDCVHydraulic diameter for CV, (m).<br/>Acceptable range:<br/>Default value:DHYDCV < 1000.0.<br/>minimum of the smallest  $D_{hyd}$  of connected JN and<br/> $(4A/\pi)^{1/2}$ , where A is the minimum of AHORCV and<br/>AVERCV.

### 2.1.9 Records: 120XXX, Control Volume Initial Conditions

Pressure of atmosp Acceptable range: Default value:	where gas in Control Volume, ( $1.0 \le PRESCV(IATMS) \le 2$ none.	(Pa). 2.09×10 <sup>7</sup> Pa.
Average temperatu Acceptable range: Default value:	the of atmosphere gas in Contract 273.2 $\leq$ TEMPCV(IATMS) saturation temperature at $T_{sat}$ (PRESCV(IATMS)).	rol Volume, (K). ≤ 3067.0 K . the total pressure,
Elevation of pool s depending on ILE 168XXX) the initi entered.	urface above bottom of CV, (n VCV. For homogeneous CV al void fraction times the vo	n) or relative pool level, / (see records 168000, lume height should be
Acceptable range:	$0.0 \le \text{ZPLSCV} \le \text{volume he}$	ight if ILEVCV=0
	$0.0 \le \text{ZPLSCV} \le 1.0$	if ILEVCV=1
Default value:	none.	
	<ul> <li>Pressure of atmosp Acceptable range: Default value:</li> <li>Average temperatu Acceptable range: Default value:</li> <li>Elevation of pool s depending on ILE 168XXX) the initia entered. Acceptable range: Default value:</li> </ul>	Pressure of atmosphere gas in Control Volume, of Acceptable range: $1.0 \leq PRESCV(IATMS) \leq 2$ Default value: none.//Average temperature of atmosphere gas in Contr Acceptable range: $273.2 \leq TEMPCV(IATMS)$ Default value: saturation temperature at $T_{sat}(PRESCV(IATMS))$ .Elevation of pool surface above bottom of CV, (r depending on ILEVCV. For homogeneous CV $168XXX$ ) the initial void fraction times the volentered. Acceptable range: $0.0 \leq ZPLSCV \leq volume$ he $0.0 \leq ZPLSCV \leq 1.0$ Default value: none.

W-4 (R):TEMPCV<br/>(IPOOL)Average temperature of liquid in Control Volume, (K).<br/>(IPOOL)(IPOOL)Acceptable range: $273.2 \le \text{TEMPCV(IPOOL)} \le \le T_{sat}(\text{PRESCV(IATMS}))$ .<br/>Default value:Default value:saturation temperature at the total pressure,<br/> $T_{sat}(\text{PRESCV(IATMS}))$ .

### 2.1.10 Records: 121XXX, Initial Composition of Atmosphere Gas

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version). The gas composition in the CV atmosphere is defined in those records. Several records with the same number may be entered. Each record may define several components of the gas mixture. The total number of entries in this record must be a multiple of 2.

W-1 (I) :	IGAS	Gas number, (-). Must be one of the available gases. The built-in gases are: $1 = H_2$ , $2 = He$ , $3 = steam$ , $4 = N_2$ , $5 = O_2$ , $6 = CO_2$ . Acceptable range: $1 \le IGAS \le NGASCV \le NGMXFL = 20$ Default value: none.
W-2 (R) :	CVAGCV (IGAS)	If IGAS $\neq$ 3 then this word gives the mole fraction of gas IGAS related to the total mass of noncondensable gases. If the sum of CVAGCV for all noncondensables is not equal to one then CVAGCV will be normalized during input processing. If IGAS = 3 then this word is interpreted as the relative humidity, RHUMCV. <i>Acceptable range:</i> 0.0 $\leq$ CVAGCV(IGAS) $\leq$ 1.0. <i>Default value:</i> 0.0.

### 2.1.11 Records: 122XXX, Initial Data for Atmosphere Droplets

W-1 (R) :	VOLFCV (IDROP)	Volumetric fraction droplets divided by Acceptable range: Default value:	a of droplets in the atmosphere, (-), (volume of the volume of atmosphere gas and droplets). $0.0 \le \text{VOLFCV(IDROP)} \le 0.5$ . 0.0.
W-2 (R) :	TEMPCV (IDROP)	Temperature of dro <i>Acceptable range:</i>	plets in the atmosphere of Control Volume, (K). $273.2 \leq \text{TEMPCV(IDROP)} \leq \leq T_{sat}(\text{PRESCV(IATMS})).$
		Default value:	atmosphere gas temperature TEMPCV(IATMS).
W-3 (R) :	DDRPCV	Diameter of the ave (m).	erage droplet in the atmosphere of Control Volume,
		Acceptable range:	$0.0 \leq \text{DDRPCV} \leq 1.0$ .

		Default value:	DDWFCV (defined in record 158XXX, see section 2.1.31).
W-4 (R) :	ZDRPCV	Position of the aver the top of Control	rage droplet in the atmosphere of CV, (m) (related to Volume).
		Acceptable range:	if there are no droplets in the atmosphere (that means: VOLFCV(IDROP)=0.0) then ZDRPCV must be equal to: ZDRPCV = $H_{CV,tot}$ - ZPLSCV. if there are droplets in the atmosphere (that means: VOLFCV(IDROP) > 0.0) then:
		Default value:	$0.0 < ZDRPCV < H_{CV,tot}$ - ZPLSCV. if there are no droplets in the atmosphere (that means: VOLFCV(IDROP) = 0.0) then the default value of ZDPCV is be equal to: $H_{CV,tot}$ - ZPLSCV. if there are droplets in the atmosphere (that means:
			VOLFCV(IDROP) > 0.0) then the default value of ZDRPCV is: ( $H_{CV,tot}$ - ZPLSCV)·ZDWFCV (defined in record 158XXX, see section 2.1.31).

### 2.1.12 Records: 123XXX, Initial Data for Pool Bubbles

W-1 (R) :	VOLFCV (IBUBB)	Volumetric fraction divided by the volu <i>Acceptable range:</i> <i>Default value:</i>	th of bubbles in the pool, (-), ( volume of bubbles time of water and bubbles in the pool). $0.0 \le \text{VOLFCV(IBUBB)} \le 0.9$ . 0.0.
W-2 (R) :	TEMPCV (IBUBB)	Temperature of bul Acceptable range: Default value:	bbles in the pool of Control Volume, (K). 273.2 ≤ TEMPCV(IBUBB) ≤ 3067.0 K . pool liquid temperature TEMPCV(IPOOL).
W-3 (R) :	DBUBCV	Diameter of the ave Acceptable range: Default value:	erage bubble in the pool of Control Volume, (m). $0.0 \le \text{DBUBCV} \le 1.0$ . DBWFCV (defined in record 158XXX, see section 2.1.31)
W-4 (R) :	ZBUBCV	Position of the ave bottom of Control Acceptable range:	erage bubble in the pool of CV, (m) (related to the Volume). if there are no bubbles in the pool (that means: VOLFCV(IBUBB) = 0.0) then ZBUBCV must be equal to: ZBUBCV = ZPLSCV.

	if there are bubbles in the pool (that means:
	VOLFCV(IBUBB) > 0.0) then:
	0.0 < ZBUBCV < ZPLSCV.
Default value:	if there are no bubbles in the pool (that means:
-	VOLFCV(IBUBB) = 0.0) then the default value of
	ZBUBCV is be equal to:
	ZPLSCV,
	if there are bubbles in the pool (that means:
	VOLFCV(IBUBB) > 0.0) then the default value of
	ZBUBCV is:
	ZPLSCV·ZDWFCV (defined in record 158XXX,
	see section 2.1.31).

### 2.1.13 Records: 124XXX, Initial Composition of Bubble Gas

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version). Those records define the gas composition of the pool bubbles. Several records with the same number may be entered. Each record may define several components of the gas mixture. The total number of entries in this record must be a multiple of 2.

W-1 (I) :	IGAS	Gas number, (-). Must be one of the available gases. The built-in gases are: $1 = H_2$ , $2 = He$ , $3 = steam$ , $4 = N_2$ , $5 = O_2$ , $6 = CO_2$ . <i>Acceptable range:</i> $1 \le IGAS \le NGASCV \le NGMXFL = 20$ <i>Default value:</i> none.	
W-2 (R) :	CVPGCV (IGAS)	If IGAS $\neq$ 3 then this word gives the mole fraction of gas IGAS related to the total mass of noncondensables. If the sum of CVPGCV for all noncondensables is not equal to one then CVPGCV will be normalized during input processing. If IGAS = 3 then this word is interpreted as the relative humidity, RHUMCV. <i>Acceptable range:</i> 0.0 $\leq$ CVPGCV(IGAS) $\leq$ 1.0. <i>Default value:</i> 1.0 for IGAS = 3; 0.0 otherwise.	

#### 2.1.14 Records: 125XXX, Time-Dependent Parameter Definition for Inactive CV

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record defines time dependent parameters (such as pressure, temperature, etc.) for inactive Control Volumes (see records 100XXX, section 2.1.1). If the record 125XXX is not used, then the parameters in the inactive Control Volume will be constant, and equal to their initial values (for example, the initial pressure and temperature are defined in records 120XXX, section 2.1.9). Using Record 125XXX the user may define some, or all of these parameters as functions of time.

Note that if non-zero values are specified in this record and the type of volume is not set as inactive in the record 100XXX, then the type of volume is automatically set to inactive, ITYPCV = 1 (see record 100XXX, section 2.1.2).

W-1 (I): IZPLCV Pointer to a Tabular or Control Function that defines the water level in this volume, (-). If the number is positive, then the water level will be defined by a Tabular Function with the reference number: IZPLCV. If the number is negative, then the water level will be defined by a Control Function with the reference number: IZPLCV |. At any given time of the transient the water level will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 0.99 times the CV height it will be set to 0.99 times the CV height. If no value is entered, or the entered value is equal to zero, the water level will be constant and equal to the value entered in record 120XXX. *Acceptable range:* must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

W-2 (I): IPRSCV Pointer to a Tabular or Control Function that defines the pressure in this volume, (-). If the number is positive, then the pressure will be defined by a Tabular Function with the reference number: IPRSCV. If the number is negative, then the pressure will be defined by a Control Function with the reference number: |IPRSCV|. At any given time of the transient the pressure will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 1.0 Pa, it will be set to 1.0 Pa. If it is larger than  $2.09 \times 10^7$  Pa it will be set to  $2.09 \times 10^7$  Pa. If no value is entered, or the entered value is equal to zero, the pressure will be constant and equal to the value entered in record 120XXX.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

W-3 (I): **ITATCV** Pointer to a Tabular or Control Function that defines the atmosphere temperature in this volume, (-). If the number is 1000, the temperature will be set to the saturation temperature at the CV pressure. If the number is smaller than 1000 and positive, then the atmosphere temperature will be defined by a Tabular Function with the reference number: ITATCV. If the number is negative, then the atmosphere temperature will be defined by a Control Function with the reference number: | ITATCV |. At any given time of the transient the atmosphere temperature will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 273.2 K, it will be set to 273.2 K. If it is larger than 3067.0 K it will be set to 3067.0 K. If no value is entered, or the entered value is equal to zero, the atmosphere temperature will be constant and equal to the value entered in record 120XXX.

Acceptable range: 0, or 1000, or a valid reference number of a Tabular, or a Control Function.

*Default value:* 0.

W-4(I): **ITPLCV** Pointer to a Tabular or Control Function that defines the pool temperature in this volume, (-).If the number is 1000, the temperature will be set to the saturation temperature at the CV pressure. If the number is smaller than 1000 and positive, then the pool temperature will be defined by a Tabular Function with the reference number: ITPLCV. If the number is negative, then the pool temperature will be defined by a Control Function with the reference number: | ITPLCV |. At any given time of the transient the pool temperature will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 273.2 K, it will be set to 273.2 K. If it is larger than the saturation temperature at the current pressure, then it will be set to the saturation temperature. If no value is entered, or the entered value is equal to zero, the atmosphere temperature will be constant and equal to the value entered in record 120XXX. Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value:

W-5 (I): IATGCV Pointer to a Tabular or Control Function that defines the volume

0

fraction of  $H_2$  in this volume, (-). If the number is positive, then the  $H_2$ 

(1)

fraction will be defined by a Tabular Function with the reference number: IATGCV(1). If the number is negative, then the  $H_2$  fraction will be defined by a Control Function with the reference number: |IATGCV(1)|. At any given time of the transient the H<sub>2</sub> fraction will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, the H<sub>2</sub> fraction will be constant and equal to the value entered in record 121XXX. The gas fractions are internally normalized, to make sure that the sum is equal to one at any moment of time.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value: 0

W-6(I): IATGCV Pointer to a Tabular or Control Function that defines the volume fraction of He in this volume, (-). If the number is positive, then the He (2)fraction will be defined by a Tabular Function with the reference number: IATGCV(2). If the number is negative, then the He fraction will be defined by a Control Function with the reference number: |IATGCV(2)|. At any given time of the transient the He fraction will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, the He fraction will be constant and equal to the value entered in record 121XXX. The gas fractions are internally normalized, to make sure that the sum is equal to one at any moment of time.

> Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

W-7 (I): IATGCV Pointer to a Tabular or Control Function that defines the relative humidity, (-). If the number is positive, then the relative humidity will (3) be defined by a Tabular Function with the reference number: IATGCV(3). If the number is negative, then the relative humidity will be defined by a Control Function with the reference number: IATGCV(3). At any given time of the transient the relative humidity will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, the relative humidity will be constant and equal to the value entered in record 121XXX. Acceptable range: must be a valid reference number of a Tabular, or a Control Function. if non-zero. Default value: 0 W-8 (I): IATGCV Pointer to a Tabular or Control Function that defines the volume

(4) fraction of  $N_2$  in this volume, (-). If the number is positive, then the  $N_2$  fraction will be defined by a Tabular Function with the reference number: IATGCV(4). If the number is negative, then the  $N_2$  fraction will be defined by a Control Function with the reference number: |IATGCV(4)|. At any given time of the transient the  $N_2$  fraction will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, the  $N_2$  fraction will be constant and equal to the value entered in record 121XXX. The gas fractions are internally normalized, to make sure that the sum is equal to one at any moment of time.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

Pointer to a Tabular or Control Function that defines the volume W-9(I): IATGCV (5) fraction of O<sub>2</sub> in this volume, (-). If the number is positive, then the O<sub>2</sub> fraction will be defined by a Tabular Function with the reference number: IATGCV(5). If the number is negative, then the  $O_2$  fraction will be defined by a Control Function with the reference number: |IATGCV(5)|. At any given time of the transient the O<sub>2</sub> fraction will be equal to the current value of the Tabular or Control Function. If the current value of the Tabular or Control Function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, the O<sub>2</sub> fraction will be constant and equal to the value entered in record 121XXX. The gas fractions are internally normalized, to make sure that the sum is equal to one at any moment of time.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

W-10 (I) :	IATGCV	Pointer to a Tabular or Control Function that defines the volume		
	(6)	fraction of CO <sub>2</sub> in this volume, (-	). If the number is positive, then the	
		$CO_2$ fraction will be defined by a	Tabular Function with the reference	
		number: IATGCV(6). If the numb	per is negative, then the CO <sub>2</sub> fraction	
		will be defined by a Control F	unction with the reference number:	
		IATGCV(6)  . At any given time	e of the transient the CO <sub>2</sub> fraction will	
		be equal to the current value of th	e Tabular or Control Function. If the	
		current value of the Tabular or Co	ontrol Function is smaller than 0.0, it	
		will be set to 0.0. If it is larger than	1.0 it will be set to 1.0. If no value is	
		entered, or the entered value is ec	ual to zero, the $CO_2$ fraction will be	
		constant and equal to the value of	entered in record 121XXX. The gas	
		fractions are internally normalized	, to make sure that the sum is equal to	
		Accortable range: must be a vali	d reference number of a Tabular, or a	
		Control Funct	ion if non zero	
		Default value: 0	ion, il non-zelo.	
		Default value. 0.		
W-11 (I) :	INITCV	Initial conditions in the inactive vo	olume:	
		=1: use the initial conditions as de	fined in the input file or the *.ICF.	
		=2: use the initial values read from	the tables defined above.	
		Acceptable range: 1.2		
		Default value: 2		
		0		

### 2.1.15 Records: 13YXXX, Control Volume Mass Source Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

Mass sources (sinks) are defined by those records. Y is the source number (consecutive, starting with 1). Up to 9 sources are allowed for one Control Volume. The mass source is defined here for a single CV; i.e. the value obtained from TF/CF defined below is multiplied by the CV multiplicity (XMLTCV, record 102XXX).

W-1 (R) : ZMSCV		Midpoint elevation for the source No. Y, relative to the bottom of Control Volume, (m).		
		Acceptable range:	ZMSCV must be greater or equal to zero and smaller or equal to the height of CV.	
		Default value:	none.	
W-2 (R) :	AMSCV	Flow area, (m <sup>2</sup> ). Acceptable range: Default value:	$0.0 < AMSCV < 10^{10}$ . none.	
W-3 (R) :	DMSCV	Diameter, (m). Acceptable range: Default value:	$0.0 < AMSCV < 10^{10}$ . $(4 \cdot AMSCV/\pi)^{1/2}$ .	
W-4 (I) :	IMMSCV	Pointer to a Tabula rate (kg/s).	ar or Control Function that defines the mass source	

IMMSCV > 0: mass source rate is defined by a Tabular Function with the reference number: IMMSCV.

IMMSCV < 0: mass source rate is defined by a Control Function with the reference number: IMMSCV.

IMMSCV = 0: mass source rate is zero (source is inactive).

IMMSCV >1000: mass source rate is linked to the isotope list number YY, where YY=IMMSCV-1000. The isotope list YY is defined in the records 8970XX. Usually isotopes are treated as trace species; the isotope mass is not considered in the CV Package. Using this option, the user may link the RT isotope masses to the CV gas masses for the cases when the effect of gas pressurization is considered non-negligible. An example is shown at the description of the record 8970XX. If this option is used, the following mass source is created:

$$S = \left( \Sigma M_{i,0} - M_{gas,0} \right) / \Delta t$$

Here:

 $M_{i,0}$  mass of isotope *i* in the CV number XXX, start of time step, (kg)  $M_{gas,0}$  mass of gas in the CV number XXX, start of time step, (kg) time step (s)  $\Delta t$ 

Because of the applied formulation, the mass of gas in the CV will be lagging by one time step compared to the mass in the RT Package. This is typically not a problem, since the isotope masses are very small a significant accumulation can only be observed for longer time frames. Since this source is intended as a gas source, it is required that the source elevation must be equal to the CV height, ZMSCV = HEIGCV.

An internal limit is imposed on the value obtained from the Tabular or Control Function. If the absolute value is smaller than  $10^{-20}$  (kg/s), then it is set to 0.0.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, or existing list, if non-zero. *Default value:* 0.

**ITMSCV** Pointer to a Tabular or Control Function that defines the temperature of the source (K).

> ITMSCV > 0: temperature is defined by a Tabular Function with the reference number: ITMSCV.

> ITMSCV < 0: temperature is defined by a Control Function with the reference number: | ITMSCV |.

ITMSCV = 0: temperature is equal to the current CV gas temperature.

W-5 (I):
		The value obtainer restricted to the rar (mass sink), then the current temperature	ed from the Tabular or Control Function will be nge of: 273.2 - 3067 K. When the source is negative he source temperature and pressure are equal to the e and pressure of the fluid being removed.
		Acceptable range: Default value:	must be a valid reference number of a Tabular, or a Control Function, if non-zero. 0.
W-6 (I) :	IPMSCV	Pointer to a Tabula source (Pa).	r or Control Function that defines the pressure of the
		IPMSCV > 0: pre reference number:	essure is defined by a Tabular Function with the IPMSCV.
		IPMSCV < 0: preference number:	essure is defined by a Control Function with the  IPMSCV .
		IPMSCV = 0: press steam mass source 0.99×saturation pre	sure is equal to the current CV pressure. If this is the e, i.e., $CGMSCV(3)>0.0$ , then pressure is equal to essure at the CV gas temperature.
		The units obtained be (Pa). The value be restricted to the negative (mass sink to the current temp	from the Tabular or Control Function are assumed to obtained from the Tabular or Control Function will e range of: $1.0 - 2.09 \times 10^7$ Pa. When the source is k), then the source temperature and pressure are equal erature and pressure of the fluid being removed.
		Acceptable range:	must be a valid reference number of a Tabular, or a Control Function, if non-zero.
		Dejauti vatue:	υ.

The following data pairs define the composition (mass fractions) of the source. The mass fractions are assumed constant (time independent).

W-7 (I) :	Ι	Id. number of the first component in the mixture (-). Zero means liquid water, positive number indicates one of the available gases. The built-in gases are: 0=liquid, 1=H <sub>2</sub> , 2=He, 3=steam, 4=N <sub>2</sub> , 5=O <sub>2</sub> , 6=CO <sub>2</sub> . Acceptable range: $0 \le I \le NGASCV \le NGMXFL = 20$ Default value: none.
W-8 (R) :	CGMSCV/ /CLMSCV	Mass fraction of the first component. If Id. number is 0 (water) then this is CLMSCV - the mass flow of water divided by the total mass flow of gas and water. If Id. number is greater than zero then this is CGMSCV - the mass flow of gas I divided by the total gas flow (gas fractions). <i>Acceptable range:</i> $0.0 \le CGMSCV/CLMSCV \le 1.0$ . <i>Default value:</i> $1.0$ for I=3 (steam), 0.0 otherwise.
W-9 (I) :	Ι	Id. number of second component in the mixture, (-). Acceptable range: $0 \le I \le NGASCV \le NGMXFL = 20$

*Default value:* none.

... etc.

#### 2.1.16 Records: 130XXX, Optional Mass Source Strength Multipliers

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (R) :	XMMSCV(1)	Source strength multiplier on the tabular mass source 1 (defined				
	in re	cord 131XXX). If a non-zero value is entered, then the mass source				
	strer	strength is multiplied by this number.				
	Acce	<i>eptable range:</i> $-10^{10} \le \text{XMMSCV}(1) \le +10^{10}$				
	Defc	ult value: 0.0				
W-2 (R) :	XMMSCV(2)	Source strength multiplier on the tabular mass source 2 (defined				
	in re	cord 132XXX). If a non-zero value is entered, then the mass source				
	strer	ight is multiplied by this number.				
	Acce	eptable range: $-10^{10} \le \text{XMMSCV}(2) \le +10^{10}$				

Default value: 0.0

... etc.

The source strength multipliers are introduced to have an easy way of defining chemical reactions, for example hydrogen recombiners. The user must define only one function, e.g. defining the hydrogen recombination rate. Then the mass sink of oxygen is obtained by multiplying this function by a constant factor of -8.0, the mass source of steam is obtained by multiplying this function by +9.0, and the energy source is obtained by multiplying this function by  $H_2$  reacted.

## 2.1.17 Records: 14YXXX, Control Volume Energy Source Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

Y is the energy source number (consecutive, starting with 1). Up to 9 energy sources are allowed for one Control Volume. The energy source is defined here for a single CV; i.e. the value obtained from TF/CF defined below is multiplied by the CV multiplicity (XMLTCV, record 102XXX).

W-1 (R) :	ZTESCV	Midpoint elevation for the energy source number Y, relative to the bottom of Control Volume, (m).Acceptable range:ZTESCV must be greater or equal to zero and smaller or equal to height of CV.Default value:none.
W-2 (I) :	ITESCV	Pointer to a Tabular or Control Function that defines the energy rate for the source number Y. If the number is positive, then the mass flux will be defined by a Tabular Function with the reference number: ITESCV. If the number is negative, then the energy rate will be defined by a Control Function with the reference number: $ TESCV $ . The units obtained from the Tabular or Control Function are assumed to be (W). Positive and negative values are allowed. Negative values will yield energy sink. If ITESCV points to a Reactor Kinetics Control Function (IGRPCF=3, INUMCF=5) and circulating fuel option is used (IFTORK=2), then: • The source is placed only in the pool of CV. • The value obtained from the reactor kinetics Control Function is used if the CV has sufficient amount of liquid, i.e. if the liquid fraction in CV is more than the limit XFULRK (record 748000). • If the pool occupies less than XFULRK of the CV volume, the source obtained from the reactor kinetics Control Function, is interpolated to obtain zero in case of empty volume, i.e. it is multiplied by ( $V_{pool}/V_{CV}$ )/XFULRK. Here $V_{pool}$ is the pool volume in CV and $V_{CV}$ is the total CV volume. This is done to automatically reduce the power generated in the pool of a CV when the pool is removed from this CV. <i>Acceptable range:</i> must be a valid reference number of a Tabular, or a Control Function, if non-zero.
W-3 (R) :	POWMCV	Constant power multiplier. The constant power multiplier is introduced to have an easy way of defining for example axial power profile. Acceptable range: $-10^{10} \le \text{POWMCV} \le 10^{10}$ Default value: 1.0

#### 2.1.18 Records: 150000, Liquid De-entrainment, Bubble De-entrainment

Using this record one may specify the parameters described in record 150XXX for all Control Volumes in the model - see description of record 150XXX below.

#### 2.1.19 Records: 150XXX, Liquid De-entrainment, Bubble De-entrainment

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R): DENHCV De-entrainment ratio for liquid (droplets) in the atmosphere due to horizontal velocity,  $D_h$ , (-). The mass change of discontinuous component (liquid droplets) in the atmosphere of a Control Volume is calculated as (see Volume 1):

$$\frac{dM_{drop}}{dt}\Big|_{h,de-ent} = D_h A_h \alpha_{drop} v_{h,drop} \rho_{drop}$$

$D_h A_h$	-	de-entrainment ratio for horizontal flow, DENHCV, atmosphere, area for flow in horizontal direction (m <sup>2</sup> )
11/1		(atmosphere vertical cross section area),
$\alpha_{drop}$	-	droplet volumetric fraction, (-),
Vh,drop	-	droplet horizontal velocity, (m/s),
$ ho_{drop}$	-	droplet density, $(kg/m^3)$ .

The value of DENTCV may be useful for example in case of spray system injecting at some angle to the vertical. Some part of the spray droplets will hit the containment walls. In that case however it is needed to modify the drop flow model parameters (section 2.1.20) to properly model the horizontal velocity component of the spray droplets (see Volume 3, simulation of NUPEC tests).

The general idea of entering the value of DENTCV is illustrated in Figure 2-1. Figure 2-1 shows a Control Volume with the cross section area for atmosphere horizontal flow equal to  $A_{h,A}$ , and a Junction with a flow area of  $A_{JN}$ . Assuming that droplet inertia is large the deentrainment parameter can be estimated as:

$$D_h = \frac{A_{h,A} - A_{JN}}{A_{h,A}}$$

In practice the droplets will change they flow direction together with the gas stream (finite inertia) or bounce back after hitting the wall. This means that the de-entrainment will be somewhat smaller than defined by

the above formula. Moreover the atmosphere cross-section area depends on the pool level and thus changes in time. Consequently it is not always easy to find the right value for the de-entrainment parameter. *Acceptable range:*  $0.0 \le \text{DENHCV} < 1.0$ . *Default value:* 0.0.



Figure 2-1 Horizontal droplet de-entrainment.

W-2 (R): DENVCV De-entrainment ratio for liquid (droplets) in the atmosphere due to vertical velocity,  $D_{\nu}$ , (-). The mass change of discontinuous component (liquid droplets) in the atmosphere of a Control Volume is calculated as (see Volume 1):

$$\frac{dM_{drop}}{dt}|_{v,de-ent} = D_v A_v \alpha_{drop} v_{v,drop} \rho_{drop}$$

		$D_{\nu}$ - de-entrainment ratio for vertical flow, DENVCV, $A_{\nu}$ - either actual pool surface area, or CV segment horizontal cross section area, depending on ISVDCV (Word 3, below), (m <sup>2</sup> ),
		$\alpha_{drop}$ - droplet volumetric fraction at pool surface elevation,
		$v_{v,drop}$ - droplet vertical velocity, (m/s),
		$\rho_{drop}$ - droplet density, (kg/m <sup>3</sup> ).
		Acceptable range: $0.0 \leq \text{DENVCV} < 1.0$ .
		<i>Default value:</i> 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0).
W-3 (I) :	ISVDCV	Indicator for droplet vertical de-entrainment area calculation, $A_{\nu}$ . ISVDCV = 0 :
		$A_{\rm v}$ is always equal to the current pool surface area - Figure 2-2 left
		$1 \leq \text{ISVDCV} \leq \text{NSEGCV}$ :
		$A_{\nu}$ is equal to horizontal area of segment ISVDCV - Figure 2-2 right
		Acceptable range: $0 \leq ISVDCV \leq NSEGCV$ .
		Default value: 0.



Figure 2-2 Use of ISVDCV, ISVBCV to define droplet and bubble vertical de-entrainment.

W-4 (I):

**ISVBCV** 

Indicator for bubble vertical de-entrainment area calculation,  $A_{\nu}$ . ISVBCV = 0 :

 $A_v$  is always equal to the current pool surface area - Figure 2-2 left

 $1 \leq ISVBCV \leq NSEGCV$ :

 $A_v$  is equal to horizontal area of segment ISVBCV - Figure 2-2 right

#### ISVBCV > NSEGCV :

ISVBCV defines a limit, in %, in the relative pool level, above which bubbles are not transported to the pool surface. For example, if ISVBCV=90, then when liquid level is above 90% of the CV height there is no transport of bubbles to the pool surface ( $A_v = 0.0$ ) A transition zone of 0.1×ISVBCV is defined, where  $A_v$  is interpolated between 0.0 and the full value. In the considered example, the full area will be for liquid levels  $\leq 0.9$ ×ISVBCV = 0.81.

This option may be useful for vertical pipes nodalized with multiple CVs. In such case use of a homogeneous CV is more appropriate - (record 168XXX, Figure 2-5). Use of heterogeneous CV leads to undesired multiple liquid levels in the pipe, with bubbles transported to the pool surface and then as atmosphere in the junction - Figure 2-3 left. Use of the ISVBCV as a cut-off parameter allows the user to define the liquid level in the CV above which there will be no transport of bubbles to the pool surface and thus there will be a flow of pool and bubbles only in all junctions - Figure 2-3 right.

**Note 1**: this option works also for aerosol particles suspended in the pool. If the particle vertical velocity is positive (VINPRT > 0.0 or drag coefficient is used with particle density < pool density), then flow of particles to the pool surface will be eliminated when liquid level is above ISVBCV %.

**Note 2**: This option requires that there is a JN connected at the top of the CV. This JN is associated with ISVBCV and is given a name JSVBJN. *Acceptable range:*  $0 \le ISVBCV \le 100$ 

*Default value:* 0



Figure 2-3 Use of ISVBCV to define vertical pool / bubble flow

#### 2.1.20 Records: 151XXX, Drop Flow Regime Parameters

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record defines data for the drift flux model, which is used for the droplet transport in atmosphere of CV. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R) :	COVACV	Constant $C_0$ for drift flux model for CV atmosphere, vertical velocity (see Volume 1) This is the value denoted in Volume 1 as: $C_{0,VA}$ (-)		
		Acceptable range:	$0.0 \le C0VACV \le 10.0$ . If no value or zero is entered, then $C_{0,vA}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.	
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0	
W-2 (R) :	VIVACV	Terminal velocity, velocity (see Volur (m/s).	$v_{\infty}$ , for drift flux model for CV atmosphere, vertical ne 1). This is the value denoted in Volume 1 as: $v_{\infty,v,A}$ ,	
		Acceptable range:	$-100.0 \le \text{VIVACV} \le 100.0$ . If no value or zero is entered, then $v_{\infty,v,A}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.	

		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-3 (R) :	XVACV	Exponent <i>x</i> for drift Volume 1). This is <i>Acceptable range:</i>	flux model for CV atmosphere, vertical velocity (see the value denoted in Volume 1 as: $x_{v,A}$ , (-). $0.0 \le XVACV \le 10.0$ . If no value or zero is entered, then $x_{v,A}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.
		Default value:	0.0
W-4 (R) :	COHACV	Constant $C_0$ for drift (see Volume 1). The Acceptable range:	ft flux model for CV atmosphere, horizontal velocity is is the value denoted in Volume 1 as: $C_{0,hA}$ , (-). $0.0 \le C0HACV \le 10.0$ . If no value or zero is entered, then $C_{0,hA}$ is calculated by the Drop Flow
			Regime Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0
W-5 (R) :	VIHACV	Terminal velocity, velocity (see Volum (m/s).	$v_{\infty}$ , for drift flux model for CV atmosphere, horizontal ne 1). This is the value denoted in Volume 1 as: $v_{\infty,h,A}$ ,
		Acceptable range:	$-100.0 \le VIHACV \le 100.0$ . If no value or zero is entered, then $v_{\infty,h,A}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-6 (R) :	XHACV	Exponent x for drift (see Volume 1). The Acceptable range:	It flux model for CV atmosphere, horizontal velocity is is the value denoted in Volume 1 as: $x_{h,A}$ , (-). $0.0 \le XHACV \le 10.0$ . If no value or zero is entered, then $x_{h,A}$ is calculated by the Drop Flow regime Model, as described in Volume 1.
		Default value:	0.0

#### 2.1.21 Records: 152XXX, Bubbly and Annular Flow Parameters

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record defines data for the drift flux model, which is used for the bubble transport in pool of CV. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R) :	COVPCV	Constant $C_0$ for d	rift flux model for CV pool, vertical velocity (see
		Volume 1). This is	the value denoted in Volume 1 as: $C_{0,vP}$ , (-).
		Acceptable range:	$0.0 \le COVPCV \le 10.0$ . If no value or zero is entered,
			then $C_{0,v,P}$ is calculated by the Bubbly Flow Regime
			Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0

W-2 (R) :	VIVPCV	Terminal velocity, (see Volume 1). The Acceptable range: Default value:	$v_{\infty}$ , for drift flux model for CV pool, vertical velocity his is the value denoted in Volume 1 as: $v_{\infty,v,P}$ , (m/s). $-100.0 \le \text{VIVPCV} \le 100.0$ . If no value or zero is entered, then $v_{\infty,v,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. $0.0$ , a small value ( $\le 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-3 (R) :	XVPCV	Exponent x for dr Volume 1). This is Acceptable range: Default value:	ift flux model for CV pool, vertical velocity (see the value denoted in Volume 1 as: $x_{v,P}$ , (-). $0.0 \le XVPCV \le 10.0$ . If no value or zero is entered, then $x_{v,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. 0.0
W-4 (R) :	C0HPCV	Constant $C_0$ for dr. Volume 1). This is Acceptable range: Default value:	ift flux model for CV pool, horizontal velocity (see the value denoted in Volume 1 as: $C_{0,hP}$ , (-). $0.0 \le COHPCV \le 10.0$ . If no value or zero is entered, then $C_{0,hP}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. $0.0$ , a small value ( $\le 10^{-50}$ ) value will set $C_0$ to 0.0
W-5 (R) :	VIHPCV	Terminal velocity, velocity (see Volum (m/s). <i>Acceptable range:</i> <i>Default value:</i>	$v_{\infty}$ , for drift flux model for CV pool, horizontal ne 1). This is the value denoted in Volume 1 as: $v_{\infty,h,P}$ , $-100.0 \le \text{VIHPCV} \le 100.0$ . If no value or zero is entered, then $v_{\infty,h,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. 0.0, a small value ( $\le 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-6 (R) :	XHPCV	Exponent x for dri Volume 1). This is Acceptable range: Default value:	ft flux model for CV pool, horizontal velocity (see the value denoted in Volume 1 as: $x_{h,P}$ , (-). $0.0 \le XHPCV \le 10.0$ . If no value or zero is entered, then $x_{h,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. 0.0
W-7 (R) :	IANNCV	Annular flow mode =1: Default mod =2: Dartmouth c Acceptable range: Default value:	el selection. lel, (see Volume 1). correlation, (see Volume 1). 1 or 2. 1.

## 2.1.22 Records: 153XXX, Plume Model for Mass Sources

These records activate plume models for one or more mass sources present in the Control Volume. The plume model may be activated only if stratification is calculated for the Control Volume (record 100XXX, section 2.1.2).

Description of the plume model is given in Volume 1. If stratifications are calculated then the plume model may be activated for any of the mass sources present in the Control Volume. To activate the model for a single source and a single component, a set of three integer numbers, described below, must be entered. To activate the model for several mass sources, several sets of three integer numbers should be entered in this record.

W-1 (I) :	Ι	Number of the mass source for which the plume model is desired. Must be equal to one of the mass sources defined for this Control Volume through records 13YXXX (section 2.1.15). Acceptable range: $1 \le I \le No.$ of sources defined on 13YXXX, <i>Default value:</i> none.
W-2 (I) :	J	Identifier of component, for which the plume model is desired. J=1: atmosphere; J=3: pool. <i>Acceptable range:</i> 1 or 3. <i>Default value:</i> none.
W-3 (I) :	IPLMCV	Plume model activator. If IPLMCV = 0 then the plume model is not active. If IPLMCV $\neq$ 0 then the plume model is active for the mass source I, in the component J of the Control Volume XXX. Note that the plume model is used only when stratification models are active. That means, the plumes may be activated in the atmosphere of the Control Volume only if ITSPCV $\neq$ 0 (section 2.1.2), and in the pool of the Control Volume only if IPSPCV $\neq$ 0 (section 2.1.2). Acceptable range: any integer. Default value: 0.

... etc., until all plumes are defined.

#### 2.1.23 Records: 154XXX, Plume Model for Energy Sources

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

These records activate plume models for one or more energy sources, present in the Control Volume. The plume model may be activated only if stratification is calculated for the Control Volume (record 100XXX, section 2.1.2).

Description of the plume model is given in Volume 1. If stratifications are calculated then the plume model may be activated for any of the energy sources present in the Control Volume. To activate the model for a single source and a single component, a set of three integer numbers, described below, must be entered. To activate the model for several energy sources, several sets of three integer numbers must be entered in this record.

W-1 (I) :	Ι	Number of the energy source for which the plume model is desired. Must be equal to one of the energy sources defined for this Control Volume through records 14YXXX (section 2.1.17). <i>Acceptable range:</i> $1 \le I \le No.$ of sources defined on 14YXXX, <i>Default value:</i> none.
W-2 (I) :	J	Identifier of component, for which the plume model is desired. J=1: atmosphere; J=3: pool. <i>Acceptable range:</i> J=1, or J=3. <i>Default value:</i> none.
W-3 (I) :	IPLECV	Plume model activator. If IPLECV = 0 then the plume model is not active. If IPLECV $\neq$ 0 then the plume model is active for the energy source I, in the component J of the Control Volume XXX. Note that the plume model is used only when stratification models are active. That means, the plumes may be activated in the atmosphere of the Control Volume only if ITSPCV $\neq$ 0 (section 2.1.2), and in the pool of the Control Volume only if IPSPCV $\neq$ 0 (section 2.1.2). <i>Acceptable range:</i> any integer. <i>Default value:</i> 0.

... etc., until all plumes are defined.

#### 2.1.24 Records: 155000, Bubble Collapse Parameters, Droplet and Bubble Activators

Using this record one may specify the parameters described in record 155XXX for all Control Volumes in the model - see description of record 155XXX below.

#### 2.1.25 Records: 155XXX, Bubble Collapse Parameters, Droplet and Bubble Activators

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . <u>NOTE: if XXX = 000, then the</u> parameters defined in this record are applied to all Control Volumes.

This record is optional. All entries from this record have their default values, recommended for general application. Note! Switching off the bubble collapse models can lead to numerical convergence problems. Specifically for boiling surfaces (XBCMCV(2)) the bubble collapse model ought not to be switched off.

W-1 (R) :	XBCMCV	Bubble collapse model at Junctions.		
	(1)	XBCMCV(1) < 0.0: model inactive,		
		XBCMCV(1) $\ge$ 0.0: model active.		
		Acceptable range: all real numbers.		
		<i>Default value:</i> +1, if an alternative fluid is used (see section 2.12),		
		then the default value is $-1$		
$W_{-2}(R)$	XBCMCV	Bubble collapse model at Solid Heat Conductor surfaces (boiling)		
11 - 2(11).		buoble conductor at solid real conductor surfaces (bonning).		
	(2)	XBCMCV(2) < 0.0: model inactive,		

		XBCMCV $(2) \ge 0.0$ Acceptable range: Default value:	<ul> <li>model active.</li> <li>all real numbers.</li> <li>+1, if an alternative fluid is used (see section 2.12), then the default value is -1</li> </ul>
W-3 (R) :	XBCMCV (3)	Bubble collapse mo XBCMCV(3) $< 0.0$ XBCMCV(3) $\ge 0.0$ Acceptable range: Default value:	<ul> <li>del at Tabular Mass Sources.</li> <li>model inactive,</li> <li>model active.</li> <li>all real numbers.</li> <li>+1, if an alternative fluid is used (see section 2.12), then the default value is -1</li> </ul>
W-4 (R)	DTBCCV	Pool subcooling to Conductors and bu Junctions, (K). If the than zero, then the (boiling) surfaces is than 2·DTBCCV the subcooling is smaller not used. Interpolat DTBCCV and 2·D flowing through Jun Acceptable range: Default value:	switch off the bubble collapse model at Solid Heat bble flow or pure steam atmosphere flow through the value of XBCMCV(2) (Word 2 above) is greater bubble collapse model at the Solid Heat Conductor used as follows. When the pool subcooling is larger en the bubble collapse model is used. When the pool er than DTBCCV then the bubble collapse model is tion is performed for the pool subcooling between TBCCV. The same logic applies for the bubbles nctions. DTBCCV > 0.0. It is not recommended to decrease DTBCCV below its default value. 0.5
W-5 (I)	IDRPCV	Droplet model act Tabular Mass Sourd always deposited di liquid is either dep elevation is below suspended in CV at Acceptable range: Default value:	ivator at Junctions, Solid Heat Conductors, and ces. If IDRPCV is equal to 1 then created liquid is rectly in the pool. If IDRPCV is equal to 2 then the posited in the pool (if Junction, SC/TC, or TMS the pool surface) or converted to droplets and mosphere (if elevation is above the pool surface). 1 or 2. 1.
W-6 (I)	IBUBCV	Bubble model acti Tabular Mass Source always deposited di then the gas is either or TMS elevation is suspended in the po <i>Acceptable range:</i> <i>Default value:</i> <i>NOTE: In the earlier</i>	ivator at Junctions, Solid Heat Conductors, and ces. If IBUBCV is equal to 1 then the created gas is irectly in the atmosphere. If IBUBCV is equal to 2 er deposited in the atmosphere (if Junction, SC/TC, above the pool surface) or converted to bubbles and ol (if elevation is below the pool surface). 1 or 2 2 er versions (prior to July 2018) the default value for
		alternative fluids we bubble tracking is n liquid metal reactor	as 1. This may speed up calculations in cases when not important, which may be the case for example in rs.
W-7 (R)	DMBLCV	Maximum depth at surface of Solid Hea bubbles are created	which bubbles are created when boiling occurs at the at Conductors, (m). If DMBLCV is less than 0.0, then at the true elevation of the Solid Heat Conductor

		surface. In reality, very little bubbles i pool surface, where parameter DMBLC number then the bu below the pool surf <i>Acceptable range:</i> <i>Default value:</i>	if the boiling surface is deeply submerged, there is n the deep pool. Bubbles are rapidly created near the e pressure is close to saturation. To simulate this the CV is used. When DMBLCV is set to a positive bbles will be created not deeper than DMBLCV (m) face. DMBLCV $\leq 0$ , or $0.5 \leq$ DMBLCV $\leq 100$ . 5.0.
W-8 (R)	DMNBCV	Maximum depth at boiling, (m). If DM created in the middl then the bubbles w the pool surface. N non-equilibrium bo section 2.1.37). Acceptable range: Default value:	t which bubbles are created during non-equilibrium INBCV is less than or equal to 0.0, then bubbles are le of the pool. If DMNBCV is set to a positive number ill be created not deeper than DMNBCV (m) below ote that DMNBCV is used only when bubbles from illing are activated (MNMTCV $\neq$ 0, record 163XXX, DMNBCV $\leq$ 0, or 0.5 $\leq$ DMNBCV $\leq$ 100 . 2.0.
W-9 (I)	IDDCCV	Calculation of the of Tabular Mass Source IDDCCV = 1: IDDCCV = 2: Acceptable range: Default value:	<ul> <li>diameter of droplets created due to Junction flows or ces.</li> <li>Use only Taylor instability model.</li> <li>Maximum of Kutateladze-Styrikovic and Taylor.</li> <li>1 or 2.</li> <li>1 (Note! Use of the second option may give unrealistic results when only small part of Junction flow area is occupied by liquid).</li> </ul>
W-10 (R)	DDMNCV	Lower limit for dia Tabular Mass Sour Acceptable range: Default value:	ameter of droplets created due to Junction flows or ces. $1.0 \times 10^{-5} \le \text{DDMNCV} \le 1.0 \times 10^{-2}.$ $1.0 \times 10^{-3}.$
W-11 (R)	DDMXCV	Upper limit for dia Tabular Mass Sour Acceptable range: Default value:	timeter of droplets created due to Junction flows or ces. DDMNCV $\leq$ DDMXCV $\leq$ 1.0×10 <sup>-1</sup> . 2.0×10 <sup>-2</sup> .
W-12 (R)	DBMNCV	Lower limit for dia Tabular Mass Sour Acceptable range: Default value:	ameter of bubbles created due to Junction flows or ces. $1.0 \cdot 10^{-4} \le \text{DBMNCV} \le 1.0 \times 10^{-1}.$ $1.0 \times 10^{-3}.$
W-13 (R)	DBMXCV	Upper limit for dia Tabular Mass Sour Acceptable range: Default value:	ameter of bubbles created due to Junction flows or ces. DBMNCV $\leq$ DBMXCV $\leq 1.0 \times 10^{+0}$ . $9.0 \times 10^{-2}$ .

#### 2.1.26 Records: 156000, Velocity Limits to Deactivate Plume Model

Using this record one may specify the parameters described in record 156XXX for all Control Volumes in the model - see description of record 156XXX below.

#### 2.1.27 Records: 156XXX, Velocity Limits to Deactivate Plume Model

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R) :	VPLCCV (iatms)	Velocity to deactivate atmosphere plume model in Junctions, (m/s). Used when Junction flow of atmosphere gas enters the atmosphere of CV, and the atmosphere plume model for this Junction is active (see section 2.2.20). If the atmosphere velocity in the Junction exceeds VPLCCV(iatms), then the atmosphere plume model is deactivated for this Junction. Acceptable range: $0.1 \leq \text{VPLCCV}(\text{iatms}) \leq 1000.0$ Default value: $1.0$ .
W-2 (R) :	VPLCCV (ipool)	Velocity to deactivate pool plume model in Junctions, (m/s). Used when Junction flow of liquid enters the pool of CV, and the pool plume model for this Junction is active (see section 2.2.20). If the pool velocity in the Junction exceeds VPLCCV(ipool), then the pool plume model is deactivated for this Junction. Acceptable range: $0.1 \le VPLCCV(ipool) \le 1000.0$ Default value: $1.0$ .
W-3 (R) :	VPLCCV (ibubb)	Velocity to deactivate pool plume model in Junctions, (m/s). Used when Junction flow of atmosphere gas enters the pool of CV, and the pool plume model for this Junction is active (see section 2.2.20). If the atmosphere velocity multiplied by: $(1 - c_{H2O})$ (where $c_{H2O}$ is the volumetric fraction of steam), in the Junction exceeds VPLCCV(ibubb), then the pool plume model is deactivated for this Junction. <i>Acceptable range:</i> $0.1 \le VPLCCV(ibubb) \le 1000.0$ <i>Default value:</i> $1.0$ .

#### 2.1.28 Records: 157000, CV Velocity Change Limits

Using this record one may specify the parameters described in record 157XXX for all Control Volumes in the model - see description of record 157XXX below.

### 2.1.29 Records: 157XXX, CV Velocity Change Limits

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R) :	DVDTCV (iatms)	Maximum velocity $dV_{atms}/dt$ , (m/s <sup>2</sup> ).	change rate for atmosphere velocities inside CV,
		Acceptable range: Default value:	$1.0 \times 10^{-2} \le \text{DVDTCV(iatms)} \le 1.0 \times 10^{\circ}$ 50.0
W-2 (R) :	DVDTCV (idrop)	Maximum velocity $dV_{drop}/dt$ , (m/s <sup>2</sup> ).	change rate for droplet velocities inside CV,
		Acceptable range: Default value:	$1.0 \times 10^{-2} \le \text{DVDTCV}(\text{idrop}) \le 1.0 \times 10^{6}$ 50.0
W-3 (R) :	DVDTCV (ipool)	Maximum velocity $dV_{noal}/dt$ , (m/s <sup>2</sup> ).	change rate for pool velocities inside CV,
		Acceptable range: Default value:	$1.0 \times 10^{-2} \le \text{DVDTCV(ipool)} \le 1.0 \times 10^{6}$ 5.0
W-4 (R) :	DVDTCV (ibubb)	Maximum velocity $dV_{bubb}/dt$ . (m/s <sup>2</sup> ).	change rate for bubble velocities inside CV,
	()	Acceptable range: Default value:	$1.0 \times 10^{-2} \le \text{DVDTCV(ibubb)} \le 1.0 \times 10^{6}$ 5.0

#### 2.1.30 Records: 158000, Treatment of Dispersed Components (Bubbles, Droplets)

Using this record one may specify the parameters described in record 158XXX for all Control Volumes in the model - see description of record 158XXX below.

#### 2.1.31 Records: 158XXX, Treatment of Dispersed Components (Bubbles, Droplets)

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

Data entered in this record defines how the dispersed components (bubbles and droplets are treated in the Control Volume. Note that by default a simple model is employed, where the number of bubbles/droplets and the average position of the bubble/droplet are not tracked (bubble/droplet count and position equations are disabled). The most accurate results are obtained with the bubble/droplet count and the bubble/droplet position calculated. This option is however more time consuming and should be employed only for selected Control Volumes, where the particle transport is particularly important.

W-1 (I): IWATCV Dispersed component treatment indicator:

IWATCV = -1: Detailed treatment of dispersed components (droplets, bubbles). Both bubble/droplet count and position equation are employed to calculate bubble/droplet average diameter and average position. This option gives most accurate results for bubbles and droplets but is most time consuming.

IWATCV = 1: Detailed treatment of dispersed components (droplets, bubbles). Simplified heat and mass transfer at the bubble-pool interphase (droplets are not affected). Use this option in case when detailed treatment of bubbles is desired but numerical problems with bubbles are encountered when IWATCV = -1 is used.

IWATCV=2: Detailed treatment of dispersed components (droplets, bubbles). Additionally mass transfer at the pool surface is deactivated. Bubble vertical de-entrainment (bubble flow to the pool surface) is deactivated if the average bubble volumetric fraction in the pool is below the limit DEWFCV (Word 2 below). This option is intended only for eventual sensitivity calculations and only for Control Volumes that are permanently filled with water (i.e. the pool level is during the whole calculations at or near the top of the Control Volume). It is not recommended to use this option.

IWATCV=3: Simplified treatment of dispersed components (droplets, bubbles), with user input average particle diameters (Words 3 and 4 below), and average particle positions (Words 5 and 6 below). <u>This is the default option, giving fast but less accurate results for bubbles/droplets.</u>

IWATCV=4: Simplified treatment of dispersed components (droplets, bubbles), with user input average particle diameters (Words 3 and 4 below), and average particle positions (Words 5 and 6 below). Additionally mass transfer at the pool surface is deactivated. Bubble vertical de-entrainment (bubble flow to the pool surface) is deactivated if the average bubble volumetric fraction in the pool is below the limit DEWFCV (Word 2 below). This option is intended only for eventual sensitivity calculations and only for Control Volumes that are permanently filled with water (i.e. the pool level is during the whole calculations at or near the top of the Control Volume). It is not recommended to use this option.

Acceptable range: any integer Default value: 3

- W-2 (R) :DEWFCVMinimum value of the average bubble volumetric fraction to activate the<br/>bubble de-entrainment (flow through pool surface to the atmosphere), (-<br/>). Used if IWATCV = 2, or IWATCV = 4.<br/>Acceptable range:  $0.0 < DEWFCV \le 0.90$ <br/>Default value: 0.90
- W-3 (R) :DDWFCVAverage droplet diameter, (m). Used if IWATCV = 3, or 4. If no value<br/>is entered, then the droplet diameter is obtained from correlations for<br/>breakup of a jet flows and atomization (see Volume 1).Acceptable range: $0.0001 \le DDWFCV \le 0.02$ <br/>Default value:0.01

- W-4 (R) :DBWFCVAverage bubble diameter, (m). Used if IWATCV = 3, or 4. If no value<br/>is entered, then the bubble diameter is obtained from correlations for<br/>bubbly and slug flow, based on flow regime map defined in record<br/>167000 (see section 2.1.42).<br/>Acceptable range:  $0.0001 \le DBWFCV \le 0.1$ , if non-zero<br/>Default value: 0.0
- W-5 (R) :ZDWFCVAverage relative droplet position (distance from the top of CV to the<br/>average droplet position, divided by the height of the CV atmosphere),<br/>(-). Used if IWATCV = 3, or 4.<br/>Acceptable range:  $0.5 \leq$  ZDWFCV  $\leq 0.9$ <br/>Default value: 0.5
- W-6 (R) :ZBWFCVAverage relative bubble position (distance from the bottom of CV to the<br/>average bubble position, divided by the height of the CV pool), (-). Used<br/>if IWATCV = 3, or 4.<br/>Acceptable range:  $0.5 \leq \text{ZBWFCV} \leq 0.9$ .<br/>Default value: 0.5
- W-7 (R) :A1WFCVLower value of the average bubble volumetric fraction for the bubble -<br/>annular transition, (-). When the average bubble volumetric fraction is<br/>smaller than A1WFCV, then the bubble average position is equal to<br/>ZBWFCV. When the average bubble volumetric fraction is larger than<br/>A2WFCV (Word 7 below), then the bubble average position is equal to<br/>0.5. Used if IWATCV = 3, or 4.<br/>Acceptable range:  $0.1 \le A1WFCV \le 0.8$ <br/>Default value: 0.75
- W-8 (R) :A2WFCVUpper value of the average bubble volumetric fraction for the bubble -<br/>annular transition, (-). When the average bubble volumetric fraction is<br/>smaller than A1WFCV (Word 6 above), then the bubble average<br/>position is equal to ZBWFCV. When the average bubble volumetric<br/>fraction is larger than A2WFCV, then the bubble average position is<br/>equal to 0.5. Used if IWATCV = 3,or 4.<br/>Acceptable range: A1WFCV+0.05  $\leq$  A2WFCV  $\leq$  0.85<br/>Default value: 0.80

#### 2.1.32 Records: 159000, Stratification Option

W-1 (I):ISTRCVStratification option. Used only for these Control Volumes for which<br/>IDSPCV is not equal to zero (see section 2.1.2).<br/>ISTRCV=0: the stratification parameter DSPCV is applied for all gases<br/>present in a given Control Volume. The stratification gradient is<br/>therefore the same for all gases.<br/>ISTRCV>0: the stratification parameter DSPCV is applied for a single<br/>gas only. The gas identification number is equal to ISTRCV (see list of<br/>available gases in the section 2.1.10). All other gases are assumed to be<br/>well mixed.<br/>Acceptable range:  $0 \leq ISTRCV \leq NGASCV \leq NGMXFL = 20$ 

*Default value:* 0

#### 2.1.33 Records: 160000, Pump/Compressor/Turbine Power Option

W-1 (I): IPPOCV
Pump power option.
IPPOCV=0: the pump/compressor/turbine power, calculated by the JN Package (calculated always for the Type 2 pumps and the mechanistic turbine models), is added to a downstream Control Volume.
IPPOCV>1: the pump/compressor/turbine power is ignored in the CV energy balance.
Acceptable range: 0 and 1 Default value: 0

#### 2.1.34 Records: 161000, Bubble Distribution Parameter and Terminal Velocity

The model for bubble distribution parameter calculation may be selected using this record. This record is optional. All entries from this record have their default values, recommended for general application.

The parameters defined in this record affect the bubble rise model in all Control Volumes and all Junctions

W-1 (I) :	MODC0	Selection of the model for bubble distribution parameter, $C_0$ , calculation. The model selected by this record will be used only if $C_0$ is calculated by the code, and not specified as an input. This means: for CV: C0VPCV = 0 (record 152XXX, section 2.1.21) for JN: C0VPJN = 0 (record 252XXX, section 2.2.19) MODC0=1: Zuber and Findlay correlation: $C_0 = 1.2$ MODC0=2: Sun et al. correlation: $C_0 = 1 / (0.82 + 0.12 p / p_{crit})$ <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 1
W-2 (I) :	MODVI	Selection of the model for bubble (and particle) terminal velocity, $v_{\infty}$ , calculation. The model selected by this record will be used only if $v_{\infty}$ is calculated by the code, and not specified as an input. This means: for CV: VIVPCV = 0 (record 152XXX, section 2.1.21) for JN: VIVPJN = 0 (record 252XXX, section 2.2.19) MODVI=1: Default set of correlations is applied for bubbles (Hadamard & Rybczynski, Peebles & Garber, Zuber, Davies & Taylor) and droplets (Hadamard & Rybczynski, Wallis) with drag coefficient $C_D$ defined by CDRGCV, below. Three $C_D$ regimes are described in Volume 1 MODVI=2: Alternative correlation is applied for bubbles, droplets and particles in the pool (if VINPRT>100, VINFRT>100). The correlation is based on drag coefficient: $v_{\infty} = \left(\frac{4/3}{C_D} \cdot \frac{Dg(\rho_f - \rho_p)}{\rho_f}\right)^{1/2}$

- g gravity constant, =  $9.81 \text{ (m/s^2)}$
- $\rho_f$  fluid density, (kg/m<sup>3</sup>)
- $\rho_p$  bubble (particle) density, (kg/m<sup>3</sup>)

1

- *D* bubble diameter, (m)
- $C_D$  drag coefficient, (CDRGCV below), five  $C_D$  regimes are described in Volume 1
- Acceptable range: 1 or 2

Default value:

W-3(R) : CDRGCV Definition of drag coefficient < 1000: CDRGCV = drag coefficient for large Re,  $C_{D,Re\to\infty}$ drag coefficient is defined by a Tabular Function number > 1000: CDRGCV–1000, as a function of Re:  $C_D = f(\text{Re})$ . The values obtained from the TF are limited to the minimum of  $10^{-2}$  and a maximum of  $10^{2}$ . Use of TF is possible only when the alternative correlation is used, MODVI=2. Acceptable range:  $0.0 < CDRGCV \le 100.0$ or reference to a Tabular Function 0.44 if MODVI = 1 (applied to droplets only; *Default value:* bubble correlation has no user-defined parameters, see Volume 1, section "Bubble velocities") 0.47 if MODVI = 2 (applied to droplets, bubbles and particles suspended in the liquid pool)

W-4 (R) : CSMLCV Constant  $C_{small}$  in the correlation for small particles:

$$v_{\infty} = \frac{1}{18} \cdot \frac{D_p^2 g(\rho_f - \rho_p)}{\eta_f} \cdot C_{small}$$

Used if MODVI=2. If a non-zero value is provided, the correlation is used if the absolute value obtained from this correlation is smaller than the absolute value obtained from the drag of the correlation. *Acceptable range:*  $0.1 < \text{CSMLCV} \le 10.0 \text{ or } 0.0$ *Default value:* 1.0 (a small value, <0.1, sets the value to zero)

Note that in order to model most accurately bubbly flow in a series of Control Volumes, the option ISVBCV should be used (Figure 2-3). This will allow to avoid bubble flow to the pool surface in CV and let the bubbles flow directly from the pool of one CV to another (see record 150XXX).

## 2.1.35 Records: 162000, Critical Depth for Bubble Formation

The model for bubble distribution parameter calculation may be selected using this record. This record is optional. All entries from this record have their default values, recommended for general application. The parameters defined in this record affect the bubble rise model in all Control Volumes.

W-1 (R) : TCMCV Critical depth/height of bubble/droplet source for the bubble/droplet formation (m). If the distance of a bubble/droplet source is smaller than TCMCV from the pool surface, then the bubbles/droplets are placed directly in the atmosphere/pool of CV. If the depth/height is larger than

2×TCMCV, the bubbles/droplets are created (if the activators IBUBCV/IDRPCV are on). An interpolation is performed for depths between TCMCV and 2×TCMCV.

Acceptable range: $0.001 < \text{TCMCV} \le 0.1$ Default value:0.01 (0.05 in code versions before Nov 2018)

The following parameters determine how the tabular mass sources for a Control Volume are handled.

- If the elevation of a tabular mass source is higher than the current pool surface + DZUPCV, then the mass source is purely for atmosphere of CV (liquid sources create droplets).
- If the elevation of a tabular mass source is lower than the current pool surface DZDNCV, then the mass source is purely for pool of CV (gas sources create bubbles).
- f the elevation of a tabular mass source is between pool surface DZDNCV and pool surface + DZUPCV, then the gas mass sources are placed in the atmosphere and liquid sources are placed in the pool of CV (bubbles or droplets are not created)

W-2 (R) :	DZUPCV	If a tabular mass DZUPCV, then the Acceptable range: Default value:	source is placed higher than the pool surface + mass source is purely for atmosphere of CV. $0.001 < DZUPCV \le 0.1$ 0.01 (0.1 in code versions before Nov 2018)
W-3 (R) :	DZDNCV	If a tabular mass DZUPCV, then the <i>Acceptable range:</i> <i>Default value:</i>	source is placed lower than the pool surface – mass source is purely for pool of CV. $0.001 < DZDNCV \le 0.1$ 0.01 (0.1 in code versions before Nov 2018)

#### 2.1.36 Records: 163000, Non-equilibrium Mass Transfer Parameters

Using this record one may specify the parameters described in record 163XXX for all Control Volumes in the model - see description of record 163XXX below.

#### 2.1.37 Records: 163XXX, Non-equilibrium Mass Transfer Parameters

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

The constants used in the non-equilibrium mass transfer models (bulk boiling and the bulk condensation - see Volume 1) may be redefined in this record. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R) :	CBBACV	Bulk boiling model constant, C <sub>BB</sub> . The model can be disabled by setting
		CBBACV to a value $\leq -1.0$ .
		Acceptable range: $10^{-4} \le CBBACV \le 0.1$ , or $CBBACV \le -1.0$ .
		Default value: 0.005.
W-2 (R) :	CBCACV	Bulk condensation model constant, $C_{BC}$ . The model can be disabled by
		setting CBCACV to a value $\leq -1.0$

Acceptable range:  $10^{-4} \le CBCACV \le 0.1$ , or  $CBCACV \le -1.0$ . Default value: 0.005.

W-3 (I): MNPBCV Treatment of steam created due to non-equilibrium boiling. MNPBCV < 0: steam is placed at the pool-atmosphere interphase. This is not a physically rigorous treatment, but it saves computing effort. MNPBCV > 0: steam bubbles are suspended in the pool. This is a rigorous physical treatment of the non-equilibrium mass transfer. However it may result in time step cuts and therefore slower calculations. This method is necessary only for rapid depressurization, for example RPV blowdown. *Acceptable range:* all integers. *Default value:* +1.

- W-4 (I): MNPCCV Treatment of water created due to non-equilibrium condensation. MNPCCV < 0: water is placed at the pool-atmosphere interphase. See comment to the Word 3 above. MNPCCV > 0: water droplets are suspended in the atmosphere (fog creation). See comment to the Word 3 above. Acceptable range: all integers. Default value: -1.
- W-5 (I): MNMDCV Activator of the non-equilibrium mass transfer model inside droplets. MNMDCV < 0: the model is inactive, MNMDCV > 0: the model is active. Typically there is no need to use the model. The model should be switched on if hot liquid, from a relatively high pressure source, is present in a Control Volume (for example RPV blowdown - see Volume 3), or when droplets are present in a strongly superheated atmosphere. *Acceptable range:* all integers.
  - *Default value:* -1.
- W-6 (I): MNMBCV Activator of the non-equilibrium mass transfer model inside bubbles. MNMBCV < 0: the model is inactive, MNMBCV > 0: the model is active. Typically there is no need to use the model. The model should be activated if the bubble relative humidity is observed to exceed 1.0. Acceptable range: all integers. Default value: -1.
- W-7 (R) :DFOGCVFog/mist diameter, (m). Used if MNPCCV>0 (Word 4) as a diameter of<br/>droplets created due to non-equilibrium condensation (fogging), or as a<br/>droplet diameter in mist flow for homogeneous volumes (IHOMCV=2)<br/>Acceptable range:  $1.0 \times 10^{-5} \le \text{DFOGCV} \le 1.0 \times 10^{-2}$ <br/>Default value:  $1.0 \times 10^{-4}$  if IHOMCV=1 (heterogeneous CV)<br/> $1.0 \times 10^{-3}$  if IHOMCV=2 (homogeneous CV)

#### 2.1.38 Records: 164000, Interphase Heat and Mass Transfer Parameters -Global

The interphase heat and mass transfer model can be deactivated using this record. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	MINGCV (IPLAT)	Interphase heat and mass transfer model global activator. Pool-atmosphere interphase. MINGCV(IPLAT) = $-1$ : inactive MINGCV(IPLAT) = $+1$ : heat and mass transfer models are active MINGCV(IPLAT) = $+2$ : only heat transfer is active. Exactly the same effect is obtained with MINGCV(IPLAT) = $+1$ if the Sherwood number multiplier, XSHPHT - section 2.13.2, is set to 0.0. Acceptable range: $-1, +1, +2$ Default value: $+1$ , if alternative fluid is used: $+2$
W-2 (I) :	MINGCV (IDPAT)	Interphase heat and mass transfer model global activator. Droplet-atmosphere interphase. MINGCV(IDPAT) = $-1$ : inactive MINGCV(IDPAT) = $+1$ : heat and mass transfer models are active MINGCV(IDPAT) = $+2$ : only heat transfer is active. Exactly the same effect is obtained with MINGCV(IDPAT) = $+1$ if the Sherwood number multiplier, XSHDHT - section 2.13.2, is set to 0.0. <i>Acceptable range:</i> $-1, +1, +2$ <i>Default value:</i> $+1$ , if alternative fluid is used: $+2$
W-3 (I) :	MINGCV (IBBPL)	Interphase heat and mass transfer model global activator. Bubble-pool interphase. MINGCV(IBBPL) = $-1$ : inactive MINGCV(IBBPL) = $+1$ : heat and mass transfer models are active MINGCV(IBBPL) = $+2$ : only heat transfer is active. Exactly the same effect is obtained with MINGCV(IBBPL) = $+1$ if the Sherwood number multiplier, XSHBHT - section 2.13.2, is set to 0.0. <i>Acceptable range:</i> $-1, +1, +2$ <i>Default value:</i> $+1$ , if alternative fluid is used: $+2$
W-4 (I) :	VINGCV (IPLAT)	Minimum velocity, (m/s), for interphase heat transfer calculation. Pool-atmosphere interphase - see Volume 1, Heat and Mass Transfer Package, description of pool-atmosphere heat and mass transfer calculation. Acceptable range: $0.0 \le \text{VINGCV(IPLAT)} \le 1000.0$ Default value: $0.0$
W-5 (I) :	VINGCV (IDPAT)	Minimum velocity, (m/s), for interphase heat transfer calculation.Droplet-atmosphere interphase - see Volume 1, Heat and Mass TransferPackage, description of droplet-atmosphere heat and mass transfercalculation.Acceptable range: $0.0 \le VINGCV(IDPAT) \le 1000.0$ Default value: $0.0$
W-6 (I) :	VINGCV (IBBPL)	Minimum velocity, (m/s), for interphase heat transfer calculation. Bubble-pool interphase - see Volume 1, Heat and Mass Transfer Package, description of bubble-pool heat and mass transfer calculation. <i>Acceptable range:</i> $0.0 \le \text{VINGCV(IBBPL)} \le 1000.0$ <i>Default value:</i> 0.0
W-7 (I) :	XINGCV	Multiplier on the interphase heat and mass transfer calculation for the

	(IPLAT)	pool-atmosphere in Acceptable range: Default value:	terphase. 0.0 < XINGCV(IPLAT) ≤ 1.0 1.0
W-8 (I) :	XINGCV (IDPAT)	Multiplier on the in droplet-atmosphere Acceptable range: Default value:	terphase heat and mass transfer calculation for the interphase. $0.0 < XINGCV(IDPAT) \le 1.0$ 1.0
W-9 (I) :	XINGCV (IBBPL)	Multiplier on the in bubble-pool interpl Acceptable range: Default value:	terphase heat and mass transfer calculation for the nase. $0.0 < \text{XINGCV(IBBPL)} \le 1.0$ 0.1 (This default value was chosen to improve the computational speed. Typically, results are not significantly affected.)

## 2.1.39 Records: 164XXX, Interphase Heat and Mass Transfer Parameters

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version). The interphase heat and mass transfer model can be deactivated using this record. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	MINTCV	Interphase heat and mass transfer model individual activator.
	(IPLAT)	Pool-atmosphere interphase.
		MINTCV(IPLAT) = -1: inactive
		MINTCV(IPLAT) = +1: heat and mass transfer models are active
		MINTCV(IPLAT) = +2: only heat transfer is active. Exactly the same
		effect is obtained with MINTCV(IPLAT) = $+1$ if the Sherwood number
		multiplier, XSHPHT - section 2.13.2, is set to 0.0.
		Acceptable range: $-1, +1, +2$ , if alternative fluid is used: $-1$ or $+2$
		Default value: MINGCV(IPLAT) - record 164000
W-2 (I) :	MINTCV	Interphase heat and mass transfer model individual activator.
	(IDPAT)	Droplet-atmosphere interphase.
		MINTCV(IDPAT) = -1: inactive
		MINTCV(IDPAT) = +1: heat and mass transfer models are active
		MINTCV(IDPAT) = +2: only heat transfer is active. Exactly the same
		effect is obtained with MINTCV(IDPAT) = $+1$ if the Sherwood number multiplier XSHDHT - section 2.13.2 is set to 0.0
		Accentable range: $-1 + 1 + 2$ if alternative fluid is used: $-1$ or $+2$
		Default value: MINGCV(IDPAT) - record 164000
W-3 (I) ·	MINTCV	Interphase heat and mass transfer model individual activator
	(IBBPL)	Bubble-pool interphase.
	()	MINTCV(IBBPL) = -1: inactive
		MINTCV(IBBPL) = +1: heat and mass transfer models are active
		MINTCV(IBBPL) = +2: only heat transfer is active. Exactly the same
		effect is obtained with MINTCV(IBBPL) = $+1$ if the Sherwood number
		multiplier, XSHBHT - section 2.13.2, is set to 0.0.

Acceptable range: -1, +1, +2, if alternative fluid is used: -1 or +2 Default value: MINGCV(IBBPL) - record 164000

W-4 (I) :	VINTCV (IPLAT)	Minimum velocity, (m/s), for interphase heat transfer calculation. Pool-atmosphere interphase - see Volume 1, Heat and Mass Transfer Package, description of pool-atmosphere heat and mass transfer calculation. Acceptable range: $0.0 < VINTCV(IPLAT) < 1000.0$
		Default value: VINGCV(IPLAT) - record 164000
W-5 (I) :	VINTCV (IDPAT)	Minimum velocity, (m/s), for interphase heat transfer calculation. Droplet-atmosphere interphase - see Volume 1, Heat and Mass Transfer Package, description of droplet-atmosphere heat and mass transfer calculation.
		Acceptable range: $0.0 \le VINTCV(IDPAT) \le 1000.0$ Default value:VINGCV(IDPAT) - record 164000
W-6 (I) :	VINTCV (IBBPL)	Minimum velocity, (m/s), for interphase heat transfer calculation. Bubble-pool interphase - see Volume 1, Heat and Mass Transfer Package, description of bubble-pool heat and mass transfer calculation. Acceptable range: $0.0 \le \text{VINTCV(IBBPL)} \le 1000.0$ Default value: VINGCV(IBBPL) - record 164000
W-7 (I) :	XINTCV (IPLAT)	Multiplier on for interphase heat and mass transfer calculation for the pool-atmosphere interphase.Acceptable range: $0.0 < XINTCV(IPLAT) \le 1.0$ Default value:XINGCV(IPLAT) - record 164000
W-8 (I) :	XINTCV (IDPAT)	Multiplier on for interphase heat and mass transfer calculation for the droplet-atmosphere interphase.Acceptable range: $0.0 < XINTCV(IDPAT) \le 1.0$ Default value:XINGCV(IDPAT) - record 164000
W-9 (I) :	XINTCV (IBBPL)	Multiplier on for interphase heat and mass transfer calculation for the bubble-pool interphase.Acceptable range: $0.0 < XINTCV(IBBPL) \le 1.0$ Default value:XINGCV(IBBPL) - record 164000 if IWATCV>0, 1.0 if IWATCV<0 (detailed bubble treatment).

## 2.1.40 Records: 165XXX, De-entrainment Calculation Options

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version). This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	MDEDCV	Droplet vertical de-entrainment calculation indicator.
		MDEDCV = 1: implicit (recommended),
		MDEDCV = 2: explicit.
		Acceptable range: 1 or 2.

*Default value:* 1.

W-2 (I): MDEBCV Bubble vertical de-entrainment calculation indicator. MDEBCV = 1: implicit (recommended), MDEBCV = 2: explicit. Acceptable range: 1 or 2. Default value: 1.

#### 2.1.41 Records: 166000, Freezing / Exceeding Fluid Property Domain Options

W-1 (I): IFRZCV Freezing option.

IFRZCV=1: freezing not allowed (code stops if freezing encountered). IFRZCV=2: freezing ignored. Temperature is set to 273 K. In this case the mass and energy balances are violated (<u>mass and energy errors</u> <u>should be checked</u> in the output file; search for :"=CV= DATA SUMMED FOR ALL CONTROL VOLUMES"). This option is convenient in case of sudden depressurization of accumulator volumes or gas cooled reactors (HTR, PBMR). *Acceptable range:* 1 or 2 *Default value:* 1

- W-2 (I): IHTOCV High temperature option. IHTOCV=1: temperatures above the maximum temperature in the Fluid Property data tables not allowed (the code stops). IHTOCV=2: temperatures above the maximum temperature in the Fluid Property data tables are ignored. Temperature is set to a maximum value in the Fluid Property data tables and calculations are continued. In this case the mass and energy balances are violated (<u>mass and energy errors</u> <u>should be checked</u> in the output file; search for :"=CV= DATA SUMMED FOR ALL CONTROL VOLUMES"). *Acceptable range:* 1 or 2 *Default value:* 1
- W-3 (I): ILPOCV Low pressure option.
  ILPOCV=1: pressures below the minimum pressure in the Fluid Property data tables not allowed (the code stops).
  IHPOCV=2: pressures below the maximum pressure in the Fluid Property data tables are ignored. Pressure is set to a minimum value in the Fluid Property data tables and calculations are continued. In this case the mass and energy balances are violated (mass and energy errors should be checked in the output file; search for :"=CV= DATA SUMMED FOR ALL CONTROL VOLUMES").
  Acceptable range: 1 or 2 Default value: 1
- W-4 (I): IHPOCV
   High pressure option.
   IHPOCV=1: pressures above the maximum pressure in the Fluid Property data tables not allowed (the code stops).
   IHPOCV=2: pressures above the maximum pressure in the Fluid Property data tables are ignored. Pressure is set to a maximum value in the Fluid Property data tables and calculations are continued. In this case

the mass and energy balances are violated (<u>mass and energy errors</u> <u>should be checked</u> in the output file; search for :"=CV= DATA SUMMED FOR ALL CONTROL VOLUMES"). *Acceptable range:* 1 or 2 *Default value:* 1

W-5 (R) : HMAXCV Minimum distance between the top of CV and the initial pool level in CV, (m). The value should be consistent with the parameter HMAXJN. Used when the elevation checking option is set (ICELJN<2). If the distance is lower than this value, then the liquid level is changed in such a way that the distance will be equal to this value and appropriate message is written to the diagnostics file. *Acceptable range:*  $0.0 < HMAXCV \le 5.0 \times 10^{-2}$ *Default value:*  $1.0 \times 10^{-2}$ 

#### 2.1.42 Records: 167000, Flow Regime Map Parameters

The parameters defined in this record are used to determine bubble size when IWATCV = 3 or 4, and DBWFCV = 0.0 (record 158XXX, section 2.1.31).

W-1 (R) :	A1BSCV	Critical void fraction for bubbly-slug transition, low mass flux, $\alpha_{1,BS}$ .Acceptable range: $0.1 \le \alpha_{1,BS} \le 0.7$ Default value: $0.25$
W-2 (R) :	A2BSCV	Critical void fraction for bubbly-slug transition, high mass flux, $\alpha_{2,BS}$ . <i>Acceptable range:</i> $0.1 \le \alpha_{2,BS} \le 0.7$ <i>Default value:</i> 0.5
W-3 (R) :	G1BSCV	Upper limit on mass flux to use $\alpha_{1,BS}$ , $G_{1,BS}$ , (kg/m <sup>2</sup> -s). For the mass fluxes <i>G</i> lower than this limit, the critical void fraction fro the bubbly - slug transition, $\alpha_{BS}$ , is equal to $\alpha_{1,BS}$ . Acceptable range: $100.0 \le G_{1,BS} \le 5000.0$ Default value: 2000.0
W-4 (R) :	G2BSCV	Lower limit on mass flux to use $\alpha_{2,BS}$ , $G_{2,BS}$ , (kg/m <sup>2</sup> -s). For the mass fluxes <i>G</i> higher than this limit, the critical void fraction fro the bubbly - slug transition, $\alpha_{BS}$ , is equal to $\alpha_{2,BS}$ . <i>Acceptable range:</i> $G_{1,BS} + 100.0 \le G_{1,BS} \le 10,000.0$ <i>Default value:</i> 3000.0 For the mass fluxes <i>G</i> within the range $G_{1,BS}$ and $G_{2,BS}$ , a linear interpolation is performed:
	(	$\alpha_{BS} = \alpha_{1,BS} + (\alpha_{1,BS} - \alpha_{1,BS}) \times \frac{G - G_{1,BS}}{G_{2,BS} - G_{1,BS}}$

W-5 (R) :DABSCVBubbly-slug transition zone width,  $\Delta \alpha_{BS}$ , (-).Pure bubbly flow occurs for: $\alpha < \alpha_{BS} - \Delta \alpha_{BS}/2$ 

		$\begin{array}{ll} \mbox{Pure slug flow occurs for:} & \alpha > \alpha_{BS} + \Delta \alpha_{BS}/2 \\ \mbox{An interpolation zone is defined for void fractions within the range:} \\ & \alpha_{BS} - \Delta \alpha_{BS}/2 < \alpha < \alpha_{BS} + \Delta \alpha_{BS}/2 \\ & \mbox{Acceptable range:} & 0.01 \leq \Delta \alpha_{BS} \leq 0.1 \end{array}$
		Default value: 0.05
W-6 (R) :	A1SACV	Void fraction for transition from bubbly/slug to annular, $\alpha_{SA}$ , (-). Applied only in Control Volumes with homogeneous thermodynamics (IHOMCV=1). Acceptable range: $0.80 \le \alpha_{SA} \le 0.95$ Default value: 0.90
W-7 (R) :	DASACV	Slug-annular transition zone width, $\Delta \alpha_{SA}$ , (-). Pure bubbly flow occurs for: $\alpha < \alpha_{SA} - \Delta \alpha_{SA}/2$ Pure slug flow occurs for: $\alpha > \alpha_{SA} + \Delta \alpha_{SA}/2$ An interpolation zone is defined for void fractions within the range: $\alpha_{SA} - \Delta \alpha_{SA}/2 < \alpha < \alpha_{SA} + \Delta \alpha_{SA}/2$ <i>Acceptable range:</i> 0.01 $\leq \Delta \alpha_{SA} \leq 0.02$ <i>Default value:</i> 0.02
W-8 (R) :	A1AMCV	Void fraction for transition from annular to mist, $\alpha_{AM}$ , (-). Applied only in Control Volumes with homogeneous thermodynamics (IHOMCV=1). <i>Acceptable range:</i> $0.98 \le \alpha_{AM} \le 0.999$ <i>Default value:</i> 0.99
W-9 (R) :	DAAMCV	Annular-mist transition zone width, $\Delta \alpha_{AM}$ , (-). Pure bubbly flow occurs for: $\alpha < \alpha_{AM} - \Delta \alpha_{AM}$ Pure slug flow occurs for: $\alpha > \alpha_{AM}$ An interpolation zone is defined for void fractions within the range: $\alpha_{AM} - \Delta \alpha_{AM} < \alpha < \alpha_{AM}$ Acceptable range: $0.001 \le \Delta \alpha_{AM} \le 0.02$ Default value: 0.01
W-10 (R) :	GSTRCV	Critical mass flux for stratified flow, $G_{strat}$ , (kg/m <sup>2</sup> -s). Stratified flow occurs when: $G < G_{strat}$
		Acceptable range: $1.0 \le GSTRCV \le 10,000.0$ Default value: $3000.0$
W-11 (R) :	VSTRCV	Critical velocity for stratified flow, $\Delta v_{strat}$ , (m/s). Stratified flow occurs when: $ v_{gas} - v_{liq}  < \Delta v_{strat}$ Acceptable range: $0.01 \le VSTRCV \le 100.0$ Default value: $1.0$
W-12 (R) :	CHORCV	Constant $C_{hor}$ The stratified flow conditions are checked if the CV flow is defined as horizontal (IHORCV=1, record 168XXX), or if the CV is not defined and the following condition is satisfied:

 $v_{hor} > v_{ver} \cdot C_{hor}$ Acceptable range:  $0.001 \le \text{CHORCV} \le 1000.0$ Default value: 2.0

#### 2.1.43 Records: 168000, Heterogeneous/Homogeneous CV, Global Activator

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W-1 (I):
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IHMGCV Heterogeneous/homogeneous CV option, global activator. The option selected in this record will be applied to all Control Volumes, unless differently specified for individual Control Volumes in the records 168XXX.

IHMGCV=1: heterogeneous CV, with pool/bubbles at the bottom of a CV and atmosphere/droplets at the top (MELCOR type Control Volumes) - see Figure 2-4.

IHMGCV=2: homogeneous CV. Bubbles and droplets are deactivated; only pool and atmosphere exist in a Control Volume. Atmosphere and pool are assumed to be homogeneously mixed (RELAP-type Control Volumes) - see Figure 2-5. The CV void fraction and gas mass fraction are given as CV-XXX-VolF-atms and CV-XXX-MasF-atms (see Table 2-23). Other volume and mass fractions, as well as the pool level, should not be used as output and plot parameters. The volume-center Control Volume pressure is available as the plot parameter: CV-XXX-Pres-pool. The plot parameter: CV-XXX-Pres-atms gives the pressure at the collapsed liquid level in CV (in a gas-filled CV this is the pressure at the CV bottom; in a liquid-filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV bottom; in a liquid filled CV this is the pressure at the CV top). Acceptable range: 1 or 2

#### 2.1.44 Records: 168XXX, Heterogeneous/Homogeneous CV, Individual Activators

W-1 (I) :	IHOMCV	Heterogeneous/homogeneous CV option, individual activator. The
		option selected in this record will be applied to Control Volume number
		XXX.
		IHOMCV=1: heterogeneous CV, with pool/bubbles at the bottom of a
		CV and atmosphere/droplets at the top (MELCOR type Control
		Volumes) - see Figure 2-4.
	IHOMCV=2: homogeneous CV. Bubbles and droplets are deactivated;	
		only pool and atmosphere exist in a Control Volume. Atmosphere and
		pool are assumed to be homogeneously mixed (RELAP-type Control
		Volumes) - see Figure 2-5. The CV void fraction and gas mass fraction
		are given as CV-XXX-VolF-atms and CV-XXX-MasF-atms (see Table
		2-23). Other volume and mass fractions, as well as the pool level, should
		not be used as output and plot parameters. The volume-center Control
		Volume pressure is available as the plot parameter: CV-XXX-Pres-pool.
		The plot parameter: CV-XXX-Pres-atms gives the pressure at the

		collapsed liquid level in CV (in a gas-filled CV this is the pressure at the CV bottom; in a liquid-filled CV this is the pressure at the CV top). <i>Acceptable range:</i> 1 or 2. <i>Default value:</i> IHMGCV, defined in record 168000
W-2 (I) :	IHORCV	Indicator for flow direction in a Homogeneous Control Volume. IHORCV=1: a horizontal flow CV, stratified flow is possible. IHORCV=2: a vertical flow CV, stratified flow is not possible. IHORCV=0: undefined CV, the criterion: $v_{hor} > v_{ver} \cdot C_{hor}$ (see record 167000, CHORCV), is used to determine whether the stratified flow is possible. <i>Acceptable range:</i> 0, 1, 2 <i>Default value:</i> 0

#### 2.1.45 Records: 169000, Accepting Mass or Energy Error

W-1 (I): IMERCV Option for mass and energy error. IMERCV=1: no mass or energy error allowed. The code stops if the flow solution results in water level in any Control Volume being higher than the volume height. In such case an error message is printed in the diagnostics file, recommending use of the second option (below). IMERCV=2: mass or energy error allowed. The code continues if the flow solution results in water level in any Control Volume being higher than the volume height. In such case the excess of water is removed automatically. The amount of removed mass and error is stored, so the user can check what is the total mass and energy error made due to this procedure. Acceptable range: 1 or 2. Default value: 1.



Figure 2-4 SPECTRA Control Volume concept: heterogeneous CV (MELCOR-type)



Figure 2-5 SPECTRA Control Volume concept: homogeneous CV (RELAP-type)

2.1.46	Records: 180000,	Hydrogen Bu	rn Model Activator
W-1 (I)	: IBGAH2	H <sub>2</sub> burn global mod	del activator, (-).
		IBGAH2 = 0:	the burn model is by default inactive in all CV; it can be activated for each volume individually, using the activator IBMAH2 (record 180XXX).
		IBGAH2 > 0 :	the burn model is by default active in all CV; it can be deactivated for each volume individually, using the activator IBMAH2 (record 180XXX).
		Acceptable range: Default value:	all integers. 0.

### 2.1.47 Records: 180XXX, Hydrogen Burn Model Data

W-1 (I) : IBMAH2		$H_2$ burn model activator, (-).		
		IBMAH2 < 0:	the burn model inactive in this CV,	
		IBMAH2 > 0:	the burn model active in this CV.	
		Acceptable range:	all integers.	
		Default value:	0.	
W-2 (R) :	DIMH2	Characteristic dime	ension for burn. (m).	
		Acceptable range:	DIMH2 > 0.0	
		Default value:	DHYDCV	
W-3 (I) :	IGNTH2	Pointer to a Tabula present.	r or Control Function defining igniter temperature, if	
		IGNTH2 = 0:	no igniter present in this CV.	
		IGNTH2 > 0 :	igniter temperature, (K), is defined by the tabular function number IGNTH2.	
		IGNTH2 < 0:	igniter temperature, (K), is defined by the control function number   IGNTH2  .	
		Acceptable range:	must be a valid reference number of a Tabular or a Control Function, if non-zero.	
		Default value:	0.	

#### 2.1.48 Records: 181XXX, Propagation Distances

With this record user can define distances required for burn to propagate to another control volume. XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (I) :	IJN	Junction number of a junction connected to the control volume XXX. Acceptable range: Must be one of the junctions connected to the control volume number XXX.	
		Default value: 0.	
W-2 (R) :	PRPDH2	Propagation distance, (m). Minimum distance that the flame must cover in the control volume XXX, before it can propagate to the control volume connected by the junction number IJN. <i>Acceptable range:</i> $0.01 \le PRPDH2 \le 1000.0$ . <i>Default value:</i> 70% of the burn characteristic dimension, DIMH2	
W-3 (I) :	IJN	Junction number of next junction connected to the control volume number XXX.	
W-4 (R) :	PRPDH2	Propagation distance, (m).	

... etc. until propagation distances are defined for all junctions connected to the control volume number XXX.

#### 2.1.49 Records: 182XXX, Combustion Completeness Model

W-1 (R) :	CCC1H2	Combustion compl CCC1H2 < 0.0 : CCC1H2 > 0.0 : Acceptable range: Default value:	eteness for slow deflagrations. Use correlation from HECTR 1.5. use constant value, equal to CCC1H2. CCC1H2 $\leq$ 1.0, if positive. 0.99.
W-2 (R) :	CCC2H2	Combustion com deflagrations. CCC2H2 < 0.0 : CCC2H2 > 0.0 : Acceptable range: Default value:	pleteness for detonations and fast turbulent Use correlation from HECTR 1.5. use constant value, equal to CCC2H2. CCC2H2 $\leq$ 1.0, if positive. 0.99.

## 2.1.50 Records: 183XXX, Detonation and Fast Deflagration Criteria

W-1 (R) : CDCH	CDCH2	Parameter selecting CDCH2 = 0.0 : CDCH2 > 0.0 :	g detonation criteria. use only the default detonation criterion. use only the criterion based on the detonation cell width, $\lambda$ (called also "the $\lambda$ criterion"). The criterion is: $D/\lambda > C$ , where D is the burn characteristic dimension, equal to DIMH2, and C is a constant, equal to CDCH2.
		CDCH2 < 0.0 :	use both the default criterion and the criterion based on detonation cell width: $D/\lambda > C$ , where D is the burn characteristic dimension, equal to DIMH2, and C is a constant, equal to $ CDCH2 $ . Detonation
		Acceptable range:	$ CDCH2  < 100.0$ . The value of 6.0 is recommended, if the $\lambda$ criterion is used.
		Default value:	0.0.
W-2 (R) :	CFCH2	Parameter selecting CFCH2 = 0.0 : CFCH2 > 0.0 :	g fast turbulent deflagration criteria. use only the default fast deflagration criterion. use only the criterion based on the expansion ratio, $\sigma$ (called also "the $\sigma$ criterion"). The criterion is: $\sigma > \sigma^*(T)$ , where $\sigma$ is the expansion ratio - the ratio of specific volumes (m <sup>3</sup> /kg) of burned to unburned gas at constant pressure, and $\sigma^*(T)$ is the critical value of the expansion ratio, calculated as follows:
		$\sigma^*(T) = 1.0 + (\sigma$	$T^*(T_0) - 1.0 \Big) \cdot \left(\frac{T_0}{T}\right)^{1.5}$
			with: $T_0$ - reference temperature, equal to 300 K, $\sigma^*(T_0)$ - value of $\sigma^*$ at the reference temperature, equal to CFCH2.
		CFCH2 < 0.0 :	use both the default criterion and the criterion based on the expansion ratio: $\sigma > \sigma^*(T)$ , where $\sigma$ is the expansion ratio - the ratio of specific volumes (m <sup>3</sup> /kg) of burned to unburned gas at constant pressure, and $\sigma^*(T)$ is the critical value of the expansion ratio, calculated as shown above, with $\sigma^*(T_0)$ equal to $ CFCH2 $
		Acceptable range:	$ CFCH2  < 100.0$ . The value of 3.5 is recommended, if the $\sigma$ criterion is used.
		Default value:	0.0 .

W-3 (R) :CMSWH2Multiplier on Mach number in shock wave calculation equation,  $C_M$ , (see<br/>Volume 1).<br/>Acceptable range:  $1.0 \le \text{CMSWH2} \le 2.0$ .<br/>Default value: 1.4.

### 2.1.51 Records: 184XXX, Flame Speed Calculation

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . The Control Volume reference numbers, XXX, need not be consecutive. The maximum number of Control Volumes is 550 (999 in LINUX version).

W-1 (R) :	RVMAH2	Ratio of maximum to average gas velocity in Control Volume. The valueis used to calculated turbulent flame speed. The default value has beenset based on results of CFD calculations (see Volume 1).Acceptable range: $0.1 \le \text{RVMAH2} \le 100.0$ Default value:8.0
W-2 (R) :	RVTMH2	Ratio of turbulent to maximum local gas velocity in Control Volume. The value is used to calculate turbulent flame speed. The default value has been set based on results of CFD calculations (see Volume 1). Acceptable range: $0.01 \le \text{RVTMH2} \le 10.0$ Default value: $0.45$
W-3 (R) :	TLAMH2	Gas temperature used for the laminar flame velocity calculation. <0.0: use the current gas temperature >0.0: use a constant temperature, TLAMH2. A value of 1150 K results in laminar flame velocities close to those calculated by the HECTR model (used by the MELCOR code) - see Volume 1. (Note that this was the default value in the earlier SPECTRA versions.) Acceptable range: TLAMH2 < 0.0 or 270.0 $\leq$ TLAMH2 $\leq$ 3000.0 Default value: -1.0

#### 2.1.52 Records: 188000, Burn Model Constants

W-1 (I): CKLIH2 Constant *C* in the Klimov expression for  $g(q, v_{lam})$ :

$$g(q, v_{lam}) = C \cdot \left( \sqrt{q} / v_{lam} \right)^{0.7}$$

Here  $v_{lam}$  is the laminar flame speed, q,  $v_{lam}$ ) is the kinetic energy density, and C is constant, equal to CKLIMH2. The best estimate value is 2.4 (see Volume 1). A value of zero will eliminate Klimov correlation. In such case only the Williams correlation is used. If CWILH2 (Word 2 below) is also set to zero, the turbulent flame speed is not taken into account and the flame speed in the slow deflagrations is always calculated from the laminar flame speed, Liu and MacFarlane correlation.

Acceptable range: $0 \le CKLIH2 \le 100.0$ <br/>a small value ( $\le 10^{-50}$ ) value will set it to 0.0Default value:2.4

W-2 (I): CWILH2 Constant C in the Williams expression for  $g(q, v_{lam})$ :

$$g(q, v_{lam}) = \left[\frac{1}{2} \cdot (1 + \sqrt{1 + (8/3) \cdot C \cdot (2q/v_{lam}^2)})\right]^{1/2}$$

Here  $v_{lam}$  is the laminar flame speed, q,  $v_{lam}$ ) is the kinetic energy density, and *C* is constant, equal to CWILH2. The best estimate value is 2.4 (see Volume 1). A value of zero will eliminate the Williams correlation. In such case only the Klimov correlation is used. If CKLIH2 is also set to zero, the turbulent flame speed is not taken into account and the flame speed in the slow deflagrations is always calculated from the laminar flame speed, Liu and MacFarlane correlation.

Acceptable range: $0 \le \text{CWILH2} \le 100.0$ <br/>a small value ( $\le 10^{-50}$ ) value will set it to 0.0Default value:2.4

#### 2.1.53 Records: 189000, Additional Print and Plot During Burn

Rapid change of parameters that may occur during burn requires that additional printouts (print edits) and plot edits should be made during burn. The additional edits are requested in this record. By default the additional edits are active, they may be deactivated by the user if too large output and plot files are being produced.

W-1 (I) :	IPRTH2	Indicator defining	if additional printouts are made during burn.
		IPRTH2 = 1:	no additional printouts are made during burn.
		IPRTH2 = 2:	additional printout is made at the start of each burn.
		Acceptable range:	IPRTH2 = 1  or  2.
		Default value:	2.
W-2 (I) :	IPLTH2	Indicator defining	if additional plot points are made during burn.
		IPLTH2 = 1:	no additional plot points are made during burn.
		IPLTH2 = 2:	additional plot point is made every time step during
			burn.
		Acceptable range:	IPLTH2 = 1  or  2.
		Default value:	2.

#### 2.1.54 Example of Control Volume Input Data

An example input for a single Control Volume is provided below. The Control Volume name is: "Example volume". There are four segments with different horizontal cross section areas. The bottom segment is 1 m height with an area of 5 m<sup>2</sup>. The bottom elevation of the CV is 5.0 m. The total height is 9 m. One of the CV segments is significantly longer than the others. Therefore the default value of the representative horizontal flow area, which is  $5.0 \text{ m}^2$  (maximum of all segment areas), is overwritten by the input value. The area of the longest segment -  $2.2 \text{ m}^2$ , is used as the representative horizontal flow area.

The default value is used for the representative vertical flow area. In this case the code will assume  $13.35 \text{ m}^2$  as the vertical flow area. Since DIPSCV is entered as zero the square root of the current pool surface area will be used as characteristic dimension for pool surface heat and mass transfer. The initial pressure is 1 bar, the gas temperature 300 K. The pool level is 2 m above the floor; the pool temperature is 295 K. The atmosphere consists of 80 % (volume fraction) nitrogen, 20 % oxygen. The relative humidity is 60 %.

There is a mass source of hydrogen. The source is located at the elevation of 7 m, the flow area is  $0.0004 \text{ m}^2$ . The mass flow rate of H<sub>2</sub> is defined by the Tabular Function TF-002. The temperature and pressure of the hydrogen source are given by the TF-003 and TF-004 respectively. There is an energy (heat) source. The energy source is located at the elevation of 9 m. The heat power is defined by the Tabular Function 007.

The  $H_2$  burn model is activated in Control Volume CV-150. The characteristic dimension for burn is not specified, thus default value will be used. An igniter is assumed to be present. The igniter temperature is defined as a function of time, by the tabular function TF-011.

The distances required to propagate burn to adjacent Control Volumes are set as 10.0 m and 20.0 respectively, for the junctions number 1 and 2. (These junctions must be connected to the control volume CV-150.)

The alternative detonation criterion, based on the detonation cell size, is requested. The value of constant is set to 6.0. Thus, the selected detonation criterion is:

$$\frac{D}{\lambda} = 6.0$$

The alternative fast deflagration criterion, based on the expansion ratio, is requested. The value of constant is set to 3.5. Thus, the selected fast turbulent deflagration criterion is:

$$\sigma > \sigma^*(T) = 1.0 + (3.5 - 1.0) \cdot \left(\frac{300}{T}\right)^{1.5}$$
\* Definition of Control Volume No. 150 \_\_\_\_\_ 105150 Example volume Height Area Segment data 
 1.00
 5.00
 \* Seg. 1

 6.00
 2.20
 \* Seg. 2

 1.00
 1.50
 \* Seg. 3

 1.00
 5.00
 \* Seg. 4
 110150 110150 110150 110150 111150 5.0 2.2 0.0 0.0 \* Elevation, A-hor, A-ver, D-pool 120150 1.0E+5 300.0 2.0 295.0 \* Pressure, Tatms, Zpool, Tpool 0.80 \* atms gas: N2 - mole fraction = 80 % 0.20 \* atms gas: O2 - mole fraction = 20 % 0.60 \* atms gas: H2O - relative humidity = 60 % 121150 4 5 3 121150 121150 \* Elev. Area Diam. IMT ITT IPT Gas No. Mass Frac. 131150 7.0 0.0004 0.02 002 003 004 1 1.0 \* M 1.0 \* H2 mass source \* Elev. IQT 141150 9.0 7 \* Energy source Definition of burn parameters for control volume No. 150 \* \_\_\_\_\_ 180000 1 Global activation of the burn model 180001 0 0.0 011 \* CV-001: - Use global activation \* - Use default characteristic dimension \* - Igniter present, temperature defined by TF-011 Propagation distances JN Dist. (m) JN Dist. (m) 181001 1 10.0 2 20.0 Combustion completeness Deflagration Detonation \* Use default values 182001 0.0 0.0 Detonation and fast turbulent deflagration criteria  $\begin{array}{rcl} D/\lambda & \sigma^{\star}\left(300\ \text{K}\right) & \star & \text{use alternative criteria} \\ 6.0 & 3.5 & \star & \text{for detonation and fast deflagration} \\ & \star & \text{The constants in the alternative criteria are:} \\ & \star & D/\lambda = 6.0; & \sigma^{\star}\left(300\ \text{K}\right) = 3.5 \end{array}$ 183001 6.0

#### 2.2 Junction Input Data

#### 2.2.1 Records: 200XXX, Junction Main Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version). No more than 50 Junctions may be connected to a single CV.

W-1 (I) :	ICVFJN	"From" Control Vo Acceptable range: Default value:	blume number, (-). must be a valid CV reference number none
W-2 (I) :	ICVTJN	"To" Control Volu: Acceptable range: Default value:	me number, (-). must be a valid CV reference number none
W-3 (R) :	AMAXJN	Flow area of fully of Acceptable range: Default value:	ppen Junction, (m <sup>2</sup> ). $0.0 < AMAXJN < 10^{10}$ . $\pi DIAMJN^2 / 4$
W-4 (R) :	ELEVJN	Elevation of middl the JN is automat { $Min[Z_{TOP}(CV_1), Z_{TOP} and Z_{TOP} are toand the "To" volu-illustrated in FigureAcceptable range:$	e point of the Junction, (m). If –999 is entered, then tically allocated to match the elevations of CV-s: $Z_{TOP}(CV_2)$ ] + Max[ $Z_{BOT}(CV_1)$ , $Z_{BOT}(CV_2)$ ]} / 2. Here op and bottom elevations of the "From" volume CV <sub>1</sub> me CV <sub>2</sub> . The automatic allocation of a Junction is e 2-6. bottom and top elevations of the Junction must lie within the Control Volumes it connects. The bottom and top elevations are calculated based on Junction height (HEIGIN) and vertical orientation (IVERIN)
		Default value:	- see Words 7 and 8, and Table 2-1. none

W-5 (R): XLENJN Momentum length, *L*, of the Junction, (m). (The value is used at the left hand side of the momentum equation:  $L \cdot dv/dt$ ). The recommended value is:

$$L_m = L + \frac{V_1}{2A_1} + \frac{V_2}{2A_2}$$

see Figure 2-7. A more detailed discussion is provided in Volume 1, section "Momentum Length and Friction Length". To use the recommended value, enter IMFLJN=1 (record 264000) and XLENJN=0.0 or IMFLJN=2.

Acceptable range:  $10^{-3} \le \text{XLENJN} \le 10^{10}$ Default value: none



Figure 2-6 Automatic allocation of JN within the boundary Control Volumes



Figure 2-7 Momentum length and friction length of a Junction

	"Froi	n" CV	"To	" CV
IVERJN	ZBOT	Ztop	ZBOT	Ztop
0 (horizontal)	ELEVJN-	ELEVJN– ELEVJN+HEIGJN/2		ELEVJN+HEIGJN/2
	HEIGJN/2		HEIGJN/2	
-1 (vert. down)	ELEVJN	ELEVJN+HEIGJN/2	ELEVJN-	ELEVJN
			HEIGJN/2	
1 (vertical up)	ELEVJN-	ELEVJN	ELEVJN	ELEVJN+HEIGJN/2
	HEIGJN/2			

Table 2-1 Bottom and top elevations of Junctions.

W-6 (R) :	DIAMJN	Diameter of the Junc <i>Acceptable range:</i> I	tion, (m). DIAMJN $> 0.0$
		Default value: (	$(4 \cdot \text{AMAXJN}/\pi)^{1/2}$
W-7 (R) :	HEIGJN	Height of the Junction of the Junction open explanation of the ma <i>Acceptable range:</i> 0 <i>Default value:</i> 4 7 t t	n, (m). Used to determine bottom and top elevations ing (Table 2-1). See Volume 1, section 4 for more eaning of HEIGJN. $0.001 \le \text{HEIGJN} \le 10^{10}$ (internal limit $\ge 0.02$ m) norizontal: = DIAMJN vertical: = DIAMJN / 2.0 The Junction height defined here is used in the code to set the opening heights in both volumes it connects. Additional limits are applied during this process - see: HMINJN, HMAXJN in the record 260000.
W-8 (I) :	IVERJN	Flow direction in the -1: vertical flow, o 0: horizontal flow, o +1: vertical flow, o The bottom and top this entry, as well as HEIGJN, as shown in Acceptable range: - Default value: 0	Junction, (-). downwards when the flow is positive, w, upwards when the flow is positive. elevations of the Junction, are calculated based on s the middle point elevation, ELEVJN and height, n Table 2-1. $1 \le IVERJN \le 1$
W-9 (R) :	EDSMJN	Smoothness of June Junction has smooth Junction has sharp correlations. Values obtained as:	ction edges. EDSMJN equal to 0.0 means the n flanges. EDSMJN equal to 1.0 means that the edged flanges. The value is used with flooding of the constants in the flooding correlations are
	C = 0	$(1 - EDSMJN) \cdot C_s$	$C_{sharp}$ + EDSMJN · $C_{sharp}$
		where $C_{smooth}$ (=1.0), appropriate for the sh	, $C_{sharp}$ (=0.525) are the values of the constant C harp and the smooth edges respectively.

Acceptable range:  $0.0 \le \text{EDSMJN} \le 1.0$ 

*Default value:* 0.474 . This value results in C=0.775, the same as in the Dartmouth correlation - see Volume 1. A small number  $(<10^{-50})$  sets the value to zero.

The following parameter is used only if IMFLJN = 1 (record 264000). It is used to calculate the friction length and the momentum length from the recommended formulae (see description of XLENJN and FRLNJN).

W-10 (R): XORFJN The "orifice length" of the Junction, (m). If the junction area is different than the area of the connected volumes, then this is the length with the JN area, denoted by *L* in Figure 2-7, Case 2. *Acceptable range:*  $0.0 \le \text{XORFJN} \le 1.0$ *Default value:* 0.0

#### 2.2.2 Records: 201XXX, Initial Velocities

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (I) :	INIVJN	Initial velocity calculation indicator.
		1: Velocities are calculated from the initial pressure differences.
		2: Input values (Words 2 and 3 below) are used. Use this option also
		when velocities should be read from an Initial Condition File -
		ICF (section 2.16.3).
		Acceptable range: 1,2
		Default value: 2
W-2 (R) :	VCMPJN	Initial velocity of atmosphere, (m/s).
( )	(IATMS)	Acceptable range: any real
	× ,	Default value: 0.0
W-3 (R) :	VCMPJN	Initial velocity of pool. (m/s).
	(IPOOL)	Acceptable range: any real
	()	Default value: 0.0

#### 2.2.3 Records: 202XXX, Multiplicity of the Junction

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

 W-1 (R): XMLTJN Multiplicity of the Junction. This is the number of Junctions that are identical to the Junction XXX. If the number is not equal to 1.0, then the flow area of this Junction, entered in the input deck, is multiplied by this number.
 Acceptable range: 0.0 < XMLTJN< 10<sup>10</sup> Default value: 1.0

#### 2.2.4 Records: 205XXX, Junction Name

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

 W-1 (A): NAMEJN User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.
 Acceptable range: any string of up to 50 characters. Default value: 50 "underline" characters: "\_".

#### 2.2.5 Records: 210XXX, Friction Loss, Form Loss and Moody Coefficient

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (R): FRLNJN Friction length,  $L_{f_2}$  (m). The value is also used to calculate  $L_{f}/D$  ratio (where D is the diameter - Word 3 below), used by the critical flow model. The recommended value is:

$$L_{f} = L + \frac{V_{1}}{2A_{1}} \cdot \left(\frac{D}{D_{1}}\right) \cdot \left(\frac{A}{A_{1}}\right)^{2} + \frac{V_{2}}{2A_{2}} \cdot \left(\frac{D}{D_{2}}\right) \cdot \left(\frac{A}{A_{2}}\right)^{2}$$

see Figure 2-7. A more detailed discussion is provided in Volume 1, section "Momentum Length and Friction Length". To use the recommended value, enter IMFLJN=1 (record 264000) and FRLNJN=0.0 or IMFLJN=2. Acceptable range:  $0.0 < FRLNJN < 10^{10}$ . Default value: XLENJN

- W-2 (R): FRRGJN Roughness, R, (m). The relative roughness is obtained as: e = R/D. Acceptable range:  $0.0 \le \text{FRRGJN} < \text{FRDHJN}$ Default value: 0.0
- W-3 (R) :FRDHJNDiameter, D, (m). The value is also used to calculate L/D ratio (where L<br/>is the friction length Word 1 above), used by the critical flow model.<br/>Acceptable range:  $0.0 < FRDHJN < 10^{10}$ <br/>Default value:DIAMJN
- W-4 (R) :FLCFJNForm loss coefficient,  $K_F$ , forward flow, (-).FLCFJN > 0: $K_F$  = constant, equal to FLCFJNFLCFJN = -XXX:  $K_F$  = Control Function XXXFLCFJN =-1XXX:  $K_F$  = Tabular Function XXX versus ReLimits of 0.0 and 10<sup>10</sup> are applied for the value obtained from CF / TF.CF/TF cannot be used for a valve (i.e. when 220XXX is present).

		Acceptable range:	$0.0 \le \text{FLCFJN} \le 10^{10}$ or reference to CF / TF. The value must be positive for a valve junction.
		Dejuuti vatue.	0.0
W-5 (R) :	FLCRJN	Form loss coefficie FLCRJN > 0: FLCRJN = -XXX FLCRJN =-1XXX Limits of 0.0 and 1 CF/TF cannot be us Acceptable range: Default value:	ent, $K_R$ , reverse flow, (-). $K_F = \text{constant}$ , equal to FLCRJN : $K_F = \text{Control Function XXX}$ : $K_F = \text{Tabular Function XXX versus Re}$ $0^{10}$ are applied for the value obtained from CF / TF. sed for a valve (i.e. when 220XXX is present). $0.0 \leq \text{FLCRJN} \leq 10^{10}$ or reference to CF / TF. The value must be positive for a valve junction. 0.0
W-6 (R) :	RFFJN	Empirical coefficie phase form loss fac shown in Table 2-2 Acceptable range: Default value:	ent in the Griffith-Rohsenow correlation for the two- ctor multiplier, $r_f$ , forward flow, (-). Values of $r_f$ are 2. The multiplier is equal to: $1.0 + r_f \cdot X \cdot v_{fg} / v_f$ . $0.0 \le \text{RFFJN} \le 10^3$ RFFGJN (see global activators, record 263000, a small number, $<10^{-50}$ , sets the value to 0.0)
W-7 (R) :	RFRJN	Empirical coefficie phase form loss fa shown in Table 2-2 Acceptable range: Default value:	ent in the Griffith-Rohsenow correlation for the two- ctor multiplier, $r_f$ , reverse flow, (-). Values of $r_f$ are 2. The multiplier is equal to: $1.0 + r_f \cdot X \cdot v_{fg} / v_f$ . $0.0 \le \text{RFRJN} \le 10^3$ RFRGJN (see global activators, record 263000, a small number, $<10^{-50}$ , sets the value to 0.0)
W-8 (R) :	CMJN	Moody coefficient for pure liquid flow 1.0 when $X=1.0$ . T equal to: CMJN + $\lambda$ is 0.7 (Volume 3). Acceptable range: Default value:	for liquid flow, $C_M$ , (-). The value of CMJN is applied w ( <i>X</i> =0.0). For <i>X</i> >0 the value is interpolated, to give Thus, the effective multiplier on the critical flow is $X \cdot (1 - CMJN)$ , see Volume 1. The best estimate value $0.1 \le CMJN \le 1.0$ CMGJN (see global activators, record 263000, a small number, $<10^{-50}$ , sets the value to 0.0)

Table 2-2 Values of *r<sub>f</sub>* for two phase form loss factor multiplier (reproduced from [7], table 7.4).

Fitting	Pressure range	Quality range (%)	$r_{f}$
Bend-short	$p/p_{crit} < 0.15$	0 - 10	1.5
Bend-short	$p/p_{crit} > 0.10$	0 - 50	4.0
Bend-long	$p/p_{crit} > 0.10$	0 - 50	2.2
Tee (serving as L)	$p/p_{crit} > 0.10$	0 - 50	1.6
Gate valve	$p/p_{crit} < 0.10$	0 - 50	1.5
Contractions	$0.015 < p/p_{crit} < 1$	0 - 50	1.0
Expansions	$0.15 < p\!/p_{crit} < 1$	0 - 50	1.1

W-9(I):

- MODFJN Model to calculate friction factor, f, (-), (see Volume 1),
  - = 1 : non-uniform roughness, Colebrook-White formula
  - = 2 : uniform roughness, Nikuradse formula
  - = 3 : simplified method, Blasius and Prandtl-Nikuradse
  - = 11 : non-uniform roughness, Beluco-Camano formula
  - = 12 : non-uniform roughness, Churchill formula
  - >1000 : f(Re,E) is given by Control Function with the number (MODFJN – 1000). It must be a 2-D Tabular Function with the first arguments being the Reynolds number (*Re*) and the second argument being the the relative roughness (*E*). The values of *Re* and *E* are those for the junction XXX, therefore the same CF may be used for multiple junctions. The actual arguments entered for the CF are not used for friction factor calculation (they will only be used to calculate the value of CF printed in the CF block output). Example:

```
Length Roughness Diameter K-for K-rev rf-for rf-rev
                                                                   CM
                                                                        MODEJIN
         (m)
                 (m)
                            (m)
                                     (-)
                                             (-)
                                                    (-)
                                                           (-)
                                                                    (-)
                                                                         (-)
210100
                 1.0E-5
                                             0.5
                                                           1.0
                                                                              * Use CF-100
        0.1
                            0.1
                                     0.5
                                                    1.0
                                                                   0.7 1100
705100 2-D Tabular Function Defining f(Re,E) for JN-100
      Group Number Fact. Const.
700100 1
            5
                   1.0 0.0 *
                                     Type : General TF
     E=0.000 E=0.005 E=0.010 E=0.05
708100 0.000 0.005
                         0.010
                                   0.05 * y-coordinate data points (relative roughness)
* Arguments
* s : (1)(2)(3)(4) Fact. Const.
710100 9 000 1 0 1.0 0.0 * x-argument: dummy argument, for the f(Re,E) calculation it
                               will be replaced by the Re-number for the given JN
710100 6 101 1 0 1.0
710100 6 102 1 0 1.0
                        0.0 * \text{ uses TF-101 for } y = 0.000
                         0.0 * \text{ uses TF-102 for } y = 0.005
710100 6 103 1 0 1.0
                         0.0 * \text{ uses TF-103 for } y = 0.010
710100 6 104 1 0 1.0
710100 9 000 1 0 1.0
                         0.0 * \text{ uses TF-103 for } y = 0.050
                         0.0 * y-argument: dummy argument, for the f(Re,E) calculation it
                               will be replaced by the relative roughness for the given JN
605101 f(Re,E=0.000)
       Re
                f
600101 1.0e5
                0.001
600101 2.0e5
               0.002
605102 f(Re,E=0.005)
       Re
                f
                0.005
600102 1.0e5
600102 2.0e5
               0.006
605103 f(Re,E=0.010)
       Re
                f
600103 1.0e5
                0.010
600103 2.0e5
              0.020
605104 f(Re,E=0.050)
              f
       Re
600104
       1.0e5
                0.050
600104 2.0e5
               0.060
                                                                              1. . .
                               C 11
                                         1. .
                                                             11
                           . • .
                                                                   .1
                                                                                    1 6
```

The following limit	ts are set internally on the value obtained from the
Control Function: 1	$0^{-6} \le f(Re, E) \le 10^6.$
Acceptable range:	MODFJN = 1, 2, 3, 11, 12, or reference to a CF
Default value:	MODGJN (see global activators, record 263000)

W-10 (I): M2PFJN Model to calculate two-phase friction multiplier,  $\Phi_f^2$ , (-), (see Vol. 1),

- = 1 : no two-phase multiplier,
- = 2 : Hancox-Nicoll model,
- = 3 : Levy Model.
- > 1000:  $\Phi_f^2$  is given by a Tabular Function with the number: (M2PFJN – 1000). The argument is void fraction. The range of independent argument (void fraction) must cover the range from 0.0 to 1.0, inclusive. The TF value must be =1.0 for the void fraction of 0.0 and >1.0 for void fractions >0.0.

Acceptable range:M2PFJN = 1, 2, 3, or reference to a TFDefault value:M2PGJN (see global activators, record 263000)

W-11 (R): CLAMJN Correction factor for non-circular tubes, *C*<sub>lam</sub>. It may also be used as a multiplier for wire-wrapped rods. The friction factor in laminar flow is obtained from:

$$f_{wall} = \frac{64 \cdot C_{lam}}{\text{Re}}$$

Rectangular channel, dimensions 0.0 < b/a < 1.0 [10] (Dia. 2-6)  $C_{lam} = 1.50$  $b/a \rightarrow 0.0$  $C_{lam} = 0.89$  $b/a \rightarrow 1.0$  (square) Tube bundle, pitch-to-diameter ratios 1.0<(*P/D*)<1.5 [10] (Dia. 2-9):  $C_{lam} = 0.89 \cdot (P/D) + 0.63$ triangular pitch  $C_{lam} = 0.96 \cdot (P/D) + 0.63$ rectangular pitch For wire-wrapped rods, Engel correlation [50] gives: f = 110/Re, so  $C_{lam}$ = 1.50 / 64 = 1.718Acceptable range:  $0.1 \leq \text{CLAMJN} \leq 10.0$ Default value: CLAGJN (see global activators, record 263000) W-12 (R): CTURJN Friction factor multiplier for turbulent flow. Applicable for example for wire-wrapped rod assemblies in fast reactors. For wire-wrapped rods, Engel correlation [50] gives:  $f = 0.55/Re^{0.25}$ , so compared to the smooth friction factor (Blasius):  $f = 0.316/Re^{0.25}$ ,  $C_{lam} =$ 0.55 / 0.316 = 1.741. A good overview of correlations: [51]. Acceptable range:  $0.1 \leq \text{CTURJN} \leq 10.0$ 

Default value: CTUGJN (see global activators, record 263000)

#### 2.2.6 Records: 220XXX, Valve Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

If the Junction flow area should change in calculations then the valve model can be used for the Junction. This is done using this record. Two types of valves are available: motor valve and check valve. Valves may only be used if the flow in this Junction is not controlled by Tabular or Control Functions (see flow control - records 230XXX, section 2.2.7).

W-1 (I): IMVLJN Indicator for "motor valve". If IMVLJN is zero then the Junction flow area is not restricted by the motor valve, and is always equal to the fully open area unless a check valve is present. If the number is positive, then

		a Tabular Function open fraction. If it a Control Function obtained from Tabu set to zero. If it is g of the valve area is <i>Acceptable range:</i> <i>Default value:</i>	with the reference number: IMVLJN will define the is negative, then the open fraction will be defined by with the reference number:  IMVLJN . If the value ular or Control Function is smaller than zero it will be reater than 1.0 it will be set to 1.0. The rate of change restricted by RACVJN (Word 4 below). must be a valid reference number of a Tabular, or a Control Function, if non-zero. 0
W-2 (R) :	DPOVJN	Opening pressure of difference in the p $\Delta p_{open,+}$ , see IBDV flow area is not res fully open area unle then check valve is required to open th <i>Acceptable range:</i> <i>Default value:</i>	difference for check valve, $\Delta p_{open}$ , (Pa) (or pressure ositive flow direction required to open a burst disk, JN, Word 9). If DPOVJN is zero then the Junction stricted by a check valve, and is always equal to the ess a motor valve is present. If the number is non-zero present and DPOVJN is the pressure difference (Pa) e check valve when closed. any real. A check valve may be used together with a motor valve (see Word 1, above). In such case the valves are assumed to be serial; the actual flow area is equal to the smaller of the two. A valve cannot be used if the Junction flow is controlled by Tabular or Control Functions (see section 2.2.7). Thus DPOVJN and IMVLJN must be zero if IGFCJN $\neq$ 0. 0.0
W-3 (R) :	DPCVJN	Closing pressure d difference in the no $\Delta p_{open,-}$ , see IBDVJ 2 above) then DPC the check valve wh Acceptable range: Default value:	lifference for check valve, $\Delta p_{close}$ , (Pa) (or pressure egative flow direction required to open a burst disk, N, Word 9). If the check valve is present (see Word VJN is the pressure difference (Pa) required to close then opened. DPCVJN < DPOVJN if check valve is present, zero otherwise. 0.0
W-4 (R) :	RACVJN	Rate of area change a motor valve, (1/A Acceptable range: Default value:	e for a check valve, maximum rate of area change for TOT)·( $dA/dt$ ), (1/s). $0.001 \le \text{RACVJN} \le 1000.0$ if a valve is present, zero otherwise. 1.0
W-5 (R) :	VIFOJN	Initial open fraction closed. VIFOJN = Acceptable range: Default value:	on, (-). VIFOJN = 0.0 means the value is initially 1.0 means the value is initially fully open. $0.0 \le \text{VIFOJN} \le 1.0$ 0.0
W-6 (R) :	VLFOJN	Leakage open fract is entered then th VLFOJN. Acceptable range: Default value:	tion for nominally closed valve (-). If positive value e valve open fraction will never be smaller than $0.0 \le \text{VLFOJN} < 1.0$ 0.0

W-7 (R): VMFOJN Maximum open fraction for nominally open valve, (-). If positive value is entered then the valve open fraction will never be greater than VMFOJN.
 Acceptable range: VLFOJN < VMFOJN < 1.0 Default value: 1.0</li>

W-8 (R): CVVLJN Coefficient used to calculate change of valve resistance with changing open fraction, (-).

If a positive value is entered then the loss factors (forward and reverse) are calculated from:

$$K_{V} = K_{0} \left[ C_{V} + \left( 1 - C_{V} \right) \frac{A_{V}}{A_{0}} \right]$$

where:  $K_V$  current valve loss coefficient, (-),

- $K_0$  loss coefficient for fully open valve, (-), (FLCFJN or FLCRJN, specified in records 210XXX see section 2.2.5).
- $C_V$  valve resistance increase coefficient, CVVLJN, (-),
- $A_V$  current valve open area, (m<sup>2</sup>),
- $A_0$  area for fully open valve, (m<sup>2</sup>).

The limiting values of the loss coefficients are equal to:

$$\begin{split} K_V &\to K_0 & \text{when } A_V \to A_0 \\ K_V &\to K_0 \cdot C_V & \text{when } A_V \to 0.0 \end{split}$$

Values of  $C_V$  may be estimated based on data in [10], chapter 9. Values appropriate for several common valve types are shown in Appendix C.1. (Typical values are: 7.0 for a butterfly valve, 25.0 for a gate valve, 1.0 for a check valve).

If a negative value is entered then the loss factor is multiplied by the value of Tabular Function number –CVVLJN, calculated for the open fraction as an argument. The loss factors (forward and reverse) are calculated from (see example in Appendix C.2):

$$K_{V} = K_{0} \cdot TF(A_{V} / A_{0})$$

where: *TF* value of Tabular Function evaluated for the current valve open fraction,  $A_V/A_0$ , (-),

Acceptable range:  $1.0 \le \text{CVVLJN} < 10^4$  or a valid reference number of a Tabular Function when negative. Default value: 5.0

W-9(I):

Burst disc idicator. If IBDVJN=1, then this valve is considered as a burst disc, with opening pressure differences for positive and negative flow directions,  $\Delta p_{open,+}$ ,  $\Delta p_{open,-}$ , defined by DPOVJN and DPCVJN respectively. Once open the valve will stay open. For a burst disc both DPOVJN and DPCVJN must be positive. If IBDVJN=0 this valve is a check valve with DPOVJN and DPCVJN being the opening and closing setpoints, as described by Words 2 and 3 above. *Acceptable range:* 0 or 1 *Default value:* 0

IBDVJN

#### 2.2.7 Records: 230XXX, Junction Flow Control

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

The user can define flow through Junctions using these records. If these records are used then the valves (records 220XXX) cannot be used. Note that if the <u>Pump Model 1</u> is used (see record 231XXX, section 2.2.8), then the interpretation of the input values is different than described below. Interpretation of IGFCJN and ILFCJN for such case is described in section 2.2.8.

W-1 (I) :	IGFCJN	Flow control for atmosphere gas. If IGFCJN = 0 then this is a "normal" Junction with flow calculated by the program. If IGFCJN > 0 then IGFCJN is the Tabular Function number which defines gas mass flow rate. If IGFCJN < 0 then the Control Function $ IGFCJN  $ defines the mass flow of gas. Gas flow will occur only if the liquid level in the upstream Control Volume is below the Junction top elevation. The value is applied only for the atmosphere gas flow. Note that the <u>total gas flow</u> <u>may be different</u> than specified by the Tabular or Control Function defined by IGFCJN, if there is a non-zero liquid flow (controlled by ILFCJN - see Word 2 below). If bubbles are present in the pool in the upstream CV then they are carried with the pool flow and the bubble gas flux will be added to the atmosphere gas flux to give the total gas flow for this Junction. <i>Acceptable range:</i> must be a valid reference number of a Tabular, or a Control Function, if non-zero if ILFCJN=0 then IGFCJN=0 if ILFCJN=0 then IGFCJN=0 0 <i>Default value:</i> 0
W-2 (I) :	ILFCJN	Flow control for pool liquid. If ILFCJN = 0 then this is a "normal" Junction with flow calculated by the program. If ILFCJN > 0 then ILFCJN is the Tabular Function number which defines liquid mass flow rate. If ILFCJN < 0 then the Control Function $ ILFCJN  $ defines the mass flow of liquid. Liquid flow will occur only if the liquid level in the upstream Control Volume is above the Junction bottom elevation. The value is applied only for the pool liquid flow. Note that the <u>total liquid flow may be different</u> than specified by the Tabular or Control Function defined by ILFCJN, if there is a non-zero gas flow (controlled by IGFCJN - see Word 1 above). If droplets are present in the atmosphere in the upstream CV then they are carried with the atmosphere flow and the droplet liquid flux will be added to the pool liquid flux to give the total liquid flow for this Junction. <i>Acceptable range:</i> must be a valid reference number of a Tabular, or a Control Function, if non-zero if ILFCJN=0 then IGFCJN=0 if ILFCJN=0 then IGFCJN=0 0

#### 2.2.8 Records: 231XXX, Pump/Compressor Model Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

There are two types of pumps in SPECTRA. The Pump Type 1 is treated as a special kind of Junction with Flow Control (see section 2.2.7), for which the volumetric flow,  $V_{pump}$ , is calculated from the user specified pump map and the pressure difference,  $\Delta P_{pump}$ :  $V_{pump} = f(\Delta P_{pump})$ . The Pump Type 2 is a standard junction for which the pressure head is added on the right hand side of the momentum equation (see Volume 1). The pressure head,  $\Delta P_{pump}$ , (or pressure ratio) is calculated based on pump map, and the current parameters, such as volumetric flow,  $V_{pump}$ , pump speed,  $\omega$ , and eventually temperature:  $\Delta P_{pump} = f(V_{pump}, \omega, T)$ . A junction with Pump Type 2 is included in the flow solution matrix, while a junction with Pump Type 1 is calculated separately, outside the flow solution matrix, as all junctions with user prescribed flow (section 2.2.7) and junctions with critical flow. Pump Type 2 offers more modelling options; it allows including temperature in the map definition (useful for compressors modelling), it allows to calculate power entering the fluid (important for compressors, typically negligible for pumps), and it allows to calculate the pump speed using the rotor inertia equation based on user specified motor torque. Therefore Type 2 is generally recommended for modelling pumps or compressors.

The pump model is based on a pump map applicable for a single-phase flow. If a two-phase mixture flows through the pump, then the map is significantly altered (see for example [4], section 8). This fact can be taken into account in calculations by using Control Functions to introduce a two-phase multiplier on the pump speed data. An example of such analysis is shown in Volume 3.

W-1 (R) :	DPNPJN	Nominal pressure head, $\Delta P_N$ , (Pa) (if > 1000.0), or nominal pressure ratio $\Pi_N$ , (-) (if $\leq 1000.0$ ). If $\Pi_N$ is specified, then the pressure head is equal to: $\Delta P_N(t) = (\Pi_N - 1) \cdot P_0(t)$ , where $P_0(t)$ is the current pressure upstream the pump. For gas compressors this option is more appropriate than using constant pressure head $\Delta P_N$ . If DPNPJN is equal to zero then the pump model is not present and the junction is either a normal junction (with flow calculated from momentum equation), or a junction with flow controlled by Tabular or Control Functions (as described in section 2.2.7). If DPNPJN is greater than zero then the pump model is used. If <u>Pump Type 1</u> is used, then parameters IGFCJN, ILFCJN must be specified in record 230XXX (section 2.2.7). These parameters are interpreted as pointers to Tabular or Control Functions, which define pump speed, $\omega$ , (1/s), as a function of time. If <u>Pump Model 2</u> is used, then parameters IGFCJN, ILFCJN must not be specified in record 230XXX (section 2.2.7). The pump speed, $\omega$ , (1/s), is defined by the pointers IOAPJN, IOPPJN (words 4 and 5 below), or by the inertia equation if the rotor moment of inertia is entered (Word 23 below). <i>Acceptable range:</i> DPNPJN $\geq 1.01$ if $\Pi_N$ is specified (DPNPJN $\leq 10^3$ ) DPNPJN $\geq 1.01 \times 10^3$ if $\Delta P_N$ is specified (DPNPJN $>10^3$ )
W-2 (R) :	VFNPJN	Nominal pump volumetric flow, $V_N$ , (m <sup>3</sup> /s).

Acceptable range: VFNPJN > 0.0. Default value: none.

W-3 (R): OMNPJN Nominal pump speed,  $\omega_N$ , (1/s). Acceptable range: OMNPJN > 0.0. Default value: none.

Words 4 and 5 are interpreted differently for the Pump Type 1 (nonzero values entered for IGFCJN and ILFCJN in record 230XXX - section 2.2.7), and for the Pump Model 2 (no values or zeroes entered in record 230XXX - section 2.2.7).

- Pump Type 1

For this pump model the pump speed,  $\omega$ , (1/s), is defined by Tabular or Control Functions, indicated by the pointers IGFCJN, ILFCJN (record 230XXX). The meaning of Words 4 and 5 is as follows:

W-4 (R): RCAPJN Maximum rate of change of atmosphere flow through the pump, (1/s). The value is used as:  $(1/V_N) \cdot dV_{atms}/dt \leq$  RCAPJN. This parameter is applied to simulate in a simplified way the flow inertia, which is not taken into account in the Type 1 pump model. Acceptable range:  $0.01 \leq$  RCAPJN  $\leq 100.0$ . Default value: 10.0.

- W-5 (R): RCPPJN Maximum rate of change of pool flow through the pump, (1/s). The value is used in as:  $(1/V_N) dV_{pool}/dt \le$  RCPPJN. This parameter is applied to simulate in a simplified way the flow inertia, which is not taken into account in the Type 1 pump model. Acceptable range:  $0.01 \le$  RCPPJN  $\le 100.0$ . Default value: 0.1.
- <u>Pump Type 2 (general pump model)</u>

If the rotor moment of inertia is not used (see Word 23 below), then the next two words define the pump speed,  $\omega$ , (1/s). If the rotor moment of inertia is used (see Word 23 below), then the next two words define the power of the pump motor,  $Q_m$ , (W).

W-4 (I) :	IOAPJN	Pointer to a tabular or a control function, which defines pump speed, a
		$(1/s)$ , or power of the pump motor, $Q_m$ , (W) for the atmosphere gas flow
		through the pump.
		If $IOAPJN = 0$ then the pump speed is equal to zero, or the motor powe
		is equal to zero.
		If $IOAPJN > 0$ then the tabular function with reference number $IOAPJN$
		defines the pump speed, $\omega$ , (1/s), or the power of the motor, $Q_m$ , (W).
		If $IOAPJN < 0$ then the control function with reference number
		IOAPJN defines the pump speed, $\omega$ , (1/s), or the power of the motor
		$Q_m$ , (W).
		Acceptable range: must be a valid reference number of a Tabular, or
		Control Function, if nonzero.
		Default value: 0.

**IOPPJN** W-5 (I): Pointer to a tabular or a control function, which defines pump speed,  $\omega$ , (1/s), or power of the pump motor,  $Q_m$ , (W) for the pool flow through the pump. If IOPPJN = 0 then the pump speed is equal to zero, or the motor power is equal to zero. If IOPPJN > 0 then the tabular function with reference number IOPPJNdefines the pump speed,  $\omega$ , (1/s), or the power of the motor,  $Q_m$ , (W). If IOPPJN < 0 then the control function with reference number **IOPPJN** defines the pump speed,  $\omega$ , (1/s), or the power of the motor,  $Q_m$ , (W). Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if nonzero. Default value: 0.

It is seen from the above description that the pump speed is defined separately for the gas flow and the liquid flow. For the gas flow the pump speed is defined by either Tabular/Control Function |IGFCJN| (Pump Type 1), or by the Tabular/Control Function |IOAPJN| (Pump Type 2). For the liquid flow the pump speed is defined by either Tabular/Control Function |ILFCJN| (Pump Type 1), or by the Tabular/Control Function |ILFCJN| (Pump Type 1), or by the Tabular/Control Function |ILFCJN| (Pump Type 1), or by the Tabular/Control Function |ILFCJN| (Pump Type 1), or by the Tabular/Control Function |IOPPJN| (Pump Type 2). This is done to allow modelling of a two-phase degradation factor. An example case with the definition of such degradation factor is shown in Volume 3.

W-6 (R) : **VF0PJN** Volumetric flow at zero pump head,  $V_0$ , (m<sup>3</sup>/s). In the previous SPECTRA version this input entry was defining the pump constant,  $C_P$ , (-), (CPMPJN). This input entry was changed to make the pump/compressor input consistent with the turbine input (see section 2.2.10). The relation between the new and the old parameter is:  $(V_0/V_N) = (C_P / (C_P-1))^{(1/c)}$ , where  $V_N$  is the nominal flow (Word 2) above), and c is the exponent CEXPJN (Word 20 below). The inverse relation is:  $C_P = (V_0/V_N)^c / ((V_0/V_N)^c - 1)$ . Note that in the previous SPECTRA version the exponent CEXPJN, was not defined by user, but it had a fixed value of 2.0. Acceptable range: Type 1:  $1.001 \le (VFOPJN / VFNPJN) \le 10$ Type 2:  $1.01 \le (VFOPJN / VFNPJN) \le 1000$ . 2.0×VFNPJN (value corresponding to  $C_P$ =1.33, for Default value: c=2.0). W-7 (R): **CRSPJN** Degradation factor for reverse pump speed,  $C_{RS}$ , (-). This is the ratio of the pressure head in normal pump speed to the head in reverse speed:  $C_{RS} = \Delta P_{reverse} / \Delta P_{max}$ , both at zero flow (see Figure 2-8). If the value is positive then at reverse pump speed the fluid is pumped in the same direction as in case of normal speed (centrifugal machines). If the value is negative then at reverse pump speed the fluid is pumped in the opposite direction (axial machines) - see appendix A. Acceptable range:  $-100.0 \le \text{CRSPJN} \le +100.0$  (a warning message is printed if the value is outside the following range: -1.0 < CRSPJN < +1.0). 0.1. The default value is appropriate for centrifugal *Default value:* pumps (see discussion of the pump maps below).



Pump/Compressor Model - Test MAP

Figure 2-8 Influence of input parameters: Vo, CRS, CDS, CVS, on the pump map.

W-8 (R): **CRFPJN** Degradation factor for reverse flow,  $C_{RF}$ , (-). The flow-dependent term in the pressure head formula is multiplied by this factor, whenever the flow is negative (reverse) - see pump model description in Appendix A.2.2, Figure 4-8. Acceptable range:  $0.0 < CRFPJN \le +100.0$  (a warning message is printed if the value is outside the range -CRFPJN  $\leq +1.0$ ). Default value: 1.0. W-9(R): **CDSPJN** Low flow degradation factor (surge factor),  $C_{DS}$ , (-). This is a ratio between the true pressure head (with surge) at zero flow, and the theoretical pressure head (no surge) at zero flow:  $C_{DS} = \Delta P_{surge} / \Delta P_{max}$ (see Figure 2-8, appendix A). In order to obtain a stable map in the entire flow range the value of  $C_{DS}$  should be: (

$$C_{DS} \ge 1 - C_{VS}^c$$

where  $C_{VS}$  is defined by the word 10 below, the exponent c is defined by the word 20 below, and the surge exponent, s, (word 26 below), should be:  $s \le 0.5$  - see appendix A.

Acceptable range:  $0.0 \le \text{CDSPJN} \le 1.0$ .

*Default value:* 0.8. (0.8-1.0 for typical water pumps, ~0.0 for gas compressors - see discussion of the pump maps below).

W-10 (I) :	IVSPJN	Pointer to a tabular function defining the limit for the low flow (surge) degradation as a function of the pump speed, $C_{VS}(\omega)$ (-). $C_{VS}$ is defined as a ratio between the volumetric flow for which surge occurs to the volumetric flow at zero head: $C_{VS}(\omega) = V_{surge}(\omega)/V_0(\omega)$ (see Figure 2-8). If the current value of the tabular function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. The argument for the Tabular Function is always the actual pump speed in rev/s. If no value is entered, or the entered value is equal to zero, then the surge model will not be used and the parabolic equation will be used for the whole flow range. If the model is used, then for the volumetric flows smaller than $V_{surge}(\omega) = C_{VS}(\omega) V_0(\omega)$ pressure head will be degraded by a factor that depends on the input parameter $C_{DS}$ (CDSPJN, Word 9 above) - see Figure 2-8. Acceptable range: must be a valid reference number of a Tabular Function, if nonzero. Default value: none.
W-11 (I) :	INFPJN	Indicator defining back flow through the pump. INFPJN = 1: Back flow is allowed (no check valve). INFPJN = 2: Back flow is not allowed (check valve present). INFPJN = 3: As 2, additionally valve closes when pump is stopped. <i>Acceptable range:</i> 1, 2, 3. <i>Default value:</i> 1.
W-12 (I) :	IMPPJN	Indicator defining flow solution scheme. IMPPJN=1: implicit.IMPPJN=2: explicit. (See Volume 3, pump model tests).Acceptable range:1, 2. For Pump Type 2 only the implicit option is available (1). When the pressure ratio is small (typical fan), and Type 1 is used, then the explicit option is recommended. The program will automatically set the explicit option for pressure ratios smaller than 1.02.Default value:1.
W-13 (R) :	OMEMJN	Minimum relative pump speed to change flow control junction into a normal junction type, $\omega_{min}/\omega_N$ (-). Used only for the <u>Type 1 pumps</u> . When pump is stopped, then in case of the Type 1 pump the flow will be equal to zero. OMEMJN converts a junction from a flow control junction into normal junction. Therefore it allows flow through the pump when the pump is stopped or pump velocity is small. <i>Acceptable range:</i> $10^{-3} \leq \text{OMEMJN} \leq 0.5$ . <i>Default value:</i> 0.1.

W-14 (R): DOMPJN Maximum relative rate of change of pump speed,  $(1/\omega_N)(d\omega/dt)$ , (1/s)Acceptable range:  $10^{-5} \le \text{DOMPJN} \le 10^3$ . Default value: 0.5 W-15 (R): TPNPJN Nominal temperature for compressors,  $T_N$ , (K). This word is used only for the <u>Type 2 pumps</u>. If no value is entered, or the entered value is equal to zero (typical pump), then the reduced volumetric flow (value used on the horizontal axis of pump maps) and the reduced speed are defined as the ratios of the current value to the nominal value (see for example [28]):

$$V_R = \left(\frac{V}{V_N}\right) \qquad \omega_R = \left(\frac{\omega}{\omega_N}\right)$$

If a positive value is entered (typical compressor), then the reduced flow (value used on the horizontal axis of pump maps) and the reduced speed are defined as the ratios of the current value to the nominal value, divided by the square root of the temperature ratio:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \qquad \omega_{R} = \frac{\left(\frac{\omega}{\omega_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}}$$

If the dynamic terms in *p*, *T* can be neglected ( $p_{tot} = p$ ,  $T_{tot} = T$ ), and the gas composition does not change during calculations, the above definition is consistent with the "corrected flow", commonly used for the compressor maps. The corrected flow,  $W_{corrt}$ , is defined as:

$$W_{corr} = W \frac{\sqrt{T_{tot}}}{p_{tot}}$$

where *W* is the mass flow rate,  $p_{tot}$  and  $T_{tot}$  are the total (static plus dynamic) pressure, and the temperature corresponding to the total (internal plus kinetic) energy - see for example reference [29] (Chapter 5) for the corrected flow definition. Derivation of the reduced flow, as used in SPECTRA, from the dimensional corrected flow is provided in Appendix A.2.

If the user wishes to take into account the dynamic terms, then he should specify the nominal velocity,  $v_N$ , (Word 16). If the user wishes to take into account possible gas composition changes, then he should specify the nominal gas constant,  $R_N$ , (Word 17).

Acceptable range: TPNPJN>273.1, or 0.0. (For the Type 1 pumps: TPNPJN=0.0).

*Default value:* 0.0.

W-16 (R): VPNPJN Nominal velocity,  $v_N$ , (m/s). This word is used only for the <u>Type 2</u> <u>pumps</u>. If the value is not entered, or the entered value is zero, then the reduced flow (value used on the horizontal axis of pump maps) definition depends on the nominal temperature entry, TPNPJN (as described above). A positive value of VPNPJN may only be entered if TPNPJN is positive. If VPNPJN is positive, then the reduced flow (value used on the horizontal axis of pump maps) is defined as:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$

If the gas composition does not change during calculations, the above definition is consistent with the corrected flow,  $W_{corr}$ , commonly used for the compressor maps. Derivation of the reduced flow, as used in SPECTRA, from the dimensional corrected flow is provided in Appendix A.2.

If the user wishes to take into account possible gas composition changes, then he should specify the nominal gas constant,  $R_N$ , (Word 17). *Acceptable range:* VPNPJN = 0.0 or VPNPJN  $\ge$  1.0 *Default value:* 0.0

W-17 (R): RPNPJN Nominal gas constant,  $R_N$ , (J/kg/K). This word is used only for the <u>Type</u> <u>2 pumps</u>. (Note that when  $R_N$  is needed, it can be taken from the SPECTRA printout - the values of R are printed in the SPECTRA Control Volume output, in the block titled fluid property data). If the value is not entered, or the entered value is zero, then the reduced flow (value used on the horizontal axis of pump maps) definition depends on the nominal temperature, TPNPJN, and velocity, VPNPJN (described above). A positive value of RPNPJN may only be entered if TPNPJN is positive. If RPNPJN is positive, then the reduced flow (value used on the horizontal axis of pump maps) is defined as described below.

• If  $v_N$  (VPNPJN, Word 16) is zero:

$$V_R = \frac{\left(\frac{V}{V_N}\right)}{\left(\frac{R}{R_N}\right)\sqrt{\frac{T}{T_N}}}$$

• If positive  $v_N$  (VPNPJN, Word 16) is specified:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\left(\frac{R}{R_{N}}\right)\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$

The last definition is always (even when the gas composition changes) consistent with the corrected flow,  $W_{corr}$ , commonly used for the

		compressor maps. I from the dimension Acceptable range: Default value:	Derivation of the reduced flow, as used in SPECTRA, nal corrected flow is provided in Appendix A.2. $100.0 \le \text{RPNPJN} \le 10000.0$ , or RPNPJN = 0.0. 0.0.
W-18 (R) :	AEXPJN	Exponent <i>a</i> in the appendix A). This <i>Acceptable range: Default value:</i>	e pump map (see description of the pump maps, word is used only for the <u>Type 2 pumps</u> . AEXPJN > 0.0, and BEXPJN $\leq$ AEXPJN $\leq$ 10.0. 2.0.
W-19 (R) :	BEXPJN	Exponent <i>b</i> in the appendix A). This <i>Acceptable range</i> :	e pump map (see description of the pump maps, word is used only for the <u>Type 2 pumps</u> . $-10.0 \le \text{BEXPJN} \le 10.0$ . Negative <i>b</i> , although generally not recommended, was found useful for matching some compressor map data. If $b < 0.0$ , then the term with $\omega_R^b$ is becoming large when the speed is small, giving unrealistically large pump head or compressor pressure ratio for a slowly turning machine. To prevent this a limit is imposed on $\omega_R^b$ : $\omega_R^b < \omega_{lim}^b = \text{BLMPJN}$ (Word 27). For lower speeds the term is linearly interpolated to give zero for zero speed (see appendix A, Figure 4-21). 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0).
W-20 (R) :	CEXPJN	Exponent <i>c</i> in the appendix A). This <i>c c c c p t d c c p t a b c c p t a b e t a d c e p t a b e t a d t c a d t c a d t a d d e t a d d d d d d d d d d</i>	e pump map (see description of the pump maps, word is used only for the <u>Type 2 pumps</u> . $0.0 < CEXPJN \le 10.0$ . 2.0.
W-21 (I):	IEPPJN	Pointer to a Tabula	ar or Control Function defining pump efficiency for

I): IEPPJN Pointer to a Tabular or Control Function defining pump efficiency for positive flow. This word is used only for the <u>Type 2 pumps</u>. If the value is positive then the efficiency will be defined by a tabular function with the number IEPPJN. If the value is negative the efficiency will be defined by a control function with the number | IEPPJN |. If the current value of the Tabular or Control Function is smaller than the minimum acceptable value (see the *Acceptable range*, below), it will be set to the minimum acceptable value. If it is larger than 1.0 it will be set to 1.0. If no value is entered then the efficiency will always be equal to 1.0. The efficiency is defined as follows:

For gas compressors this is an isentropic efficiency, defined as:

$$\eta = \frac{V\rho c_P T (\Pi^{(\kappa-1)/\kappa} - 1)}{Q_{hvdr}}$$

where *V* is the volumetric flow (m<sup>3</sup>/s),  $\rho$  is the density (kg/m<sup>3</sup>),  $c_P$  is the specific heat (J/kg/K), *T* is the inlet temperature (K),  $\Pi$  is the pressure ratio, and  $Q_{hydr}$  is the total power source for the fluid (W) (the value is positive during normal pump/compressor operation). If the power,  $Q_{hydr}$ , becomes negative, then the efficiency is given by inverse of the above formula.

For water pumps the efficiency is defined as:

$$\eta = \frac{V \,\Delta P}{Q_{hydr}}$$

where V is the volumetric flow  $(m^3/s)$ ,  $\Delta P$  is the pressure head (Pa), and  $Q_{hvdr}$  is the total power source for the fluid (W) (the value is positive during normal pump/compressor operation). If the power,  $Q_{hydr}$ , becomes negative, then the efficiency is given by inverse of the above formula.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero. (For the Type 1 pumps the value must be zero.) The efficiency is restricted by the maximum value of 1.0, and the minimum value, which depends on the power sign. In case of positive power (typical pump/compressor) the efficiency can only be positive, and the minimum limit is set at 0.1. In case of negative power (typical turbine) negative efficiency is possible (see Figure 2-10). The negative efficiency that the fluid is being decompressed and in spite of this the machine is consuming power - point 2c in Figure 2-10. Physically it means a large amount of energy is dissipated as heat due to large friction. This may happen for example in case of a turbine running with reverse speed - see appendix B. In case of negative power the minimum limit of efficiency is set to -10.0 0.

determined by the Tabular or Control Functions indicated by IOAPJN

Default value:

W-22 (I): **IENPJN** Pointer to a Tabular or Control Function defining the pump efficiency for negative flow. This word is used only for the Type 2 pumps. The efficiency definitions are similar as above, with V replaced by |V|. If the value is positive then the efficiency will be defined by a tabular function with the number IENPJN. If the value is negative the efficiency will be defined by a control function with the number | IENPJN |. If the current value of the Tabular or Control Function is smaller than the minimum acceptable value (see the Acceptable range, of IEPPJN, above), it will be set to the minimum acceptable value. If it is larger than 1.0 it will be set to 1.0. If no value is entered then the efficiency will always be equal to 1.0. Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero. (For the Type 1 pumps the value must be zero.) Default value: 0. W-23 (R): **PMIPJN** Pump rotor moment of inertia, I, (kg·m<sup>2</sup>). This word is used only for the Type 2 pumps. If no value is entered, or the entered value is equal to zero, then the inertia equation is not used, and the pump speed is

and IOPPJN (words 4 and 5 above). If a positive value is entered, then the pump speed is determined by the inertia equation:

$$I\frac{d(2\pi\omega)}{dt} = T_m - T_{hydr} - T_{fric}$$

where  $\omega$  is the pump speed (rev/s), *T* is torque, and the subscripts *m*, *hydr*, *fric*, signify motor, hydraulic and friction respectively. The factor  $2\pi$  is a consequence of  $\omega$  being expressed in revolutions per second rather than radians per second. The friction torque is assumed to be proportional to the speed, with the proportionality constant  $C_f$ ,  $(T_{fric} = C_f \cdot 2\pi\omega)$  The above equation is re-written using power instead of torque  $(Q = 2\pi\omega T)$ :

$$I\frac{d(2\pi\omega)}{dt} = \frac{Q_m}{2\pi\omega} - \frac{Q_{hydr}}{2\pi\omega} - C_f 2\pi\omega$$
  
or:

$$\frac{d\omega}{dt} = \frac{1}{I} \left( \frac{Q_m - Q_{hydr}}{4\pi^2 \omega} - C_f \omega \right)$$

This equation is used to determine the pump/compressor speed. The motor torque,  $Q_m$ , is defined by a tabular or a control function indicated by IOAPJN and IOPPJN. (Thus, if I > 0.0 then the interpretation of IOAPJN, IOPPJN is different than when I = 0.0). The friction coefficient,  $C_f$ , is defined below.

*Acceptable range:* PMIPJN≥0.0, (for the Type 1 pumps: PMIPJN=0.0).

*Default value:* 0.0.

- W-24 (R): CF1PJN Friction coefficient,  $C_f$ , (W·s<sup>2</sup>)=(kg·m<sup>2</sup>/s). This word is used for the Type 2 pumps, when the rotor moment of inertia is used to determine the pump speed (PMIPJN>0). The value is used to calculate the friction power in the pump inertia equation. The friction power is equal to  $Q_f = 4\pi^2 C_f \omega |\omega|$  (see the equation shown at PMIPJN description, above). Acceptable range: CF1PJN≥0.0, (for the Type 1 pumps: CF1PJN=0.0). Default value: 0.0.
- W-25 (R): ISNPJN Pointer to a Tabular or Control Function, which controls the eventual synchronization of the pump. ISNPJN is used only if a positive moment of inertia, PMIPJN (Word 23) is specified.

If the value of the Tabular or Control Function is smaller than, or equal to zero, then the pump's motor is not synchronized, and the pump speed is calculated using the pump moment of inertia, PMIPJN (Word 23), and the motor power,  $Q_m$ , defined by a tabular or a control function indicated by IOAPJN and IOPPJN (Words 4 and 5).

If the value of the tabular or a control function is greater than zero, then the pump's motor is synchronized, and the pump speed is constant and equal to the nominal speed, OMNPJN (Word 3), multiplied by the value obtained from the Tabular or Control Function indicated by ISNPJN. At the moment the pump is synchronized (the value of Tabular or Control

Function | ISNPJN | turns positive), its speed begins to change and it changes until the target speed is reached. The relative rate of this change is equal to DOMPJN (Word 14).

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero. 0.

Default value:

W-26 (R): **SEXPJN** Exponent s, applied in the surge region (see description of the pump maps, appendix A). The value is used to define the pressure head through the "effective speed",  $\omega$ ', defined as:

$$\omega' = \omega \cdot [C_{DS}^{1/a} + (1 - C_{DS}^{1/a}) \cdot (V/V_{surge})^{1/s}]$$

where  $\omega$  is the true speed,  $C_{DS}$  is the surge degradation factor (CDSPJN), V is the volumetric flow,  $V_{surge}$  is the volumetric flow at surge (defined by IVSPJN), and a is the exponent (AEXPJN). In order to obtain stable performance of the pump, SEXPJN should be set to 0.5 (or smaller) see description of the word CDSPJN above and appendix A. Acceptable range:  $0.1 < \text{SEXPJN} \le 10.0$ . Default value: 1.0.

Limit on  $\omega_R^{\ b}$  in case of negative b (see description of the pump maps, **BLMPJN** W-27 (R): appendix A, Figure 4-21). Acceptable range:  $1.0 < BLMPJN \le 10.0$ Default value: 2.0

#### 2.2.9 Records: 232XXX, **Simplified Turbine Data**

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

This record describes a simple turbine model, not recommended for general modelling. This was the first turbine model applied in an early version of SPECTRA, and it is preserved in the code to keep compatibility with earlier input decks. A more sophisticated turbine model, recommended for general application, is based on maps similar to those defining pump/compressors, and is described in the next section.

The simplified "turbine" is treated as a special kind of Junction with flow loss coefficient that may vary in time. An effective "turbine loss coefficient" is calculated based on the turbine data specified below (such as nominal turbine pressure difference, nominal flow, etc.), and is added to the normal loss coefficients, FLCFJN, FLCRJN, which are defined in record 210XXX (section 2.2.5), to determine the overall loss coefficient during the transient. If the nominal turbine data indicate that the overall loss coefficient should be smaller than FLCFJN, then an error message is printed and execution is stopped. In such case user should increase the flow area of turbine Junction, or decrease FLCFJN.

The nominal turbine parameters define the nominal turbine loss factor,  $C_N$ , as:

$$C_N = \Delta P_N \cdot \frac{2 \cdot A_{JN}^2}{\rho_N \cdot V_N^2}$$

where:	$\Delta P_N$	-	nominal turbine pressure drop, (Pa), (DPNTJN),
	$A_{JN}$	-	Junction flow area, $(m^2)$ , (AMAXJN, section 2.2.1),
	$ ho_N$	-	nominal turbine density, (kg/m <sup>3</sup> ), (RHNTJN), this is the density in the volume
			upstream the turbine Junction,
	$V_N$	-	nominal turbine flow, (kg/s), (VFNTJN).
			-

The actual turbine loss coefficient,  $C_t$ , is obtained during the transient from:

$$C_t = C_N f_t(\frac{\omega}{\omega_N})$$

where: $\omega_N$ $\omega$ $f_t$	<ul> <li>nomi</li> <li>actua</li> <li>indic</li> <li>Tabu</li> <li>facto</li> </ul>	nal turbine speed, (1/s), (OMNTJN), al turbine speed, (1/s), defined by a Tabular or a Control Function, ated by the pointer IOMTJN, lar Function defining "turbine map", that means relative turbine loss r $C_t/C_N$ as a function of relative turbine speed $\omega/\omega_N$ .
W-1 (R) :	DPNTJN	Nominal pressure ratio $\Pi_N$ , (-) (if $\leq 1000.0$ ), or nominal pressure head, $\Delta P_N$ , (Pa) (if > 1000.0). If $\Pi_N$ is specified, then turbine pressure head is equal to: $\Delta P_N(t) = \Pi_N \cdot P_0(t)$ , where $P_0(t)$ is the current pressure upstream the turbine. For gas turbines this option is more appropriate than using constant pressure head $\Delta P_N$ . If DPNTJN is equal to zero then the turbine model is not used and the flow loss coefficients in this Junction are constant, and equal to the values of FLCFJN, FLCRJN, defined in record 210XXX (section 2.2.5). If DPNTJN is positive, then the turbine model is used, and the turbine loss coefficient, $C_i$ , calculated as shown above, is added to FLCFJN, FLCRJN, to obtain the overall loss coefficient for this JN. Acceptable range: DPNPJN $\geq 1.01$ if $\Pi_N$ is specified (DPNPJN $\leq 10^3$ ) DPNPJN $\geq 1.01 \times 10^3$ if $\Delta P_N$ is specified (DPNPJN $> 10^3$ ) Default value: 0.0
W-2 (R) :	VFNTJN	Nominal turbine volumetric flow, $V_N$ , (m <sup>3</sup> /s). Acceptable range: VFNTJN > 0.0 Default value: none
W-3 (R) :	OMNTJN	Nominal turbine speed, $\omega_N$ , (1/s). <i>Acceptable range:</i> OMNTJN > 0.0 <i>Default value:</i> none
W-4 (I) :	IOMTJN	Pointer to a Tabular Function or a Control Function which defines the turbine speed, $\omega(t)$ . If the number is positive then the turbine speed will be defined by the Tabular Function IOMTJN. If the number is negative then the turbine speed will be defined by the value of Control Function –IOMTJN. <i>Acceptable range:</i> must be a valid reference number of a Tabular or a Control Function, if non-zero.

Default value: 0

W-5 (R) :	DOMTJN	Maximum relative : Acceptable range: Default value:	rate of change of turbine speed, $(1/\omega_N)(d\omega/dt)$ , $(1/s)$ $10^{-5} \le \text{DOMPJN} \le 10^3$ 0.5
W-6 (R) :	PRNTJN	Nominal turbine pro Acceptable range: Default value:	essure (in upstream CV), $p_N$ , (kg/m <sup>3</sup> ). PRNTJN > 0.0 initial pressure in the upstream CV
W-7 (R) :	RHNTJN	Nominal turbine de Acceptable range: Default value:	nsity (in upstream CV), $\rho_N$ , (kg/m <sup>3</sup> ). RHNTJN > 0.0 initial gas density in the upstream CV

W-8 (I): ITCTIN Number of the Tabular Function defining turbine map. If positive, then the TF number ITCTJN defines relative turbine loss factors:  $C_t/C_N$ , as a function of relative turbine speed  $\omega/\omega_N$ . If zero then the relative loss factor is always equal to one, which means:  $C_t = C_N$ . If the value obtained from the TF is smaller than zero then it will be set to zero. Acceptable range: must be a valid reference number of a Tabular Function, if non-zero 0

Default value:

W-9(I): **IEPPJN** Pointer to a Tabular or Control Function defining turbine efficiency for positive flow. If the value is positive then the efficiency will be defined by a tabular function with the number IEPPJN. If the value is negative the efficiency will be defined by a control function with the number **IEPPJN** . If the current value of the tabular function is smaller than the minimum acceptable value (see the Acceptable range, below), it will be set to the minimum acceptable value. If it is larger than 1.0 it will be set to 1.0. If no value is entered then the efficiency will always be equal to 1.0. The efficiency is defined as follows:

For gas turbine this is an isentropic efficiency, defined as:

$$\eta = \frac{Q_{hydr}}{V \rho c_P T \left[ (1/\Pi)^{(\kappa-1)/\kappa} - 1 \right]}$$

where V is the volumetric flow (m<sup>3</sup>/s),  $\rho$  is the density (kg/m<sup>3</sup>),  $c_P$  is the specific heat (J/kg/K), T is the inlet temperature (K),  $\Pi$  is the turbine pressure ratio, and  $Q_{hydr}$  is the total power source for the fluid (W) (the value is negative during normal turbine operation; note that the denominator is also negative during normal operation). If the power,  $Q_{hvdr}$ , becomes positive, then the efficiency is given by inverse of the above formula.

For water turbines the efficiency is defined as:

$$\eta = \frac{Q_{hydr}}{V \ \Delta P}$$

$Q_{hydr}$ is the total power source for the fluid (W) (the value is negative during normal turbine operation). If the power, $Q_{hydr}$ , becomes positive, then the efficiency is given by inverse of the above formula. Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero. The efficiency is further restricted as described in section 2.2.10, Word 21.Default value:0
during normal turbine operation). If the power, $Q_{hydr}$ , becomes positive, then the efficiency is given by inverse of the above formula.Acceptable range:must be a valid reference number of a Tabular or a Control Function, if nonzero. The efficiency is further restricted as described in section 2.2.10, Word 21.Default value:0
then the efficiency is given by inverse of the above formula.Acceptable range:must be a valid reference number of a Tabular or a Control Function, if nonzero. The efficiency is further restricted as described in section 2.2.10, Word 21.Default value:0
Acceptable range:must be a valid reference number of a Tabular or a Control Function, if nonzero. The efficiency is further restricted as described in section 2.2.10, Word 21.Default value:0
Control Function, if nonzero. The efficiency is further restricted as described in section 2.2.10, Word 21.Default value:0
further restricted as described in section 2.2.10, Word 21. Default value: 0
Word 21. Default value: 0
Default value: 0
W-10 (I): IENPJN Pointer to a Tabular or Control Function defining the turbine efficiency for negative flow. The efficiency definitions are similar as above, with $V$ replaced by $ V $ .
Acceptable range: must be a valid reference number of a Tabular or a
Control Function, if nonzero.
Control Function, if nonzero.

#### 2.2.10 Records: 233XXX, Turbine Model Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

The turbine model is based on the same approach as the pump/compressor Type 2 model (see section 2.2.8). In fact the turbine model uses exactly the same subroutine as the Type 2 pump/compressor. Only the input procedures are slightly different. Most of the input parameters are the same as in case of the Type 2 pump/compressor. The turbine nominal parameters, such as nominal flow and pressure ratio or head, are internally converted by the code into nominal parameters of an "equivalent pump", as shown in Figure 2-9. The equivalent pump is defined as a pump/compressor that has exactly the same map as the turbine, if the map is plotted in terms of the pump pressure ratio (outlet divided by inlet pressure) rather than the turbine pressure ratio (inlet divided by outlet pressure).

The "equivalent pump" approach allows to perform calculations using the same subroutines that calculate pumps/compressors. The discussion of turbine maps is provided in appendix B.

W-1 (R) :	DPNPJN	Nominal pressure ra	tio $\Pi_N$ , (-) (if $\leq 1000.0$ ), or nominal pressure head,
		$\Delta P_N$ , (Pa) (if > 1000	.0). If $\Pi_N$ is specified, then turbine pressure head is
		equal to: $\Delta P_N(t) = \Pi_N$	$P_0(t)$ , where $P_0(t)$ is the current pressure upstream
		the turbine. For gas	turbines this option is more appropriate than using
		constant pressure he	ad $\Delta P_N$ .
		If DPNPJN is equal	to zero then the turbine model is not present and the
		junction is a norma	l junction (with flow calculated from momentum
		equation), a junction	on with flow controlled by Tabular or Control
		Functions (as desc	ribed in section 2.2.7), or a simplified turbine
		(described in section	n 2.2.9). If DPNPJN is greater than zero then the
		turbine model is use	d. The turbine model cannot be used if pump model
		is used for the same	junction (record 231XXX).
		Acceptable range:	
		DPNPJN $\geq 1.01$	if $\Pi_N$ is specified (DPNPJN $\leq 10^3$ ).
		DPNPJN $\geq 1.01 \times 10$	<sup>3</sup> if $\Delta P_N$ is specified (DPNPJN>10 <sup>3</sup> ).
		Default value:	0.0.



Turbine Model - Test MAP

Figure 2-9 Turbine map - conversion of the turbine parameters into the "Equivalent Pump" parameters, performed internally by the code.

W-2 (R) :	VFNPJN	Nominal turbine volumetric flow, $V_N$ , (m <sup>3</sup> /s). Acceptable range: VFNPJN > 0.0. Default value: none.
W-3 (R) :	OMNPJN	Nominal turbine speed, $\omega_N$ , (1/s). Acceptable range: OMNPJN > 0.0. Default value: none.
W-4 (I) :	IOAPJN	Pointer to a tabular or a control function, which defines turbine speed, $\omega$ , (1/s) (if the rotor moment of inertia is not used), or power of the machine receiving power (generator), $Q_m$ , (W) (if the rotor moment of inertia is specified - Word 20 below) for the atmosphere gas flow through the turbine. Note that if receiving power, $Q_m$ , is specified, then the value is normally negative (power is taken from the turbine). If IOAPJN = 0 then the turbine speed is zero, or the motor power is equal to zero. If IOAPJN > 0 then the tabular function with reference number IOAPJN defines the turbine speed, $\omega$ , (1/s), or the power of the machine receiving power (generator), $Q_m$ , (W). If IOAPJN < 0 then the control function with reference number $ IOAPJN $ defines the turbine speed, $\omega$ , (1/s), or the power of the machine receiving machine receiving power (generator), $Q_m$ , (W).

		Acceptable range:	must be a valid reference number of a Tabular, or a Control Function, if nonzero.
		Default value:	0.
W-5 (I) :	IOPPJN	Pointer to a tabulat $\omega$ , (1/s) (if the rot machine receiving inertia is specified turbine. Note that is normally negative If IOPPJN = 0 then to zero. If IOPPJN > 0 then defines the turbine power (generator), If IOPPJN < 0 to  IOPPJN  defines machine receiving Acceptable range: Default value:	r or a control function, which defines turbine speed, or moment of inertia is not used), or power of the power (generator), $Q_m$ , (W) (if the rotor moment of 1 - Word 20 below) for the pool flow through the f receiving power, $Q_m$ , is specified, then the value is (power is taken from the turbine). the turbine speed is zero, or the motor power is equal a the tabular function with reference number IOPPJN speed, $\omega$ , (1/s), or the power of the machine receiving $Q_m$ , (W). then the control function with reference number s the turbine speed, $\omega$ , (1/s), or the power of the power (generator), $Q_m$ , (W). must be a valid reference number of a Tabular, or a Control Function, if nonzero. 0.
W-6 (R) :	VFOPJN	Volumetric flow for Acceptable range: Default value:	or zero-head $\Delta P = 0.0$ (or $\Pi = 1.0$ ), $V_0$ , (m <sup>3</sup> /s). 0.01 ≤ (VF0PJN / VFNPJN) ≤ 0.95. 0.6×VFNPJN.
W-7 (R) :	CRSPJN	Degradation factor pump/compressor ratio) in normal tur flow: $C_{RS} = (1/\Pi_{rev}$ then at reverse turb (i.e. the line crosse negative then at re- direction (i.e. the d $\Pi = 1.0$ line). Note larger when the tur Acceptable range: Default value:	for reverse speed, $C_{RS}$ (-). Defined as in case of the model, as the ratio of the pressure head (pressure bine speed to the head in reverse speed, both at zero $e_{rse}/(1/\Pi_{max})$ (see Figure 2-9). If the value is positive bine speed the pressure head is in the same direction es the $\Pi = 1.0$ line - see Figure 2-9). If the value is everse turbine speed the pressure head has opposite lashed line shown in Figure 2-9 would be above the that the pressure head (thus the hydraulic torque) is bine turns on reverse than during normal operation. -100.0 $\leq$ CRSPJN $\leq$ +100.0. -1.5. The default value was selected based on turbine data from reference [27] - see appendix B.
W-8 (R) :	CRFPJN	Degradation factor in the pressure hea flow is negative (r A.2.2. Acceptable range: Default value:	for reverse flow, $C_{RF}$ , (-). The flow-dependent term d formula is multiplied by this factor, whenever the reverse) - see pump model description in Appendix $0.0 < CRFPJN \le +100.0$ (a warning message is printed if the value is outside the range – 0.0 < CRFPJN < +1.0). 0.05. The default value was selected based on turbine data from reference [27] - see appendix B.

- W-9(R): **CDSPJN** Low flow degradation factor,  $C_{DS}$ , (-). Defined as in case of pump/compressor model, as a ratio between the true pressure head at zero flow, to theoretical pressure head at zero flow. This parameter is typically not used for turbine modelling. Should a value less than 1.0 be entered, the line  $\omega_N$  in Figure 2-9 would bend at low flow range (say for  $V < 0.2 \text{ m}^{3}/\text{s}$ ) towards the point ( $\Pi = 1.0, V < 0.0$ ). Acceptable range:  $0.0 \le \text{CDSPJN} \le 1.0$ . Default value: 1.0.
- W-10(I): **IVSPJN** Pointer to a tabular function defining the limit for the low flow (surge) degradation as a function of the turbine speed,  $C_{VS}(\omega)$  (-). As the word above, this is a pump/compressor model parameter and typically is not be used for turbines. It is defined as a ratio between the volumetric flow for which surge occurs to the volumetric flow at zero head:  $C_{VS}(\omega) =$  $V_{surge}(\omega)/V_0(\omega)$  (compare Figure 2-8). If the current value of the tabular function is smaller than 0.0, it will be set to 0.0. If it is larger than 1.0 it will be set to 1.0. The argument for the Tabular Function will always be the current turbine speed in rev/s. If no value is entered, or the entered value is equal to zero, then surge model will not be used and the parabolic equation will be used for the whole flow range.

Acceptable range: must be a valid reference number of a Tabular Function, if nonzero. none.

Default value:

- W-11 (D): INFPJN Indicator defining back flow through the turbine. INFPJN = 1: Back flow is allowed (no check valve). INFPJN = 2: Back flow is not allowed (check valve present). INFPJN = 3: As 2, additionally valve closes when pump is stopped. Acceptable range: 1 and 2. Default value: 1.
- **IMPPJN** Indicator defining flow solution scheme. IMPPJN=1: implicit. W-12 (I): IMPPJN=2: explicit. Acceptable range: 1. For turbines only the implicit method is allowed. Default value: 1
- W-13 (R): OMEMJN Not used for turbine. (pump Type 1 parameter - see section 2.2.8)

W-14 (R): DOMPJN Maximum relative rate of change of turbine speed,  $(1/\omega_N)(d\omega/dt)$ , (1/s)Acceptable range:  $10^{-5} \leq \text{DOMPJN} \leq 10^3$ . Default value: 0.5

W-15 (R): TPNPJN Nominal temperature,  $T_N$ , (K). If no value is entered, or the entered value is equal to zero, then the reduced flow (value used on the horizontal axis of turbine maps) and the reduced speed are defined as the ratios of the current value to the nominal value:

$$V_R = \frac{V}{V_N}$$
  $\omega_R = \frac{\omega}{\omega_N}$ 

If positive value is entered, then the reduced flow (value used on the horizontal axis of turbine maps) and the reduced speed are defined as the ratios of the current value to the nominal value, divided by the square root of the inlet temperature ratio:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \qquad \omega_{R} = \frac{\left(\frac{\omega}{\omega_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}}$$

If the dynamic terms in *p*, *T* can be neglected ( $p_{tot} = p$ ,  $T_{tot} = T$ ), and the gas composition does not change during calculations, the above definition is consistent with the "corrected flow", commonly used for the gas turbine maps. The corrected flow is defined as:

$$W_{corr} = W \frac{\sqrt{T_{tot}}}{p_{tot}}$$

where  $p_{tot}$  and  $T_{tot}$  are the total (static plus dynamic) pressure, and the temperature corresponding to the total (internal plus kinetic) energy - see for example reference [29] (Chapter 5) for the corrected flow definition. Derivation of the reduced flow, as used in SPECTRA, from the dimensional corrected flow is provided in Appendix A.2.

If the user wishes to take into account the dynamic terms, then he should specify the nominal velocity,  $v_N$ , (Word 15). If the user wishes to take into account possible gas composition changes, then he should specify the nominal gas constant,  $R_N$ , (Word 16).

*Acceptable range:* TPNPJN>273.1, or 0.0. *Default value:* 0.0.

W-16 (R): VPNPJN Nominal velocity,  $v_N$ , (m/s). If the value is not entered, or the entered value is zero, then the reduced flow (value used on the horizontal axis of turbine maps) definition depends on the nominal temperature entry, TPNPJN (as described above). A positive value of VPNPJN may only be entered if TPNPJN is positive. If VPNPJN is positive, then the reduced flow (value used on the horizontal axis of pump maps) is defined as:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$

If the gas composition does not change during calculations, the above definition is consistent with the corrected flow,  $W_{corr}$ , commonly used for the gas turbine maps. Derivation of the reduced flow, as used in SPECTRA, from the dimensional corrected flow is provided in Appendix A.2.

If the user wishes to take into account possible gas composition changes, then he should specify the nominal gas constant,  $R_N$ , (Word 16). *Acceptable range:* VPNPJN = 0.0 or VPNPJN  $\ge$  1.0 *Default value:* 0.0

W-17 (R): RPNPJN Nominal gas constant,  $R_N$ , (J/kg/K). (Note that when  $R_N$  is needed, it can be taken from the SPECTRA printout - the values of R are printed in the SPECTRA Control Volume output, in the block titled fluid property data). If the value is not entered, or the entered value is zero, then the reduced flow (value used on the horizontal axis of turbine maps) definition depends on the nominal temperature, TPNPJN, and velocity, VPNPJN (described above). A positive value of RPNPJN may only be entered if TPNPJN is positive. If RPNPJN is positive, then the reduced flow (value used on the horizontal axis of pump maps) is defined as described below.

• If  $v_N$  (VPNPJN, Word 15) is zero:

$$V_R = \frac{\left(\frac{V}{V_N}\right)}{\left(\frac{R}{R_N}\right)\sqrt{\frac{T}{T_N}}}$$

• If positive  $v_N$  (VPNPJN, Word 15) is specified:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\left(\frac{R}{R_{N}}\right)\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$

The last definition is always (even when the gas composition changes) consistent with the corrected flow,  $W_{corr}$ , commonly used for the gas turbine maps. Derivation of the reduced flow, as used in SPECTRA, from the dimensional corrected flow is provided in Appendix A.2. Acceptable range:  $100.0 \le \text{RPNPJN} \le 10000.0$ , or RPNPJN = 0.0. Default value: 0.0.

- W-18 (R):AEXPJNExponent a in the turbine map (see description of the turbine maps,<br/>appendix B).<br/>Acceptable range:<br/>AEXPJN > 0.0, and BEXPJN  $\leq$  AEXPJN  $\leq$  10.0<br/>Default value:2.0.
- W-19 (R):BEXPJNExponent b in the turbine map (see description of the turbine maps, appendix B).Acceptable range: $-10.0 \le \text{BEXPJN} \le 10.0$ .Default value:1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0).

- W-20 (R): CEXPJN Exponent *c* in the turbine map (see description of the turbine maps, appendix B). Acceptable range:  $0.0 < CEXPJN \le 10.0$ . Default value: 2.0.
- W-21 (I): IEPPJN Pointer to a Tabular or Control Function defining turbine efficiency for positive flow. If the value is positive then the efficiency will be defined by a tabular function with the number IEPPJN. If the value is negative the efficiency will be defined by a control function with the number | IEPPJN|. If the current value of the tabular function is smaller than the minimum acceptable value (see the *Acceptable range*, below), it will be set to the minimum acceptable value. If it is larger than 1.0 it will be set to 1.0. If no value is entered then the efficiency will always be equal to 1.0. The efficiency is defined as follows:

For gas turbine this is an isentropic efficiency, defined as:

$$\eta = \frac{Q_{hydr}}{V \rho c_P T \left[ (1/\Pi)^{(\kappa-1)/\kappa} - 1 \right]}$$

where *V* is the volumetric flow (m<sup>3</sup>/s),  $\rho$  is the density (kg/m<sup>3</sup>),  $c_P$  is the specific heat (J/kg/K), *T* is the inlet temperature (K),  $\Pi$  is the turbine pressure ratio, and  $Q_{hydr}$  is the total power source for the fluid (W) (the value is negative during normal turbine operation; note that the denominator is also negative during normal operation). If the power,  $Q_{hydr}$ , becomes positive, then the efficiency is given by inverse of the above formula.

For water turbines the efficiency is defined as:

$$\eta = \frac{Q_{hydr}}{V \ \Delta P}$$

where *V* is the volumetric flow (m<sup>3</sup>/s),  $\Delta P$  is the pressure head (Pa), and  $Q_{hydr}$  is the total power source for the fluid (W) (the value is negative during normal turbine operation). If the power,  $Q_{hydr}$ , becomes positive, then the efficiency is given by inverse of the above formula.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero. The efficiency is further restricted by the maximum value of 1.0, and the minimum value, which depends on the power In case of positive power (typical sign. pump/compressor) the efficiency can only be positive, and the minimum limit is set at 0.1. In case of negative power (typical turbine) negative efficiency is possible (see Figure 2-10). The negative efficiency means that the fluid is being decompressed and in spite of this the machine is consuming power - point 2c in Figure 2-10. Physically it means a large amount of energy is dissipated as heat due to large friction. This may happen for example in case of a turbine running with reverse speed - see appendix B. In case of negative power the minimum limit of efficiency is set to -10.0.



0. Default value:

Figure 2-10 Turbine decompression in a *h*-s diagram.

W-22 (I): **IENPJN** Pointer to a Tabular or Control Function defining the turbine efficiency for negative flow. The efficiency definitions are similar as above, with V replaced by |V|.

If the value is positive then the efficiency will be defined by a tabular function with the number IENPJN. If the value is negative the efficiency will be defined by a control function with the number | IENPJN |. If the current value of the Tabular or Control Function is smaller than the minimum acceptable value (see the Acceptable range, of IEPPJN, above), it will be set to the minimum acceptable value. If it is larger than 1.0 it will be set to 1.0. If no value is entered then the efficiency will always be equal to 1.0.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero.

Default value:

W-23 (R): **PMIPJN** Turbine rotor moment of inertia, I, (kg·m<sup>2</sup>). If no value is entered, or the entered value is equal to zero, then the inertia equation is not used, and the turbine speed is determined by the Tabular or Control Functions indicated by IOAPJN and IOPPJN (words 4 and 5 above). If a positive value is entered, then the turbine speed is determined by the inertia equation:

0.

$$I\frac{d(2\pi\omega)}{dt} = T_m - T_{hydr} - T_{frid}$$

where  $\omega$  is the turbine speed, T is torque, and the subscripts m, hydr, fric, signify machine receiving power (generator), hydraulic and friction respectively. The factor  $2\pi$  is a consequence of  $\omega$  being expressed in revolutions per second rather than radians per second The friction torque is assumed to be proportional to the speed, with the proportionality constant  $C_f$ ,  $(T_{fric} = C_f \cdot 2\pi\omega)$ . The above equation is re-written using power instead of torque  $(Q = 2\pi\omega T)$ :

$$I\frac{d(2\pi\omega)}{dt} = \frac{Q_m}{2\pi\omega} - \frac{Q_{hydr}}{2\pi\omega} - C_f 2\pi\omega$$

or:

$$\frac{d\omega}{dt} = \frac{1}{I} \left( \frac{Q_m - Q_{hydr}}{4\pi^2 \omega} - C_f \omega \right)$$

This equation is used to determine the turbine speed. The motor torque,  $Q_m$ , is defined by a tabular or a control function indicated by IOAPJN and IOPPJN. (Thus, if I > 0.0 then the interpretation of IOAPJN, IOPPJN is different from their interpretation when I = 0.0). The friction coefficient,  $C_f$ , is defined below. Acceptable range: PMIPJN $\geq 0.0$ .

Default value: 0.0.

- W-24 (R): CF1PJN Friction coefficient,  $C_f$ , (W/s<sup>2</sup>). The value is used to calculate the friction power in the turbine inertia equation. The friction power is equal to  $Q_f = 4\pi^2 C_f \omega |\omega|$  (see the equation shown at PMIPJN description, above). *Acceptable range:* CF1PJN $\geq$ 0.0. *Default value:* 0.0.
- W-25 (R): ISNPJN Pointer to a Tabular or Control Function, which controls the eventual synchronization of the turbine. ISNPJN is used only if a positive moment of inertia, PMIPJN (Word 20) is specified.

If the value of the Tabular or Control Function is smaller than, or equal to zero, then the turbine's motor (generator) is not synchronized, and the turbine speed is calculated using the turbine moment of inertia, PMPIJN (Word 20), and the motor power,  $Q_m$ , defined by a tabular or a control function indicated by IOAPJN and IOPPJN (Words 5 and 6).

If the value of the Tabular or Control Function is greater than zero, then the turbine's motor (generator) is synchronized, and the turbine speed is constant and equal to the nominal speed, OMNPJN (Word 4), multiplied by the value obtained from the Tabular or Control Function indicated by ISNPJN. At the moment the turbine is synchronized (the value of a Tabular or Control Function turns positive), its speed begins to change and it changes until the target speed is reached. The relative rate of this change is limited by DOMPJN (Word 14).

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if nonzero.

*Default value:* 0.

W-26 (R): SEXPJN Exponent *s*, applied in the surge region. This exponent is analogical to the same exponent in the pump/compressor model. Since the surge

model is typically not applied for turbines, the value of s is meaningless<br/>for the turbine.Acceptable range: $0.1 < SEXPJN \le 10.0$ .<br/>Default value:W-27 (R):BLMPJNLimit on  $\omega^b$  in case of negative b (see description of the pump maps,<br/>appendix A).<br/>Acceptable range:2.0 < BLMPJN  $\le 20.0$ .<br/>Default value:10.0.

#### 2.2.11 Records: 235XXX, Pump/Turbine Additional Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version). In this record the user can define:

- The initial speed and speed limits for a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction).
- The minimum reduced flow used for power calculation in nearly zero flow region. Typically the efficiency of pumps/compressors decrease with decreasing flow. In the limit of zero flow, the efficiency is zero; the isentropic power is zero; and the true power is positive. In the code the true power to fluid,  $Q_{hydr}$ , is computed from:

$$Q_{hydr} = \frac{Q_{isent}}{\eta}$$

In case of zero flow both  $Q_{isentr}$  and  $\eta$  are zero, so the symbol becomes undefined. In order to be able to define a non-zero power at zero flow (pump operating with valve closed), the concept of minimum velocity for power calculation is introduced.

W-1 (R) :	OTAPJN	Initial speed, $\omega$ , of a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction). Acceptable range: $-10 \cdot \omega_N < \omega < 10 \cdot \omega_N$ ( $\omega_N$ is the nominal speed). Default value: 0.0.
W-2 (R) :	VFAPJN	Initial volumetric flow of atmosphere (gas), $V_a$ , through a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction). Acceptable range: $-10 \cdot V_N < V_a < 10 \cdot V_N$ ( $V_N$ is the nominal flow). Default value: 0.0.
W-3 (R) :	VFPPJN	Initial volumetric flow of pool (liquid), $V_p$ , through a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction) Acceptable range: $-10V_N < V_p < 10V_N$ . ( $V_N$ is the nominal flow). Default value: 0.0.
W-4 (R) :	OM1PJN	Minimum rotational speed, $\omega_{min}$ , of a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction)

Acceptable range:  $\omega_{min} < \omega_N$ . ( $\omega_N$  is the nominal speed). Default value:  $-100.0 \omega_N$ .

W-5 (R): OM2PJN Maximum rotational speed,  $\omega_{max}$ , of a pump (if record 231XXX is present for this Junction) or a turbine (if record 233XXX is present for this Junction) Acceptable range:  $\omega_{max} > \omega_N$ . ( $\omega_N$  is the nominal speed). Default value:  $+100.0 \omega_N$ .

W-6 (R): VMNPJN Multiplier defining the minimum reduced flow for power calculation. Used whenever the reduced flow is smaller than  $V_{min}$ , defined as:

$$V_{min} = VMNPJN \times V_N \times \left(\frac{\omega_R^a}{\omega_R^b}\right)^1$$

where  $V_N$  is the nominal flow of a pump. In case of a turbine this is a nominal flow of the "equivalent pump" (the "equivalent pump" data is printed in the output file).  $\omega_R$  is the reduced speed, and *a*, *b*, *c* are the exponents in the pump/compressor/turbine map. The power is calculated by replacing the actual reduced flow by the minimum flow. For example, in case of water pump the power is given by:

$$Q_{hydr} = V_{min} \Delta P$$

The efficiency is then re-defined. The actual efficiency is given by:

$$\eta = \frac{V \ \Delta P}{Q_{hydr}}$$

Thus when the pump flow is zero, V=0.0, then the efficiency (above formula) is zero, and the power, which enters the fluid, is positive  $(=V_{min} \Delta P)$ 

Acceptable range: $10^{-2} \le \text{VMNPJN} \le 2.0.$ Default value:0.5.

#### 2.2.12 Records: 236XXX, Simplified Pump/Turbine Data

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version). In this record the user can define the pump head through a Tabular or Control Function. The value obtained from the TF / CF may be positive (pump) as well as negative (turbine).

W-1 (I): IPTAJN Pointer to a Tabular or Control Function that defines the pump/turbine head (Pa) for the atmosphere flow through the Junction XXX. If the number is positive, then the head will be defined by a Tabular Function with the reference number: IPTAJN. If the number is negative, then the head will be defined by a Control Function with the reference number: |IPTAJN|.
		Acceptable range:	must be a valid reference number of a Tabular or a Control Function, if non-zero.
		Default value:	0.
W-2 (I) :	IPTPJN	Pointer to a Tabula head (Pa) for the po positive, then the h reference number: 1 be defined by a Cor <i>Acceptable range:</i> <i>Default value:</i>	ar or Control Function that defines the pump/turbine bol flow through the Junction XXX. If the number is nead will be defined by a Tabular Function with the IPTPJN. If the number is negative, then the head will ntrol Function with the reference number:   IPTPJN  . must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.

Note: in case of TF, the user defines the pump head as a function of time.

#### 2.2.13 Records: 237XXX, Request for Pump Curves

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

Pump characteristic curves (performance maps) are determined by the input parameters such as VF0PJN, CRSPJN, etc., defined in the input records 231XXX. In order to make it easy to compare the curves with source data, SPECTRA prints the pump curves for several selected pump speeds. In this record the user can define the pump speeds for which the curves will be printed in the output file. By default the curves are printed for reduced speeds of 0.2, 0.4, 0.6, 0.8, 1.0, and 1.2. The curves are printed for both positive and negative speeds. An example of such printout is shown below.

REDU	JCED PRESSURE	HEAD FOR FORM	WARD PUMP SPE	ED:			
i	V-red	N-red = 2.000E-01	N-red = 4.000E-01	N-red = 6.000E-01	N-red = 8.000E-01	N-red = 1.000E+00	N-red = 1.200E+00
	0.00000E+00	5.33333E-02	2.13333E-01	4.80000E-01	8.53333E-01	1.33333E+00	1.92000E+00
1	2.00000E-01	4.00000E-02	2.00000E-01	4.66667E-01	8.40000E-01	1.32000E+00	1.90667E+00
2	4.00000E-01	2.08167E-17	1.60000E-01	4.26667E-01	8.00000E-01	1.28000E+00	1.86667E+00
3	6.00000E-01	-6.66667E-02	9.33333E-02	3.60000E-01	7.33333E-01	1.21333E+00	1.80000E+00
4	8.00000E-01	-1.60000E-01	8.32667E-17	2.66667E-01	6.40000E-01	1.12000E+00	1.70667E+00
5	1.00000E+00	-2.80000E-01	-1.20000E-01	1.46667E-01	5.20000E-01	1.00000E+00	1.58667E+00
6	1.20000E+00	-4.26667E-01	-2.66667E-01	2.22045E-16	3.73333E-01	8.53333E-01	1.44000E+00
7	1.40000E+00	-6.00000E-01	-4.40000E-01	-1.73333E-01	2.00000E-01	6.80000E-01	1.26667E+00
8	1.60000E+00	-8.00000E-01	-6.40000E-01	-3.73333E-01	3.33067E-16	4.80000E-01	1.06667E+00
9	1.80000E+00	-1.02667E+00	-8.66667E-01	-6.00000E-01	-2.26667E-01	2.53333E-01	8.40000E-01
10	2.00000E+00	-1.28000E+00	-1.12000E+00	-8.53333E-01	-4.80000E-01	2.22045E-16	5.86667E-01
W-1 (R) :	OMR	PJN(1) Rela	tive pump sp	peed $(\omega/\omega_N)$	number 1	0	
		Acceptable range. $0.0 < \text{OWRPJN}(1) < 2.0$					
		Defa	ult value:	0.2			
W-2 (R) :	OMR	PJN(2) Rela Accej Defai	tive pump sp ptable range ult value:	beed $(\omega/\omega_N)$ : 0.0 < OM 0.4	number 2 RPJN(2) < 2	.0	
W-3 (R) :	OMR	PJN(3) Rela	tive pump s	beed ( $\omega/\omega_N$ )	number 3		
		Acce	ptable range	: 0.0 < OM	RPJN(3) < 2	.0	
		Defa	ult value:	0.6			

OMRPJN(4) Relative pump spe	eed ( $\omega/\omega_N$ ) number 4
Acceptable range:	0.0 < OMRPJN(4) < 2.0
Default value:	0.8
OMRPJN(5) Relative pump spe	eed ( $\omega/\omega_N$ ) number 5
Acceptable range:	0.0 < OMRPJN(5) < 2.0
Default value:	1.0
OMRPJN(6) Relative pump spe	eed ( $\omega/\omega_N$ ) number 6
Acceptable range:	0.0 < OMRPJN(6) < 2.0
Default value:	1.2
	OMRPJN(4) Relative pump spectra Acceptable range: Default value: OMRPJN(5) Relative pump spectra Acceptable range: Default value: OMRPJN(6) Relative pump spectra Acceptable range: Default value:

#### 2.2.14 Records: 238XXX, User-Defined Fluid Properties - Positive Flow Direction

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

If this record is not present or default values are entered, then the fluid properties (liquid temperature, gas temperature, gas composition) in the junction are always taken from the upstream CV. Note that if stratification models are present in the upstream CV, then the local fluid properties at junction elevation are used.

Using this record the parameters can be defined by using Tabular or Control Functions. This may be useful in case of coupled code calculations - if local properties are known from more detailed outside calculations (e.g. CFD code with fine mesh) they may be passed on to the junction. **The data entered in this record is used only if the flow direction is positive, to make sure that the information coming from another code is used only when the flow direction is right.** When the flow is negative, then the upstream CV properties are used, unless record 239XXX is defined. Simultaneous use of 238XXX and 239XXX indicate erroneous input model definition and in such case a warning is given in the diagnostics file.

W-1 (I) :	IAT1JN	Pointer to a Tabular or Control Function that defines the temperature of atmosphere gas flowing through the junction. If the number is positive, the temperature will be defined by a Tabular Function with the reference number: IAT1JN. If the number is negative, the temperature will be defined by a Control Function with the reference number: $ IAT1JN $ . At any given time of the transient the temperature will be equal to the current value of the Tabular or Control Function with the following limits: $T_{sat} \leq T_{atms} \leq 3070$ . Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero.Default value:0.
W-2 (I) :	IPL1JN	Pointer to a Tabular or Control Function that defines the temperature of pool flowing through the junction. If the number is positive, the temperature will be defined by a Tabular Function with the reference number: IPL1JN. If the number is negative, the temperature will be defined by a Control Function with the reference number: IPL1JN.

At any given time of the transient the temperature will be equal to the

current value of the Tabular or Control Function with the following limits:  $273.2 \le T_{pool} \le T_{sat}$ . Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero. Default value: 0 W-3 (I): IGS1JN(1) Pointer to a Tabular or Control Function that defines the mole fraction of gas 1 flowing through the junction. If the number is positive, the fraction will be defined by a Tabular Function with the reference number: IGS1JN. If the number is negative, the fraction will be defined by a Control Function with the reference number: | IGS1JN |. At any given time of the transient the mole fractions will be equal to the current value of the Tabular or Control Function with the following limits: 0.0  $\leq X(1) \leq 1.0.$ Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero. Default value: 0. W-4 (I): IGS1JN(2) The same for gas number 2. Note that the user-defined gas mole fractions must either be specified for all gases or none.

(...) until all gases are defined. Normalization is performed to ensure that sum of all fractions is equal to 1.0.

#### 2.2.15 Records: 239XXX, User-Defined Fluid Properties - Negative Flow Direction

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

This record defines the same parameters as record 238XXX but these to be applied **only when the flow direction is negative.** Changing the definition of JN flow direction in the input file and replacing 238XXX by 239XXX will yield the identical results. Simultaneous use of 238XXX and 239XXX indicate erroneous input model definition and in such case a warning is given in the diagnostics file.

W-1 (I) :	IAT2JN	Pointer to a Tabular or Control Function that defines the temperature of atmosphere gas flowing through the junction. If the number is positive, the temperature will be defined by a Tabular Function with the reference number: IAT2JN. If the number is negative, the temperature will be defined by a Control Function with the reference number: $ IAT2JN $ . At any given time of the transient the temperature will be equal to the current value of the Tabular or Control Function with the following limits: $T_{sat} \leq T_{atms} \leq 3070$ . Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero.Default value:0.
W-2 (I) :	IPL2JN	Pointer to a Tabular or Control Function that defines the temperature of

W-2 (I): IPL2JN Pointer to a Tabular or Control Function that defines the temperature of pool flowing through the junction. If the number is positive, the temperature will be defined by a Tabular Function with the reference number: IPL2JN. If the number is negative, the temperature will be

		defined by a Contr At any given time current value of the limits: $273.2 \le T_{pool}$ Acceptable range: Default value:	ol Function with the reference number: $ IPL2JN $ . of the transient the temperature will be equal to the re Tabular or Control Function with the following $\leq T_{sat}$ . must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-3 (I) :	IGS2JN(1)	Pointer to a Tabula of gas 1 flowing t fraction will be d number: IGS2JN. If by a Control Funct given time of the tra- value of the Tabula $\leq X(1) \leq 1.0.$ <i>Acceptable range:</i> <i>Default value:</i>	r or Control Function that defines the mole fraction hrough the junction. If the number is positive, the efined by a Tabular Function with the reference f the number is negative, the fraction will be defined ion with the reference number: $ IGS2JN $ . At any ansient the mole fractions will be equal to the current ar or Control Function with the following limits: 0.0 must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-4 (I) :	IGS2JN(2)	The same for gas must either be spec	umber 2. Note that the user-defined gas mole fraction ified for all gases or none.

(...) until all gases are defined. Normalization is performed to ensure that sum of all fractions is equal to 1.0.

#### 2.2.16 Records: 240XXX, **Flow Composition Parameters**

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

The user can influence the composition of gas flowing through Junctions using these records. The Flow Composition Parameters (FCP) may be defined for each gas by those records. If those records are not present then the gas composition will always be equal to the gas composition in the upstream Control Volume, at the elevation of the Junction. If the FCP are entered then the volume fractions for each gas are multiplied by the FCP for this gas and divided by the sum of FCP for all gases. Using the FCP the user can introduce additional conservatism into the analysis. For example in BWR containments the steam flow through vacuum breakers can be restricted, which will typically result in higher containment pressures. Several records with the same number may be entered. Each record defines FCP for one gas. Flow Composition Parameters are applied only for the atmosphere gases and not for the bubble gases.

W-1 (I) :	IGAS	Gas number, (-). Must be one of the available gases. The built-in gases are: $1 = H_2$ , $2 = He$ , $3 =$ steam, $4 = N_2$ , $5 = O_2$ , $6 = CO_2$ . Acceptable range: $1 \le IGAS \le NGASCV \le NGMXFL = 20$ Default value: none.
W-2 (I) :	IFCPJN	Indicator for Flow Composition Parameter (FCP) for gas IGAS. If IFCPJN is zero then the FCP for this gas is equal to 1.0. If the number is

positive then the Tabular Function IFCPJN will define the FCP for this gas. If it is negative the FCP will be defined by the Control Function – IFCPJN. The following limits are imposed on the values of FCP:  $1.0 \times 10^{-3} < FCP < 1.0 \times 10^{3}$ . If the value obtained from the Tabular or Control Function is outside this range it will be set to the nearest value within the range. If FCP are used then the gas composition in Junction is determined as:

$$v_{i,JN} = \frac{v_{i,CV} \cdot FCP_i}{\sum_{k=1}^{N_{GAS}} v_{k,CV} \cdot FCP_k}$$

where:  $v_{i, JN}$  is the volume fraction of gas i in the Junction,  $v_{k, CV}$  is the volume fraction of gas k in the upstream CV, at the Junction elevation, *FCP*<sub>k</sub> is the Flow Composition Parameter for the gas k.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero.

Default value:

#### 2.2.17 Records: 250XXX, Entrainment Indicators

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version). The use of the entrainment indicators is explained in Volume 1, in the section describing the equation of mass conservation.

0.

W-1 (R) : ENTRJN(1) Entrainment indicator for atmosphere flow,  $E_{atms}$ . If  $E_{atms}$ =0.0 then the JN atmosphere flow is deposited in atmosphere of the receiving CV, as long as the liquid level in the receiving CV is below the top of the Junction. When the liquid level is above the top of the Junction then the atmosphere flow is a source of bubbles in the receiving CV. If  $E_{atms}$ =1.0 then part of the JN atmosphere flow is entrained into pool as bubbles, whenever the pool level in the receiving CV is above the pool level in the Junction. Note that bubbles are created in the receiving CV only when the bubble model is activated for that volume (IBUBCV=2 - see record 155XXX).

Acceptable range: $0.0 \le \text{ENTRJN}(1) \le 1.0$ Default value:0.0

W-2 (R) : ENTRJN(2) Entrainment indicator for droplet flow,  $E_{drop}$ . If  $E_{drop}$ =0.0 then the JN droplet flow is deposited in the pool of the receiving CV, as long as the liquid level in the receiving CV is above the bottom of the Junction. When the liquid level is below the bottom of the Junction then the droplet flow is a source of droplets in the receiving CV. If  $E_{drop}$ =1.0 then part of the JN droplet flow is entrained into atmosphere, already when the pool level in the receiving CV is below the top of the Junction. Note that droplets are created in the receiving CV only when the droplet model is activated for that volume (IDRPCV=2 - see record 155XXX).

Acceptable range: $0.0 \le \text{ENTRJN}(2) \le 1.0$ Default value:1.0 (a small number,  $<10^{-50}$ , sets the value to 0).

- W-3 (R) : ENTRJN(3) Entrainment indicator for pool flow,  $E_{pool}$ . If  $E_{pool}=0.0$  then the JN pool flow is deposited in the pool of the receiving CV, as long as the liquid level in the receiving CV is above the bottom of the Junction. When the liquid level is below the bottom of the Junction then the pool flow is a source of droplets in the receiving CV. If  $E_{pool}=1.0$  then part of the JN pool flow is entrained into atmosphere as droplets, whenever the pool level in the receiving CV is below the pool level in the Junction. Note that droplets are created in the receiving CV only when the droplet model is activated for that volume (IDRPCV =2 see record 155XXX). Acceptable range:  $0.0 \leq \text{ENTRJN3} \leq 1.0$  Default value: 0.0.
- W-4 (R) : ENTRJN(4) Entrainment indicator for bubble flow,  $E_{bubb}$ . If  $E_{bubb}$ =0.0 then the JN bubble flow is deposited in the atmosphere of the receiving CV, as long as the liquid level in the receiving CV is below the top of the Junction. When the liquid level is above the top of the Junction then the bubble flow is a source of bubbles in the receiving CV. If  $E_{bubb}$ =1.0 then part of the JN bubble flow is entrained into pool, already when the pool level in the receiving CV is above the bottom of the Junction. Note that bubbles are created in the receiving CV only when the bubble model is activated for that volume (IBUBCV=2 see record 155XXX). Acceptable range:  $0.0 \le \text{ENTRJN4} \le 1.0$  Default value: 1.0 (a small number, <10<sup>-50</sup>, sets the value to 0).

#### 2.2.18 Records: 251XXX, Drop Flow Regime Model Parameters

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (R) :	C0VAJN	Constant $C_0$ for a velocity (see Volum $_{\nu A}$ , (-).	rift flux model for Junction atmosphere, vertical ne 1). This is the value denoted in Volume 1 as: $C_{0,1}$		
		Acceptable range:	$0.0 \le \text{COVAJN} \le 10.0$ . If no value or zero is entered, then $C_{0, vA}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.		
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0		
W-2 (R) :	VIVAJN	Terminal velocity, vertical velocity (se as: $v_{xy}$ , (m/s).	$v_{\infty}$ , for drift flux model for Junction atmosphere, ee Volume 1). This is the value denoted in Volume 1		
		Acceptable range:	$-100.0 \le \text{VIVAJN} \le 100.0$ . If no value or zero is entered, then $v_{\alpha\nu, A}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.		
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $v_{\infty}$ to 0.0		

W-3 (R) :	XVAJN	Exponent $x$ for drift flux model for Junction atmosphere, vevelocity (see Volume 1). This is the value denoted in Volume 1 as (-).	
		Acceptable range:	$0.0 \le \text{XVAJN} \le 10.0$ . If no value or zero is entered, then $x_{v,A}$ is calculated by the Drop Flow Regime Model.
		Default value:	0.0
W-4 (R) :	COHAJN	Constant $C_0$ for drivelocity (see Volum hA, (-).	tift flux model for Junction atmosphere, horizontal me 1). This is the value denoted in Volume 1 as: $C_{0,}$
		Acceptable range:	$0.0 \le \text{COHAJN} \le 10.0$ . If no value or zero is entered, then $C_{0,hA}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0
W-5 (R) :	VIHAJN	Terminal velocity, horizontal velocity 1 as: $v_{\pi h A}$ (m/s).	$v_{\infty}$ , for drift flux model for Junction atmosphere, (see Volume 1). This is the value denoted in Volume
		Acceptable range:	$-100.0 \le$ VIHAJN $\le 100.0$ . If no value or zero is entered, then $v_{\alpha h,A}$ is calculated by the Drop Flow Regime Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-6 (R) :	XHAJN	Exponent <i>x</i> for dr velocity (see Volur (-).	ift flux model for Junction atmosphere, horizontal me 1). This is the value denoted in Volume 1 as: $x_{h,A}$ ,
		Acceptable range:	$0.0 \le \text{XHAJN} \le 10.0$ . If no value or zero is entered, then $x_{h,A}$ is calculated by the Drop Flow Regime Model.
		Default value:	0.0
W-7 (I) :	IDFAJN	Droplet flow activa = 0: droplet flow ≠ 0: droplet flow Acceptable range: Default value:	ator: through junctions is possible through junctions is not possible any integer 0

#### 2.2.19 Records: 252XXX, Bubbly and Annular Flow Parameters

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (R) :	COVPJN	Constant $C_0$ for dri	ft flux model for Junction pool, vertical velocity (see
		Volume 1). This is	the value denoted in Volume 1 as: $C_{0,\nu P}$ , (-).
		Acceptable range:	$0.0 \le \text{COVPJN} \le 10.0$ . If no value or zero is entered,
			then $C_{0,v,P}$ is calculated by the Bubbly Flow Regime
			Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0

W-2 (R) :	VIVPJN	Terminal velocity, velocity (see Volum (m/s)	$v_{\infty}$ , for drift flux model for Junction pool, vertical ne 1). This is the value denoted in Volume 1 as: $v_{\alpha,\nu,P}$ ,
		Acceptable range:	$-100.0 \le \text{VIVPJN} \le 100.0$ . If no value or zero is entered, then $v_{\alpha,\nu,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1.
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-3 (R) :	XVPJN	Exponent <i>x</i> for drift Volume 1). This is <i>Acceptable range:</i>	It flux model for Junction pool, vertical velocity (see the value denoted in Volume 1 as: $x_{v,P}$ , (-). $0.0 \le \text{XVPJN} \le 10.0$ . If no value or zero is entered, then $x_{v,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1.
		Default value:	0.0.
W-4 (R) :	COHPJN	Constant $C_0$ for dr (see Volume 1). The Acceptable range:	ift flux model for Junction pool, horizontal velocity is is the value denoted in Volume 1 as: $C_{0,hP}$ , (-). $0.0 \le \text{COHPJN} \le 10.0$ . If no value or zero is entered, then $C_{0,hP}$ is calculated by the Bubbly Flow Regime Model as described in Volume 1
		Default value:	0.0, a small value ( $\leq 10^{-50}$ ) value will set $C_0$ to 0.0
W-5 (R) :	VIHPJN	Terminal velocity, velocity (see Volum (m/s).	$v_{\infty}$ , for drift flux model for Junction pool, horizontal ne 1). This is the value denoted in Volume 1 as: $v_{\infty h,P}$ ,
		Acceptable range: Default value:	$-100.0 \le \text{VIHPJN} \le 100.0$ . If no value or zero is entered, then $v_{\infty,h,P}$ is calculated by the Bubbly Flow Regime Model, as described in Volume 1. 0.0, a small value ( $\le 10^{-50}$ ) value will set $v_{\infty}$ to 0.0
W-6 (R) :	XHPJN	Exponent <i>x</i> for dri (see Volume 1). The <i>Acceptable range:</i>	ft flux model for Junction pool, horizontal velocity is is the value denoted in Volume 1 as: $x_{h,P}$ , (-). $0.0 \le \text{XHPJN} \le 10.0$ . If no value or zero is entered,
		Default value:	Model, as described in Volume 1. 0.0.
W-7 (I) :	IANNJN	Annular flow mode =1: Default mod =2: Dartmouth c Acceptable range: Default value:	el selection. lel, see Volume 1. correlation, see Volume 1. 1 or 2. 1.
W-8 (I) :	IBFAJN	Bubble flow activa = 0: bubble flow $\neq$ 0: bubble flow Acceptable range: Default value:	tor: through junctions is possible through junctions is not possible any integer 0

#### 2.2.20 Records: 253XXX, Plume Model for Junction Flows

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

These records activate plume models for the material flowing through the Junction. The plume model is used in Control Volumes in which stratification is calculated. Thus, it will be used only if there is stratification model active in one (or both) Control Volumes connected by this Junction. A description of the plume model is given in Volume 1. To activate the model for a single component, a set of two integer numbers, described below, must be entered. To activate the model for two components, two sets of pairs should be entered in this record.

W-1 (I) :	J	Identifier of component, for which the plume model is desired. J=1: atmosphere; J=3: pool. <i>Acceptable range:</i> J=1, or J=3. <i>Default value:</i> none.
W-2 (I) :	IPLMJN	Plume model activator. If IPLMJN = 0 then the plume model is not active. If IPLMJN $\neq$ 0 then the plume model is active for the component J and Junction XXX. Note that the plume model is used only when stratification models are active in Control Volumes. The plume model will be deactivated if Junction velocities exceed certain limits (see section 2.1.27). Acceptable range: any integer. Default value: 0.

... etc., until all plumes are defined.

#### 2.2.21 Records: 255XXX, Counter-current Flow Model Constants

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (R): CCFVJN Counter-current flow constant for vertical flow,  $C_{cf, v}$ . The countercurrent flow limit is defined by the equation:

$$\alpha = \frac{|v_g|}{|v_g| + |v_l| \cdot C_{cf,v}}$$

where  $\alpha$  is a void fraction,  $v_g$ ,  $v_l$  are the gas and liquid velocities respectively. Generally, a larger value of CCFVJN causes smaller flow resistance in counter-current flow. A large value ( $\geq 10^9$ ) eliminates the counter current flow.

Acceptable range: $10^{-10} \le \text{CCFVJN} \le 10^{10}$ Default value:0.1

W-2 (R): CCFHJN Counter-current flow constant for horizontal flow,  $C_{cf. h}$ . The countercurrent flow limit is defined by the equation:

$$\alpha = \frac{|v_g|}{|v_g| + |v_l| \cdot C_{cf,h}}$$

where  $\alpha$  is a void fraction,  $v_g$ ,  $v_l$  are the gas and liquid velocities respectively. Generally, a larger value of CCFHJN causes smaller flow resistance in counter-current flow. A large value ( $\geq 10^9$ ) eliminates the counter current flow.

Acceptable range: $10^{-10} \le \text{CCFHJN} \le 10^{10}$ Default value:10.0

#### 2.2.22 Records: 256000, Diffusion Model - Global Activator

W-1 (I) :	JDIFJN	Global indicator for diffusion calculation in junction. = 1: diffusion is not calculated = 2: diffusion is calculated. If activated, diffusion is calculated for a gas flow through a junction. Diffusion does not result in a net flow but only in change of gas concentrations. A description of the diffusion model is provided in Volume 1. Diffusion is only important in case of a very small velocity in a junction. The diffusion calculation is automatically turned off in those junctions where the gas velocity is higher than a certain limit (set by the input parameter VMDFJN). <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 1
W-2 (I) :	LDIFJN	Request for diffusion plot parameters = 1: diffusion plot parameters not requested = 2: diffusion plot parameters requested If diffusion parameters are requested, then the volume change due to diffusion is available in the plot file as JN-xxx-VDif-yyyy, where xxx is the junction number and yyyy is the gas name. In such case the plot parameters replace the default parameters JN-xxx-Cgas-yyyy (Table 2-24). The diffusion volume change is always available in the output file *.OUT. Acceptable range: 1 or 2 Default value: JDIFJN

#### 2.2.23 Records: 256XXX, Diffusion Model - Individual Activators

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The Junction reference numbers, XXX, need not be consecutive. The maximum number of Junctions is 600 (999 in LINUX version).

W-1 (I) :	IDIFJN	Indicator for diffusion calculation in junction.
		= 1: diffusion is not calculated
		= 2: diffusion is calculated.

		If activated, diffusion is calculated for a gas flow through a junction. Diffusion does not result in a net flow but only in change of gas concentrations. A description of the diffusion model is provided in Volume 1. Diffusion is only important in case of a very small velocity in a junction. The diffusion calculation is automatically turned off in those junctions where the gas velocity is higher than a certain limit (set by the input parameter VMDFJN). The model is applied to CV gases, defined in the FL Package. It may also be applied for the fission product vapours, defined in the RT Package. To do so; the user must supply the diffusion volumes (SGFPRT, record 886XXY), needed to calculate diffusion coefficients. <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> JDIFJN
W-2 (R) :	X1DFJN	Diffusion length in the 'from-CV', $L_{from-CV}$ , (m).Acceptable range: $10^{-4} \le X1DFJN \le 10^{10}$ Default value:FRLNJN/2.0 (half of the friction length)
W-3 (R) :	X2DFJN	Diffusion length in the 'to-CV', $L_{to-CV}$ , (m).Acceptable range: $10^{-4} \le X2DFJN \le 10^{10}$ Default value:FRLNJN/2.0 (half of the friction length)

### 2.2.24 Records: 260000, Options for Critical Velocity, Elevation and Area Checking

The options below are applied to all Junctions.

W-1 (R) :	VMCFJN	Velocity below which the critical flow calculation is bypassed, (m/s).Acceptable range: $0.0 < VMCFJN \le 1.0 \times 10^6$ Default value:10.0
W-2 (I) :	ICELJN	<ul> <li>Elevation checking option.</li> <li>=-1: Check elevations close to CV bottom or top. Adjust JN elevations and CV heights if needed. This option, or option +1, should be used for two-phase systems.</li> <li>=+1: Check elevations close to CV bottom or top. Adjust JN elevations if needed. This option, or option -1, should be used for two-phase systems.</li> <li>=+2: Do not check nor adjust elevations close to CV bottom or top. This option can be used for single-phase (pure gas) systems.</li> <li>Acceptable range: -1, 1, 2</li> <li>Default value: 1</li> </ul>
W-3 (I) :	ICVAJN	<ul> <li>CV horizontal and vertical area (AHORCV, AVERCV, record 111XXX) checking option. In general any of these flow areas should not be smaller than the largest flow area of the Junctions connected to a given CV. If the user wishes to apply smaller flow areas, he must allow the code to accept such input by setting the value to 2.</li> <li>=1: CV horizontal or vertical area smaller than the largest flow area of the junctions connected to the given CV is flagged as an error and is not accepted for calculations.</li> </ul>

		=2: CV horizontal or vertical area smaller than the largest flow area
		=3: CV areas are modified automatically by the code.
		(A) If CV vertical area (AVERCV) is smaller than the maximum
		flow area of all horizontal junctions connected to this CV, then it
		is set to the maximum JN area.
		(B) If CV horizontal area (AHORCV) is smaller than the
		maximum flow area of all vertical junctions connected to this CV,
		-4. Junction flow group are modified outomatically by the code
		-4. Junction now area of a vertical junction is larger than the
		minimum horizontal flow area of the two connected CV-s, the
		junction area is set to the smaller CV horizontal area.
		B) If the flow area of a horizontal junction is larger than the
		smaller of the minimum vertical flow area of the two connected
		CV-s, the Junction area is automatically set to the smaller CV
		horizontal area.
		Acceptable range: 1, 2, 3, 4 Default value: 1
W-4 (R) :	HMINJN	Minimum distance between bottom of CV and JN bottom, (m). Used when the elevation checking option is set (ICELJN<2). If the JN bottom
		elevation, calculated from the JN level and JN height specified in the
		input deck, is lower than the limit imposed by this value, it is
		automatically reset by the code. A comparison $0.0 \le HMININ \le 1.0 \times 10^{-2}$
		Default value: $1.0 \times 10^{-4}$
W-5 (R) :	HMAXJN	Minimum distance between top of JN and CV top, (m). The value should be consistent with the parameter HMAXCV. Used when the elevation checking option is set (ICELJN<2). If the JN top elevation, calculated from the JN level and JN height specified in the input deck, is higher than the limit imposed by this value, it is automatically reset by the code. <i>Acceptable range:</i> $0.0 < HMAXJN \le 5.0 \times 10^{-2}$ <i>Default value:</i> $1.0 \times 10^{-2}$
W-6 (R) :	VMDFJN	Velocity above which the diffusion mass transfer calculation is
		bypassed, (m/s). See the input parameter IDIFJN.
		Acceptable range: $1.0 \times 10^{-3} < \text{VMDFJN} \le 1.0 \times 10^{-1}$
		Default value: 1.0×10 <sup>-2</sup>
W-7 (R) :	XMDFJN	Interpolation range for the diffusion mass transfer calculation. The
		velocity-dependent multiplier is defined as: $-1.0$ for the gas velocity $v_{\perp} < VMDEIN \times XMDEIN$
		= 0.0 for the gas velocity $v_{gas} > VMDFJN$
		= $(\text{VMDFJN} - v_{gas}) / (\text{VMDFJN} - \text{VMDFJN} \times \text{XMDFJN})$
		Acceptable range: $0.1 < \text{XMDFJN} \le 0.9$
		Default value: 0.5

#### 2.2.25 Records: 261000, Minimum Reynolds Number for Friction Calculation

The value below is applied to all Junctions.

W-1 (R) : REMNJN Minimum Reynolds number for friction calculation,  $Re_{\min}$  (-). In the laminar range the friction factor is calculated from:

$$f = \frac{64}{Re}$$

A limit is imposed on the Reynolds number:  $Re < Re_{min}$ . With the default value, the friction factor is not larger than 10.0. The limit must be decreased to analyze low velocity flows, for which Re < 6.4. Acceptable range:  $6.4 \times 10^{-2} < VMCFJN \le 6.4 \times 10^{2}$ Default value: 6.4

#### 2.2.26 Records: 262000, User-Defined Critical Flow Model

This record activates the user-defined critical flow model. The model is intended to be applied for alternative liquids or sensitivity calculations. If defined, the values below are applied to all Junctions.

W-1 (I): ITFGJN Tabular Function,  $f_{gas}$ , defining the critical velocity for the gas phase. The TF value gives critical velocity,  $c_{gas}$  (m/s), as a function of gas temperature,  $T_{gas}$  (K):

$$c_{gas} = f_{gas}(T_{gas})$$

The following limits are imposed on the value obtained from the Tabular Function:  $10.0 \le c_{gas} \le 10^6$  m/s.

Acceptable range: 0 or reference to a Tabular Function. A positive value must be used in case of alternative fluid (IFLDFL>1)

*Default value:* 0

W-2 (I): ITFLJN Tabular Function,  $f_{liq}$ , defining the critical velocity for the liquid phase. The TF value gives the the critical velocity,  $c_{liq}$  (m/s), as a function of liquid temperature,  $T_{liq}$  (K):

$$c_{liq} = f_{liq}(T_{liq})$$

0

The following limits are imposed on the value obtained from the Tabular Function:  $100.0 \le c_{liq} \le 10^6$  m/s.

Acceptable range: 0 or reference to a Tabular Function. A positive value must be used in case of alternative fluid (IFLDFL>1)

Default value:

### 2.2.27 Records: 263000, Friction Model Global Activators

This records specifies default values of the friction model parameters. The default values can be redefined for each individual junction in the records 210XXX.

W-1 (R) :	RFFGJN	Empirical coefficient in the Griffith-Rohsenow correlation for the two- phase form loss factor multiplier, $r_f$ , forward flow, (-). Values of $r_f$ are shown in Table 2-2. The multiplier is equal to: $1.0 + r_f \cdot X \cdot v_{fg} / v_f$ . <i>Acceptable range:</i> $0.0 \le \text{RFFGJN} \le 10^3$ <i>Default value:</i> 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0)
W-2 (R) :	RFRGJN	Empirical coefficient in the Griffith-Rohsenow correlation for the two- phase form loss factor multiplier, $r_f$ , reverse flow, (-). Values of $r_f$ are shown in Table 2-2. The multiplier is equal to: $1.0 + r_f \cdot X \cdot v_{fg} / v_f$ . <i>Acceptable range:</i> $0.0 \le \text{RFRGJN} \le 10^3$ <i>Default value:</i> 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0)
W-3 (R) :	CMGJN	Moody coefficient for liquid flow, $C_M$ , (-). The value of CMJN is applied for pure liquid flow ( <i>X</i> =0.0). For <i>X</i> >0 the value is interpolated, to give 1.0 when <i>X</i> =1.0. Thus, the effective multiplier on the critical flow is equal to: $C_M + X \cdot (1 - C_M)$ , see Volume 1. The best estimate value is 0.7 (Volume 3). <i>Acceptable range:</i> $0.1 \le \text{CMGJN} \le 1.0$ <i>Default value:</i> 0.7
W-4 (I) :	MODGJN	Model to calculate friction factor, f, (-), (see Volume 1),= 1 :non-uniform roughness, Colebrook-White formula,= 2 :uniform roughness, Nikuradse formula,= 3 :simplified method, Blasius and Prandtl-Nikuradse,= 11 :non-uniform roughness, Beluco-Camano formula= 12 :non-uniform roughness, Churchill formulaAcceptable range:MODGJN = 1, 2, 3, 11, 12Default value:11
W-5 (I) :	M2PGJN	Model to calculate two-phase friction multiplier, $\Phi_f^2$ , (-), (see Vol. 1),= 1 :no two-phase multiplier,= 2 :Hancox-Nicoll model,= 3 :Levy Model.> 1000: $\Phi_f^2$ is given by a Tabular Function with the number: (M2PFJN - 1000). The argument is void fraction. The range of independent argument (void fraction) must cover the range from 0.0 to 1.0, inclusive. The TF value must be =1.0 for the void fraction of 0.0 and >1.0 for void fractions >0.0.Acceptable range:M2PGJN = 1, 2, or 3. Default value:
W-61 (R) :	CLAGJN	Correction factor for non-circular tubes, $C_{lam}$ . It may also be used as a multiplier for wire-wrapped rods. The friction factor in laminar flow is obtained from:

$$f_{wall} = \frac{64 \cdot C_{lam}}{\text{Re}}$$

Rectangular channel, dimensions 0.0 < b/a < 1.0 [10] (Dia. 2-6) $C_{lam} = 1.50$  $b/a \rightarrow 0.0$  $C_{lam} = 0.89$  $b/a \rightarrow 1.0$  (square)Tube bundle, pitch-to-diameter ratios 1.0 < (P/D) < 1.5 [10] (Dia. 2-9): $C_{lam} = 0.89 \cdot (P/D) + 0.63$ triangular pitch $C_{lam} = 0.96 \cdot (P/D) + 0.63$ rectangular pitchFor wire-wrapped rods, Engel correlation [50] gives: f = 110/Re, so  $C_{lam}$ = 1.50 / 64 = 1.718Acceptable range: $0.1 \le CLAGJN \le 10.0$ Default value:1.0

W-7 (R): CTUGJN Friction factor multiplier for turbulent flow. Applicable for example for wire-wrapped rod assemblies in fast reactors. For wire-wrapped rods, Engel correlation [50] gives:  $f = 0.55/Re^{0.25}$ , so compared to the smooth friction factor (Blasius):  $f = 0.316/Re^{0.25}$ ,  $C_{lan} = 0.55 / 0.316 = 1.741$ . A good overview of correlations: [51]. Acceptable range:  $0.1 \le \text{CTUGJN} \le 10.0$ Default value: 1.0

#### 2.2.28 Records: 264000, Momentum Length, Friction Length Options

The momentum length, XLENJN is defined in the record 200XXX. In case of liquid-full volumes the momentum length is automatically reduced by the program is to the minimum value, defined in this record.

W-1 (R) :	XLMNJN	Minimum momentum length for junctions connecting Control Volumesthat are filled with liquid.Acceptable range: $0.01 \le XLMNJN \le 100.0$ Default value: $0.05$
W-2 (I) :	IMFLJN	Option to calculate the momentum length (XLENJN) and the friction length (FRLNJN) automatically by the code: = 0: momentum and friction length are defined by the user, = 1: momentum and friction length are calculated by the code from the recommended formulae (see description of XLENJN and FRLNJN) if XLENJN and FRLNJN are entered as 0.0. If a positive value of XLENJN or FRLNJN is entered, it is compared to the recommended value. If the relative difference is larger than 0.1, a warning message is printed. = 2: momentum and friction length are always calculated by the code from the recommended formulae (see description of XLENJN and FRLNJN), independently of the values entered. <i>Acceptable range:</i> 0, 1, 2 <i>Default value:</i> 0

### 2.2.29 Records: 265000, Hydraulic Diameter - JN Versus CV

W-1 (I): IDHDJN Option to calculate the CV hydraulic diameter (DHYDCV) based on JN hydraulic diameter (DIAMJN).
= 1: option not used. DHYDCV is defined by the user. If no value is defined, then the default value is used.
= 2: option used. With this option DHYDCV is compared to the junction diameter, DIAMJN. If DIAMJN < DHYDCV, then DHYDCV is set to DIAMJN. This option is consistent with SPECTRA version of April 2023 or earlier.</li>
Acceptable range: 1, 2
Default value: 1

#### 2.2.30 Records: 270000, Solution of the Junction Flow Matrix

The "Junction Flow Matrix" (see Volume 1, Chapter 2) is used to calculate flows through all Junctions. The dimension of the matrix is equal to the number of active Junctions (all Junctions except for closed valves, Junctions with tabular flow control and critical Junctions). If the dimension is small then a typical method of matrix solution (L-U decomposition - see Volume 1) is preferable. For matrices of large dimension the bi-conjugate gradient method is available.

W-1 (I) :	MSFMJN	Method of solving the flow matrix dimension. 1 = only the Full Flow Matrix (FFM) is solved. 2 = the Full Flow Matrix is solved in the first iteration, subsequently the Limited Flow Matrix (LFM) is solved. Acceptable range: 1, 2 Default value: 1
W-2 (I) :	IMSFJN	<ul> <li>Indicator of the Junction Flow Matrix solution frequency.</li> <li>1 = Junction Flow Matrix is solved at the beginning of a time step.</li> <li>2 = Junction Flow Matrix is re-solved during iterations.</li> <li>Acceptable range: 1, 2; any other entry is set to the default value Default value: 2</li> </ul>
W-3 (I) :	MXFSJN	Maximum number of Junction flow matrix solutions per time step. Usedif IMSFJN (Word 2 above) is equal to 2.Acceptable range: $2 \le MXFSJN \le 10$ Default value: $2$
W-4 (R) :	XCFMJN	Minimum velocity for $C_f$ and $C_i$ calculation, (m/s), (see Volume 1). Acceptable range: $10^{-6} \le \text{XCFMJN} \le 0.1$ . Default value: $10^{-3}$ .
W-5 (R) :	CLCMJN	Multiplier in the time step limit for gas composition change. The time step is limited if the gas composition in any Junction at the end of the time step is very different than at the beginning of the time step. This limit is specifically important in case of explicit definition of the

Junction donor quantities (IMPLJN = 2, Word 11 below). The time step is limited to:

$$\Delta t = CLCMJN \times Min\left(\frac{c_i}{\left|c_i - c_i^0\right|}\right) \Delta t'$$

where: $c_i^0$ -mass fraction of gas i, end of time step, $c_i^0$ -mass fraction of gas i, start of time step, $\Delta t'$ -previous value of time step, (s).Acceptable range: $0.0 < \text{CLCMJN} \le 1.0$ Default value:0.1

W-6 (R): CLMAJN Multiplier in the mass change limit for the atmosphere gas transport (Courant Limit for gas flow - see also word 12 below). The time step is limited if the gas mass flows through Junctions are large, compared to the gas mass in a Control Volume. The time step is limited to:

$$\Delta t = CLMAJN \times Min\left(\frac{M_{atms}}{Max(|W_{atms}|)}\right)$$

where:

 $M_{atms}$  - mass of gas in a Control Volume (kg),  $W_{atms}$  - gas flow through a Junction connected to the Control Volume, (kg/s). Maximum is taken over all Junctions connected to the given Control Volume.

Acceptable range: $0.0 < \text{CLMAJN} \le 1.0$ Default value:0.50

W-7 (R): CLCEJN Multiplier in the energy transfer time step limit. The time step is limited if the energy transfer in or from a Control Volume is large, compared to the gas heat capacity in a Control Volume. The time step is limited to:

$$\Delta t = CLCEJN \times Min\left(\frac{M_{CV}c_p\Delta T_{max}}{|Q_{atms}|}\right)$$

where:	$M_{CV}$	-	mass of gas in Control Volume (kg),
	$C_p$	-	specific heat of the atmosphere gas, (J/kg/K).
	$\Delta T_{max}$	-	maximum temperature change (=100 K).
	$Q_{atms}$	-	total heat in or out the atmosphere of the
			Control Volume, (W).
Acceptable	e range:	0.0 <	$CLMMJN \le 10.0$
Default va	lue:	1.0	

W-8 (R): CLCPJN Multiplier in the volume flow change limit for compressors and pumps. The criterion applied for all Type 1 Pump/Compressor (see section 2.2.8) Junctions is:

$$\Delta t = CLCPJN \times Min\left(\frac{1}{Max(R_{atms,JN}, R_{pool,JN})}\right)$$

 $R_{atms, JN}$ 

where:

maximum rate of change of atmosphere flow through the compressor (1/s), = RCAPJN (see 2.2.8),

R<sub>pool</sub> IN

maximum rate of change of pool flow through the pump (1/s), = RCPPJN (see section 2.2.8).

The criterion applied for those Type 2 Pump/Compressor (see section 2.2.8) for which moment of inertia is used to calculate the speed, is:

$$\Delta t = CLCPJN \times \frac{I \,\omega_N \,\Delta\omega}{Q}$$

where:

Default value:

moment of inertia,  $(kg \cdot m^2)$ . Ι nominal speed,  $(s^{-1})$ . \_  $\omega_N$ speed change, (s<sup>-1</sup>), taken equal to 10% of  $\omega_N$ .  $\Delta \omega$ -Q current power, (W). Acceptable range:  $0.0 < \text{CLCPJN} \le 10.0$ 1.0

Multiplier in the velocity change limit. The velocity change limit may CVCLJN be activated if the change of velocities in the last two time advancements are in the opposite directions (oscillating velocities). The time step is limited to:

$$\Delta t = CVCLJN \times Min\left(\frac{\Delta v_2}{\Delta v_1}\right) \cdot \Delta t'$$

where:  $\Delta v_1$ = $v_k - v_{k-1}$ ,  $\Delta v_2 =$  $v_{k-1} - v_{k-2}$ , velocity at *k*-th (last) advancement, (m/s),  $v_k$ *Vk*–1 – velocity at k-1 advancement, (m/s), velocity at k-2 advancement, (m/s), - $V_{k-2}$ \_ previous value of the time step, (s).  $\Delta t'$ 

The limit is activated only if  $\Delta v_1 > \text{CVCLJN} \times \Delta v_2$ , and if the absolute value of either  $v_{k-1}$  or  $v_{k-2}$  is larger than the minimum velocity, defined by the Word 10 below.

Acceptable range:  $0.0 < \text{CVCLJN} \le 1.0$ Default value: 0.5.

W-10(R): **VVCLJN** Minimum velocity to apply velocity change limit (m/s) (see Word 9 above). Acceptable range:  $0.0 < VVCLJN \le 1000.0$ . Default value: 10.0. If density stratification is active in any Control Volume (IDSPCV $\neq$ 0) and the link with thermal stratification is not used (DTSPCV<0.0 - see section 2.1.2), or if compressors with surge factor CDSPJN<0.1 (section 2.2.8) are used, then the default value is 1000.0. This means in practice that no velocity change limit is applied. This setting was motivated by observation that strong stratification may sometimes lead to oscillations in flow solution, which have little effect on the overall results. To avoid time step cuts in such cases, the velocity change limit is suppressed.

- W-11 (I): IMPLJN Method of calculating donor quantities in the Junction flow solution matrix. If the value is 1 then the donor quantities (gas compositions, temperatures) are implicit (end of time step value). This may require a very large number of iterations if the number of Junctions is significant. If IMPLJN = 2 then the explicit formulation is used and the donor quantities are defined by the beginning of time step values. *Acceptable range:* 1, 2. *Default value:* 2.
- W-12 (R): CLMPJN Multiplier in the mass change limit for the pool transport (Courant Limit for liquid flow see also Word 6 above). The time step is limited if the liquid mass flows through Junctions are large, compared to the liquid mass in a Control Volume. The time step is limited to:

$$\Delta t = CLMPJN \times Min\left(\frac{M_{pool}}{Max(|W_{pool}|)}\right)$$

 $M_{pool}$  -  $W_{pool}$  -

where:

mass of liquid in a Control Volume (kg), liquid flow through a Junction connected to the Control Volume, (kg/s). Maximum is taken over all Junctions connected to the given Control Volume.

Acceptable range: $0.0 < \text{CLMPJN} \le 1.0$ Default value:CLMAJN (Word 6 above).

W-13 (I): IACCJN Acceleration pressure drop calculation. The acceleration pressure drop is calculated from:

$$\Delta p_{acc} = \frac{\rho \left( v_D^2 - v_U^2 \right)}{2}$$

where  $v_U$ ,  $v_D$  are the average velocities in the upstream and the downstream Control Volumes respectively.

- 1: acceleration pressure drop not included (compatible with SPECTRA Version 2.00 and earlier).
- 2: acceleration pressure drop included for atmosphere flow only.
- 3: acceleration pressure drop included for pool flow only.
- 4: acceleration pressure drop included for atmosphere and pool flows. *Acceptable range:* 1, 2, 3, 4

		Default value: 4
W-14 (I) :	INTFJN	Interface friction calculation. 1 : interface friction not calculated 2 : interface friction calculated Acceptable range: 1, 2 Default value: 2
W-15 (I) :	INRTJN	<ul> <li>Inertial "pressure drop" calculation in the Limited Flow Matrix.</li> <li>1 : inertial "pressure drop" reduced by with user-defined reduction factors, defined by the next two words.</li> <li>2 : inertial "pressure drop" calculated without the reduction factors.</li> <li>Acceptable range: 1, 2</li> <li>Default value: 1</li> </ul>
W-16 (R) :	ALFMJN	Reduction factor for atmosphere flow. Used if INRTJN =1.Acceptable range: $1.0 \times 10^{-4} \le ALFMJN \le 1.0$ Default value: $1.0$
W-17 (R) :	PLFMJN	Reduction factor for pool flow. Used if INRTJN =1. Acceptable range: $1.0 \times 10^{-4} \le PLFMJN \le 1.0$ Default value: $1.0 \times 10^{-2}$
W-18 (I) :	ILFMJN	<ul> <li>Immediate time step request activator in case the discrepancy between the velocities calculated by the Full Flow Matrix and the Limited Flow Matrix are larger than 50% or values have different signs</li> <li>1 : a request for an immediate time step cut is send to the numerical Solver Package,</li> <li>2 : a request for an immediate time step cut is NOT send.</li> <li>Acceptable range: 1, 2</li> <li>Default value: 2</li> </ul>
W-19 (R) :	CLCDJN	Multiplier in droplet flow time limit (Courant Limit for droplet flow). The time step is limited if the droplet vertical velocity and vertical height of Control Volume. The time step is limited to:
		$\Delta t = CLCDJN \times \left(\frac{H_{CV}}{v_{drop}}\right)$

where:	$H_{CV}$	-	height of a Control Volume (m),
	$V_{drop}$	-	droplet vertical velocity (m/s)
Acceptable	e range:	0.00 <	$<$ CLCDJN $\le 100.0$
Default va	lue:	1.00	

#### 2.2.31 Example of the Junction Data

The example input of Junction data given below defines a check valve Junction, JN-150, named "Example Junction", allowing flow from CV-200 to CV-100, when the pressure in CV-200 is higher by 0.1 bar than the pressure in CV-100, and closes when the CV-200 pressure exceeds the CV-100 pressure by less than 0.01 bar. The steam flow is restricted by the Flow Composition Parameter (FCP) of 10<sup>-3</sup>. The FCP is defined by Tabular Function TF-100.

*	Definition of Junction No. 001									
*										
205150 *	Exam	ple Ju	nction							
* 200150 *	From 200	To 100	Area E (m2) 0.05	levation (m) 5.0	Length (m) 0.1	Diame (m) 0.1	ter He	eight 1 (m) Di: 0.1	Flow rection 0	Edges 0.0
* 210150	Lengt (m) 0.1	h Rou 1	ughness (m) 0E-5	Diameter (m) 0.1	K-for (-) 0.5	K-rev (-) 0.5	rf-for (-) 1.0	rf-rev (-) 1.0	v CM (-) 0.7	MOD (-) 1
*	Valv	e								
*	Moto	r c	lP-open	dP-close	9					
220150 *	0	C	.10E+5	0.01E+5						
* 240150 *	Gas 3	TF nu 100	umber							
605100 600100	TF d 0.0	efinir 1.0E	ng CFP f 2-03	or check w	valve, f	or cons	ervativ	ve BWR an	nalysis.	

#### 2.3 1-D Solid Heat Conductor Input Data

### 2.3.1 Records: 300XXX, 1-D Solid Heat Conductor Main Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (I) :	IGEOSC	Geometry type, (-). IGEOSC = 1 : IGEOSC = 2 : IGEOSC = 3 : Acceptable range: Default value:	rectangular geometry, cylindrical geometry, spherical geometry. 1, 2, 3. none.
W-2 (R) :	SIZESC	Size of solid condu IGEOSC = 1 : IGEOSC = 2 : IGEOSC = 3 : Acceptable range: Default value:	actor. The interpretation depends on the geometry: area of the conductor surface, $(m^2)$ , length of the cylinder, $(m)$ , not used. $0.0 < SIZESC \le 10^{10}$ . none.
W-3 (R) :	X0SC	Left (inner) side co type. IGEOSC = 1 : IGEOSC = 2 : IGEOSC = 3 : Acceptable range: Default value:	ordinate. The interpretation depends on the geometry not used, inner radius of the cylinder, (m), inner radius of the sphere, (m). $0.0 \le X0SC \le 10^{10}$ . 0.0.
W-4 (R) :	ELEVSC	Elevation of middle the SC is automat {Min[ $Z_{TOP}$ (CV <sub>1</sub> ), Z $Z_{TOP}$ and $Z_{TOP}$ are to CV <sub>1</sub> and the right b 1-D Solid Heat Con 1, description of the Acceptable range: Default value:	e point of the conductor, (m). If –999 is entered, then tically allocated to match the elevations of CV-s: $Z_{TOP}(CV_2)$ ] + Max[ $Z_{BOT}(CV_1)$ , $Z_{BOT}(CV_2)$ ]} / 2. Here op and bottom elevations of the left boundary volume boundary volume CV <sub>2</sub> . The automatic allocation of a nductor is illustrated in Figure 2-12 (see also Volume e SC boundary conditions). elevations of the boundary surfaces that transfer heat to Control Volumes must lie within the elevations of the corresponding Control Volumes 0.0

W-5 (I) :	IVERSC	Vertical orientation of conducto Rectangular: $IVERSC = 0$ : IVERSC = +1: IVERSC = -1: Cylindrical: $IVERSC = 0$ : IVERSC = 0: IVERSC = +1: Acceptable range: -1, 0, +1 Default value: 0	or, (-), see Figure 2-11. vertical wall horizontal wall, left surface up horizontal wall, left surface down vertical cylinder horizontal cylinder
W-6 (R) :	POWRSC	Internal power source, (W). In on the value of POWRSC is multi defined by IPOWSC (word 7) and (word 9), if present. Acceptable range: $-10^{10} \le POW$ Default value: 0.0.	rder to obtain the current internal source, iplied by the time dependent multiplier nd by the constant multiplier POWMSC WRSC $\leq 10^{10}$ .



Figure 2-11 Vertical orientations of 1-D Solid Heat Conductors

Right surface

ŝ



- Figure 2-12 Automatic allocation of SC within the boundary Control Volumes
- W-7 (I): IPOWSC Pointer to a Tabular or Control Function which defines the internal power multiplier. If the number is equal to zero, then internal power source is constant, and equal to POWRSC (Word 6). If the number is positive, then the internal power multiplier will be defined by the Tabular Function IPOWSC. If it is negative the multiplier will be defined by the Control Function |IPOWSC|. No lower or upper limit is imposed on the value obtained from a Tabular or Control Function (thus a negative power source is allowed). If there is no internal power source (POWRSC=0.0) then IPOWSC must also be equal to zero. *Acceptable range:* must be a valid reference number of a Tabular, or a Control Function, if non-zero.

0.

Default value:

- W-8 (R) :HINCSCInclination of nearly horizontal tubes, (degree). Tubes that have small<br/>inclination should be modelled as horizontal (IVERSC=±1, see Word 5<br/>above) with HINCSC > 0.0°. The value is used by the condensation<br/>model.<br/><br/>Acceptable range:  $0.0^{\circ} \leq \text{HINCSC} \leq 20.0^{\circ}$ .<br/><br/>Default value:  $0.0^{\circ}$ .
- W-9 (R) :POWMSCConstant power multiplier. The constant power multiplier is introduced<br/>to have an easy way of defining for example axial power profile.Acceptable range: $-10^{10} \le \text{POWMSC} \le 10^{10}$ <br/>Default value:1.0

#### 2.3.2 Records: 301000, SC Groups - General Data

W-1 (I): KGRPSC Default SC group number. SC groups are introduced for editing; at the end of input processing volumes and masses of all materials is printed for each SC group. SC groups may be used to check the volumes and masses of materials in primary system, secondary system, etc. Acceptable range:  $1 \le \text{KGRPSC} \le 20$ Default value: 1

#### 2.3.3 Records: 301XXX, Initial and Transient Temperatures, SC Group Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	INTSC	Initial temperature calculation indicator.
		1: Initial temperature distribution is calculated. If this option is selected, the program calculates temperature distribution performing conduction calculation with a large ( $\Delta t$ =10 <sup>99</sup> s) time step. In rare cases convergence failure may be encountered when performing the initial step. Usually it is good to ignore the convergence failure, since the calculated initial temperatures are typically better than could be obtained by manual initialization. The convergence failure can be ignored, by setting IACSFL (Word 8 in record 020000, see section 2.16.5).
		(word 8 in record 920000 - see section 2.10.5).
		<ul> <li>2: Input values (Words 4 in records 310XXX) are used. Use this option also if temperatures should be read from an Initial Condition File - ICF (section 2.16.3).</li> <li>Acceptable range: 1, 2.</li> <li>Default value: 2</li> </ul>
		Dejumi vame. 2.

W-2 (R): ITYPSC Transient temperature calculation indicator.

- 1: Temperatures are time independent; that means the initial temperatures are kept through the transient.
- 2: Transient temperatures are calculated from conduction equation (normal SC type).

Acceptable range: 1, 2. Default value: 2.

W-3 (I):IGRPSCSC group number. SC groups are introduced for editing; at the end of<br/>input processing volumes and masses of all materials is printed for each<br/>SC group. SC groups may be used to check the volumes and masses of<br/>materials in primary system, secondary system, etc.<br/>Acceptable range:  $1 \leq IGRPSC \leq 20$ <br/>Default value:KGRPSC (defined in record 301000)

#### 2.3.4 Records: 302XXX, Multiplicity of the 1-D Solid Heat Conductor

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (R) :	XMLTSC	Multiplicity of the	1-D solid conductor. This is the number of solid
		conductors that are	identical to the conductor XXX. If XMLTSC<0 then
		multiplicity will be	time-dependent and defined by a Control Function
		with reference num	iber  –XMLTSC .
		Acceptable range:	$0.0 < \text{XMLTSC} < 10^{10} \text{ or CF}$ reference number
		Default value:	1.0 .

#### 2.3.5 Records: 303000, Numerical Integration Method, Global Activator

W-1 (I) :	NIMGSC	<ul> <li>Numerical integration method - Figure 2-13.</li> <li>=1: Nodes at cell-centers. This was the only method available in earlier SPECTRA versions</li> <li>=2: Nodes at cell-edges (used in MELCOR, RELAP, etc.). An advantage is an more accurate stationary state temperature distribution in case of a coarse nodalization and nonuniform power profile - see Volume 3, section: "Integration methods 1 and 2 -Non-uniform Power, Comparison with MELCOR").</li> <li>Acceptable range: 1 and 2 Default value: 1</li> </ul>
W-2 (I) :	NDGSC	<ul> <li>For numerical integration method 2, this is the node number for axial conduction or direct contact conduction.</li> <li>=1: left boundary node,</li> <li>=2: right boundary node,</li> <li>=3: average of the left and right boundary nodes.</li> <li>Acceptable range: 1, 2, 3</li> <li>Default value: 1</li> </ul>

#### 2.3.6 Records: 303XXX, Numerical Integration Method, Individual Activators

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

- W-1 (R): NIMISC Numerical integration method Figure 2-13.
  - =1: Nodes at cell-centers.
  - This was the only method available in earlier SPECTRA versions=2: Nodes at cell-edges (used in MELCOR, RELAP, etc.).
  - An advantage is an more accurate stationary state temperature distribution in case of a coarse nodalization and nonuniform power profile see Volume 3, section: "Integration methods 1 and 2 -Non-uniform Power, Comparison with MELCOR").

Note! Method 2 is used only for temperature distribution calculation. The fission product diffusion is always calculated using the Method 1. The diffusion results are practically independent of the method used for temperature calculation. The only difference is introduced by the temperature-dependent diffusion coefficient. If Method 1 is used, then there is a direct correspondence between the temperature nodes and the diffusion nodes. In such case the diffusion coefficient in cell *i* is obtained using the temperature in the same cell:  $D_i = f_i(T_i)$ . If Method 2 is used, the diffusion coefficient in a given cell is obtained using the average temperature of the two temperature nodes bounding the computational cell: temperature in the same cell:  $D_i = f_i((T_i + T_{i+1})/2)$ . Acceptable range: 1 and 2.

Default value: NIMGSC

W-2 (I): NDISC

contact conduction.

=1: left boundary node,

=2: right boundary node,

=3: average of the left and right boundary nodes.

Note: implicit solution of direct contact is available only for NDISC = 1 or 2. For these values the minimum resistance is  $10^{-5}$  (m-K/W). For NDISC=3, the minimum resistance is equal to  $10^{-3}$  (m-K/W) - see description of IHAXSC, record 390XXX).

For NIMISC=2, this is the node number for axial conduction or direct

Acceptable range: 1, 2, 3

Default value: NDGSC



Figure 2-13 Numerical integration methods: SPECTRA original method, nodes at cell centers left: MELCOR/RELAP method, nodes at cell edges right

#### 2.3.7 Records: 304XXX, **Optional Size Change During Transient**

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (I): IAHTSC Pointer to a Tabular or Control Function that defines a multiplier on the SC size (left and right surface area) during the transient. If the number is positive, then the multiplier will be defined by a Tabular Function with the reference number: IAHTSC. If the number is negative, then the multiplier will be defined by a Control Function with the reference number: | IAHTSC |. The value obtained from the Tabular or Control Function will be internally limited to the range between  $10^{-6}$  and 1.0. The thickness and node sizes are not affected. If the size change is applied and the SC has an internal heat source, the source strength will follow the size change (i.e. the power density, W/m<sup>3</sup>, will remain the same). The plot parameter SC-xxx-Ocel-xxxx, giving the power generation in each cell, is however not reflecting this fact (it gives power of the "full size" SC, independently of the value of the multiplier). The model can be used for SCs with direct contact (records 390XXX) but in such case the SC size multiplier should be made the same for the SCs that are in contact. The size change can be applied for the cases when:

1. SC surfaces are convecting heat,

2. simple radiation-model between the SC surface and gas is used,

3. structure-to-structure radiation model is used.

Examples of all three cases are shown in Volume 3. The model cannot be used if SC is a member of the detailed radiation model network (section 2.6), because the radiation view factors do not change in time.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero. 1

Default value:

#### 2.3.8 Records: 305XXX, Name of the 1-D Solid Heat Conductor

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (A) : NAMESC User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* 50 "underline" characters: "\_".

#### 2.3.9 Records: 310XXX, Cell Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

Several records with the same number may be entered. Each record with this number contains data for NC cells. Cell data are read sequentially - the first record in the input is interpreted as containing the data for the first (leftmost) NC cells. The total number of cells of a 1-D Solid Heat Conductor may not exceed 100 and may not be smaller than 2.

W-1 (R) :	CELLSC	Cell width, (m). For thermal penetration	r the boundary cells the cell width is compared to the depth (see Volume 1):
		$d_{pen}(t) = C \cdot \sqrt{at} =$	$= 7.09 \cdot \sqrt{k / (\rho \cdot c_p) \cdot t}$
		A warning message	e is printed if:
		CELLSC>dpen(10	$^{2}$ )=70.9·( k/( $\rho \cdot c_{p}$ ) ) <sup>1/2</sup> .
		An error message is	s issued if:
		CELLSC>dpen(10	$(k/(\rho \cdot c_p))^{1/2}$
		Acceptable range: Default value:	$0.0 < CELLSC < 10^{10}$ . none.
W-2 (I) :	MATCSC	Pointer to a material of a single material Acceptable range:	al number, (-). Each cell is assumed to be composed defined by this word. must be a valid reference number of a solid material, defined in records 801XXX, 802XXX, 803XXX - see section 2.10).
		Default value:	none.
W-3 (R) :	QFRCSC	Relative power den be scaled by any fa	sity in this cell, (-). The values are relative and may ctor. The values will be normalized during the input

			prov alw Cor PO' for zero Acc Def	cessing so ays equa ntrol Fund WRSC, is at least of o, then QI eptable r ault value	o that l to Po ction s greate ne cell FRCSO <i>ange:</i> e:	the tota OWRSO IPOWS er than z . If the i 0.0 $\leq$ 0 0.0.	d in C m SC   zero, inter be ec QFR	ternal ultiplie (if us then Q nal po qual to $CSC \leq$	powe d by ed). QFRC wer s zero 10 <sup>10</sup>	er source the va If the in CSC mu source, for all o	e of t lue of nterna st be g POWI cells.	the cor the T l powe greater RSC, i	nductor i 'abular o er source than zer s equal t	s r >, 0
W-4 (R)	: ]	TINCS	C Init If N cell	ial cell te IMISC=	mperat 1 (node	ture, (K) es at cel	). Us l-cei	sed onl nters) t	ly if I his is	NTSC= the cer	=2 (seo nter ter	ction 2 mperat	.3.3). The of the	e
			If N The 311	IMISC=2 right ten XXX.	2 (node nperate	es at cell ure of th	l-edg ne la	ges) thi st cell	is is t is in	he left t such ca	emper ise spo	ature c	of the cel in recor	l. d
			Acc Def	eptable r ault valu	ange: e:	273.0 s none.	≤TI	NCSC	≤ 10	,000.0.				
W-5 (I) :	Υ	٩C	Nun the fron reco Acc Def	mber of co cell numb n the cell pords with <i>peptable r</i> <i>cault value</i>	ells. De ber NF l numb this nu ange: e:	ata word , if a non- per N+1 umber. $\geq 1$ . Th NC ent- be with 1	ds 1 nzero, wh e to terec nin t	- 4 are to value here N tal nur in all he rang	applie is sp is the nber reconge of	ied for N becified e sum c of cells rds, NC : $2 \le NC$	NC cel for W of NC s, equa ELSC CELSO	lls, star ford 6, for all al to th $C = \sum (N)$ $C \le 10^{10}$	ting fror otherwis previou ne sum c NC), mus 0.	n s f
W-6 (I) :	Υ	ΝF	Star firs prev for <i>Acc</i> <i>Def</i>	rting cell t yet unsp vious reco a new cel <i>eptable r</i> <i>cault value</i>	numbe becified ords w l or ce <i>ange:</i> e:	er. If th 1  cell,  i.4 1  tht this  i 1  lls. If N $1 \leq \text{NI}$ previou N+1	is nu e. ce num F < N $F \le 1$ us re	umber ell N+1 lber. If I+1, th N+1, v ecords	is m , who NF= is is a where with	issing, t ere N is N+1, th a replac e N is t this nur	the sta the su is rec ement he sun nber	arting o um of l ord de t data. m of N	cell is th NC for a fines dat NC for a	e 11 a 11
Example	1: five c	ells wit	h materi	al 101, tv	vo cell	s with n	nate	rial 102	2:					
	x-cell 0.001	Mat 101	0.0	300.0	INC 5	NE	*	data	for	cells	1-5,	Mat.	101	
310101	0.001	102	0.0	300.0	2		*	data	for	cells	6-7,	Mat.	102	
Example * 310101 310101	2: three x-cell 0.001 0.001	cells w Mat 101 102	ith mate Power 0.0 0.0	rial 101, t T (K) 300.0 300.0	wo ce NC 5 2	lls with <sub>NF</sub>	mat * *	erial 1( data data	05, tw for for	vo cells cells cells	with: 1-5, 6-7,	Mat. Mat.	al 102: 101 102	
310101	0.001	105	0.0	300.0	2	4	*	data	for	cells	4-5	redef:	ined	

to Mat. 105

\*

#### 2.3.10 Records: 311XXX, Right Surface Temperature

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

This record is needed if the second numerical integration method is used, NIMISC=2 (nodes at cell-edges).

W-1 (R) :TINRSCInitial temperature at the right surface of SC. This is the right surface<br/>temperature of the last cell. The left surface temperatures for all cells are<br/>defined in the records 310XXX.<br/>Acceptable range:  $273.0 \le \text{TINRSC} \le 10,000.0$ .<br/>Default value:temperature of the previous node.

#### 2.3.11 Records: 321XXX, Left (Inside) Side Boundary Conditions

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (I): **IVLLSC** Control Volume number for convective heat transfer. The value specifies the Control Volume, which is associated with the left (inside) boundary surface. If zero is entered, then the left surface is either insulated, or the convective heat transfer coefficient and the fluid temperature are specified by Tabular or Control Functions (defined by words 3 and 4 below). If IVLLSC>0, then heat is transferred to/from the CV using the standard heat and mass transfer package (Volume 1). It is also possible to overrule the use of the standard heat and mass transfer package, and use a Tabular or Control Function (defined by word 3 below) to determine the heat transfer coefficient. Also the fluid temperature can be altered by a Tabular or Control Function, by using the Word 4 below. In such case the value obtained from the Tabular or Control Function will be taken with weighting factor of 0.5, and the true (Control Volume) fluid temperature will be taken with the weighting factor of 0.5. If the heat transfer coefficient or the fluid temperature are defined by Tabular or Control Functions, then only heat transfer will occur on the surface, mass transfer (boiling/condensation) will not be calculated. Acceptable range: must be a valid reference number of a Control Volume, if non-zero. Default value: 0. W-2(R): HGTLSC Height of the left surface of the SC (elevation difference between the uppermost and the lowermost point of the surface). Used only if IVLLSC > 0. Used to determine pool and atmosphere fractions in case the surface is partly covered by pool. Acceptable range:  $0 \leq \text{HGTLSC} < 10^{10}$ .

*Default value:* RECTANGULAR geometry (IGEOSC=1):

- HORIZONTAL (IVERSC≠0): zero.
- VERTICAL (IVERSC=0): square root of the surface area, given by SIZESC (section 2.3.1). It is appropriate for square surfaces, thus for a rectangular geometry the default value should not generally be used. The appropriate value, wall height, should be entered.
- CYLINDRICAL geometry (IGEOSC=2):
- HORIZONTAL (IVERSC≠0): inner diameter, calculated from X0SC.
- VERTICAL (IVERSC=0):
- cylinder length, given by SIZESC. SPHERICAL geometry (IGEOSC=3):
  - inner diameter, calculated from X0SC.
- W-3 (I): **IHTLSC** Pointer to a Tabular or Control Function defining the convective heat transfer coefficient (HTC) at the left surface. If zero then the HTC is calculated by the code for the thermal-hydraulic conditions taken from the volume IVLLSC (Word 1). If the value is positive, HTC will be defined by the Tabular Function IHTLSC. If it is negative, it will be defined by the Control Function | IHTLSC |. The units of the quantities obtained from the Tabular or Control Function are assumed to be  $(W/m^2/K)$ . If the obtained value is negative, it will be set to zero. Note that if IHTLSC≠0 then the fluid temperature, needed to calculate the boundary heat flux, is taken as:
  - if IVLLSC>0 then the fluid temperature in Control Volume \_ IVLLSC is used.
  - if ITPLSC = 0 then the fluid temperature is given by a Tabular or Control Function, defined by ITPLSC (word 4 below).
  - if IVLLSC=0 and ITPLSC=0 then the fluid temperature is set to 300 K.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value: 0.

W-4 (I): **ITPLSC** Pointer to a Tabular or Control Function defining the fluid temperature at the left surface for convective heat transfer. If the value is positive, the fluid temperature will be defined by the Tabular Function ITPLSC. If it is negative, it will be defined by the Control Function | ITPLSC |. The units of quantity obtained from the Tabular or Control Function are assumed to be (K). If the obtained value is negative, it will be set to zero. If ITPLSC $\neq 0$  and IVLLSC>0 (heat transfer to a Control Volume), then the value obtained from Tabular or Control Function will be used with the weighting factor of FINTSC. The true fluid temperature (from Control Volume) will be used with the weighting factor of 1.0–FINTSC. Boiling and condensation models will be disabled by setting CSFLSC to -1.0 and ICNLSC to -4. In the past the input combination of IPTLSC $\neq 0$ and IVLLSC>0 was used to perform temperature averaging for heat exchangers. Currently it is not recommended to use this method. A more

elaborate temperature averaging model has been developed, and is available through input records 325XXX, 326XXX (see sections 2.3.15 and 2.3.16).

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value:

W-5 (I): IQRLSC Indicator for non-convective heat flux at the left boundary. The heat flux defined by this pointer is used only on the uncovered part of the SC (above water level). With this pointer a user can model in a simple way radiative heat transfer. If the net enclosure thermal radiation model is used, and this surface is associated with one of the radiating surfaces (section 2.6.3), then this parameter must not be used. The meaning is as follows:

0.

#### IQRLSC>1000:

Simple radiation model between the left SC surface and atmosphere gas is used to determine the non-convective heat transfer. The grey gas model is used, atmosphere is assumed to be opaque (the reason for assuming opaque atmosphere is discussed in Volume 3). The heat flux is equal to:

$$q = \varepsilon(T_w) \sigma \left(T_w^4 - T_g^4\right)$$

where  $\varepsilon(T_w)$  is the wall emissivity,  $\sigma$  is the Stefan-Boltzmann constant,  $T_w$ ,  $T_g$  are the wall and gas temperatures respectively. The emissivity is obtained from the Tabular Function number: (IQRLSC – 1000). The argument for the Tabular Function is the wall surface temperature, (K).

#### 0<IQRLSC<1000:

The heat flux is obtained from the Tabular Function number IQRLSC. The units of the quantities obtained from the Tabular Function are assumed to be:  $(W/m^2)$ . Positive heat flux means that the heat is emitted from the surface.

#### IQRLSC<0:

The heat flux is obtained from the Control Function number |IQRLSC|. The units of the quantities obtained from the Control Function are assumed to be: (W/m<sup>2</sup>). Positive heat flux means that the heat is emitted from the surface.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

*Default value:* 0.

W-6 (I) :	INCLSC	Configuration indicator for	or nat	ural convection.	The value is us	sed only
		when IVLLSC is positive.	The	meaning of this	variable is as fol	llows:
		Rectangular geometry:	0	vertical wall,		

0	vortiour wan,
-1	horizontal wall facing down,

+1 horizontal wall facing up.

Cylindrical geometry: 0 vertical cylinder,

-1 horizontal cylinder, inside,

Spherical geometry:

+1 horizontal cylinder, outside.

-1 sphere, inside,

+1 sphere, outside.

Default values are provided for each geometrical configuration, based on IGEOSC and IVERSC parameters (section 2.3.1) - see Table 2-6 and Table 2-7.

Acceptable range:	-1, 0, +1.
Default value:	RECTANG

efault value:	RECTANGULAR geometry (IGEOSC=1):	
	- VERTICAL (IVERSC=0): 0,	
	- HORIZONTAL down (IVERSC=-1): -1,	
	- HORIZONTAL up (IVERSC=+1): +1,	
	CYLINDRICAL geometry (IGEOSC=2):	
	- VERTICAL (IVERSC=0): 0,	
	- HORIZONTAL (IVERSC= $\pm 1$ ): $-1$ ,	
	SPHERICAL geometry (IGEOSC=1): -1.	

W-7 (R): DNCLSC Characteristic dimension for natural convection at the left boundary surface, (m). The value is used only when IVLLSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DNCLSC should be equal to (see Table 2-6 and Table 2-7): for vertical plates - height; for horizontal plates - width; for vertical cylinders - cylinder length; for horizontal cylinders - maximum of length and 2 times the inner diameter; for spheres - inner diameter. Note that the default value for plates (rectangular geometry) is only appropriate for the square surfaces.

Acceptable range:  $0.0 < \text{DNCLSC} < 10^{10}$ .

Default value: height, given by HGTLSC (Word 2 above). If HGTLSC is equal to zero (horizontal rectangular surfaces) then the square root of the surface area, given by SIZESC (section 2.3.1). The value is appropriate for square surfaces. Thus <u>for horizontal</u> rectangular surfaces the default value should not generally be used. The appropriate value, width, <u>should be entered</u>.

CYLINDRICAL geometry (IGEOSC=2):

inner diameter, calculated from X0SC (section 2.3.1).

SPHERICAL geometry (IGEOSC=3):

inner diameter, calculated from X0SC (section 2.3.1).

W-8 (I):

IFCLSC Configuration indicator for forced convection, as well as the nucleate boiling model and the model for critical heat flux calculation. The value is used only when IVLLSC is positive and no alternative liquid is used. For the alternative liquid the forced convection correlation is selected by Word 21 (IHCLSC). The meaning of this variable is as follows:

-1 internal flow, Chen correlation for nucleate boiling, Zuber and USSR Academy of Science models for critical heat flux calculations (Zuber for non-flow, USSR A. S. for flow conditions).

+1 external flow, Rohsenow correlation for nucleate boiling, Zuber model for critical heat flux calculation.
Default values are provided for each geometrical configuration, based on IGEOSC (section 2.3.1) - see Table 2-8 and Table 2-9.
Acceptable range: -1, +1.

*Default value:* -1.

W-9 (R): DFCLSC Characteristic dimension for forced convection at the left boundary surface, (m). The value is used only when IVLLSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFCLSC should be equal to (see Table 2-8 and Table 2-9): for internal flow - hydraulic diameter; for external flow - width (rectangular wall). Note that for cylinders and spheres the external flow type, defined by IFCLSC (see above) is not available. For the internal flow type the default value is the same as for the external flow type. Therefore for the internal flow type the default value should not be used. The appropriate value (hydraulic diameter) should be entered.

Acceptable range:  $0.0 < \text{DFCLSC} < 10^{10}$ .

neceptuble range.	0.0 < D1 CLDC < 10.
Default value:	RECTANGULAR geometry (IGEOSC=1):
	HGTLSC (if entered) or square root of the surface
	area, given by SIZESC (section 2.3.1). The value is
	appropriate for square surfaces. Thus for rectangular
	geometry the default value should not generally be
	used. The appropriate value should be entered: for
	internal flow - hydraulic diameter, for external flow
	- width.
	CYLINDRICAL geometry (IGEOSC=2):
	inner diameter, calculated from XOSC (section
	2.3.1).
	SPHERICAL geometry (IGEOSC=3):
	inner diameter, calculated from X0SC (section
	2.3.1).

W-10 (I) :

IFBLSC C

Configuration indicator for film boiling. The value is used only when IVLLSC is positive. The meaning of this variable is as follows:

0 vertical surface,

- $\pm 1$  horizontal cylinder,
- -1 horizontal plate, facing down,
- +1 horizontal plate, facing up.

Default values are provided for each geometrical configuration, based on IGEOSC and IVERSC (section 2.3.1) - see Table 2-10 and Table 2-11.

Acceptable range: -1,0,+1.

Default value: RECTANGULAR geometry (IGEOSC=1):

- VERTICAL (IVERSC=0):
- HORIZONTAL down (IVERSC=-1): -1,

+ HORIZONTAL up (IVERSC=+1): +1,

CYLINDRICAL geometry (IGEOSC=2):

- VERTICAL (IVERSC=0): 0,
- HORIZONTAL (IVERSC= $\pm 1$ ): +1,
- SPHERICAL geometry (IGEOSC=1): +1.

0.

W-11 (R): DFBLSC Characteristic dimension for film boiling at the left boundary surface, (m). The value is used only when IVLLSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFBLSC should be equal to (see Table 2-10 and Table 2-11): for vertical walls height; for horizontal plates - width; for cylinders and spheres - inner diameter.

Acceptable range:  $0.0 < \text{DFCLSC} < 10^{10}$ .

Default value:

RECTANGULAR geometry (IGEOSC=1): square root of the surface area, given by SIZESC (section 2.3.1). The value is appropriate for square surfaces. Thus <u>for rectangular geometry the default</u> value should not generally be used. The appropriate value should be entered: for internal flow hydraulic diameter, for external flow - width. CYLINDRICAL geometry (IGEOSC=2):

- VERTICAL (IVERSC = 0): length, given by SIZESC (section 2.3.1);
- HORIZONTAL (IVERSC = ±1): inner diameter, calculated from X0SC.
   SPHERICAL geometry (IGEOSC=3): inner diameter, calculated from X0SC

inner diameter, calculated from X0SC.

W-12 (I) :

ICNLSC

LSC Configuration indicator for condensation. The value is used only when IVLLSC is positive. The meaning of this variable is as follows:

- $\leq$  -4 model disabled
- = -3 condensation on horizontal wall facing up,
- = -2 condensation on horizontal wall facing down,
- = -1 condensation inside horizontal tubes,
- = 0 condensation on vertical walls,
- =+1 condensation on outside surface of horizontal tube.
- $\geq$  +2 condensation on outside surface of horizontal tube bank. ICNLSC is equal to the number of vertical rows of tubes.

Default values are provided for each geometrical configuration based on IGEOSC and IVERSC (section 2.3.1) - see Table 2-12 and Table 2-13. *Acceptable range:* all integers.

*Default value:* RECTANGULAR geometry (IGEOSC=1):

-	VERTICAL (IVERSC=0):	0;
-	HORIZONTAL down (IVERSC=-1	): -2;
	HORIZONTAL up (IVERSC=+1):	-3;
	however, if fins are present	
	(ITFLSC>0) then:	0;
CYLINDRICAL geometry (IGEOSC=2):		
-	VERTICAL (IVERSC=0):	0;
-	HORIZONTAL (IVERSC=±1):	-1;
SPH	ERICAL geometry (IGEOSC=3):	-1.

W-13 (R): DCNLSC Characteristic dimension for condensation at the left boundary surface, (m). The value is used only when IVLLSC is positive. Best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DCNLSC
should be equal to (see Table 2-12 and Table 2-13): for vertical walls (or cylinders) - wall height; inside horizontal tubes - inner diameter; outside surface of horizontal tubes or tube banks - outer diameter; horizontal walls facing up - maximum film thickness (equilibrium thickness of water layer with free fall of liquid at the edges of the wall). The condensation type is defined by ICNLSC (word 12).

In case of vertical walls the user may wish divide the total wall into a certain number of segments, modelled by separate conductors. Thus the conductors are stacked one over the other. To take into account the behavior of the condensate film in this case the characteristic dimension of the conductor number k in the stack (counting from the top) should be defined as follows:

$$DCNLSC(k) = \left(\frac{z_{BOT}(k)^{5/4} - z_{TOP}(k)^{5/4}}{z_{BOT}(k) - z_{TOP}(k)}\right)^{4}$$

where:  $z_{BOT}(k)$ 

 $z_{TOP}(k)$ 

distance from the bottom of the conductor k to the top of the stack, (m), distance from the top of the conductor k to

distance from the top of the conductor k to the top of the stack, (m).

If the height of each conductor in the stack is identical then the above formula reduces to:

$$DCNLSC(k) = \left(k^{5/4} - (k-1)^{5/4}\right)^4 \frac{H}{N}$$

where: H - total height of the wall, (m), N - number of conductors in the stack. The ratio: (H/N) is the height of a single conductor in the stack. Note that only for k=1 DCNLSC is equal to the physical height of the conductor, (H/N). For k>1 DCNLSC is greater than (H/N). For k=N DCNLSC is always greater than the total wall height, H. Acceptable range:  $0.0 < DCNLSC < 10^{10}$ . Default value: height, given by HGTLSC (Word 2 above). For horizontal walls facing up the default value is  $10^{-2}$ .

```
W-14 (R):CSFLSCThe constant C_{sf} in the Rohsenow equation for nucleate boiling (see<br/>Volume 1). The values of C_{sf} for different surfaces are given in the Table<br/>2-3. Entering a negative value will disable the full boiling model.<br/>Acceptable range: all reals.<br/>Default value:0.013.
```

Table 2-3	Values of	of	$C_{sf}$ for	Rohsenow	correlation.
-----------	-----------	----	--------------	----------	--------------

Surface type	$C_{sf}$	Surface type	$C_{sf}$
Nickel	0.0060	Platinum	0.0130
Ground and polished stainless steel	0.0080	Brass	0.0060
Teflon pitted stainless steel	0.0058	Polished copper	0.0128
Chemically etched stainless steel	0.0133	Lapped copper	0.0147
Mechanically polished stainless steel	0.0132	Scored copper	0.0068

W-15 (I): Critical heat flux model selection. The value is used only when IVLLSC MCFLSC > 0.

- Zuber pool boiling correlation with Ivey-Morris correction for 1 subcooling.
- 2 Combination of model based on USSR Academy of Sciences CHF look-up tables for high flow, with Zuber and Ivey-Morris for low flow.
- 3 Combination of Biasi correlation for high flow, with Zuber and Ivey-Morris for low flow.
- 4 Groeneveld (1986) look-up tables.
- CHF is calculated by a user-defined Control Function with the <0 number | MCFLSC |.

Acceptable range: 1, 2, 3 or reference to a Control Function Default value: 2.

W-16(I): MNCLSC Selection of model for the influence of non-condensable gases for condensation. The value is used only when IVLLSC is positive and ICNLSC is greater than –4. The meaning of this variable is as follows:

- Kuhn-Shrock-Petersen (KSP) correlations recommended for 1 condensation on the inside surface of tubes.
- 2 Ogg correlations.
- Modified Ogg correlations recommended for condensation on 3 the outside surface of tubes, plates, etc.

Default values are provided - see Table 2-14 and Table 2-15.

Acceptable range: 1, 2, 3. 3.

Default value:

W-17 (R): **CFDLSC** Indicator of condensate film drainage behaviour.

If the value is <u>positive</u> then CFDLSC is the height of the left SC surface. The elevation of the lowermost point of this surface is equal to the elevation of its center point, minus CFDLSC/2.0. The drainage from this surface is either deposited in the pool of a CV (if the lowest point of the surface is immersed in pool), or converted to droplets and suspended in the atmosphere of a CV as "rain" drops (if the lowest point of the surface is not immersed in the pool).

If the value is negative then the drainage is assumed to be deposited on a surface of other (lower) Solid Conductor. The absolute value of CFDLSC must then be equal to the number of SC at the bottom of the stack.

The use of the drainage parameter, CFDLSC, and the condensation characteristic dimension, DCNLSC, in case of individual and stacked conductors is illustrated in Figure 2-14 (see also Volume 3). The length of all conductors is assumed to be 0.5 m. Appropriate values of DCNLSC and CFDLSC are shown in Table 2-4.

Acceptable range: if CFDLSC<0.0 then the left surface of SC No. CFDLSC | must be connected to a Control Volume (not necessarily equal to IVLLSC),

> if CFDLSC>0.0 then the bottom elevation of the left surface (center point elevation minus CFDLSC/2.0) must be within the boundary Control Volume.

Default value:

the default value is set to twice the distance between the center point of the left surface and the bottom of the boundary Control Volume. That value will result in deposition of condensate always in the pool. This is done to avoid numerical problems, and time step reduction, when condensate is converted into droplets.



Figure 2-14 Condensation example cases (A) and (B).

Table 2-4	Values of DCNLSC and CFDLSC for the example cases (	(A)	and (	B)
i able 2-4	values of DCNLSC and CFDLSC for the example cases (	$(\mathbf{A})$	anu (	1

	Case (A)		Case (B)		
SC	DCNLSC	CFDLSC	DCNLSC	CFDLSC	
1	$0.5 \cdot (1^{5/4} - 0^{5/4})^4 = 0.50$	-5.0	0.50	0.5	
2	$0.5 \cdot (2^{5/4} - 1^{5/4})^4 = 1.81$	-5.0	$0.5 \cdot (1^{5/4} - 0^{5/4})^4 = 0.50$	-3.0	
3	$0.5 \cdot (3^{5/4} - 2^{5/4})^4 = 3.04$	-5.0	$0.5 \cdot (2^{5/4} - 1^{5/4})^4 = 1.81$	0.5	
4	$0.5 \cdot (4^{5/4} - 3^{5/4})^4 = 4.26$	-5.0	$0.5 \cdot (1^{5/4} - 0^{5/4})^4 = 0.50$	-5.0	
5	$0.5 \cdot (5^{5/4} - 4^{5/4})^4 = 5.48$	0.5	$0.5 \cdot (2^{5/4} - 1^{5/4})^4 = 1.81$	0.5	

W-18 (I) :	IHDLSC	Indicator of CV flow direction relative to the left SC surface. Used only for rectangular (IGEOSC=1) SC's. The meaning is:For vertical SC's (IVERSC=0): $v_{SC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2}$ ,0:CV horizontal flow is parallel, for horizontal SC's (IVERSC<>0): $v_{SC} = v_{CV,ver}$ .For horizontal SC's (IVERSC<>0): $v_{SC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2}$ ,1:CV vertical flow is parallel, is parallel, i: $v_{SC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2}$ ,1:CV vertical flow is perpendicular, is per
W-19 (I) :	THTLSC	Contact angle, $\theta$ , (degree). Used to determine the diameter of bubbles created during nucleate boiling: $D = 0.0208 \cdot \theta \cdot (\sigma/g/(\rho_{liq}-\rho_{gas}))^{(1/2)}$ . Acceptable range: $10^{\circ} \leq \text{THTLSC} \leq 180^{\circ}$ . Default value: $96^{\circ}$ .
W-20 (R) :	XRBLSC	Multiplier for convective heat transfer, $X_{RB}$ . XRBLSC<0.0: HTC is multiplied by  XRBLSC  in both natural and force convection. It may be used to obtain a conservative estimation of heat transfer. XRBLSC>0.0: HTC is multiplied by XRBLSC only in case of turbulent forced convection (FC-TUR), internal flow (IFCLSC = -1). It is intended to allow the user to define a rod bundle multiplier in forced convection: $Nu_{tur} = X_{RB} 0.023 \ Re^{0.8} \ Pr^{0.4}$ Appropriate values for parallel flow and cross-flow may be found in literature. The ratio of pitch over diameter is a good approximation (see Volume 1 description of forced convection):
		$X_{_{RR}} = P / D$
		For tube arrangements other than equilateral triangle pitch, the multiplier is given by: $X_{RB} = \left(\frac{P_1 \cdot P_2}{P_2}\right)$
		Note that the rod bundle multiplier may be different for different fluids. For example, for the liquid metals the value may even show different tendency (see Volume 1, description of liquid metals correlations):
		$X_{RB} = 1 - \exp[-3.8 \cdot (P/D - 1)]$
		Acceptable range: $0.0 \le  \text{XRBLSC}  \le 10^6$ Default value:XRBLHT (global activator, defined in the record 810020)
W-21 (I) :	IHCLSC	Selection of heat transfer correlation for alternative fluid. <i>Acceptable range:</i> one of the correlations defined in records 843XXX or 843YYY

01	0-5111
Default value: re	ctangular: 1, cylindrical: 2, spherical: 3.

#### 2.3.12 Records: 322XXX, Right (Outside) Side Boundary Conditions

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 1-D Solid Heat Conductors is 550 (999 in LINUX version).

W-1 (I): **IVLRSC** Control Volume number for convective heat transfer. The value specifies the Control Volume, which is associated with the right (outside) boundary surface. If zero is entered then the right surface is either insulated, or the convective heat transfer coefficient and fluid temperature are specified by Tabular or Control Functions (defined by words 3 and 4 below). If IVLRSC>0 then heat is transferred to/from the CV using the standard heat and mass transfer package (Volume 1). It is also possible to overrule the use of the standard heat and mass transfer package, and use a Tabular or Control Function (defined by word 3 below) to determine the heat transfer coefficient. Also the fluid temperature can be altered by a Tabular or a Control Function, by using the Word 4 below. In such case the value obtained from the Tabular or Control Function will be taken with weighting factor of 0.5, and the true (Control Volume) fluid temperature will be taken with the weighting factor of 0.5. If the heat transfer coefficient or the fluid temperature are defined by Tabular or Control Functions, then only heat transfer will occur on the surface, mass transfer (boiling/condensation) will not be calculated.

Acceptable range: must be a valid reference number of a Control Volume, if non-zero.

Default value:

 $\begin{array}{lll} W-2 \ (R): & HGTRSC & Height of the right surface of the SC (elevation difference between the uppermost and the lowermost point of the surface). Used only if IVLRSC > 0. Used to determine pool and atmosphere fractions in case the surface is partly covered by pool. \\ \end{array}$ 

0.

Acceptable range:  $0 \leq \text{HGTRSC} < 10^{10}$ .

*Default value:* RECTANGULAR geometry (IGEOSC=1):

- HORIZONTAL (IVERSC≠0): zero.
  - VERTICAL (IVERSC=0):
    - square root of the surface area, given by SIZESC (sec. 1.3.1). It is appropriate for square surfaces, thus <u>for a rectangular</u> <u>geometry the default value should not</u> <u>generally be used. The appropriate value,</u> <u>wall height, should be entered</u>.

CYLINDRICAL geometry (IGEOSC=2):

- HORIZONTAL (IVERSC≠0): outer diameter, calculated from X0SC and CELLSC.
- VERTICAL (IVERSC=0): cylinder length, given by SIZESC.

SPHERICAL geometry (IGEOSC=3):

outer diameter, calculated from X0SC and CELLSC.

W-3 (I): **IHTRSC** Pointer to a Tabular or Control Function defining the convective heat transfer coefficient (HTC) at the right surface. If zero then the HTC is calculated by the code for the thermal-hydraulic conditions taken from the volume IVLRSC (Word 1). If the value is positive, HTC will be defined by the Tabular Function IHTRSC. If it is negative, it will be defined by the Control Function | IHTRSC |. The units of the quantities obtained from the Tabular or Control Function are assumed to be  $(W/m^2/K)$ . If the obtained value is negative, it will be set to zero. Note that if IHTRSC≠0 then the fluid temperature, needed to calculate the boundary heat flux, is taken as: if IVLRSC>0 then the fluid temperature in Control Volume IVLRSC is used. if ITPRSC = 0 then the fluid temperature is given by a Tabular or Control Function, defined by ITPRSC (word 4 below). if IVLRSC=0 and ITPRSC=0 then the fluid temperature is set to 300 K. Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero. Default value: 0. W-4 (I): **ITPRSC** Pointer to a Tabular or Control Function defining the fluid temperature at the right surface for convective heat transfer. If the value is positive, the fluid temperature will be defined by the Tabular Function ITPRSC. If it is negative, it will be defined by the Control Function **ITPRSC**. The units of quantity obtained from the Tabular or Control Function are assumed to be (K). If the obtained value is negative, it will be set to zero. If ITPRSC≠0 and IVLRSC>0 (heat transfer to a Control Volume), then the value obtained from Tabular or Control Function will be used with the weighting factor of FINTSC. The true fluid temperature (from Control Volume) will be used with the weighting factor of 1.0–FINTSC. Boiling and condensation models will be disabled by setting CSFRSC to -1.0 and ICNRSC to -4. In the past the input combination of IPTLSC $\neq 0$  and IVLLSC>0 was used to perform temperature averaging for heat exchangers. Currently it is not recommended to use this method. A more elaborate temperature averaging model has been developed, and is available through input records 325XXX, 326XXX (see sections 2.3.15 and 2.3.16). Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero. Default value: 0. W-5 (I): **IORRSC** Indicator for non-convective heat flux at the right boundary. The heat flux defined by this pointer is used only on the uncovered part of the SC (above water level). With this pointer a user can model in a simple way radiative heat transfer. If the net enclosure thermal radiation model is used, and this surface is associated with one of the radiating surfaces (section 2.6.3), then this parameter must not be used. The meaning is as follows:

#### IORRSC>1000:

Simple radiation model between the right SC surface and atmosphere gas is used to determine the non-convective heat transfer. The grey gas model is used, atmosphere is assumed to be opaque (the reason for assuming opaque atmosphere is discussed in Volume 3). The heat flux is equal to:

 $q = \varepsilon(T_w) \sigma \left(T_w^4 - T_g^4\right)$ 

where  $\varepsilon(T_w)$  is the wall emissivity,  $\sigma$  is the Stefan-Boltzmann constant,  $T_{w}$ ,  $T_{g}$  are the wall and gas temperatures respectively. The emissivity is obtained from the Tabular Function number: (IQRRSC-1000). The argument for the Tabular Function is the wall surface temperature, (K).

#### 0<IORRSC<1000:

The heat flux is obtained from the Tabular Function number IORRSC. The units of the quantities obtained from the Tabular Function are assumed to be:  $(W/m^2)$ . Positive heat flux means that the heat is emitted from the surface.

### IQRRSC<0:

The heat flux is obtained from the Control Function number IORRSC. The units of the quantities obtained from the Control Function are assumed to be: (W/m<sup>2</sup>). Positive heat flux means that the heat is emitted from the surface.

Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value: 0.

Cylindrical geometry:

W-6(I):

**INCRSC** Configuration indicator for natural convection. The value is used only when IVLRSC is positive. The meaning of this variable is as follows:

> Rectangular geometry: 0

- vertical wall, -1 horizontal wall facing down,
- horizontal wall facing up. +1
- 0 vertical cylinder.
- -1
- horizontal cylinder, inside,

+1horizontal cylinder, outside. Spherical geometry:

- -1 sphere, inside,
- +1sphere, outside.

Default values are provided for each geometrical configuration, based on IGEOSC and IVERSC parameters (section 2.3.1) - see Table 2-6 and Table 2-7.

Acceptable range: -1, 0, +1.

Default value: RECTANGULAR geometry (IGEOSC=1):

- VERTICAL (IVERSC=0): 0.
- HORIZONTAL down (IVERSC=-1): +1,
- HORIZONTAL up (IVERSC=+1): -1.
- CYLINDRICAL geometry (IGEOSC=2):
- VERTICAL (IVERSC=0): 0.
- HORIZONTAL (IVERSC=±1): 1,

however, if fins are present (ITFRSC=1) then: 0; SPHERICAL geometry (IGEOSC=1): 1.

W-7 (R) : DNCRSC Characteristic dimension for natural convection at the right boundary surface, (m). The value is used only when IVLRSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DNCRSC should be equal to (see Table 2-6 and Table 2-7): for vertical plates - height; for horizontal plates - width; for vertical cylinders cylinder length; for horizontal cylinders - outer diameter; for spheres outer diameter. Note that the default value for plates (rectangular geometry) is only appropriate for the square walls.

Acceptable range:  $0.0 < \text{DNCRSC} < 10^{10}$ .

height, given by HGTRSC (Word 2 above). If Default value: HGTRSC is equal to zero (horizontal rectangular surfaces) then the square root of the surface area, given by SIZESC (section 2.3.1). The value is appropriate for square surfaces. Thus for horizontal rectangular surfaces the default value should not generally be used. The appropriate value, width, should be entered. CYLINDRICAL geometry (IGEOSC=2): outer diameter, calculated from X0SC and CELLSC (sections 2.3.1 and 2.3.9). SPHERICAL geometry (IGEOSC=3): outer diameter, calculated from X0SC and CELLSC (sections 2.3.1 and 2.3.9).

W-8 (I): **IFCRSC** Configuration indicator for forced convection, as well as the nucleate boiling model and the model for critical heat flux calculation. The value is used only when IVLRSC is positive and no alternative liquid is used. For the alternative liquid the forced convection correlation is selected by Word 21 (IHCRSC). The meaning of this variable is as follows:

- internal flow, Chen correlation for nucleate boiling, Zuber and -1USSR Academy of Science models for critical heat flux calculations (Zuber for non-flow, USSR A. S. for flow conditions).
- +1external flow, Rohsenow correlation for nucleate boiling, Zuber model for critical heat flux calculation.

Default values are provided for each geometrical configuration, based on IGEOSC (section 2.3.1) - see Table 2-8 and Table 2-9.

Acceptable range:  $-1 \leq \text{IFCRSC} \leq +1$ . Default value: -1.

W-9(R):DFCRSC Characteristic dimension for forced convection at the right boundary surface, (m). The value is used only when IVLRSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFCRSC should be equal to (see Table 2-8 and Table 2-9): for internal flow - hydraulic diameter; for external flow - width (rectangular wall) or outer diameter (cylinders, spheres). The internal/external flow type is

defined by IFCRSC (see above). For the internal flow type the default value is the same as for the external flow type. Therefore for the internal flow type the default value should not be used, but the appropriate value for DFCRSC should be entered.

Acceptable range:  $0.0 < DFCRSC < 10^{10}$ . Default value: RECTANGULAR geometry (IGEOSC=1): HGTRSC (if entered) or square root of the surface area, given by SIZESC (section 2.3.1). CYLINDRICAL geometry (IGEOSC=2): outer diameter, calculated from X0SC and CELLSC (sections 2.3.1 and 2.3.9). SPHERICAL geometry (IGEOSC=3): outer diameter, calculated from X0SC and CELLSC (sections 2.3.1 and 2.3.9).

W-10(I): IFBRSC Configuration indicator for film boiling. The value is used only when IVLRSC is positive. The meaning of this variable is as follows:

- 0 vertical surface,
- $\pm 1$ horizontal cylinder.
- horizontal plate, facing down, -1
- horizontal plate, facing up. +1

Default values are provided for each geometrical configuration, based on IGEOSC and IVERSC (section 2.3.1) - see Table 2-10 and Table 2-11.

Acceptable range: -1, 0, +1.

Acceptable range:	$-1, 0, \pm 1.$		
Default value:	RECTANGULAR geometry (IGEOSC=1):		
	- VERTICAL (IVERSC=0):		
	0; not changeable by user,		
	- HORIZONTAL down (IVERSC=-1):		
	-1; not changeable by user,		
	- HORIZONTAL up (IVERSC=+1):		

- +1; not changeable by user.
- CYLINDRICAL geometry (IGEOSC=2):
- VERTICAL (IVERSC=0):
  - not changeable by user, 0:
  - HORIZONTAL (IVERSC=±1):
    - 1: not changeable by user,
- SPHERICAL geometry (IGEOSC=1):
  - not changeable by user. 1:

CYLINDRICAL geometry (IGEOSC=2):

W-11 (R): DFBRSC Characteristic dimension for film boiling at the right boundary surface, (m). The value is used only when IVLRSC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFBRSC should be equal to (see Table 2-10 and Table 2-11): for vertical walls height; for horizontal plates - width; for cylinders and spheres - outer diameter. Acceptable range:  $0.0 < \text{DFCRSC} < 10^{10}$ . Default value: RECTANGULAR geometry (IGEOSC=1): HGTRSC (if entered) or square root of the surface area, given by SIZESC (section 2.3.1).

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outer diameter, calculated from X0SC and CELLSC. SPHERICAL geometry (IGEOSC=3): outer diameter, calculated from X0SC and CELLSC.

ICNRSC Configuration indicator for condensation. The value is used only when IVLRSC is positive. The meaning of this variable is as follows:

- $\leq -4$  model disabled
- = -3 condensation on horizontal wall facing up,
- = -2 condensation on horizontal wall facing down,
- = -1 condensation inside horizontal tubes,
- = 0 condensation on vertical walls,
- =+1 condensation on outside surface of horizontal tube.
- $\geq +2$  condensation on outside surface of horizontal tube bank. The value of ICNRSC is equal to the number of rows of tubes in vertical direction.

Default values are provided for each geometrical configuration based on IGEOSC and IVERSC (section 2.3.1) - see Table 2-12 and Table 2-13. *Acceptable range:* all integers.

*Default value:* RECTANGULAR geometry (IGEOSC=1):

- VERTICAL (IVERSC=0): 0;
   HORIZONTAL down (IVERSC=+1): -2; HORIZONTAL up (IVERSC=-1): -3; however, if fins are present (ITFRSC=1) then: 0;
   CYLINDRICAL geometry (IGEOSC=2):
   VERTICAL (IVERSC=0): 0;
   HORIZONTAL (IVERSC=±1): +1; however, if fins are present
  - (ITFRSC=1) then: 0;
- SPHERICAL geometry (IGEOSC=3): +1.
- W-13 (R): DCNRSC Characteristic dimension for condensation at the right boundary surface, (m). The value is used only when IVLRSC is positive. Best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DCNRSC should be equal to (see Table 2-12 and Table 2-13): for vertical walls (or cylinders) wall height; inside horizontal tubes inner diameter; outside surface of horizontal tubes or tube banks outer diameter; horizontal walls facing up maximum film thickness (equilibrium thickness of water layer with free fall of liquid at the edges of the wall). The condensation type is defined by ICNRSC (word 12).

In case of vertical walls the user may wish divide the total wall into a certain number of segments, modelled by separate conductors. Thus the conductors are stacked one over the other. To take into account the behavior of the condensate film in this case the characteristic dimension of the conductor number k in the stack (counting from the top) should be defined as follows:

W-12 (I) :

$$DCNLSC(k) = \left(\frac{z_{BOT}(k)^{5/4} - z_{TOP}(k)^{5/4}}{z_{BOT}(k) - z_{TOP}(k)}\right)^{4}$$

where:  $z_{BOT}(k)$ 

 $Z_{TOP}(k)$ 

distance from the bottom of the conductor k to the top of the stack, (m),

distance from the top of the conductor k to the top of the stack, (m).

If the height of each conductor in the stack is identical then the above formula reduces to:

$$DCNLSC(k) = \left(k^{5/4} - (k-1)^{5/4}\right)^4 \frac{H}{N}$$

where:	H	-	total height of the wall, (m),
	N	-	number of conductors in the stack

The ratio: (*H/N*) is the height of a single conductor in the stack. Note that only for k=1 DCNRSC is equal to the physical height of the conductor, (*H/N*). For k>1 DCNRSC is greater than (H/N). For k=N DCNRSC is always greater than the total wall height, H. *Acceptable range:* 0.0 < DCNRSC <  $10^{10}$ . *Default value:* height, given by HGTRSC (Word 2 above). For horizontal walls facing up the default value is equal to  $10^{-3}$ .

W-14 (R): CSFRSC The constant  $C_{sf}$  in the Rohsenow equation for nucleate boiling (see Volume 1). The values of  $C_{sf}$  for different surfaces are given in Table 2-5. Entering a negative value will disable the full boiling model. Acceptable range: all reals. Default value: 0.013.

Table 2-5 Values of  $C_{sf}$  for Rohsenow correlation.

Surface type	$C_{sf}$	Surface type	$C_{sf}$
Nickel	0.0060	Platinum	0.0130
Ground and polished stainless steel	0.0080	Brass	0.0060
Teflon pitted stainless steel	0.0058	Polished copper	0.0128
Chemically etched stainless steel	0.0133	Lapped copper	0.0147
Mechanically polished stainless steel	0.0132	Scored copper	0.0068

W-15 (I) :

MCFRSC Critical heat flux model selection. The value is used only when IVLRSC > 0.

- 1 Zuber pool boiling correlation with Ivey-Morris correction for subcooling.
- 2 Combination of model based on USSR Academy of Sciences CHF look-up tables for high flow, with Zuber and Ivey-Morris for low flow.

- 3 Combination of Biasi correlation for high flow, with Zuber and Ivey-Morris for low flow.
- Groeneveld (1986) look-up tables. 4
- $<\!\!0$ CHF is calculated by a user-defined Control Function with the number | MCFRSC |.

Acceptable range: 1, 2, 3 or reference to a Control Function Default value: 2.

W-16(I): MNCRSC Selection of model for the influence of noncondensable gases for condensation. The value is used only when IVLRSC is positive and ICNRSC is greater than –4. The meaning of this variable is as follows:

- Kuhn-Shrock-Petersen (KSP) correlations recommended for 1 condensation on the inside surface of tubes,
- 2 Ogg correlations,
- Modified Ogg correlations recommended for condensation on 3 the outside surface of tubes, plates, etc.

Default values are provided - see Table 2-14 and Table 2-15).

Acceptable range: 1, 2, 3. 3.

Default value:

W-17 (R): **CFDRSC** Indicator of condensate film drainage behavior.

If the value is positive then CFDRSC is the height of the right SC surface. The elevation of the lowermost point of this surface is equal to the elevation of its center point, minus CFDRSC/2.0.

The drainage from this surface is either deposited in the pool of a CV (if the lowest point of the surface is immersed in pool), or converted to droplets and suspended in the atmosphere of a CV as "rain" drops (if the lowest point of the surface is not immersed in the pool).

If the value is <u>negative</u> then the drainage is assumed to be deposited on a surface of other (lower) Solid Conductor. The absolute value of CFDRSC must then be equal to the number of SC at the bottom of the stack.

The use of the drainage parameter, CFDRSC, and the condensation characteristic dimension, DCNRSC, on the right surface of SC is the same as for the left surface of SC. The use of DCNRSC and CFDRSC in case of individual and stacked conductors is illustrated in Figure 2-14 and Table 2-4, section 2.3.11.

Acceptable range: if CFDRSC<0.0 then the right surface of SC No. CFDRSC must be connected to a Control Volume (not necessarily equal to IVLRSC), if CFDRSC>0.0 then the bottom elevation of the right surface (centre point elevation, minus CFDRSC/2.0) must be within the boundary Control Volume.

the default value is set to twice the distance between Default value: the centre point of the right surface and the bottom of the boundary Control Volume. That value will result in deposition of condensate always in the pool. This is done to avoid numerical problems, and time step reduction, when condensate is converted into droplets. The most realistic treatment (although typically more time consuming) is obtained by

setting CFDRSC equal to the physical height of the right surface. The influence of the value of CFDRSC on the results is, in practical cases, negligible.

W-18 (I): IHDRSC Indicator of CV flow direction relative to the right SC surface. Used only for rectangular (IGEOSC=1) SC's. The meaning is: For vertical SC's (IVERSC=0): CV horizontal flow is parallel,  $v_{SC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2},$ 0: CV horizontal flow is perpendicular,  $v_{SC} = v_{CV,ver}$ . 1: For horizontal SC's (IVERSC<>0):  $v_{SC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2},$ CV vertical flow is parallel, 0: CV vertical flow is perpendicular, 1:  $v_{SC} = v_{CV,ver}$ . Acceptable range:  $0 \leq \text{IHDRSC} \leq 1$ . Default value: 0.

W-19 (I): THTRSC Contact angle,  $\theta$ , (degree). Used to determine diameter of bubbles created during nucleate boiling:  $D = 0.0208 \cdot \theta \cdot (\sigma/g/(\rho_{liq}-\rho_{gas}))^{(1/2)}$ . Acceptable range:  $10^{\circ} \leq \text{THTRSC} \leq 180^{\circ}$ . Default value:  $96^{\circ}$ .

W-20 (R): XRBRSC Multiplier for convective heat transfer,  $X_{RB}$ . XRBRSC<0.0: HTC is multiplied by |XRBRSC| in both natural and force convection. It may be used to obtain a conservative estimation of heat transfer. XRBRSC>0.0: HTC is multiplied by XRBRSC only in case of turbulent forced convection (FC-TUR), internal flow (IFCRSC = -1). It is intended to allow the user to define a rod bundle multiplier in forced convection:

 $Nu_{tur} = X_{RB} 0.023 Re^{0.8} Pr^{0.4}$ 

Appropriate values for parallel flow and cross-flow may be found in literature. The ratio of pitch over diameter is a good approximation (see Volume 1, description of forced convection correlations):

$$X_{RB} = P / D$$

For tube arrangements other than equilateral triangle pitch, the multiplier is given by:

$$X_{RB} = \left(\frac{P_1 \cdot P_2}{D^2}\right)$$

Note that the rod bundle multiplier may be different for different fluids. For example, for the liquid metals the value may even show different tendency (see Volume 1, description of liquid metals correlations):

$$X_{RB} = 1 - \exp[-3.8 \cdot (P/D - 1)]$$

		Acceptable range: Default value:	$0.0 \le  \text{XRBRSC}  \le 10^6$ XRBRHT (global activator, defined in the record 810020)
W-21 (I) :	IHCRSC	Selection of heat tra Acceptable range:	ansfer correlation for alternative fluid. one of the correlations defined in records 843XXX or 843YYY
		Default value:	rectangular: 1, cylindrical: 2, spherical: 3.

IVE-	Rectangular		Cylin	Cylindrical		Spherical	
RSC	Left	Right	Left	Right	Left Right		
0	INCLSC: 0	INCRSC: 0	INCLSC: 0	INCRSC: 0	INCLSC: -1	INCRSC: +1	
	DNCLSC: H	DNCRSC: H	DNCLSC: L	DNCRSC: L	DNCLSC: D	DNCRSC: D	
	Eq. Set: (1)	Eq. Set: (1)	Eq. Set: (1)	Eq. Set: (1)	Eq. Set: (6)	Eq. Set: (6)	
	alternative:	alternative:	alternative:	alternative:	no alternative:	no alternative:	
	INCLSC: $\neq 0$	INCLSC: $\neq 0$	INCLSC: $\neq 0$	INCLSC: $\neq 0$			
-1	INCLSC: -1	INCRSC: +1	INCLSC: -1	INCRSC: +1			
	DNCLSC: W	DNCRSC: W	DNCLSC:L<2D	DNCRSC: D			
	Eq. Set:	Eq. Set:	Eq. Set: (4)	Eq. Set: (5)			
	- if $T_w > T_f$ (3)	- if $T_w > T_f$ (2)					
	- if $T_w < T_f$ (2)	- if $T_w < T_f$ (3)	alternative:	alternative:			
+1	INCLSC: +1	INCRSC: -1	INCLSC: $\neq -1$	INCLSC: $\neq +1$			
	DNCLSC: W	DNCRSC: W					
	Eq. Set:	Eq. Set:					
	- if $T_w > T_f$ (2)	- if $T_w > T_f$ (3)					
	- if $T_w < T_f$ (3)	- if $T_w < T_f$ (2)					

Table 2-6 Natural convection - input options, characteristic dimensions, equations.

H - height, W - width, L - length, D - diameter.

Table 2-7	Natural convection correlations (for (Gr Pr)<10 <sup>4</sup> the "recommended curves" - see
	Volume 1 - are used).

Geometry	0	Open for natural circulation <sup>(*)</sup>	Closed f	for natural circulation <sup>(*)</sup> (enclosures)
Vertical plate	Source:	McAdams, Holman	N/A	
	Ch. Dim.:	height, H		
	Correl.:	$Nu = 0.59 \cdot (Gr \cdot Pr)^{1/4}$		
		$Nu = 0.10 \cdot (Gr \cdot Pr)^{1/3}$		
	Set No.:	(1)		
Horizontal plate	Source:	McAdams	Source:	McAdams
	Ch. Dim.:	width, W	Ch. Dim.:	width, W
	Correl.:	$Nu = 0.54 \cdot (Gr \cdot Pr)^{1/4}$	Correl.:	$Nu = 0.27 \cdot (Gr \cdot Pr)^{1/4}$
		$Nu = 0.14 \cdot (Gr \cdot Pr)^{1/3}$		
	Set No.:	(2)	Set No.:	(3)
Vertical cylinder	Source:	McAdams, Holman	Source:	Holman
	Ch. Dim.:	length, L	Ch. Dim.:	length, $L < 2D$
	Correl.:	$Nu = 0.59 \cdot (Gr \cdot Pr)^{1/4}$	Correl.:	$Nu = 0.55 \cdot (Gr \cdot Pr)^{1/4}$
		$Nu = 0.10 \cdot (Gr \cdot Pr)^{1/3}$		
	Set No.:	(1)	Set No.:	(4)
Horizontal cylinder	Source:	McAdams, Holman	Source:	Holman
	Ch. Dim.:	diameter, D	Ch. Dim.:	diameter, D
	Correl.:	$Nu = 0.53 \cdot (Gr \cdot Pr)^{1/4}$	Correl.:	$Nu = 0.55 \cdot (Gr \cdot Pr)^{1/4}$
		$Nu = 0.13 \cdot (Gr \cdot Pr)^{1/3}$		
	Set No.:	(5)	Set No.:	(4)
Sphere	Source:	Holman	Source:	Holman
	Ch. Dim.:	diameter, D	Ch. Dim.:	diameter, D
	Correl.:	$Nu = 2 + 0.43 \cdot (Gr \cdot Pr)^{1/4}$	Correl.:	$Nu = 2 + 0.43 \cdot (Gr \cdot Pr)^{1/4}$
	Set No.:	(6)	Set No.:	(6)

References are: Holman [9], McAdams [18].

(\*) The meaning of "Open" and "Closed" is as follows:

-	Horizontal plates	Open:	hot surface facing upwards or cold surface facing downwards.
		Closed:	cold surface facing upwards or hot surface facing downwards.
-	Cylinders	Open:	large vertical cylinders, outer surface of horizontal cylinders that are not enclosed by other surfaces
		Closed:	inner surface of small cylinders, horizontal cylinders enclosed by other surfaces
-	Spheres	Open:	large spheres, outer surface of spheres that are not enclosed by other surfaces
		Closed:	inner surface of small spheres, sphere surfaces enclosed by other surfaces

Table 2-8 Forced convection - input options, characteristic dimensions, equations.

Rectar	ngular	Cylin	drical	Spherical			
Left	Right	Left	Right	Left	Right		
IFCLSC:-1DFCLSC:DhydEq. Set:(1)	IFCRSC:-1DFCRSC:DhydEq. Set:(1)	IFCLSC: -1 DFCLSC: D <sub>hyd</sub> Eq. Set: (1)	IFCRSC:-1DFCRSC:DhydEq. Set:(1)	IFCLSC: -1 DFCLSC: D <sub>hyd</sub> Eq. Set: (1)	IFCRSC: -1 DFCRSC: D <sub>hyd</sub> Eq. Set: (1)		
alternative: IFCLSC: +1 DFCLSC: W Eq. Set: (2)	alternative: IFCLSC: +1 DFCLSC: W Eq. Set: (2)	alternative: IFCLSC: +1 DFCLSC: D Eq. Set: (2)	alternative: IFCRSC: +1 DFCRSC: D Eq. Set: (2)	alternative: IFCLSC: +1 DFCLSC: D Eq. Set: (3)	alternative: IFCRSC: +1 DFCRSC: D Eq. Set: (3)		

W - width, D<sub>hyd</sub> - hydraulic diameter.

Geometry	Internal flow	External flow
Rectangular	Source : Rohsenow	Source : Holman
-	Ch.Dim.: hydraulic diameter, D <sub>hyd</sub>	Ch.Dim.: width, W
	Correl.: $Nu = 3.656$	Correl.: $Nu = (0.35 + 0.56 Re^{0.52}) Pr^{0.3}$
	$Nu = 0.023 \ Re^{0.8} \ Pr^{0.4}$	$Nu = 0.037 \ Re^{0.8} \ Pr^{1/3}$
	Set No.: (1)	Set No.: (2)
Cylindrical	Source : Rohsenow	Source : Holman
	Ch.Dim.: hydraulic diameter, D <sub>hyd</sub>	Ch.Dim.: diameter, D
	Correl.: $Nu = 3.656$	Correl.: $Nu = (0.35 + 0.56 Re^{0.52}) Pr^{0.3}$
	$Nu = 0.023 \ Re^{0.8} \ Pr^{0.4}$	$Nu = 0.037 \ Re^{0.8} \ Pr^{1/3}$
	Set No.: (1)	Set No.: (2)
Spherical	Source : Rohsenow	Source : Holman
	Ch.Dim.: hydraulic diameter, D <sub>hyd</sub>	Ch.Dim.: diameter, D
	Correl.: $Nu = 3.656$	Correl.: $Nu = 2 + (0.4 Re^{0.5} + Pr^{0.3})$
	$Nu = 0.023 \ Re^{0.8} \ Pr^{0.4}$	$+ 0.06 Re^{2/3}) Pr^{1/3}$
	Set No.: (1)	Set No.: (3)

Table 2-9 Forced convection correlations.

References: Holman [9], Rohsenow [14].

IVE-	Recta	ngular	Cylin	drical	Spherical		
RSC	Left	Right	Left	Right	Left	Right	
0	IFBLSC: 0	IFBRSC: 0	IFBLSC: 0	IFBRSC: 0	IFBLSC: 0,	IFBRSC: 0,	
	DFBLSC: H	DFBRSC: H	DFBLSC: L	DFBRSC: L	±1	±1	
	Eq. Set: (1)	Eq. Set: (1)	Eq. Set: (1)	Eq. Set: (1)	DFBLSC: D	DFBRSC: D	
					Eq. Set: (4)	Eq. Set: (4)	
	alternative:	alternative:	alternative:	alternative:	_	_	
	IFBLSC $\neq 0$	IFBLSC $\neq 0$	IFBLSC $\neq 0$	IFBLSC $\neq 0$	no alternative	no alternative	
-1	IFBLSC: -1	IFBRSC: +1	IFBLSC: ±1	IFBRSC: ±1			
	DFBLSC: W	DFBRSC: cw	DFBLSC: D	DFBRSC: D			
	Eq. Set: (3)	Eq. Set: (2)	Eq. Set: (4)	Eq. Set: (4)			
			_	_			
	alternative:	alternative:	alternative:	alternative:			
	IFBLSC $\neq -1$	IFBLSC $\neq +1$	IFBLSC = 0	IFBLSC = 0			
+1	IFBLSC: +1	IFBRSC: -1					
	DFBLSC: cw	DFBRSC: W					
	Eq. Set: (2)	Eq. Set: (3)					
	alternative:	alternative:					
	IFBLSC $\neq +1$	IFBLSC ≠ −1					

#### Table 2-10 Film boiling - input options, characteristic dimensions, equations.

H - height, W - width, L - length, D - diameter, cw - critical wavelength,  $cw = (\sigma/g(\rho_1 - \rho_g)^{1/2} (calculated internally by the code).$ 

Except for the spherical geometry, the user can select the film boiling correlation by changing the default value of IFBLSC / IFBRSC. For example, in case of rectangular geometry, IGEOSC = 1, horizontal, left side down structure, IVERSC= -1, the default value on the film boiling indicator on the left surface is IFBLSC = -1 (downwards surface). The user can change it to 0 (vertical) or even +1 (upwards surface), thus activating the appropriate correlations. There should be however a clear reason to change the default settings for the film boiling model.

Table 2-11	Film	boilina	correlations.
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Geometry	Correlation	Geometry	Correlation		
Vertical walls	Correl.: Bromley	Vertical cylinders	Correl.: Bromley		
	Const. : $C = 0.625$		Const. : $C = 0.625$		
	Ch.dim.: $D_0$ = height, H		Ch.dim.: $D_0 =$ height, H		
	Eq.No.: (1)		Eq.No.: (1)		
Horizontal walls,	Correl.: Berenson	Horizontal cylinders	Correl.: Bromley		
facing up	Const. : $C = 0.425$		Const. : $C = 0.620$		
	Ch.dim.: $D_0 = (\sigma/g(\rho_{\text{liq}} - \rho_{\text{vap}}))^{1/2}$		Ch.dim.: $D_0$ = diameter		
	Eq.No.: (2)		Eq.No.: (4)		
Horizontal walls,	Correl.: Berenson	Spheres	Correl.: Bromley		
facing down	Const. : $C = 0.425$		Const. : $C = 0.620$		
	Ch.dim.: $D_0$ = width, W		Ch.dim.: $D_0$ = diameter		
	Eq.No.: (3)		Eq.No.: (4)		

References: Bromley [19], Berenson [20].

The table above gives the value of the constant C, and the characteristic dimension  $D_0$ , in the general film boiling correlation:

$$h = C \left( \frac{k_{vap}^{3} \rho_{vap} g(\rho_{liq} - \rho_{vap})(h_{l-v} + 0.4c_{p,vap} \Delta T_{sat}}{\eta_{vap} D_{0} \Delta T_{sat}} \right)^{0.25}$$

IVERSC	Rectangular		Cylin	drical	Spherical		
	Left Right		Left Right		Left	Right	
0	ICNLSC: 0	ICNRSC: 0	ICNLSC: 0	ICNRSC: 0	ICNLSC: -1	ICNRSC: -1	
	DCNLSC: H	DCNRSC: H	DCNLSC: L	DCNRSC: L	DCNLSC: D	DCNRSC: D	
	Eq. No. (1)	Eq. No. (1)	Eq. No. (1)	Eq. No. (1)	Eq. No. (2)	Eq. No. (2)	
	alternative:	alternative:	alternative:	alternative:	alternative:	alternative:	
	ICNLSC $\neq 0$	ICNRSC $\neq 0$	ICNLSC $\neq 0$	ICNRSC $\neq 0$	ICNLSC $\neq -1$	ICNRSC $\neq -1$	
-1	ICNLSC: -2	ICNRSC: -3	ICNLSC: -1	ICNRSC: -1			
	DCNLSC: cw	DCNRSC: <b>δ</b>	DCNLSC: D	DCNRSC: D			
	Eq. No. (4)	Eq. No. (5)	Eq. No. (2)	Eq. No. (2)			
	alternative:	alternative:	alternative:	alternative:			
	ICNLSC $\neq -2$	ICNRSC ≠ -3	ICNLSC $\neq -1$	ICNRSC $\neq -1$			
+1	ICNLSC: -3	ICNRSC: -2					
	DCNLSC: <b>δ</b>	DCNRSC: cw					
	Eq. No. (5)	Eq. No. (4)					
	alternative:	alternative:					
	ICNLSC $\neq -2$	ICNRSC ≠ −2					

Table 2-12 Pure steam condensation - input options, characteristic dimensions, equations.

H - height, W - width, L - length, D - diameter, cw - critical wavelength,  $cw = (\sigma/g(\rho_{\Gamma}-\rho_{g})^{1/2} (calculated internally by the code).$ 

Configuration	Correlation					
Vertical walls and cylinders	Source :	Nusselt,				
	Ch.Dim.:	wall height, H				
	Correl.:	$0.943 (g \rho_{liq} (\rho_{liq} - \rho_{gas}) k^{3}_{liq} h_{l-v} / H \eta_{liq} \Delta T_{sat.})^{0.25}$				
	Eq. No.:	(1)				
Inside tubes	Source :	Nusselt, Chato,				
	Ch.Dim.:	inner diameter, D				
	Correl.:	$0.555 (g \rho_{liq} (\rho_{liq} - \rho_{gas}) k^{3}_{liq} h_{l-\nu} / D \eta_{liq} \Delta T_{sat.})^{0.25} (1+\theta^{\circ}/100)$				
	Eq. No.:	(2)				
Outside tubes and tube banks	Source :	Nusselt,				
	Ch.Dim.:	outer diameter, D				
	Correl.:	$0.728 (g \rho_{liq} (\rho_{liq} - \rho_{gas}) k^{3}_{liq} h_{l.v} / N_{row} D \eta_{liq} \Delta T_{sat.})^{0.25}$				
	Eq. No.:	(3)				
Horizontal walls, facing down	Source :	Gerstmann and Griffith,				
	Ch.Dim.:	not used				
	Correl.:	$k_{liq}/D_x 0.9 \tau^{-1/6}/(1+1.1 \tau^{1/6})$ where $D_x$ is the critical wavelength				
	Eq. No.:	(4)				
Horizontal walls, facing up	Source :	Maximum film thickness concept				
	Ch.Dim.:	Maximum film thickness, $\delta$				
	Correl.:	$k_{liq}/\delta$				
	Eq. No.:	(5)				

References: Nusselt [23], Chato [21], Gerstmann and Griffith [22].

				r				r			
Rectangular			Cylindrical			Vertical					
Left		Right		Left		Right	:	Left		Right	
MCNLSC:	3	MCNRSC:	3	MCNLSC:	3	MCNRSC:	3	MCNLSC:	3	MCNRSC:	3
Corr.:		Corr.:		Corr.:		Corr.:		Corr.:		Corr.:	
M.Ogg		M.Ogg		M.Ogg		M.Ogg		M.Ogg		M.Ogg	
Eq. No.	(3)	Eq. No.	(3)	Eq. No.	(3)	Eq. No.	(3)	Eq. No.	(3)	Eq. No.	(3)
-		-		-		-		-		-	
alternative:		alternative:		alternative:		alternative:		alternative:		alternative:	
MCNLSC:	1	MCNRSC:	1	MCNLSC:	1	MCNRSC:	1	MCNLSC:	1	MCNRSC:	1
Corr.:	KSP	Corr.:	KSP	Corr.:	KSP	Corr.:	KSP	Corr.:	KSP	Corr.:	KSP
Eq. No.:	(1)	Eq. No.:	(1)	Eq. No.:	(1)	Eq. No.:	(1)	Eq. No.:	(1)	Eq. No.:	(1)
-		_		_		_		_		_	
MNCLSC:	2	MNCRSC:	2	MNCLSC:	2	MNCRSC:	2	MNCLSC:	2	MNCRSC:	2
Corr.:	Ogg	Corr.:	Ogg	Corr.:	Ogg	Corr.:	Ogg	Corr.:	Ogg	Corr.:	Ogg
Eq. No.:	(2)	Eq. No.:	(2)	Eq. No.:	(2)	Eq. No.:	(2)	Eq. No.:	(2)	Eq. No.:	(2)

Table 2-14 Non-condensable degradation factor - input options, equations.

Table 2-15 Non-condensable degradation factor correlations.

Model	
Kuhn-Shrock-Petersen	Source : KSP (inside tube condensation)
	Correl.: steam-air: $f_{NC}=1-2.601 X_a^{0.701}$ for $X_a < 0.10$
	$1 - X_a^{0.292}$ for $X_a > 0.10$
	steam-He: $f_{NC}=1-35.81 \text{ X}_{He}^{1.074}$ for $X_{He} < 0.01$
	$1 - 2.09 X_{\rm He}^{0.457}$ for $X_{\rm He} < 0.10$
	$1 - X_{He}^{0.137}$ for $X_{He} > 0.10$
	Set No.: (1)
Ogg	Source : Ogg (outside wall condensation)
	Correl.: steam-air: $f_{NC}=1-1.165 X_a^{0.26}$ for $X_a < 0.30$
	$1 - 0.905 X_a^{0.05}$ for $X_a < 0.90$
	$1 - X_a$ for $X_a > 0.90$
	steam-He: $f_{NC}=1-1.590 \text{ X}_{\text{He}}^{0.29}$ for $\text{X}_{\text{He}} < 0.11$
	$1 - 1.865 X_{\rm He}^{0.014}$ for $X_{\rm He} < 0.86$
	$1 - X_{He}$ for $X_{He} > 0.86$
	Set No.: (2)
Modified Ogg	Source : Modified Ogg (outside wall condensation)
	Correl.: steam-air: $f_{NC}=1-1.165 X_a^{0.26}$ for $X_a < 0.30$
	$0.21 - 0.21 X_a$ for $X_a < 0.30$
	steam-He: $f_{NC}=1-1.590 \text{ X}_{\text{He}}^{0.29}$ for $\text{X}_{\text{He}} < 0.12$
	$0.16 - 0.16 X_{He}$ for $X_{He} > 0.12$
	Set No.: (3)

References: KSP [24], Ogg [25], Modified Ogg [25], [26].

#### 2.3.13 Records: 323XXX, Left Side Extended Surface Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . It should be noted that if a Solid Conductor is used to represent a wall with fins or spines then the cell data (records 310XXX) should represent only the wall, and not the fins/spines. Fins/spines are accounted for in calculations using a simplified method, based on theoretical temperature profiles inside fins/spines. Those profiles are appropriate for steady-state conditions (see Volume 1).

- W-1 (I): ITFLSC Type of extended surface:
  - 1: fins (Figure 2-15 a, b),

2: spines (Figure 2-15 c).

- Acceptable range: 0, 1, 2. Fins are allowed only if IGEOSC = 1 or 2 (rectangular or cylindrical). If fins are used on the left surface of a cylindrical SC, then the rectangular fin model (Figure 2-15 a) is used. This means the inner radius of the cylinder is assumed to be large compared to the fin size. Spines can be used with all For cylindrical and spherical geometries. geometries it is assumed that the surface radius of curvature is large compared to the spine length. Fins and spines can be used only if IVLLSC > 0. Default value: 0 (no extended surface model).
- W-2 (R):THFLSCHalf thickness of fin/spine, (m). THFLSC is denoted in Figure 2-15 as: t.Acceptable range: $0.0 < THFLSC \le 1.0$ .Default value:none.



Figure 2-15 Fins and spines.

W-3 (R) :	XLFLSC	Length of fin/spine Acceptable range:	e, (m). XLFLSC is denoted in Figure 2-15 as: L. $10^{-10} < XLFLSC \le 10.0$ . In case of fins on cylinders and spines on cylinders and spheres, the length cannot be greater than 90% of the inner radius XLFLSC $\le XOSC \times 0.90$ .			
		Default value:	none.			
W-4 (R) :	DDFLSC	Effective distance	between fin/spines, (m). DDFLSC is denoted in			

**W-4 (R)**: DDFLSC Effective distance between fm/spines, (m). DDFLSC is denoted in Figure 2-15 as:  $\Delta$ . In case of fins  $\Delta$  is equal to the distance between the fin centers - Figure 2-15 (a). In case of spines  $\Delta$  is equal to the diameter of a circle which has the same area as the area associated with a single spine - Figure 2-15 (c). If the spines are arranged in a square lattice, then the surface area associated with a single spine is equal to:  $a^2_{centre}$ , where  $a_{centre}$  is the distance between the centers of two neighboring spines. The effective distance,  $\Delta$ , is obtained from:  $\pi \cdot \Delta^2/4 = a^2_{centre}$ . Thus:

$$\begin{split} \Delta &= a_{centre} \cdot 2/\pi^{1/2} = 1.128 \cdot a_{centre}. \\ \text{In case of hexagonal spines arrangement the effective distance is equal to:} \\ \Delta &= \Delta_{\text{centre}} \cdot (2/\pi)^{1/2} \cdot 3^{1/4} = 1.050 \cdot a_{centre}. \\ Acceptable range: 2 \cdot t < \text{DDFLSC} \le 1.0 . \\ Default value: none. \end{split}$$

- W-5 (R): TCFLSC Thermal conductivity of the fin/spine material, (W/m<sup>2</sup>K). If a positive number is entered, the fin conductivity is constant and equal to this value while the fin heat capacity is neglected. If a negative number is entered, the absolute value is the reference number of the fin material.
  - Acceptable range: TCFLSC  $\leq 10^{10}$ . Must be a valid reference to an existing material, if less than zero.
  - *Default value:* reference number of the boundary cell material. If the fin material is different from the boundary cell material then those materials must have the same or similar heat capacities.

diagnostics output will point out that DNCLSC is

W-6 (R) :DNFLSCCharacteristic dimension for natural convection, (m). When the<br/>extended surface model is activated, then the characteristic dimension<br/>for the left surface natural convection (DNCLSC, entered in the record<br/>321XXX - section 2.3.11), is overwritten by this value.<br/>Acceptable range: the same as for DNCLSC:<br/> $0.0 < DNFLSC < 10^{10}$ <br/>Note! This input entry is only used to overwrite the<br/>value of DNCLSC for this surface. Further<br/>diagnostics is performed for DNCLSC. Thus if an<br/>unacceptable value is entered for DNFLSC then the

*Default value:* out of the permitted range. length of the fin/spine: L.

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W-7 (R) :	DFFLSC	Characteristic dime surface model is ac surface forced com section 2.3.11), is of <i>Acceptable range:</i> <i>Default value:</i>	ension for forced convection, (m). When the extended etivated, then the characteristic dimension for the left vection (DFCLSC, entered in the record 321XXX - overwritten by this value. the same as for DFCLSC: $0.0 < DFFLSC < 10^{10}$ . Note! This input entry is only used to overwrite the value of DFCLSC for this surface. Further diagnostics is performed for DFCLSC. Thus if an unacceptable value is entered for DFFLSC then the diagnostics output will point out that DFCLSC is out of the permitted range. effective distance between fins/spines: $\Delta$ .
W-8 (R) :	DBFLSC	Characteristic dim surface model is ac surface film boiling 2.3.11), is overwrit Acceptable range: Default value:	ension for film boiling, (m). When the extended trivated, then the characteristic dimension for the left g (DFBLSC, entered in the record 321XXX - section ten by this value. the same as for DFBLSC: $0.0 < DBFLSC < 10^{10}$ . Note! This input entry is only used to overwrite the value of DFBLSC for this surface. Further diagnostics is performed for DFBLSC. Thus if an unacceptable value is entered for DBFLSC then the diagnostics output will point out that DFBLSC is out of the permitted range. length of the fins/spines: L.
W-9 (R) :	DMFLSC	Characteristic dime surface model is ac surface condensati section 2.3.11), is of <i>Acceptable range:</i> <i>Default value:</i>	ension for condensation, (m). When the extended tivated, then the characteristic dimension for the left on (DCNLSC, entered in the record 321XXX - overwritten by this value. the same as for DCNLSC: $0.0 < DMFLSC < 10^{10}$ . Note! This input entry is only used to overwrite the value of DCNLSC for this surface. Further diagnostics is performed for DCNLSC. Thus if an unacceptable value is entered for DMFLSC then the diagnostics output will point out that DCNLSC is out of the permitted range. length of the fins/spines: L.

## 2.3.14 Records: 324XXX, Right Side Extended Surface Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . It should be noted that if a Solid Conductor is used to represent a wall with fins or spines then the cell data (records 310XXX) should represent only the wall, and not the fins/spines. Fins/spines are accounted for in calculations using a simplified method, based on theoretical temperature profiles inside fins/spines. Those profiles are appropriate for steady-state conditions (see Volume 1).

W-1 (I):	ITFRSC	C Type of extended surface:			
		1: fins (Figure	2-15 a, b),		
		2: spines (Figu	re 2-15 c).		
		Acceptable range:	0, 1, 2. Fins are allowed only if $IGEOSC = 1$ or 2		
			(rectangular or cylindrical). If fins are used on the		
			right surface of a cylindrical SC, then the cylindrical		
			fin model (Figure 2-15 b) is used. Spines can be		
			used with all geometries. For cylindrical and		
			spherical geometries it is assumed that the surface		
			radius of curvature is large compared to the spine		
			> 0		
		Default value:	0 (no extended surface model).		
		2 550000 700000			
W-2 (R) :	THFRSC	Half thickness of fi	n/spine, (m). THFRSC is denoted in Figure 2-15 as: t.		
		Acceptable range:	$0.0 < \text{THFRSC} \le 1.0$ .		
		Default value:	none.		
W-3 (R) :	XLFRSC	Length of fin/spine	(m). XLFRSC is denoted in Figure 2-15 as: L.		
		Acceptable range:	$10^{-10} < \text{XLFRSC} \le 10.0$ .		
		Default value:	none.		
W-4(R)	DDFRSC	Effective distance	between fin/spines (m) DDFRSC is denoted in		
	DDIIGC	Figure 2-15 as: $\Delta$ .	In case of fins $\Delta$ is equal to the distance between the		
		fin centers - Figure	e 2-15 (a) and (b). In case of spines $\Delta$ is equal to the		
		diameter of a circle	e that has the same area as the area associated with a		
		single spine - Figu	are 2-15 (c). If the spines are arranged in a square		
		lattice, then the sur	face area associated with a single spine is equal to:		
		$a^{2}_{centre}$ , where $a_{cer}$	tre is the distance between the centers of two		
		neighboring spine	s. The effective distance, $\Delta$ , is obtained from:		
		$\pi \cdot \Delta^2/4 = a^2_{centre}$ . Thu	S:		
		$\Delta = a_{centre} \cdot 2/\pi^{1/2}$	$= 1.128 \cdot a_{centre}.$		
		to:	ai spines arrangement me effective distance is equal		
		$\Delta = \Delta_{\text{centre}} \cdot (2/\pi)^{1/2} \cdot 3$	$^{1/4} = 1.050 \cdot a_{centre}.$		
		Acceptable range:	$2 \cdot t < \text{DDFRSC} \le 1.0$ .		
		Default value:	none.		

TCFRSC W-5 (R): Thermal conductivity of the fin/spine material,  $(W/m^2/K)$ . If a positive number is entered, the fin conductivity is constant and equal to this value while the fin heat capacity is neglected. If a negative number is entered, the absolute value is the reference number of the fin material. Acceptable range: TCFRSC  $\leq 10^{10}$ . Must be a valid reference to an existing material, if less than zero. reference number of the boundary cell material. If Default value: the fin material is different from the boundary cell material then those materials must have the same or similar heat capacities. W-6(R): **DNFRSC** Characteristic dimension for natural convection, (m). When the extended surface model is activated, then the characteristic dimension for the right surface natural convection (DNCRSC, entered in the record 322XXX - section 2.3.12), is overwritten by this value. Acceptable range: the same as for DNCRSC:  $0.0 < DNFRSC < 10^{10}$ . Note! This input entry is only used to overwrite the value of DNCRSC for this surface. Further diagnostics is performed for DNCRSC. Thus if an unacceptable value is entered for DNFRSC then the diagnostics output will point out that DNCRSC is out of the permitted range. Default value: spines and fins for rectangular geometry: length of the fin/spine: L; fins for cylindrical geometry:  $(\pi/4)\cdot(D_{fin}^2-D_{tube}^2)/D_{fin}$ , where  $D_{tube}$  is the outer diameter of the tube, and  $D_{\text{fin}}$  is the outer diameter of the fin, equal to:  $(D_{tube} + 2 \cdot L)$  - see Figure 2-15. The formula applied here is the same as that used typically to determine the characteristic dimension for condensation [3]. W-7 (R): DFFRSC Characteristic dimension for forced convection, (m). When the extended surface model is activated, then the characteristic dimension for the right surface forced convection (DFCRSC, entered in the record 322XXX section 2.3.12), is overwritten by this value. Acceptable range: the same as for DFCRSC:  $0.0 < DFFRSC < 10^{10}$ . Note! This input entry is only used to overwrite the value of DFCRSC for this surface. Further diagnostics is performed for DFCRSC. Thus if an

> out of the permitted range. *Default value:* effective distance between fins/spines:  $\Delta$ .

unacceptable value is entered for DFFRSC then the diagnostics output will point out that DFCRSC is

W-8 (R): DBFRSC Characteristic dimension for film boiling, (m). When the extended surface model is activated, then the characteristic dimension for the right surface film boiling (DFBRSC, entered in the record 322XXX - section 2.3.12), is overwritten by this value.

Acceptable range: the same as for DFBRSC:

neceptuble tange.	the sume as for DI DRDC.
	$0.0 < DBFRSC < 10^{10}$
	Note! This input entry is only used to overwrite the
	value of DFBRSC for this surface. Further
	diagnostics is performed for DFBRSC. Thus if an
	unacceptable value is entered for DBFRSC then the
	diagnostics output will point out that DFBRSC is
	out of the permitted range.
Default value:	spines and fins for rectangular geometry:
	length of the fin/spine: L;
	fins for cylindrical geometry:
	$(\pi/4) \cdot (D_{\text{fin}}^2 - D_{\text{tube}}^2) / D_{\text{fin}}$ , where $D_{\text{tube}}$ is the outer
	diameter of the tube, and D <sub>fin</sub> is the outer diameter
	of the fin. equal to: $(D_{tube} + 2 \cdot L)$ - see Figure 2-15.
	The formula applied here is the same as that used
	typically to determine the characteristic dimension
	for condensation [3].

W-9 (R): DMFRSC Characteristic dimension for condensation, (m). When the extended surface model is activated, then the characteristic dimension for the right surface condensation (DCNRSC, entered in the record 322XXX - section 2.3.12), is overwritten by this value. *Acceptable range:* the same as for DCNRSC:

1 0	
	$0.0 < DMFRSC < 10^{10}$
	Note! This input entry is only used to overwrite the
	value of DCNRSC for this surface. Further
	diagnostics is performed for DCNRSC. Thus if an
	unacceptable value is entered for DMFRSC then the
	diagnostics output will point out that DCNRSC is
	out of the permitted range.
Default value:	spines and fins for rectangular geometry:
	length of the fin/spine: L;
	fins for cylindrical geometry [3]:
	$(\pi/4) \cdot (D_{\text{fin}}^2 - D_{\text{tube}}^2) / D_{\text{fin}}$ , where $D_{\text{tube}}$ is the outer
	diameter of the tube, and $D_{fin}$ is the outer diameter

of the fin, equal to:  $(D_{tube} + 2 \cdot L)$  - see Figure 2-15.

### 2.3.15 Records: 325XXX, Left Side Heat Exchanger Temperature Averaging

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records may be used to model a heat exchanger. If these records are used, then an averaging procedure will be applied to calculate the representative fluid temperature at the SC surface. The representative fluid temperature will be equal to the weighted average of the inlet and outlet fluid temperatures. Note that if the temperature averaging is not used, then the representative fluid temperature is always equal to the fluid temperature in the boundary volume, which means it is equal to the outlet temperature. As shown in Volume 3, when the temperature-averaging concept is not used, a large number of nodes (~100) may be required to obtain accurate results. With the temperature averaging the same accuracy may be obtained using only a few nodes. An example of the temperature averaging is shown below - see Figure 2-16 and the corresponding discussion.

Inlet Junction Data:

W-1 (I) :	JTALSC (1)	Junction reference number of the inlet Junction on the current (left)side.Acceptable range:must be a Junction connected to the left boundary Control Volume (IVLLSC), if non-zero.Default value:none.
W-2 (R) :	WTALSC (1)	Limiting mass flow in the inlet Junction JTALSC(1) for full temperature averaging ( $W_{TA,L}$ in Figure 2-16 (a) ). Applied when there is a flow through JTALSC(1) into IVLLSC and there is no flow through KTALSC(1) into IVLRSC - <u>normal flow direction on both left (primary)</u> and right (secondary) side). The temperature of the fluid entering through the Junction JTALSC(1) will be used with maximum weighting factor if the mass flow at the Junction is larger than WTALSC(1) ( $W_{JN}$ > WTALSC(1)). Generally speaking, WTALSC(1) is a flow for which the temperature distribution in the left boundary Control Volume is approximately linear, provided that there is flow in through JTALSC(1) and there is no flow in through KTALSC(1). Roughly, this number can be viewed as a nominal flow through the heat exchanger. <i>Acceptable range:</i> $10^{-10} < WTALSC(1) < 10^{10}$ . <i>Default value:</i> none.
W-3 (I) :	KTALSC (1)	Junction reference number of the outlet Junction on the other (right)side.Acceptable range:must be a Junction connected to the right boundary Control Volume (IVLRSC), if non-zero.Default value:none.
W-4 (R) :	XTALSC (1)	Limiting mass flow in the Junction JTALSC(1) for full temperature averaging ( $X_{TA,L}$ in Figure 2-16 (c) ). Applied when there is flow through JTALSC(1) into IVLLSC and simultaneously there is flow through KTALSC(1) into IVLRSC - <u>normal flow direction on the left (primary)</u> side, reversed right (secondary) side flow. The temperature of the fluid entering through the Junction JTALSC(1) will be used with maximum weighting factor if the mass flow at the Junction is larger than XTALSC(1) ( $W_{JN} > XTALSC(1)$ ). The input entries KTALSC(1) and XTALSC(1) allow the user to change the averaging weighting factors

		when flow conditions in the heat exchangers change, for example when a counter-current flow becomes co-current. Typically the temperature averaging is needed in counter-flow conditions, while it is not needed in co-flow conditions. This can be achieved by setting XTALSC(1) to a large number (for example XTALSC(1)=10 <sup>6</sup> ). Generally speaking, XTALSC(1) is a flow for which the temperature distribution in the left boundary Control Volume is approximately linear, provided that there is flow in through JTALSC(1) and KTALSC(1). <i>Acceptable range:</i> $10^{-10} < XTALSC(1) < 10^{10}$ . <i>Default value:</i> none.
		Outlet Junction Data:
W-5 (I) :	JTALSC (2)	Junction reference number of the outlet Junction on the current (left) side.
		Default value:       number of a summer of the order of the fort boundary Control Volume (IVLLSC), if non-zero.
W-6 (R) :	WTALSC (2)	Limiting mass flow in the outlet Junction JTALSC(2) for full tempera- ture averaging ( $W_{TA,L}$ in Figure 2-16 (b) ). Applied when there is flow through JTALSC(2) into IVLLSC and there is no flow through KTALSC(2) into IVLRSC - <u>reversed flow on the left (primary) side</u> , <u>normal flow direction on the right (secondary) side</u> . The temperature of the fluid entering through the Junction JTALSC(2) will be used with maximum weighting factor if the mass flow at the Junction is larger than WTALSC(2) ( $W_{JN} >$ WTALSC(2) ). Generally speaking, WTALSC(2) is a flow for which the temperature distribution in the left boundary Control Volume is approximately linear, provided that there is flow in through JTALSC(2) and there is no flow in through KTALSC(2). <i>Acceptable range:</i> 10 <sup>-10</sup> < WTALSC(2) < 10 <sup>10</sup> . <i>Default value:</i> none.
W-7 (I) :	KTALSC (2)	Junction reference number of the outlet Junction on the other (right) side. <i>Acceptable range:</i> must be a Junction connected to the right boundary
		Control Volume (IVLRSC), if non-zero. Default value: none.
W-8 (R) :	XTALSC (2)	Limiting mass flow in the outlet Junction JTALSC(2) for full tempera- ture averaging ( $X_{TA,L}$ in Figure 2-16 (d) ). Applied when there is flow through JTALSC(2) into IVLLSC and simultaneously there is flow through KTALSC(2) into IVLRSC - reversed flow on both left (primary) and right (secondary) side. The temperature of the fluid entering through the Junction JTALSC(2) will be used with maximum weighting factor if the mass flow at the Junction is larger than XTALSC(2) ( $W_{JN} > XTALSC(2)$ ). The input entries KTALSC(2) and XTALSC(2) allow the user to change the averaging weighting factors when flow conditions in the heat exchangers change, for example when a counter-current flow becomes co-current. Typically the temperature averaging is needed in counter-flow conditions, while it is not needed in co-flow conditions. This can be achieved by setting XTALSC(2) to a

large number (for example XTALSC(2)=10<sup>6</sup>). Generally speaking, XTALSC(2) is a flow for which the temperature distribution in the left boundary Control Volume is approximately linear, provided that there is flow in through JTALSC(2) and KTALSC(2). *Acceptable range:*  $10^{-10} <$ XTALSC(2)  $< 10^{10}$ . *Default value:* none.



Figure 2-16 Example of temperature averaging for a counter-flow heat exchanger.

#### 2.3.16 Records: 326XXX, Right Side Heat Exchanger Temperature Averaging

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records define the temperature averaging for the right surface of a Solid Heat Conductor (see section 2.3.15).

Inlet Junction Data

W-1 (I):	JTARSC (1)	Junction reference i side. Acceptable range: Default value:	number of the inlet Junction on the current (right) must be a Junction connected to the right boundary Control Volume (IVLRSC), if non-zero. none.
W-2 (R) :	WTARSC (1)	Limiting mass flow re averaging ( $W_{TA,I}$ , through JTARSC( KTARSC into IV (secondary) and left through the Junction factor if the mass f > WTARSC(1)). Of the temperature dis approximately lines and there is no flow be viewed as a norm <i>Acceptable range:</i> <i>Default value:</i>	<i>a</i> in the inlet Junction JTARSC(1) for full temperatu- <i>R</i> in Figure 2-16 (a) ). Applied when there is flow 1) into IVLRSC and there is no flow through <i>VLLSC</i> - <u>normal flow direction on both right</u> <u>t (primary) side</u> . The temperature of the fluid entering n JTARSC(1) will be used with maximum weighting low at the Junction is larger than WTARSC(1) ( $W_{JN}$ Generally speaking, WTARSC(1) is a flow for which stribution in the right boundary Control Volume is ar, provided that there is flow in through JTARSC(1) <i>w</i> in through KTARSC(1). Roughly, this number can ninal flow through the heat exchanger. $10^{-10} < WTARSC(1) < 10^{10}$ . none.
W-3 (I) :	KTARSC (1)	Junction reference Acceptable range: Default value:	number of the outlet Junction on the other (left) side. must be a Junction connected to the left boundary Control Volume (IVLLSC), if non-zero. none.
W-4 (R) :	XTARSC (1)	Limiting mass flow averaging ( $X_{TA,R}$ in I JTARSC(1) into T KTARSC(1) into T KTARSC(1) into T (secondary) side, re- the fluid entering t maximum weightin XTARSC(1) ( $W_{JN}$ : XTARSC(1) ( $W_{JN}$ : XTARSC(1) allow when flow condition a counter-current f averaging is needed co-flow conditions large number (for XTARSC(1) is a fle boundary Control V flow in through JTA Acceptable range: Default value:	<i>x</i> in the Junction JTARSC(1) for full temperature Figure 2-16 (b) ). Applied when there is flow through VLRSC and simultaneously there is flow through IVLLSC - <u>normal flow direction on the right</u> <u>eversed left (primary) side flow</u> . The temperature of through the Junction JTARSC(1) will be used with the factor if the mass flow at the Junction is larger than > XTARSC(1) ). The input entries KTARSC(1) and the user to change the averaging weighting factors ons in the heat exchangers change, for example when low becomes co-current. Typically the temperature 1 in counter-flow conditions, while it is not needed in . This can be achieved by setting XTARSC(1) to a the example XTARSC(1)=10 <sup>6</sup> ). Generally speaking, ow for which the temperature distribution in the right Volume is approximately linear, provided that there is ARSC(1) and KTARSC(1). $10^{-10} < XTARSC(1) < 10^{10}$ . none.

W-5 (I): JTARSC Junction reference number of the outlet Junction on the current (right) (2) side.

		Acceptable range:	must be a Junction connected to the right boundary Control Volume (IVLRSC), if non-zero.
		Default value:	none.
W-6 (R) :	WTARSC (2)	Limiting mass flow ture averaging (W) through JTARSC( KTARSC(2) into T and normal flow di the fluid entering to maximum weightin WTARSC(2) (W <sub>JN</sub> is a flow for which Control Volume is through JTARSC(2) Acceptable range: Default value:	<i>TARSC</i> (2) for full tempera- <i>TAR</i> in Figure 2-16 (c) ). Applied when there is a 2) into IVLRSC and there is no flow through VLLSC - <u>reversed flow on the right (secondary) side</u> rection on the left (primary) side. The temperature of through the Junction JTARSC(2) will be used with a factor if the mass flow at the Junction is larger than > WTARSC(2) ). Generally speaking, WTARSC(2) in the temperature distribution in the right boundary approximately linear, provided that there is flow in 2) and there is no flow in through KTARSC(2). $10^{-10} < WTARSC(2) < 10^{10}$ . none.
W-7 (I) :	KTARSC (2)	Junction reference Acceptable range: Default value:	number of the outlet Junction on the other (left) side. must be a Junction connected to the left boundary Control Volume (IVLLSC), if non-zero. none.
W-8 (R) :	XTARSC (2)	Limiting mass flow ture averaging (X <sub>T</sub> through JTARSC( through KTARSC (secondary) side an entering through the weighting factor if XTARSC(2) (W <sub>JN</sub> : XTARSC(2) allow when flow conditions a counter-current f averaging is needed co-flow conditions large number (for XTARSC(2) is a fle boundary Control V flow in through JT. Acceptable range: Default value:	<i>A</i> in the outlet Junction JTARSC(2) for full tempera- <i>A</i> <sub><i>A</i>,<i>R</i></sub> in Figure 2-16 (d) ). Applied when there is a 2) into IVLRSC and simultaneously there is flow (2) into IVLLSC - reversed flow on both right nd left (primary) side. The temperature of the fluid the Junction JTARSC(2) will be used with maximum if the mass flow at the Junction is larger than > XTARSC(2) ). The input entries KTARSC(2) and the user to change the averaging weighting factors ons in the heat exchangers change, for example when low becomes co-current. Typically the temperature d in counter-flow conditions, while it is not needed in . This can be achieved by setting XTARSC(2) to a example XTARSC(2)=10 <sup>6</sup> ). Generally speaking, ow for which the temperature distribution in the right Volume is approximately linear, provided that there is ARSC(2) and KTARSC(2). $10^{-10} < XTARSC(2) < 10^{10}$ . none.

An example of temperature averaging for a counter-flow heat exchanger is shown in Figure 2-16. For the case shown in this figure appropriate input entries are:

SC-01 left surface, inlet Junction:

•	JTALSC=11	JN-11 is the inlet Junction on the left surface.	
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• WTALSC= $W_{NL}$  nominal flow for the normal counter-flow conditions - Figure 2-16 (a).

- KTALSC=22 if there is flow in through JN-11, and simultaneously through JN-22, the flow is co-current and WTALSC needs to be replaced by XTALSC, below.
- XTALSC= $10^6$  a large value, appropriate for co-flow conditions -Figure 2-16 (c).

SC-01 left surface, outlet Junction:

- JTALSC=12 JN-12 is the outlet Junction on the left surface; when there is flow in through this Junction, the flow is co-current and WTALSC should be large.
- WTALSC=10<sup>6</sup> a large value, appropriate for co-flow conditions -Figure 2-16 (b).
   KTALSC=22 if there is flow in through JN-12, and simultaneously through JN-22, the flow is counter-current and WTALSC needs to be replaced by XTALSC, below.
- XTALSC= $W_{NL}$  nominal flow for the reversed counter-flow conditions Figure 2-16 (d).

SC-01 right surface, inlet Junction:

- JTARSC=21 JN-21 is the inlet Junction on the right surface.
- WTARSC=W<sub>NR</sub> nominal flow for the normal counter-flow conditions Figure 2-16 (a).
   KTARSC=12 if there is flow in through JN-21, and simultaneously through JN-12, the flow is co-current and WTARSC needs to be replaced by XTARSC, below.
- XTARSC= $10^6$  a large value, appropriate for co-flow conditions Figure 2-16 (b).

SC-01 right surface, outlet Junction:

٠		JTARSC=22 JN-22 is the outlet Junction on the left surface;						
		when there is flow in through this Junction, the flow is co-current and						
		WTARSC should be large.						
•	WTARSC=10 <sup>6</sup>	<sup>6</sup> a large value, appropriate for co-flow conditions - Figure 2-16 (c).						
•		KTARSC=12 if there is flow in through JN-22, and						
		simultaneously through JN-12, the flow is counter-current and						
		WTARSC needs to be replaced by XTARSC, below.						
•	XTARSC=W <sub>NLR</sub>	nominal flow for the reversed counter-flow conditions - Figure 2-16 (a).						

Suppose the nominal flow is 100.0 kg/s on both left and right side. The input deck for the SC-01 Temperature Averaging (Figure 2-16) looks like this:

* INLET JUNCT		NCTION	OUTLET JUNCTION						
*	JTALSC	WTALSC	KTALSC	XTALSC	JTALSC	WTALSC	KTALSC	XTALSC	
325001	011	100.0	022	1.0E+6	012	1.0E+6	022	100.0	* Left side
326001	021	100.0	012	1.0E+6	022	1.0E+6	012	100.0	* Right side

Note that the limiting flow for T-A is affected by the multipliers CMN1SC, CMN2SC, defined in the record 360000 (section 2.3.23). Generally one should make sure that the limiting flows,  $W_{TA}$ , approximately fulfil the relation:

$$\left(W_{TA}c_{p}\right)_{primary} \approx \left(W_{TA}c_{p}\right)_{secondary}$$

The multipliers will then assure proper temperature averaging in case when the flow on the primary side is becoming very different from the flow on the secondary side.

#### 2.3.17 Records: 327XXX, Left Side Structure-to-Structure Radiation

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

Default value:

The effective emissivity of a pair of 1-D Solid Heat Conductor surfaces and the radiation heat fluxes are obtained from:

1.0

$$\begin{split} \varepsilon_{1-2} = & \left(\frac{1}{\varepsilon_1} + \frac{A_1}{A_2} \cdot \left(\frac{1}{\varepsilon_2} - 1\right) + \frac{1}{F_{1-2}} - 1\right)^{-1} \\ q_{1-2} = & \varepsilon_{1-2} \cdot \sigma \cdot \left(T_1^4 - T_2^4\right) \\ q_{2-1} = & \varepsilon_{1-2} \cdot \sigma \cdot \left(T_2^4 - T_1^4\right) \cdot \frac{A_1}{A_2} \end{split}$$

- $q_{1-2}$  heat flux from surface 1 to 2, W/m<sup>2</sup>,
- $\sigma$  Stefan-Boltzmann constant, =5.67×10<sup>-8</sup> W/(m<sup>2</sup>-K<sup>4</sup>),
- $T_1$  temperature of surface 1, K,
- $T_2$  temperature of surface 2, K,
- $\varepsilon_{1-2}$  effective emissivity between surfaces 1 and 2.
- $A_1$  area of surface 1, m<sup>2</sup>, (the smaller surface)
- $A_2$  area of surface 2, m<sup>2</sup>, (the larger surface)
- $\varepsilon_1$  emissivity (temperature-dependent) of surface 1,

- $\varepsilon_2$  emissivity (temperature-dependent) of surface 2,
- $F_{1-2}$  view factor from surface 1 (the smaller surface) to surface 2 (the larger surface).

#### 2.3.18 Records: 328XXX, Right Side Structure-to-Structure Radiation

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

- W-1 (I): JQRRSC Reference number of the 1-D Solid Heat Conductor member of the structure-to-structure radiation pair. A left side surface of JQRRSC is identified by the use of a negative Solid Conductor number while a right side surface of JQRRSC is identified by a positive Solid Conductor number. A single SC may be a member of a single radiating pair only. The model need to be defined on one of the radiating surfaces. If it is defined on both radiating surfaces, the input must be consistent. Emissivity must be defined for both surface: IQRRSC > 1000: for the Solid Conductor XXX IORLSC > 1000: for the Solid Conductor –JORRSC, if JORRSC<0 for the Solid Conductor JQRRSC, if JQRRSC>0 IORRSC > 1000: Acceptable range: must be a valid reference number of a 1-D Solid Heat Conductor, if non-zero Default value: 0 FORRSC View factor from the smaller surface to the larger surface,  $F_{1-2}$ . Note W-2(R): that this always the view factor from the smaller surface of the pair.
- w-2 (R): FQRRSC View factor from the smaller surface to the larger surface,  $F_{1-2}$ . Note that this always the view factor from the smaller surface of the pair. Acceptable range:  $0.0 < FQRRSC \le 1.0$ . Default value: 1.0

#### **Example 1**

The example below defines a radiating pair consisting of the right surface of SC-100 and the left surface of SC-200. Default value of the view factor from the smaller surface,  $F_{1-2} = 1.0$ , is used. The view factor from the larger surface (computed internally by the code) is equal to  $F_{2-1} = A_1/A_2$ .

328100 -200 \* SC-100 right to SC-200 left

#### Example 2

The example below defines a radiating pair consisting of the right surface of SC-100 and the left surface of SC-200. The view factor from the smaller surface is equal to  $F_{1-2} = 0.5$ . The view factor from the larger surface (computed internally by the code) is equal to  $F_{2-1} = F_{1-2} \times A_1/A_2$ .

328100 -200 0.5 \* SC-100 right to SC-200 left , view fac=0.5

It is sufficient to define the pair for one of the two radiating surfaces. The definition below will give exactly the same results as the definition above:

327200 100 0.5 \* SC-200 left to SC-100 right, view fac=0.5

The radiating pair of surfaces may also be defined twice. In this case both definitions must be consistent, otherwise an input error is generated. The following definition:

328100 -200 0.5 \* SC-100 right to SC-200 left , view fac=0.5 327200 100 0.5 \* SC-200 left to SC-100 right, view fac=0.5

will give exactly the same results as the definitions shown earlier: Note that the view factor FQRRSC is always interpreted as the view factor from the smaller of the two surfaces. Therefore the value is the same, independently of which record, 328100 or 327200, is used. The view factor from the larger surface is always calculated obtained internally in the code.

#### 2.3.19 Records: 350XXX, Boundary Fluid Temperature Calculation

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record describes boundary fluid temperature calculation in case of intensive boiling. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I): IBPTSC Indicator for boundary fluid temperature calculation for pool-bubble flow. Typically the pool temperature is used as boundary fluid temperature for Solid Heat Conductors. In case of intensive boiling the program assumes that bubbles rise up in a plume of relatively warm water (see Volume 1). The water temperature in this plume is equal to the local saturation temperature, and is therefore higher than the pool average temperature, which is no higher than the saturation temperature at the pool surface pressure. The indicator IBPTSC defines how the program should determine whether the SC surface will be exposed to the warm plume or to the relatively cold pool outside the plume. Three factors may be used by the program: the void fraction factor,  $f_{\alpha}$ , the temperature factor,  $f_{T}$ , and the submergence factor,  $f_{Z}$ . Those factors are defined as follows:

a) The void fraction factor,  $f_{\alpha}$ :

$$f_{\alpha} = \begin{cases} 0.0 & \text{if} \quad \alpha \leq \alpha_1 \\ (3 - 2X)X^2 & \text{if} \quad \alpha_1 < \alpha < \alpha_2 \\ 1.0 & \text{if} \quad \alpha \geq \alpha_2 \end{cases}$$

where  $\alpha$  is the average void fraction in the pool, X is the interpolation factor, equal to:  $X = (\alpha - \alpha_1)/(\alpha_2 - \alpha_1)$ , and the boundary values of void fractions,  $\alpha_1$ ,  $\alpha_2$ , are defined below (words 2 and 3). Note that the cubic interpolation is used, which ensures continuity of the function as well as its first derivative.

b) The surface temperature factor,  $f_T$ :

$$f_{T} = \begin{cases} 0.0 & if & T_{SC} \leq T_{int} + \Delta T_{1} \\ (3 - 2X)X^{2} & if & T_{int} + \Delta T_{1} < T_{SC} < T_{int} + \Delta T_{2} \\ 1.0 & if & T_{SC} \geq T_{int} + \Delta T_{2} \end{cases}$$

where  $T_{SC}$  is the surface temperature of the Solid Heat Conductor,  $T_{int}$  is the liquid temperature at the pool-bubble interphase, X is the interpolation factor, equal to:

 $X = (T_{SC} - (T_{int} + \Delta T_1)) / ((T_{int} + \Delta T_2) - (T_{int} + \Delta T_1)),$ and the boundary values of  $\Delta T$  are defined below (words 4 and 5).

c) The surface submergence factor, fz:

$$f_{T} = \begin{cases} (3 - 2X_{1})X_{1}^{2} & \text{if} & 0 \le Z < Z_{bubb} \\ 1.0 & \text{if} & Z_{bubb} \le Z \le Z_{bubb}Z_{m1} \\ (3 - 2X_{2})X_{2}^{2} & \text{if} & Z_{bubb}Z_{m1} < Z < Z_{bubb}Z_{m2} \\ 0.0 & \text{if} & Z_{bubb}Z_{m2} \le Z \end{cases}$$

where Z is the SC submergence (equal to the distance between the pool surface and the elevation of the middle point of this part of the SC which is covered by water),  $Z_{bub}$  is the submergence of average bubble,  $X_1$  and  $X_2$  are the interpolation factors, equal to:

$$X_1 = Z/Z_{bub},$$
  

$$X_2 = (Z-Z_{bub} \cdot Z_{m2})/(Z_{bub} \cdot Z_{m1} - Z_{bub} \cdot Z_2).$$

Values of the multipliers,  $Z_{m1}$  and  $Z_{m2}$ , are defined below (words 6, 7).

The parameter IBPTSC defines which of the factors described above should be used. The interpretation is as follows:

IBPTSC = -1: No factors are used. When the surface is exposed to a boiling pool, the boundary fluid temperature is always equal to the pool temperature,  $T_{pool}$  (approximately equal to the saturation temperature for the pressure at the pool surface).

$$T_{fluid} = T_{pool}$$

IBPTSC = 1 : Only the void fraction factor is taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot f_{\alpha}$$

where  $T_{pool}$  is the pool average temperature, and  $T_{int}$  is the liquid temperature at the pool-bubble interphase (thus the warm plume temperature, approximately equal to the saturation temperature for the pressure at the elevation of average bubble).

IBPTSC = 2: The void fraction factor and the temperature factor are taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_{T})$$

IBPTSC = 3 : The void fraction factor and the submergence factor are taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_{z})$$

IBPTSC = 4 : All factors are taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_T f_Z)$$

Acceptable range:  $-1 \leq \text{IBPTSC} \leq +4$ . Default value: +4. If IWATCV>0 (see section 2.1.31) then the default value is -1.

- W-2 (R): ALP1SC Upper limit of void fraction to use only the pool temperature as boundary fluid temperature for the SC surface,  $\alpha_1$ , (-). Used if IBPTSC (word 1 above) is positive. If the average void fraction in the pool is below  $\alpha_1$  then the Solid Heat Conductor surface is not exposed to the warm plume. *Acceptable range:*  $10^{-5} \le ALP1SC \le 0.1$ . *Default value:*  $10^{-3}$ .
- W-3 (R):ALP2SCLower limit of void fraction to use the warm plume temperature as<br/>boundary fluid temperature for the SC surface,  $\alpha_2$ , (-). Used if IBPTSC<br/>(word 1 above) is positive. If the average void fraction in the pool is<br/>above  $\alpha_2$  then the Solid Heat Conductor surface can be exposed to the<br/>warm plume (depending on other conditions if they are applied).<br/>Acceptable range:  $2.0 \cdot ALP1SC \leq ALP2SC \leq 0.5$ .<br/>Default value: 0.05.
- W-4 (R): TSC1SC Upper limit of SC surface superheat to use only the pool temperature as boundary fluid temperature for the SC surface,  $\Delta T_1$ , (K). Used if IBPTSC (word 1 above) is equal to 2 or 4. If the SC surface temperature is lower than the liquid temperature at the pool-bubble interphase (warm plume temperature) plus TSC1SC then the Solid Heat Conductor surface is not exposed to the warm plume. *Acceptable range:*  $0.1 \leq TSC1SC \leq 10.0$ .

Default value: 1.0.
Acceptable range:  $2.0 \cdot \text{TSC1SC} \le \text{TSC2SC} \le 30.0$ . Default value: 3.0.

 $\begin{array}{lll} W\text{-}6\,(R): & ZSC1SC & Lower multiplier on bubble submergence to use the warm plume temperature as boundary fluid temperature for the SC surface, Z_m1, (-). \\ & Used if IBPTSC (word 1 above) is equal to 3 or 4. If the SC surface submergence is smaller than the average bubble submergence multiplied by ZSC1SC then the Solid Heat Conductor surface can be exposed to the warm plume (depending on other conditions if they are applied). \\ & Acceptable range: \ 1.0 \leq ZSC1SC \leq 10.0 \ . \\ & Default value: \ 2.0 \ . \end{array}$ 

## 2.3.20 Records: 351XXX, Boundary Fluid Velocity Multiplier

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record is optional. The velocity multiplier may be used for to account for own movement of structures, such as for example rotor blades. In such case the relative velocity surface-to-gas velocity is different than the gas velocity in a Control Volume. The user may take into account that difference using a Control Function that depends on the rotational speed, etc.

W-1 (I): VLMLSC Velocity multiplier,  $C_{\nu}$ , for the boundary surface velocity calculation. If a positive value is entered, the velocity multiplier is constant, and equal to this value. If a negative value is entered, the velocity multiplier is obtained from the Control Function equal to |VLMLSC|. An absolute value of the number obtained from the Control Function is used. Furthermore the value is limited to a maximum of  $10^{10}$ .

The fluid velocity at the SC boundary surface is obtained from:

If IHDLSC=0 (Word 18, record 321XXX):

$$v_{SC} = C_v \cdot \sqrt{v_{CV,hor}^2 + v_{CV,ver}^2}$$

If IHDLSC=1, IVERSC=0 (vertical SC, Word 5, record 300XXX):

$$v_{SC} = C_v \cdot v_{CV,ver}$$

If IHDLSC=1, IVERSC≠0 (horizontal SC, Word 5, record 300XXX):

$$v_{SC} = C_v \cdot v_{CV,hor}$$

Acceptable range: $0.0 \le VLMLSC \le 10^{10}$ <br/>or reference to a Control Function.Default value:1.0

#### 2.3.21 Records: 352XXX, Limit for Simultaneous Transfer to Pool and Atmosphere

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

- W-1 (R): PMXLSC Critical (maximum) fraction of left surface area covered by pool to allow simultaneous heat transfer to pool and atmosphere. If no value is given, simultaneous heat transfer to pool and atmosphere is always possible. This may lead to too large condensation in some cases. To eliminate it, the user may restrict the simultaneous heat transfer to a situation when the pool-covered fraction is smaller than PMXLSC. This input parameter is similar to CPFPL in the MELCOR code. An interpolation zone is defined. The full transfer to gas occurs when the pool fraction is below 0.9 of the critical value, a linear interpolation is performed in the range between 0.9 and 1.0 times the critical value. Acceptable range:  $0.0 \le \text{PMXLSC} \le 1.0$ Default value: 0.0 Maximum fraction of right surface area covered by pool to allow W-1 (R): PMXRSC
- W-1 (R): PMXRSC Maximum fraction of right surface area covered by pool to allow simultaneous heat transfer to pool and atmosphere. The same as PMXLSC but applied for the right surface). Acceptable range:  $0.0 \le PMXRSC \le 1.0$ Default value: 0.0.

As example of such situation is discussed in Volume 1. As a reference case, a fine nodalization is used (Figure 2-17, left). Coarse nodalization and consequent too slow heat up due to artificial heat transfer from atmosphere to pool through the solid structure is shown in Figure 2-17, middle. This is prevented by using the parameter PMXRSC. A value of PMXRSC=0.01 was used (Figure 2-17, right). The heat transfer from atmosphere to pool is practically eliminated. However, a direct heat transfer still exists at the pool-atmosphere interphase. Therefore it is advisable to eliminate the pool-atmosphere heat transfer at the same time (input record 164XXX). This was done in the considered example.





Figure 2-17 Simultaneous heat transfer to pool and atmosphere

## 2.3.22 Records: 353XXX, Plume Model for Heat and Mass Transfer

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records activate plume models for the heat and mass transferred at the surface of the Solid Heat Conductor. The plume model is used in Control Volumes, in which stratification is calculated. Thus, it will be used only if the stratification model is active for the boundary (left or right) volume for this Solid Heat Conductor. A description of the plume model is given in Volume 1. To activate the model for a single component, a set of two integer numbers, described below, must be entered. To activate the model for both atmosphere and pool, two pairs of data should be entered in this record.

W-1 (I) :	J	Identifier of component, for which the plume model is desired. J=1: atmosphere; J=3: pool. <i>Acceptable range:</i> J=1, or J=3. <i>Default value:</i> none.
W-2 (I) :	IPLMSC	Plume model activator. If IPLMSC = 0 then the plume model is not active. If IPLMSC $\neq 0$ then the plume model is active for the component J and Solid Heat Conductor XXX. Note that the plume model is used only when stratification models are active in Control Volumes associated with left or right boundary surface of the Solid Heat Conductor. Acceptable range: any integer. Default value: 0.

etc., until all plumes are defined. . . .

## 2.3.23 Records: 360000, Global Data: Film Boiling, Slip Ratio, TA, Oxidation

Parameters defined in this record are applied for all 1-D Solid Heat Conductors.

W-1 (R) :	AMFBSC	First coefficient in the Simon Minimum Film Boiling correlation, $A_{MFB}$ , (-). SPECTRA selects correlation that gives maximum value of the $T_{MFB}$ , therefore the Simon correlation may be deactivated by setting AMFBSC and BMFBSC to small values. Acceptable range: $0.0 < AMFBSC \le 1.0$ Default value: 0.13.
W-2 (R) :	BMFBSC	Second coefficient in the Simon Minimum Film Boiling correlation, $B_{MFB}$ , (-). SPECTRA selects correlation that gives maximum value of the $T_{MFB}$ , therefore the Simon correlation may be deactivated by setting AMFBSC and BMFBSC to small values. ACCeptable range: $0.0 < BMFBSC \le 2.0$ Default value: $0.86$ .
W-3 (R) :	CMFBSC	Coefficient in the Berenson Minimum Film Boiling correlation, $C_{MFB}$ , (-). SPECTRA selects correlation that gives maximum value of the $T_{MFB}$ , therefore the Berenson correlation may be deactivated by setting CMFBSC to a small value. Acceptable range: $0.0 < \text{CMFBSC} \le 1.0$ Default value: $0.127$
W-4 (R) :	TFMNSC	Minimum value of the Minimum Film Boiling (MFB) temperature minus the Critical Heat Flux (CHF) temperature: $(T_{MFB} - T_{CHF})$ , (K). The MFB temperature, calculated from the Simon correlation is limited by this word so that it will never be lower than $T_{CHF}$ + TFMNSC. <i>Acceptable range:</i> $5.0 \le$ TFMNSC $\le$ 1000.0 <i>Default value:</i> 5.0.
W-5 (R) :	TFMXSC	Maximum value of the Minimum Film Boiling (MFB) temperature minus the Critical Heat Flux (CHF) temperature: $(T_{MFB} - T_{CHF})$ , (K). The minimum film boiling temperature, calculated from the Simon correlation is limited by this word so that it will never be higher than $T_{CHF}$ + TFMXSC. <i>Acceptable range:</i> TFMNSC $\leq$ TFMXSC $\leq$ 1000.0 <i>Default value:</i> 1000.0.
W-6 (R) :	XTRBSC	Coefficient in the Kalinin Transition Boiling correlation, $X_{TB}$ , (-). Acceptable range: $0.5 < \text{XTRBSC} \le 20.0$ Default value: 7.0.
W-7 (R) :	ASFBSC	Correction for subcooling in the film boiling correlation, $A_{SFB}$ , (-). In case of a subcooled film boiling, the total heat flux is calculated from:

 $q = q_{FB} + A_{SFB} \cdot h_{conv} \cdot \left(T_{sat} - T_{fluid}\right)$ 

where  $q_{FB}$  is the saturated film boiling heat flux while  $h_{conv}$  is a convective heat transfer coefficient, equal to: Max( $h_{FC}$ ,  $h_{NC}$ ) with  $h_{FC}$ ,  $h_{NC}$  being the forved and the natural convective heat transfer coefficients *Acceptable range:*  $0.0 \le \text{ASFBSC} \le 2.0$ *Default value:* 0.0

W-8 (R): SMAXSC Maximum value of the slip ratio, ( $v_{bubb} / v_{pool}$ ), (-). Used for CHF calculations. The slip ratio which is used in the CHF correlation is equal to the minimum of  $v_{bubb} / v_{pool}$  and SMAXSC. Acceptable range:  $1.0 \le$  SMAXSC  $\le 1000.0$ Default value: 100.0.

W-9 (R): CMN1SC Multiplier for the first (counter-current) Temperature Averaging (T-A) mode. The nominal flows for the T-A on both primary and secondary side of a heat exchanger are entered in the records 325XXX 326XXX. If the flows exceed the nominal flows, full T-A is performed. If flows are decreased then also the T-A is decreased - see section 2.3.15 and 2.3.16. This treatment is approximately correct if flow changes only on one side of the heat exchanger. If the flow changes simultaneously on both sides of the heat exchanger, then T-A should be used for flows much smaller than nominal. This multiplier defines how much the limiting flow (typically taken as a nominal flow) can be decreased when the flow on the other side of a heat exchanger decreases.

The default value of 0.01 means that in nominal counter-flow conditions full T-A will be performed if the flows decrease down to 1% of the nominal flow, provided that they will decrease simultaneously on both sides of the heat exchanger.

Generally the limiting flow on a given side of a heat exchanger is:

$$W_{TA} = Min\left[\frac{W_{TA}}{C_{MN1}}, Max\left(W_{TA}C_{MN1}, W_{TA}\frac{W_{otherside}}{W_{TA, otherside}}\right)\right]$$

where  $W_{TA}$  is the limiting flow for full T-A,  $C_{MNI}$  is the factor CMN1SC,  $W_{TA, other side}$  is the limiting flow for full T-A on the other side, and  $W_{other side}$  is the current flow on the other side. Note that with this definition, the limiting flow for T-A can be either decreased or increased, and the actual value will always be within the range:

$$W_{TA}C_{MN1} \le W_{TA} \le \frac{W_{TA}}{C_{MN1}}$$

The limiting flow will be small when the other side flow is small, and large when the other side flow is large. This is the most appropriate treatment of a heat exchanger, provided that the limiting flows, defined in records 325XXX, 326XXX for both primary and secondary side, fulfil approximately the relation:

$$(W_{TA}c_p)_{primary} \approx (W_{TA}c_p)_{secondary}$$

Acceptable range:  $0.001 \le \text{CMN1SC} \le 1.0$ 

*Default value:* 0.01.

- W-10 (R): CMN2SC Multiplier for the second (co-current) Temperature Averaging (T-A) mode. Works the same as CMN1SC, but in case when the flow is cocurrent. Default value means that CMN2SC is not used in co-flow conditions. It is recommended to disable T-A in co-flow by setting the limiting flow to a large value - see section 2.3.15 and 2.3.16. In such case the value of CMN2SC is not very important. For consistency it should be equal to 1.0 when T-A is disabled. *Acceptable range:*  $0.001 \le \text{CMN2SC} \le 1.0$ *Default value:* 1.0.
- W-11 (R): VGLMSC Gas velocity limit,  $v_{g,lm}$  (m/s), to switch off the Temperature Averaging (T-A). Numerical problems may be encountered when T-A is used in case of low velocities and changes of flow direction. To avoid this problems the T-A is turned off when the velocity is smaller than the limit defined by this word. An interpolation zone is defined for gas velocities between VGLMSC and 2×VGLMSC.

$$X_{TA,eff} = \begin{cases} X_{TA} & \text{if } v_g > 2v_{g,lm} \\ X_{TA} \cdot (v_g - v_{g,lm}) / v_{g,lm} & \text{if } v_{g,lm} < v_g < 2v_{g,lm} \\ 0.0 & \text{if } v_g < v_{g,lm} \end{cases}$$

where  $X_{TA}$  is the Temperature Averaging factor for full T-A,  $X_{TA,eff}$  is the effective T-A factor,  $v_g$  is the gas velocity and  $v_{g,lm}$  is the limiting gas velocity, VGLMSC.

Acceptable range: $0.001 \le \text{VGLMSC} \le 100.0$ Default value:1.0

W-12 (R): VLLMSC Liquid velocity limit,  $v_{l,lm}$  (m/s), to switch off the Temperature Averaging (T-A). Numerical problems may be encountered when T-A is used in case of low velocities and changes of flow direction. To avoid this problems the T-A is turned off when the velocity is smaller than the limit defined by this word. An interpolation zone is defined for liquid velocities between VLLMSC and 2×VLLMSC.

$$X_{TA,eff} = \begin{cases} X_{TA} & \text{if } v_l > 2v_{l,lm} \\ X_{TA} \cdot (v_l - v_{l,lm}) / v_{l,lm} & \text{if } v_{l,lm} < v_l < 2v_{l,lm} \\ 0.0 & \text{if } v_l < v_{l,lm} \end{cases}$$

where  $X_{TA}$  is the Temperature Averaging factor for full T-A,  $X_{TA,eff}$  is the effective T-A factor,  $v_l$  is the liquid velocity and  $v_{l,bn}$  is the limiting liquid velocity, VLLMSC. Acceptable range:  $0.001 \le \text{VLLMSC} \le 100.0$ Default value: 0.1

W-13 (I): IOXNSC Option for oxidation on surfaces not connected to Control Volumes.

		<ul> <li>=1: oxidation is calculated on SC surfaces not connected to a CV. It will be assumed that all oxidizing gases are always available at the surface.</li> <li>=2: oxidation is disabled on SC surfaces not connected to a CV. <i>Acceptable range:</i> 1, 2 <i>Default value:</i> none</li> </ul>
W-14 (I) :	ISEQSC	Indicator for multiple oxidation reactions. =1: all oxidation reactions proceed simultaneously. =2: dominant reactions: oxidation reactions proceed in sequence, defined in records 381XXX, 382XXX. If there is enough oxidant (gas fraction > XLIMSC) for the first reaction, only this reaction occurs. If not, second reaction starts, then third, etc. This option is available because, according to [52], reaction with oxygen dominates over reactions with steam and nitrogen. <i>Acceptable range:</i> 1, 2 <i>Default value:</i> 1
W-15 (R) :	XLIMSC	Limit for dominant reactions. The default oxidation starvation limits are: $C1OX = 1.0 \times 10^{-4}$ : full strength oxidation $C0OX = C1OX / 10.0 = 1.0 \times 10^{-5}$ : no oxidation The default value of XLIMSC was selected approximately in the middle of the interpolation zone, when the dominant reaction strength is reduced roughly by half. <i>Acceptable range:</i> $1.0 \times 10^{-7} \le XLIMSC \le 1.0 \times 10^{-2}$ <i>Default value:</i> XLIMSC = C1OX / 2.0
W-16 (I) :	IMPGSC	<ul> <li>Implicit/explicit use of gas concentration for oxidation calculations.</li> <li>= 1: implicit (end of time step value is used).</li> <li>= 2: explicit (beginning of time step value is used).</li> <li>Acceptable range: 1 or 2</li> <li>Default value: 1</li> </ul>
W17 - (I)	IAVESC	Method used to calculate average SC temperature. In SPECTRA output and plot files, the average temperatures are given next to the cell temperatures. This entry defines how the average temperature is obtained. = 1: volume average: $\overline{T} = \sum_{i} V_i \cdot T_i / \sum_{i} V_i$ = 2: mass-average: $\overline{T} = \sum_{i} M_i \cdot T_i / \sum_{i} M_i$ Here $M_i$ , $V_i$ , $T_i$ are the mass, volume and temperature of the cell <i>i</i> . <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 2
W-18 (I) :	ITAISC	A value of ITAISC > 0 activates the averaging scheme (T-A) also for isotopes in circulating fuel. The averaging weighting factor is divided by ITAISC. ITAISC = 1 means full averaging (both current CV value and the value at the inlet to CV are taken with weights of 0.5. A value > 1 means that the current CV value gets higher weight. For example, ITAISC = 3 means that the current CV is taken with the weight of 0.75 and the inlet value with the weight of 0.25 (see Volume 1).

Acceptable range:  $ITAISC \ge 0$ Default value: 0

W-19 (I): IQPLSC Power versus power density as plot parameters - Table 2-25.
= 1: Power (W) is used as plot parameters: SC-XXX-Qcel-YYYY
= 2: Power density (W/m<sup>3</sup>) is used: SC-XXX-qcel-YYYY
Acceptable range: 1 or 2
Default value: 1

## 2.3.24 Records: 365000, Hydraulic Diameter - SC Versus CV

W-1 (I): IDHDSC Option to check consistency between the CV hydraulic diameter (DHYDCV) and the SC hydraulic diameter (DFCLSC/DFCRSC). = 1: consistency is not required. If DFCLSC  $\neq$  DHYDCV or DFCRSC  $\neq$  DHYDCV, then a warning message is issued. = 2: consistency is required. If DFCLSC  $\neq$  DHYDCV or DFCRSC  $\neq$  DHYDCV, then an error message is issued. Acceptable range: 1, 2 Default value: 1

## 2.3.25 Records: 381XXX, Left Side Oxidation Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records activate the oxidation model on the left surface of a 1-D Solid Heat Conductor. Each surface can have several different oxidation reactions associated with it, for example: a Zircaloy cladding may be oxidized by steam, Zr+H<sub>2</sub>O, and oxygen, Zr+O<sub>2</sub>. Maximum number of oxidation reactions is 5.

W-1 (R) :	XMTLSC	Initial thickness of the 1-D Solid Heat	material available for oxidation on the left surface of Conductor, (m).
		Acceptable range:	$XMTLSC \le$ thickness of the SC for 1-side reaction $XMTLSC \le$ half-thickness for both sides reaction
		Default value:	cell width of the leftmost (first) mesh cell
W-2 (R) :	XOXLSC	Initial thickness of Heat Conductor, (n	oxidized material on the left surface of the 1-D Solid n).
		Acceptable range: Default value:	$0.0 \le \text{XOXLSC} \le \text{total thickness of SC.}$ 0.0.
W-3 (I) :	IOXLSC(1)	Oxidation reaction	1.
		= $-1$ : Zr oxidation	by steam, Cathcart model
		=-2: Zr oxidation	by steam, Urbanic-Heidrich model
		= -3: Steel oxidation	on by steam, white model
		= -4. ZI OXIGATION = 5: Graphite oxi	dation by O <sub>2</sub> . Boes model
		> 0: Oxidation r	nodel with user-defined coefficient set number
		IOXLSC. The us	er-defined coefficients are specified in records
		8500XX, 8510XX,	, where XX is the set number (see section 2.14.1).
		Acceptable range:	$-5 \leq \text{IOXLSC} \leq 10$ , IOXLSC $\neq 0$ . If a positive
		1 0	number is specified, then a user-defined oxidation
			model must be defined in records 8500XX,
			8510XX,, with XX=IOXLSC.
		Default value:	none.
W-4 (I) :	IOXLSC(2)	Oxidation reaction	2. See above for description of available reactions.
		Acceptable range:	$-5 \le 10 \times 10^{\circ}$ IO $\times 10^{\circ}$ , IO $\times 10^{\circ}$ II a positive number is specified, then a user-defined oxidation
			model must be defined in records 8500XX, 8510XX, with XX=IOXLSC. If several reactions
			are specified, then they must be different, i.e.:
		<b>5</b> 4 4 5	$IOXLSC(i) \neq IOXLSC(j).$
		Default value:	none.

W-5 (I) : IOXLSC(3) Oxidation reaction 3.

... etc. until all reactions are defined. The maximum number of oxidation reactions per surface is 5.

## 2.3.26 Records: 382XXX, Right Side Oxidation Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records activate the oxidation model on the right surface of a 1-D Solid Heat Conductor. Each surface can have several different oxidation reactions associated with it, for example: a Zircaloy cladding may be oxidized by steam, Zr+H<sub>2</sub>O, and oxygen, Zr+O<sub>2</sub>. Maximum number of oxidation reactions is 5.

W-1 (R) :	XMTRSC	Initial thickness of material available for oxidation on the right surface of the 1-D Solid Heat Conductor (m)		
		Acceptable range:	$XMTLSC \leq$ thickness of the SC for 1-side reaction	
			$XMTLSC \leq$ half-thickness for both sides reaction	
		Default value:	cell width of the rightmost (last) mesh cell	
W-2 (R) :	XOXRSC	Initial thickness of Heat Conductor, (r	oxidized material on the right surface of the 1-D Solid n).	
		Acceptable range:	$0.0 \leq \text{XOXRSC} \leq \text{total thickness of SC}$ .	
		Default value:	0.0.	
W-3 (I) :	IOXRSC(1	) Oxidation reaction	1.	
		= $-1$ : Zr oxidation	by steam, Cathcart model	
		= $-2$ : Zr oxidation	by steam, Urbanic-Heidrich model	
		= $-3$ : Steel oxidat	ion by steam, White model	
		= -4: Zr oxidation	h by $O_2$ , Benjamin et al. model	
		=-5: Graphite ox	idation by O <sub>2</sub> , Roes model	
		> 0: Oxidation	model with user-defined coefficient set, number	
		IOXRSC. The us 8500XX, 8510XX,	ser-defined coefficients are specified in records ,, where XX is the set number (see section 2.14.1).	
		Acceptable range:	$-5 \le IOXRSC \le 10$ , $IOXRSC \ne 0$ . If a positive number is specified, then a user-defined oxidation model must be defined in records 8500XX,	
			8510XX,, with XX=IOXRSC.	
		Default value:	none.	
W-4 (I) :	IOXRSC(2	) Oxidation reaction	2. See above for description of available reactions.	
		Acceptable range:	$-5 \leq IOXRSC \leq 10$ , $IOXRSC \neq 0$ . If a positive number is specified, then a user-defined oxidation model must be defined in records 8500XX, 8510XX,, with XX=IOXRSC. If several reactions are specified, then they must be different,	
			i.e.: IOXRSC( <i>i</i> )≠IOXRSC( <i>j</i> ).	
		Default value:	none.	
W-5 (I) :	IOXRSC(3	) Oxidation reaction	3.	

... etc. until all reactions are defined. The maximum number of oxidation reactions per surface is 5.

The example input below defines oxidation reactions for two surfaces. First, Zr oxidation by  $O_2$  and  $H_2O$  for the 1-D Heat Conductor SC-100, left surface. The initial cladding thickness is 0.001 m. The initial oxide thickness is 0.0 m. The built-in reaction models are used (model indicator = -4 for oxygen reaction, and -1 for steam reaction, see section 2.14.1).

Second, steel oxidation by  $O_2$  and  $H_2O$  for the 1-D Heat Conductor SC-100, right surface. The initial thickness of material which can be oxidized is 0.001 m. The initial oxide thickness is 0.0 m. For steel-steam reaction the built-in model is used (model indicator = -3, see section 2.14.1). For steel-oxygen reaction a user-defined model number 4 is used. The records 850004, 8510004, ..., must be specified in the input deck. Example input for steel-oxygen reaction is shown in section 2.14.1.

 \*
 Un-oxidized Oxide
 Reactions

 381100
 0.001
 0.0
 -4
 -1
 \*
 Zr oxidation by O2 and H2O

 382100
 0.001
 0.0
 4
 -3
 \*
 Steel oxidation by O2 and H2O

## 2.3.27 Record: 330XXX, Failure Parameters

\*

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record activates the failure model for this 1-D Solid Heat Conductor. The failure model considers the following three failure mechanisms:

• •	<ul><li>Ultimate strength failur</li><li>Creep rupture</li><li>Meltdown</li></ul>		ilure (failure mod (failure mod (failure mod	e (failure mode = 1) (failure mode = 2) (failure mode = 3)		
W-1 (I)	:	IFFASC	Failure model activ =0: failure model n >0: failure model r failure model a records 39Y000 Acceptable range: Default value:	vator. Not requested for this SC equested for this SC. The properties required by the re defined with the material number IFFASC in the D IFFASC $\ge 0$ 0		
W-2 (I)	:	ITFASC	Indicator defining h failure calculations =1: use maximum t =2: use volume-we Acceptable range: Default value:	how the representative temperature is obtained for the . temperature of all SC nodes ighted average temperature 1 or 2 1		
W-3 (I)	:	ISFASC	<ul> <li>Indicator defining which pressures are used for to determine the stress needed for the failure calculations</li> <li>&lt;0: use Control Function number  ISFASC  </li> <li>=0: pressure is not used (value is set to 1.0). Stress is constant, and give directly by XSFASC (next word).</li> <li>=1: use CV pressure from the left boundary CV</li> <li>=2: use CV pressure from the right boundary CV</li> <li>=3: use absolute value of the difference between the left and the rig volume pressures</li> <li><i>Acceptable range:</i> 1 ≤ ISFASC ≤ 3 or reference to a Control Function Default value:</li> <li>1 if a CV is present only on the left side of the SC 2 if a CV is present only on the right side of the SC</li> </ul>			

3 if CV-s present on both sides of the SC 0 if there is no CV on neither left nor right side

W-4 (R): XSFASC Ratio of stress and pressure (defined by the word above),  $(\sigma/p)$ . For example in case of a tube with the inner diameter *D* and the thickness *t*, the relation between the overpressure inside the tube, *p*, and the stress,  $\sigma$ , (see Figure 2-18):



Figure 2-18 Relation between stress and pressure for a tube.

$$p \cdot D = \sigma \cdot 2t$$
  
Therefore:  
$$\sigma = p \cdot (D/2t)$$
  
This for this case the ratio is equal to XSFASC = (LACC) Acceptable range: XSFASC > 0.0  
Default value: rectangular geometry: none

cylindrical geometry:

spherical geometry:

#### 2.3.28 Records: 33Y000, Material Properties Needed for Failure Calculations

Y is the material number,  $1 \le Y \le 9$ . The failure model considers the following three failure mechanisms:

- Ultimate strength failure (failure mode = 1)
- Creep rupture (failure mode = 2)
- Meltdown (failure mode = 3)

Creep rupture is calculated using the method proposed by Larson and Miller [40]. The time to rupture is obtained from the following relation (see Volume 1):

$$\log_{10}(t_r) = \frac{LMP}{T} - C$$

= (D/2t).

(D/2t)

(D/4t)

The Larson-Miller parameter, *LMP*, is approximated in SPECTRA by the following correlation:

$$LMP = A - B \cdot \log_{10}(\sigma)$$

The properties for some materials are shown in Table 2-16.

Table 2-16 Failure model data for some frequently used materials

	Material				
Constants	Inconel-600	Steel 304SS	Steel SA106B	Steel SA533B1	
Α	54,086	58,763	46,129	74,768	
В	4,968.5	5,086.4	4,237.9	6,970.9	
С	9.44	12.44	9.44	16.44	
$T_M$	1644.0	1671.0	1789.0	1789.0	
$\sigma_{U,lowT}$	$7.3 \times 10^{8}$	$6.4 \times 10^{8}$	$5.5 \times 10^{8}$	$5.5 \times 10^{8}$	
$t_{U,highT}$	634.0	1120.0	515.0	30.0	

W-1 (R) :	AFASC	If a positive number Miller parameter for data from Table 2- used. The material -1: Inconel-600 -2: Stainless steel 3 -3: Carbon steel SA -4: Carbon steel SA Acceptable range: Default value:	er is entered this is the coefficient A in the Larson- or creep rupture. If a negative number is entered, then 16 is used. In such case words 2 through 7 are not identifiers are: 804SS A106B A533B1 $10^3 \le AFASC \le 10^6$ or $AFASC = -1, -2, -3, -4$ none
W-2(R) :	BFASC	Coefficient <i>B</i> in the <i>Acceptable range: Default value:</i>	e Larson-Miller parameter for creep rupture. $10^2 \text{ BFASC} \le 10^5$ none
W-3 (R) :	CFASC	Coefficient <i>C</i> in the <i>Acceptable range: Default value:</i>	e Larson-Miller parameter for creep rupture. $1 \le CFASC \le 10^3$ none
W-4 (R) :	TMFASC	Melting temperatur Acceptable range: Default value:	re, $T_M$ , (K). $500 \le \text{TMFASC} \le 10,000$ none
W-6 (R) :	USFASC	Low temperature u Acceptable range: Default value:	Itimate strength, $\sigma_{U,lowT}$ , (Pa). $10^6 \leq \text{USFASC} \leq 10^{10}$ none
W-7 (R) :	TUFASC	High temperature u Acceptable range: Default value:	ltimate strength parameter, $t_{U,highT}$ , (s). $1 \leq \text{TUFASC} \leq 10^4$ none

## 2.3.29 Record: 340000, Definition of Fuel Regions for Gap Calculations

This record is needed if the user wishes to apply the gap conductance model. The record defines core fuel regions, which are to be viewed as structures - 1-D or 2-D Solid Heat Conductors - that represent fuel rods in a nuclear reactor. The gap properties and the location of the gap within the 1-D or the 2-D Solid Heat Conductor, are specified in this record.

If the RT (Radioactive Particle Transport) Package is used, and the RT fuel regions are used (record 883000), the fuel regions in the RT Package must be consistent with the fuel regions for the SC Package, defined in this record. The maximum number of fuel regions is NFRMSC = 200.

W-1 (I) :	L1FRSC	Core fuel region ine =1: this fuel region =2: this fuel region Acceptable range: Default value:	dicator 1. is represented by a 1-D Solid Heat Conductor, is represented by a 2-D Solid Heat Conductor. 1 or 2 . if the reactor kinetics model is used, the default values are equal to the regions indicators ITF1RK, specified for the fuel temperature weighting factor in record 791XXX. In this case the region indicator ITF1RK must refer to a 1-D or 2-D Heat Conductor (=1 or 2).
W-2 (I) :	L2FRSC	Core fuel region in Reference number Reference number Acceptable range: Default value:	dicator 2. Equal to: of a 1-D Solid Heat Conductor, if L1FRSC = 1, of a 2-D Solid Heat Conductor, if L1FRSC = 2. Must be a valid reference number of a 1-D or a 2-D Solid Heat Conductor. The geometry of the Solid Heat Conductor must be cylindrical. If the reactor kinetics model is used, the default values are equal to the regions indicators ITF2RK, specified for the fuel temperature weighting factor in record 791XXX.
W-3 (I) :	NGFRSC	Cell indicator for th present in the cell N (if L1FRSC=1), or reference number I <i>Acceptable range:</i> <i>Default value:</i>	he gap model (see record 3410XX). The gap will be IGFRSC of the SC with a reference number L2FRSC in the radial ring number NGFRSC of the TC with a .2FRSC (if L1FRSC=2). Must not be a boundary cell of a 1-D or a 2-D Solid Heat Conductor. This means: =1 < NGFRSC < NCELSC, in case of SC =1 < NGFRSC < NCELSC, in case of SC =1 < NGFRSC < NCLXTC, in case of TC =NCELSC-1, in case of SC (L2FRSC=1), =NCLXTC-1, in case of TC (L2FRSC=2).
W-4 (I) :	MGFRSC	Gap model indicate will be applied in the Acceptable range: Default value:	or (see record 3410XX). The gap model MGFRSC ne gap present in the cell NGFRSC. $1 \le MGFRSC \le NGPMSC = 10$ none

The set of four words defined above is repeated until all fuel regions are described. The total number of entries in this record must be a multiple of 4. Multiple records with the same record identified (340000) may be entered. Data is read in the order in which these records appear in the input. If the Reactor Kinetics Package is used, the total number of fuel regions must be the same as the number of the weighting factors in the Reactor Kinetics Package.

#### 2.3.30 Record: 340001, Initial Gap Size and Dynamic Expansion Model

W-1 (R) :	DGPISC	Gap size, (m), for inputs are zero, the non-zero values are expansion model w <i>Acceptable range:</i> <i>Default value:</i>	the core fuel region number 1. If the following six e gap size will be constant and equal to DGPISC. If e entered for the following six inputs, the dynamic till be used. In such case DGPISC is not used. $0.0 \le \text{DGPISC} \le 10^{-2} \text{ m}$ thickness of the gap node (node number NGFRSC)
W-2 (R) :	RDFSSC	Radial displacement the core fuel region <i>Acceptable range:</i> <i>Default value:</i>	nt due to fission gas-induced fuel swelling, (m), for number 1. $0.0 \le \text{RDFSSC} \le 1.0 \times 10^{-2} \text{ m}$ 0.0
W-3 (R) :	RDCCSC	Radial displacemer region number 1. Acceptable range: Default value:	th due to cladding creepdown, (m), for the core fuel $-1.0 \times 10^{-2} \le \text{RDCCSC} \le 0.0 \text{ m}$ 0.0
W-4 (R) :	FCCSSC	Fuel-cladding center Acceptable range: Default value:	erline shift ratio, for the core fuel region number 1. $0.0 \le \text{FCCSSC} \le 1.0$ 0.0
W-5 (R) :	IFTESC	Tabular Function temperature $T$ , for to fuel due to therm	defining the strain function, $\varepsilon_{TF}(T)$ (-), versus the fuel thermal expansion. The radial displacement hal expansion is calculated from:

$$x_{FT} = \sum_{i=1}^{N_G - 1} d_i \cdot \varepsilon_{FT}(T_i)$$

Here *i* is the node number,  $N_G$  is gap node number (NGFRSC),  $d_i$  is the thickness of the node *i*,  $T_i$  is the temperature of the node *i* (cell-center),  $\varepsilon_{FT}$  is the strain function calculated from Tabular Function IFTESC. For UO<sub>2</sub> and PuO<sub>2</sub> fuels, the strain function is given by:

$$UO_{2} : \varepsilon_{FT}(T) = 1.0 \times 10^{-5} T - 3.0 \times 10^{-3} + 4.0 \times 10^{-2} \exp\left(\frac{-6.9 \times 10^{-20}}{k_{B}T}\right)$$
$$PuO_{2} : \varepsilon_{FT}(T) = 9.0 \times 10^{-6} T - 2.7 \times 10^{-3} + 7.0 \times 10^{-2} \exp\left(\frac{-7.0 \times 10^{-20}}{k_{B}T}\right)$$

Here T is the temperature (K),  $k_B = 1.38 \times 10^{-23}$  J/K is the Boltzmann constant. Values tabulated for relevant temperature range are shown in Figure 2-19.

Acceptable range: a reference to a valid Tabular Function if non-zero, all tabulated values must be within the range  $0.0 \leq$  $\varepsilon_{FT}(T) \leq 0.1$ Default value: 0

W-6(R): **ICTESC** Tabular Function defining the strain function,  $\varepsilon_{CT}(T)$  (-), versus temperature T, for the cladding thermal expansion. The radial displacement of cladding due to thermal expansion is calculated from:

$$x_{CT} = r_{cm} \cdot \varepsilon_{CT}(T_c)$$

Here  $r_{cm}$  is the cladding mid-point radius,  $T_c$  is the average cladding temperature (K),  $\varepsilon_{CT}$  is the strain function calculated from Tabular Function ICTESC. For Zircaloy cladding, the strain function is given by:

$$\varepsilon_{CT}(T) = -2.373 \times 10^{-4} + 6.721 \times 10^{-6}(T - 273) \qquad for \quad T < 1073$$
  
$$\varepsilon_{CT}(T) = -6.800 \times 10^{-3} + 9.700 \times 10^{-6}(T - 273) \qquad for \quad T > 1273$$

Here T is the temperature (K). Values tabulated for relevant temperature range are shown in Figure 2-19.

Acceptable range: a reference to a valid Tabular Function if non-zero, all tabulated values must be within the range  $0.0 \leq$  $\varepsilon_{CT}(T) \leq 0.1$ 0

Default value:



Figure 2-19 Gap model data for frequently used materials - strain function

W-7 (R): IYMCSC Tabular Function defining the Young modulus E(T) (Pa), versus temperature T, for the cladding. The cladding elastic deformation is calculated from:

$$x_{CE} = r_{cm} \left( \frac{\sigma_h - v \sigma_z}{E} \right)$$

Here  $r_{cm}$  is the cladding mid-point radius,  $\sigma_h$  is the cladding hoop stress (Pa),  $\sigma_z$  is the cladding axial stress (Pa), v is the Poisons ratio. The hoop and axial stresses are given by:

$$\sigma_{h} = \frac{P_{I} \cdot r_{I} - P_{O} \cdot r_{O}}{r_{O} - r_{I}} \qquad \sigma_{z} = \frac{P_{I} \cdot r_{I}^{2} - P_{O} \cdot r_{O}^{2}}{r_{O}^{2} - r_{I}^{2}}$$

P = pressure (Pa), r = cladding radius (m), subscripts: I = inner surface of cladding (gap), O = outer surface of cladding (fluid). E is the Young modulus calculated from Tabular Function IYMCSC. <u>NOTE: cladding</u> elastic deformation is calculated only when there is a boundary volume defined (in 1-D IVLRSC>0, in 2-D IVLBTC>0), because only then the cladding outer pressure,  $P_{O}$ , is available as the pressure in the boundary volume.

For the Zircaloy cladding, the Young modulus is given by:

$$E(T) = 1.088 \times 10^{11} - 5.475 \times 10^{7} T \qquad for \quad T < 1090$$
$$E(T) = 9.210 \times 10^{10} - 4.050 \times 10^{7} T \qquad for \quad T > 1240$$

Here *T* is the temperature (K). Values of the Young modulus tabulated for relevant temperature range are shown in Figure 2-20.



Figure 2-20 Gap model data for frequently used materials - Young modulus

Acceptable range:	a reference to a valid Tabular Function if non-zero,
	all tabulated values must be within the range $10^7 \leq$
	$E(T) \le 10^{12}  \mathrm{Pa}$
Default value:	0

The set of 7 words defined above is repeated until all fuel regions are described. The total number of entries in this record must be a multiple of 7. The number of sets per single input record must not be larger than 5. Multiple records with the same record identified (340001) may be entered. Data is read in the order in which these records appear in the input. The number of fuel regions must be the same as in the records 340000.

#### 2.3.31 Record: 340002, User-defined Gap Conductance

A user-defined gap conductance may be specified in this record. The gap conductance may be either constant or time-dependent, calculated by a Control Function.

W-1 (R): HGPCSC Gap conductance for the core fuel region number 1, defined as follows:  
HGPCSC>0: Constant gap conductance, 
$$h_{gap}$$
 (W/m<sup>2</sup>-K)  
HGPCSC<0: Gap conductance will be calculated by the Control  
Function with the number |HGPCSC|. The value obtained from the CF  
will be interpreted as gap conductance  $h_{gap}$  (W/m<sup>2</sup>-K), with the following  
limits:  $1.0 \le h_{gap} \le 1.0 \times 10^{10}$   
HGPCSC=0: Gap conductance will be calculated based on the data  
entered in the following input records.  
*Acceptable range:*  $0.0 \le$  HGPCSC  $\le 1.0 \times 10^{10}$   
*Default value:* 0.0

... until constant gap conductance is defined for all fuel regions. Multiple records with the same record identified (340002) may be entered. Data is read in the order in which these records appear in the input. If the record is entered, the number of fuel regions must be the same as in the records 340000 and 340001.

#### 2.3.32 Record: 3410XX, Gap Data

XX is the gap model number,  $1 \le XX \le 10$ . The maximum number of the gap models is 10. The overall heat transfer coefficient in gap is computed as a sum of thee terms:

$$h_{gap} = h_r + h_c + h_s$$

 $h_r$  radiation, (W/m<sup>2</sup>-K)

- $h_c$  conduction through gas, (W/m<sup>2</sup>-K)
- $h_s$  conduction through solid, due to contact of fuel and cladding, (W/m<sup>2</sup>-K)

• *Radiation*. The radiation term is obtained as:

$$h_r = \sigma \cdot \left(\frac{1}{\varepsilon_f} + \frac{1}{\varepsilon_c} - 1\right)^{-1} \cdot \left(T_f^2 + T_c^2\right) \cdot \left(T_f + T_c\right)$$

Here  $\varepsilon_f$ ,  $\varepsilon_c$ , are the emissivities of fuel and cladding,  $T_f$ ,  $T_c$ , are the surface temperatures of fuel and cladding,  $\sigma$  is the Stefan-Boltzmann constant, equal to  $5.67 \times 10^{-8}$  (W/m<sup>2</sup>-K<sup>4</sup>).

• *Gas conduction*. The conduction term is obtained as:

$$h_c = \frac{k_g}{d_{gap} + d_{\min} + (g_f + g_c)}$$

Here  $k_g$  is the conductivity of the gas mixture,  $d_{gap}$  is the gap thickness,  $d_{\min}$  is related to the roughness of the two surfaces,  $g_f$ ,  $g_c$ , are the temperature jump distances. The  $d_{\min}$  is obtained from:

$$d_{\min} = C_d \cdot (r_f + r_c)$$

Here  $r_{f}$ ,  $r_{c}$ , are the surface roughness of fuel and cladding respectively, and  $C_{d}$  is constant. The temperature jump distances are obtained from:

$$(g_{f} + g_{c}) = C_{j} \cdot \frac{k_{g} \cdot \sqrt{T_{g}}}{p_{g} \cdot \sum_{i=1}^{N_{gas}} X_{i} a_{i} M_{i}^{-1/2}}$$

Here  $C_j$  is constant,  $a_i$  is the accommodation coefficient (-),  $T_g$  is the gap gas temperature (K),  $M_i$  is the gas molar weight (kg/kmol),  $X_i$  is the gas molar fraction (-), and  $p_g$  is the gas pressure in the gap (Pa). The thermal accommodation coefficient is based on Ullman data [44]:

$$a_{i} = a_{He} + \frac{M_{i} - M_{He}}{M_{Xe} - M_{He}} \cdot (a_{Xe} - a_{He})$$
$$a_{He} = 0.425 - 2.3 \times 10^{-4} \cdot T_{g}$$
$$a_{Xe} = 0.740 - 2.5 \times 10^{-4} \cdot T_{g}$$

The gas pressure in the gap is computed from:

$$p_g = \frac{p_0}{T_0} \cdot T_g$$

Here  $p_0$ ,  $T_0$  are the gas pressure and temperature in reference state and  $T_g$  is the current gas temperature in the gas plenum. The gas plenum is defined by the user for each common region. A CV fluid temperature or SC/TC node temperature may be selected. This should be selected as the volume or structure most closely associated with the non-fuel region in a fuel pin at the top of a stack of fuel pellets.

• *Solid conduction.* The heat transfer due to fuel-cladding contact is obtained as:

$$h_s = C_s \cdot \frac{k_s}{\sqrt{r_t}} \cdot \left(\frac{p_a}{H_c}\right)^n$$

Here  $C_s$  is constant,  $k_s$  is the effective solid conductivity,  $p_a$  is the apparent interfacial pressure in the point of contact, H is the Meyer hardness of the softer material (typically cladding),  $r_t$ is the effective surface roughness. The effective solid conductivity is obtained from:

$$k_s = 2 \cdot \frac{k_f \cdot k_c}{k_f + k_c}$$

Here  $k_f$ ,  $k_c$ , are the conductivities (W/m-K) of fuel and cladding respectively. The effective surface roughness is obtained from the Ross and Stoute model [45]:

$$r_t = \sqrt{\frac{r_f^2 + r_c^2}{2}}$$

The input parameters needed for the three terms are described subsequently below.

• Radiation data

W-1 (R):	EFGCMP	Emissivity of fuel, <i>Acceptable range:</i>	$\varepsilon_{f}$ , (-). $0.0 < \text{EFGCSC} \le 1.0$ (a small number, $< 10^{-50}$ , sets the value to 0.0)
		Default value:	0.8
W-2 (R) :	ECGCMP	Emissivity of cladd Acceptable range:	ling, $\varepsilon_c$ , (-). $0.0 \leq \text{ECGCSC} \leq 1.0$ (a small number $< 10^{-50}$ sets the value to 0.0)
		Default value:	0.9
• Gas con	nduction date	a	
W-3 (R) :	CDGCMP	Constant $C_d$ , (-). Acceptable range:	$0.0 \le CDGCSC \le 10^{10}$
		Default value:	(a small number, $<10^{-50}$ , sets the value to 0.0) 1.5
W-4 (R) :	RFGCMP	Fuel surface rought Acceptable range:	ness, $r_f$ , (m). $0.0 \le \operatorname{RFGCSC} \le 1.0 \times 10^{-3}$
		Default value:	$3.3 \times 10^{-6}$
W-5 (R) :	RCGCMP	Cladding surface ro Acceptable range:	bughness, $r_c$ , (m). $0.0 \le \operatorname{RCGCSC} \le 1.0 \times 10^{-3}$ (a small number $< 10^{-50}$ sets the value to 0.0)
		Default value:	$1.78 \times 10^{-6}$

W-6 (R): CJGCMP Constant  $C_j$ , (-). Acceptable range:  $0.0 \le CJGCSC \le 1.0$ (a small number,  $<10^{-50}$ , sets the value to 0.0) Default value: 0.0247

• Solid conduction data

W-7 (R) :	CSGCMP	Constant $C_{s}$ , (m <sup>-1/2</sup> ).						
		Acceptable range:	$0.0 \le CSGCSC \le 1000.0$					
		Default value:	$1.189 \times 10^1$ (Ross and Stoute model [45])					
			(a small number, $<10^{-50}$ , sets the value to 0.0)					

## W-8 (R) : PAGCMP Apparent interfacial pressure in the point of contact $p_a$ , (Pa).

0 < PAGCMP < 1000: the interfacial pressure is defined by the TF with number PAGCMP. The table gives  $p_a$  in (Pa) versus time (s). The values obtained from the TF are limited by a minimum of 0.0 Pa and a maximum of  $10^{12}$  Pa.

-1000 < PAGCMP < 0: the interfacial pressure is defined by the CF with number |PAGCMP|. The function gives  $p_a$  in (Pa) versus time (s). The values obtained from the CF are limited by a minimum of 0.0 Pa and a maximum of  $10^{12}$  Pa.

 $PAGCMP \ge 1000$ : The interfacial pressure is constant and equal to PAGCMP.

PAGCMP ≤ –1000: The interfacial pressure is calculated from dynamic expansion model. It is equal to zero if the cladding inner radius is larger or equal to the fuel outer radius. If the cladding inner radius,  $r_{c,i}$  is smaller than the fuel outer radius,  $r_{f,o}$ , then the cladding inner radius is assumed to change due to elastic deformation The cladding elastic deformation due to fuel rod expansion is equal to:  $\delta_{CE} = r_{f,o} - r_{c,i}$ . The interfacial pressure is calculated from:

$$p_a = \frac{E}{r_{cm}} \cdot \frac{r_o - r_I}{r_I} \cdot \delta_{CE} \cdot X_P$$

Here  $r_{cm}$  is the cladding mean radius (m),  $r_I$  is the inner radius of cladding,  $r_O$  is the outer radius of cladding, E is the Young modulus (Pa),  $X_P$  is a user-defined multiplier XPGCMP (Word 11 below). Acceptable range: PAGCMP $\leq 10^{12}$  or reference to a TF or a CF

*Default value:* -1000.0 if the dynamic expansion is used, 0.0 otherwise

## W-9 (I): HCGCMP Indicator defining Meyer hardness of cladding, $H_c$ , (Pa).

HCGCSC < 1000: The Meyer hardness is defined by the Tabular Function with number HCGCSC. The table gives Meyer hardness in (Pa) versus temperature (K). The values obtained from the Tabular Function are limited by a minimum of  $10^6$  Pa and a maximum of  $10^{12}$ . HCGCSC > 1000: The Meyer hardness is constant and equal to HCGCSC. Approximate values for SS304 and Zircaloy are shown in Figure 2-21.

Approximate values for SS504 and Zircaroy are shown in Figure 2-21. Acceptable range:  $10^6 < H_c < 10^{12}$ , or reference to a Tabular Function Default value:  $1000 \times 10^6$  Pa

W-10 (R): XNGCMP Power n, (-), in the formula for  $h_s$ . Acceptable range:  $0.0 \le \text{XNGCSC} \le 5.0$ Default value: 1.0 (Ross and Stoute model [45])



Figure 2-21 Meyer hardness of SS-304 and Zircaloy

W-11 (R): XPGCMP User-defined multiplier  $X_P$ , (-), in the formula for  $p_a$ . Acceptable range:  $0.0 \le \text{XPGCSC} \le 1.0$ Default value: 1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0)

## 2.3.33 Record: 342XXX, Definition of Common Fuel Regions for Gap Calculations

XXX is the common fuel region for gap calculations (single fuel rod). The region numbers must be consecutive. The common fuel rod regions are introduced for the following reason. If a fuel rod is represented by several Solid Heat Conductors (there is an axial division of the fuel rods), then the gap parameters, such as gas pressure and gas composition in the gap, are common for each such region. Therefore the common fuel regions must reflect the axial nodalization of the fuel rods.

If the Radioactive Particle Transport Package is used, and the RT core regions are used (record 883000), the common fuel regions for cladding failure in the RT Package (records 8832XX) must be consistent with the common fuel regions for gap calculations in the SC Package, defined in this record. The maximum number of common fuel regions is NCRMSC = 200.

W-1 (I) :	IICRSC(1)	Fuel region number to the common fuel be the same in the of <i>Acceptable range:</i> <i>Default value:</i>	r IICRSC(1) (defined in the record 340000) belongs l region XX. Gap pressure and gas composition will common fuel regions. must be one of the core regions defined in records 340000. XX.
W-2 (I) :	IICRSC(2)	Fuel region number to the common fuel be the same in the of <i>Acceptable range:</i> <i>Default value:</i>	r IICRSC(2) (defined in the record 340000) belongs l region XX. Gap pressure and gas composition will common fuel regions. must be one of the core regions defined in records 340000. none
W-3 (I) :	IICRSC(3)	Fuel region number to the common fuel be the same in the of <i>Acceptable range:</i> <i>Default value:</i>	r IICRSC(3) (defined in the record 340000) belongs l region XX. Gap pressure and gas composition will common fuel regions. must be one of the core regions defined in records 340000. none

... until all members of the common fuel regions are defined. The maximum number of fuel regions in a single common fuel region is 200. Several records with the same number may be entered. Data is read in the order in which these records appear in the input.

## 2.3.34 Record: 343XXX, Composition of the Gap Gas

XXX is the common fuel region number,  $1 \le XXX \le 200$ . The common fuel regions for fuel rods are defined in the records 342XXX. The maximum number of the common fuel regions is NCRMSC = 200. The gas composition in the gap is defined in those records. The total number of entries in this record must be a multiple of 2.

W-1 (I) :	IGAS	Gas number, (-). M	lust be one of the available gases. The built-in gases
		are: $1 = H_2$ , $2 = He_2$	$3 = $ steam, $4 = N_2$ , $5 = O_2$ , $6 = CO_2$ .
		Acceptable range:	$1 \le IGAS \le NGASCV \le NGMXFL = 20$
		Default value:	2 (Helium)

W-2 (R):CVCRSCMole fraction of gas IGAS. If the sum of CVCRSC for all<br/>noncondensables is not equal to one, then CVCRSC will be normalized<br/>during input processing.Acceptable range: $0.0 \leq CVCRSC(IGAS) \leq 1.0$ <br/>Default value:0.0 (if no data is specified, assume 100% Helium)

## 2.3.35 Record: 344XXX, Reference Parameters of the Gap Gas

XXX is the common fuel region number,  $1 \le XXX \le 200$ . The common fuel regions for fuel rods are defined in the records 342XXX. The maximum number of the common fuel regions is NCRMSC = 200. The gas pressure in the gap is computed from:

$$p_g = \frac{p_0}{T_0} \cdot T_g$$

W-1 (R):TOCRSCReference temperature of the gap gas,  $T_0$  (K).Acceptable range: $270.0 \le \text{TOCRSC} \le 10,000.0$ Default value:300.0

W-2 (R) :POCRSCReference pressure of the gap gas,  $p_0$  (Pa) at the reference temperature,<br/> $T_0$ .<br/>Acceptable range:  $1.0 \le \text{POCRSC} \le 1.0 \times 10^{10}$ <br/>Default value:  $1.0 \times 10^5$ 

 $T_g$  is the current gas temperature in the gas plenum. The gas plenum is defined below. A CV fluid temperature or SC/TC node temperature may be selected. If nothing is selected by default the temperature of the gap node of the SC or TC listed as first on the common fuel region will be used.

W-3 (I) :	IGP1SC	<ul> <li>Indicator 1 of the gas gap plenum</li> <li>= 1: CV atmosphere or pool temperature defines the gap gas plenum temperature.</li> <li>= 2: SC node number defines the gap gas plenum temperature.</li> <li>= 3: TC node number defines the gap gas plenum temperature.</li> <li>Acceptable range: 1, 2, and 3</li> <li>Default value: 2 or 3.</li> </ul>						
W-4 (I) :	IGP2SC	Region indicator 2. if IGP1SC=1: if IGP1SC=2: if IGP1SC=3: Acceptable range: Default value:	Defines CV, SC, or TC number. CV reference number SC reference number TC reference number must be a valid reference number of a Control Volume, 1-D, or 2-D Solid Heat Conductor. SC or TC number which is first on the list for this common region					
W-5 (I) :	IGP3SC	Region indicator 3 if IGP1SC=1: if IGP1SC=2:	1 = CV atmosphere, $2 = CV$ pool temperature SC cell number					

if IGP1SC=3:	TC cell number
Acceptable range:	
if IGP1SC=1:	1 or 2
if IGP1SC=2	$1 \leq IGP3SC \leq No.$ of cells in SC IGP2SC
if IGP1SC=3	$1 \leq IGP3SC \leq No.$ of cells in TC IGP2SC
Default value:	gap cell of SC or TC

#### 2.3.36 Record: 345000, Number of Integration Points for the Gap Calculations

In case of fuel-cladding centerline shift (FCCSSC>0.0) the overall gap conductance,  $h_g$ , is computed based on the local gap conductances,  $h_g'(d_g')$ , obtained for the local gap size,  $d_g'$ , from the following formula:

$$h_g = \frac{1}{\pi} \int_0^{\pi} h_g' [d_g'(\theta)] \cdot d\theta = \frac{1}{N} \sum_{i=1}^N h_g' [d_g'(\theta_i)]$$
$$\theta_i = \frac{i-1}{N-1} \cdot \pi$$

The local gap size is obtained from (Figure 2-22):

$$d_{g}'(\theta_{i}) \approx R_{c,i} - R_{f,o} - \Delta \cdot \cos(\theta_{i})$$

Approximation is good for gaps small compared to the cladding and fuel radii,  $d_g \ll R_{c,i} \approx R_{r,o}$ .





W-1 (I): NIGCMP Number of integration points. The minimum number of points is 2. In such case the local gap conductance is calculated in two points only, the smallest gap ( $\theta = 0$ ) and the largest gap ( $\theta = \pi$ ). Influence of the number of integration points is shown in Figure 2-23. It is seen that in practice 50 points are sufficient to obtain an accurate (*N*-independent value of  $h_{gap}$ . Figure 2-24 shows the effect of centerline shift on  $h_{gap}$ . for several different gap thickness. Note that the value of gap conductance for the fuel-cladding centerline shift of 1.0 is between a factor of 2 and a factor of 4 larger than the value for no shift. *Acceptable range:*  $2 \le \text{NIGCMP} \le 1000$ *Default value:* 100





Figure 2-23 Influence of number of points, *N*, on gap conductance *h*<sub>gap</sub>



Figure 2-24 Influence of centerline shift on gap conductance

## 2.3.37 Record: 390XXX, Axial Conduction and Direct Contact Conduction

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record activates the axial heat transfer process for this 1-D Solid Heat Conductor. The maximum number of axial heat transfer processes is 10 for a single 1-D Solid Heat Conductor and 100 for a single 2-D Conductor.

The axial heat conduction or direct contact heat transfer between two structures, i (the "current solid heat conductor", XXX) and j (the "other solid heat conductor"), is considered - Figure 2-25. The heat transfer between the two solid heat conductors is calculated from:

$$Q_{i-j} = A_{i-j} \frac{T_i - T_j}{R_{i-j}}$$

 $Q_{i-j}$  heat transferred between the solid heat conductors *i* and *j*, (W)

 $A_{i-j}$  area of contact between the solid heat conductors *i* and *j*, (m<sup>2</sup>)

 $T_i$  temperature of the solid heat conductor *i* (local or averaged - see Word 2 below), (K)

 $T_j$  temperature of the solid heat conductor j (local or averaged - see Word 2 below), (K)

 $R_{i-j}$  thermal resistance for the axial heat flow between the solid conductors *i* and *j*, (m<sup>2</sup>-K/W)

The thermal resistance for the heat flow is obtained from:

$$R_{i-j} = \frac{L_i}{k_i} + \frac{1}{h_{i-j}} + \frac{L_j}{k_j}$$

*L<sub>i</sub>* length for axial conduction in the solid heat conductor *i* (input parameter X1AXSC)

 $k_i$  thermal conductivity in the solid heat conductor *i* 

 $L_i$  length for axial conduction in the solid heat conductor *j* (input parameter X2AXSC)

- $k_j$  thermal conductivity in the solid heat conductor j
- $h_{ij}$  heat transfer coefficient at the point of contact of solid heat conductors *i* and *j*

W-1 (I) :	J1AXSC	<ul> <li>First indicator of the other solid heat conductor (j).</li> <li>=1: 1-D Solid Heat Conductor (SC)</li> <li>=2: 2-D Solid Heat Conductor (TC) - not used, transfer between 1-D and 2-D can be defined in the records 490XXX</li> <li>Acceptable range: 1</li> <li>Default value: none</li> </ul>
W-2 (I) :	J2AXSC	Second indicator of the other solid heat conductor (j).if J1AXSC=1:SC reference numberif J1AXSC=2:TC reference number - not used, transfer between 1-D and 2-D can be defined in the records 490XXXAcceptable range:must be a valid reference number of SCDefault value:none
W-3 (I) :	IIAXSC	Cell number for axial or direct contact heat conduction through the current solid heat conductor, <i>i</i> . >0: cell number for direct contact heat transfer (Figure 2-25–b), see Volume 3, discussion on direct contact heat transfer modeling.

		=0: axial heat tra cell or cells in the I2AXSC = 0, the nodalization. <i>Acceptable range:</i> <i>Default value:</i>	ansfer with all cells transferring h other solid heat conductor (Fig n both solid heat conductors r cell number or 0 none	eat to corresponding ure 2-25–a). If also nust have identical
W-4 (I) :	I2AXSC	Cell number for ax solid heat conducto >0: cell number Volume 3, discussi =0: axial heat tra cell or cells in the I1AXSC = 0, the nodalization. Acceptable range: Default value:	ial or direct contact heat conduction, <i>j</i> . for direct contact heat transfer ( ion on direct contact heat transfer ansfer with all cells transferring h other solid heat conductor (Fig n both solid heat conductors r cell number or 0 none	on through the other Figure 2-25–b), see modeling. eat to corresponding ure 2-25–a). If also nust have identical
W-5 (R) :	X1AXSC	Length of the axia heat conductor, <i>L<sub>i</sub></i> ( <i>Acceptable range:</i> <i>Default values:</i>	l heat conduction (Figure 2-25) (m). $0.0 \le X1AXSC \le 10,000.0$ half of the current SC length, 0.0	in the current solid if I1AXSC=0 if I1AXSC>0
W-6 (R) :	X2AXSC	Length of the axial conductor, $L_j$ (m). Acceptable range: Default values:	heat conduction (Figure 2-25) ir $0.0 \le X2AXSC \le 10,000.0$ half of the other SC length, 0.0	if I2AXSC=0 if I2AXSC>0
W-7 (I) :	IHAXSC	Pointer to a Tabula heat transfer coeff depending on MH then $h_{i,j}$ or $1/h_{i,j}$ wil number: IHAXSC. defined by a Contr If the current value to 0.0, there will b 0.0). The value ob internally limited to is implied (IIAXS resistance may cau $1/h_{i,j} = 10^{-3} \text{ m}^2\text{-K/W}$ contact. However, allows smaller con is $1/h_{i,j} = 10^{-5} \text{ m}^2\text{-K/W}$ <i>Acceptable range:</i>	ar or Control Function that defin- icient, $h_{i:j}$ (W/m <sup>2</sup> -K), or resistan AXSC (Word 10 below). If the l be defined by a Tabular Function. If the number is negative, then ol Function with the reference nu of the Tabular or Control Function is no resistance at the contact por tained from the Tabular or Control to the range $10^{-10} - 10^{10}$ . If direct for the range $10^{-10} - 10^{10}$ . If direct for C > 0 and I2AXSC $> 0$ ) then a use numerical instabilities. A min- v is applied in case of SC-to-TC a in case of SC-to-SC a special r tact resistance. In such case the two special reference numb Control Function, if non-zero. 0.	es the direct contact ce, $1/h_{i\cdot j}$ (m <sup>2</sup> -K/W), number is positive, on with the reference $h_{i\cdot j}$ or $1/h_{i\cdot j}$ will be mber:  IHAXSC . on is smaller or equal bint ( $h_{i\cdot j} = \infty$ , $1/h_{i\cdot j} =$ rol Function will be contact heat transfer a very small contact himum resistance of and TC-to-TC direct numerical procedure minimum resistance C, record 303XXX). ber of a Tabular or a

- W-8 (R): **A1AXSC** Multiplier on the heat transfer area, (-). The area of heat transfer,  $A_{i,j}$ , is automatically calculated by the code as the smaller of the areas of the connected conductor cells multiplied by the corresponding multiplier. A1AXSC is applied for the cell in the "current" SC (while A2AXSC is applied to the "other" SC). Note that in case of axial heat transfer (heat transfer perpendicular to the normal heat transfer in this conductor), the cross-sectional area of the cell is used. In case of direct contact heat transfer (heat transfer along the normal heat transfer in this conductor), the area of boundary surface. The value obtained in this way is multiplied by A1AXSC. NOTE: The user may also define the area directly, by using the AXAXSC (W-15 below). In this case the multipliers A1AXSC, A2AXSC will be ignored. Acceptable range:  $0.0 < A1AXSC \le 10^{10}$ Default value: 1.0
- Multiplier on the heat transfer area, (-). The area of heat transfer,  $A_{i-i}$ , is W-9(R): A2AXSC automatically calculated by the code as the smaller of the areas of the connected conductor cells multiplied by the corresponding multiplier. A2AXSC is applied to the "other" SC (while A1AXSC is applied for the cell in the "current" SC). Note that in case of axial heat transfer (heat transfer perpendicular to the normal heat transfer in this conductor), the cross-sectional area of the cell is used. In case of direct contact heat transfer (heat transfer along the normal heat transfer in this conductor), the area of boundary surface. The value obtained in this way is multiplied by A2AXSC. NOTE: The user may also define the area directly, by using the AXAXSC (W-15 below). In this case the multipliers A1AXSC, A2AXSC will be ignored. Acceptable range:  $0.0 < A2AXSC \le 10^{10}$ Default value: 1.0
- W-10(I): MHAXSC Parameter affecting direct contact conduction: =1: IHAXSC defines the heat transfer coefficient,  $h_{i-j}$  (W/m<sup>2</sup>-K) =2: IHAXSC defines the resistance,  $1/h_{i-i}$  (m<sup>2</sup>-K/W) Acceptable range: 1 or 2 Default value: 1
- W-11 (I): M1AXSC Pointer to a material number which defines thermal conductivity in the current solid heat conductor. If zero or no value is specified the conductivity of the actual material, defined in the records 310XXX, is used. If a positive value is defined then the thermal conductivity of the material M1AXSC is used. For example, in case of a pebble bed model, the actual material should represent the true material of a pebble, to get a correct surface-to-center temperature difference. M1AXSC should be an artificial material, which is used to define the effective conductivity of the pebble bed, for example from Zehner-Schlunder or Robold correlation (see Volume 3, test PBR-k-eff).
  - Acceptable range: must be a valid reference number of a solid material, defined in records 801XXX, 802XXX, 803XXX - see section 2.10). 0

Default value:

W-12 (I): M2AXSC Pointer to a material number which defines thermal conductivity in the other solid heat conductor. If zero or no value is specified the conductivity of the actual material, defined in the records 310XXX, is used. If a positive value is defined then the thermal conductivity of the material M2AXSC is used. For example, in case of a pebble bed model, the actual material should represent the true material of a pebble, to get a correct surface-to-center temperature difference. M2AXSC should be an artificial material, which is used to define the effective conductivity of the pebble bed, for example from Zehner-Schlunder or Robold correlation (see Volume 3, test PBR-k-eff).

Acceptable range: must be a valid reference number of a solid material, defined in records 801XXX, 802XXX, 803XXX - see section 2.10).

*Default value:* 0

W-13 (I): L1AXSC Option for the direct contact transfer (I1AXSC > 0 and I2AXSC > 0) in the current solid heat conductor.

=0: Cell-to-cell direct contact. The temperature  $T_i$  is taken from the cell I1AXSC. The calculated heat is removed/added to the cell I1AXSC. =1: Global radial transfer. The temperature  $T_i$  is equal to the average temperature of the current solid heat conductor (mass-averaged or volume-averaged, depending of IAVESC). The calculated heat is distributed over all cells, proportionally to the cell volume or cell mass. The input parameter I1AXSC is used only to determine the area for the heat transfer. This option is intended to model the effective conductivity of the pebble bed or prismatic blocks (see Volume 3, tests PBR-k-eff, PMR-k-eff).

Acceptable range:0 or 1Default value:0

W-14 (I): L2AXSC Option for the direct contact transfer (I1AXSC > 0 and I2AXSC > 0) y in the other solid heat conductor. Cell-to-cell direct contact. The temperature  $T_i$  is taken from the =0:cell I2AXSC. The calculated heat is removed/added to the cell I2AXSC. Global radial transfer. The temperature  $T_i$  is equal to the average =1: temperature of the other solid heat conductor (mass-averaged or volumeaveraged, depending of IAVESC). The calculated heat is distributed over all cells, proportionally to the cell volume or cell mass. The input parameter I2AXSC is used only to determine the area for the heat transfer. This option is intended to model the effective conductivity of the pebble bed or prismatic blocks (see Volume 3, tests PBR-k-eff, PMR-k-eff). Acceptable range: 0 or 1 Default value: 0

W-15 (R): AXAXSC Area of heat transfer, (m<sup>2</sup>). If zero or no value is entered, then the area is calculated as the smaller value of the cell areas (multiplicity included):

 $A_{HT} = MIN (A_{cell,SC-1} \times A1AXSC, A_{cell,SC-2} \times A2AXSC)$ 

If a positive value is entered, then the heat transfer area is equal to the entered value:

## $A_{HT} = AXAXSC$

Acceptable range:  $0.0 \le AXAXSC \le 10^{10}$ Default value: 0.0

W-16 (I): KAXSC Sequential number of the axial heat transfer process. If no value or zero is entered, then the data are read sequentially - the first record 390XXX in the input file is interpreted as containing the first axial transfer process, the second record with this number the second heat transfer process, etc. *Acceptable range:* I = 1, 2, ..., 6 *Default value:* none

Examples are shown in Figure 2-25. Further examples and discussion is included in Volume 3.

Cases (a) and (c) - cell-to-cell axial heat conduction

\* SC-100 heat transfer to SC-200 \* - cell-to-cell transfer for all cells \* - "axial" heat transfer - perpendicular to the normal conduction heat flow \* - conduction length: L = 0.5 m for SC-100, L=0.6 m for SC-200 \* - contact h = TF-900 \* \* SC Cell-i Cell-j L-i L-j h 390100 1 200 0 0 0.5 0.6 900 \* Input for SC-100

alternatively the following input may be defined for SC-200:

\* SC Cell-i Cell-j L-i L-j h 390200 1 100 0 0 0.6 0.5 900 \* Input for SC-200

If both records are present, then an error "double specification of axial transfer" - will be encountered.



Figure 2-25 Axial conduction, direct contact between different SC

#### Cases (b) and (d) - all cells (axial) to one cell (direct contact)

```
* SC-100: heat transfer to SC-200
* - all cells from SC-100 transfer heat to cell 5 of SC-200
* - "axial" heat transfer for SC-100, normal conduction heat flow in SC-200
* - axial conduction length: L = 0.5 m for SC-100, L=0.0 m for SC-200
* - contact h = TF-900
* SC Cell-i Cell-j L-i L-j h
390100 1 200 0 5 0.5 0.0 900 * Input for SC-100
```

alternatively the following input may be defined for SC-200:

\* SC Cell-i Cell-j L-i L-j h 390200 1 100 5 0 0.0 0.5 900 \* Input for SC-200

If both records are present, then an error "double specification of axial transfer" - will be encountered.

Case (e) - all cells (axial) to one cell (direct contact)

```
* SC-100: heat transfer to SC-200
* - all cells from SC-200 transfer heat to cell 3 of SC-100
* - "axial" heat transfer - perpendicular to the normal conduction heat flow
* - conduction length: L = 0.5 m for SC-100, L=0.3 m for SC-200
* - contact h = TF-900
*
* SC Cell-i Cell-j L-i L-j h
390100 1 200 3 0 0.5 0.3 900 * Input for SC-100
```

## Case (f) - single cell to single cell heat transfer

```
* SC-100: heat transfer to SC-200
* - outer cell of SC-200 transfer heat to cell 3 of SC-100
* - "radial" heat transfer
* - conduction length: L = 0.0 m for SC-100, L=0.0 m for SC-200
* - contact h = TF-900
*
* SC Cell-i Cell-j L-i L-j h
390100 1 200 3 3 0.0 0.0 900 * Input for SC-100
```

Example of pebble reactor. Inlet pipes passing through s reflector structure - Figure 2-26.



Figure 2-26 Example of SC-to-SC transfer (see Volume 3, PBMR-IP

Example input, linking SC-130, which represents space around the inlet channels and SC-120, which represents the reflector, is shown below. This example case is discussed further in Volume 3.

\*
 SC i j L-i L-j h A1 A2
390130 1 120 3 5 0.01 0.00 200 0 0 \* Axial heat transfer to SC-120, contact h = TF-200
605200 h-c(1), W/m/K
600200 0.0 10000.0



**Example of pebble reactor.** pebble bed effective conductivity - Figure 2-27.

Figure 2-27 Example of pebble bed heat transfer

Example input, linking SC-130, which represents the inner pebble ring, and SC-120, which represents the outer pebble ring, is shown below. This example case is discussed further in Volume 3.

*	S	SC	i	j	L-i	L-j	h	A1	A2									
390130	1	120	3	5	0.01	0.00	200	0	0 *	Axial	heat	transfer	to	SC-120,	contact	h =	TF	-200

**Example of prismatic reactor geometry.** Effective conductivity for block-to-block transfer - Figure 2-28.



Figure 2-28 Example of prismatic block heat transfer

Example input, linking SC-130, which represents the inner prismatic block, and SC-120, which represents the outer prismatic block, is shown below. This example case is discussed further in Volume 3.

\* SC i j L-i L-j h A1 A2 390130 1 120 3 5 0.01 0.00 200 0 0 \* Axial heat transfer to SC-120, contact h = TF-200

#### 2.3.38 Record: 399000, Interpolation Factor for Boundary Temperature

W-1 (R):FINTSCInterpolation factor. Used only if a boundary surface is linked to a<br/>Control Volume (IVLLSC > 0 or IVLRSC>0) and at the same time the<br/>boundary fluid temperature is defined by a Tabular or Control Function<br/>(ITPLSC $\neq$ 0 or ITPLSC $\neq$ 0). In such case the value obtained from the<br/>Tabular or Control Function is taken with the weighting factor of<br/>FINTSC and the temperature in the Control Volume is taken with the<br/>weighting factor of 1.0 – FINTSC.<br/>Acceptable range: 0.0 < FINTSC ≤ 1.0<br/>Default value: 0.5

#### 2.3.39 Examples of the 1-D Solid Heat Conductor Input Data

#### Example 1

As a first example, a cylindrical space, partly filled with water, is considered (Figure 2-29). Six 1-D Solid Conductors are used to model the walls, roof and floor. The walls are divided into upper part (above the liquid level) and lower part (below the liquid level). Thickness of all conductors is 1.0 m. The conductors are modelled using 10 cells of equal size (0.1 m each). The heat transfer from the outer side of the outer wall (SC-001 and SC-005) is modelled using Tabular Functions TF-005 and TF-006 for the heat transfer coefficient and the fluid temperature respectively. The heat transfer from the inner side of the inner wall (SC-002 and SC-006) is modelled using the Tabular Functions TF-003 and TF-004.



Figure 2-29 Geometrical configuration for Solid Conductor example problem
The heat transfer from the upper surface of the roof (SC-003) is modelled using the Tabular Functions TF-001 and TF-002. The lower part of the floor (SC-004) is insulated.

The SC input data for the example problem is shown below. Note that the surface areas of SC-003 and SC-004, which are equal to  $200\pi$ , were entered with a fair accuracy. This was done to be consistent with the view factors, needed when the thermal radiation models are applied for this configuration (see section 2.6.9).

```
* ----- SC-001
305001 Outer wall, upper part

      300001
      2
      5.0
      15.0
      7.5
      0
      * Main data : GEO, LEN, XO, ELEV, VER

      310001
      0.05
      1
      0.0
      358.0
      20
      * Cell data : DX, MAT, Q, T

      321001
      001
      *
      Left side : Vol

      322001
      000
      005
      006
      * Right side: Vol, H, HTC, Tfluid

* ----- SC-002
305002 Inner wall, upper part

      305002 inner wall, upper part

      300002 2
      5.0
      4.0
      7.5
      0
      * Main data : GEO, LEN, XO, ELEV, VER

      310002 0.05
      1
      0.0
      358.0
      20
      * Cell data : DX, MAT, Q, T

      321002 000
      003 004
      *
      Left side : Vol, H, HTC, Tfluid

      322002 002
      *
      Right side: Vol

* ----- SC-003
305003 Roof
300003 1 628.31853 0.0 10.5 1 * Main data : GEO,LEN,X0,ELEV,VER
310003 0.05 1 0.0 358.0 20 * Cell data : DX, MAT, Q, T

      310003 0.05
      1 0.0
      550.0
      20
      001 acc 1
      1.1

      321003 000 0 001 002
      *
      Left side : Vol, H, HTC, Tfluid

      322003 001
      *
      Right side: Vol

* ----- SC-004
305004 Floor
300004 1 628.31853 0.0 -0.5 -1 * Main data : GEO,LEN,X0,ELEV,VER
310004 0.05 1 0.0 358.0 20 * Cell data : DX, MAT, Q, T
                                                                                                             * Left side : Vol
321004 000
                                                                                                              * Right side: Vol
322004 001
* ----- SC-005
305005 Outer wall, lower part

      305005 Outer wall, lower part

      300005 2
      5.0
      15.0
      2.5
      0
      * Main data : GEO, LEN, XO, ELEV, VER

      310005 0.05
      1
      0.0
      358.0
      20
      * Cell data : DX, MAT, Q, T

      321005 001
      *
      Left side : Vol
      *

      322005 000 0
      005 006
      * Right side: Vol, H, HTC, Tfluid

* ----- SC-006
305006 Inner wall, lower part

      305006 Inner wall, lower part

      300006 2
      5.0
      4.0
      2.5
      0
      * Main data : GEO, LEN, XO, ELEV, VER

      310006 0.05
      1
      0.0
      358.0
      20
      * Cell data : DX, MAT, Q, T

      321006 000
      003 004
      *
      Left side : Vol, H, HTC, Tfluid

      322006 001
      *
      Right side: Vol

 * ----- Tabular Functions
* x y
600001 0.0 2000.00 * drywell-to-roof heat transfer coefficient
600002 0.0 415.00 * drywell (above roof) temperature
600003 0.0 2000.00 * drywell-to-inner wall heat transfer coefficient
600004 0.0 415.00 * drywell (left inner wall) temperature
600005 0.0 5.00 * outer wall-to-atmosphere heat transfer coefficient
600006 0.0 308.00 * atmosphere temperature
```

#### Example 2

As a second example a reactor core is modelled. The core consists of one hot rod and one average rod, each of them is represented by five 1-D Solid Heat Conductors in the axial direction (Figure 2-30). The hot rod is represented by SC-101 through SC-105. The average rod is represented by SC-201 through SC-205. The fuel regions and the common fuel regions are in such case defined as follows:

- Fuel regions (total reactor core): SC-101, SC-102, SC-103, SC-104, SC-105, SC-201, SC-202, SC-203, SC-204, SC-205
- Common fuel regions:
  - Common region 1 (hot rod):
    - SC-101, SC-102, SC-103, SC-104, SC-105
  - Common region 2 (average rod): SC-201, SC-202, SC-203, SC-204, SC-205

The hot rod and the average rod, shown in Figure 2-30, are made of 6 nodes. Nodes 1 - 4 represent the fuel, node 5 represents the gap, node 6 represents the cladding. This is the case for all SC-s in Figure 2-30. This is not a formal requirement; i.e. the gap node number may be different for different fuel regions or even for the same common fuel region. The only requirement is that all nodes representing the same gap must have the same thickness.

Gap Example		F	uel Ho	ot Rod	Gap	Clad			F	uel Avei	rage R	od <sub>Gap</sub>	Clad
SPECTRA		•	•	•	•		SC-201		•	•	•	•	
	Node 1	Node 2	Node 3	Node 4	Node 5	Node 6		Node 1	Node 2	Node 3	Node 4	Node 5	Node 6
SC-102	Node 1	Node 2 🕒	Node 3	Node 4 🕒	Node 5 🌑	Node 6	SC-202	Node 1	Node 2 🕒	Node 3	Node 4	Node 5	Node 6
SC-103	Node 1	Node 2 🔴	Node 3 🕒	Node 4 🔵	Node 5	Node 6	SC-203	Node 1	Node 2 🕒	Node 3 🕒	Node 4 🌒	Node 5 🕒	Node 6
SC-104	Node 1	Node 2 🕒	Node 3 🕒	Node 4 🔵	Node 5 🌒	Node 6	SC-204	Node 1	Node 2 🕒	Node 3 🕒	Node 4 🌒	Node 5 🌒	Node 6 🕳
SC-105	Node 1	Node 2 🕒	Node 3 🔴	Node 4 🕒	Node 5 🌑	Node 6 🕳	SC-205	Node 1	Node 2 🕒	Node 3 🔴	Node 4 🌑	Node 5	Node 6 🕳

Figure 2-30 Example model for fuel and gap calculations

Listing of the input defining the fuel regions, the gap and all Solid Heat Conductors, is provided below.

FUEL REGION DEFINITION 3 \* Region: 1 2 3 4 5 \* SC Node Gap 340000 1 101 0 1 1102 0 1 1103 0 1 1104 0 1 1105 0 1 \* Region: 6 7 8 9 10 \* Region: 6 / 8 9 10 \* SC Node Gap 340000 1 201 0 1 1 202 0 1 1 203 0 1 1 204 0 1 1 205 0 1 COMMON REGIONS 340201 1 2 3 4 5 \* Hot rod 340202 6 7 8 9 10 \* Average rod GAP DATA 341001 \* GAP 1 - USE DEFAULTS 305101 Hot rod, Level 1 305102 Hot rod, Level 2 305103 Hot rod, Level 3 305104 Hot rod, Level 4 305105 Hot rod, Level 5 Ν 302101 1 \* Hot rod, Level 1 302102 1 \* Hot rod, Level 2 302103 1 \* Hot rod, Level 3 302104 1 \* Hot rod, Level 4 302105 1 \* Hot rod, Level 5 GEO L X0 ELEV VER POWER 300101 2 0.5 0.0 2.25 0 1000 100 \* Hot rod, Level 1 
 300102
 2
 0.5
 0.0
 1.75
 0
 1000
 100 \*
 Hot rod,
 Level 2

 300103
 2
 0.5
 0.0
 1.25
 0
 1000
 100 \*
 Hot rod,
 Level 3
 300104 2 0.5 0.0 0.75 0 1000 100 \* Hot rod, Level 4 300105 2 0.5 0.0 0.25 0 1000 100 \* Hot rod, Level 5 Fuel 

 \*
 dx
 mat
 power
 T
 nodes

 310101
 0.0005
 101
 1.0
 500.0
 1
 \* Hot rod, Level 1

 310102
 0.0005
 101
 1.0
 500.0
 1
 \* Hot rod, Level 2

 310103
 0.0005
 101
 1.0
 500.0
 1
 \* Hot rod, Level 3

 310104
 0.0005
 101
 1.0
 500.0
 1
 \* Hot rod, Level 4

 310105
 0.0005
 101
 1.0
 500.0
 1
 \* Hot rod, Level 5

 Fuel 

 \*
 dx
 mat
 power
 T
 nodes

 310101
 0.001
 101
 1.0
 500.0
 3
 \* Hot rod, Level 1

 310102
 0.001
 101
 1.0
 500.0
 3
 \* Hot rod, Level 2

 310103
 0.001
 101
 1.0
 500.0
 3
 \* Hot rod, Level 3

 310104
 0.001
 101
 1.0
 500.0
 3
 \* Hot rod, Level 4

 310105
 0.001
 101
 1.0
 500.0
 3
 \* Hot rod, Level 5

 Gap \* dx mat power T nodes 310101 0.001 001 0.01 500.0 1 \* Hot rod, Level 1 310102 0.001 001 0.01 500.0 1 \* Hot rod, Level 2 

 310102 0.001
 001
 0.01 500.0
 1
 \* Hot rod, Level 2

 310103 0.001
 001
 0.01 500.0
 1
 \* Hot rod, Level 3

 310104 0.001
 001
 0.01 500.0
 1
 \* Hot rod, Level 4

 310105 0.001
 001
 0.01 500.0
 1
 \* Hot rod, Level 4

 \* Cladding \* dx mat power T nodes 310101 0.001 102 0.01 500.0 1 \* Hot rod, Level 1 310102 0.001 102 0.01 500.0 1 \* Hot rod, Level 2 310103 0.001 102 0.01 500.0 1 \* Hot rod, Level 3 310104 0.001 102 0.01 500.0 1 \* Hot rod, Level 4 310105 0.001 102 0.01 500.0 1 \* Hot rod, Level 5

\* Right CV \* Hot rod, Level 1 \* Hot rod, Level 2 322101 100 322102 100 \* Hot rod, Level 3 322103 100 322104 \* Hot rod, Level 4 100 322105 100 \* Hot rod, Level 5 305201 Average rod, Level 1 305202 Average rod, Level 2 305203 Average rod, Level 3 305204 Average rod, Level 4 305205 Average rod, Level 5 Ν 302201 1000 \* Average rod, Level 1 302202 1000 \* Average rod, Level 2 302203 1000 \* Average rod, Level 3 302204 1000 \* Average rod, Level 4 302205 1000 \* Average rod, Level 5 GEO L Х0 ELEV VER POWER 300201 2 0.5 0.0 2.25 0 500 100 \* Average rod, Level 1 300202 2 0.5 0.0 1.75 0 500 100 \* Average rod, Level 2 300203 2 0.5 0.0 1.25 0 500 100 \* Average rod, Level 3 
 300204
 2
 0.5
 0.0
 0.75
 0
 500
 100
 Average
 rod,
 Level 4

 300205
 2
 0.5
 0.0
 0.25
 0
 500
 100
 \*
 Average
 rod,
 Level 4

 300205
 2
 0.5
 0.0
 0.25
 0
 500
 100
 \*
 Average
 rod,
 Level 5
 Fuel mat power T \* dx mat power T nodes 310201 0.0005 101 1.0 500.0 1 \* Hot rod, Level 1 310202 0.0005 101 1.0 500.0 1 \* Hot rod, Level 2 dx nodes 

 1.0
 500.0
 1
 \* Hot rod, Level 2

 1.0
 500.0
 1
 \* Hot rod, Level 3

 1.0
 500.0
 1
 \* Hot rod, Level 4

 1.0
 500.0
 1
 \* Hot rod, Level 5

 310203 0.0005 101 
 310204
 0.0005
 101

 310205
 0.0005
 101
 Fuel mat power T dx nodes 310201 0.001 3 \* Hot rod, Level 1 3 \* Hot rod, Level 2 
 101
 1.0
 500.0

 101
 1.0
 500.0
 310202 0.001 
 101
 1.0
 500.0

 101
 1.0
 500.0

 101
 1.0
 500.0

 101
 1.0
 500.0
 3 \* Hot rod, Level 3 3 \* Hot rod, Level 4 3 \* Hot rod, Level 5 310203 0.001 310204 0.001 310205 0.001 Gap + mat power T nodes dx 1 \* Hot rod, Level 1 1 \* Hot rod, Level 2 001 0.01 500.0 001 0.01 500.0 310201 0.001 310202 0.001 1 \* Hot rod, Level 3 1 \* Hot rod, Level 4 1 \* Hot rod, Level 5 310203 0.001 001 0.01 500.0 3102040.0010010.01500.03102050.0010010.01500.0 Cladding dx mat power T nodes 1 \* Hot rod, Level 1 102 0.01 500.0 102 0.01 500.0 310201 0.001 310202 0.001 \* Hot rod, Level 2 1 

 310203
 0.001
 102
 0.01
 500.0
 1
 \* Hot rod, Level 3

 310204
 0.001
 102
 0.01
 500.0
 1
 \* Hot rod, Level 4

 310205
 0.001
 102
 0.01
 500.0
 1
 \* Hot rod, Level 4

 Right CV 322201 100 \* Average rod, Level 1 322202 100 \* Average rod, Level 2 \* Average rod, Level 3 322203 100 322204 100 322205 100 \* Average rod, Level 4 \* Average rod, Level 5 605100 Power table \* t (s) Relative power No. 600100 -1000.0 1.0

#### 2.4 2-D Solid Heat Conductor Input Data

### 2.4.1 Records: 400XXX, 2-D Solid Heat Conductor Main Data

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (I) :	IGEOTC	Geometry type, (-). IGEOTC = 1 : IGEOTC = 2 : Acceptable range: Default value:	rectangular geometry, cylindrical geometry, 1, 2. none.
W-2 (R) :	SIZETC	Size of solid cond type. IGEOTC = 1 : IGEOTC = 2 : Acceptable range: Default value:	uctor. The interpretation depends on the geometry length ( <i>z</i> -coordinate) of the 2-D structure, (m), not used. $0.0 < \text{SIZETC} \le 10^{10}$ . none.
W-3 (R) :	X0TC	Left side coordinate IGEOTC = 1 : IGEOTC = 2 : Acceptable range: Default value:	e. The interpretation depends on the geometry type. not used, inner radius of the cylinder, (m), $0.0 \le \text{X0TC} \le 10^{10}$ . 0.0.
W-4 (R) :	ELEVTC	Elevation of highes cylinder this is the <i>Acceptable range:</i> <i>Default value:</i>	st point of the conductor, (m). In case of a horizontal elevation of the cylinder axis - Figure 2-31. all real numbers (note that the elevations of these boundary cells that transfer heat to Control Volumes must lie within the elevations of the corresponding Control Volumes). 0.0.
W-5 (I) :	IVERTC	Vertical orientation Rectangular geomet IVERTC = 0 : IVERTC = 1 : Cylindrical geomet IVERTC = 0 : IVERTC = 1 : Acceptable range: Default value:	a of conductor, (-), see Figure 2-31. etry: <i>x-y</i> surface is horizontal, <i>z</i> -coordinate is vertical <i>x-y</i> surface is vertical, <i>z</i> -coordinate is horizontal, <i>y</i> - coordinate is vertical down ry: vertical cylinder ( <i>z</i> -coordinate is vertical) horizontal cylinder ( <i>z</i> -coordinate is horizontal) 0, 1 0





Figure 2-31 Vertical orientations of 2-D Solid Heat Conductors

- W-6(R) : POWRTC Internal power source, (W). In order to obtain the current internal source, the value of POWRTC is multiplied by the time dependent multiplier defined by IPOWTC (word 7) and by the constant multiplier POWMTC (word 9), if present. Acceptable range:  $-10^{10} \le \text{POWRTC} \le 10^{10}$ . Default value: 0.0.
- W-7 (I): **IPOWTC** Pointer to a Tabular Function which defines the internal power multiplier. If the number is equal to zero, then internal power source is constant, and equal to POWRTC (Word 6). If the number is positive, then the internal power multiplier will be defined by the Tabular Function IPOWTC. If it is negative, the multiplier will be defined by the Control Function | IPOWTC |. No lower or upper limit is imposed on the value obtained from Tabular or Control Function (thus negative power source is allowed). If there is no internal power source (POWRTC=0.0) then IPOWTC must also be equal to zero. Acceptable range: must be a valid reference number of a Tabular, or a Control Function, if non-zero.

Default value: 0.

W-8 (R): HINCTC Inclination of nearly horizontal tubes, (degree). Tubes that have small inclination should be modelled as horizontal (IVERTC=1, see Word 5 above) with HINCTC >  $0.0^{\circ}$ . The value is used by the condensation model.

Acceptable range:  $0.0^{\circ} \leq \text{HINCSC} \leq 20.0^{\circ}$ .

Default value:  $0.0^{\circ}$ .

W-9 (R) :POWMTCConstant power multiplier. The constant power multiplier is introduced<br/>to have an easy way of defining for example axial power profile.Acceptable range: $-10^{10} \le \text{POWMTC} \le 10^{10}$ <br/>Default value:1.0

#### 2.4.2 Records: 401000, TC Groups - General Data

W-1 (I): KGRPTC Default TC group number. TC groups are introduced for editing; at the end of input processing volumes and masses of all materials is printed for each TC group. TC groups may be used to check the volumes and masses of materials in primary system, secondary system, etc. Acceptable range:  $1 \le \text{KGRPTC} \le 10$ Default value: 1

#### 2.4.3 Records: 401XXX, Initial and Transient Temperatures

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	INTTC	Initial temperature calculation indicator.
w-1 (1) .	INTIC	1: Initial temperature distribution is calculated. If this option is selected, the program calculates the temperature distribution performing conduction calculation with a large ( $\Delta t$ =10 <sup>99</sup> s) time step. In rare cases convergence failure may be encountered when performing the initial step. Usually it is good to ignore the convergence failure, since the calculated initial temperatures are typically better than could be obtained by manual initialization.
		The convergence failure can be ignored, by setting IACSFL (Word 8 in record 920000 - see section 2.16.5).
		<ul> <li>Input values (Words 4 in records 310XXX) are used. Use this option also if temperatures should be read from an Initial Condition File - ICF (section 2.16.3).</li> </ul>
		Default value: 2
W-2 (R) :	ITYPTC	Transient temperature calculation indicator.
		1: Temperatures are time independent; that means the initial temperatures are kept through the transient.
		2: Transient temperatures are calculated from the conduction equation (normal TC type).
		Acceptable range: 1, 2.

Default value: 2.

W-3 (I):IGRPTCTC group number.TC groups are introduced for editing; at the end of<br/>input processing volumes and masses of all materials is printed for each<br/>TC group. TC groups may be used to check the volumes and masses of<br/>materials in primary system, secondary system, etc.<br/>Acceptable range:  $1 \leq IGRPTC \leq 10$ <br/>Default value:KGRPTC (defined in record 401000)

#### 2.4.4 Records: 402XXX, Multiplicity of the 2-D Solid Heat Conductor

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (R): XMLTTC Multiplicity of the 2-D solid conductor. This is the number of solid conductors that are identical to the conductor XXX. If XMLTTC<0 then multiplicity will be time-dependent and defined by a Control Function with reference number |-XMLTTC|.</li>
 Acceptable range: 0.0 < XMLTTC < 10<sup>10</sup> or CF reference number Default value: 1.0.

## 2.4.5 Records: 405XXX, Name of the 2-D Solid Heat Conductor

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (A) : NAMETC User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* 50 "underline" characters: "\_".

#### 2.4.6 Records: 410XXX, Number of Cells of the 2-D Solid Heat Conductor

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

- W-1 (I): NCLXTC Number of cells in *x*-direction (horizontal direction in rectangular geometry and radial direction in cylindrical geometry).
  - Acceptable range:  $2 \le \text{NCLXTC} \le 51$ . (The maximum value is 51 rather than 50 because it is convenient to use odd number of cells rather than even. Since the first and the last cell is often half filled see example 1 in

	Figure 2-32 - it is easier to nodalize a structure with
	equidistant nodes.)
Default value:	none.

W-2 (I):NCLYTCNumber of cells in y-direction (vertical direction in rectangular geometry<br/>and axial direction in cylindrical geometry).Acceptable range: $2 \le NCLYTC \le 51$ .<br/>Default value:none.

#### 2.4.7 Records: 411XXX, Cell Sizes - x-direction

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (R) :	CELXTC (1)	The size of half-cell, x-i considers all cells as co parameter is the half-cell can be totally filled we quarter-cell, three-quart <i>Acceptable range:</i> 0.0 <i>Default value:</i> non	row number 1, (m). Since the SPECTRA code nsisting of four identical quarter-cells, the input ll size, rather than a total size. Note that each cell ith material (full cell), partly filled (half-cell, er-cell) or empty (see section 2.4.9). $< CELXTC(1) \le 10^{10}$ . e.
W-2 (R) :	CELXTC (2)	The size of half-cell, x-rAcceptable range:0.0Default value:non	row number 2, (m). $< CELXTC(2) \le 10^{10}$ . e.
W-3 (R) :	CELXTC (3)	The size of half-cell, x-1Acceptable range:0.0Default value:non	row number 3, (m). $< CELXTC(2) \le 10^{10}$ . e.

... etc. until all NCLXTC cell sizes are specified.

#### 2.4.8 Records: 412XXX, Cell Sizes - y-direction

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (R) :	CELYTC (1)	The size of half-cell, y-row number 1, (m). Acceptable range: $0.0 < \text{CELYTC}(1) \le 10^{10}$ . Default value: none.
W-2 (R) :	CELYTC (2)	The size of half-cell, y-row number 2, (m). Acceptable range: $0.0 < \text{CELYTC}(2) \le 10^{10}$ . Default value: none.
W-3 (R) :	CELYTC	The size of half-cell, y-row number 3, (m).

(3) Acceptable range:  $0.0 < \text{CELYTC}(2) \le 10^{10}$ . Default value: none.

... etc. until all NCLYTC cell sizes are specified.

#### 2.4.9 Records: 413XXX, Cell Types

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (I) :	L	Row number in y-c values of cell types Acceptable range: Default value:	lirection. The following data must specify NCLXTC in the y-row number L $1 \le L \le NCLYTC$ . none.
W-2 (I) :	IT00TC (1,L)	Cell type for cell (1 The input entry ITG filling of each of th ITOOTC = $abcd$ , wi a - upper b - upper c - lower d - lower Each of the digits i 1 if the quarter-cell Acceptable range: Default value:	<ul> <li>L), (x-row 1, y-row L), (-).</li> <li>DOTC consists of four digits; each digit specifies the e four quarter-cells.</li> <li>here:</li> <li>-left quarter-cell.</li> <li>-left quarter-cell.</li> <li>-left quarter-cell.</li> <li>-left quarter-cell.</li> <li>-left quarter-cell.</li> <li>s equal to 0 if the quarter cell is empty, and equal to is filled with material.</li> <li>(see Figure 2-32)</li> <li>0000 (empty cell), 1111 (full cell)</li> <li>0001, 0010, 0100, 1000 (quarter-cells)</li> <li>0011, 0101, 1010, 1100 (half-cells)</li> <li>1110, 1101, 1011, 0111 (three-quarter-cells)</li> <li>1001, 0110 (two separate quarter-cells)</li> <li>For each quarter-cell must be adjacent to a filled quarter-cell in the neighboring cell, while an empty quarter-cell in the neighboring cells in a real 2-D Heat Conductor. (Note that the left side of Figure 2-32 shows definitions of cell types, arranged in rows of similar cells. The rows do not represent any particular structures, like the ones shown in the Example 1 and 2, on the right side of Figure 2-32.)</li> </ul>
W-3 (I) :	IT00TC(2,1	) Cell type for cell (	(2,L), ( <i>x</i> -row 2, <i>y</i> -row L), (-).

W-4 (I): IT00TC(3,1) Cell type for cell (3,L), (*x*-row 3, *y*-row L), (-).

..., etc., until all NCLXTC cells are defined for a given row. Figure 2-32 shows definitions of the cell types and two examples of simple 2-D structures, together with the corresponding cell type definitions.



Figure 2-32 Cell type definitions and examples of 2-D structures.

#### 2.4.10 Records: 414XXX, Material Data

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (I) :	L	Row number in <i>y</i> -direction. The following data must specify NCLXTC values of material identifiers for all cells in the <i>y</i> -row number L <i>Acceptable range:</i> $1 \le L \le NCLYTC$ . <i>Default value:</i> none.
W-2 (I) :	MATITC (1,L)	Pointer to a material number for cell (1,L), ( <i>x</i> -row 1, <i>y</i> -row L), (-). The cell in <i>x</i> -row 1, <i>y</i> -row L is assumed to be composed of a single material defined by this word.
		Acceptable range: must be a valid reference number of a solid material (defined in records 801XXX, 802XXX, 803XXX - see section 2.10). For an empty cell (IT00TC=0000) zero must be entered.

W-3 (I) :	MATITC (2,L)	Pointer to a material number for cell (2,L), ( <i>x</i> -row 2, <i>y</i> -row L), (-). The cell in <i>x</i> -row 2, <i>y</i> -row L is assumed to be composed of a single material defined by this word.
W-4 (I) :	MATITC (3,L)	Pointer to a material number for cell (3,L), ( <i>x</i> -row 3, <i>y</i> -row L), (-). The cell in <i>x</i> -row 3, <i>y</i> -row L is assumed to be composed of a single material defined by this word.

..., etc., until material data is defined for all NCLXTC cells in a given row.

## 2.4.11 Records: 415XXX, Internal Power Distribution

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (I) :	L	Row number in <i>y</i> -direction. The following data must specify NCLXTC values of internal power for all cells in the <i>y</i> -row number L. Acceptable range: $1 \le L \le NCLYTC$ . Default value: none.
W-2 (I) :	QFRCTC (1,L)	Relative power density in the cell (1,L), (x-row 1, y-row L), (-). The values are relative and may be scaled by any factor. The values will be normalized during the input processing so that the total internal power source of the conductor is always equal to POWRTC multiplied by the value of the Tabular or Control Function   IPOWTC   (if used). If the internal power source, POWRTC, is greater than zero, then QFRCTC must be greater than zero for at least one cell. If the internal power source, POWRTC, is equal to zero, then QFRCTC must be equal to zero for all cells. Acceptable range: $0.0 \leq QFRCTC \leq 10^{10}$ . For an empty cell (IT00TC=0000) zero must be entered. Default value: none.
W-3 (I) :	QFRCTC (2,L)	Relative power density in the cell (2,L), ( <i>x</i> -row 2, <i>y</i> -row L), (-).
W-4 (I) :	QFRCTC (3,L)	Relative power density in the cell (3,L), ( <i>x</i> -row 3, <i>y</i> -row L), (-).

..., etc., until relative power fractions are defined for all NCLXTC cells in a given row.

#### 2.4.12 Records: 416XXX, Initial Temperatures

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used).

W-1 (I) :	L	Row number in y-direction. The following data must specify NCLXTC temperatures for all cells in the y-row number L Acceptable range: $1 \le L \le NCLYTC$ . Default value: none.
W-2 (I) :	TCELTC (1,L)	Initial temperature in the cell (1,L), (x-row 1, y-row L), (-).Used only if INTTC=2 (see section 2.4.3).Acceptable range: $273.0 \le \text{TCELTC} \le 10,000.0$ . For an empty cell (IT00TC=0000) zero must be entered.Default value:none.
W-3 (I) :	TCELTC (2,L)	Initial temperature in the cell (2,L), ( <i>x</i> -row 2, <i>y</i> -row L), (-). Used only if INTTC=2 (see section 2.4.3).
W-4 (I) :	TCELTC (3,L)	Initial temperature in the cell (3,L), ( <i>x</i> -row 3, <i>y</i> -row L), (-). Used only if INTTC=2 (see section 2.4.3).

..., etc., until initial temperatures are defined for all NCLXTC cells in a given row.

#### 2.4.13 Records: 420XXX, Boundary Conditions

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . The 2-D Solid Heat Conductor reference numbers, XXX, need not be consecutive. The maximum number of 2-D Solid Heat Conductors is 20 (10 if the RT Package is used). The maximum number of boundary cells for each 2-D Solid Heat Conductor is 200.

W-1 (I) :	К	Row number in <i>x</i> -conditions for the b	direction. The data in this record defines boundary boundary cell (K, L), (x-row K, y-row L).
		Acceptable range:	$1 \leq K \leq$ NCLXTC. The cell (K, L) must be a
			boundary cell, i.e. it cannot be an empty cell
			(IT00TC=0000), or a filled cell (IT00TC=1111).
		Default value:	none.
W-2 (I) :	L	Row number in y-	direction. The data in this record defines boundary
		conditions for the b	boundary cell (K, L), (x-row K, y-row L).
		Acceptable range:	$1 \leq L \leq$ NCLYTC. The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell
			(IT00TC=0000), or a filled cell (IT00TC=1111).
		Default value:	none.
W-3 (I) :	IOXBTC	Indicator for heat the	ransfer in the x-direction (r in cylindrical geometry).
		= -1: heat transfer	in the <i>x</i> -direction not allowed.
		=+1: heat transfer	in the x-direction allowed.
		The use of IQXBT	C and IQYBTC (below) allows some flexibility in the
		definition of bound	ary conditions for the cells which have boundaries in

		both <i>x</i> and <i>y</i> directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32). <i>Acceptable range:</i> IQXBTC = $-1$ , or IQXBTC = $+1$ . <i>Default value:</i> $+1$ .
W-4 (I) :	IQYBTC	Indicator for heat transfer in the <i>y</i> -direction ( <i>z</i> in cylindrical geometry). = $-1$ : heat transfer in the <i>y</i> -direction not allowed. = $+1$ : heat transfer in the <i>y</i> -direction allowed. The use of IQYBTC and IQXBTC (above) allows some flexibility in the definition of boundary conditions for the cells which have boundaries in both <i>x</i> and <i>y</i> directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32). <i>Acceptable range:</i> IQYBTC = $-1$ , or IQYBTC = $+1$ . <i>Default value:</i> $+1$ .
W-5 (I) :	IVLBTC	Control Volume number for convective heat transfer. The value specifies the Control Volume, which is associated with the boundary cell (K, L), ( <i>x</i> -row K, <i>y</i> -row L). If zero is entered, then the boundary cell surface is either insulated, or the convective heat transfer coefficient and the fluid temperature are specified by Tabular or Control Functions (defined by words 6 and 7 below). If IVLBTC>0, then heat is transferred to/from the CV using the standard heat and mass transfer package (see Volume 1). It is also possible to overrule the use of the standard heat and mass transfer package, and use a Tabular or Control Function (defined by word 6 below) to determine the heat transfer coefficient. Also the fluid temperature can be altered by a Tabular or a Control Function, by using the Word 7 below. In such case the value obtained from the Tabular or Control Function will be taken with weighting factor of 0.5, and the true (Control Volume) fluid temperature will be taken with the weighting factor of 0.5. If the heat transfer coefficient or the fluid temperature are defined by Tabular or Control Functions, then only heat transfer will occur on the surface, mass transfer (boiling/condensation) will not be calculated. <i>Acceptable range:</i> must be a valid reference number of a Control Volume, if non-zero. <i>Default value:</i> 0.
W-6 (I) :	IHTBTC	<ul> <li>Pointer to a Tabular or Control Function defining the convective heat transfer coefficient (HTC) at the surface of the boundary cell (K, L), (<i>x</i>-row K, <i>y</i>-row L). If zero then the HTC is calculated by the code for the thermal-hydraulic conditions taken from the volume IVLBTC (Word 1). If the value is positive, the heat transfer coefficient will be defined by the Tabular Function IHTBTC. If it is negative, it will be defined by the Control Function   IHTBTC  . The units of the quantities obtained from the Tabular or Control Function are assumed to be (W/m²/K). If the obtained value is negative, it will be set to zero. If IHTBTC≠0 then the fluid temperature, needed to calculate the boundary heat flux, is taken as:</li> <li>if IVLBTC&gt;0 then the fluid temperature in Control Volume IVLBTC is used.</li> </ul>

 if ITPBTC≠0 then the fluid temperature is given by a Tabular or Control Function, defined by ITPBTC (word 4 below).

if IVLBTC=0 and ITPBTC=0 then the fluid temperature is set to 300 K.

Acceptable range: must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.

Default value:

W-7(I): **ITPBTC** Pointer to a Tabular or Control Function defining the fluid temperature at the boundary cell (K, L), (x-row K, y-row L). If the value is positive, the fluid temperature will be defined by the Tabular Function ITPBTC. If it is negative, it will be defined by the Control Function | ITPBTC |. The units of quantity obtained from the Tabular or Control Function are assumed to be (K). If the obtained value is negative, it will be set to zero. If ITPBTC≠0 and IVLBTC>0 (heat transfer to a Control Volume), then the value obtained from the Tabular or Control Function will be used with the weighting factor of FINTTC. The true fluid temperature (from Control Volume) will be used with the weighting factor of 1.0–FINTTC. Boiling and condensation models will be disabled by setting CSFBTC to -1.0 and ICNBTC to -4. In the past the input combination of IPTBTC≠0 and IVLBTC>0 was used to perform temperature averaging for heat exchangers. Currently it is not recommended to use this method. A more elaborate temperature averaging model has been developed, and is available through input records 425XXX (see section 2.4.14). Acceptable range: must be a valid reference number of a Tabular, or a

Control Function, if non-zero. 0.

Default value:

W-8 (I): **IORBTC** Indicator for non-convective heat flux at the boundary cell (K, L), (xrow K, y-row L). The heat flux defined by this pointer is used only on the uncovered part of the cell (above water level). With this pointer a user can model in a simple way radiative heat transfer. If the net enclosure thermal radiation model is used, and this cell surface is associated with one of the radiating surfaces (section 2.6.3), then this parameter must not be used. The meaning is as follows:

## IQRBTC>1000:

A simple radiation model between the cell (K, L) surface and atmosphere gas is used to determine the non-convective heat transfer. The grey gas model is used, the atmosphere is assumed to be opaque (the reason for assuming opaque atmosphere is discussed in Volume 3). The heat flux is equal to:

$$q = \varepsilon(T_w) \sigma \left(T_w^4 - T_g^4\right)$$

where  $\varepsilon(T_w)$  is the wall emissivity,  $\sigma$  is the Stefan-Boltzmann constant,  $T_w$ ,  $T_g$  are the wall and gas temperatures respectively. The emissivity is obtained from the Tabular Function number: (IQRBTC - 1000). The argument for the Tabular Function is the wall surface temperature, (K).

## 0<IORBTC<1000:

The heat flux is obtained from the Tabular Function number IORBTC. The units of the quantities obtained from the Tabular Function are

assumed to be: (W/m<sup>2</sup>). Positive heat flux means that the heat is emitted from the surface.

		IQRBTC<0:
W-9 (I) :	INCBTC	Configuration indicator for natural convection at the boundary cell (K, L), (x-row K, y-row L). The value is used only when IVLBTC is positive. The meaning of this variable is as follows: Rectangular geometry: 0 vertical wall, -1 horizontal wall facing down, +1 horizontal wall facing up. Cylindrical geometry: 0 vertical cylinder.
		<ul> <li>horizontal cylinder, inside,</li> <li>horizontal cylinder, inside,</li> <li>horizontal cylinder, outside.</li> </ul> Default values are provided for each geometrical configuration, based on cell surface orientation. If the cell has a boundary surface in both vertical and horizontal directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32), then a vertical surface is assumed. The default value can always be overridden by user's input. Acceptable range: -1, 0, +1. Default value: depending on the cell free surface orientation.
W-10 (R) :	DNCBTC	Characteristic dimension for natural convection at the boundary cell (K, L), ( <i>x</i> -row K, <i>y</i> -row L), (m). The value is used only when IVLBTC is positive and no alternative liquid is used. For the alternative liquid the forced convection correlation is selected by Word 24 (IHCBTC). <i>Acceptable range:</i> $0.0 < \text{DNCBTC} < 10^{10}$ . <i>Default value:</i> height, for rectangular geometry, inner or outer diameter for the cylindrical geometry cells.
W-11 (I) :	IFCBTC	<ul> <li>Configuration indicator for forced convection, as well as the nucleate boiling model and the model for critical heat flux calculation. The value is used only when IVLBTC is positive. The meaning of this variable is as follows:</li> <li>-1 internal flow, Chen correlation for nucleate boiling, Zuber and USSR Academy of Science models for critical heat flux calculations (Zuber for non-flow, USSR A. S. for flow conditions).</li> <li>+1 external flow, Rohsenow correlation for nucleate boiling, Zuber model for critical heat flux calculation.</li> <li>Acceptable range: -1, +1.</li> <li>Default value: -1.</li> </ul>
W-12 (R) :	DFCBTC	Characteristic dimension for forced convection at the boundary cell (K, L), ( <i>x</i> -row K, <i>y</i> -row L), (m). The value is used only when IVLBTC is

positive. Best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFCBTC should be equal to: for internal flow - hydraulic diameter; for external flow - width (rectangular wall). *Acceptable range:*  $0.0 < DFCBTC < 10^{10}$ .

Default value:

RECTANGULAR geometry (IGEOTC=1): *x*-coordinate total length, if cell has horizontal boundary surface, *y*-coordinate total length, if cell has vertical boundary surface (or vertical and horizontal).

CYLINDRICAL geometry (IGEOTC=2):

inner diameter  $(2.0 \times R0TC)$  for the inner cylindrical surfaces; outer diameter for the outer cylindrical surfaces as well as the flat surfaces.

W-13 (I): IFBBTC Configuration indicator for film boiling. The value is used only when IVLBTC is positive. The meaning of this variable is as follows:

- 0 vertical surface,
- $\pm 1$  horizontal cylinder,
- -1 horizontal plate, facing down,
- +1 horizontal plate, facing up.

Acceptable range:  $-1 \leq \text{IFBBTC} \leq +1$ .

*Default value:* depend on boundary surface orientation. If the cell has the boundary surface in both vertical and horizontal directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32), then the surface is interpreted as vertical.

W-14 (R): DFBBTC Characteristic dimension for film boiling, (m). The value is used only when IVLBTC is positive. A best estimate value is provided for each geometrical configuration. Thus the value need not be entered or may be entered as zero. The value of DFBBTC should be equal to: for vertical walls - height; for horizontal plates - width; for cylinders and spheres - diameter.

Acceptable range:  $0.0 < \text{DFCBTC} < 10^{10}$ .

*Default value:* height, for rectangular geometry, inner or outer diameter for the cylindrical geometry cells.

- W-15 (I): ICNBTC Configuration indicator for condensation. The value is used only when IVLBTC is positive. The meaning of this variable is as follows:
  - -4 condensation model disabled (the same for ICNBTC<-4)
  - -3 condensation on horizontal wall facing up,
  - -2 condensation on horizontal wall facing down,
  - -1 condensation inside horizontal tubes,
  - 0 condensation on vertical walls,
  - 1 condensation on outside surface of horizontal tube.
  - $\geq 2$  condensation on outside surface of horizontal tube bank. ICNBTC is equal to the number of vertical rows of tubes.

Acceptable range: all integers.

*Default value:* depends on the boundary surface orientation. If the cell has the boundary surface in both vertical and

horizontal directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32), then the surface is interpreted as vertical.

W-16 (R): DCNBTC Characteristic dimension for condensation, (m). The value is used only when IVLBTC is positive. The value of DCNBTC should be equal to: for vertical walls (or cylinders) - wall height; inside horizontal tubes - inner diameter; outside surface of horizontal tubes or tube banks - outer diameter; horizontal walls facing up - maximum film thickness (equilibrium thickness of water layer with free fall of liquid at the edges of the wall). The condensation type is defined by ICNBTC (word 15). In case of condensate flow through a stack of cells the characteristic dimension of the cell number k in the stack (counting from the top) should be defined as follows:

$$DCNBTC(k) = \left(\frac{z_{BOT}(k)^{5/4} - z_{TOP}(k)^{5/4}}{z_{BOT}(k) - z_{TOP}(k)}\right)^{4}$$

 $z_{BOT}(k)$ 

 $z_{TOP}(k)$ 

where:

distance from the bottom of the cell (K, L) to the top of the stack, (m), distance from the top of the cell (K, L) to the top of the stack, (m).

If the height of each cell in the stack is identical then the above formula reduces to:

DCNBTC (k) = 
$$\left(k^{5/4} - (k-1)^{5/4}\right)^4 \frac{H}{N}$$

where: H - total height of the wall, (m), N - number of cells in the stack.

The ratio: (*H/N*) is the height of a single conductor in the stack. Note that only for k=1 DCNBTC is equal to the physical height of the conductor, (*H/N*). For k>1 DCNBTC is greater than (*H/N*). For k=N DCNBTC is always greater than the total wall height, *H*.

Acceptable range: $0.0 < \text{DCNBTC} < 10^{10}$ .Default value:depends on boundary st

depends on boundary surface orientation. If the cell has the boundary surface in both vertical and horizontal directions (such as for example the quarter-cells, or the three-quarter-cells, shown in Figure 2-32), then the surface is interpreted as vertical.

W-17 (R): CSFBTC The constant  $C_{sf}$  in the Rohsenow equation for nucleate boiling (see Volume 1). The values of  $C_{sf}$  for different surfaces are given in table below. Entering a negative value will disable the full boiling model. Acceptable range: all reals. Default value: 0.013.

Table 2-17	Values	of	$C_{sf}$ for	Rohsenow	correlation.
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Surface type	$C_{sf}$	Surface type	$C_{sf}$
Nickel	0.0060	Platinum	0.0130
Ground and polished stainless steel	0.0080	Brass	0.0060
Teflon pitted stainless steel	0.0058	Polished copper	0.0128
Chemically etched stainless steel	0.0133	Lapped copper	0.0147
Mechanically polished stainless steel	0.0132	Scored copper	0.0068

W-18 (I) :	MCFBTC	Critical heat flux model selection. The value is used only when IVLBTC
		> 0

- 1 Zuber pool boiling correlation with Ivey-Morris correction for subcooling.
- 2 Combination of model based on USSR Academy of Sciences CHF look-up tables for high flow, with Zuber and Ivey-Morris for low flow.
- 3 Combination of Biasi correlation for high flow, with Zuber and Ivey-Morris for low flow.
- 4 Groeneveld (1986) look-up tables.
- <0 CHF is calculated by a user-defined Control Function with the number |MCFBTC|.

*Acceptable range:* 1, 2, 3 or reference to a Control Function *Default value:* 2.

W-19 (I): MNCBTC Selection of model for the influence of non-condensable gases for condensation. The value is used only when IVLBTC is positive and ICNBTC is greater than -2. The meaning of this variable is as follows:

- 1 Kuhn-Shrock-Petersen (KSP) correlations recommended for condensation on the inside surface of tubes,
- 2 Ogg correlations,
- 3 Modified Ogg correlations recommended for condensation on the outside surface of tubes, plates, etc.

*Acceptable range:* 1, 2, 3. *Default value:* 3.

W-20 (R): CFDBTC Indicator of condensate film drainage behavior.

If the value is <u>positive</u> then CFDBTC is the height of the cell. The elevation of the lowermost point of this surface is equal to the elevation of the cell center minus CFDBTC/2.0. The drainage from this surface is either deposited in the pool of a CV (if the lowest point of the surface is immersed in pool), or converted to droplets and suspended in the atmosphere of a CV as "rain" drops (if the lowest point of the surface is not immersed in the pool).

If the value is <u>negative</u> then the drainage is assumed to be deposited on a surface of another (lower) cell of the same 2-D Solid Conductor. The absolute value of CFDBTC must then be equal to the number of a boundary cell at the bottom of the stack. Note that the <u>boundary cell</u> <u>number must be used</u>. The cell numbers and boundary cell numbers are internally assigned by the program, and therefore the user must look-up the boundary cell number in the boundary cell numbering map, printed in the SPECTRA output of the TC data.

The use of the drainage parameter, CFDBTC, and the condensation characteristic dimension, DCNBTC, in case of individual and stacked conductors is illustrated in Figure 2-33 (see also Volume 3). The halfcell size all cells is assumed to be 0.05 m. The appropriate values of DCNBTC and CFDBTC are shown in Table 2-18.

Acceptable range: if CFDBTC<0.0 then the boundary cell No. CFDBTC must be connected to a Control Volume (not necessarily equal to IVLBTC), if CFDBTC>0.0 then the bottom elevation of the

left surface (center point elevation minus CFDBTC/2.0) must be within the boundary Control Volume.

- Default value: the default value is set to twice the distance between the center point of the left surface and the bottom of the boundary Control Volume. That value will result in deposition of condensate always in the pool. This is done to avoid numerical problems, and time step reduction, when condensate is converted into droplets.
- W-21 (I): **IHDBTC** Indicator of CV flow direction relative to the cell (K, L). Used only for rectangular geometry (IGEOTC=1). The meaning is: For vertical TC's (IVERTC=0):
  - CV horizontal flow is parallel, 0:
  - CV horizontal flow is perpendicular,  $v_{TC} = v_{CV,ver}$ . For horizontal SC's (IVERSC<>0):

```
v_{TC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2}
```

- 0: CV vertical flow is parallel,
- CV vertical flow is perpendicular, 1:
- For cylindrical geometry always:
- $v_{TC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2}$  $v_{TC} = v_{CV,ver}$ .  $v_{TC} = (v_{CV,ver}^2 + v_{CV,hor}^2)^{1/2},$

Acceptable range: 0, 1. Default value: 0.



1:

Figure 2-33 Condensation example cases (A) and (B). The half cell size is 0.05 m.

Table 2-18	Values of DCNBTC and CFDBTC for the example cases (A) and (B).
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Bnd.	Case (A)		Case (B)	
Cell	DCNBTC	CFDBTC	DCNBTC	CFDBTC
1	$((0.05^{5/4} - 0.00^{5/4})/(0.05 - 0.00))^4 = 0.050$	-0006	$((0.05^{5/4} - 0.00^{5/4})/(0.05 - 0.00))^4 = 0.050$	-0002
2	$((0.15^{5/4} - 0.05^{5/4})/(0.15 - 0.05))^4 = 0.236$	-0006	$((0.15^{5/4} - 0.05^{5/4})/(0.15 - 0.05))^4 = 0.236$	0.05
3	$((0.25^{5/4} - 0.15^{5/4})/(0.25 - 0.15))^4 = 0.484$	-0006	$((0.05^{5/4} - 0.00^{5/4})/(0.05 - 0.00))^4 = 0.050$	-0005
4	$((0.35^{5/4} - 0.25^{5/4})/(0.35 - 0.25))^4 = 0.730$	-0006	$((0.15^{5/4} - 0.05^{5/4})/(0.15 - 0.05))^4 = 0.236$	-0005
5	$((0.45^{5/4} - 0.35^{5/4})/(0.45 - 0.35))^4 = 0.975$	-0006	$((0.20^{5/4} - 0.15^{5/4})/(0.20 - 0.15))^4 = 0.426$	0.05
6	$((0.50^{5/4} - 0.45^{5/4})/(0.50 - 0.45))^4 = 1.159$	0.05	$((0.05^{5/4} - 0.00^{5/4})/(0.05 - 0.00))^4 = 0.050$	-0008
7	-	-	$((0.15^{5/4} - 0.05^{5/4})/(0.15 - 0.05))^4 = 0.236$	-0008
8	-	-	$((0.20^{5/4} - 0.15^{5/4})/(0.20 - 0.15))^4 = 0.426$	0.05

W-22 (I): THTBTC Contact angle,  $\theta$ , (degree). Used to determine the diameter of bubbles created during nucleate boiling:  $D = 0.0208 \cdot \theta \cdot (\sigma/g/(\rho_{liq}-\rho_{gas}))^{(1/2)}$ . Acceptable range:  $10^{\circ} \leq \text{THTBTC} \leq 180^{\circ}$ . Default value:  $96^{\circ}$ .

W-23 (R): XRBBTC Multiplier for convective heat transfer,  $X_{RB}$ .

XRBBTC<0.0: HTC is multiplied by |XRBBTC| in both natural and force convection. It may be used to obtain a conservative estimation of heat transfer.

XRBBTC>0.0: HTC is multiplied by XRBBTC only in case of turbulent forced convection (FC-TUR), internal flow (IFCBTC = -1). It is intended to allow the user to define a rod bundle multiplier in forced convection:

 $Nu_{tur} = X_{RB} \ 0.023 \ Re^{0.8} \ Pr^{0.4}$ 

Appropriate values for parallel flow and cross-flow may be found in literature. The ratio of pitch over diameter is a good approximation (see Volume 1, description of forced convection correlations):

$$X_{RR} = P / D$$

For tube arrangements other than equilateral triangle pitch, the multiplier is given by:

$$X_{RB} = \left(\frac{P_1 \cdot P_2}{D^2}\right)$$

Note that the rod bundle multiplier may be different for different fluids. For example, for the liquid metals the value may even show different tendency (see Volume 1, description of liquid metals correlations):

$$X_{RB} = 1 - \exp[-3.8 \cdot (P/D-1)]$$

Acceptable range: $0.0 \le |\text{XRBBTC}| \le 10^6$ Default value:XRBBHT<br/>(global activator, defined in the record 810020)

W-24 (I): IHCBTC Selection of heat transfer correlation for alternative fluid.

Acceptable range:	one of the correlations defined in records 843XXX
	or 843YYY
Default value:	rectangular: 1, cylindrical: 2.

#### 2.4.14 Records: 425XXX, Heat Exchanger Temperature Averaging

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records may be used to model a heat exchanger. If these records are used, then an averaging procedure will be applied to calculate the representative fluid temperature at the TC cell surface. The representative fluid temperature will be equal to the weighted average of the inlet and outlet fluid temperatures. Note that if the temperature averaging is not used, then the representative fluid temperature is always equal to the fluid temperature in the boundary volume, which means it is equal to the outlet temperature. As shown in Volume 3, when the temperature-averaging concept is not used, a large number of nodes (~100) may be required to obtain accurate results. With the temperature averaging the same accuracy may be obtained using only a few nodes. An example of the temperature averaging is shown below see Figure 2-34 and the corresponding discussion.

Inlet Junction Data:

W-1 (I) :	11	Boundary cell number. Using I1 and I2 (below) the user specifies the cell range for which the temperature averaging data defined in this record will be applied. The temperature averaging data will be applied for the boundary cells IBC: $I1 \le IBC \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. <i>Default value:</i> none.
W-2 (I) :	12	Boundary cell number. Using I2 and I1 (above) the user specifies the cell range for which the temperature averaging data defined in this record will be applied. The temperature averaging data will be applied for the boundary cells IBC: $I1 \le IBC \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. $I2 \ge I1$ . <i>Default value:</i> none.
W-3 (I) :	JTABTC (1)	Junction reference number of the inlet Junction on the "primary" side (the side of the heat exchanger adjacent to cells I1 - I2). <i>Acceptable range:</i> must be a Junction connected to the boundary Control Volume of all cells I1 - I2, if non-zero. <i>Default value:</i> none.
W-4 (R) :	WTABTC (1)	Limiting mass flow in the inlet Junction JTABTC(1) for full temperature averaging ( $W_{TA,L}$ in Figure 2-16 (a)). Applied when there is a flow through JTABTC(1) into IVLBTC and there is no flow through KTABTC(1) - <u>normal flow direction on both primary and secondary</u> <u>side</u> . The temperature of the fluid entering through the Junction JTABTC(1) will be used with maximum weighting factor if the mass flow at the Junction is larger than WTABTC(1) ( $W_{JN} >$ WTABTC(1)). Generally speaking, WTABTC(1) is a flow for which the temperature distribution in the boundary Control Volume is approximately linear, provided that there is flow in through JTABTC(1) and there is no flow

		in through KTAB' nominal flow throu Acceptable range: Default value:	TC(1). Roughly, this number can be viewed as a gh the heat exchanger. $10^{-10} < WTABTC(1) < 10^{10}$ . none.
W-5 (I) :	KTABTC (1)	Junction reference side (the side adjac Acceptable range:	number of the outlet Junction on the "secondary" ent to cell LTABTC(1)). must be a Junction connected to the boundary Control Volume of the cell LTABTC(1), if non- zero.
		Default value:	none.
W-6 (R) :	XTABTC (1)	Limiting mass flow averaging ( $X_{TA,L}$ in	w in the Junction KTABTC(1) for full temperature Figure 2-16 (c) ). Applied when there is flow through the CV adjacent to cells I1 - I2 and simultaneously the KTABTC(1) into the CV adjacent to LTABTC(1) ction on the primary side, reversed secondary side ature of the fluid entering through the Junction be used with maximum weighting factor if the mass in is larger than XTABTC(1) ( $W_{JN} > XTABTC(1)$ ). KTABTC(1) and XTABTC(1) allow the user to ng weighting factors when flow conditions in the heat , for example when a counter-current flow becomes ly the temperature averaging is needed in counter- hile it is not needed in co-flow conditions. This can thing XTABTC(1) to a large number (for example Generally speaking, XTABTC(1) is a flow for which listribution in the boundary Control Volume is ar, provided that there is flow in through JTABTC(1) $10^{-10} < XTABTC(1) < 10^{10}$ . none.
W-7 (I) :	LTABTC (1)	Reference boundar Acceptable range: Default value:	y cell number for the "secondary" side. must be an existing boundary cell number. none.
		Outlet Junction Da	ta:
W-8 (I) :	JTABTC (2)	Junction reference (the side of the hea <i>Acceptable range:</i>	number of the outlet Junction on the "primary" side t exchanger adjacent to cells I1 - I2). must be a Junction connected to the boundary Control Volume of all cells I1 - I2, if non-zero.
		Default value:	none.
W-9 (R) :	WTABTC (2)	Limiting mass flow ture averaging ( <i>W</i> <sub>7</sub> through JTABTC(2 no flow through <u>reversed flow on th</u> The temperature of will be used with	<i>v</i> in the outlet Junction JTABTC(2) for full tempera- AL in Figure 2-16 (b) ). Applied when there is flow (2) into the CV adjacent to the cells I1 - I2 and there is KTABTC(2) into CV adjacent to LTABTC(2) - the primary side, normal flow on the secondary side. The fluid entering through the Junction JTABTC(2) maximum weighting factor if the mass flow at the

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		Junction is larger than WTABTC(2) ( $W_{JN} >$ WTABTC(2) ). Generally speaking, WTABTC(2) is a flow for which the temperature distribution in the boundary Control Volume is approximately linear, provided that there is flow in through JTABTC(2) and no flow in through KTABTC(2). <i>Acceptable range:</i> $10^{-10} <$ WTABTC(2) $< 10^{10}$ . <i>Default value:</i> none.
W-10 (I) :	KTABTC (2)	Junction reference number of the outlet Junction on the "secondary"side.Acceptable range:must be a Junction connected to the boundary Control Volume of the cell LTABTC(1), if non- zero.Default value:none.
W-11 (R) :	XTABTC (2)	Limiting mass flow in the outlet Junction KTABTC(2) for full temperature averaging ( $X_{TA,L}$ in Figure 2-16 (d) ). Applied when there is in-flow through JTABTC(2) and simultaneously there is in-flow through KTABTC(2) - reversed flow on both primary and secondary side. The temperature of the fluid entering through the Junction JTABTC(2) will be used with maximum weighting factor if the mass flow at the Junction is larger than XTABTC(2) ( $W_{JN} > XTABTC(2)$ ). The input entries KTABTC(2) and XTABTC(2) allow the user to change the averaging weighting factors when flow conditions in the heat exchangers change, for example when a counter-current flow becomes co-current. Typically the temperature averaging is needed in counter-flow conditions, while it is not needed in co-flow conditions. This can be achieved by setting XTABTC(2) to a large number (for example XTABTC(2)=10 <sup>6</sup> ). Generally speaking, XTABTC(2) is a flow for which the temperature distribution in the boundary Control Volume is approximately linear, provided that there is flow in through JTABTC(2) and KTABTC(2). <i>Acceptable range:</i> 10 <sup>-10</sup> < XTABTC(2) < 10 <sup>10</sup> . <i>Default value:</i> none.

The concept of the temperature averaging is essentially the same as in case of 1-D Solid Heat Conductors, and can be visualized using the Figure 2-16. The only modification being the SC-01 replaced by TC-01. The 2-D model may be needed to take into account shape changes in the direction perpendicular to the flow, for example a finned wall shown in Figure 2-34.

The example shown here is very similar to the 1-D example. The nominal flow is again 100.0 kg/s on both left and right side; the temperature averaging in the co-current flow is avoided by using a large number (10<sup>6</sup>). The input deck for TC-01 (Figure 2-34) is shown below.

*			II	NLET JUN	CTION					OUTLET	JUNCTIO	N		
*	I1	I2	JTABTC	WTABTC	KTABTC	XTABTC	LTABTC	JTABTC	WTABTC	KTABTC	XTABTC	LTABTC		
425001	1	1	011	100.0	022	1.0E+6	10	012	1.0E+6	022	100.0	10	*	Primary
425001	3	3	011	100.0	022	1.0E+6	10	012	1.0E+6	022	100.0	10	*	Primary
425001	5	5	011	100.0	022	1.0E+6	10	012	1.0E+6	022	100.0	10	*	Primary
425001	7	7	011	100.0	022	1.0E+6	10	012	1.0E+6	022	100.0	10	*	Primary
425001	9	9	011	100.0	022	1.0E+6	10	012	1.0E+6	022	100.0	10	*	Primary
*														

425001	2	2	021	100.0	012	1.0E+6	1	022	1.0E+6	012	100.0	1	* Secondary
425001	4	4	021	100.0	012	1.0E+6	1	022	1.0E+6	012	100.0	1	* Secondary
425001	6	6	021	100.0	012	1.0E+6	1	022	1.0E+6	012	100.0	1	* Secondary
425001	8	8	021	100.0	012	1.0E+6	1	022	1.0E+6	012	100.0	1	* Secondary
425001	10	10	021	100.0	012	1.0E+6	1	022	1.0E+6	012	100.0	1	* Secondary

Compared to the 1-D heat conductors, the extra input includes cell identifiers I1, I2, and the "other side" cell identifier, LTABTC.

Using the cell identifiers I1, I2 one can specify a cell range and therefore limit the amount of input. In the present example it is impossible to take advantage of that because no consecutive cells can be found transferring heat to the same Control Volume. Therefore the input above consists of five lines for each heat exchanger side. If the cells were numbered differently (by horizontal rows rather than vertical) only two lines would be needed, first with I1=1, I2=5, specifying data for the primary side (CV-10), and second with I1=6, I2=10, specifying data for the secondary side (CV-20). The user however, cannot affect the cell numbering. The cells are numbered internally by the SPECTRA code. The code optimizes the numbering scheme in order to minimize the computational effort, i.e. to minimize the size of the band diagonal matrix that needs to be solved for a 2-D Solid Heat Conductor (see Volume 1). In the case shown in Figure 2-34 the band size is smaller (2) when cells are numbered vertically, than it would be (5) if the cells were numbered horizontally.

In the present example cell 10 is used arbitrarily as the secondary side identifier. This choice is arbitrary; it could be any of the cells facing CV-20 (cells 2, 4, 6, 8). For the primary side identifier the cell 1 is used; again it could be any of the cells facing CV-10 (3, 5, 7, 9).

Note that the limiting flow for T-A is affected by the multipliers CMN1TC, CMN2TC, defined in record 460XXX (section 2.4.18). Generally one should make sure that the limiting flows,  $W_{TA}$ , approximately fulfil the relation:

$$\left(W_{TA}c_{p}\right)_{primary} \approx \left(W_{TA}c_{p}\right)_{secondary}$$

The multipliers will then assure proper temperature averaging in case the flow on the primary side becomes very different from the flow on the secondary side.



Figure 2-34 Temperature averaging for a 2-D Solid Heat Conductor.

#### 2.4.15 Records: 450XXX, Boundary Fluid Temperature Calculation

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record describes the boundary fluid temperature calculation in case of intensive boiling. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (I) :	K	Row number in <i>x</i> - conditions for the b <i>Acceptable range:</i>	direction. The data in this record defines boundary boundary cell (K, L), (x-row K, y-row L). $1 \le K \le NCLXTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000) or a filled cell (IT00TC=1111)
		Default value:	none.
W-2 (I) :	L	Row number in <i>y</i> - conditions for the b <i>Acceptable range:</i> <i>Default value:</i>	direction. The data in this record defines boundary boundary cell (K, L), (x-row K, y-row L). $1 \le L \le NCLYTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000), or a filled cell (IT00TC=1111). none.
W-3 (I) ·	IBPTTC	Indicator for boun	dary fluid temperature calculation for pool-bubble

W-3 (I): IBPITC Indicator for boundary fluid temperature calculation for pool-bubble flow. Typically the pool temperature is used as boundary fluid temperature for Solid Heat Conductors. In case of intensive boiling the program assumes that bubbles rise up in a plume of relatively warm water (see Volume 1). The water temperature in this plume is equal to the local saturation temperature, and is therefore higher than the pool average temperature, which is no higher than the saturation temperature at the pool surface pressure. The indicator IBPTTC defines how the program should determine whether the TC surface will be exposed to the warm plume or to the relatively cold pool outside the plume. Three factors may be used by the program: the void fraction factor,  $f_a$ , the temperature factor,  $f_T$ , and the submergence factor,  $f_z$ . Those factors are defined as follows:

a) The void fraction factor,  $f_{\alpha}$ :

 $f_{\alpha} = \begin{cases} 0.0 & \text{if} \quad \alpha \leq \alpha_1 \\ (3 - 2X)X^2 & \text{if} \quad \alpha_1 < \alpha < \alpha_2 \\ 1.0 & \text{if} \quad \alpha \geq \alpha_2 \end{cases}$ 

where  $\alpha$  is the average void fraction in the pool, *X* is the interpolation factor, equal to:  $X = (\alpha - \alpha_1)/(\alpha_2 - \alpha_1)$ , and the boundary values of void fractions,  $\alpha_1$ ,  $\alpha_2$ , are defined below (words 2 and 3). Note that the cubic interpolation is used, which ensures continuity of the function as well as its first derivative.

b) The surface temperature factor,  $f_T$ :

$$f_{T} = \begin{cases} 0.0 & if & T_{TC} \leq T_{int} + \Delta T_{1} \\ (3 - 2X)X^{2} & if & T_{int} + \Delta T_{1} < T_{TC} < T_{int} + \Delta T_{2} \\ 1.0 & if & T_{TC} \geq T_{int} + \Delta T_{2} \end{cases}$$

where  $T_{TC}$  is the surface temperature of the Solid Heat Conductor,  $T_{int}$  is the liquid temperature at the pool-bubble interphase, X is the interpolation factor, equal to:  $X = (T_{TC} - (T_{int} + \Delta T_1))/((T_{int} + \Delta T_2) - (T_{int} + \Delta T_1)),$ 

and the boundary values of  $\Delta T$  are defined below (words 4 and 5).

c) The surface submergence factor, *f<sub>Z</sub>*:

$$f_{T} = \begin{cases} (3 - 2X_{1})X_{1}^{2} & \text{if} & 0 \le Z < Z_{bubb} \\ 1.0 & \text{if} & Z_{bubb} \le Z \le Z_{bubb}Z_{m1} \\ (3 - 2X_{2})X_{2}^{2} & \text{if} & Z_{bubb}Z_{m1} < Z < Z_{bubb}Z_{m2} \\ 0.0 & \text{if} & Z_{bubb}Z_{m2} \le Z \end{cases}$$

where Z is the TC submergence (equal to the distance between the pool surface and the elevation of the middle point of this part of the TC which is covered by water),  $Z_{bub}$  is the submergence of average bubble,  $X_1$  and  $X_2$  are the interpolation factors, equal to:

$$X_1 = Z/Z_{bu}$$

 $X_2 = (Z - Z_{bub} \cdot Z_{m2})/(Z_{bub} \cdot Z_{m1} - Z_{bub} \cdot Z_2).$ 

Values of the multipliers,  $Z_{m1}$  and  $Z_{m2}$ , are defined below (words 6, 7).

The parameter IBPTTC defines which of the factors described above should be used. The interpretation is as follows:

IBPTTC = -1: No factors are used. When surface is exposed to a boiling pool, the boundary fluid temperature is always equal to the pool temperature,  $T_{pool}$  (approximately equal to the saturation temperature for the pressure at the pool surface).

$$T_{fluid} = T_{pool}$$

IBPTTC = 1 : Only the void fraction factor is taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot f_{\alpha}$$

where  $T_{pool}$  is the pool average temperature, and  $T_{int}$  is the liquid temperature at the pool-bubble interphase (thus the warm plume temperature, approximately equal to the saturation temperature for the pressure at the elevation of average bubble).

IBPTTC = 2: The void fraction factor and the temperature factor are taken into account. The boundary fluid temperature is calculated as:

$$T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_T)$$

IBPTTC = 3: The void fraction factor and the submergence factor are taken into account. The boundary fluid temperature is calculated as:

 $T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_{z})$ 

IBPTTC = 4 : All factors are taken into account. The boundary fluid temperature is calculated as:

 $T_{fluid} = T_{pool} + (T_{int} - T_{pool}) \cdot (f_{\alpha} f_T f_Z)$ 

Acceptable range:  $-1 \leq \text{IBPTTC} \leq +4$ . Default value: +4. If IWATCV>0 (see section 2.1.31) then the default value is -1.

W-4 (R): ALP1TC Upper limit of void fraction to use only the pool temperature as the boundary fluid temperature for the TC surface,  $\alpha_1$ , (-). Used if IBPTTC (word 1 above) is positive. If the average void fraction in the pool is below  $\alpha_1$  then the Solid Heat Conductor surface is not exposed to the warm plume.

 $\begin{array}{ll} \mbox{Acceptable range:} & 10^{-5} \leq \mbox{ALP1TC} \leq 0.1 \ . \\ \mbox{Default value:} & 10^{-3} \ . \end{array}$ 

- W-5 (R) :ALP2TCLower limit of void fraction to use the warm plume temperature as the<br/>boundary fluid temperature for the TC surface,  $\alpha_2$ , (-). Used if IBPTTC<br/>(word 1 above) is positive. If the average void fraction in the pool is<br/>above  $\alpha_2$  then the Solid Heat Conductor surface can be exposed to the<br/>warm plume (depending on other conditions if they are applied).<br/>Acceptable range: 2.0·ALP1TC  $\leq$  ALP2TC  $\leq$  0.5 .<br/>Default value: 0.05 .
- W-6 (R): TSC1TC Upper limit of TC surface superheat to use only the pool temperature as the boundary fluid temperature for the TC surface,  $\Delta T_1$ , (K). Used if IBPTTC (word 1 above) is equal to 2 or 4. If the TC surface temperature is lower than the liquid temperature at the pool-bubble interphase (warm plume temperature) plus TSC1TC, then the Solid Heat Conductor surface is not exposed to the warm plume. *Acceptable range:* 0.1  $\leq$  TSC1TC  $\leq$  10.0. *Default value:* 1.0.
- W-7 (R): TSC2TC Lower limit of TC surface superheat to use the warm plume temperature as boundary fluid temperature for the TC surface,  $\Delta T_2$ , (K). Used if IBPTTC (word 1 above) is equal to 2 or 4. If the TC surface temperature is higher than the liquid temperature at the pool-bubble interphase (warm plume temperature) plus TSC2TC, then the Solid Heat Conductor surface can be exposed to the warm plume (depending on other conditions if they are applied). *Acceptable range:* 2.0·TSC1TC  $\leq$  TSC2TC  $\leq$  30.0. *Default value:* 3.0.

- $\begin{array}{lll} W-8 \ (R): & ZSC1TC & Lower multiplier on bubble submergence to use the warm plume temperature as the boundary fluid temperature for the TC surface, Z_{m1}, (-). Used if IBPTTC (word 1 above) is equal to 3 or 4. If the TC surface submergence is smaller than the average bubble submergence multiplied by ZSC1TC then the Solid Heat Conductor surface can be exposed to the warm plume (depending on other conditions if they are applied).$  $Acceptable range: 1.0 \leq ZSC1TC \leq 10.0$ . Default value: 2.0.
- W-9 (R):ZSC2TCUpper multiplier on bubble submergence to use only the pool<br/>temperature as the boundary fluid temperature for the TC surface,  $Z_{m2}$ ,<br/>(-). Used if IBPTTC (word 1 above) is equal to 3 or 4. If the TC surface<br/>submergence is larger than the average bubble submergence multiplied<br/>by ZSC2TC then the Solid Heat Conductor surface is not exposed to the<br/>warm plume.<br/>
  <hr/>
  Acceptable range: 1.2·ZSC1TC  $\leq$  ZSC2TC  $\leq$  15.0.
  Default value:

#### 2.4.16 Records: 451XXX, Boundary Fluid Velocity Multiplier

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record is optional. The velocity multiplier may be used for to account for own movement of structures, such as for example rotor blades. In such case the relative velocity surface-to-gas velocity is different than the gas velocity in a Control Volume. The user may take into account that difference using a Control Function that depends on the rotational speed, etc.

W-1 (I): VLMBTC Velocity multiplier,  $C_{\nu}$ , for the boundary surface velocity calculation. If a positive value is entered, the velocity multiplier is constant, and equal to this value. If a negative value is entered, the velocity multiplier is obtained from the Control Function equal to |VLMBTC|. An absolute value of the number obtained from the Control Function is used. Furthermore the value is limited to a maximum of  $10^{10}$ .

The fluid velocity at the TC boundary surface is obtained from:

If IHDBTC=0 (Word 21, record 420XXX):

$$v_{TC} = C_v \cdot \sqrt{v_{CV,hor}^2 + v_{CV,ver}^2}$$

If IHDBTC=1, IVERSC=0 (vertical TC, Word 5, record 400XXX):

$$v_{SC} = C_v \cdot v_{CV,ver}$$

If IHDBTC=1, IVERTC≠0 (horizontal TC, Word 5, record 300XXX):

 $v_{SC} = C_v \cdot v_{CV,hor}$ 

Acceptable range:  $0.0 \le \text{VLMLSC} \le 10^{10}$ 

or reference to a Control Function.Default value:1.0

#### 2.4.17 Records: 452XXX, Limit for Simultaneous Transfer to Pool and Atmosphere

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	К	Row number in <i>x</i> -direction. The data in this record defines boundary conditions for the boundary cell (K, L), ( <i>x</i> -row K, <i>y</i> -row L).				
		Acceptable range:	$1 \le K \le NCLXTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000) or a filled cell (IT00TC=1111)			
		Default value:	(11001C=0000), of a fined cen (11001C=1111). none.			
W-2 (I) :	L	Row number in y- conditions for the b Acceptable range:	direction. The data in this record defines boundary boundary cell (K, L), (x-row K, y-row L). $1 \le L \le NCLYTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000), or a filled cell (IT00TC=1111).			
		Default value:	none.			
W-3 (R) :	PMXBTC	Critical (maximum pool to allow simu value is given, sin always possible. Th To eliminate it, the situation when the p input parameter is interpolation zone pool fraction is bel performed in the ra <i>Acceptable range:</i> <i>Default value</i> :	a) fraction of the boundary surface area covered by ltaneous heat transfer to pool and atmosphere. If no nultaneous heat transfer to pool and atmosphere is his may lead to too large condensation in some cases. User may restrict the simultaneous heat transfer to a pool-covered fraction is smaller than PMXBTC. This is similar to CPFPL in the MELCOR code. An is defined. The full transfer to gas occurs when the ow 0.9 of the critical value, a linear interpolation is nge between 0.9 and 1.0 times the critical value. $0.0 \le PMXBTC \le 1.0$ 0.0			

As example of such situation is discussed in Volume 1. As a reference case, a fine nodalization is used (Figure 2-17, left). Coarse nodalization and consequent too slow heat up due to artificial heat transfer from atmosphere to pool through the solid structure is shown in Figure 2-17, middle. This is prevented by using the critical pool fraction of 0.01 (Figure 2-17, right). The heat transfer from atmosphere to pool is practically eliminated. However, a direct heat transfer still exists at the pool-atmosphere interphase. Therefore it is advisable to eliminate the pool-atmosphere heat transfer at the same time (input record 164XXX). This was done in the considered example.

#### 2.4.18 Records: 460000, Global Data: Film Boiling, Slip Ratio, TA, Oxidation

Parameters defined in this record are applied for all 2-D Solid Heat Conductors.

W-1 (R): AMFBTC First coefficient in the Simon Minimum Film Boiling correlation,  $A_{MFB}$ , (-). SPECTRA selects correlation that gives maximum value of the  $T_{MFB}$ ,

therefore the Simon correlation may be deactivated by setting AMFBTCand BMFBTC to small values.Acceptable range: $0.0 < AMFBTC \le 1.0$ Default value:0.13.

- W-2 (R): BMFBTC Second coefficient in the Simon Minimum Film Boiling correlation,  $B_{MFB}$ , (-).SPECTRA selects correlation that gives maximum value of the  $T_{MFB}$ , therefore the Simon correlation may be deactivated by setting AMFBTC and BMFBTC to small values. Acceptable range: 0.0 < BMFBTC  $\leq$  2.0 Default value: 0.86.
- W-3 (R) :CMFBTCCoefficient in the Berenson Minimum Film Boiling correlation,  $C_{MFB}$ , (-).). SPECTRA selects correlation that gives maximum value of the  $T_{MFB}$ ,<br/>therefore the Berenson correlation may be deactivated by setting<br/>CMFBTC to a small value.<br/>Acceptable range:  $0.0 < \text{CMFBTC} \le 1.0$ <br/>Default value: 0.127
- W-4 (R): TFMNTC Minimum value of the Minimum Film Boiling (MFB) temperature minus the Critical Heat Flux (CHF) temperature:  $(T_{MFB} T_{CHF})$ , (K). The MFB temperature, calculated from the Simon correlation is limited by this word so that it will never be lower than  $T_{CHF}$  + TFMNTC. Acceptable range:  $5.0 \le$  TFMNTC  $\le$  1000.0 Default value: 5.0.
- W-5 (R) : TFMXTC Maximum value of the Minimum Film Boiling (MFB) temperature minus the Critical Heat Flux (CHF) temperature:  $(T_{MFB} - T_{CHF})$ , (K). The MFB temperature, calculated from the Simon correlation is limited by this word so that it will never be higher than  $T_{CHF}$  + TFMXTC. *Acceptable range:* TFMNTC  $\leq$  TFMXTC  $\leq$  1000.0 *Default value:* 1000.0.
- W-6 (R): XTRBTC Coefficient in the Kalinin Transition Boiling correlation,  $X_{TB}$ , (-). Acceptable range:  $0.5 < \text{XTRBTC} \le 20.0$ Default value: 7.0.
- W-7 (R): ASFBTC Correction for subcooling in the film boiling correlation,  $A_{SFB}$ , (-). In case of a subcooled film boiling, the total heat flux is calculated from:

$$q = q_{FB} + A_{SFB} \cdot h_{conv} \cdot \left(T_{sat} - T_{fluid}\right)$$

where  $q_{FB}$  is the saturated film boiling heat flux and  $h_{conv}$  is the convective heat transfer coefficient, calculated for the bulk liquid temperature,  $T_{fluid}$ .

Acceptable range:  $0.0 \le \text{ASFBTC} \le 2.0$ 

*Default value:* 1.0 (based on comparison with results obtained using RELAP5/MOD3.3).

- W-8 (R): SMAXTC Maximum value of the slip ratio, ( $v_{bubb} / v_{pool}$ ), (-). Used for CHF calculations. The slip ratio which is used in the CHF correlation is equal to the minimum of  $v_{bubb} / v_{pool}$  and SMAXTC. Acceptable range:  $1.0 \le$  SMAXTC  $\le 1000.0$ Default value: 100.0.
- W-9 (R): CMN1TC Multiplier for the first (counter-current) Temperature Averaging (T-A) mode. The nominal flows for the T-A on both primary and secondary side of a heat exchanger are entered in the records 425XXX. If the flows exceed the nominal flows, full T-A is performed. If flows are decreased then also the T-A is decreased see section 2.4.14. This treatment is approximately correct if flow changes only on one side of the heat exchanger. If the flow changes simultaneously on both sides of the heat exchanger, then T-A should be used for flows much smaller than nominal. This multiplier defines how much the limiting flow (typically taken as the nominal flow) can be decreased when the flow on the other side of a heat exchanger decreases.

The default value of 0.01 means that in nominal counter-flow conditions full T-A will be performed if the flows decrease down to 1% of the nominal flow, provided that they will decrease simultaneously on both sides of the heat exchanger.

Generally the limiting flow on a given side of a heat exchanger is equal to:

$$W_{TA} = Min\left[\frac{W_{TA}}{C_{MN1}}, Max\left(W_{TA}C_{MN1}, W_{TA}\frac{W_{otherside}}{W_{TA, otherside}}\right)\right]$$

where  $W_L$  is the limiting flow for full T-A,  $C_{MNI}$  is the factor CMN1TC,  $W_{L, other side}$  is the limiting flow for full T-A on the other side, and  $W_{other side}$  is the current flow on the other side. Note that with this definition, the limiting flow for T-A can be either decreased or increased, and the actual value will always be within the range:

$$W_{TA}C_{MN1} \le W_{TA} \le \frac{W_{TA}}{C_{MN1}}$$

The limiting flow will be small when the other side flow is small, and large when the other side flow is large. This is the most appropriate treatment of a heat exchanger, provided that the limiting flows, defined in records 425XXX for both primary and secondary side, fulfil approximately the relation:

$$(W_{TA}c_p)_{primary} \approx (W_{TA}c_p)_{secondary}$$

Acceptable range: $0.001 \le \text{CMN1TC} \le 1.0$ Default value:0.01.

W-10 (R): CMN2TC Multiplier for the second (co-current) Temperature Averaging (T-A) mode. Works the same as CMN1TC, but in case when the flow is co-current. Default value means that CMN2TC is not used in co-flow

conditions. It is recommended to disable T-A in co-flow by setting the limiting flow to a large value - see section 2.4.14. In such case the value of CMN2TC is not very important. For consistency it should be equal to 1.0 when T-A is disabled. Acceptable range:  $0.001 \le \text{CMN2TC} \le 1.0$ 

*Default value:* 1.0.

W-11 (R): VGLMTC Gas velocity limit,  $v_{g,lm}$  (m/s), to switch off the Temperature Averaging (T-A). Numerical problems may be encountered when T-A is used in case of low velocities and changes of flow direction. To avoid this problems the T-A is turned off when the velocity is smaller than the limit defined by this word. An interpolation zone is defined for gas velocities between VGLMTC and 2×VGLMTC.

$$X_{TA,eff} = \begin{cases} X_{TA} & \text{if } v_g > 2v_{g,lm} \\ X_{TA} \cdot (v_g - v_{g,lm}) / v_{g,lm} & \text{if } v_{g,lm} < v_g < 2v_{g,lm} \\ 0.0 & \text{if } v_g < v_{g,lm} \end{cases}$$

where  $X_{TA}$  is the Temperature Averaging factor for full T-A,  $X_{TA.eff}$  is the effective T-A factor,  $v_g$  is the gas velocity and  $v_{g.lm}$  is the limiting gas velocity, VGLMTC.

Acceptable range: $0.001 \le \text{VGLMTC} \le 100.0$ Default value:1.0

W-12 (R): VLLMTC Liquid velocity limit,  $v_{l,lm}$  (m/s), to switch off the Temperature Averaging (T-A). Numerical problems may be encountered when T-A is used in case of low velocities and changes of flow direction. To avoid this problems the T-A is turned off when the velocity is smaller than the limit defined by this word. An interpolation zone is defined for liquid velocities between VLLMTC and 2×VLLMTC.

$$X_{TA,eff} = \begin{cases} X_{TA} & \text{if } v_l > 2v_{l,lm} \\ X_{TA} \cdot (v_l - v_{l,lm}) / v_{l,lm} & \text{if } v_{l,lm} < v_l < 2v_{l,lm} \\ 0.0 & \text{if } v_l < v_{l,lm} \end{cases}$$

where  $X_{TA}$  is the Temperature Averaging factor for full T-A,  $X_{TA,eff}$  is the effective T-A factor,  $v_l$  is the liquid velocity and  $v_{l,lm}$  is the limiting liquid velocity, VLLMTC. Acceptable range:  $0.001 \le \text{VLLMTC} \le 100.0$ 

*Default value:* 0.1

- W-13 (I): IOXNTC Option for oxidation on surfaces not connected to Control Volumes.
  =1: oxidation is calculated on TC surfaces not connected to a CV. It will be assumed that all oxidizing gases are always available at the surface.
  =2: oxidation is disabled on TC surfaces not connected to a CV. Acceptable range: 1, 2 Default value: none
- W-14 (I): ISEQTC Indicator for multiple oxidation reactions.
   =1: all oxidation reactions proceed simultaneously.
   =2: dominant reactions: oxidation reactions proceed in sequence, defined in records 480XXX. If there is enough oxidant (gas fraction >

		XLIMTC) for the first reaction, only this reaction occurs. If not, second reaction starts, then third, etc. This option is available because, according to [52], reaction with oxygen dominates over reactions with steam and nitrogen. Acceptable range: 1, 2 Default value: 1
W-15 (R) :	XLIMTC	Limit for dominant reactions. The default oxidation starvation limits are: $C1OX = 1.0 \times 10^{-4}$ : full strength oxidation $C0OX = C1OX / 10.0 = 1.0 \times 10^{-5}$ : no oxidation The default value of XLIMTC was selected approximately in the middle of the interpolation zone, when the dominant reaction strength is reduced roughly by half. <i>Acceptable range:</i> $1.0 \times 10^{-7} \le XLIMTC \le 1.0 \times 10^{-2}$ <i>Default value:</i> XLIMTC = C1OX / 2.0
W-16 (I) :	IMPGTC	<ul> <li>Implicit/explicit use of gas concentration for oxidation calculations.</li> <li>= 1: implicit (end of time step value is used).</li> <li>= 2: explicit (beginning of time step value is used).</li> <li>Acceptable range: 1 or 2</li> <li>Default value: 1</li> </ul>
W17 - (I)	IAVETC	Method used to calculate average TC temperature. In the SPECTRA output and plot files, the average temperatures are given next to the cell temperatures. This entry defines how the average temperature is obtained. = 1: volume average: $\overline{T} = \sum_{i} V_i \cdot T_i / \sum_{i} V_i$ = 2: mass-average: $\overline{T} = \sum_{i} M_i \cdot T_i / \sum_{i} M_i$ Here $M_i$ , $V_i$ , $T_i$ are the mass, volume and temperature of the cell <i>i</i> . <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 2
W-18 (I) :	IQPLTC	Power versus power density as plot parameters - Table 2-26. = 1: Power (W) is used as plot parameters: TC-XXX-Qcel-YYYY = 2: Power density (W/m <sup>3</sup> ) is used: TC-XXX-qcel-YYYY <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 1
2.4.19 Record	ds: 465000,	Hydraulic Diameter - TC Versus CV
W-1 (I):	IDHDTC	Option to check consistency between the CV hydraulic diameter

W-1 (I): IDHDTC Option to check consistency between the CV hydraulic diameter (DHYDCV) and the TC hydraulic diameter (DFCBTC). = 1: consistency is not required. If DFCBTC  $\neq$  DHYDCV, then a warning message is issued. = 2: consistency is required. If DFCBTC  $\neq$  DHYDCV, then an error message is issued. Acceptable range: 1, 2

#### Default value: 1

## 2.4.20 Records: 480XXX, Boundary Cell Oxidation Data

XXX is the Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records activate the oxidation model on the boundary cell of a 2-D Solid Heat Conductor. Each surface can have several different oxidation reactions associated with it, for example: a Zircaloy cladding may be oxidized by steam, Zr+H<sub>2</sub>O, and oxygen, Zr+O<sub>2</sub>. Maximum number of oxidation reactions is 5.

W-1 (I) :	К	Row number in <i>x</i> -parameters for the <i>Acceptable range</i> : <i>Default value</i> :	direction. The data in this record defines oxidation boundary cell (K, L), (x-row K, y-row L). $1 \le K \le NCLXTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000), or a filled cell (IT00TC=1111). none.
W-2 (I) :	L	Row number in y- parameters for the Acceptable range: Default value:	direction. The data in this record defines oxidation boundary cell (K, L), (x-row K, y-row L). $1 \le L \le NCLYTC$ . The cell (K, L) must be a boundary cell, i.e. it cannot be an empty cell (IT00TC=0000), or a filled cell (IT00TC=1111). none.
W-3 (R) :	XMTBTC	Initial thickness of 2-D Solid Heat Con Acceptable range: Default value:	material available for oxidation on the surface of the nductor, (m). $0.0 \le \text{XMTBTC} \le \text{half of the maximum thickness of TC.}$ smaller dimension of the cell (K,L).
W-4 (R) :	XOXBTC	Initial thickness of Conductor, (m). Acceptable range: Default value:	oxidized material on the surface of the 2-D Solid Heat $0.0 \le \text{XOXBTC} \le \text{half of the maximum thickness of TC.}$ 0.0.
W-5 (I) :	IOXBTC(1	) Oxidation reaction = -1: Zr oxidation = -2: Zr oxidation = -3: Steel oxidati = -4: Zr oxidation = -5: Graphite oxi > 0: Oxidation r IOXBTC. The us 8500XX, 8510XX, Acceptable range: Default value:	1. by steam, Cathcart model by steam, Urbanic-Heidrich model on by steam, White model by $O_2$ , Benjamin et al. model dation by $O_2$ , Roes model nodel with user-defined coefficient set, number ser-defined coefficients are specified in records , where XX is the set number (see section 2.14.1). $-5 \le IOXBTC \le 10$ , IOXBTC $\neq 0$ . If a positive number is specified, then a user-defined oxidation model must be defined in records 8500XX, 8510XX,, with XX=IOXBTC. none.

W-6 (I):IOXBTC(2) Oxidation reaction 2. See above for description of available reactions.<br/>
Acceptable range:  $-5 \leq IOXBTC \leq 10$ ,  $IOXBTC \neq 0$ . If a positive<br/>
number is specified, then a user-defined oxidation<br/>
model must be defined in records 8500XX,<br/>
8510XX, with XX=IOXBTC. If several reactions<br/>
are specified, then they must be different, i.e.:<br/>
IOXBTC(i) $\neq$ IOXBTC(j).<br/>
Default value:<br/>
none.

W-7 (I): IOXBTC(3) Oxidation reaction 3.

... etc. until all reactions are defined. The maximum number of oxidation reactions per surface is 5.

The example input below defines oxidation reactions for two surfaces. First, Zr oxidation by  $O_2$  and  $H_2O$  for the 2-D Heat Conductor TC-100, left surface. The initial cladding thickness is 0.001 m. The initial oxide thickness is 0.0 m. The built-in reaction models are used (model indicator = -4 for oxygen reaction, and -1 for steam reaction, see section 2.14.1).

Second, steel oxidation by  $O_2$  and  $H_2O$  for the 2-D Heat Conductor TC-100, right surface. The initial thickness of material which can be oxidized is 0.001 m. The initial oxide thickness is 0.0 m. For steel-steam reaction the built-in model is used (model indicator = -3, see section 2.14.1). For steel-oxygen reaction a user-defined model number 4 is used. The records 850004, 8510004, ..., must be specified in the input deck. Example input for steel-oxygen reaction is shown in section 2.14.1.

 \*
 (K,L)
 Un-oxidized Oxide
 Reactions

 480100
 2 5
 0.001
 0.0
 -4
 -1
 \*
 Zr oxidation by O2 and H2O

 480100
 3 1
 0.001
 0.0
 4
 -3
 \*
 Steel oxidation by O2 and H2O

#### 2.4.21 Records: 430XXX, Failure Parameters

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . These records activate the failure model for this 2-D Solid Heat Conductor. The failure model considers the following three failure mechanisms:

٠	Ultimate strength failure	(failure mode $= 1$ )
•	Creep rupture	(failure mode $= 2$ )
•	Meltdown	(failure mode $= 3$ )

W-1 (I) :	IFFATC	Failure model activator.
		=0: failure model not requested for this TC
		>0: failure model requested for this TC. The properties required by the
		failure model are defined with the material number IFFATC in the records 49Y000
		Acceptable range: IFFATC $\geq 0$
		Default value: 0
W-2 (I) :	ITFATC	Indicator defining how the representative temperature is obtained for the failure calculations. =1: use maximum temperature of all TC nodes =2: use volume-weighted average temperature <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 1
-----------	--------	---
W-3 (I) :	ISFATC	<ul> <li>Indicator defining which pressures are used for to determine the stress, needed for the failure calculations</li> <li>&lt;0: use Control Function number  ISFATC  </li> <li>=0: pressure is not used (value is set to 1.0). Stress is constant, and given directly by XSFATC (next word).</li> <li>&gt;0: use CV pressure from the CV at the boundary cell ISFATC <i>Acceptable range:</i> reference to a Control Function or a boundary cell <i>Default value:</i> 0</li> </ul>
W-4 (R) :	XSFATC	Ratio of stress and pressure (defined by the word above), $(\sigma/p)$ . For example in case of a tube with the inner diameter <i>D</i> and the thickness <i>t</i> , the relation between the overpressure inside the tube, <i>p</i> , and the stress, $\sigma$ , (see Figure 2-18): $p \cdot D = \sigma \cdot 2t$

Therefore:

$$\sigma = p \cdot (D/2t)$$

This for this case the ratio is equal to XSFATC = (D/2t). Acceptable range: XSFATC > 0.0Default value: none



Figure 2-35 Relation between stress and pressure for a tube.

#### 2.4.22 Records: 43Y000, Material Properties Needed for Failure Calculations

Y is the material number,  $1 \le Y \le 9$ . The failure model considers the following three failure mechanisms:

- Ultimate strength failure (failure mode = 1)
  Creep rupture (failure mode = 2)
  Meltdown (failure mode = 3)
- (randre mode = 3)

Creep rupture is calculated using the method proposed by Larson and Miller [40]. The time to rupture is obtained from the following relation (see Volume 1):

$$\log_{10}(t_r) = \frac{LMP}{T} - C$$

The Larson-Miller parameter, *LMP*, is approximated in SPECTRA by the following correlation:

$$LMP = A - B \cdot \log_{10}(\sigma)$$

The properties for some materials are shown in Table 2-19.

	Material				
Constants	Inconel-600	Steel 304SS	Steel SA106B	Steel SA533B1	
Α	54,086	58,763	46,129	74,768	
В	4,968.5	5,086.4	4,237.9	6,970.9	
С	9.44	12.44	9.44	16.44	
$T_M$	1644.0	1671.0	1789.0	1789.0	
$\sigma_{U,lowT}$	$7.3 \times 10^{8}$	$6.4 \times 10^{8}$	$5.5 \times 10^{8}$	$5.5 \times 10^{8}$	
$t_{U,highT}$	634.0	1120.0	515.0	30.0	

Table 2-19 Failure model data for some frequently used materials

W-1 (R): AFATC If a positive number is entered this is the coefficient A in the Larson-Miller parameter for creep rupture. If a negative number is entered, then data from Table 2-16 is used. In such case words 2 through 7 are not used. The material identifiers are:
-1: Inconel-600
-2: Stainless steel 304SS
-3: Carbon steel SA106B
-4: Carbon steel SA533B1

Acceptable range:  $10^3 \le \text{AFATC} \le 10^6$  or AFATC = -1, -2, -3, -4Default value: none

W-2(R):	BFATC	Coefficient <i>B</i> in the <i>Acceptable range: Default value:</i>	e Larson-Miller parameter for creep rupture. $10^2 \text{ BFATC} \le 10^5$ none
W-3 (R) :	CFATC	Coefficient <i>C</i> in the <i>Acceptable range: Default value:</i>	e Larson-Miller parameter for creep rupture. $1 \le CFATC \le 10^3$ none
W-4 (R) :	TMFATC	Melting temperatur Acceptable range: Default value:	e, $T_M$ , (K). $500 \leq \text{TMFATC} \leq 10,000$ none
W-6 (R) :	USFATC	Low temperature u Acceptable range: Default value:	Itimate strength, $\sigma_{U,lowT}$ , (Pa). $10^6 \leq \text{USFATC} \leq 10^{10}$ none
W-7 (R) :	TUFATC	High temperature u Acceptable range: Default value:	ltimate strength parameter, $t_{U,highT}$ , (s). $1 \le \text{TUFATC} \le 10^4$ none

#### 2.4.23 Record: 490XXX, Axial Conduction and Direct Contact Conduction

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record activates the axial heat transfer process for this 2-D Solid Heat Conductor. The maximum number of axial heat transfer processes is 100 (10 for 1-D Solid Heat Conductors).

The axial heat conduction or direct contact heat transfer between two structures, i (the "current solid heat conductor", XXX) and j (the "other solid heat conductor"), is considered - Figure 2-36. The heat transfer between the two solid heat conductors is calculated from:

$$Q_{i-j} = A_{i-j} \frac{T_i - T_j}{R_{i-j}}$$

 $Q_{i\cdot j}$  heat transferred between the solid heat conductors *i* and *j*, (W)

 $A_{i-j}$  area of contact between the solid heat conductors *i* and *j*, (m<sup>2</sup>)

 $T_i$  temperature of the solid heat conductor *i* (local or averaged - see Word 2 below), (K)

 $T_i$  temperature of the solid heat conductor *j* (local or averaged - see Word 2 below), (K)

 $R_{ij}$  thermal resistance for the axial heat flow between the solid conductors *i* and *j*, (m<sup>2</sup>-K/W)

The thermal resistance for the heat flow is obtained from:

$$R_{i-j} = \frac{L_i}{k_i} + \frac{1}{h_{i-j}} + \frac{L_j}{k_j}$$

- $L_i$  length for axial conduction in the solid heat conductor *i* (input parameter X1AXTC)
- $k_i$  thermal conductivity in the solid heat conductor *i*

 $L_j$  length for axial conduction in the solid heat conductor *j* (input parameter X2AXTC)

- $k_j$  thermal conductivity in the solid heat conductor j
- $h_{ij}$  heat transfer coefficient at the point of contact of solid heat conductors *i* and *j*

W-1 (I) :	J1AXTC	<ul> <li>First indicator of the other solid heat conductor (<i>j</i>).</li> <li>=1: 1-D Solid Heat Conductor (SC)</li> <li>=2: 2-D Solid Heat Conductor (TC)</li> <li>Acceptable range: 1 or 2</li> <li>Default value: none</li> </ul>
W-2 (I) :	J2AXTC	Second indicator of the other solid heat conductor (j).if J1AXTC=1:SC reference numberif J1AXTC=2:TC reference numberAcceptable range:must be a valid reference number of SC or TCDefault value:none
W-3 (I) :	I1AXTC	Cell number for axial or direct contact heat conduction through the current solid heat conductor, <i>i</i> .

>0: cell reference number, *xxyy*, where xx = x-coordinate (*r* for cylindrical geometry), yy = y-coordinate (*z* for cylindrical geometry), for direct contact heat transfer (see Figure 2-31, Figure 2-36). If the cell *xxyy* is a boundary cell, the heat transfer area is equal to the boundary surface heat transfer area. If the cell *xxyy* is an internal call, the heat transfer area of this cell.

=0: axial heat transfer with all cells transferring heat to the corresponding cell or cells in the other solid heat conductor (Figure 2-36-a). If also I2AXTC = 0, then both solid heat conductors must have identical nodalization.

<0: semi-axial heat transfer for a cylindrical 2-D Solid Heat Conductor: all cells of the axial level |I1AXTC| are transferring heat to corresponding cell or cells in the other solid heat conductor (Figure 2-36-d). The row number must be equal to 1 ("top" row) or the last row ("bottom" row). If also I1AXTC  $\leq 0$ , then both solid heat conductors must have identical nodalization.

Acceptable range: cell number, or 0, or row number in cylindrical TC Default value: none

W-4 (I): I2AXTC Cell number for axial or direct contact heat conduction through the other solid heat conductor, j.

>0: cell reference number, If this is TC (J1AXTC=2) then the format is *xxyy*, where xx = x-coordinate (row) number, yy = y-coordinate (column) number, for direct contact heat transfer (Figure 2-36–b). If the cell *xxyy* is a boundary cell, the heat transfer area is equal to the boundary surface heat transfer area. If the cell *xxyy* is an internal cell, the heat transfer area is equal to the cross-section area of this cell.

=0: axial heat transfer with all cells are transferring heat to corresponding cell or cells in the other solid heat conductor (Figure 2-36-a). If also IIAXTC = 0, then both solid heat conductors must have identical nodalization.

<0: semi-axial heat transfer for a cylindrical 2-D Solid Heat Conductor: all cells of the axial level |I2AXST| are transferring heat to corresponding cell or cells in the other solid heat conductor (Figure 2-36-d). The row number must be equal to 1 ("top" row) or the last row ("bottom" row). If also I1AXTC  $\leq 0$ , then both solid heat conductors must have identical nodalization.

*Acceptable range:* cell number, or 0, or row number in cylindrical TC *Default value:* none

W-5 (R): X1AXTC Length of the axial heat conduction (Figure 2-36) in the current solid heat conductor,  $L_i$  (m).

Acceptable range:  $0.0 \le X1AXTC \le 10,000.0$ Default value: half of the current SC length, if I1AXTC=0

0.0 if I1AXTC>0

W-6 (R) :	X2AXTC	Length of the axial conductor, $L_j$ (m). Acceptable range:	heat conduction (Figure 2-36) in $0.0 \le X2AXTC \le 10.000.0$	n the other solid heat
		Default value:	half of the other SC length, 0.0	if I2AXTC=0 if I2AXTC>0
W-7 (I) :	IHAXTC	Pointer to a Tabula heat transfer coeffi depending on MH. then $h_{i,j}$ or $1/h_{i,j}$ will number: IHAXTC. defined by a Control If the current value to 0.0, there will b 0.0). The value obtinternally limited to is implied (I1AXT resistance may cau $1/h_{i,j} = 10^{-3} \text{ m}^2\text{-K/W}$ <i>Acceptable range:</i> <i>Default value:</i>	ar or Control Function that definition in the end of the function that definition is a state of the function is negative, the function with the reference of the function of the function. A minimum state of the function, if non-zero. 0.	es the direct contact ice, $1/h_{i\cdot j}$ (m <sup>2</sup> -K/W), number is positive, on with the reference a $h_{i\cdot j}$ or $1/h_{i\cdot j}$ will be imber:  IHAXTC . on is smaller or equal bint ( $h_{i\cdot j} = \infty$ , $1/h_{i\cdot j} =$ rol Function will be contact heat transfer a very small contact himum resistance of ber of a Tabular or a
W-8 (R) :	A1AXTC	Multiplier on the he automatically calcu connected conduct A1AXTC is applie	eat transfer area, (-). The area of ulated by the code as the smalle or cells multiplied by the correst d for the cell in the "current" TC	heat transfer, $A_{i\cdot j}$ , is r of the areas of the sponding multiplier. c (while A2AXTC is

applied to the "other" TC or SC). Note that in case of axial heat transfer (heat transfer perpendicular to the normal heat transfer in this conductor), the cross-sectional area of the cell is used. In case of direct contact heat transfer (heat transfer along the normal heat transfer in this conductor), the area of boundary surface. The value obtained in this way is multiplied by A1AXTC. NOTE: The user may also define the area directly, by using the AXAXTC (W-15 below). In this case the multipliers A1AXTC, A2AXTC will be ignored. Acceptable range:  $0.0 < A1AXTC \le 10^{10}$ 1.0

Default value:

W-9(R): A2AXTC Multiplier on the heat transfer area, (-). The area of heat transfer,  $A_{i-i}$ , is automatically calculated by the code as the smaller of the areas of the connected conductor cells multiplied by the corresponding multiplier. A2AXTC is applied to the "other" TC or SC (while A1AXTC is applied for the cell in the "current" TC). Note that in case of axial heat transfer (heat transfer perpendicular to the normal heat transfer in this conductor), the cross-sectional area of the cell is used. In case of direct contact heat transfer (heat transfer along the normal heat transfer in this conductor), the area of boundary surface. The value obtained in this way is multiplied by A2AXTC. NOTE: The user may also define the area directly, by using the AXAXTC (W-15 below). In this case the multipliers A1AXTC, A2AXTC will be ignored. Acceptable range:  $0.0 < A2AXTC \le 10^{10}$ 

Default value: 1.0

W-10 (I) :	MHAXTC	Parameter affecting direct contact conduction:
		=1: IHAXTC defines the heat transfer coefficient, $h_{i,j}$ (W/m <sup>2</sup> -K)
		=2: IHAXTC defines the resistance, $1/h_{i,j}$ (m <sup>2</sup> -K/W)
		Acceptable range: 1 or 2
		Default value: 1

W-11 (I): M1AXTC Pointer to a material number which defines thermal conductivity in the current solid heat conductor. If zero or no value is specified the conductivity of the actual material, defined in the records 410XXX, is used. If a positive value is defined then the thermal conductivity of the material M1AXTC is used. For example, in case of a pebble bed model, the actual material should represent the true material of a pebble, to get a correct surface-to-center temperature difference. M1AXTC should be an artificial material, which is used to define the effective conductivity of the pebble bed, for example from Zehner-Schlunder or Robold correlation (see Volume 3, test PBR-k-eff).

Acceptable range: must be a valid reference number of a solid material, defined in records 801XXX, 802XXX, 803XXX - see section 2.10).

Default value:

W-12(I): M2AXTC Pointer to a material number which defines thermal conductivity in the other solid heat conductor. If zero or no value is specified the conductivity of the actual material, defined in the records 410XXX, is used. If a positive value is defined then the thermal conductivity of the material M2AXTC is used. For example, in case of a pebble bed model, the actual material should represent the true material of a pebble, to get a correct surface-to-center temperature difference. M2AXTC should be an artificial material, which is used to define the effective conductivity of the pebble bed, for example from Zehner-Schlunder or Robold correlation (see Volume 3, test PBR-k-eff).

0

Acceptable range: must be a valid reference number of a solid material, defined in records 801XXX, 802XXX, 803XXX - see section 2.10). 0

Default value:

W-13 (D): Option used for the direct contact transfer (I1AXTC > 0 and I2AXTC >L1AXTC 0) in the current solid heat conductor.

> Cell-to-cell direct contact. The temperature  $T_i$  is taken from the =0:cell I1AXTC. The calculated heat is removed/added to the cell I1AXTC. Global radial transfer. The temperature  $T_i$  is equal to the average =1: temperature of the linked Solid Heat Conductors (mass-averaged or volume-averaged, depending of IAVETC). The calculated heat is distributed over all cells, proportionally to the cell volume or cell mass. The input parameter I1AXTC is used only to determine the area for the heat transfer. This option is intended to model the effective conductivity of the pebble bed or prismatic blocks (see Volume 3, tests PBR-k-eff, PMR-k-eff).

Acceptable range: 0 or 1 Default value: 0

W-14 (I): L2AXTC Option used for the direct contact transfer (I1AXTC > 0 and I2AXTC >0) in the other solid heat conductor. Cell-to-cell direct contact. The temperature  $T_i$  is taken from the =0: cell I2AXTC. The calculated heat is removed/added to the cell I2AXTC. Global radial transfer. The temperature  $T_i$  is equal to the average =1: temperature of the other solid heat conductor (mass-averaged or volumeaveraged, depending of IAVETC). The calculated heat is distributed over all cells, proportionally to the cell volume or cell mass. The input parameter I2AXTC is used only to determine the area for the heat transfer. This option is intended to model the effective conductivity of the pebble bed or prismatic blocks (see Volume 3, tests PBR-k-eff, PMR-k-eff). Acceptable range: 0 or 1 *Default value:* 0 W-15 (R): AXAXTC Area of heat transfer,  $(m^2)$ . If zero or no value is entered, then the area is calculated as the smaller value of the cell areas (multiplicity included):  $A_{HT} = MIN (A_{cell,TC-1} \times A1AXTC, A_{cell,TC-2} \times A2AXTC)$ If a positive value is entered, then the heat transfer area is equal to the entered value:  $A_{HT} = AXAXTC$ Acceptable range:  $0.0 \le AXAXTC \le 10^{10}$ Default value: 0.0 W-16(I): KAXTC Sequential number of the axial heat transfer process. If no value or zero is entered, then the data are read sequentially - the first record 490XXX in the input file is interpreted as containing the first axial transfer process, the second record with this number the second heat transfer process, etc. Acceptable range: I = 1, 2, ..., 6*Default value:* none

Examples are shown in Figure 2-36. Further examples and discussion is included in Volume 3.

Figure 2-36 Cases (a) and (c) - cell-to-cell axial heat conduction

```
* Rectangular geometry - Case (a)
* - "axial" heat transfer - perpendicular to the normal conduction heat flow
\star - conduction length: L = 0.05 m
* - contact h = TF-210
* All cells of TC-220 to all cells of TC-210
* All cells of TC-220 to all cells of TC-230
     TC ijL-i L-j h A-frac
490220 2 210 0 0 0.05 0.05 210 1.0 * Axial heat transfer to TC-210
490220 2 230 0 0 0.05 0.05 210 1.0 * Axial heat transfer to TC-230
* Cylindrical geometry - Case (b)
* - "axial" heat transfer - perpendicular to the normal conduction heat flow
* - conduction length: L = 0.05 \text{ m}
* - contact h = TF-210
* Cells of level 1 of TC-210 to level 2 of TC-230 and level 1 of TC-230 to level 2 of TC-250
     TC i j L-i
                        L-j h A-frac
490210 2 230 -1 -2 0.05 0.05 210 1.0 * Axial heat transfer to TC-230
490230 2 250 -1 -2 0.05 0.05 210 1.0 * Axial heat transfer to TC-230
```

#### Figure 2-36 Cases (b) and (d) - all cells (axial) to one cell (direct contact)

```
* TC-220: heat transfer to TC-210 - Case (b)
* - all cells from TC-220 transfer heat to cell 0101 of TC-210
* - "axial" heat transfer for TC-220, normal conduction heat flow in TC-210
* - axial conduction length: L = 0.05 m for TC-220, L=0.0 m for TC-210
* - contact h = TF-220
    TC i j L-i L-j
                          h A-frac
490220 2 210 0 0101 0.05 0.0 210 1.0 * Axial heat transfer to TC-220
* TC-220: heat transfer to TC-210 - Case (d)
* - level 5 cells from TC-220 transfer heat to cell 0101 of TC-210
* - "axial" heat transfer for TC-220, normal conduction heat flow in TC-210
* - axial conduction length: L = 0.05 m for TC-220, L=0.0 m for TC-210
* - contact h = TF-220
     TC
          i j
                    L-i L-j
                                h A-frac
490220 2 210 -5 0101 0.05 0.00 0 1.0 * TC-220 - Axial heat transfer to TC-210
     HOLE 01: LOWER LEFT, X-CELLS 04-06, Y-CELLS 09-11
       SC i j L-i L-j h Al-frac A2-frac
490120 1 122 0409 2 0.0 0.0 0 100.0
                                              0.125
490120 1 122 0509 2 0.0 0.0 0 100.0
                                              0.125
                            0
490120 1 122 0609 2 0.0 0.0
                                   100.0
                                               0.125
490120 1 122 0410 2 0.0 0.0 0 100.0
                                               0.125
490120 1 122 0610 2 0.0 0.0 0 100.0
                                             0.125
490120 1 122 0411 2 0.0 0.0 0 100.0
                                             0.125
490120 1 122 0511 2 0.0 0.0 0 100.0
                                             0.125
490120 1 122 0611 2 0.0 0.0 0 100.0 0.125
```



Figure 2-36 Axial conduction, direct contact between different TC



Figure 2-37 Axial conduction, example of TC-SC transfer

#### 2.4.24 Record: 499000, Interpolation Factor for Boundary Temperature

W-1 (R): FINTTC Interpolation factor. Used only if a boundary surface is linked to a Control Volume (IVLBTC>0) and at the same time the boundary fluid temperature is defined by a Tabular or Control Function (ITPBTC $\neq$ 0). In such case the value obtained from the Tabular or Control Function is taken with the weighting factor of FINTTC and the temperature in the Control Volume is taken with the weighting factor of 1.0 – FINTTC. *Acceptable range:* 0.0 < FINTTC  $\leq$  1.0 *Default value:* 0.5

#### 2.4.25 Example of the 2-D Solid Heat Conductor Input Data

As an example problem a simple geometry, shown as the Example Problem 2 in Figure 2-32, is considered. The geometry is shown again below, in Figure 2-38.



Figure 2-38 Example of 2-D Solid Heat Conductor.



Figure 2-39 Results of the 2-D test case - stationary conditions.

The example consists of a simple structure with insulation (symmetry) at the external boundaries. At the internal boundaries a fixed heat transfer coefficient of 100.0 W/(m<sup>2</sup>K), and a constant fluid temperature of 300 K is used. The heat transfer coefficient is defined using TF-001, while the fluid temperature is specified using TF-002. The half-cell size is 0.01 m. Therefore the size of the structure is 0.6 m in both x and y direction. The length of the structure (the third, z, dimension) is 1.0 m. There is a uniform internal heat source of Q=1000.0 W.

The input deck is shown below. Results of this test case, obtained for a stationary state, are shown in Figure 2-39.

\* 405100 Steady state with heat source - rectangular, 2-D

400100 1 1.0 0.0 0.0 0 1.0E+3 \* Main data : GEO,L,X0,ELEV,VER,POWER (W), 401100 2 \* USE ENTERED TEMPERATURES \* NUMBER OF CELLS 410100 3 3 \* X-CELL SIZES \* 1 2 3 411100 0.01 0.01 0.01 \* Y-CELL SIZES \* 1 2 3 412100 0.01 0.01 0.01 TC MAP \* \* 1 2 3 413100 1 1110 1101 1111 413100 2 1011 0110 1101 413100 3 1111 1011 0111 \* TC CELL MATERIAL \* 1 2 3 414100 1 1 1 1 414100 2 1 1 1 414100 3 1 1 1 \* TC CELL POWER \* 1 2 3 415100 1 1.0 1.0 1.0 415100 2 1.0 1.0 1.0 415100 3 1.0 1.0 1.0 \* TC CELL TEMPERATURES \* 1 2 3 416100 1 300. 300. 300. 416100 2 300. 300. 300. 416100 3 300. 300. 300. BOUNDARY CONDITIONS \* K L X Y CV HTC T 420100 1 1 0 0 000 001 002 \* 420100 1 2 0 0 000 001 002 \* 420100 2 1 0 0 000 001 002 \* 420100 2 2 0 0 000 001 002 \* 420100 2 3 0 0 000 001 002 \* 420100 3 2 0 0 000 001 002 \* 420100 3 3 0 0 000 001 002 \* \* ====== Tabular Functions \* \* TF-001 - constant htc of 200 W/m/K \* time htc \* 600001 0.0 200.0 \* TF-002 - constant temperature of 300 K \* time temp 600002 0.0 300.0

#### 2.5 MCCI Input Data

#### 2.5.1 Records: 440000, MCCI Main Data

The MCCI model may be activated with this record and the main MCCI data defined. Note that MCCI is always using a cell network of 2-D Solid Heat Conductor. Therefore it must be defined in the input. If more than one TC is defined, the first one is used for MCCI. The TC must be a vertical cylinder.

W-1 (I) :	IMMCTC	MCCI model active = 0 : not active, = 1 : active, liquid = 2 : active, simplif Acceptable range: Default value:	ator: flow calculated from Navier-Stokes equation fied calculation 0, 1, 2 0
W-2 (I) :	ICTPTC	Concrete type: = 0 : user-defined, = 1 : Basaltic aggre = 2 : Limestone co = 3 : Limestone co = 4 : Siliceous 1 [5 = 5 : Siliceous 2 [3 Acceptable range: Default value:	egate concrete [35], mmon sand 1 [57], mmon sand 2 [35], 7], 5], 0, 1, 2, 3, 4, 5 0
W-3 (I) :	ITSCTC	Reference to a Table temperature versus Data for several co 2-40. The figure available in the Z-INPUTS\TC\MO Acceptable range: Default value:	ular Function defining the solidus line, i.e. the solidus concrete weight fraction in a UO <sub>2</sub> -concrete mixture. Increte types, obtained from [58], is shown in Figure was digitized and the appropriate data files are folder with SPECTRA inputs (input file: CCI\Model\TLIQSOL). must be a reference to a valid Tabular Function none
W-4 (I) :	ITLCTC	Reference to a Ta liquidus temperatur mixture. Acceptable range: Default value:	abular Function defining the liquidus line, i.e. the re versus concrete weight fraction in a UO <sub>2</sub> -concrete must be a reference to a valid Tabular Function none
W-5 (I) :	ICCMTC	Material number of Acceptable range: Default value:	f concrete. must be a reference to a valid material defined in the MP Package none
W-6 (I) :	ICMMTC	Material number of Acceptable range: Default value:	f corium. must be a reference to a valid material defined in the MP Package none





Figure 2-40 Solidus and liquidus temperature for corium/concrete mixtures [58] (digitized)

W-7 (R) :	ZRCMTC	Oxidic corium com of UO <sub>2</sub> and ZrO <sub>2</sub> . Z corium.	position. Oxidic corium is assumed to be composed ZRCMTC is the molar (volume) fraction of $ZrO_2$ in
		Acceptable range:	$0.0 \le \text{ZRCMTC} \le 1.0$
		Default value:	0.385 [58]
		5	(a small number $<10^{-50}$ , sets the value to 0.0)
W-8 (R) :	XMETTC	Mass of metallic m the total mass of m total mass of UO <sub>2</sub> -	naterial related to the mass of oxidic corium. This is netals: Fe, Cr, Ni, and unoxidized Zr, divided by the $+ZrO_2$ .
		Acceptable range:	$0.0 \le \text{XMETTC} \le 1.0$
		Default value:	0.2
		5	(a small number $<10^{-50}$ , sets the value to 0.0)
W-9 (R) :	XMFETC	Mass fraction of Fe	e in the metallic material.
		Acceptable range:	$0.0 \le \text{XMFETC} \le 1.0$
		Default value:	0.74
		5	(a small number $<10^{-50}$ , sets the value to 0.0)
W-10 (R) :	XMCRTC	Mass fraction of C	r in the metallic material.
		Acceptable range:	$0.0 \le \text{XMCRTC} \le 1.0$
		Default value:	0.18
		-	(a small number $< 10^{-50}$ , sets the value to 0.0)

W-11 (R) :	XMNITC	Mass fraction of Ni Acceptable range: Default value:	in the metallic material. $0.0 \le \text{XMNITC} \le 1.0$ 0.08 (a small number <10 <sup>-50</sup> , sets the value to 0.0)
W-12 (R) :	XMZRTC	Mass fraction of Zr Acceptable range: Default value:	in the metallic material. $0.0 \le \text{XMZRTC} \le 1.0$ 0.0
W-13 (I)	ICVMTC	CV reference numl namely: H <sub>2</sub> O, H <sub>2</sub> , C <i>Acceptable range:</i> <i>Default value:</i>	ber of the volume receiving gas products of MCCI, CO <sub>2</sub> , CO. valid reference to a CV first boundary CV defined in records 420XXX
W-14 (I)	ICOMTC	Gas number of CO. gas number ICOM Acceptable range: Default value:	The mass of CO released from MCCI will appear as IC in the Control Volume ICVMTC. number of an existing user-defined gas. 7

#### 2.5.2 Records: 44010X, MCCI Material Property Data

This record defines the properties of materials that may undergo phase transition. Here X is the material number: X = 1: concrete, X = 2: UO<sub>2</sub>, X = 3: ZrO<sub>2</sub>.

The properties of solid phase are defined by the standard MP Package, with references to the appropriate materials defined in the main data (record 440000, inputs ICCMTC and ICMMTC). This record defines the liquid properties and the phase change properties. The properties of a molten corium-concrete mixtures are calculated as molar averages of the individual components [58].

W-1 (R) :	DENMTC	Density of liquid material X, $(kg/m^3)$ . For UO <sub>2</sub> and ZrO <sub>2</sub> a temperature- dependent correlation from [60] is used, with DENMTC being a user- defined multiplier:
		-

UO <sub>2</sub> :	$\rho = 11800 - 0.93 \times T \times \text{DENMTC}$
ZrO <sub>2</sub> :	$\rho = 8620 - 0.89 \times T \times \text{DENMTC}$
Acceptabl	<i>e range:</i> $0.1 \le \text{DENMTC} \le 15000.0$
Default vo	<i>alue:</i> 2200 for X=1 [58], 1.0 for X=2 and 3

W-2 (R): CPLMTC Specific heat of liquid material X, (J/kg). For UO<sub>2</sub> and ZrO<sub>2</sub> a temperature-dependent correlation from [60] is used, with DENMTC being a user-defined multiplier:

UO <sub>2</sub> :	$Cp = 390 - 0.90 \times 10^{-4} \times T \times CPLMTC$
ZrO <sub>2</sub> :	$Cp = 940 - 3.36 \times 10^{-2} \times T \times CPLMTC$

Acceptable range:  $0.1 \le \text{CPLMTC} \le 5000.0$ 

*Default value:* 837.3 for X=1 [59], 1.0 for X=2 and 3

W-3 (R): TCLMTC Thermal conductivity of liquid material X, (W/m-K). For UO<sub>2</sub> and ZrO<sub>2</sub> a temperature-dependent correlation from [60] is used, with TCLMTC being a user-defined multiplier:

UO<sub>2</sub>:  $k = 1.64 + 4.74 \times 10^{-2} \times T \times exp(-1.45 \times 10^{4}/T) \times TCLMTC$ ZrO<sub>2</sub>:  $k = 2.11 + 4.46 \times T \times exp(-2.75 \times 10^{4}/T) \times TCLMTC$ 

Acceptable range: $0.01 \le \text{TCLMTC} \le 1000.0$ Default value:1.1 for X=1 [58], 1.0 for X=2 and 3

W-4 (R): VSLMTC Dynamic viscosity of liquid material X, (kg/m-s). For UO<sub>2</sub> and ZrO<sub>2</sub> a temperature-dependent correlation from [59] is used, with VSLMTC being a user-defined multiplier:

UO<sub>2</sub>:  $\mu = 0.52 \times \exp(8.26 \times 10^3/T) \times \text{VSLMTC}$ ZrO<sub>2</sub>:  $\mu = 0.32 \times \exp(8.79 \times 10^3/T) \times \text{VSLMTC}$ 

Acceptable range: $0.01 \le VSLMTC \le 1000.0$ Default value:0.3 for X=1 [58], 1.0 for X=2 and=3

#### for X = 2 and $3 (UO_2 and ZrO_2)$ :

W-5 (R): HFUSTC		Heat of fusion, (J/kg).	
		Acceptable range:	$0.0 < HFUSTC \le 1.0 \times 10^7$
		Default value:	$2.18 \times 10^5$ for X = 2, $2.60 \times 10^5$ for X = 3 [60]

W-6 (R) :TLIQTCMelting temperature, (K). The value must be consistent with the value<br/>defined in the function ITLCTC.<br/>Acceptable range:  $1000.0 \le \text{TLIQTC} \le 9000.0$ <br/>Default value: 3113 for X = 2, 2990 for X = 3 [60]

#### for X = 1 (concrete):

W-5 (R) :	HABLTC	Ablation enthalpy, (J/kg).		
		Acceptable range:	$0.0 < \text{HABLTC} \le 1.0 \times 10^7$	
		Default value:	defined for the built-in concrete types (ICTPTC>0)	
W-6 (R) :	TLIQTC	Liquidus temperatu defined in the funct	Ire, (K). The value must be consistent with the value tion ITSCTC.	
		Acceptable range:	$1000.0 \le TLIQTC \le 9000.0$	
		Default value:	defined for the built-in concrete types (ICTPTC>0)	
W-7 (R) :	TSOLTC	Solidus temperatur defined in the function	re, (K). The value must be consistent with the value tion ITLCTC.	
		Acceptable range:	$400.0 \le \text{TSOLTC} \le 5000.0$	
		Default value:	defined for the built-in concrete types (ICTPTC>0)	

W-8 (R) :TABLTCAblation temperature, (K).<br/>Acceptable range:  $400.0 \le \text{TABLTC} \le 5000.0$ <br/>Default value:Comparison of the state of the s

Properties from several sources: [58], [59], [60], are presented in Table 2-20. In some cases different values were given in different references. In those cases the default values were taken from [60]. The user may wish to perform a sensitivity calculation using the alternative sources shown in the table (or other sources). Further discussion on the liquid properties is provided in Volume 1.

	Concrete	UO <sub>2</sub>	ZrO <sub>2</sub>	Reference
$\rho$ (kg/m <sup>3</sup> )	2200	8860	5150	[58], sec. 3.5, p.33
	2306	10960	5600	[59], MP-RM
$C_p$ (J/kg-K)	837.3	503.0	544.3	[59], MP-RM
<i>k</i> (W/m-K)	1.10	3.05	2.49	[58], sec. 3.5, p.35
$\mu$ (kg/m-s)	0.3 (LCS)	-	-	[58], sec. 3.5, p.33
	1.5 (L)			[58], sec. 3.5, p.33
H (J/kg)	-	2.74E5	7.07E5	[59], MP-RM
		2.18E5	2.60E5	[60]
$T_m(\mathbf{K})$	-	3113	2990	[59], MP-RM
		3200	3000	[60]

Table 2-20 Properties of relevant materials in liquid state

#### 2.5.3 Records: 4402XX, Concrete Composition

The concrete composition is defined with this record. XX is the substance number,  $XX \le 15$ .

W-1 (R):CCOMTCMass fraction of substance XX - see Table 2-21 for substance numbers.<br/>Acceptable range:<br/> $0.0 \le \text{CCOMTC} \le 1.0$ <br/>defined for the built-in concrete types (ICTPTC>0)

The concrete composition as well as the main properties for the built-in concrete types are shown in Table 2-21.

		Concrete composition, mass fractions (%)				
N0.	Substance	Basaltic	Limestone	Limestone	Siliceous 1	Siliceous 2
		aggregate	c. sand 1	c. sand 2		
1	CO <sub>2</sub>	1.5	30.46	21.15	10.0	0
2	H <sub>2</sub> O	5.68	4.46	4.7	3.78	4.0
3	K <sub>2</sub> O	5.39	0.56	1.22	0.83	0
4	Na <sub>2</sub> O	1.8	0.32	0.08	0.68	0
5	TiO <sub>2</sub>	1.05	0.14	0.18	0.16	0
6	SiO <sub>2</sub>	54.84	22.0	35.806	61.34	65.0
7	CaO	8.82	26.4	31.3	17.2	0
8	MgO	6.16	11.7	0.48	0.87	0
9	Al <sub>2</sub> O <sub>3</sub>	6.32	2.54	3.6	3.61	20.0
10	Fe <sub>2</sub> O <sub>3</sub>	6.26	1.42	1.44	1.53	0
11	$Cr_2O_3$	0	0	0.014	0	0
12	CaCO <sub>3</sub>	0	0	0	0	3.0
13	Ca(OH) <sub>2</sub>	0	0	0	0	8.0
14	MnO	0	0	0.03	0	0
15	SO <sub>3</sub>	0	0	0	0	0
T(s	solidus) (K)	1350	1392	1420	1403	1350
T(l	iquidus) (K)	1650	1568	1670	1523	1650
T(a	blation) (K)	1450	1500	1500	1450	1450
dens	sity $\rho$ (kg/m <sup>3</sup> )	2340	2340	2340	2340	2400
Abl. e	enth. $\Delta H$ (J/kg)	$2.8 \times 10^{6}$	$2.4 \times 10^{6}$	$2.4 \times 10^{6}$	$1.95 \times 10^{6}$	$1.95 \times 10^{6}$
Х	K(ablation)	0.333	0.614	0.320	0.392	0.333
	Source	[59]	[57]	[59]	[57]	[59]
		(CAV-UG)		(CAV-UG)		(CAV-UG)

Table 2-21 Built-in concrete composition and properties.

#### 2.5.4 Records: 440300, Model Coefficients

W-1 (R): CRAMTC Coefficient in Ramacciotti correlation [61] for two-phase viscosity:

 $\mu_2 = \mu_1 \exp(2.5 \times CRAMTC \times \phi)$ 

If a negative value is entered, then Kunitz correlation is used (Figure 2-41):

 $\mu_2 = \mu_1 (1+0.5 \times \phi) / (1+\phi)^4$ 

Here  $\mu_1$  is the liquid viscosity,  $\mu_2$  is the two-phase viscosity and  $\phi$  is the solid fraction in the mixture.

Acceptable range: $0.1 \le CRAMTC \le 10.0 \text{ or } < 0.0$ <br/>(note: [59] recommends 4.0 - 8.0)Default value:4.0



Figure 2-41 Comparison of Ramacciotti and Kunitz correlations.

W-2 (R) :	XRAPTC	Radial erosion parameter. Fraction of ablated concrete that is removed from a cell (replaced by corium) in a time step. If the entered value is smaller than the minimum set by mass balance, which is equal to the ratio of degassed mass to the ablated mass (XRAPTC= $V_{deg}/V_{abl}$ ), the latter will be used. A large value may be used to speed up removal of ablated concrete from a cell. Acceptable range: $0.0 \leq XRAPTC \leq 0.9$ Default value: $0.0$
W-3 (R) :	XZAPTC	Axial erosion parameter. Fraction of ablated concrete that is removed from a cell (replaced by corium) in a time step. If the entered value is smaller than the minimum set by the mass balance, which gives the value equal to the ratio of degassed mass to the ablated mass (XZAPTC = $V_{deg}/V_{abl}$ ), the latter will be used. A large value may be used to speed up removal of ablated concrete from a cell. <i>Acceptable range:</i> 0.0 ≤ XZAPTC ≤ 0.9 <i>Default value:</i> 0.0
W-4 (R) :	XDISTC	Maximum dissolution of ablated concrete in corium. If zero or no value is entered, the value is calculated from the ratio of degassed mass and the ablated mass as follows: XDISTC = $1 - V_{deg}/V_{abl}$ . Acceptable range: $0.1 \le \text{XDISTC} \le 0.9$ or XDISTC= $0.0$ Default value: $1.0 - V_{deg}/V_{abl}$
W-5 (R) :	IDEPTC	Indicator for corium depression calculation in simplified model (IMMCTC=2). =1: depression not calculated =2: depression calculated <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> 2

W-6 (R) : IRSQTC Indicator for reaction sequence. =1: all reactions proceed simultaneously >1: reactions proceed in a sequence, following [58]: "Zr is oxidized first, and Si, Cr, and Fe follow". The relative strength of reaction is proportional to  $10^{X}$ , where X = 1 - IRSQTC. The sequential effect becomes stronger with increasing value of IRSQTC. *Acceptable range:* 1, 2, 3, 4 *Default value:* 3

#### 2.5.5 Records: 441001, Initial Velocities, Horizontal (Radial) Direction

The initial velocities in molten cells or partially molten cells are defined with this record. The values are used only if IMMCTC=1.

W-1 (I) :	L	Row number in y (axial) direction. The following data must specifyNCLXTC-1 velocities in the y-row number L.Acceptable range: $1 \le L \le NCLYTC$ Default value:none
W-2 (R) :	VELXTC (1,L)	Initial velocity (m/s), cell (1,L)Acceptable range: $-100.0 \le VELXTC \le 100.0$ Default value: $0.0$
W-3 (R) :	VELXTC (2,L)	Initial velocity (m/s), cell (2,L)Acceptable range: $-100.0 \le VELXTC \le 100.0$ Default value: $0.0$

..., etc. until velocities are defined for all cells (NCLXTC-1 velocities should be entered).

#### 2.5.6 Records: 441002, Initial Velocities, Vertical (Axial) Direction

The initial velocities in molten cells or partially molten cells are defined with this record. The values are used only if IMMCTC=1.

W-1 (I) :	L	Row number. The following data must specify NCLXTC velocities in the <i>y</i> -row number L. Acceptable range: $1 \le L \le NCLYTC - 1$ Default value: none
W-2 (R) :	VELYTC (1,L)	Initial velocity (m/s), cell (1,L)Acceptable range: $-100.0 \le VELYTC \le 100.0$ Default value: $0.0$
W-3 (R) :	VELYTC (2,L)	Initial velocity (m/s), cell (2,L)Acceptable range: $-100.0 \le VELYTC \le 100.0$ Default value: 0.0

.., etc. until velocities are defined for all cells (NCLXTC-1 velocities should be entered).

#### 2.5.7 Records: 441003, Initial Porosities

The initial porosities are defined with this record.

W-1 (I) :	L	Row number. The the y-row number I Acceptable range: Default value:	following data must specify NCLXTC porosities in 1. $1 \le L \le NCLYTC$ none
W-2 (R) :	POROTC (1,L)	Initial porosity (-), Acceptable range: Default value:	cell (1,L) 0.0 ≤ POROTC ≤ 1.0 0.0
W-3 (R) :	POROTC (2,L)	Initial porosity (-), Acceptable range: Default value:	cell (2,L) 0.0 ≤ POROTC ≤ 1.0 0.0

..., etc. until porosities are defined for all cells (NCLXTC porosities should be entered).

#### 2.5.8 Records: 441004, Initial Concrete Fractions

The initial concrete fractions are typically defined by the code using the cell material data and the input parameter ICCMTC (record 440000), as follows:

- XCONTC = 1.0 if the material number in the cell is equal to ICCMTC
- XCONTC = 0.0 otherwise

It is possible to define different initial conditions using this record.

W-1 (I) :	L	Row number. The f y-row number L. Acceptable range: Default value:	ollowing data must specify NCLXTC fractions in the $1 \le L \le NCLYTC$ none
W-2 (R) :	XCONTC (1,L)	Initial concrete frac Acceptable range: Default value:	tion (-), cell (1,L) $0.0 \le \text{XCONTC} \le 1.0$ 1.0 if the cell material = ICCMTC, 0.0 otherwise
W-3 (R) :	XCONTC (2,L)	Initial concrete frac Acceptable range: Default value:	tion (-), cell (2,L) $0.0 \le \text{XCONTC} \le 1.0$ 1.0 if the cell material = ICCMTC, 0.0 otherwise

.., etc. until concrete fractions are defined for all cells (NCLXTC fractions should be entered).

## 2.5.9 Records: 441005, Initial Ablated Concrete Fractions

The initial ablated concrete fractions are typically set as zero. It is possible to define different initial ablated fractions using this record.

W-1 (I) :	L	Row number. The f y-row number L. Acceptable range: Default value:	ollowing data must specify NCLXTC fractions in the $1 \le L \le NCLXTC$ none
W-2 (R) :	XABLTC (1,L)	Initial ablated conce Acceptable range: Default value:	rete fraction (-), cell (1,L) $0.0 \le \text{XCONTC} \le 1.0$ 1.0 if the cell material = ICCMTC, 0.0 otherwise
W-3 (R) :	XABLTC (2,L)	Initial ablated conce Acceptable range: Default value:	rete fraction (-), cell (2,L) 0.0 ≤ XCONTC ≤ 1.0 1.0 if the cell material = ICCMTC, 0.0 otherwise

.., etc. until concrete fractions are defined for all cells (NCLXTC porosities should be entered).

#### 2.6 Thermal Radiation Input Data

#### 2.6.1 Records: 500Y00, Thermal Radiation Model Selection

Y = 1, ..., 9, is the radiating system number. Up to 9 systems are allowed. The numbering must be consecutive. Each system may consist of up to 90 radiating surfaces. Surfaces radiate among each other within each system. There is no direct radiation between surfaces belonging to different radiating systems.

W-1 (I): MODRAD Radiation model. MODRAD = 1 - radiation in grey enclosure with non-absorbing/non-emitting gas. MODRAD = 2 - radiation in grey enclosure with absorbing/emitting gas. The radiation model is used only if the number of radiating surfaces, entered on the records 510YXX, is greater than 1. Application of the thermal radiation model often involves significant effort, needed to prepare the view factor and beam length data. For cases when thermal radiation is less important, a simple wall-gas radiation model is available for Solid Heat Conductors (see sections 1.3.6, 1.3.7). Acceptable range: 1, 2

Acceptable range: 1, 2 Default value: 2

W-2 (I): IWTRAD Selector of option for radiating surfaces covered by water.

= 1: do not radiate to water. Stop calculations if more than 10% of any radiating surface is covered by water.

= 2: the water-covered part of the surface radiates to the water pool. The global energy remains conserved. The thermal radiation is completely deactivated if more than 50% of all surfaces is covered with water.

= 3: the water-covered part does not radiate. The global energy is, in general, not conserved (with this option the global energy is conserved only if the water-covered fraction is the same for all radiating surfaces). The thermal radiation is completely deactivated if more than 50% of all surfaces is covered with water.

Acceptable range: 1, 2, 3 Default value: 2

W-3 (R) :XWTRADMinimum fraction of fluid volume occupied by water to switch off the<br/>thermal radiation model. Used only for RADMOD =2 (enclosure with<br/>participating gas). If the water level in a volume representing an<br/>enclosure is higher than XWTRAD times the volume height, the thermal<br/>radiation model is switched off for this particular enclosure.<br/>
Acceptable range:  $0.1 \le XWTRAD \le 1.0$ <br/>
Default value: 0.9

#### 2.6.2 Records: 505Y00, Radiating System Name

Y = 1, ..., 9, is the radiating system number.

W-1 (A): NAMETR User defined name of the radiating system Y, length up to 50 characters. The name is read as a 50-character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* 50 "underline" characters: "\_".

#### 2.6.3 Records: 510YXX, Radiating Surface Data

Y = 1, ..., 9, is the radiating system number. The numbering of radiating systems must be consecutive. XX is the reference number of a radiating surface. XX need not be consecutive. The maximum number of radiating surfaces in each radiating system is 90.

Data on those records associate radiating surfaces with the surfaces of 1-D or 2-D Solid Heat Conductors.

W-1 (I) : IS	ISCRAD	Number of 1-D Solid Heat Conductor (if ITCRAD=0, see Word 4 below), or a 2-D Solid Heat Conductor (if ITCRAD>0) for the surface
		XXX. If ITCRAD=0, then ISCRAD < 0 indicates the left surface of the
		1-D Solid Conductor $ $ ISCRAD $ $ , while ISCRAD > 0 indicates the right
		surface of Solid Conductor number ISCRAD as the radiating surface
		XXX. If ITCRAD>0, then ITCRAD indicates the boundary cell number
		of the 2-D Solid Heat Conductor ISCRAD, as the radiating surface
		XXX. When ITCRAD=0, ISCRAD < 0, then the left boundary heat flux
		for the 1-D Solid Conductor  ISCRAD  cannot be specified using
		Tabular or Control Functions; IQRLSC must be equal to zero (see
		section 2.3.11). When ITCRAD=0, ISCRAD $> 0$ , then the right
		boundary heat flux for the 1-D Solid Conductor ISCRAD cannot be
		specified using Tabular or Control Functions; IQRRSC must be equal to
		zero (see section 2.3.12). When ITCRAD>0, then the heat flux for the
		cell number ITCRAD of the 2-D Solid Conductor ISCRAD cannot be
		specified using Tabular or Control Functions; IQRBTC must be equal to
		zero (see section 2.4.13).
		Only one radiating surface may be associated with a given SC or TC
		surface. Both left and right surfaces of a SC can be associated with
		radiating surfaces, belonging to the same or to different radiating
		systems. Multiple boundary cell surfaces of a TC can be associated with
		systems.
		Acceptable range: must be a valid reference number of a 1-D or a 2-D
		Solid Heat Conductor.
		Default value: none.
W-2 (I) :	IESRAD	Pointer to a Tabular Function or a Control Function that defines the
		surface emissivity. If the number is positive then the emissivity of the

surface XXX will be calculated using the Tabular Function IESRAD. The argument for the Tabular Function IESRAD will always be the surface temperature. The emissivity will therefore not be equal to the value of the Tabular Function itself, because Tabular Function values are always printed as functions of time. If the number is negative then the emissivity will be defined by the value of Control Function | IESRAD|. If the value obtained from Tabular Function or Control Function is smaller than 10<sup>-5</sup>, then it will be set to 10<sup>-5</sup>. If it is larger than 1.0 it will be set to 1.0. If no value is entered, or the entered value is equal to zero, then the emissivity is set to 1.0 (black surface).

Acceptable range: must be a valid reference number of a Tabular or a Control Function.

*Default value:* 0.

W-3 (I) :

IPLRAD Activates pool radiation option for this surface (only for 1-D Conductors)

If  $\underline{IPLRAD} = 0$  then the pool option is deactivated. In this case the treatment of radiating surface is defined by IWTRAD (Word 2 in record 500Y00.

If <u>IPLRAD > 0</u> then the pool in the Control Volume adjacent to the surface will participate in radiation heat transfer. When IPLRAD > 0 then the surface XXX is considered as a "floor", that can be covered by water. The following conditions must be met to use the pool radiation option:

- The elevation of the surface must be equal to the bottom elevation of the corresponding Control Volume: IVLLSC(|ISCRAD|) if ISCRAD<0, or IVLRSC(ISCRAD) if ISCRAD > 0.

- The geometry must be rectangular: IGEOSC(|ISCRAD|) = 1.

- The surface must be horizontal: IVERSC(|ISCRAD|) = ±1.

- The surface area must be the same as the bottom (segment number 1) cross section area of the corresponding Control Volume:

ASEGCV(1,IV) = SIZESC(|ISCRAD|), where IV is the Control Volume number: IVLLSC(|ISCRAD|) or IVLRSC(ISCRAD), depending on the sign of ISCRAD.

If the above conditions are met then the radiative heat exchange for this surface is calculated as follows:

- If the pool liquid level exceeds the surface elevation by more than  $\Delta Z = 10^{-3}$  m, then the surface temperature is set to the pool temperature, the emissivity is set to the liquid water emissivity (0.96 - [14], page 15-23):

$$\begin{array}{rcl} T &=& T_{POOL},\\ \varepsilon &=& 0.96 \,. \end{array}$$

where  $T_{POOL}$  is the pool temperature. The calculated radiant heat flux is deposited in the pool.

- If the pool level is below 10<sup>-3</sup> m, temperature and emissivity is linearly interpolated between the pool values and the radiation surface values:

$$\begin{array}{rcl} T & = & T_{POOL} \, \Delta Z/10^{-3} & + & T_{SC} \, (10^{-3} - \Delta Z)/10^{-3} \\ \varepsilon & = & 0.96 \, \Delta Z/10^{-3} & + & \varepsilon_{SC} \, (10^{-3} - \Delta Z)/10^{-3} \end{array}$$

where:  $T_{SC}$  is the surface temperature equal to the left or right temperature of the Solid Conductor |ISCRAD|, and  $\epsilon_{SC}$  is the emissivity obtained from the Tabular Function or the Control Function

IESRAD. The obtained heat flux is partitioned between pool and Solid Conductor:

 $Q_{POOL} = Q_{TOT} \Delta Z/10^{-3}$ ,  $Q_{SC} = Q_{TOT} (10^{-3} - \Delta Z)/10^{-3}$ . where  $Q_{POOL}$  is heat deposited in the water pool,  $Q_{SC}$  is the heat deposited at the surface of the Solid Conductor | ISCRAD|, and  $Q_{TOT}$  is the total heat flux calculated for this surface by the radiation heat exchange

The surface area of the pool is assumed to be always equal to the area of the surface XXX. This may not be true if Control Volume consists of several segments with different cross section areas. In that case calculations will still be performed but a warning message will be issued. It is recommended to use a single-segment Control Volume in case the pool radiation option is activated.

Acceptable range: the pool option is available only for 1-D Solid Heat Conductors.

Default value:

model.

W-4 (I): ITCRAD Boundary cell number of the 2-D Solid Heat Conductor (defined by ISCRAD - Word 1 above) associated with this radiating surface. Used only if a 2-D Solid Heat Conductor should be associated with this surface. If a 1-D Solid Heat Conductor should be associated with this surface, then the number must be zero. *Acceptable range:* must be a valid boundary cell number if non-zero. *Default value:* 0.

0.

#### 2.6.4 Records: 520YXX, View Factors

Y = 1, ..., 9, is the radiating system number. The numbering of radiating systems must be consecutive. XX is the reference number of a radiating surface. XX need not be consecutive. The maximum number of radiating surfaces in each radiating system is 90.

The data on records 520YXX give view factors from the surface XX to all other surfaces belonging to the system Y. Several records with the same number may be entered. The data is read sequentially.

W-1 (R) :	VFCRAD	View factor from the surface YXX to the surface Y01, $F_{YXX \rightarrow Y01}$ . This is the fraction of the total power emitted by the surface YXX that reaches the surface Y01. Acceptable range: $0.0 \le VFCRAD \le 1.0$ . Default value: none.
W-2 (R) :	VFCRAD	View factor from the surface YXX to the surface Y02, $F_{YXX \to Y02}$ . The II- th word on the record gives the view factor from the surface YXX to the surface YII. NSFRAD numbers must be entered. Several records with the same number may be used. The records are read sequentially in the order they appear in the input deck. <i>Acceptable range:</i> $0.0 \le VFCRAD \le 1.0$ . <i>Default value:</i> none.
•••	VFCRAD	until NSFRAD(Y) numbers are entered.

Conservation of energy in a system of radiating surfaces depends on the fact whether the reciprocity relation and closure relation is fulfilled with good accuracy. The reciprocity relation is:

$$A_i F_{i \to j} = A_j F_{j \to i}$$

where  $A_i$  is the surface area, m<sup>2</sup>, of the i-th radiating surface. The closure relation is:

$$\sum_{j=1}^{N} F_{i \to j} = 1.0$$

where N is the total number of radiating surfaces within a given radiating system, NSFRAD(Y). The program checks if those relations are fulfilled with an accuracy of at least 8 decimal places. Therefore view factors must be carefully evaluated before the radiation model can be activated.

#### 2.6.5 Records: 530YXX, Beam Lengths

Y = 1, ..., 9, is the radiating system number. The numbering of radiating systems must be consecutive. XX is the reference number of a radiating surface. XX need not be consecutive. The maximum number of radiating surfaces in each radiating system is 90.

The data on records 530YXX give average beam lengths between the surface XX and all other surfaces belonging to the system Y. Several records with the same number may be entered. The data is read sequentially.

W-1 (R) :	XBLRAD	Average beam length between the surface YXX and the surface Y01,		
		$L_{YXX \rightarrow Y01}$ . This nur	nber is used to determine the gas emissivity and	
		absorptivity on the	path between surface YXX and Y01.	
		Acceptable range:	XBLRAD = 0.0, if the corresponding view factor,	
			VFCRAD, is equal to zero;	
			$10^{-10} \leq \text{XBLRAD} \leq 10^{10}$ , if the corresponding view	
			factor, VFCRAD, is positive.	
		Default value:	none.	
W-2 (R) :	XBLRAD	Average beam len	gth between the surface YXX and the surface Y02,	
		$L_{YXX \rightarrow Y02}$ . The II-th	word on the record gives the beam length between	
		the surface YXX	and the surface YII. NSFRAD numbers must be	
		entered. Several rec	cords with the same number may be used. The records	
		are read sequential	ly in the order they appear in the input deck.	
		Acceptable range:	XBLRAD = 0.0, if the corresponding view factor,	
			VFCRAD, is equal to zero;	
			$10^{-10} \le \text{XBLRAD} \le 10^{10}$ , if the corresponding view	
			factor, VFCRAD, is positive.	
		Default value:	none.	
	XBLRAD	until NSFRAD nur	nbers are entered.	

#### 2.6.6 Records: 531YXX, Beam Lengths for Multiple CV Paths

Y = 1, ..., 9, is the radiating system number. The numbering of radiating systems must be consecutive. XX is the reference number of a radiating surface. XX need not be consecutive. The maximum number of radiating surfaces in each radiating system is 90.

The data on records 531YXX give average beam lengths for cases when beam passes through several Control Volumes. f a set of volumes is specified for radiation path between surfaces *i* and *j*, then exactly the same set of volumes must be supplied for the path between surfaces *j* and *i*. In fact it is better to specify data for one direction only (for example  $i \rightarrow j$ ). In such case the code will assume the same volumes and beam length for the "return" path  $(j \rightarrow i)$ . If the beam length on the path  $i \rightarrow j$  are different then the lengths on the path  $j \rightarrow i$ , then a warning message is printed but such input is accepted for calculations. It may be used if gas emissivity is close to 1.0 and all radiation is absorbed on the in the vicinity of the radiating surface.

W-1 (I) :	JJ	Surface number. The between surface Y	he following entries define beam lengths on the path XX and YJJ.
		Acceptable range:	JJ must be a valid surface number in the system Y.
		Default value:	none.
W-2 (I) :	ICV(1)	Control Volume nu	imber.
		Acceptable range:	ICV(1) must be a valid Control Volume number.
		Default value:	none.
W-3 (R) :	YBLRAD(1	) Average beam le	ngth in the Control Volume ICV(1).
		Acceptable range:	YBLRAD(1) > 0.0, Sum of all values of
			YBLRAD(i) must be the same as the total beam
			length, XBLRAD, entered in the record 530YXX.
		Default value:	none.
W-4 (I) :	ICV(2)	Control Volume nu	imber.
		Acceptable range:	ICV(2) must be a valid Control Volume number.
		Default value:	none.
W-5 (R) :	YBLRAD(2	2) Average beam lea	ngth in the Control Volume ICV(2).
		Acceptable range:	YBLRAD(2) > 0.0, Sum of all values of
			YBLRAD(i) must be the same as the total beam
			length, XBLRAD, entered in the record 530YXX.
		Default value:	none.
	until all beam leng	ths are defined. The	e maximum number of Control Volumes on a single
	L L	·	8

#### 2.6.7 Records: 5400XX, Radiation Properties of Gases

radiation beam path is 10.

XX = 01, 02, ..., NGAS is the ID number of the gas. The number of gases is the same as in the gas property main data base. The following built-in gases are built-in:  $1 = H_2, 2 = He, 3 = H_2O, 4 = N_2, 5 = O_2, 6 = CO_2$ 

The radiation properties of gases are defined in this record. The same radiation properties of gases are used for all radiating systems. This record is optional. All entries from this record have their default values, recommended for general application.

W-1 (R): EMSMAX Gas emissivity at infinite path length,  $\epsilon_{\infty}$ . This number is also used as a selector of the gas emissivity correlation. If the value is:  $0.0 < EMSMAX \le 1.0$  the emissivity for gas i (i=XXX) is calculated from the following correlation:

$$\varepsilon_{i} = \varepsilon_{i,\infty} \left\{ 1 - \exp\left[-\left(a_{i} + b_{i}T\right)\left(p_{i}L\right)^{c_{i}}\right] \right\}$$

where  $\varepsilon_{i,\infty}$ ,  $a_i$ ,  $b_i$ ,  $c_i$  are user input constants.

EMSMAX=0.0: gas does not participate in radiative heat transfer. EMSMAX>0.0: maximum emissivity = EMSMAX, gray gas model is applied for spectral overlap:  $\Delta \varepsilon_g = \varepsilon_{H_2O} \cdot \varepsilon_{CO_2}$  (see Volume 1)

EMSMAX<0.0: recommended Kostowski correlations are used for steam and CO<sub>2</sub>. The correlation for spectral overlap,  $\Delta \varepsilon_g = f(T, p_{H_2O}, p_{CO_2})$ , described in Volume 1, is used, with the limit set by the gray gas model:  $\Delta \varepsilon_a \leq \varepsilon_{H_2O} \cdot \varepsilon_{CO_2}$ .

*Note*! For gases other than steam and  $CO_2$  EMSMAX < 0 gives the same effect as EMSMAX = 0.0, no emission/absorption. Note that if zero is entered then the default value is assumed which for steam and  $CO_2$  is: – 1, and leads to Kostowski correlations. If the emissivity of these gases needs to be switched off then a small positive value,  $10^{-90}$ , should be entered.

Acceptable range: $0.0 \le EMSMAX \le 1.0$  or EMSMAX = -1.0Default value:-1.0, if XX = 3 (H<sub>2</sub>O) or XX = 6 (CO<sub>2</sub>),<br/>0.0, for all other gases.

- W-2 (R): AEMISG Constant  $a_i$  in general equation for gas emissivity. Used only if EMSMAX is greater than zero for this gas. Acceptable range: AEMISG  $\geq 0.0$ . Default value: 0.0.
- W-3 (R): BEMISG Constant  $b_i$  in general equation for gas emissivity. Used only if EMSMAX is greater than zero for this gas. The values of  $a_i + b_i T$  must be positive to obtain physically correct results. Input processing subroutines check if the condition is fulfilled for up to 2200 K, that means:  $a_i + b_i 2200 \ge 0.0$ . The calculation procedures ensure that the sum  $a_i + b_i T$  is never negative. If a negative value is obtained it will be set to zero. *Acceptable range:* BEMISG  $\ge$  -AEMISG/2200.0. *Default value:* 0.0.
- W-4 (R): CEMISG Constant  $c_i$  in general equation for gas emissivity. Used only if EMSMAX is greater than zero for this gas. Acceptable range: CEMISG  $\geq 0.0$ . Default value: 0.0.

W-5 (R): XABSPG Exponent, n, in gas absorptivity correlation. Absorptivity is calculated from the following correlation:

$$a_{g} = \left(\frac{T_{g}}{T_{w}}\right)^{n} \varepsilon_{g}\left(T_{w}, pL\frac{T_{w}}{T_{g}}\right)$$

where:	$T_{g}$	-	gas temperature, (K),
	$T_w$	-	wall temperature, (K),
	pL	-	optical length, (Pa m),
	$\mathcal{E}_{g}$	-	gas emissivity calculated at wall temperature
	0		and optical length multiplied by the radio
			$(T_w/T_g),$ (-),
	n	-	constant defined by user $=$ XABSPG.
The value	e of XA	BSPG	is used only if the gas is participating in the

The value of XABSPG is used only if the gas is participating in the radiative heat transfer, that means if EMSMAX > 0.0 (for all gases), or if EMSMAX < 0.0 (for steam and CO<sub>2</sub>). Acceptable range:  $0.0 \le XABSPG \le 1.0$ .

 Default value:
 0.45, if XXX = 3 (H<sub>2</sub>O),

 0.65, if XXX = 6 (CO<sub>2</sub>),

 0.50, for all other gases.

#### 2.6.8 Records: 541000, Radiation Properties of Aerosols

The radiation properties of aerosols are defined in this record. The same radiation properties of aerosols are used for all radiating systems. This record is optional. Note: in order to take the aerosol radiation into account, the parameters present in this record must be defined, as described below.

The emissivity of a mixture of gases and aerosol particles is obtained from:

$$\varepsilon_{mix} = 1 - (1 - \varepsilon_{aer}) \cdot \prod_{k=1}^{N_{gas}} (1 - \varepsilon_k)$$

The aerosol emissivity is calculated from (see Volume 1):

$$\mathcal{E}_{aer} = 1 - \exp\left[-L \cdot \sum_{i=1}^{N_{six}} n_i \cdot \left(\frac{\pi D_i^2}{4}\right) \cdot (a_{aer} + b_{aer} T^{c_{aer}})\right]$$

Eaer	emissivity of aerosols, (-)
L	radiation beam length, (m)
n <sub>i</sub>	density of aerosol size section $i$ , $(1/m^3)$
$D_i$	diameter of aerosol size section $i$ , (m)
Т	temperature, (K)
Nsize	number of aerosol size sections
a <sub>aer</sub> , b <sub>aer</sub> , c <sub>aer</sub>	user-defined constants, entered in this record

In absence of a more detailed data, a simple way to take the aerosol emissivity into account is to use the following values of the model constants:  $a_{aer} = 1.0$ ,  $b_{aer} = 0.0$ ,  $c_{aer} = 0.0$ . In such case the aerosol emissivity is equal to:

$$\varepsilon_{aer} = 1 - \exp\left[-L \cdot \sum_{i=1}^{N_{sige}} n_i \cdot \left(\frac{\pi D_i^2}{4}\right)\right]$$

- W-2 (R): AAERTR Constant  $a_{aer}$  in the equation for the aerosol emissivity. If the value is zero then the aerosol emissivity is not taken into account. Acceptable range: AAERTR  $\geq 0.0$ Default value: 0.0
- W-3 (R): BAERTR Constant  $b_{aer}$  in the equation for the aerosol emissivity. Acceptable range: BAERTR  $\geq 0.0$ Default value: 0.0.
- W-4 (R) :CAERTRConstant  $c_{aer}$  in the equation for the aerosol emissivity.Acceptable range: $-10.0 \le \text{CAERTR} \le 10.0$ .Default value:0.0.

#### 2.6.9 Example of Thermal Radiation Input Data

As an example problem the radiative heat transfer inside a cylindrical space, partly filled with liquid water is considered. The geometrical configuration is shown in Figure 2-42. A single Control Volume is used, which is filled with liquid water up to the height of  $H_{pool}$ . The remaining, gas filled part of the CV, has the height of  $H_{gas}$ .



Figure 2-42 Geometrical configuration for Thermal Radiation example problem.

Four solid conductors are used to model the walls, ceiling and floor of the volume (see example problem in section 2.3.39). SC-001 is a cylindrical Heat Conductor, which represents the outer wall, above the liquid level. The inner radius of this wall is equal to the outer radius of the cylindrical space,  $R_{out}$ . The height is equal to the height of gas space,  $H_{gas}$ . SC-002 represents the inner wall. The outer radius of this SC is equal to  $R_{in}$ . SC-3 is a rectangular conductor, which represents the ceiling. SC-004 represents the floor. Additional conductors may be used in the model to represent the cylindrical walls below the liquid level, (as in the example problem shown in section 2.3.39), but are not considered here since they will not participate in radiation heat transfer.

The thermal radiation input is created in three steps:

I First, the surfaces which will be allowed to participate in radiation heat transfer are chosen and associated with the appropriate SC surfaces. In this problem the following associations are made:

Surface: 1	-	SC-1, left side,
Surface: 2	-	SC-2, right side,
Surface: 3	-	SC-3, right side (this must be the lower side of SC-3. The right side is the lower
		one if $IVERSC = 1$ for this SC, see section 2.3.39),
Surface: 4	-	SC-4, right side (this must be the upper side of SC-4. The right side is the upper
		one if IVERSC = $-1$ for this SC, see section 2.3.39).

For the surface 4 the pool radiation option is chosen. The SC is considered as a floor for the pool. When the pool is present the radiative flux will be deposited at the pool surface. If there is no pool in the CV then the right surface of SC-4 will participate in radiation heat transfer. The area of SC-4 must be equal to the cross section area of the CV, so that the view factors calculated based on surface area of SC-4 are appropriate for the pool surface too. If the pool level changes during the calculations it may partly cover the SC-1 and SC-2. Still the radiation heat transfer areas and the view factors will remain the same. The view factors are not recalculated during transient. Consequently the areas must remain the same to avoid violation of radiant energy conservation.

II Second, view factors must be calculated. The view factors must be supplied with good accuracy (see Volume 1). For the considered geometry the view factors may be calculated using the formulae shown in [14] (page 15-46):

View factor from the outer wall to the inner wall is equal to:

$$F_{1 \to 2} = \frac{1}{X} - \frac{1}{\pi X} \cdot \left[ \arccos\left(\frac{b}{a}\right) - \frac{1}{2Y} \cdot \left(\sqrt{(a+2)^2 - (2X)^2} \cdot \arccos\left(\frac{b}{aX}\right) + b \cdot \arcsin\left(\frac{1}{X}\right) - \frac{\pi a}{2} \right) \right]$$

View factor from the outer wall to the outer wall itself is equal to:

$$F_{1\to1} = 1 - \frac{1}{X} + \frac{2}{\pi X} \cdot \arctan\left(\frac{2\sqrt{X^2 - 1}}{Y}\right) - \frac{Y}{2\pi X} \cdot \left[\frac{\sqrt{4X^2 + Y^2}}{Y} \cdot \arcsin\left(\frac{4(X^2 - 1) + Y^2 / X^2 \cdot (X^2 - 2)}{Y^2 + 4 \cdot (X^2 - 1)}\right) - \arcsin\left(\frac{X^2 - 2}{X^2}\right) + \frac{\pi}{2} \cdot \left(\frac{\sqrt{4X^2 + Y^2}}{Y} - 1\right)\right]$$

The meaning of the symbols in the above equations is as follows:  $X = R_{out}/R_{in}$   $Y = H_{gas}/R_{in}$   $a = Y^2 + X^2 - 1$  $b = Y^2 - X^2 + 1$ 

Due to symmetry the values of  $F_{1\rightarrow3}$  and  $F_{1\rightarrow4}$  are equal. Thus once  $F_{1\rightarrow2}$  and  $F_{1\rightarrow1}$  are known the values of  $F_{1\rightarrow3}$  and  $F_{1\rightarrow4}$  are obtained as:

$$F_{1\to3} = F_{1\to4} = \frac{1}{2} \cdot \left(1 - F_{1\to2} - F_{1\to2}\right)$$

The remaining view factors are obtained using the reciprocity  $(A_iF_{i\rightarrow j} = A_jF_{j\rightarrow i})$  and the closure  $(\Sigma F_{i\rightarrow j} = 1)$  relations.

For the example problem the following data were assumed:  $R_{in} = 5$  m,  $R_{out} = 15$  m,  $H_{gas} = 5$  m. The resulting view factors are:

- $F_{1\to 1} = 0.117156532$
- $F_{1\to 2} = 0.092480799$
- $F_{1\to3} = F_{1\to4} = 0.395181335$

Values of other view factors, calculated using the reciprocity and closure relations, are shown in the listing below.

Note that the surface area of rectangular conductors (3 and 4), which is equal to 628.31853 (=200  $\pi$ ), must be entered with the accuracy corresponding to the accuracy of view factors (see section 2.3.39). For the cylindrical SC the program calculates the area internally using the length and radius.

III The last step is to calculate the mean beam lengths. The exact values may be obtained by rather complicated integration. However there is no need to calculate beam lengths with very good accuracy. They are used to obtain gas emissivity/absorptivity. This is done by correlations, which have, at best, the accuracy of two decimal places. Here a simplified method, described below, is used to obtained the mean beam lengths.

The mean beam lengths for all paths except  $L_{1\to 1}$ , are calculated by multiplying the distance between the centres of surfaces by a constant factor, greater than one,  $(1 + \varphi)$ . The  $L_{1\to 1}$  length was estimated by multiplying the maximum possible beam length by the factor  $(1 - \varphi)$ .

$$\begin{split} L_{1\to2} &= (1+\varphi) \cdot (R_{out} - R_{in}) \\ L_{3\to4} &= (1+\varphi) \cdot H_{gas} \\ L_{1\to3} &= (1+\varphi) \cdot \frac{1}{2} \cdot \sqrt{H_{gas} + (R_{out} - R_{in})^2} = L_{1\to4} \\ L_{1\to1} &= (1-\varphi) \cdot 2 \cdot \sqrt{R_{out}^2 - R_{in}^2} \end{split}$$

The other lengths were calculated assuming that  $L_{i \rightarrow j} = L_{j \rightarrow i}$ . The value of  $\varphi$  was taken as 0.3. The calculated beam lengths are shown in the printout below.

The average value of the beam length for an enclosure is calculated by the program internally, as:

$$L_{ave} = \frac{\sum_{i=1}^{N} \sum_{j=1}^{N} A_i \cdot F_{i \to j} \cdot L_{i \to j}}{\sum_{i=1}^{N} \sum_{j=1}^{N} A_i \cdot F_{i \to j}}$$

where:  $A_i$  -

 $A_i$  - area of surface *i*, (m<sup>2</sup>),

 $F_{i \rightarrow j}$  - view factor between surface i and j, (-),  $L_{i \rightarrow i}$  - mean beam length between surface i and j, (m).

The average value is compared with an "engineering estimation" of mean beam length in an enclosure, which is ([14] page 15-65):

$$L_{eng} = \frac{4V}{A}$$

where: V - total volume of the enclosure, (m<sup>3</sup>) A - total surface area of the enclosure, =  $\Sigma A_i$ , (m<sup>2</sup>)

In the presented example the  $L_{ave}$  is equal to 7.60, while  $L_{eng}$  is equal to 7.93. Another possibility of calculating the beam lengths is to calculate  $L_{eng}$  and then use this value for all  $L_{i \rightarrow j}$ .

A program to calculate view factors and beam lengths in a cylindrical enclosure, using the formulae shown above on is provided in: \Z-INPUTS\TR\CylVF. SPECTRA input for the example problem is shown below. The default gas radiation models are used in the presented example.

```
----- Thermal radiation data
505100 Cylindrical system with radiation to pool
500100 2 * radiation model : absorbing/emitting medium
510101
              7
                   0 *
                           TR-101 = SC-001, left surface
        1
              7 0 * TR-102 = SC-002, right surface
7 0 * TR-103 = SC-003, right surface
        2
510102
510103
         3
        4
            7
                  1 * TR-104 = SC-004, right surface, pool option
510104
        View factors, F(i\Box > j)
                                   j=2
                                                      j=3
*
     \j
               j=1
                                                                        j=4
*
     i\
                            0.0924807990.3951813350.3951813350.000000000.3612788010.3612788010.0903197000.000000000.6132942990.0903197000.6132942990.00000000
520101
           0.117156532
          0.277442397
520102
520103
           0.296386001
        0.296386001
520104
        Beam lengths, L(i->j)
*
    λj
             j=1 j=2 j=3
                                   j=4
*
    i\
530101
             19.8 13.0
                           7.3
                                   7.3
530102
             13.0 0.0
                            7.3
                                   7.3
530103
               7.3
                     7.3
                            0.0
                                   6.5
530104
              7.3
                   7.3
                           6.5
                                  0.0
```
#### 2.7 Tabular Function Input Data

#### 2.7.1 Records: 605XXX, Tabular Function Name

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

 W-1 (A): NAMETF User defined name, length up to 50 characters. The name is read as a 50-character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.
 Acceptable range: any string of up to 50 characters. Default value: 50 "underline" characters: "\_".

#### 2.7.2 Records: 601XXX, Scaling Factor and Additive Constant

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

W-1 (R) :	SCLFTF	Scaling factor, <i>S</i> . The interactively by the understand the <i>Acceptable range:</i> a <i>Default value:</i> 1	the value defined by the tabulated data points, aser, is multiplied by this factor. All real numbers. $1.0$ (a small number $<10^{-50}$ , sets the value to 0.0).	or
W-2 (R) :	ADDCTF	Additive constant, A defined by the tabula value of Tabular Fund	. The value of this constant is added to the val ated data points, or interactively by the user. T action is:	ue 'he

 $TF(t) = f(t) \cdot S + A$ 

*Acceptable range:* all real numbers. *Default value:* 0.0.

#### 2.7.3 Records: 602XXX, Lower and Upper Limits, Rate Change Limits

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

W-1 (R) :	VMINTF	Minimum value of Tabular Function: $TF(t) \ge VMINTF$ .Acceptable range: $-10^{99} \le VMINTF \le +10^{99}$ Default value: $-10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-2 (R) :	VMAXTF	Maximum value of Tabular Function: $TF(t) \leq$ VMAXTF. Acceptable range: $-10^{99} \leq$ VMAXTF $\leq +10^{99}$

		Default value:	$+10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-3 (R) :	DDDTTF	Maximum rate of c $d TF(t) / dt \ge DDD$ Acceptable range:	hange in case of decreasing value of TF: TTF. $-10^{99} \le \text{DDDTTF} \le 0.0$
		Default value:	$-10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-4 (R) :	DIDTTF	Maximum rate of c $d TF(t) / dt \le +DID$	hange in case of increasing value of TF: TTF.
		Acceptable range: Default value:	$0.0 \le \text{DIDTTF} \le +10^{59}$ +10 <sup>99</sup> (a small number <10 <sup>-50</sup> , sets the value to 0.0)

#### 2.7.4 Records: 603XXX, Rate Change Limits for Generating Message

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . A message is written to the message file (and optionally screen) if the TF value or the rate of change exceeds the values defined in this record.

W-1 (R) :	VMNMTF	Minimum limit for messaging. Message is generated if: TF(t) < VMNMTF. Acceptable range: $-10^{99} \le VMNMTF \le +10^{99}$ Default value: $-10^{99}$
W-2 (R) :	VMAXTF	Maximum limit for messaging. Message is generated if: TF(t) > VMAXTF. Acceptable range: $-10^{99} \le VMAXTF \le +10^{99}$ Default value: $+10^{99}$
W-3 (R) :	DDDMTF	Rate of change in case of decreasing value of TF. Message is generated if the rate of change is $d TF(t) / dt < DDDMTF$ . Acceptable range: $-10^{99} \le DDDMTF \le 0.0$ Default value: $-10^{99}$
W-4 (R) :	DIDMTF	Rate of change in case of increasing value of TF. Message is generated if the rate of change is $d TF(t) / dt > +DIDMTF$ . Acceptable range: $0.0 \le DIDMTF \le +10^{99}$ Default value: $+10^{99}$

#### 2.7.5 Records: 610XXX, Interpolation Type, Interactive Type

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

W-1 (I) : INTKTF The absolute value determines the type of interpolation, while the sign determines whether this TF is an interactive function INTKTF > 0

Non-interactive TF - the value of the TF is always determined by the table, entered in the input deck.

INTKTF < 0

Interactive Tabular Function - this type of TF is useful in the simulation mode. At any time of calculations the TF value may be modified in the file \*.TFD (see section 3.6). The value that needs to be specified in the \*.TFD file is simply the TF number and the value that it should take. Therefore, to set the value of TF-120 to 521.0 one needs to type (or the simulation tool needs to send) the following line in the \*.TFD file:  $120 \qquad 521.0$ 

If there is no data for the TF in the \*.TFD file, then the value of the function will be determined by the table present in the input deck. If the value is present in the \*.TFD file, then the value of TF will change, the rate of change being limited by the DDDTTF and DIDTTF, until it reaches the value designated in \*.TFD file, provided that it is not outside the limits given by VMINTF, VMAXTF. The TF will stay at that value for as long as it is present in the \*.TFD file. If the value in the \*.TFD value should change, the TF will start changing to reach the new value, again respecting the limits set by DDDTTF, DIDTTF, VMINTF, VMAXTF. If the value disappears from the \*.TFD file, then the TF will start changing to reach the value prescribed for it by the tabulated data pairs, again respecting the limits set by DDDTTF, DIDTTF, VMINTF, VMAXTF.

The type of interpolation is used only when the TF is using the data table, not the value from the \*.TFD file (in other words, when the \*.TFD file does not contain a value of this TF). The possible types of interpolations are (see Figure 2-43):

IINTKTF|=1:linear interpolation (continuous function).IINTKTF|=3:cubic interpolation ("smooth" function - continuous function and it's first derivative).Acceptable range:-3, -1, +1, +3.Default value:-1.

#### 2.7.6 Records: 611XXX, Automatic Reset Option for Interactive TF

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

W-1 (R): RSETTF Automatic reset for interactive TF. If the value of an interactive Tabular Function has been specified in the \*.TFD file, it is being used until a new value is specified or the current value is removed. In order to switch back to the TF data tabulated in the input deck, one must remove all definitions of given TF from the TFD file. This can be done automatically using the automatic reset option.
=0.0: automatic reset to the tabulated TF after the time of RSETTF (s) since the function has been specified in the \*.TFD file. This option removes the definition of the given TF from the \*.TFD file after specified amount of seconds elapses.

Acceptable range:RSETTF  $\geq 0.0$ Default value:0.0

#### 2.7.7 Records: 600XXX, Tabular Function Data Records

XXX is the Tabular Function reference number,  $001 \le XXX \le 999$ . The TF reference numbers need not be consecutive. The maximum number of Tabular Functions is 999.

Each data record contains one data pair. The total number of data pairs may not exceed 20,000, for a single Tabular Function.

W-1 (R) :	TBFUNX	Value of the independent the independent varia tables for which the in Control Functions (see Acceptable range: Va fo va Default value: no	lent variable, point I. In case of Tabular Functions able is always time (s). If the user wishes to use adependent variable is other than time, he must use action 2.8). alues of TBFUNX must increase. Thus the value or a given point must be greater than the previous alue (TBFUNX for the previous point). one.
W-2 (R) :	TBFUNY	Value of the depended Function XXX, $f(t)$ , at interactive TF the value by the numbers enter *.TFD. Acceptable range: all Default value: not	ent variable, point I. The value of the Tabular t time equal to $t = \text{TBFUNX}$ . Note that in case of ues tabulated in the input deck may be overridden red by the user (or a simulation tool) in the file I real numbers.
W-3 (I) :	Ι	Point number. If no v read sequentially - the the first point (I=1), th <i>Acceptable range:</i> 0 - <i>Default value:</i> no	value, or zero is entered, then the data points are first record in the input is interpreted as containing then I=2, etc. $< I \le 20,000.$

#### 2.7.8 Examples of Tabular Function Input and Use of \*.TFD

The example input of the Tabular Function data defines two Tabular Functions. TF-001 uses linear interpolation between the data points. TF-002 uses cubic interpolation between the data points. Both Tabular Functions are defined by seven data points. Negative value of the TF type means that the interactive option is used, and the TF value may be redefined during calculations in the \*.TFD file. The limits of 0.0 and 99.0 are imposed on the values read from the \*.TFD file.

```
        605001
        Example 1 of Tabular Function

        601001
        1.0
        0.0
        * Scaling factor, Additive constant

        602001
        0.0
        99.0
        * Limits

        610001
        -1
        * Interactive, Linear Interpolation TF

        *
        Time
        Value

        600001
        5.0
        0.10
```

10.0	1.10	*	
15.0	1.10	*	
25.0	0.20	*	
30.0	2.50	*	
35.0	1.00	*	
45.0	1.00	*	
Examp	le 2 of	Tab	ular Function
1.0	0.0	*	Scaling factor, Additive constant
0.0	99.0	*	Limits
-3		*	Interactive, Cubic Interpolation TF
Time	Value		
5.0	2.10	*	
10.0	3.10	*	
15.0	3.10	*	
25.0	2.20	*	
30.0	4.50	*	
35.0	3.00	*	
45.0	3.00	*	
	10.0 15.0 25.0 30.0 35.0 45.0 Examp 1.0 0.0 -3 Time 5.0 10.0 25.0 30.0 35.0 45.0	10.0 1.10 15.0 1.10 25.0 0.20 30.0 2.50 35.0 1.00 45.0 1.00 Example 2 of 1.0 0.0 0.0 99.0 -3 Time Value 5.0 2.10 10.0 3.10 15.0 3.10 25.0 2.20 30.0 4.50 35.0 3.00	10.0 1.10 * 15.0 1.10 * 25.0 0.20 * 30.0 2.50 * 35.0 1.00 * 45.0 1.00 * Example 2 of Tab 1.0 0.0 * 0.0 99.0 * -3 * Time Value 5.0 2.10 * 10.0 3.10 * 15.0 3.10 * 25.0 2.20 * 30.0 4.50 * 35.0 3.00 *

Figure 2-43 shows the values of TF-001 and TF-002, as well as the data points. The data points are shown using markers. The values of TF-001 and TF-002, calculated for times between 0 and 50 s, are marked by lines.

The cubic interpolation ensures continuity of the first derivative in all range except for the boundary (first and last) data points. In those points the derivative "jumps" to zero, since flat lines are used outside the data points. The discontinuity was programmed on purpose, because this formulation is considered safer for practical use. The cubic interpolation subroutine is used in SPECTRA, among others, for the calculation of water properties. In this case the applied formulation allows to obtain



problem.

correct behavior of the interpolated functions in the region close to the freezing point. The fact that the functions won't be smooth if the temperature drops below the freezing point has no practical meaning. If the user wishes to avoid this discontinuity, he can do that by specific definition of the data points near the boundary, as shown below.

The last two data points of TF-002 were given the same value. It is seen in Figure 2-43 that the discontinuity of the derivative, clearly seen at the left boundary of this function, is not present at the right boundary.

Figure 2-43 Values of Tabular Functions (lines) and data points (markers) for the two Tabular Functions, defined in the example

By including the point numbers (Word 3) the data can be entered in an arbitrary order. For example, the two definitions shown below are equivalent:

```
605001Example 1 of Tabular Function6010011.00.0* Scaling factor, Additive constant6020010.099.0* Limits610001-1* Interactive, Linear Interpolation TF
```

*	Time	Value	Poin	t	
600001	5.0	0.10	1	*	
600001	10.0	1.10	2	*	
600001	15.0	1.10	3	*	
600001	25.0	0.20	4	*	
600001	30.0	2.50	5	*	
600001	35.0	1.00	6	*	
600001	45.0	1.00	7	*	
605001	Exam	ple 1 of	Tabu	lar	Function
601001	1.0	0.0	* S	cal	ing factor, Additive constant
602001	0.0	99.0	* L	imi	ts
610001	-1		* I	nte	ractive, Linear Interpolation TF
*					· -
*	Time	Value	Poin	t	
600001	45.0	1.00	7	*	
600001	5.0	0.10	1	*	
600001	35.0	1.00	6	*	
600001	10.0	1.10	2	*	
600001	15.0	1.10	3	*	
600001	25.0	0.20	4	*	
600001	30.0	2.50	5	*	

Both sets of records shown above define the same function.

The data present in the \*.TFD file may have two formats:

•	Arbitrary number of pairs, for example:
	120 1.0 200 1.5 250 -5.0
	The above record will set (immediately as it appears in the *.TFD file) the following
	values: TF-120=1.0, TF-200=1.5, TF-250=-5.0
•	Three input parameters, single TF definition with TIMEON. For example:
	120 1.0 1000.0
	The above record will set TF-120=1.0 at the time = $TIMEOF = 1000.0$ s (or immediately if
	the current time is larger than 1000.0 s.
	Another example. The following records:
	120 1.0 1000.0
	120 2.0 2000.0
	120 5.0 3000.0
	will set the value of TF-120 to 1.0 at $t = 1000.0$ s, to 2.0 at $t = 2000.0$ s, and finally to 5.0
	at $t = 5000.0 \text{ s}$ .

Note that the maximum amount of data pairs that can be defined in a single line is 20. This means up to 20 Tabular Function values can be specified in a single record, if the first format (immediate action) is used.

#### 2.8 Control Function Input Data

#### 2.8.1 Records: 700XXX, Control Function Main Data

XXX is the Control Function reference number,  $001 \le XXX \le 999$ . The CF reference numbers need not be consecutive. The maximum number of Control Functions is 999.

W-1 (I) :	IGRPCF	First identifier defining the type of Control Function - see Table 2-22.Acceptable range: $1 \leq IGRPCF \leq 3$ .Default value:none.
W-2 (I) :	INUMCF	Second identifier defining the type of Control Function, Table 2-22. Acceptable range: $1 \le INUMCF \le 9$ , if IGRPCF = 1, $1 \le INUMCF \le 16$ , if IGRPCF = 2, $1 \le INUMCF \le 5$ if IGRPCF = 3
		Default value: none.
W-3 (R) :	SCLFCF	Scaling factor, S. The result of the function defined by previous twointegers is multiplied by this factor.Acceptable range:all real numbersDefault value:1.0 (a small number <10 <sup>-50</sup> , sets the value to 0.0)
W-4 (R) :	ADDFCF	Additive constant, <i>A</i> . The value of this constant is added to the calculated value of the function. The value of Control Function is:
		$CF(t) = f(x_1, x_2,) \cdot S + A$

Acceptable range:all real numbersDefault value:0.0.

#### 2.8.2 Records: 701XXX, Initial Value

XXX is the Control Function reference number,  $001 \le XXX \le 999$ .

W-1 (I) : INTCF		Initial value calculation indicator.				
		1: Initial value	is calculated.			
		2: Input value (	Word 2 below) is used. Use this option also when the			
		initial value	should be read from an Initial Condition File - ICF			
		(section 2.16	5.3).			
		Acceptable range:	1, 2. For integral type CF the initial value must be specified, therefor INTCF must be equal to 2			
		Default value:	1 for all CF types except integral, 2 for integral.			
W-2 (R) :	CONFUN	Initial value of the	Control Function.			
		Acceptable range:	$-10^{99} \le \text{CONFUN} \le +10^{99}.$			
		Default value:	0.0 .			

Group a	and No.		Number	
		Function type	of	FORTRAN definition
			arguments	
IGRPCF	INUMCF			
1	1	Add / subtract	≤ 100	$f = a_1 + (-) a_2 + (-) \dots + (-) a_n$
	2	Multiply / divide	≤ 100	$f = a_1 \cdot (/) a_2 \cdot (/) \dots (/) a_n$
	3	Power function	2	$f = a_1 * a_2 if a_1 > 0$
				$f = - a_1  ** a_2$ if $a_1 < 0$
	4	Selected argument	4	IF $(a_1 .LT. a_2)$ THEN
				L = A3 ELSE
				f = a <sub>4</sub>
				ENDIF
	5	General tabular function	≤ 100	see example in section 2.8.6
	6	Hysteresis	3	see example in section 2.8.11
	7	Derivative	1	$f = (a_1 - a_1^0) / \Delta t$
	8	Integral	1	$f = f^0 + a_1 \cdot \Delta t$
	9	Random number	1	$f = rnd() \cdot S(a_1) + A(a_1)$
2	1	Absolute value	1	$f = DABS(a_1)$
	2	Minimum value	≤ 100	$f = DMIN1(a_1, a_2,, a_n)$
	3	Maximum value	≤ 100	$f = DMAX1(a_1, a_2, a_n)$
	4	Square root	1	f = DSQRT(a <sub>1</sub> )
	5	Exponent	1	$f = DEXP(a_1)$
	6	Natural logarithm	1	$f = DLOG(a_1)$
	7	Decimal logarithm	1	$f = DLOG10(a_1)$
	8	Sine	1	$f = DSIN(a_1)$
	9	Cosine	1	$f = DCOS(a_1)$
	10	Tangent	1	$f = DTAN(a_1)$
	11	Arc sine	1	$f = DASIN(a_1)$
	12	Arc cosine	1	$f = DACOS(a_1)$
	13	Arc tangent	1	$f = DATAN(a_1)$
	14	Hyperbolic sine	1	$f = DSINH(a_1)$
	15	Hyperbolic cosine	1	f = DCOSH(a1)
	16	Hyperbolic tangent	1	f = DTANH(a1)
3	1	Error function	1	$f = DERF(a_1)$
	2	Complementary error f.	1	$f = DERFC(a_1)$
	3	Gamma function	1	f = DGAMMA(a1)
	4	Log gamma function	1	f = DLGAMA(a1)
	5	Reactor Kinetics	1	see Volume 1

Table 2-22 Types of Control Functions.

#### 2.8.3 Records: 702XXX, Lower and Upper Limits, Rate Change Limits

XXX is the Control Function reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	VMINCF	Minimum value of Control Function: $CF(t) \ge VMINCF$ .Acceptable range: $-10^{99} \le VMINCF \le +10^{99}$ Default value: $-10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-2 (R) :	VMAXCF	Maximum value of Control Function: $CF(t) \leq$ VMAXCF.Acceptable range: $-10^{99} \leq$ VMAXCF $\leq +10^{99}$ Default value: $+10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-3 (R) :	DDDTCF	Maximum rate of change in case of decreasing value of CF: $d CF(t) / dt \ge DDDTCF.$ Acceptable range: $-10^{99} \le DDDTCF \le 0.0$ Default value: $-10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)
W-4 (R) :	DIDTCF	Maximum rate of change in case of increasing value of CF: $d CF(t) / dt \le \text{DIDTCF}.$ Acceptable range: $0.0 \le \text{DIDTCF} \le +10^{99}$ Default value: $+10^{99}$ (a small number $<10^{-50}$ , sets the value to 0.0)

#### 2.8.4 Records: 703XXX, Rate Change Limits for Generating Message

XXX is the Control Function reference number,  $001 \le XXX \le 999$ . A message is written to the message file (and optionally screen) if the CF value or the rate of change exceeds the values defined in this record.

W-1 (R) :	VMNMCF	Minimum limit for $CF(t) < VMNMCF$ . Acceptable range: Default value:	messaging. Message is generated if: $-10^{99} \leq \text{VMNMCF} \leq +10^{99}$ $-10^{99}$
W-2 (R) :	VMAXTF	Maximum limit for <i>CF</i> ( <i>t</i> ) > VMAXCF. <i>Acceptable range:</i> <i>Default value:</i>	messaging. Message is generated if: $-10^{99} \le VMAXCF \le +10^{99}$ $+10^{99}$
W-3 (R) :	DDDMCF	Rate of change in ca Message is generate Acceptable range: Default value:	ase of decreasing value of CF. ed if the rate of change is $d CF(t) / dt < DDDMCF$ . $-10^{99} \le DDDMCF \le 0.0$ $-10^{99}$
W-4 (R) :	DIDMCF	Rate of change in ca Message is generate Acceptable range: Default value:	ase of increasing value of CF. ed if the rate of change is $d CF(t) / dt > +DIDMCF$ . $0.0 \le DIDMCF \le +10^{99}$

#### 2.8.5 Records: 705XXX, Control Function Name

XXX is the Control Function reference number,  $001 \le XXX \le 999$ .

W-1 (A): NAMECF User defined name, length up to 50 characters. The name is read as a 50character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* 50 "underline" characters: "\_".

#### 2.8.6 Records: 708XXX, Y-Coordinate Points for 2-D Tabular Functions

XXX is the Control Function reference number,  $001 \le XXX \le 999$ .

A General Tabular Function is one of the types of a Control Function (IGRPCF=1, INUMCF=5, - see Table 2-22). The main difference between a Tabular Function (section 2.7) and a General Tabular Function from the CF Package is the argument type. In case of a TF the argument is always time. This allows excluding all TF from the main iteration loop to obtain implicit solution (the implicit values of all TF is known; they are tabulated versus time, so the value at any given time point is readily available). On the other hand the General Tabular Function type of a CF (IGRPCF=1, INUMCF=5, - see Table 2-22) may use any variable from the SPECTRA data base as an argument. Since the implicit value of its argument may not be available at the start of the time step, this CF, like all other CF, is included in the main iteration loop to obtain implicit solution (the implicit treatment of CF may be altered by setting argument calculation on explicit - record 709XXX, or by the implicit solution indicator - record 715000).

There are two kinds of a General Tabular Function:

• A simple, one-dimensional general Tabular Function. This function has two arguments. The first argument defines an independent variable for this function. The second argument is a reference number of a Tabular Function from the TF data base. An example is shown below.

```
605105 Tabular Function TF-123
              f(x)
        Х
600105 300.0
               0.0
600105 400.0
               1.0
705105 1-D General Tabular Function
                      Fact.
      Group
             Number
                                    Const.
700105
       1
                             1.0
                                     0.0
                                             *
                                                Туре
                                                        : General TF
                 5
      Arguments
* Pointers: (1) (2) (3) (4) Fact.
                                     Const.
        1 125
6 105 1
710105
               123 14
                                     0.0 *
                                             Use CV-123-Temp-atms as argument
                        1
                             1.0
                                     0.0 *
710105
                        0
                             1.0
                                            Use table TF-105
```

In the above example Tabular Function, TF-105 and a General Tabular Function, CF-105, are defined. The value of TF-105 will be equal to zero for times t < 300.0 s, increase linearly to 1.0 during 300.0 < t < 400.0 s, and remain equal to 1.0 afterwards. The value of CF-105 will be equal to zero when the atmosphere temperature in CV-123 is below T < 300.0 K, increase

linearly to 1.0 with the temperature increasing between 300.0 < T < 400.0 K, and remain equal to 1.0 for higher temperatures.

• A two-dimensional Tabular Function, F(x,y), may be created, where x is the first argument and y is the second argument. In this case the general Tabular Function should be defined by a number of TFs, each TF defining the value of function versus the argument x for one value of the argument y. The y-arguments are defined in this record. An example of a 2-D function is shown below.

```
605101 Efficiency versus flow, pump speed of 20 rev/s
                 f(x)
         х
600101 0.05
600101 0.2
                  0.30
                  0.60
600101 0.5
                 0.72
600101 0.8
600101 1.0
                0.80
0.75
600101 1.1
                 0.70
605102 Efficiency versus flow, pump speed of 40 rev/s
         х
                  f(x)
600102 0.05
                  0.40
600102 0.1
600102 0.2
                  0.60
                  0.70
600102 0.5
                 0.82
600102 1.0
600102 1.1
                 0.85
                  0.81
605103 Efficiency versus flow, pump speed of 50 rev/s
                f(x)
         X
600103 0.05
                  0.50
600103 0.1
                  0.70
600103 0.2
                 0.80
600103 0.35
                 0.90
600103 1.0
                 0.92
600103 1.1
                 0.88
705100 2-D General Tabular Function
       Group Number Fact.
                                           Const.
               يون
2
پ2
700100 1
                                                     * Туре
                                 1.0
                                            0.0
                                                                   : General TF
         y1
                      yЗ
708100 20.0 40.0 50.0 * y-coordinate data points (pump speeds)
      Arguments
* Pointers: (1) (2) (3) (4) Fact. Const.
           s: (1) (2) (3) (4) Fact. Const.
2 500 37 2 1.0 0.0 * x-argument: JN-500, pump flow (pool)
6 101 1 0 1.0 0.0 * uses TF-101 for y = y1
6 102 1 0 1.0 0.0 * uses TF-102 for y = y2
6 103 1 0 1.0 0.0 * uses TF-103 for y = y3
710100
710100
710100
710100
               2 500 36 2 1.0 0.0 * y-argument: JN-500, pump speed (pool)
710100
```

The above example defines the pump efficiency, as a function of pump volumetric flow and pump speed. During the calculations a 2-D interpolation is performed to find the value of a function.

For example, suppose that during the execution the CF-100 (pump efficiency) should be calculated for the Volumetric flow of V = 0.15 m<sup>3</sup>/s and speed of 45 rev/s. First the *x*-coordinate interpolations are performed; the calculated values are (see the data values above):

$\omega = 40.0 \text{ rev/s}$	TF-102 ( $x=0.15$ ) = 0.65
$\omega = 50.0 \text{ rev/s}$	TF-103 ( <i>x</i> =0.15) = 0.75

Now the linear interpolations between the two points shown above is performed, to give:

 $\omega = 45.0 \text{ rev/s}$  CF-100 (x=0.15, y=45.0) = 0.70



Figure 2-44 Example of a 2-D General Tabular Function

The *y*-coordinate data points are defined by the following data words:

W-1 (R) :	ARG2CF (1)	The first y-coordina Acceptable range: Default value:	ate value for the 2-D interpolation. any real. none.
W-2 (R) :	ARG2CF (2)	The second y-coord Acceptable range: Default value:	dinate value for the 2-D interpolation ARG2CF(2) > ARG2CF(1). none.

... until all arguments are entered. The number of *y*-coordinate data points must be the same as the number of Tabular Functions used with this CF. The first argument for the general Tabular Function defines an independent variable for the *x*-coordinate. The last argument defines an independent variable for the *y*-coordinate. All other arguments are pointing to Tabular Functions. Since the total number of arguments of any CF is limited to 100, and the first and last argument are defining the independent variables, therefore the maximum number of Tabular Functions (and simultaneously the maximum number of *y*-coordinate data points) is 98.

#### 2.8.7 Records: 709000, Implicit/Explicit Use of Arguments - Global Activator

This records specifies the implicit/explicit use of CF arguments for all Control Function. The values can be redefined for each individual CF using the records 709XXX.

W-1 (A) : IMARCF Indicator defining the method of using CF arguments. IMARCF = 1: Implicit (use end of time step value). IMARCF = 2: Explicit (use beginning of time step value, if such value is available).

By default the implicit method is used. If convergence problems are observed for Control Functions, then the explicit method should be used. Note that not all variables are kept at the two levels: new time step and old time step. Those variables for which the old time step value is available and the explicit method may be used, are marked by the symbol **I/E** in Table 2-23 through Table 2-32. Those for which only implicit method is available are marked by the symbol **I/E**. *Acceptable range:* 1 or 2. *Default value:* 1.

This records specifies default values of the friction model parameters. The default values can be redefined for each individual junction in the records 210XXX.

#### 2.8.8 Records: 709XXX, Implicit/Explicit Use of Arguments

This records specifies the implicit/explicit use of CF arguments for Control Function with reference number XXX,  $001 \le XXX \le 999$ .

W-1 (A): IMARCF Indicator defining the method of using CF arguments. IMARCF = 1: Implicit (use end of time step value). IMARCF = 2: Explicit (use beginning of time step value, if such value is available).

By default the implicit method is used. If convergence problems are observed for Control Functions, then the explicit method should be used. Note that not all variables are kept at the two levels: new time step and old time step. Those variables for which the old time step value is available and the explicit method may be used, are marked by the symbol **I/E** in Table 2-23 through Table 2-32. Those for which only implicit method is available are marked by the symbol **I/-**. *Acceptable range:* 1 or 2. *Default value:* 1.

#### 2.8.9 Records: 710XXX, Control Function Arguments

XXX is the Control Function reference number,  $001 \le XXX \le 999$ . Each record with this number defines one argument of the Control Function. Total number of arguments must be in agreement with the number of arguments for the given type of Control Function, shown in Table 2-22.

W-1 (I): IARG1C First pointer for Control Function argument. The absolute value of this pointer defines the data base from which the argument must be taken. The sign of IARG1C is significant for the "Add" and "Multiply" functions. A positive value means that during the calculation of the Control Function this argument is added to ("Add" CF) or multiplied by ("Multiply" CF) the Control Function. A negative value means that during the calculation of the Control Function this argument is subtracted from the Control Function ("Add" CF) or that the Control Function is divided by this argument ("Multiply" CF). The absolute values should be as follows: |IARG1C| = 1: the argument will be taken from Control Volume Data Base. |IARG1C| = 2: Junction Data Base. |IARG1C| = 3: 1-D Solid Conductor Data Base. IARG10

ARGIC	= 4:	2-D	Conductor Data Base.
~ . ~	l _		

|ARG1C| = 5: Thermal Radiation Data Base.

|ARG1C| = 6: Tabular Function Data Base.

|ARG1C| = 7: Control Function or Reactor Kinetics Data Base.

|ARG1C| = 8: Radioactive Particle Transport Data Base.

|IARG1C| = 9: The SOLVER Data Base.

In case of a Tabular Function (IGRPCF=1, INUMCF=5) the second argument points to the Tabular Function Data Base (see Volume 1, section XXX) and the value of IARG1C for the second argument must be equal to 6, unless the first argument is time. In case of a hysteresis function (IGRPCF=1, INUMCF=6) the second and third arguments point to the Tabular Function Data Base and the values of IARG1C for the second and third arguments must be equal to 6. Examples of the hysteresis functions are shown in section 2.8.11.

Acceptable range:  $1 \le |\text{IARG1C}| \le 9$ . Default value: none.

W-2 (I): IARG2C Second pointer for Control Function argument. This pointer defines the component number, which holds the data needed for Control Function argument. The following values should be used:

0	
IARG2C = CV number,	if $IARG1C = 1$ ,
IARG2C = JN number,	if IARG1C = $2$ ,
IARG2C = SC number,	if IARG1C = $3$ ,
IARG2C = TC number,	if IARG1C = 4,
IARG2C = TR number,	if IARG1C = 5,
IARG2C = TF number,	if IARG1C = $6$ ,
IARG2C = CF number or zero for RK,	if IARG1C = $7$ ,
IARG2C = CV, JN, SC, TC number, or 0,	if IARG1C = $8$ ,
IARG2C = not used,	if IARG1C = 9.
Acceptable range: must be a valid reference	e number, if non-zero.

Default value: none.

W-3 (I): IARG3C Third pointer for Control Function argument. This pointer defines the type of parameter (variable name). The values of IARG3C and their interpretation are shown in Table 2-23 through Table 2-32. Acceptable range:  $0 \leq IARG3C \leq 131$ ; if IARG1C=1.  $1 \leq IARG3C \leq 47;$ if IARG1C=2.  $0 \leq IARG3C \leq 43;$ if IARG1C=3.  $0 \leq IARG3C \leq 59;$ if IARG1C=4.  $1 \leq IARG3C \leq 8;$ if IARG1C=5, IARG3C = 1; if IARG1C=6,  $0 \leq IARG3C \leq 25$ : if IARG1C=7,  $1 \leq IARG3C \leq 323;$ if IARG1C=8.  $1 \leq IARG3C \leq 8;$ if IARG1C=9. Default value: none. W-4 (I): IARG4C Fourth pointer for Control Function argument. For example, if the Control Volume temperature is needed (IARG1C = 1, IARG3C = 14; see Table 2-23) then this pointer specifies whether the temperature of the atmosphere gas (IARG4C = 1), atmosphere droplets (=2), pool liquid (=3), or pool bubbles (=4), is used. If the Solid Heat Conductor Temperature is needed (IARG1C = 3, IARG3C = 16; see Table 2-23) then this pointer specifies the node number. The values of IARG4C, their interpretation and acceptable range, are shown in Table 2-23 through Table 2-32. Acceptable range: indicated in Table 2-23 through Table 2-32. Default value: none. W-5 (R): SCLACF Scaling factor for the CF argument. The value of the argument, defined

- by previous four integers, a(t), is multiplied by this factor. Acceptable range: all real numbers. Default value: 1.0 (a small number <10<sup>-50</sup>, sets the value to 0.0)
- W-6 (R): ADDACF Additive constant for the CF argument. The value of this constant is added to the calculated value of the argument. The argument value, used by the Control Function is:

 $Arg_i(t) = a_i(t) \cdot SCLACF_i + ADDACF_i$ 

*Acceptable range:* all real numbers. *Default value:* 0.0.

W-7 (I): I Argument number. If no value, or zero is entered, then the argument data are read sequentially - the first record in the input is interpreted as containing the first argument (I=1), then I=2, etc. Acceptable range:  $0 < I \le 100$ . Default value: none.

Additional pointers for the Radioactive Particle Transport Package

- W-8 (I): IARG5C Fifth pointer for Control Function argument. This pointer is used for some parameters in the Radioactive Particle Transport Package Table 2-28. For example, if the gravitational deposition velocity of aerosol particles is needed (IARG1C = 8, IARG3C = 53 or 74, see Table 2-28) then this pointer specifies the aerosol size section number. (Note that in this case the fourth pointer specifies the boundary cell number). The values of IARG5C, their interpretation and acceptable range, are shown in Table 2-28. *Acceptable range:* indicated in Table 2-28. *Default value:* none.
- W-9 (I) : IARG6C Sixth pointer for Control Function argument. This pointer is used for some parameters in the Radioactive Particle Transport Package Table 2-28. For example, if the deposited fractions in given  $F_a$ -section (adhesion force section) is needed (IARG1C = 8, IARG3C = 65 or 86, see Table 2-28) then this pointer specifies  $F_a$ -section number. (Note that in this case the fifth pointer specifies the aerosol size section number and the fourth pointer specifies the boundary cell number). The values of IARG6C, their interpretation and acceptable range, are shown in Table 2-28.

*Acceptable range:* indicated in Table 2-28. *Default value:* none.

Code name: CV

# Table 2-23 List of arguments available for Control Functions, variables available in Control Volume Data Base.

Pointer	rs 3, 4		Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
	1	Stratification data	-	
1		Density Stratification Parameter	CV-123- DSP-0000	T/E
2		Thermal Stratification Parameter	CV-123- TSP-0000	T/E
3		Pool Stratification Parameter	CV-123- PSP-0000	T/E
4	-	Atmosphere temperature, bottom of CV or pool surface. K	CV-123-Tatb-0000	T/E
5		Atmosphere temperature top of CV K	CV-123-Tatt-0000	1/1 1/F
6		Real temperature, bettem of CV K	CV-123-Tp1b-0000	1/13 T/17
7		Pool temperature, pool surface, K	CV-123-Tp1b-0000	1/E T/F
/		Pool cemperature, poor surface, K	CV-125-1p18-0000	1/15
0	1	Pool Sufface dat	CV 102 F-1- 0000	т / п
0		Yelesite (unreade) of the need conference (	CV-123-2p15-0000	1/1
9		Velocity (upwards) of the pool surface, m/s	CV-123-Vp18-0000	1/1
10	-	Area of the pool surface, m <sup>2</sup>	CV-123-Apis-0000	1/-
11		volumetric fraction of droplets at the pool surface	CV-123-Dp1s-0000	1/E
12		Volumetric fraction of bubbles at the pool surface	CV-123-Bp1s-0000	I/E
		Thermodynamic data		
13		Pressure, Pa	CV-123-Pres-atms	I/E
14		Temperature, K	CV-123-Temp-drop	I/E
15		Saturation temperature, K	CV-123-Tsat-pool	I/E
16	1=atms	Saturation pressure, Pa	CV-123-Psat-bubb	I/-
17	2=drop	Volumetric fraction of dispersed in continuous comp.	CV-123-VolF-atms	I/-
18	3=pool	Mass fraction of dispersed in continuous comp.	CV-123-MasF-drop	I/-
19	4=bubb	Volume, m <sup>3</sup>	CV-123-Volm-pool	I/E
20		Mass, kg	CV-123-Mass-atms	I/E
21		Total internal energy, J	CV-123-Enrg-drop	I/E
2.2		Vertical velocity (atms drop: down; pool bubb: up), m/s	CV-123-Vvrt-pool	T/E
23		Horizontal velocity, m/s	CV-123-Vhor-bubb	T/E
		Fluid property data		_/ _
24		Density m <sup>3</sup> /s	CV-123-Dens-atms	T/E
25		Specific internal energy J/kg	CV-123-SEpredrop	I/ =
26		Specific enthalpy J/kg	CV-123-Enth-pool	T/E
20	1	Viacocity kg/m/c	CV 123 Migg bubb	1/L T/
20	2-drop	Thermal conductivity W/m/K	CV-123-VISC-DUDD	I/- T/-
20	2=urop	Specific best at constant pressure of T/kg/K	CV-123-1COII-achis	1/- 1/E
20	J-pubb	Specific heat at constant pressure, cp, 0/kg/k	CV-123Cp-diop	1/E
21	4-DUDD	Dread the number	CV-123CV-p001	1/1
31		Prandul number		1/-
32		Thermal expansion coefficient, 1/K	CV-123-Beta-atms	1/-
33	1, 4	Diffusion coefficient, m <sup>2</sup> /s	CV-123-DifC-atms	I/-
34	2,3	Surface tension, N/m	CV-123-Sigm-drop	I/-
	1	Atmosphere and bubble gas data		
35		Atmosphere, mass of given gas, kg	CV-123Mag-H2	I/E
36	1=H <sub>2</sub>	Atmosphere, gas partial pressure, Pa	CV-123-PPag-He	I/-
37	2=He	Atmosphere, mass fraction of given gas	CV-123-CMag-H20_	I/E
38	3=H <sub>2</sub> O	Atmosphere, volume fraction of gas	CV-123-CVag-N2	I/E
39	4=N <sub>2</sub>	Bubbles, mass of given gas, kg	CV-123Mpg-02	I/E
40	5=O2	Bubbles, gas partial pressure, Pa	CV-123-PPpg-CO2_	I/-
41	6=CO2	Bubbles, mass fraction of given gas	СV-123-СМрд-Н2	I/E
42		Bubbles, volume fraction of gas	CV-123-CVpg-He	I/E
43	1=atms	Relative humidity	CV-123-RHum-atms	I/-
	2=bubb		CV-123-RHum-bubb	,
		Dispersed component - particle data (bubbles and dro	pplets)	I
11		Number of particles in a continuous component of a CV	CV-123-P No-drop	T/F
45	1=drop	Average position (bubb: from bottom drop: from top) m	CV-123-P Po-bubb	1/1 1/F
46	2=bubb	Average diameter of a single particle m	CV-123-P Di-drop	T/=
47	2-5400	Average volume of a single particle m <sup>3</sup>	CV-123-P Vo-bubb	±/- τ/-
4/	1	Average volume of a single particite, m	ddud-0v_123-F_v0-bubb	1/-
10	1	Mass sources - Junction source data	017 100 Mm TAT	τ /
40	1=atms	Total mass source from all UN into a CV, Kg/s	CV-123-WMJN-atms	1/-
49	2=drop	Enthalpy source associated with the mass source, J/s	CV-123-HmJN-drop	I/-
	3=pool			
	4=bubb			
50	consec	Diameter of created droplets, m	CV-123-DdJN-0001	I/-
51	JN	Diameter of created bubbles, m	CV-123-DbJN-0002	I/-
52	number	Droplet source strength, drop/s	CV-123-SdJN-0003	I/-
53	in CV	Bubble source strength, bubb/s	CV-123-Sb.TN-0004	т/-

#### Pointer 1: IARG1C = 1, Control Volume Data Base Pointer 2: IARG2C = CV reference number

#### continued.

Pointers 3, 4			Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		Mass source data - 1-D Solid Heat Conductor source	data	1 ' 1
54	1==+me	Total mass source from all SC mass transfer	CV-123-WmSC-atms	т/-
55	2=drop	(boiling condensation) in a CV kg/s	ev 125 Milbe dello	±7
55	3=pool	Enthalpy source associated with the mass source .I/s	CV-123-HmSC-drop	т/-
	4=bubb	Encharpy boarde abboarded with the water boarder, e, e	ov 120 mileo arop	- /
56	consoc	Diamotor of greated droplets m	CV-123-DdgC-0001	т/_
57	sc	Diameter of created hubbles m	CV-123-DbsC-0002	I/
58	number	Droplet source strength drop/s	CV-123-5d5C-0002	I/
59	in CV	Bubble source strength bubb/s	CV-123-SbSC-0004	I/-
33	111 01	Mass source data - Non-equilibrium mass transfer	data	1
60	1==+ms	Total mass source from all non-equilibrium processes	CV-123-WmNE-atms	т/-
61	2=drop	(flashing forging) in a CV kg/s	CV 125 WHINE ACHIS	1/
01	3=pool	Enthalpy source associated with the mass source . I/s	CV-123-HmNE-drop	т/-
	4=bubb	Encharpy source associated with the mass source, 0/s	ev izo innive drop	1/
62	1 5455	Diameter of created droplets m	CV-123-DdNE-0000	т/-
63	_	Diameter of created hubbles m	CV-123-DbNE-0000	I/
64		Droplet source strength drop/s	CV-123-SdNE-0000	I/-
65		Bubble source strength bubb/s	CV-123-SbNE-0000	I/
0.5		Mass source data - Inter-phase mass transfer da	CV 123 3DNE 0000	± /
6.6	1====	Mass source data - inter-phase mass transfer da	CV 122 NmTN atma	т / г
00	2=drop	(overage and an and an and an are processes,	CV-123-WILLIN-ACIUS	1/5
67	2-urop	(evaporation, condensation) in a CV, Kg/S	CV-123_UmtN dage	т /
0/	J-pool	Encharpy source associated with the mass source, J/S	Cv-123-nmin-arop	±/-
<u> </u>	4-DUDD	T-t	017 100 8 717 11	T / 5
68	1=p001	Inter-phase area, m-	CV-123-A_IN-p1>a	1/E T /
69	-atms	Mass flux at the inter-phase, Kg/s/m <sup>2</sup>	CV-123-W_IN-dp>a	1/-
70	2=arop	Heat flux at the inter-phase, W/m <sup>2</sup>	CV-123-QnIN-p1>b	1/-
/1	-atms	Enthalpy flux due to mass transfer, W/m2	CV-123-QmIN-p1>a	1/-
12	3=bubb	Liquid temperature at the inter-phase, K	CV-123-TIIN-dp>a	1/-
	-poo1			
		Mass source data - De-entrainment data		- /
73	1=atms	Total mass source from all de-entrainment processes,	CV-123-WmDE-atms	I/-
	2=drop	(droplet, bubble; vertical horizontal) in a CV, kg/s		- /
/4	3=pool	Enthalpy source associated with the mass source, J/s	CV-123-HmDE-drop	1/-
	4=bubb			- /
75	1=drop	Mass transfer fluxes from individual processes, kg/s	CV-123-WiDE-dp>v	I/-
	vert.			
	2=drop		CV-123-WiDE-dp>h	
	nor.		CH 100 H DE LLA	
	adua=c		CV-123-WIDE-DD>V	
	vert.	Maria and the main large and the		
7.6	1	Mass source data - Tabular mass sources	CTL 102 FL M2	<b>T</b> /
76	1=atms	Total mass source from all tabular mass sources	CV-123-WMMS-atms	1/-
	2=arop	in a CV, kg/s	and 100 m Ma 1	- /
//	3=pool	Enthalpy source associated with the mass source, J/s	CV-123-HmMS-drop	1/-
	4=bubb		and 100 p hts 0001	- /
/8	consec	Diameter of created droplets, m	CV-123-DdMS-0001	1/-
/9	source	Diameter of created bubbles, m	CV-123-DDMS-0002	1/-
80	number	Dropiel source strength, arop/s	CV-123-SdMS-0003	1/-
σ⊥	IN CV	Bubble source strength, bubb/s	CV-123-5DMS-0004	1/-
		Energy source data		- /
82	1	Total energy source due to convection from all SC, W	CV-123-Q_SC-atms	1/-
83	1=atms	Total energy source due to radiation from all SC, W	CV-123-Qrad-drop	I/-
84	2=drop	Total energy source due to inter-phase processes, W	CV-123-Q_IN-pool	1/-
85	3=pool	Total energy source for pool due to bubble collapse, W	CV-123-Qcol-bubb	I/-
86	4=bubb	Total energy source due to tabular energy sources, W	CV-123-Q_ES-atms	1/-
8.1	l	work, (p·dV/dt), W	CV-123-PdVT-drop	⊥/-
		Bubble collapse data for Junction flows		- /
88		Bubble Collapse time, s	CV-123-TCJN-0001	1/-
89	consec	Buddle flow time, s	CV-123-T±JN-0002	1/- T/
90	JN	POOL bypass fraction	CV-123-PsJN-0003	1/-
91	number	Heat transfer coefficient during bubble collapse, W/m <sup>2</sup> K	CV-123-HtJN-0004	1/-
92		Heat ILUX, W/m <sup>2</sup>	CV-123-QtJN-0005	⊥/-
	1	Bubble collapse data for Solid Heat Conductors		- 1
93		Bubble collapse time, s	CV-123-TcSC-0001	I/-
94	consec	Bubble flow time, s	CV-123-TfSC-0002	I/-
95	SC	Pool bypass fraction	CV-123-PsSC-0003	I/-
96	number	Heat transfer coefficient during bubble collapse, W/m <sup>2</sup> K	CV-123-HtSC-0004	I/-
97		Heat flux, W/m <sup>2</sup>	CV-123-QtSC-0005	I/-

continued.

Pointer	rs 3, 4		Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		Bubble collapse data for the tabular mass sourc	es	
98		Bubble collapse time, s	CV-123-TcMS-0001	I/-
99	consec	Bubble flow time, s	CV-123-TfMS-0002	I/-
100	source	Pool bypass fraction	CV-123-PsMS-0003	I/-
101	number	Heat transfer coefficient during bubble collapse, $\ensuremath{\mathbb{W}}\xspace/\ensuremath{\mathbb{W}}\xspace$	CV-123-HtMS-0004	I/-
102		Heat flux, W/m <sup>2</sup>	CV-123-QtMS-0005	I/-
		Summed quantities - individual gas masses (second pointer,	IARG2C=000)	
103	1=H2	Sum of masses of a given gas in the atmosphere	CV-000-MagT-H2	I/-
	2=He	of all CV in the model, kg	CV-000-MagT-He	
	3=H <sub>2</sub> O		CV-000-MagT-H20_	
104	4=N <sub>2</sub>	Sum of masses of a given gas in the pool bubbles	CV-000-MpgT-N2	I/-
	5=0 <sub>2</sub>	of all CV in the model, kg	CV-000-MpgT-02	
	6=CO <sub>2</sub>		CV-000-MpgT-CO2_	
		Summed quantities - component data (second pointer, IA	RG2C=000)	
105	1=atms	Sum of the volumes occupied by a given component in all	CV-000-VolT-atms	I/-
	2=drop	CV in the model, m <sup>3</sup>		
106	3=pool	Sum of the masses of a given component in all CV, kg	CV-000-MasT-drop	I/-
107	4=bubb	Sum of the energies of a given component in all CV, kg	CV-000-EnrT-pool	I/-
	1	Summed quantities - overall data (second pointer, IAR	G2C=000)	
108		Sum of the volumes occupied by all components in all CV	CV-000-VolX-0000	I/-
		in the model, m <sup>3</sup>		- /
109		Sum of the masses of all components in all CV, kg	CV-000-MasX-0000	I/-
110	-	Sum of the energies of all components in all CV, kg	CV-000-EnrX-0000	I/-
111		Mass error, kg	CV-000-ErrM-0000	I/-
112		Energy error, J	CV-000-ErrE-0000	1/-
		Hydrogen burn data		- /
113		Igniter temperature, K	CV-123-Tign-0000	1/-
114		Maximum temperature of all structures present in CV, K	CV-123-Twa1-0000	1/-
115		Gas temperature, K	CV-123-Tgas-0000	1/-
117		Gas Velocity, m/s	CV-123-Vgas-0000	1/-
11/		Gas findimability,	CV-123-F1am-0000	1/-
		1 = slow deflagration expected if ignited		
		2 = FTD expected		
		3 = detonation expected		
118	-	Burn mode.	CV-123-Burn-0000	T/E
110		0 = no burn	ov ilo bain oooo	1/2
		1 = slow deflagration in progress		
		2 = FTD in progress		
		3 = detonation in progress		
119		Flame velocity, m/s	CV-123-Vflm-0000	I/E
120		H <sub>2</sub> consumption rate, kg/s	CV-123- mH2-0000	I/-
121		O2 consumption rate, kg/s	CV-123-mO2-0000	I/-
122		H <sub>2</sub> O production rate, kg/s	CV-123-mH2O-0000	I/-
123		Heat produced due to burn, W	CV-123-Qbrn-0000	I/-
124		Time of start of burn (zero if no burn), s	CV-123-Tbrn-0000	I/-
125		Length flame has propagated since start of burn, m	CV-123-Prop-0000	I/-
126		$H_2$ fraction expected at the end of the burn	CV-123-Feob-0000	I/-
127		Shock wave pressure, Pa	CV-123-PshW-0000	I/-
128		Critical elevation (stratified volumes)	CV-123-Zcrt-0000	I/-
	1=H2		CV-123-Ccrt-H2	
	2=He		CV-123-Ccrt-He	
129	3=H <sub>2</sub> O	Gas volume fractions at the critical elevation	CV-123-Ccrt-H20_	I/-
	4=N <sub>2</sub>		CV-123-Ccrt-N2	
	5=0 <sub>2</sub>		CV-123-Ccrt-02	
	6=CO2		CV-123-Ccrt-CO2_	
		Oxidation data		- 1
130	1=H2	Mass source due to oxidation reactions in a CV, kg/s	CV-123-WmOX-H2	I/-
	2=He		CV-123-WmOX-He	
101	3=H <sub>2</sub> O		CV-123-WmOX-H20_	<b>T</b> (
131	4=N2	specific enthalpy of oxidizing gases, J/kg	CV-123-HMOX-N2	1/-
	5=0 <sub>2</sub>		CV-123-HMUX-U2	
1	0-002		UV-IZ3-MINUX-UUZ	

Code name: CV

Code name: three digits

continued - Homogeneous Control Volumes

Pointe	rs 3, 4		Code Name	
IARG3C	IARG4C	Description	Example	Impl/Expl
	•	Stratification data	•	•
		Thermodynamic data		
13	3	Volume center pressure, Pa	CV-123-Pres-pool	I/E
17	1	Void fraction, -, (volume fraction of gas)	CV-123-VolF-atms	I/-
18	1	Mass fraction of gas, -	CV-123-MasF-atms	I/-
14		Temperature, K	CV-123-Temp-atms	I/E
15		Saturation temperature, K	CV-123-Tsat-pool	I/E
16		Saturation pressure, Pa	CV-123-Psat-atms	I/-
10	1=gas	Volume, m <sup>3</sup>	CV-123-Volm-pool	I/E
19	3=liq	Mass, kg	CV-123-Mass-atms	I/E
20		Total internal energy, J	CV-123-Enrg-pool	I/E
21		Vertical velocity (gas down; pool bubb: up), m/s	CV-123-Vvrt-atms	I/E
22		Horizontal velocity, m/s	CV-123-Vhor-pool	I/E
23				
		Fluid property data	÷	
24		Density, m <sup>3</sup> /s	CV-123-Dens-atms	I/E
25		Specific internal energy, J/kg	CV-123-SEnr-pool	I/-
2.6		Specific enthalpy, J/kg	CV-123-Enth-atms	I/E
27	1=gas	Viscosity, kg/m/s	CV-123-Visc-pool	I/-
27	3=liq	Thermal conductivity, W/m/K	CV-123-Tcon-atms	I/-
28		Specific heat at constant pressure, cp, J/kg/K	CV-123Cp-pool	I/E
29		Specific heat at constant volume, cv J/kg/K	CV-123Cv-atms	I/E
30		Prandtl number	CV-123Pr-pool	I/-
31		Thermal expansion coefficient, 1/K	CV-123-Beta-atms	1/-
32				
33	1=gas	Diffusion coefficient, m <sup>2</sup> /s	CV-123-DifC-atms	I/-
34	3=liq	Surface tension, N/m	CV-123-Sigm-pool	I/-

Pointer 1: IARG1C = 1, Control Volume Data Base Pointer 2: IARG2C = CV reference number

Other parameters (IARG3C > 35) are available as for heterogeneous Control Volumes but only parameters with the suffixes: -atms and -pool are available, with -atms meaning the gas phase and -pool meaning the liquid phase. Parameters with the suffixes: -bubb -drop are not available, except for bubble or droplet diameter and volume, CV-xxx-P\_Di-bubb, CV-xxx-P\_Di-drop, CV-xxx-P\_Vo-bubb, CV-xxx-P\_Vo-drop.

Apart from the -bubb -drop, the following plot parameters are not available and should not be used for the homogeneous CV:

Volume fraction of liquid	CV-xxx-VolF-pool	(use:	1.0 -	CV-xxx-VolF-atms)
Mass fraction of liquid	CV-xxx-MasF-pool	(use:	1.0 -	CV-xxx-MasF-atms)

The pool level can be used. It gives the collapsed liquid level in a homogeneous CV:

```
Pool level: CV-xxx-Zpls-0000 collapsed liquid level.
```

The volume-center Control Volume pressure is available as the plot parameter: CV-XXX-Pres-pool. The plot parameter: CV-XXX-Pres-atms gives the pressure at the collapsed liquid level in CV (in a gas-filled CV this is the pressure at the CV bottom; in a liquid-filled CV this is the pressure at the CV top).

#### Table 2-24 List of arguments available for Control Functions, variables available in Junction Data Base.

Pointer 1: IARG1C = 2, Junction Data Base Code name: JN

Pointer 2: IARG2C = JN reference number Code name: three digits Pointers 3, 4 Code Name Description Examples Impl/Expl TARG3C TARG4C Component data JN-234-Velo-atms Velocity, m/s I/E 2 Mass flow, kg/s JN-234-Flow-drop I/E 3 1=atms Flow area, m<sup>2</sup> JN-234-Area-pool I/E 4 2=drop Temperature, K JN-234-Temp-bubb I/-3=pool Density, kg/m<sup>3</sup> JN-234-Dens-atms I/-5 I/-6 4=bubb Specific enthalpy, J/kg JN-234-Enth-drop JN-234-\_\_Cv-pool JN-234-\_\_Cp-bubb . I/-Specific heat at constant pressure,  $c_p$ , J/kg/K т/-Specific heat at constant volume, cv J/kg/K 8 Gas composition data 1=H2 Atmosphere gas - mass fraction of given gas JN-234-CMag-H2 I/-9 10 2=Не Atmosphere gas - volume fraction of given gas JN-234-CVag-He I/-JN-234-CMpg-H20\_ 11 3=H<sub>2</sub>O Pool bubbles - mass fraction of given gas Pool bubbles - volume fraction of given gas I/-12  $4=N_2$ JN-234-CVpg-N2\_ т/-5=02 6=C0 Overall data Flow area of gas (atmosphere + bubbles), ma JN-234-Agas-0000 I/-13 14 Flow area of liquid (pool + droplets), ma JN-234-Aliq-0000 . I/-I/E 15 Total flow area, m<sup>2</sup> JN-234-Area-0000 16 Mass flow of gas (atmosphere + bubbles), kg/s JN-234-Wgas-0000 I/-17 Mass flow of liquid (pool + droplets), kg/s JN-234-Wliq-0000 т/-I/-18 JN-234-Wtot-0000 Total mass flow, kg/s Average enthalpy of gas (atmosphere & bubbles), J/kg Average enthalpy of liquid (pool & droplets), J/kg JN-234-Hgas-0000 I/-19 I/-20 JN-234-Hliq-0000 JN-234-Htot-0000 21 Average enthalpy of fluid (gas & liquid), J/kg I/-22 Average velocity of gas (atmosphere & bubbles), m/s JN-234-Vgas-0000 I/т/-23 Average velocity of liquid (pool & droplets), m/s JN-234-Vliq-0000 JN-234-Cgas-H2\_\_\_ 24 1=H\_ Average gas composition (atmosphere & bubbles) I/-JN-234-Cgas-He т/-2=He NOTE . JN-234-Cgas-H20 I/-3=H<sub>2</sub>O If diffusion parameters are requested (input record 256000, LDIFJN=2), then this parameter is replaced by: I/- $4=N_2$ JN-234-Cgas-N2 Volume transfer rate due to diffusion, m<sup>3</sup>/s, e.g.: 5=02 JN-234-Cgas-02 I/-6=CO<sub>2</sub> JN-234-VDif-H2 JN-234-Cgas-CO2 I/-Valve data 25 Fraction open JN-234-FrOp-0000 I/-Critical flow data JN-234-\_ICF-0000 JN-234-Gcrt-0000 26 Critical flow indicator т/-I/-Critical mass flux, kg/m<sup>2</sup>/s 27 Atmosphere and pool data Pressure at JN elevation, upstream (from) CV, Pa JN-234-\_P-F-atms 28 T/E JN-234-P-T-pool JN-234-Re-atms JN-234-ff-pool 29 1=atms Pressure at JN elevation, downstream (to) CV, Pa T/E 30 Reynolds number I/-2=pool 31 Wall friction factor I/-JN-234 \_\_\_\_\_ poor JN-234\_Kfac-atms 32 Form loss factor (K-factor), (-) I/-JN-234-Zpol-0000 33 Pool level in JN, m I/-Ratio of  $c_{\rm p}/c_{\nu}$  for gas (atmosphere & bubbles) 34 JN-234-CpCv-0000 I/-I/-35 Density of gas (atmosphere & bubbles),  $kg/m^3$ JN-234-Rgas-0000 Pump/compressor/turbine data 36 Pump/compressor/turbine speed, rev/s JN-234-PSpd-atms т/-JN-234-PVF1-pool I/E 37 Pump/compressor/turbine volumetric flow, m3/s Pump/compressor/turbine pressure ratio JN-234-PRpr-atms 38 1=atms I/E Pump/compressor/turbine pressure head, Pa 39 2=pool JN-234-PHef-pool I/-40 Pump/compressor/turbine degradation factor (surge) JN-234-PHdf-atms I/-41 Pump/compressor/turbine efficiency JN-234-PEff-pool I/E 42 Pump/compressor/turbine power into fluid, W JN-234-QPmp-atms T/E 43 Pump/compressor/turbine total power into fluid, W JN-234-QPmp-0000 T/E Pump/compressor/turbine friction power, =4 $\pi^2 \, C_F \omega^2$ , W Pump/compressor/turbine fluid plus friction power, W JN-234-Qfrp-0000 44 I/-JN-234-OPfp-0000 т/-45 JN-234-Vred-atms 46 1=atms Reduced flow divided by a function of reduced speed: I/-2=pool  $V_R / (\omega_R^{a-b})^{1/c}$ , JN-234-Vred-pool I/-Friction pressure loss + Local pressure loss Single phase pressure loss (friction + local), [Pa] dP(f+K) = (K + fL/D) ( $\rho v^2/2$ ) JN-234-DPfr-atms 47 1=atms I/-

2=pool

I/-

JN-234-DPfr-pool

#### Table 2-25 List of arguments available for Control Functions, variables available in 1-D Solid Heat Conductor Data Base.

#### Pointer 1: IARG1C = 3, 1-D Solid Heat Conductor Data Base Code name: SC

Pointer 2: IARG2C = SC reference number Code name: three digits

Pointe	ers 3, 4		Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		SC aumface data	1 1	1, 1
		SC Sufface data	T	
1	-1=left	Fraction of the surface immersed in the pool of a CV	SC-345-Pool-left	I/-
	+1=right			
2	coll No	Internal beat generation W in a coll of a single SC	SC-345-0co1-0001	т/_
2	CEIL NO	internal heat generation, w, in a ceri of a single sc	SC-343-QCE1-0001	1/-
	or O	or total SC (including multiplicity) when IARG4C=0		
		If IQPLSC=2, power density (W/m <sup>3</sup> ) (SC-345-qcel-0001)		
		Fluid data at SC surfaces	•	
-	10 3 51		22 045 EC1 1 1	= /
3	<u=leit< td=""><td>Fluid temperature, K</td><td>SC-345-TILd-1-at</td><td>1/-</td></u=leit<>	Fluid temperature, K	SC-345-TILd-1-at	1/-
4	>0=right	Heat transfer coefficient, W/m <sup>2</sup> /K (for fins->19)	SC-345- HTC-1-pl	I/-
5	1 =atms	Convective heat flux, W/m <sup>2</sup> (for fins->20)	SC-345-Fcnv-l-rp	I/-
6	121-2001	Convective best W (total including multiplicity)	SC-345-Ocpuration	_, /_
0	121-poor	convective heat, w (cotal, including multiplicity)	SC-545-QCIIV-I-at	1/-
7	3 =repr	Fluid velocity, m/s (only  1  and  2  for IARG4C)	SC-345-Vfld-r-pl	I/-
		Thermal radiation data		
8	-1=1oft	Padiative heat flux W/m2	SC-345-Erad-left	т/-
0	I-ICIC	Radiacive heat fits, w/m	SC 545 FIAG TELC	± /
9	+l=right	Radiative heat, W (total, including multiplicity)	SC-345-Qrad-righ	1/-
		Local gas or particle concentrations at the SC su	rface	
10	<0=loft	Volume fraction of gas or particle type	SC-345-Vfrc-H2 1	T/F
10	<pre>&gt;U-IEIC</pre>	Volume fraction of gas of particle type	3C-343-VIIC-H2_1	1/15
	>0=right		SC-345-Virc-H201	
	1   =H <sub>2</sub>		SC-345-Vfrc-C021	
1	121-40		SC=345=Vfro=dp 1	1
	121-ne		50-345-VIIC-up.1	
	3   =H <sub>2</sub> O		SC-345-Vfrc-bb.1	
11	$ 4  = N_2$	Mass fraction of gas or particle type	SC-345-Mfrc-H2 r	I/E
	151-0-	The second	SC-345-Mfro-420~	, –
	101-02		SC-345-MLLC=HZOF	
	6   =CO <sub>2</sub>		SC-345-Mfrc-CO2r	
	7 =drop		SC-345-Mfrc-dp.r	
	191-bubb		SC-345-Mfra-bb r	
	101-0000		3C-343-MIIC-DD.I	
		Condensation and boiling data		
12		Condensate film thickness, m	SC-345-Dcnd-left	I/-
13	-1-1oft	Critical beat flux W/m2	SC-345-CUE-righ	т/_
13	-I-IEIC	Cifcical fieat fiux, w/m	SC-545-qCHF-LIGH	1/-
14	+1=right	Condensation mass transfer rate, kg/m <sup>2</sup> /s	SC-345-Mcnd-left	I/-
1.5		Boiling mass transfer rate, kg/m <sup>2</sup> /s	SC-345-Mboi-righ	т/-
		Mach call data	00 010 1.000 g.:	= /
		Mesh Celi Gata	I	· · ·
16	cell No.	Cell temperature, K	SC-345-Tcel-0001	I/E
	or O	or volume-averaged SC temperature when IARG4C=0		
	•	Extended surfaces (fins, spines) data		
1.0			22 045 DCCD 1	= /
1/		Efficiency of fins	SC-345-EffF-1-at	1/-
18	<0=left	Enhancement of heat & mass transfer due to fins	SC-345-EnhF-1-pl	I/-
19	>0=right	True heat transfer coefficient $W/m^2/K$ (do not use 4)	SC-345-HTCE-r-at	т/-
10	>0 right	The heat film of (2)		± /
20	1 =atms	True neat ILUX, W/M <sup>2</sup> (do not use 5)	SC-345-qcnF-r-pl	1/-
21	2 =pool	True mass flux, kg/m <sup>2</sup> /s	SC-345-MmtF-1-at	I/-
22	-	True enthalow flux due to mass flux $W/m^2$	SC-345-Hmt F-1-p1	т/-
22		The chemistry flaw due to made find, w/m	CC 245 mfin n st	± /
23		Fin average temperature based on fin efficiency, K	SC-345-TIIN-r-at	1/-
		Summed quantities (second pointer, IARG2C=000	)	
24		Sum of convective heat of all SC. W	SC-000-0cnS-0000	т/-
25		Sum of integrated convective best of all SC T	SC-000-0227 0000	_ / T /
20		Sum of integrated convective near of all SC, J	3C-000-QCH1-0000	±/_
26	-	Sum of radiative heat of all SC, W	SC-000-QrdS-0000	I/-
27		Sum of integrated radiative heat of all SC. J	SC-000-0rdT-0000	т/-
20		Sum of convective + radiative best of all CC M	8C-000-0++9 0000	_ / _ /
20		Sum of convective + fautacive field of dif Sc, W		±/-
29		Sum of integrated convective+radiative heat all SC, W	SC-000-QttI-0000	I/-
		Oxidation data		
30		Thickness of the un-ovidized material m	SC-3/5-VM+1-1of+	т /г
20		michield of the un original material, m	SC 345 MACT-TELL	1/10 7/10
31		Thickness of the oxide layer, m	SC-345-XOxd-righ	⊥/E
32	-1=left	Total gas consumption rate due to oxidation, kg/m <sup>2</sup> /s	SC-345-W1OX-left	I/-
	+1=right	(for multiple reactions sum of all reacting gases)	1	
22	·	matel are presention water 1 (22/)	CO SAE MOON ST	<b>T</b> /
33		TOLAL gas generation rate, kg/m²/s	SC-345-W2OX-righ	⊥/-
		(for multiple reactions sum of all produced gases)	1	
34		Total heat generation due to oxidation reactions $W/m^2$	SC-345-Ooxi-left	т/-
51	1	Total hour generation due to okidation reactions, w/m	L SS SIS YOAT TELL	± /
		Fallure data (or graphite ignition parameters - see	(wolea	
35		Cumulative damage, (-)	SC-345-CDam-0000	I/E
36	_	Time to failure (s)	SC-345-T+E1-0000	т/_
50			SC 345 F 10000	±/-=
37		Failure mode, (-) (1=u.strength, 2=creep, 3=meltdown)	SC-345-Fail-0000	I/-
38		Time of failue (if occurred, zero otherwise)	SC-345-ToF1-0000	I/-
	•	Gan data		
2.0		Gap data	00.045 0.0000	<b>T</b> /
39		Gap thickness, (m)	SC-345-xGap-0000	⊥/-
40	-	Gap conductance, (W/m <sup>2</sup> -K)	SC-345-hGap-0000	I/-
41		Can left (fuel outer surface) temperature (K)	SC-345-Tfuo-0000	т/_
41		Gap fere (fuer outer sufface) temperature (K)	5C-345-1100-0000	±/-
42		Gap right (clad inner surface) temperature (K)	SC-345-Tcld-0000	1/-
		BDC data		
10	_1_1_f+	PDC host flux W/m2	8C-345-~PDC 1of+	т /
43	-i-terc	DDC HEAC IIUX, W/HT	SC-S42-JRDC-TELL	1/-
1	1 = mi ab +		1	1

Notes:

(1) For IARG3C = 3 through 6 the user can request three values

- atmosphere
- pool
- representative

Definition of the representative values is provided in Volume 1, section: "Representative Boundary Conditions". The representative values are recommended for general use. In the case of 2-D Solid Heat Conductors only the representative values are available for IARG3C = 3 through 6.

(2) If the graphite oxidation model of Roes is used (IOXLSC/IOXRSC=-5), the graphite ignition criterion is calculated from the correlation shown in Volume 1. In such case the ignition parameters may be plotted using IARG3C = 35 through 38. This is possible only if the failure model is not simultaneously used. In such case the plot parameters are defined as follows:

	Graphite ignition parameters				
35		Ignition temperature (K), left surface	SC-345-CDam-0000	I/E	
36	-	Time when the ignition temperature was exceeded (s)	SC-345-TtF1-0000	I/-	
37		Ignition temperature (K), right surface	SC-345-Fail-0000	I/-	
38		Time when the ignition temperature was exceeded (s)	SC-345-ToF1-0000	I/-	

#### Table 2-26 List of arguments available for Control Functions, variables available in 2-D Solid Heat Conductor Data Base.

#### Pointer 1: IARG1C = 4, 2-D Solid Heat Conductor Data Base Code name: TC

Pointer 2: IARG2C = TC reference number Code name: three digits

Pointers 3, 4			Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		TC surface (boundary cell) data	-	
1	boundary	Fraction of the surface immersed in the pool of a CV	TC-456-Pool-0001	I/-
	cell No.			I/-
2	cell No	Internal heat generation. W. in a cell of a single TC	TC-456-0ce1-0001	т/-
-	or 0	or total TC (including multiplicity) when IARG4C=0	10 100 2001 0001	- /
	01 0	If $TOPLTC=2$ , power density ( $W/m^3$ ) (TC-456-gcel-0001)		
		Fluid data at TC surfaces (boundary cells)		
3		Fluid temperature K	TC-456-Tfld-0001	т/-
4	boundary	Heat transfer coefficient W/m <sup>2</sup> /K	TC-456- HTC-0002	I/ T/-
5	cell No	Convective heat flux W/m <sup>2</sup>	TC-456-Ecov-0003	I/ T/-
6	CEII NO.	Convective heat W (total including multiplicity)	TC-456-0cpv-0004	I/ T/-
7		Eluid vologity m/s	TC-456-Vf1d-0005	±/
/		Thermal radiation data at TC surfaces (houndary of	10-430-0110-0003	1/-
<u>^</u>	, ,	Thermal radiation data at it surfaces (boundary ce		- /
8	boundary	Radiative heat flux, W/m <sup>2</sup>	TC-456-Frad-0001	1/-
9	CEII NO.	Radiative neat, w (total, including multiplicity)	TC-456-Qrad-0002	1/-
		Local steam concentrations at the TC surfaces (boundar	ry cells)	_ /_
10	boundary	Volume fraction of steam at the boundary cell surface	TC-456-Vfrc-0001	I/E
11	cell No.	Mass fraction of steam at the boundary cell surface	TC-456-Mirc-0002	1/E
		Condensation and boiling data at TC surfaces (boundar	y cells)	
12		Condensate film thickness, m	TC-456-Dcnd-0001	I/-
13	boundary	Critical heat flux, W/m <sup>2</sup>	TC-456-qCHF-0002	I/-
14	cell No.	Condensation mass transfer rate, kg/m <sup>2</sup> /s	TC-456-Mcnd-0003	I/-
15		Boiling mass transfer rate, kg/m²/s	TC-456-Mboi-0004	I/-
		Mesh cell data		
16	cell No.	Cell temperature, K (*)	TC-456-Tcel-0001	I/E
	or O	or volume-averaged SC temperature when IARG4C=0		
		Summed quantities (second pointer, IARG2C=000)	)	
17		Sum of convective heat of all TC, W	TC-000-QcnT-0000	I/-
18		Sum of integrated convective heat of all TC, J	TC-000-QcnI-0000	I/-
19	-	Sum of radiative heat of all TC, W	TC-000-QrdT-0000	I/-
20		Sum of integrated radiative heat of all TC, J	TC-000-QrdI-0000	I/-
21		Sum of convective + radiative heat of all TC, W	TC-000-QttT-0000	I/-
22		Sum of integrated convective+radiative heat all TC, W	TC-000-QttI-0000	I/-
		Oxidation data at TC surfaces (boundary cells)	)	
23		Thickness of the un-oxidized material, m	TC-456-XMtl-0001	I/E
24		Thickness of the oxide layer, m	TC-456-X0xd-0002	I/E
25	boundary	Total gas consumption rate due to oxidation, kg/m <sup>2</sup> /s	TC-456-W1OX-0003	I/-
	cell No.	(for multiple reactions sum of all reacting gases)		
26		Total gas generation rate, kg/m <sup>2</sup> /s	TC-456-W2OX-0004	I/-
		(for multiple reactions sum of all produced gases)		
27		Total heat generation due to oxidation reactions, $W/m^2$	TC-456-Qoxi-0005	I/-
		Failure data		
28		Cumulative damage, (-)	TC-456-CDam-0000	I/E
29	-	Time to failure, (s)	TC-456-TtF1-0000	I/-
30		Failure mode, (-) (1=u.strength, 2=creep, 3=meltdown)	TC-456-Fail-0000	I/-
31		Time of failue (if occurred, zero otherwise)	TC-456-ToF1-0000	I/-
		Gap data		
32		Gap thickness, (m)	TC-456-xGap-0001	I/-
33	axial	Gap conductance, (W/m <sup>2</sup> -K)	TC-456-hGap-0002	I/-
34	level No	Fuel surface (gap left) temperature (K)	TC-456-Tfue-0003	I/-
35		Cladding surface (gap right) temperature (K)	TC-456-Tcld-0004	I/-
		BDC data		
36	boundary	BDC heat flux, W/m <sup>2</sup>	TC-456-qBDC-0001	I/-
	cell No.		_	

(\*) Note: in the case of cell temperatures (IARG3C=16), the cell numbers are as follows.

For plotting: *xxyy*, where *xx* is the column number and *yy* is the row number.

- For Control Functions: internal cell number printed in the \*.OUT file, e.g.:

=TC= TC-100, CELL NUMBERING MAP

In this example, the cell number 26 has the plotting number (in the \*.PLT file) of 0603.

continued

Pointers 3,4			Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
	·	·	•	
		MCCI data ( <b>MC</b> )		
	The sec	ond pointer must refer to the first TC in the model if m	ore TCs are present	
		MCCI data per cell		_ /_
37		X-velocities, (m/s)	TC-456-VelX-0001	1/E 7/D
38		Y-velocities, (m/s)	TC-456-VelY-0001	1/E
39		Porosity of the cell, (-)	TC-456-Poro-0001	1/E
40	cell No.	Concrete fraction in a cell, (-)	TC-456-XCon-0001	1/E
41		Corium fraction in a cell, (-)	TC-456-XCor-0002	1/-
42		Liquid fraction in a cell, (-)	TC-456-XL1q-0003	1/-
43		Ablated fraction in a cell, (-)	TC-456-XAb1-0004	I/E
		Metals in corium	1	
44		Total mass of metals in corium (kg)	TC-456-MMet-0000	I/E
45		Total mass of Fe in corium (kg)	TC-456-MMFe-0000	I/E
46	0	Total mass of Cr in corium (kg)	TC-456-MMCr-0000	I/E
47		Total mass of Ni in corium (kg)	TC-456-MMNi-0000	I/E
48	<u> </u>	Total mass of Zr in corium (kg)	TC-456-MMZr-0000	I/E
		Concrete ablation		
49	-	Volume of ablated concrete (m <sup>3</sup> )	TC-456-VAb1-0000	I/E
50		Mass of ablated concrete (kg)	TC-456-MAbl-0000	I/E
		Gas release due to MCCI		
51		Total mass of H <sub>2</sub> O released, (kg)	TC-456-MH2O-0000	I/E
52		Total mass of H <sub>2</sub> released, (kg)	TC-456-MH20000	I/E
53	-	Total mass of CO <sub>2</sub> released, (kg)	TC-456-MCO2-0000	I/E
54		Total mass of CO released, (kg)	TC-456-MCO0000	I/E
55		Release rate of $H_2O$ , (kg/s)	TC-456-RH2O-0000	I/E
56		Release rate of H <sub>2</sub> , (kg/s)	TC-456-RH2 -0000	I/E
57	-	Release rate of CO <sub>2</sub> , (kg/s)	TC-456-RC02-0000	I/E
58		Release rate of CO, (kg/s)	TC-456-RCO0000	I/E
			_	
		Heating data		
59	-	Heating rate by chemical reactions, (W)	TC-456-QChe-0000	I/E
60		Power used for concrete ablation, (W)	TC-456-QAbl-0000	I/E
61		Integrated heating rate by chemical reactions, (J)	TC-456-EChe-0000	I/E
62		Integrated power used for concrete ablation, (J)	TC-456-EAbl-0000	I/E
		Maximum ablation data (m)		
63	-	Maximum ablation in radial (horizontal)direction, (m)	TC-456-RAbl-0000	I/-
64		Maximum ablation in axial (vertical)direction, (m)	TC-456-ZAb1-0000	I/-
		Concrete and corium masses and volumes		<u> </u>
65		Total volume of concrete, (m <sup>3</sup> )	TC-456-VCon-0000	I/-
66		Total mass of concrete, (kg)	TC-456-MCon-0000	I/-
67		Total volume of corium, (m <sup>3</sup> )	TC-456-VCor-0000	I/-
68		Total mass of corium, (kg)	TC-456-MCor-0000	I/-
69		Total volume of concrete lost due to de-gassing, (m <sup>3</sup> )	TC-456-VGas-0000	I/-
70		Total mass of concrete lost due to de-gassing, (kg)	TC-456-MGas-0000	I/E
71		Total volume of corium increase to oxidation, (m <sup>3</sup> )	TC-456-VOxi-0000	I/-
72		Total mass of corium increase to oxidation, (kg)	TC-456-MOxi-0000	I/E

# Table 2-27 List of arguments available for Control Functions, variables available in Thermal Radiation Data Base.

Pointer 1:	IARG1C =	5, Thermal Radiation Data Base Code name:	TR		
Pointer 2:	IARG2C = 1	IR system No. / surface reference No. Code name:	one	digit / two digits	
Pointe	ers 3, 4			Code Name	
IARG3C	IARG4C	Description		Examples	Impl/Expl
		TR surface data			
1		Surface temperature, K		TR-511-Tsrf-0000	I/-
2	-	Surface emissivity		TR-512-Esrf-0000	I/-
3		Radiative heat flux, W/m <sup>2</sup>		TR-513-Fsrf-0000	I/-
4		Radiative heat, W		TR-514-Qsrf-0000	I/-
		Gas radiative properties			
5	j=other	Gas emissivity from current (511) to j (512) sur	face	TR-511-Egas-0512	I/-
6	surface	Gas absorptivity from current (513) to j (514) s	urf.	TR-513-Agas-0514	I/-
7	j=above	Gas emissivity from (511) to (512) through CV 01		TR-511-Eg01-0512	I/-
8	IARG5C:	Gas absorptivity from (513) to (514) through CV	02	TR-513-Ag02-0514	I/-
	CV path				

#### Table 2-28 List of arguments available for Control Functions, variables available in Radioactive Particle Transport Data Base.

Pointer 1:IARG1C = 8, Radioactive P. Transport Data BaseCode name:RT (IARG1C=CV/JN/SC/TC/RT)Pointer 2:IARG2C = CV, JN, SC, or TC reference numberCode name:three digits

Pointe	ers 3, 4		Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
	PART I - AEROSOL DATA					
		Control Volume related data ( <b>CV</b> )				
Keep	in mind th	hat although these are CV related parameters, the pointer IARGIC=8	1 is equal to 8 an	d not 1		
	Airborne aerosols and aerosols suspended in the CV pool - sources and masses					
1		External (TF/CF) source of airborne aerosols, (kg/s)	CV-123-ASEm-0001	I/-		
2		External (TE/CE) source of airborne aer (part/m <sup>3</sup> -s)	CV-123-ASED-0002	т/-		
3		Release source of airborne aerosols (kg/s)	CV-123-ASBm-0003	т/-		
4		Release source of airborne aerosols $(ngrt/m^3-g)$	CV-123-ASPD-0004	т/-		
		Nerease source of arround due to all TN flows (kg/s)	CV-123-ASRP-0004	1/- T/		
S		Airborne aerosof source due to air on flows, (kg/s)	CV-123-ASJIII-0003	1/-		
6		Airborne aer. source due to all JN flows, (part/m <sup>3</sup> -s)	CV-123-ASJP-0001	1/-		
7	Size	External (TF/CF) source of pool aerosols, (kg/s)	CV-123-PSEm-0002	I/-		
8	section	External (TF/CF) source of pool aerosols, (part/m <sup>3</sup> -s)	CV-123-PSEp-0003	I/-		
9	number	Release source of pool aerosols, (kg/s)	CV-123-PSRm-0004	т/-		
10		Release source of pool aerosols. $(n_3, r_3, r_3)$	CV-123-PSBp-0005	т/-		
11		Pool aerosol source due to all JN flows $(ka/s)$	CV-123-PS.Tm-0001	т/-		
12		Pool acrosol source due to all IN flows, $(ng/s)^{-1}$	CV-123-PS TD-0002	I/_		
12		rooi aerosor source due to air on riows, (part/m-s)	CV-125-F50P-0002	1/-		
13		Airborne aerosol mass, (kg)	CV-123-Maer-0003	I/E		
14		Airborne aerosol density, (part/m3)	CV-123-Daer-0004	I/E		
15		Airborne aerosol heat source (W)	CV-123-0aer-0005	I/-		
16		Airborne aerosol activity, (Bg)	CV-123-Aaer-0001	I/-		
		Airborne aerosols - data summed for all size sect	ions			
17		Airborne aerosol mass, all size sections, (kg)	CV-123-SMae-0000	I/-		
18	-	Airborne aerosol density, all size sections (part/m3)	CV-123-SDae-0000	I/E		
19		Airborne aerosol heat source, all size sections, (W)	CV-123-SOae-0000	I/-		
20		Airborne aerosol activity, all size sections, (Bg)	CV-123-SAae-0000	I/-		
		Deposition and resuspension data for CV pool sur:	face			
21		Deposition velocity, gravitational, (m/s)	CV-123-VdgP-0001	I/-		
22		Deposition velocity, Brownian, (m/s)	CV-123-VdbP-0002	I/-		
23		Deposition velocity, thermophoretic, (m/s)	CV-123-VdtP-0003	I/-		
2.4		Deposition velocity, diffusiophoretic, (m/s)	CV-123-VddP-0004	т/-		
25		Deposition velocity turbulent impaction (m/s)	CV-123-VdiP-0005	т/-		
26		Deposition velocity, effective (m/s)	CV-123-VdeP-0001	т/-		
20			01 120 1001 0001	- /		
27	Size	Deposition rate for CV pool surface. (kg/s)	CV-123-DRPL-0002	I/-		
28	section	Resuspension rate for CV pool surface, (kg/s)	CV-123-BBPL-0003	т/-		
29	number	Deposition rate total including SC/TC (kg/s)	CV-123-Depm-0004	т/-		
30	TURNOCT	Deposition rate total including $SC/TC$ (hg/3)	CV-123-Depp=0005	±/ T/=		
31		Reguenencion rates total including SC/TC, (parc/MT-S)	CV-123-Room-0001	±/- τ/-		
20		Resuspension rates total including SC/IC, (kg/S)	CV-123-Resil-0001	1/-		
32		Resuspension rates total including sc/rc, (part/m <sup>3</sup> -s)	Cv-123-Kesp-0002	1/-		
33		Pool aerosol mass, (kg)	CV-123-MaeP-0003	I/E		
34		Pool aerosol density, (part/m3)	CV-123-DaeP-0004	I/E		
35		Pool aerosol heat source (W)	CV-123-QaeP-0005	I/-		
36		Pool aerosol activity, (Bg)	CV-123-AaeP-0001	I/-		
	P	Aerosols suspended in the CV pool - data summed for all s	ize sections			
37	-	Pool aerosol mass, all size sections, (kg)	CV-123-SMaP-0000	I/-		
38	-	Pool aerosol density, all size sections (part/m3)	CV-123-SDaP-0000	I/-		
39		Pool aerosol heat source, all size sections. (W)	CV-123-SOaP-0000	I/-		
40		Pool aerosol activity, all size sections, (Bq)	CV-123-SAaP-0000	I/-		

continued

Pointer	s 3,4,5,6		Code Name				
IARG3C	IARG4C	Description	Examples	Impl/Expl			
Keep	Junction related data $(JN)$ Keep in mind that although these are JN related parameters, the pointer 1 is equal to 8 and not 2 IARG1C=8						
		Junction area data					
41	-	Area reduction due to aerosol deposition, (m2)	JN-234-Ared-0000	I/-			
42		Mass flow of atmosphere aerosols, (kg/s)	JN-234-WmAf-0000	I/-			
43	>0: sec.	Mass flow of pool aerosols, (kg/s)	JN-234-WmPf-0001	I/-			
44	number	Efficiency of filter, (-)	JN-234-EffF-0002	I/-			
45		Mass deposited on the filter, (kg)	JN-234-MdpF-0003	I/E			
46	(42, 43:	Number of particles deposited on the filter, (-)	JN-234-NdpF-0004	I/-			
47	=0:total	Heat of aerosols deposited on the filter, (W)	JN-234-QdpF-0005	I/-			
48	flow)	Activity of aerosols deposited on the filter, (W)	JN-234-AdpF-0001	I/-			
49		Deposited aerosol mass, all size sections, (kg)	JN-234-SMdF-0000	I/-			
50	-	Deposited aerosol density, all size sec., (part/m2)	JN-234-SNdF-0000	I/-			
51		Deposited aerosol heat source, all size sections, (W)	JN-234-SQdF-0000	I/-			
52		Deposited aerosol activity, all size sections, (Bq)	JN-234-SAdF-0000	I/-			
Keep	in mind th	1-D Solid Heat Conductor related data ( <b>SC</b> ) at although these are SC related parameters, the pointer	l is equal to 8 an	d not 3			
		IARGIC=0					
		SC surface denosition data for different size sect	ions				
5.2	r	Deposition valoaity growity aize and No. (m/a)	CC 245 V/201 0001	т /			
54		Deposition velocity, gravity, size sec. No., (m/s)	SC-345-Vg01-0001	I/-			
55	Surface	Deposition velocity, Brownian, Size Sec. No., (m/s)	SC-345-VD02-0002	1/= T/-			
56	number.	Deposition velocity, diffusionhoretic, sec. No., (m/s)	SC-345-V205-0001	I/- T/-			
57	1=loft	Deposition velocity, diffusiophorecic, sec. No. $(m/s)$	SC-345-Vi05-0001	I/ T/-			
58	2=right	Deposition velocity, turbutent, size sec. No., (m/s)	SC-345-V105-0001	I/- T/-			
50	2-right	beposition verocity, effective, size sec. No., (m/s)	50 545 7601 0002	1/			
59	TARGSC	Deposition rate for SC surface size sec No (kg/s)	SC-345-DB02-0001	T/E			
60	size sec	Resuspension rate for SC surface, sec. No., (kg/s)	SC-345-BB03-0002	I/=			
61	$=0.1 - N_{coc}$	Deposited aerosol mass, size sec No. (kg)	SC-345-Md04-0001	T/E			
62		Deposited aerosol density, size sec. No., (part/m2)	SC-345-Dd05-0002	T/E			
63		Deposited aerosol heat source, size sec. No., (W)	SC-345-0d01-0001	T/-			
64		Deposited aerosol activity, size sec. No., (Bg)	SC-345-Ad02-0002	T/-			
	Surface			_,			
	number:						
	1=left						
	2=right						
	-						
65	IARG5C:	Deposited frac. in $F_a$ -sec. No. (01), size sec. No.(03)	SC-345-0103-0001	I/-			
	size sec						
	=01-Nsec						
	IARG6C:						
	$F_a$ -sec.=						
	=01-99						
	1	SC surface deposition - size sections independent	data				
66	Surface	Deposited aerosol mass, all size sections, (kg)	SC-345-SMd1-0001	I/-			
67	number:	Deposited aerosol density, all size sec., (part/m2)	SC-345-SDd1-0002	I/-			
68	1=left	Deposited aerosol heat source, all size sections, (W)	SC-345-SQd1-0001	I/-			
69	2=right	Deposited aerosol activity, all size sections, (Bq)	SC-345-SAd1-0002	I/-			
70		Thickness of deposited aerosol layer, (m)	sC-345-Tdp1-0001	I/-			
71	Surface	It IARG5C = 0:	00 045 B 51 0000	<b>T</b> (			
	number	Deposition rate due to inertial impaction, (kg/s)	SC-345-DrI1-0002	I/-			
		II LARGOC > U:	00.045 7501 0000	- /			
		inertial impaction efficiency, size section No. (01)	SC-345-1E01-0002	1/-			
72	Surface	Reduction of atms. heat transfer due to deposition, %	SC-345-Ared-0001	I/-			
73	number	Reduction of pool heat transfer due to deposition, 🖇	SC-345-Pred-0002	I/-			

continued

Pointe	ers 3, 4		Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		2-D Solid Heat Conductor related data ( <b>TC</b> )		
Keep	in mind th	at although these are TC related parameters, the pointer	1 is equal to 8 an	d not 4
		IARG1C=8		
		TC surface deposition data for different size sect	ions	1
74		Deposition velocity, gravity, size sec. No., (m/s)	TC-456-Vg01-0001	I/-
75		Deposition velocity, Brownian, size sec. No., (m/s)	TC-456-Vb02-0002	I/-
/6	Boundary	Deposition velocity, thermophoretic, sec. No., (m/s)	TC-456-Vt03-0003	1/-
77	Cell	Deposition velocity, diffusiophoretic, sec. No. (m/s)	TC-456-Vd04-0004	1/-
78	number	Deposition velocity, turbulent, size sec. No., (m/s)	TC-456-V105-0005	1/-
79		Deposition verocity, effective, size sec. No., (m/s)	TC-456-VE01-0006	1/-
80	TARGSC	Deposition rate for TC surface size sec No (kg/s)	TC-456-DB02-0007	T/E
81	size sec	Resuspension rate for TC surface sec. No. (kg/s)	TC-456-BB03-0008	I/ _
82	=01-Nees	Deposited aerosol mass size sec No (kg)	TC-456-Md04-0009	T/E
83	Of NSEC	Deposited aerosol density, size sec. No., (kg)	TC-456-Dd05-0010	T/E
84		Deposited aerosol heat source, size sec. No., (W)	TC-456-0d01-0011	T/-
85		Deposited aerosol activity, size sec. No., (Bg)	TC-456-Ad02-0012	T/-
	Boundary			- /
	cell			
	number			
	IARG5C:			
	size sec	Deposited frac. in $F_a$ -sec. No.(01), size sec. No.(03)	TC-456-0103-0013	I/-
86	=01- <i>N</i> sec			
	IARG6C:			
	$F_a$ -sec.=			
	=01-99			
	1	TC surface deposition - size sections independent	data	
87		Deposited aerosol mass, all size sections, (kg)	TC-456-SMd2-0001	I/-
88	Boundary	Deposited aerosol density, all size sec., (part/m2)	TC-456-SDd2-0002	I/-
89	cell	Deposited aerosol heat source, all size sections, (W)	TC-456-SQd2-0003	I/-
90	number	Deposited aerosol activity, all size sections, (Bq)	TC-456-SAd2-0004	I/-
91		Thickness of deposited aerosol layer, (m)	TC-456-Tdp2-0005	1/-
92	Boundary	II IARG5C = 0: Dependential imposition $(\log n)$	TC 456 DTT2 0006	т /
	Cell	If TARGEC > 0.	TC-456-DE12-0006	1/-
	number	Inertial impaction efficiency size section No. (01)	TC-456-IE01-0006	т/-
9.3	Boundary	Reduction of atms, heat transfer due to deposition, %	TC-456-Ared-0007	T/-
94	cell no.	Reduction of pool heat transfer due to deposition, %	TC-456-Pred-0008	I/-
		Global parameters - Summed aerosol masses ( <b>RT</b> )		
95		Total mass of airborne aerosols in all CV, (kg)	RT-000-GMae-0000	I/-
96		Summed density of airborne aerosols, (part/m3)	RT-000-GDae-0000	I/-
97		Total heat of airborne aerosols, (W)	RT-000-GQae-0000	I/-
98		Total activity of airborne aerosols, (Bq)	KT-000-GAae-0000	I/-
0.0		Motol maga of mool armonia in all (M. (1.))	DE 000 CM-D 0000	<b>T</b> /
39		Summed density of pool services in all CV, (Kg)	RT-000-GMaP-0000	1/- T/
101		Summed density of pool aerosols, (part/m3)	RT-000-GDaP-0000	1/- T/
102	_	Total activity of pool aerosols (Rg)	RT-000-GQar-0000	±/= T/=
TUZ	_	TOTAL ACCINICA OF BOOT GELOPOILS' (Ed)	11 000-GAAF-0000	±/ -
103		Total mass of filter aerosols in all CV. (kg)	RT-000-GMdF-0000	т/-
104		Summed density of filter aerosols. (part/m3)	RT-000-GDdF-0000	I/-
105		Total heat of filter aerosols. (W)	RT-000-GOdF-0000	I/-
106		Total activity of filter aerosols, (Bg)	RT-000-GAdF-0000	I/-
				l <sup>'</sup>
107		Total mass deposited on all SC, (kg)	RT-000-GMd1-0000	I/-
108		Summed density of SC deposited aerosols, (part/m2)	RT-000-GDd1-0000	I/-
109		Total heat of SC deposited aerosols, $(W)$	RT-000-GQd1-0000	I/-
110		Total activity of SC deposited aerosols, (Bq)	RT-000-GAd1-0000	I/-
111		Total mass deposited on all TC, (kg)	RT-000-GMd2-0000	I/-
112		Summed density of TC deposited aerosols, (part/m2)	RT-000-GDd2-0000	I/-
113		Total heat of TC deposited aerosols, (W)	RT-000-GQd2-0000	I/-
114		Total activity of TC deposited aerosols, (Bq)	RT-000-GAd2-0000	I/-
			( <b>DM</b> )	
		GIODAI PARAMETERS - TOTAI AEROSOL MASS AND OVERALL ER	101 ( <b>KT</b> )	
115		Sum of CV. SC. TC aerosol masses Mare (kg)	RT-000-Mtot-0000	т/-
116	-	Integrated aerosol sources + initial mass. Marg. (kg)	RT-000-Marc-0000	I/-
117		Aerosol mass error $(M_{tot} - M_{src})/M_{tot}$ , (-)	RT-000-Merr-0000	I/-

#### continued

Pointers 3, 4			Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
PART II - RADIOACTIVE FISSION PRODUCT DATA						
		Core data ( <b>RT</b> )				
118		In-core mass at location L (L = IARG2C), (kg)	RT-001-MCor-0101	I/E		
119	isotope	No. of nuclides at location L, (nucl.)	RT-001-NCor-0102	I/E		
120	No.:0XXY	Decay heat of isotope XXY at location L, (W)	RT-001-QCor-0103	I/-		
121		Activity of isotope XXY at location L, (Bq)	RT-001-ACor-0104	I/-		
	XX=chain					
122	Y=isot.	Gap mass of isotope XXY at location L, (kg)	RT-001-MGap-0111	I/E		
123		Gap fraction (gap mass divided by in-core mass), (-)	RT-001-FGap-0112	I/-		
124		Released mass of isotope XXY at location L, (kg)	RT-001-MRe1-0113	I/E		
		Control Volume related data ( ${old CV}$ ) - Isotopes in CV at	nosphere			
Keep	in mind th	hat although these are CV related parameters, the pointer IARG1C=8	1 is equal to 8 an	d not 1		
105		Mana of TD monor in strength and (COM, (1))	017 100 MT	т /		
125	F.F.	Mass of FP vapor in atmosphere of CV, (kg)	CV-123-MVap-0001	1/- T/		
120	vapor	Saturation pressure of FP vanor (Pa)	CV-123-FVap-0002	1/- T/-		
120	isotopo	Mass of jectone XXX as vanor in CV atms (kg) (000)	CV-123-FSVP-0003	1/= T/E		
120	No ·OXXX	No. of nuclides of XXX in atmosphere of CV (nucl/m <sup>3</sup> )	CV-123-NIAi-0101	1/E T/F		
130	XX=chain	Decay heat of XXY in atmosphere of CV. (W)	CV-123-0TA1-0102	T/-		
131	Y=isot.	Activity of XXY in atmosphere of CV, (M)	CV-123-AIAi-0104	I/-		
1.32		Mass of all isotopes as vapor in atms. of CV, (kg)	CV-123-MTAt-0000	T/-		
133	-	No. of all nuclides in atmosphere of CV, (nucl/m <sup>3</sup> )	CV-123-NIAt-0000	I/-		
134		Decay heat of all nuclides in atmosphere of CV, (W)	CV-123-0IAt-0000	I/-		
135		Activity of all nuclides atmosphere of CV, (Bq)	CV-123-AIAt-0000	I/-		
136		External (TF/CF) source of isotope XXY, (kg/s)	CV-123-ESAm-0111	I/-		
137		External (TF/CF) source of isotope XXY, (nucl/s)	CV-123-ESAn-0112	I/-		
138		Core release source of isotope XXY, (kg/s)	CV-123-RSAm-0113	I/-		
139		Core release source of isotope XXY, (nucl/s)	CV-123-RSAn-0114	I/-		
140	isotope	Source of isotope XXY due to all JN flows, (kg/s)	CV-123-FSAm-0115	I/-		
141	No.:0XXY	Source of isotope XXY due to all JN flows, (nucl/s)	CV-123-FSNn-0116	I/-		
140	VV-shada	matel memory 1 of WW due to all adapted into (he/a)	0101	T / D		
142	XX=Chain	Total removal of XXY due to all adsorptions, (kg/s)	CV-123-AdAm-0121	1/E T/-		
143	I-150C.	Total source of XXX due to all desorptions, (huci/s)	CV-123-AdAII-0122 CV-123-DeAm-0123	1/= 1/F		
145		Total source of XXY due to all desorptions, (kg/s)	CV-123-DeAn-0124	T/-		
145		iotal source of AAT due to all desorptions, (naci/s)	CV 125 DEAN 0124	1/		
146		Saturation mass of isotope XXY in atms. of CV, (kg)	CV-123-Msat-0131	т/-		
147		Condensation mass transfer rate of XXY, (kg/s)	CV-123-Cond-0132	I/-		
	Co	r	CV atmosphere			
	00.		2. acmosphere			
148	FP	Total mass, sorbed vapor (11), size sec.No.(01), (kg)	CV-123-MT01-0011	I/E		
149	vapor	Penetrated mass, sorbed vap.(12) , size.No.(02), (kg)	CV-123-MP02-0012	I/E		
150	number	Sorption flux, vapor (13), size sec.No.(03), (kg/m <sup>2</sup> -s)	CV-123-SF03-0013	I/-		
151		$C_{rev}$ of vapor (14) on size sec.No.(04), (kg/m <sup>2</sup> )	CV-123-Cr04-0014	I/E		
152	IARG5C:	Available sites, vapor (15) size sec.No.(05), (kg/m <sup>2</sup> )	CV-123-Cx05-0015	I/-		
153	size sec	C <sub>rev</sub> of vapor (16) on size sec. No. (01), (nucl/m <sup>2</sup> )	CV-123-Nr01-0016	I/E		
154	=01- <i>N</i> sec	Available sites, vapor (17) size sec.No.(02) (nucl/m <sup>2</sup> )	CV-123-Nx02-0017	I/-		
	isotope					
1 5 5	NO.:UXXY	No. of multiples of VVV (201) on size and No. (05)	CTT 102 NAME 0201	T / D		
100	LARGSC:	NO. OF HUCTTORS OF ANY (321) ON SIZE SEC. NO. (05), $(p_{12}c_{1}/m^{2})$	CV-123-NAU5-U321	T / Fi		
	=01-N	(11401) 11 /				
156	isotope	Mass of isotope XXY on all size sec. (kg) (000)	CV-000-MAAi-0102	т/-		
157	No.: 0XXY	No. of nuclides of XXY on all size sec., (nucl)	CV-123-NAAi-0102	I/-		
158	XX=chain	Decay heat of XXY on all size sec., (W)	CV-123-QAAi-0103	I/-		
159	Y=isot.	Activity of XXY on all size sec., (Bq)	CV-123-AAAi-0104	I/-		
160		Mass of all isotopes on all size sec. (kg)	CV-123-MAAt-0000	I/-		
161	-	No. of all nuclides on all size sec., (nucl)	CV-123-NAAt-0000	I/-		
162		Decay heat of all nuclides on all size sec., (W)	CV-123-QAAt-0000	I/-		
163		Activity of all nuclides on all size sec., (Bq)	CV-123-AAAt-0000	I/-		

(000) The second pointer may be zero instead of CV number; in such case the parameter gives the total mass for all Control Volumes.

continued

Pointer	s 3, 4, 5		Code Name				
IARG3C	IARG4C	Description	Examples	Impl/Expl			
		Control Volume related data (CV) Jactanes in CV	2221				
Keep	Keep in mind that although these are CV related parameters, the pointer 1 is equal to 8 and not 1						
-		IARG1C=8					
164		Pool-gas mass transfer rate, (kg/s)	CV-123-FmPA-0101	I/-			
165	isotope	Pool-gas nuclide transfer rate, (nucl/s)	CV-123-FnPA-0101	I/-			
166	NO.:UAAI	Mass of isotope XXX as wapor in CV pool (kg) (000)	CV-000-MTPi-0101	T/E			
167	XX=chain	No. of nuclides of XXY in pool of CV, (nucl/m <sup>3</sup> )	CV-123-NIPi-0102	I/E			
168	Y=isot.	Decay heat of XXY in pool of CV, (W)	CV-123-QIPi-0103	I/-			
169		Activity of XXY in pool of CV, (Bq)	CV-123-AIPi-0104	I/-			
170		Mass of all isotopes as vapor in pool of CV, (kg)	CV-123-MIPt-0000	I/-			
171	-	No. of all nuclides in pool of CV, (nucl/m <sup>3</sup> )	CV-123-NIPt-0000	I/-			
172		Decay heat of all nuclides in pool of CV, (W)	CV-123-QIPt-0000	I/-			
174		Activity of all nuclides pool of CV, (Bq)	CV-123-AIPt-0000	1/-			
174		External (TF/CF/RK) source of isotope XXI, (Kg/S)(^)	CV-123-ESPM-0111 CV-123-ESPm-0112	1/- T/-			
176	isotope	Core release source of isotope XXY. (kg/s)	CV-123-RSPm-0113	T/-			
177	No.:0XXY	Core release source of isotope XXY, (nucl/s)	CV-123-RSPn-0114	I/-			
178		Source of isotope XXY due to all JN flows, (kg/s)	CV-123-FSPm-0115	I/-			
179	XX=chain	Source of isotope XXY due to all JN flows, (nucl/s)	CV-123-FSPn-0116	I/-			
	Y=isot.						
180		Total removal of XXY due to all adsorptions, (kg/s)	CV-123-AdPm-0121	I/E			
181		Total removal of XXY due to all adsorptions, (nucl/s)	CV-123-AdPn-0122	I/- I/D			
182		Total source of XXY due to all desorptions, (kg/s)	CV-123-DePm-0123	1/E T/=			
105		iotal source of AAI due to all desorptions, (nucl/s)	CV-125-Dern-0124	1/-			
	Cont.	rol Volume related data ( <b>CV</b> ) - Isotopes on aerosols depos	sited in CV pool				
			-				
184	FP	Total mass, sorbed vapor (11), size sec.No.(01), (kg)	CV-123-MT01-1011	I/E			
185	vapor	Penetrated mass, sorbed vap.(12) , size.No.(02), (kg)	CV-123-MP02-1012	I/E			
186	number	Sorption flux, vapor (13), size sec.No.(03), (kg/m <sup>2</sup> -s)	CV-123-SF03-1013	I/- I/D			
188	TARCSC	$C_{rev}$ of Vapor (14) on Size Sec.NO.(04), (Kg/m <sup>2</sup> )	CV-123-Cr04-1014	1/E T/-			
189	size sec	$C_{rm}$ of vapor (16) on size sec. No. (01), (nucl/m <sup>2</sup> )	CV-123-Nr01-1016	T/E			
190	=01-Nsec	Available sites, vapor (17) size sec.No.(02) (nucl/m <sup>2</sup> )	CV-123-Nx02-1017	I/-			
	isotope						
	No.:1XXY						
191	IARG5C:	No. of nuclides of XXY (321) on size sec. No.(05)	CV-123-NA05-1321	I/E			
	size sec	(nucl/m²)					
100	=UI-Nsec	Mass of isotone XXX on all size sec. (kg) (000)	CV-000-MAD;-0100	т/_			
192	No ·OXXV	No of nuclides of XXY on all size sec. (Kg) (VOU)	CV-123-NAPi-0102	±/= T/-			
194	XX=chain	Decay heat of XXY on all size sec., (W)	CV-123-OAPi-0103	I/-			
195	Y=isot.	Activity of XXY on all size sec., (Bq)	CV-123-AAPi-0104	I/-			
196		Mass of all isotopes on all size sec. (kg)	CV-123-MAPt-0000	I/-			
197	-	No. of all nuclides on all size sec., (nucl)	CV-123-NAPt-0000	I/-			
198		Decay heat of all nuclides on all size sec., (W)	CV-123-QAPt-0000	I/-			
199		Activity of all nuclides on all size sec., (Bq)	CV-123-AAPt-0000	I/-			
		Control Volume related data (CV) - Evnocura and d	0565				
		control volume related data (CV) - Exposure and d	0363				
200		Exposure rate, y-rays, ((C/kg)/s)	CV-123-ExvC-0000	I/-			
201		Exposure rate, y-rays, (R/s)	CV-123-ExyR-0000	I/-			
202		Dose rate, γ-rays, (Gy/s)	CV-123-DsyG-0000	I/-			
203	-	Dose rate, $\gamma$ -rays, (rad/s)	CV-123-DsyR-0000	I/-			
204		Dose rate, $\beta$ -rays, (Gy/s)	CV-123-DsbG-0000	I/-			
205		Dose rate, β-rays, (rad/s)	CV-123-DsbR-0000	I/-			
205		Dose equivalent rate (rem/s)	CV-123-DSES-0000	1/- T/-			
201		pope edutateur tace! (tem/p)	C* 172 D9EV-0000	±/ -			

(\*) In case of circulating fuel, the sources are calculated by the RK package, including the delayed neutron precursors.

(000) The second pointer may be zero instead of a CV number; in such case the parameter gives the total mass for all Control Volumes.

continued

Pointer	s 3, 4, 5		Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
Junction related data (JN)         Keep in mind that although these are JN related parameters, the pointer 1 is equal to 8 and not 2         IARGIC=8						
208 209	isotope No.:0XXY	Flow of isotope XXY with atmosphere, (kg/s) Flow of isotope XXY with pool, (kg/s)	JN-234-WISA-0101 JN-234-WISP-0102	I/- I/-		
210 211 212 213	XX=chain Y=isot.	Mass of isotope XXY on vapor filter, (kg) (000) No. of nuclides of XXY on vapor filter, (nucl) Decay heat of XXY on vapor filter, (W) Activity of XXY on vapor filter, (Bq)	JN-000-MVF1-0111 JN-234-NVF1-0112 JN-234-QVF1-0113 JN-234-AVF1-0114	I/E I/E I/- I/-		
214	isotope No.:0XXY <b>IARG5C:</b> size sec =01-Nsec	No. of nucl. of XXY on aerosol filter, size sec. No. (05), (nucl)	JN-234-NF05-0112	I/E		
215 216 217	isotope No.:0XXY XX=chain	Mass of XXY on aerosol filter, all sizes, (kg) (000) No. of nuclides of XXY on aerosol filter, (nucl) Decay heat of XXY on aerosol filter, (W)	JN-000-MAF1-0111 JN-234-NAF1-0112 JN-234-QAF1-0113	I/- I/- I/-		
218	Y=isot.	Activity of XXY on aerosol filter, (Bq)	JN-234-AAF1-0114	1/-		

(000) The second pointer may be zero instead of a JN number; in such case the parameter gives the total mass for all Junctions.

continued

Pointer	s 3,4,5,6		Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
1-D Solid Heat Conductor related data ( <b>SC</b> ) - Sorbed isotopes Keep in mind that although these are SC related parameters, the pointer 1 is equal to 8 and not 3						
Reep	IARGIC=8					
	-		-			
219	FP vapor	Total mass of sorbed vapor, (kg)	SC-345-MTot-0001	I/-		
220	number	Penetrated mass of sorbed vapor, (kg)	SC-345-MPen-0002	I/-		
	Cell No.					
221	IARG5C:	Concentration of penetrated vapor No.(12), (kg/m <sup>3</sup> )	SC-345-CV12-0001	I/E		
	Vapor No					
	=01-N <sub>vap</sub>					
222	Surf.No.	Sorption flux of vapor No.(11), (kg/m <sup>2</sup> -s)	SC-345-SF11-0001	I/-		
223	1=left	Desorption flux (pool) of vapor No.(12), (kg/m <sup>2</sup> -s)	SC-345-DF12-0002	I/-		
224	2=right	C <sub>rev</sub> of vapor No.(13), (kg/m <sup>2</sup> )	SC-345-Cr13-0001	I/E		
225	IARG5C:	Available sites for vapor No.(14), (kg/m <sup>2</sup> )	SC-345-Cx14-0002	I/-		
226	Vapor No	C <sub>rev</sub> of vapor No.(15), (nucl/m <sup>2</sup> )	SC-345-Nr15-0001	I/E		
227	$=0.1 - N_{vap}$	Available sites for vapor No.(16), (nucl/m <sup>2</sup> )	SC-345-Nx16-0002	I/-		
228	isotope	Sorbed mass of isotope XXY, (kg) (000)	SC-000-MIsi-0102	I/E		
229	No.: 0XXY	No. of nuclides of sorbed isotope XXY, $(nucl/m^2)$	SC-345-NIsi-0102	T/E		
230	XX=chain	Decay heat of sorbed isotope XXY. $(W)$	SC-345-01si-0103	т/-		
231	Y=isot	Activity of sorbed isotope XXY. (Bg)	SC-345-ATsi-0104	_, т/-		
232	1 10000	Mass of all sorbed isotopes (kg)	SC-345-MIst-0000	I/-		
232	_	No. of nuclidos of all sorbod isotopos (nucl/m <sup>2</sup> )	SC-345-NISt-0000	1/ T/-		
234		Decay heat of all serbed isotopes, (Mucr/M)	SC-345-01st-0000	1/ T/-		
235		Activity of all sorbed isotopos (Rg)	SC-345-QISC-0000	I/- T/-		
233	I	Accivity of all solbed isocopes, (Eq)	50 545 AISC 0000	1/		
i	l-D Solid H	eat Conductor related data ( <b>SC</b> ) - Isotopes on aerosols de	eposited in SC surfa	ices		
236	Surf.No.	Mass of sorbed vap. No.(12) size sec. No.(7), (kg)	SC-345-MT12-7001	I/E		
237	1=left	Penetrated mass, vap. No.(13) size sec. No.(8), (kg)	SC-345-MP13-8002	I/E		
238	2=right	Sorption flux, vap. No.(01) size sec.No.(9), (kg/m <sup>2</sup> -s)	SC-345-SF01-9001	I/-		
239	IARG5C:	Desorp. flux, vap. No.(02) size sec. No.(10),(kg/m <sup>2</sup> -s)	SC-345-DF02-A001	I/-		
240	size sec	C <sub>rev</sub> , vap. No.(03) size sec. No.(11), (kg/m <sup>2</sup> )	SC-345-Cr03-B002	I/E		
241	$=1-N_{sec}$	Available sites, vap. No.(04) sec. No.(12), (kg/m <sup>2</sup> )	SC-345-Cx04-C001	I/-		
242	IARG6C:	Crev, vap. No.(05) size sec. No.(13) (nucl/m <sup>2</sup> )	SC-345-Nr05-D002	I/E		
243	Vapor No	Available sites, vap. No.(06) sec. No.(14) (nucl/m <sup>2</sup> )	SC-345-Nx06-E001	I/-		
	$= 0.1 - N_{var}$					
	Surf.No.					
	1=left					
	2=right					
	IARG5C:					
244	size sec	No. of nuclides of isotope No. (101) on aerosols	SC-345-Y101-F001	I/E		
	$=1 - N_{coc}$	size sec No (15), (nucl/m <sup>2</sup> )		-/ -		
	TARGEC	5126 566. Hol (16)/ (Ha01/M)				
	isotope					
	No ·XXX					
	Surf No					
245	1=1of+	Mass of isotope No. (101) on all size sec. (kg) (000)	SC-000-M101-0000	т/-		
246	2=right	No of nuclides of No (102) on all size sec. (Ng) (000)	SC-345-N102-0002	±/- T/-		
240	TAPCEC	No. of indefines of No. (102) on all size sec., (IIICI)	SC 345_0103_0001	±/- τ/-		
24/	isotopo	Activity of isotopo No. (103) on all size sec., (W)	SC-345-Q103-0001	1/- T/		
240	TROCODE	ACCIVICY OF ISOCOPE NO. (104) ON ALL SIZE SEC., (BQ)	30-343-A104-0002	1/-		
2.4.0	NU. AAI	Mars of all interes on all since (1.5)	00 345 M371 0001	т /		
249	SUTI.NO.	Mass of all isotopes on all size sec. (kg)	SC-345-MAIt-0001	1/-		
250	1=leit	NO. OF ALL NUCLIDES ON ALL SIZE SEC., (NUCL)	SC-345-NAIT-0002	1/- T/		
251	∠=right	Decay neat of all nuclides on all size sec., (W)	SC-345-QAIt-0001	1/-		
252	1	ACLIVICY OF ALL NUCLIDES ON ALL SIZE SEC., (Bq)	SC-345-AAIt-0002	⊥/-		

(000) The second pointer may be zero instead of a SC number; in such case the parameter gives the total mass for all Solid Heat Conductors (also boundary cell number must be zero for IARG2C=245).

continued

Pointers 3,4,5,6			Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
2-D Solid Heat Conductor related data ( <b>TC</b> ) - Sorbed isotopes						
Keep	Keep in mind that although these are TC related parameters, the pointer 1 is equal to 8 and not 4 IARG1C=8					
253	FP vapor	Total mass of sorbed vapor, (kg)	TC-456-MTot-0001	I/-		
254	number	Penetrated mass of sorbed vapor, (kg)	TC-456-MPen-0002	I/-		
255	Cell No. IARG5C:	Concentration of penetrated vapor No.(12), (kg/m <sup>3</sup> )	TC-456-CV12-0001	I/E		
	Vapor No					
05.0	=01-Nvap		TO 456 0711 0101	<b>T</b> /		
250	Boundary	Sorption flux of vapor No. (11), $(kg/m^2-s)$	TC-456-SF11-0121	1/-		
257	Cell NO.	Desorption flux (pool) of vapor No.(12), (kg/m <sup>2</sup> -S)	TC-456-DF12-0122	1/-		
258	735656	$C_{rev}$ OI Vapor NO. (13), (Kg/m <sup>2</sup> )	TC-456-CF13-0123	1/1		
259	IARG5C:	Available sites for vapor No. (14), (kg/m <sup>2</sup> )	TC-456-CX14-0124	1/-		
260	Vapor No	Crev OI Vapor No.(15), (nucl/m <sup>2</sup> )	TC-456-Nr15-0125	1/E T/		
261	=01-Nvap	Available sites for vapor No. (16), (nucl/m <sup>2</sup> )	TC-456-NX16-0126	1/-		
262	isotope	Sorbed mass of isotope XXY, (kg) (000)	TC-000-MIsi-0102	1/E		
263	No.:UXXY	No. of nuclides of sorbed isotope XXY, (nucl/m <sup>2</sup> )	TC-456-N1s1-0102	1/E		
264	XX=chain	Decay heat of sorbed isotope XXY, (W)	TC-456-QIsi-0103	I/-		
265	Y=isot.	Activity of sorbed isotope XXY, (Bq)	TC-456-AIsi-0104	I/-		
266		Mass of all sorbed isotopes (kg)	TC-456-MIst-0000	I/-		
267	-	No. of nuclides of all sorbed isotopes, (nucl/m <sup>2</sup> )	TC-456-NIst-0000	I/-		
268		Decay heat of all sorbed isotopes, (W)	TC-456-QIst-0000	I/-		
269		Activity of all sorbed isotopes, (Bq)	TC-456-AIst-0000	I/-		
2	2-D Solid H	eat Conductor related data ( <b>TC</b> ) - Isotopes on aerosols d	eposited in SC surf.	aces		
270	Boundary	Mass of sorbed vap. No.(12) size sec. No.(7), (kg)	SC-345-MT12-7001	I/E		
271	cell No.	Penetrated mass, vap. No.(13) size sec. No.(8), (kg)	SC-345-MP13-8002	I/E		
272	IARG5C:	Sorption flux, vap. No.(01) size sec. No.(9),(kg/m <sup>2</sup> -s)	SC-345-SF01-9003	I/-		
273	size sec	Desorp. flux, vap. No.(02) size sec. No.(10),(kg/m <sup>2</sup> -s)	SC-345-DF02-A004	I/-		
274	$=1-N_{sec}$	C <sub>rev</sub> , vap. No.(03) size sec. No.(11), (kg/m <sup>2</sup> )	SC-345-Cr03-B005	I/E		
275	IARG6C:	Available sites, vap. No.(04) sec. No.(12), (kg/m <sup>2</sup> )	SC-345-Cx04-C006	I/-		
276	Vapor No	C <sub>rev</sub> , vap. No.(05) size sec. No.(13) (nucl/m <sup>2</sup> )	SC-345-Nr05-D007	I/E		
277	$=01-N_{vap}$	Available sites, vap. No.(06) sec. No.(14) (nucl/m <sup>2</sup> )	SC-345-Nx06-E008	I/-		
	Boundary					
	TARG5C ·					
278	size sec	No of nuclides of isotone No. (101) on serosols	TC-456-V101-E023	T/F		
270	=1=N	size sec No (15) (kg) (boundary cell 023)	10-450-1101-1025	1/15		
	TARCEC	$(nucl/m^2)$				
	isotopo	(Hutt) m)				
	No.:XXY					
279	Boundarv	Mass of isotope No. (101) on all size sec. (kg) (000)	TC-000-M101-0000	I/-		
280	cell No.	No. of nuclides of No. (102) on all size sec., (nucl)	TC-456-N102-0332	I/-		
281	IARG5C:	Decay heat of isotope No. (103) on all size sec., (W)	TC-456-Q103-0333	I/-		
282	isotope	Activity of isotope No. (104) on all size sec., (Bq)	TC-456-A104-0334	I/-		
	No.:XXY					
283		Mass of all isotopes on all size sec. (kg)	TC-456-MAIt-0341	I/-		
284	Boundarv	No. of all nuclides on all size sec., (nucl)	TC-456-NAIt-0342	I/-		
285	cell No.	Decay heat of all nuclides on all size sec (W)	TC-456-0AIt-0343	I/-		
286		Activity of all nuclides on all size sec. (Bg)	TC-456-AATt-0344	т/-		

(000) The second pointer may be zero instead of a TC number; in such case the parameter gives the total mass for all Solid Heat Conductors (also boundary cell number must be zero for IARG2C=279).

#### continued

Pointers 3,4			Code Name		
IARG3C	IARG4C	Description	Examples	Impl/Expl	
Glob	al paramete	ers - Isotopes in atmosphere and pool of all CV-s, sorbed	by all SC-s and TC	-s ( <b>RT</b> )	
	-				
287		Mass of all isotopes, atms of all CV-s, (kg)	RT-000-MIAG-0000	I/-	
288		No. of all nuclides, atms of all CV-s, (nucl)	RT-000-NIAG-0000	I/-	
289		Decay heat of all nuclides, atms of all CV-s, (W)	RT-000-QIAG-0000	I/-	
290		Activity of all nuclides, atms of all CV-s, (Bq)	RT-000-AIAG-0000	I/-	
291		Mass of all isotopes, pool of all CV-s, (kg)	RT-000-MIPG-0000	I/-	
292		No. of all nuclides, pool of all CV-s, (nucl)	RT-000-NIPG-0000	I/-	
2.93		Decay heat of all nuclides, pool of all CV-s. (W)	RT-000-01PG-0000	т/-	
294		Activity of all nuclides, pool of all CV-s, (Bq)	RT-000-AIPG-0000	I/-	
295	-	Mass of all isotopes on all SC-s, (kg)	RT-000-MSCG-0000	I/-	
296		No. of all nuclides on all SC-s, (nucl)	RT-000-NSCG-0000	I/-	
297		Decay heat of all nuclides on all SC-s, (W)	RT-000-QSCG-0000	I/-	
298		Activity of all nuclides on all SC-s, (Bq)	RT-000-ASCG-0000	I/-	
299		Mass of all isotopes on all TC-s, (kg)	RT-000-MTCG-0000	I/-	
300		No. of all nuclides on all TC-s, (nucl)	RT-000-NTCG-0000	I/-	
301		Decay heat of all nuclides on all TC-s. (W)	BT-000-0TCG-0000	T/-	
302		Activity of all nuclides on all TC-s, (Bq)	RT-000-ATCG-0000	I/-	
Global parameters – Isotopes on aerosols in all CV-s, deposited on all SC-s and TC-s ( $RT$ )					
303		Mass of all isotopes, aerosols in all CV-s, (kg)	RT-000-MAAG-0000	I/-	
304		No. of all nuclides, aerosols in all CV-s, (nucl)	RT-000-NAAG-0000	I/-	
305		Decay heat of all nuclides, aerosols in all CV-s, (W)	RT-000-QAAG-0000	I/-	
306		Activity of all nuclides, aerosols in all CV-s, (Bq)	RT-000-AAAG-0000	I/-	
307		Mass of all isotopes, pool-aerosols in all CV-s, (kg)	RT-000-MAPG-0000	I/-	
308		No. of all nuclides, pool-aerosols in all CV-s, (nucl	RT-000-NAPG-0000	I/-	
309		Decay heat of all nuclides, pool-aer.in all CV-s, (W)	RT-000-0APG-0000	I/-	
310		Activity of all nuclides, pool-aer in all CV-s. (Bg)	BT-000-AAPG-0000	т/-	
011	-			- /	
311		Mass of all isotopes, aerosols on all SU-s, (kg)	RT-UUU-MASG-UUUU	1/- T/	
312		No. of all nuclides, aerosols on all SC-s, (nucl)	RT-000-NASG-0000	1/-	
313		Decay heat of all nuclides, aerosols on all SC-s, (W)	RT-000-QASG-0000	1/-	
314		Activity of all nuclides, aerosols on all SC-s, (Bq)	RT-000-AASG-0000	1/-	
315		Mass of all isotopes, aerosols on all TC-s, (kg)	RT-000-MATG-0000	I/-	
316		No. of all nuclides, aerosols on all TC-s, (nucl)	RT-000-NATG-0000	I/-	
317		Decay heat of all nuclides, aerosols on all TC-s, (W)	RT-000-QATG-0000	I/-	
318		Activity of all nuclides, aerosols on all TC-s, (Bq)	RT-000-AATG-0000	I/-	
Global parameters - Total number of nuclides and overall error ( <b>RT</b> )					
319		Total number of nuclides of all isotopes, $N_{tot}$ , (nucl)	RT-000-Ntot-0000	I/-	
320	-	Integrated sources + initial masses, N <sub>src</sub> , (nucl)	RT-000-Nsrc-0000	I/-	
321		Relative error (N <sub>tot</sub> - N <sub>src</sub> )/N <sub>tot</sub> , (-)	RT-000-Nerr-0000	I/-	
		Reactor Kinetics for Circulating Fuel ( <b>RT</b> )			
322	-	Volume of active core, (m <sup>3</sup> )	RT-000-RVol-0000	I/-	
323		Reactivity feedback from the core volume change, (\$)	RT-000-ReVo-0000	I/-	

Table 2-29 List of arguments available for Control Functions, variables available in Reactor Kinetics Data Base.

Pointer 1:	IARG1C = 7, Reactor Kir	netics Data Base	Code name:	RK
Pointer 2:	IARG2C = 0	for the point kinetics	Code name:	three digits
	node number	for the nodal kinetics		
		available for IARG1CF = 2	through 18 as	nd 25

Pointe	ointers 3, 4 Code Name				
IARG3C	IARG4C	Description	Examples	Impl/Expl	
		Reactor Kinetic	s data	<u>.</u>	
1		not used (to avoid confusion with CF)		-	-
2		Neutron density, (1/m <sup>3</sup> )	(000=A)	RK-000-Neut-0000	I/E
3		Neutron flux, (1/m <sup>2</sup> /s)	(000=A)	RK-000-Flux-0000	I/-
4		Average fuel temperature, K	(000=A)	RK-000-Tfue-0000	I/-
5		Average moderator temperature, K, or	density (kg/m <sup>3</sup> )	RK-000-Tmod-0000	I/-
	-	depending on IRFDRK (record 780000)	(000=A)		
6		Average void fraction	(000=A)	RK-000-Void-0000	I/-
7		Reactivity, (\$)	(000=A)	RK-000-Reac-0000	I/-
		NOTE: If multiplication factor is	requested (record		
		750999, IRPLRK=2), then reactivity is	replaced by:		
		- in the point kinetics: k <sub>eff</sub> (-) RK	-000-Keff-0000		
		- in the nodal kinetics: $k_{\infty}$ (-) RK	-001-Kinf-0000		
8		Control rod reactivity, (\$)	(000=A)	RK-000-ReCR-0000	I/-
9		Reactivity from thermal feedback, \$	(000=A)	RK-000-ReTF-0000	I/-
10		Reactivity from isotope changes, (\$)	(000=A)	RK-000-ReNF-0000	I/-
		Reactivity from core volume change $\rightarrow$	RT-000-ReVo-0000		
		Delayed neutron pred	cursor data		
11	Group No	Precursor concentration, 1/m <sup>3</sup>		RK-000-Cpre-0001	I/E
		Isotope da	ta		
12	Isotope	Isotope concentration, (1/m <sup>3</sup> )		RK-000-Nucl-0108	I/E
13	refe-	Isotope decay heat density, (W/m <sup>3</sup> ) RK-000-Qidc-		RK-000-Qidc-0201	I/-
14	-rence	Reactivity due to given isotope, (\$)	RK-000-RiNu-0302	I/-	
15	No.	Reactivity change due to change of gi	RK-000-DiNu-0403	I/-	
		Overall power	data		
16		Total decay heat density, (W/m <sup>3</sup> )		RK-000-Qddc-0000	I/-
17	-	Total decay power, (W)	(000=S)	RK-000-Qdec-0000	I/-
18		Total fission power, (W)	(000=S)	RK-000-Qfis-0000	I/-
		Isotope data for circ	ulating fuel		
19		Isotope concentration in liquid, (1/m	1 <sup>3</sup> )	RK-000-Nliq-0108	I/-
20	Isotope	Isotope concentration in solid, (1/m <sup>3</sup> )		RK-000-Nsol-0201	I/-
21	refe-	Isotope concentration in gas, (1/m <sup>3</sup> ) RK-000-Ngas-0302		I/-	
22	-rence	Effective concentration, liquid, (1/m <sup>3</sup> ), see RLIRTK RK-000-Xliq-0403 I			I/-
23	No.	Effective concentration, solid, (1/m <sup>3</sup> ), see RSITRK RK-000-Xsol-0502 I.			I/-
24		Effective concentration, gas, $(1/m^3)$ ,	see RGITRK	RK-000-Xgas-0108	I/-
25	-	Macroscopic fission cross section (1)	(m) (000-A)	PK-000-SigE-0000	т/-

 $(000{=}S)$  Nodal kinetics: the second pointer of zero means value summed for all nodes

(000=A) Nodal kinetics: the second pointer of zero means volume-averaged value

# Table 2-30 List of arguments available for Control Functions, variables available in Tabular Function Data Base.

Pointer 1:	IARG1C = 6, Tabular Function Data Base	Code name:	TF
Pointer 2:	IARG2C = TF reference number	Code name:	three digits

Pointers 3, 4			Code Name	
IARG3C	IARG4C	IARG4C Description		Impl/Expl
TF data				
1	-	Value of the Tabular Function	TF-678-Valu-0000	I/-

Table 2-31 List of arguments available for Control Functions, variables available in Control Function Data Base.

Pointer 1:	IARG1C = 7, Control Function Data Base	Code name:	CF
Pointer 2:	IARG2C = CF reference number	Code name:	three digits

Pointers 3, 4			Code Name			
IARG3C	IARG4C	Description	Examples	Impl/Expl		
	CF data					
1	-	Value of the Control Function	CF-789-Valu-0000	I/E		

Table 2-32 List of arguments available for Control Functions, variables available in Numerical Solver Data Base.

Pointer 1:	IARG1C = 9, Numerical Solver Data Base	Code na
Pointer 2:	IARG2C = Not used - must be equal to zero	Code na

ame: SL ame: three digits

Pointers 3, 4			Code Name	
IARG3C	IARG4C	Description	Examples	Impl/Expl
		Material property data		
1		Current model time, s	SL-000-Time-0000	I/-
2		Current time step, s	SL-000Dt-0000	I/-
3		Current CPU time (processor usage), s SL-000- CPU-0000		I/-
4	-	Warp factor (model time / CPU time)	SL-000-Warp-0000	I/-
5		Current run time (clock time), s	SL-000-RunT-0000	I/-
6		Run time ratio (run time / model time)	SL-000-RunR-0000	I/-
7		Local warp factor (within the last plot interval)	SL-000-WarL-0000	I/-
8		Local run ratio (within the last plot interval)	SL-000-RunL-0000	I/-

2.8.10 Records: 715000, Implicit Solution of All Control Functions

The Control Functions are always included in the main iteration loop to obtain implicit solution. Therefore the CF values are (like all other parameters in the implicit solution) controlled by the SPECTRA Numerical Solver. The main iteration is finished after all end-of-time-step values assumed and calculated are in agreement, according to the Solver criteria). In some cases the Control Functions are last to converge. In such case a warning message is printed by the Solver, advising the user to ignore the CF convergence criteria. In most cases the CF accuracy is sufficient even when the CF convergence is ignored by the Solver.

W-1 (A) :	IMPLCF	Indicator defining the CF convergence		
		IMPLCF = 1:	CF convergence criteria must be satisfied in order to complete the iteration.	
		IMPLCF = 2:	CF convergence criteria are ignored. When all other parameters are converged, then the iteration is completed even if the CF convergence is not yet satisfactory.	
		Acceptable range:	1 or 2 .	
		Default value:	1.	
#### 2.8.11 Examples of Control Function Input Data

#### MAXIMUM

The function CF-100 below calculates the maximum temperature of a 1-D Solid Heat Conductor SC-123.

705100	Maxin	num ·	tempe	erati	ire (	of :	sc-1	.23								
*	(The	"Ma:	x" Cl	E)	S	cal	е	Ad	ditive							
*	Group		Numbe	er	Fa	act		C	onst.							
700100	2		3			1.0			0.0 *							
*	Argun	nent	S													
* Point	cers:	(1)	(2)	(3)	(4)	*	(1)			(2)		(3)		(4)		
710100		3	123	16	1	*	SC	data	base,	SC	-123,	Cell	temperature,	Cell	No.	1
710100		3	123	16	2	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	2
710100		3	123	16	3	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	3
710100		3	123	16	4	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	4
710100		3	123	16	5	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	5
710100		3	123	16	6	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	6
710100		3	123	16	7	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	7
710100		3	123	16	8	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	8
710100		3	123	16	9	*	SC	data	base,	SC	123,	Cell	temperature,	Cell	No.	9

#### **IF-THEN-ELSE**

CF-182 is an example of an IF-THEN-ELSE function. The function CF-182 checks the rotational speed of the pump JN-100, and computes the pump status signal, as:

if the pump speed is less that 1.0 rev/s, then the status signal is 0.0 (off), if the pump speed is larger than 1.0 rev/s then the status signal is 1.0 (on).

In order to obtain a constant value a "dummy" variable is used. The dummy variable is the current time step (pointers: 9 0 2 0). The value of the dummy variable is multiplied by zero, and the required constant is added. Note that the multipliers of 1.0E-90 were used whenever zero was desired. This must be done to prevent the program from assigning the default multiplier of 1.0, which is done when no value is entered or the entered value is zero.

705182	STATU	s:	Gas	Pump	) (SG	SP)				
*	Group		Numbe	er	Fa	uct.	Const.			
700182	1		4		1	.0	0.0	*	Type : IF-THEN-ELSE	
709182	2							*	Arg. : Explicit	
*	Argum	lent	s							
* Point	cers:	(1)	(2)	(3)	(4)	Fact.	Const.			
710182		2	100	35	1	1.0	0.0	*	IF ( JN-100 pump speed <	
710182		9	0	2	0	1.0E-	90 1.0	*	< 1.0 rev/s )	
710182		9	0	2	0	1.0E-	-90 0.0	*	THEN signal = 0.0	
710182		9	0	2	0	1.0E-	90 1.0	*	ELSE signal = 1.0	

Below, another example of the IF-THEN-ELSE function is given. This time the function defines the control rod reactivity after scram. The scram signal is given by the function CF-901. When the scram signal is received, the control rods start moving down with a delay of 0.1 s. The control rod reactivity is tabulated as a function of time after scram as TF-900. Note that <u>if a TF is used within an IF-THEN-ELSE function and the TF is not an interactive type, then the argument for the TF is always the current time minus the time when the corresponding IF-THEN-ELSE was last becoming true.</u>

705900 Control rod reactivity \* Group Number Fact. Const.

700900	1	4		1.	0	C	0.0	*	Type : IF-THEN-ELSE
709900	2							*	Arg. : Explicit
*	Argument	s							
* Point	ters: (1)	(2)	(3)	(4)	Fact	. Cor	nst.		
710900	7	901	1	0	1.0	C	0.0	*	IF ( CF-901 (scram signal) <
710900	9	0	2	0	1.01	E-90 1	.0	*	< 1.0 )
710900	9	0	2	0	1.01	E-90 C	0.0	*	THEN rod reactivity is zero
710900 *	6	900	1	0	1.0	C	0.0	*	ELSE use TF-900 to define rod reactivity
605900	Control	rod	react	tivit	y aft	cer so	eram		
*	Fact.	(	Const		-				
601900	1.0		0.0		*	Scali	ng		
602900	-30.0	0.0	0.0	0.0	*	Limit	s: Min	, 1	Max, dTF/dt
610900	1				*	Type:	NON	-II	NTERACTIVE !! otherwise the program will use
*					*		the	a	ctual value of TF and not TF(t-to)
*									
*	Time af	ter :	scram	R	eact	ivity	(\$)		
600900	Ο.	. 0			0.0				
600900	0.	.1			0.0				
600900	Ο.	.2			-1.0				
600900	0.	. 3		-	30.0				

Apart from reactor scram, such function may be useful to model pump trip with pump coastdown curve versus time, etc.

#### **HYSTERESIS**

An example of the hysteresis function type 1, shown in Figure 2-45, is shown below.

```
705200 Example of a Hysteresis Function Type 1
*
       Group Number Fact. Const.
700200 1
                                                      * Type
                     6
                                   1.0
                                            0.0
                                                                 : Hysteresis
       Arguments
* Pointers: (1) (2) (3) (4) Fact. Const.
              1 333 13 1 1.0E-6 0.0 * uses CV-333 pressure (in MPa) as an argument
6 201 1 0 1.0 0.0 * uses TF-201 as a definition of the first poin
6 202 1 0 1.0 0.0 * uses TF-202 as a definition of the second point
710200
                                       0.0 * uses TF-201 as a definition of the first point
710200
                                         0.0 * uses TF-202 as a definition of the second point
710200
605201 Hysteresis point 1
                  f(x)
          х
                          * single data pair means hysteresis type 1
600201
          0.0
                   2.5
605202 Hysteresis point 2
                  f(x)
3.7
          х
600202
         0.0
                        * single data pair means hysteresis type 1
```



Figure 2-45 Hysteresis function type 1

An example of the hysteresis function type 2, shown in Figure 2-45, is shown below.

```
705300 Example of a Hysteresis Function Type 2
       Group Number
                              Fact.
                                      Const.
700300
                                                 * Type
                                                            : Hysteresis
        1
                  6
                               1.0
                                        0.0
      Arguments
* Pointers: (1) (2) (3) (4) Fact. Const.
                         1 1.0E-6 0.0 * uses CV-333 pressure (in MPa) as an argument
0 1.0 0.0 * uses TF-301 as the Forward function
             1 333 13
6 301 1
710300
                333 13
710300
                                     0.0 * uses TF-302 as the Reverse function
710300
             6 302 1
                          0 1.0
605301 Forward function
         х
                f(x)
         2.0
                       * multiple data pair means hysteresis type 2
600301
                0.0
600301
         3.0
                 0.0
600301
         4.0
                1.0
605302 Reverse function
                 f(x)
         Х
         2.0
600302
                0.0
                       * multiple data pair means hysteresis type 2
600302
        3.0
                1.0
600302
        4.0
                1.0
```



Figure 2-46 Hysteresis function type 2

#### **GENERAL TABULAR FUNCTIONS**

Examples of general tabular functions, including a 1-D and a 2-D function, are shown in section 2.8.6.

## 2.9 Reactor Kinetics Input Data

In order to activate the reactor kinetics model, a Control Function "reactor kinetics" (group number 3, type number 5 - see section 2.8.1, Table 2-22) must be present in the input deck. The reactor power, calculated by the Reactor Kinetics Package, is assigned to this Control Function. The reactor kinetics Control Function has one argument: the problem time. The value of the CF is the total reactor power (fission+decay) in case of normal (solid) fuel. In case of circulating fuel (IFTORK=2), the reactor kinetics function gives only the fission power, since in such case the decay power is calculated by the RT Package and is automatically added to the pool of Control Volumes. Furthermore, in case of circulating fuel, the following steps are taken:

- If the power source for a Control Volume, ITESCV, is defined through the "reactor kinetics" the power is added to the pool of CV only, never to the atmosphere.
- The value obtained from the reactor kinetics Control Function is used if the CV has sufficient amount of liquid, i.e. if the liquid fraction in CV is more than the limit XFULRK (record 748000).
- If the pool occupies less than XFULRK of the CV volume, the source obtained from the reactor kinetics Control Function is interpolated to obtain zero in case of empty volume, i.e. it is multiplied by  $(V_{pool}/V_{CV})/XFULRK$ . Here  $V_{pool}$  is the pool volume in CV and  $V_{CV}$  is the total volume of CV. This is done to automatically reduce the power generated in the pool of a CV when the pool is removed from this CV.

If the nodal point kinetics is used, then the total reactor power is available in the "reactor kinetics" Control Function, while the node-specific power is given in the subsequent Control Functions. For example, if the reactor kinetics function is defined as CF-100 and the nodal point kinetics model is used with 10 nodes, then the power is available as:

CF-100	tota	l reactor power,
0	CF-101	power in the node 1,
0	CF-102	power in the node 2,
0	CF-103	power in the node 3,
0	CF-104	power in the node 4,
0	CF-105	power in the node 5,
0	CF-106	power in the node 6,
0	CF-107	power in the node 7,
0	CF-108	power in the node 8,
0	CF-109	power in the node 9,
0	CF-110	power in the node 10.

The functions 101 through 110 must be present in the input deck and they must also be the "reactor kinetics" type (group number 3, type number 5)

# 2.9.1 Record: 750000, Reactor Kinetics Main Data

W-1 (R): PNGTRK Prompt neutron generation time,  $\Lambda$ , (s). If a negative value is entered, the generation time is computed from the Control Function |PNGTRK|. The value obtained from the Control Function is restricted to the range of:  $10^{-7} - 1.0$ . *Acceptable range:*  $10^{-7} \le \text{PNGTRK} \le 1.0$ . or reference to a Control Function

•

Default value:  $\Lambda = (v\Sigma_f v_n)^{-1}$ (all variables in this formula are defined below).

W-2 (R): SIGFRK Macroscopic fission cross section,  $\Sigma_f$ , (1/m). No default value is provided. A value for given reactor type must be entered (see example in 2.9.21 below). Acceptable range:  $10^{-4} \leq \text{SIGFRK} \leq 10^3$ Default value: none.

- W-3 (R) :XNPFRKNumber of neutrons generated per fission, v, (-).Acceptable range: $1.0 \le$  XNPFRK  $\le 5.0$ .Default value:2.5 ([1], sections 1.5.1, 1.5.2).
- W-4 (R) : QFISRK Heat released per fission,  $q_f$ , (J). Acceptable range:  $1.0 \cdot 10^{-13} \le \text{QFISRK} \le 1.0 \cdot 10^{-9}$ . Default value:  $3.09 \cdot 10^{-11}$ Note that  $1 \text{ MeV} = 1.602 \cdot 10^{-13}$  J. The default value is equal to 192.9 MeV, based on [5], 2, table 2-5.
- W-5 (R): CTHNRK Constant in thermal neutron velocity calculation,  $C_n$ . Thermal neutron velocity,  $v_n$ , is calculated from:

$$v_n = C_n \sqrt{T}$$

where *T* is temperature, determined by the word 6 below. Acceptable range:  $10.0 \leq \text{CTHNRK} \leq 1000.0$ . Default value: 128.0 ([5], equation 9-10). W-6(I): **ITN1RK** Indicator for thermal neutron temperature calculation. = 0: T is constant and equal to 400.0 K. This yields thermal neutron velocity of 2560 m/s. T is equal to the moderator temperature, defined by weighting = 1: factors, described in 2.9.19. = 2:T is equal to the fuel temperature, defined by weighting factors, described in section 2.9.18. = 3: T is equal to the value of Tabular Function No. ITN2RK (Word 7 below). = 4: T is equal to the value of Control Function No. ITN2RK (Word 7 below). Acceptable range:  $0 \leq \text{ITN1RK} \leq 4$ . Default value: 0. W-7 (I): ITN2RK Indicator for thermal neutron temperature calculation. if ITN1RK = 3: ITN2RK is a Tabular Function number, if ITN1RK = 4: ITN2RK is a Control Function number. *Acceptable range:* if ITN1RK = 3: valid reference number of a TF. valid reference number of a CF. if ITN1RK = 4: Default value: none. W-8 (R): EPSRK Fast fission factor,  $\varepsilon$ .

Acceptable range:  $1.0 \le \varepsilon \le 1.20$ .

		Default value:	1.02 ([5], chapter 3).		
W-9 (R) :	PRESRK	Resonance escape j Acceptable range:	probability, $p$ . $0.5 \le p \le 1.00$ . 0.87 ((51  shorter  2))		
W-10 (R) :	PFNLRK	Non-leakage proba	bility for fast neutrons, $P_{FNL}$ , (-).		
		Acceptable range: Default value:	$0.5 \le P_{FNL} \le 1.0.$ 0.97 ([5], chapter 3).		
W-11 (R) :	PTNLRK	Non-leakage proba Acceptable range:	bility for thermal neutrons, $P_{TNL}$ , (-). $0.5 \le P_{TNL} \le 1.0$ . $P_{FNL} \cdot P_{TNL} \ge 1/v$ or $\ge 1/(v \cdot p \cdot \varepsilon)$ , depending on the value of IDEPDK (word 12).		
		Default value:	0.99 ([5], chapter 3).		
W-12 (R) :	QDMLRK	Multiplier on decay Acceptable range: Default value:	wheat (for decay heat see sections 2.9.25, 2.9.36). $0.0 \le \text{QDMLRK} \le 5.0.$ 1.0.		
W-13 (I) :	IPERRK	Indicator defining how the reactivity effect due to isotope concentration changes is calculated (note: the reactivity effect due to isotope concentration changes can be disabled by using the input parameter IREIRK, record 748000): =1: do not include $p\varepsilon$ in reactivity effect calculation. In this case the reactivity effect is proportional to $1/(v \cdot P_{FNL} \cdot P_{TNL})$ - Volume 1), =2: include $p\varepsilon$ in reactivity effect calculation; in this case the reactivity effect is proportional to $1/(v \cdot p \cdot \varepsilon \cdot P_{FNL} \cdot P_{TNL})$ . Acceptable range: IPERRK = 1 or 2. Default value: 1.			
W-14 (R) :	SIGMRK	Minimum value of a fission cross section Acceptable range: Default value:	$\Sigma_f$ , (1/m). Calculations are stopped if the macroscopic n is smaller than this number. $0.0 \leq \text{SIGMRK} \leq 10^{-5}$ $10^{-6}$		

## 2.9.2 Record: 750XXX, Nodal Point Kinetics - Main Data

This record defines data for the nodal point kinetics model. XXX is the node number, *i*. The maximum number of nodes is NRKMAX = 50. This record defines the node specific values of the first two inputs in the record 750000:

- W-1, the prompt neutron generation time, PNGTRK(*i*) and
- W-2, the macroscopic fission cross section, SIGFRK(*i*).

The remaining input entries defined in the record 750000 (W-3 through W-14) are used for all nodes.

W-1 (R): PNGTRK(*i*)Prompt neutron generation time,  $\Lambda_i$ , (s), for the node i = XXX. If a negative value is entered, the generation time is computed from the

		Control Function	PNGTRK( <i>i</i> ) . The value obtained from the Control
		Function is restricted	ed to the range of: $10^{-7}$ - 1.0.
		Acceptable range:	$10^{-7} \le \text{PNGTRK} \le 1.0.$
			or reference to a Control Function
		Default value:	PNGTRK defined in the record 750000
W-2 (R) :	SIGFRK(i)	Macroscopic fission	n cross section, $\Sigma_{f,i}$ , (1/m), for the node $i = XXX$ .
		Acceptable range:	$10^{-4} \leq \text{SIGFRK}(i) \leq 10^3$
		Default value:	SIGFRK defined in the record 750000

The following input entries must be defined for the nodal point kinetics.

W-3 (R) : DCXNRK(*i*) Diffusion coefficient  $D_i$ , (m), in the node i = XXX. The diffusion coefficient is equal to:

$$D_i = \frac{1}{3\Sigma_{tri}}$$

Here  $\Sigma_{tr,i}$  is the macroscopic transport cross section (1/m). If a value <1.0 is entered, then the diffusion coefficient is constant and equal to the input value. If the value is  $\geq$  1.0 then the value is defined by a Tabular Function with the number DCXNRK. The argument for the Tabular Function is the node temperature, (K). The values obtained from the Tabular Function are internally limited to the range between 10<sup>-6</sup> and 1.0.

Acceptable range: $10^{-30} \leq \text{DCPKRK}(i) < 1.0$ <br/>or a reference to a valid Tabular Function<br/>noneDefault value:none

- W-4 (R) :DNXNRK(i)Thickness,  $d_i$ , (m), of the node i = XXX.<br/>Acceptable range:  $10^{-2} \leq \text{DNPKRK}(i) \leq 10^2$ <br/>Default value: none
- W-5 (R) : ANXNRK(*i*) Cross section area between the nodes i-1 and i,  $A_i$ , (m<sup>2</sup>). Acceptable range:  $0.0 \le \text{ANXNRK}(i) \le 10^4$ Default value: none

The nodal point kinetics discretization is shown in Figure 2-47. The nomenclature is as follows:



- volume of node i, (m<sup>3</sup>), RVOLRK,
- diffusion coefficient, node *i*, (m), DCXNRK,
- thickness, node *i*, (m), DNXNRK,
- area between nodes i-1 and i, (m<sup>2</sup>), ANXNRK,
- $n_i$  neutron density in, node *i*, (1/m<sup>3</sup>),
- $\Phi_i$  neutron flux, node *i*, (1/m<sup>2</sup>-s).

Figure 2-47 Discretization in the nodal point kinetics model

#### 2.9.3 Record: 750990, Nodal Point Kinetics - Additional Data

This record defines data for the nodal point kinetics model.

W-4 (R) :	ANXNRK(	N+1) Cross sectio Acceptable range: Default value:	n area at the last node, (m <sup>2</sup> ). $0.0 \le ANXNRK(N+1) \le 10^4$ ANXNRK(N)
W-2 (R) :	R1XNRK	Reflection factor, reflection (all neut neutron loss).	$F_{R1}$ , (-), for the first node. $F_{R1} = 0.0$ means no rons are lost), $F_{R1} = 1.0$ means perfect reflection (no
		Acceptable range:	$0.0 \le R1XNRK \le 1.0$
		Default value:	0.0
W-3 (R) :	RNXNRK	Reflection factor, reflection (all neutrineutron loss).	$F_{RN}$ , (-), for the last node. $F_{RN} = 0.0$ means no rons are lost), $F_{RN} = 1.0$ means perfect reflection (no
		Acceptable range:	$0.0 \le \text{RNXNRK} \le 1.0$
		Default value:	0.0

#### 2.9.4 Record: 750999, Nodal and Point Kinetics - Initialization Requests

This record defines data for the nodal point kinetics model or point kinetics.

W-1 (I): INONRK Initialization option: = 0: normal run = 1: initialization run applicable for nodal kinetics but not for circulating fuel (IFTORK=2). The nodal power distribution is calculated together with the initial concentrations of isotopes, using stationary-state formulation of isotope concentrations. Therefore the equilibrium concentrations of isotopes may be found relatively quickly for the nodal kinetics. Calculations are stopped when the desired accuracy is obtained. = 2: initialization run. general, applicable circulating fuel. This option can be used for nodal kinetics, however, the initial concentrations of isotopes (e.g. Xe-135) are those corresponding to the input power distribution and therefore very long calculations will be needed to obtain stationary concentrations of isotopes. The option INONRK = 2 simply provides an automatic power control for the reactor kinetics model. All parameters are calculated using transient equations, as in the case without power control (INONRK=0). Acceptable range: INONRK =0, 1, 2 Default value: 0

When INONRK>0 the code is automatically controlling the total reactor power through a PI controller, in order to keep the total power constant. The proportional and integral coefficients are defined in the input record 761000.

if ININRK=1:

W-2 (R): XCNNRK Convergence criterion. Used if INONRK=1. Calculations are stopped automatically, if maximum value of the relative change of neutron density in all nodes is smaller than this value:

$$XMXNRK = Max\left(\frac{1}{n_i}\frac{dn_i}{dt}\right) = Max\left(\frac{1}{n_i}\frac{\Delta n_i}{\Delta t}\right) < XCNNRK$$

- $n_i$  neutron density (1/m<sup>3</sup>) in the node *i*
- $\Delta n_i$  change of neutron density (1/m<sup>3</sup>) over a time step
- $\Delta t$  time step size (s)

If INONRK=1, the relative change  $(1/n_i)(dn_i/dt)$  is printed in the output file and the calculation is stopped when the maximum value <XCNNRK. If the maximum value is larger than XCNNRK until the end of the run, an error message is printed in the diagnostics file. Acceptable range:  $0.0 \le XCNNRK \le 10^{-5}$ Default value:  $10^{-7}$ 

a small number  $<10^{-50}$ , sets the value to 0.0; setting the value to 0.0 prevents the run from stopping

#### if ININRK=2:

W-2 (R): XCNNRK End-time for applying power control (s). The PI controller will be used only for time t < XCNNRK. *Acceptable range:* any real number *Default value:* 0.0

if ININRK=1 or 2:

W-3 (R): POW0RK Target total power, (W). Used if INONRK=1. Acceptable range: within 10% of the default, if non-zero Default value: described below

The user defines the fission power in every node in the record 751XXX, PINIRK(*i*). The total fission power is obtained as:

$$SPOWRK = \sum_{i} PINIRK(i)$$

If the Isotope Transformation model is used, then the decay power summed in all nodes is added to the fission power.

$$SQDPRK = \sum_{i} QDTPRK(i)$$

The node decay power, QDTPRK(i), is calculated as selected by the indicator ICITRK (input record 740000). Finally, the default value of the target power is equal to:

$$POW0RK = SPOWRK + SQDPRK$$

W-4 (I) :	IRPLRK	Reactivity versus multiplication factor as plot parameters - Table 2-29.
		= 1: reactivity is used as plot parameters: RK-000-Reac-0000

= 2: multiplication factors are used as plot parameters point kinetics:  $k_{eff}$  = RK-000-Keff-0000 nodal kinetics:  $k_{\infty}$  = RK-000-Kinf-0000

Acceptable range:	1 or 2	
Default value:	point kinetics:	1
	nodal kinetics:	2

#### 2.9.5 Record: 751000, Volume, Initial Fission Power and Initial Reactivity Data

W-1 (R) : RVOLRK	Total reactor volun	ne (fuel + moderator), $V_R$ , (m <sup>3</sup> ).		
	Acceptable range:	RVOLRK > 0.0.		
	Default value:	none.		

W-2 (R) : PINIRK Initial fission power, (W) (do not include the decay power). Acceptable range: PINIRK  $\geq 0.0$ . Default value: 0.0.

W-3 (R) : RINIRK Initial reactivity, (\$). Here 1 = sum of the global DNP yields for all groups,  $\sum$ [BTDNRK(i)] - section 2.9.12. The actual initial reactivity that is used (and can be plotted) will be converted based on the actual DNP yields calculated for the current fuel composition and the individual DNP yields, defined as input parameters BIDNRK. *Acceptable range:* all real numbers. *Default value:* 0.0.

W-4 (I) : IINIRK Indicator for the initial reactivity calculation:

- =1: Initial reactivity is given by RINIRK.
- =2: Initial reactivity is given by the Control Function ICINIRK. The Control Rod reactivity is included, i.e. the initial reactivity will be equal to the value of the Control Function ICINIRK, independently of the initial value of the Control Rod reactivity, defined in the record 760000.
- =3: Initial reactivity is given by the Control Function ICINIRK. The Control Rod reactivity is excluded, i.e. the initial reactivity will be equal to the value of the Control Function ICINIRK plus the initial value of the Control Rod reactivity, defined in the record 760000.
- Acceptable range: 1, 2, 3 Default value: 1
- W-5 (I): ICNIRK Control Function defining the initial reactivity, (\$) if the value of IINIRK is equal to 2 or 3.
  Acceptable range: a reference number of a Control Function if IINIRK is equal to 2 or 3. Zero if IINIRK is equal to 1.
  Default value: 0

#### 2.9.6 Record: 751XXX, Nodal Point Kinetics - Volume, etc. Data

This record defines data for the nodal point kinetics model. XXX is the node number, *i*. The maximum number of nodes is NRKMAX = 50. This record defines the node-specific values, which for the point kinetics model are defined in the record 751000.

W-1 (R) : RVOLRK(*i*) Total reactor volume (fuel + moderator),  $V_R$ , (m<sup>3</sup>), for the node i = XXX.

*Acceptable range:* RVOLRK > 0.0. *Default value:* none.

W-2 (R) : PINIRK(i)Initial fission power, (W) (do not include the decay power), for the node i = XXX.Acceptable range:PINIRK  $\geq 0.0$ .Default value:0.0.

- W-3 (R) : RINIRK(*i*) Initial reactivity, (\$), for the node i = XXX. *Acceptable range:* all real numbers. *Default value:* 0.0.
- W-4 (I) : IINIRK(*i*) Indicator for the initial reactivity calculation for the node i = XXX:
  - =1: Initial reactivity is given by RINIRK(*i*).
  - =2: Initial reactivity is given by the Control Function ICINIRK(*i*). The Control Rod reactivity is included, i.e. the initial reactivity will be equal to the value of the Control Function ICINIRK(*i*), independently of the initial value of the Control Rod reactivity, defined in the record 760XXX.
  - =3: Initial reactivity is given by the Control Function ICINIRK(*i*). The Control Rod reactivity is excluded, i.e. the initial reactivity will be equal to the value of the Control Function ICINIRK(*i*) plus the initial value of the Control Rod reactivity, defined in the record 760XXX.
    Acceptable range: 1, 2, 3

*Default value:* 1

W-5 (I): ICNIRK(i) Control Function defining the initial reactivity, (\$), for the node i = XXX. Only used if the value of IINIRK(i) is equal to 2 or 3.
Acceptable range: must be a valid reference number of a Control Function if IINIRK(i) is equal to 2 or 3.
Default value: 0

#### 2.9.7 Record: 755000, External Neutron Source Data

W-1 (I):ISRCRKPointer to a Tabular or Control Function that defines the external neutron<br/>source, S. If the number is positive then the source will be defined by a<br/>Tabular Function with the number: ISRCRK. If the number is negative<br/>then the source will be defined by a Control Function with the number:<br/>| ISRCRK |. The units obtained from the Tabular or Control Function<br/>are assumed to be (neutrons/s). The volumetric source,  $S_V$ , is equal to:  $S_V$ <br/> $= S/V_R$ , where  $V_R$  is the reactor volume, defined in record 751000 (2.9.5).<br/>Acceptable range:<br/>must be a valid reference number of a tabular or a<br/>Control Function. The "Reactor Kinetics" type CF<br/>cannot be used.<br/>Default value:<br/>0.

## 2.9.8 Record: 755XXX, Nodal Point Kinetics - External Neutron Source Data

This record defines data for the nodal point kinetics model. XXX is the node number, *i*. The maximum number of nodes is NRKMAX = 50. This record defines the node-specific values, which for the point kinetics model are defined in the record 755000.

W-1 (I) :ISRCRK(i)Pointer to a Tabular or Control Function that defines the external neutron<br/>source, S, for the node i = XXX. If the number is positive then the source<br/>will be defined by a Tabular Function with the number: ISRCRK. If the<br/>number is negative then the source will be defined by a Control Function<br/>with the number: | ISRCRK|. The units obtained from the Tabular or<br/>Control Function are assumed to be (neutrons/s). The volumetric source,<br/> $S_V$ , is equal to:  $S_V = S/V_R$ , where  $V_R$  is the reactor volume, defined in<br/>record 751XXX.<br/>Acceptable range: must be a valid reference number of a tabular or a<br/>Control Function. The "Reactor Kinetics" type CF<br/>cannot be used.<br/>Default value: 0.

#### 2.9.9 Record: 760000, Control Rod Reactivity Data

- W-1 (I): IREARK(1) Pointer to a Tabular or Control Function that defines the reactivity. If the number is positive then the reactivity will be defined by a Tabular Function with the number: IREARK(1). If the number is negative then the reactivity will be defined by a Control Function with the number: |IREARK(1)|. The units obtained from the Tabular or Control Function are assumed to be (\$). Here 1\$ = sum of the global DNP yields for all groups,  $\sum [BTDNRK(i)]$  section 2.9.12.
  - Acceptable range: must be a valid reference number of a tabular or a Control Function. The "Reactor Kinetics" type CF cannot be used.

*Default value:* 0.

W-2 (I):IREARK(2)Pointer to a Tabular or Control Function that defines the<br/>reactivity. If the number is positive then the reactivity will be defined by<br/>a Tabular Function with the number: IREARK(2). If the number is<br/>negative then the reactivity will be defined by a Control Function with<br/>the number: |IREARK(2)|. The units obtained from the Tabular or<br/>Control Function are assumed to be (\$). Here 1\$ = sum of the global<br/>DNP yields for all groups,  $\sum [BTDNRK(i)]$  - section 2.9.12.<br/>Acceptable range: must be a valid reference number of a tabular or a<br/>Control Function. The "Reactor Kinetics" type CF<br/>cannot be used.<br/>Default value: 0.

... until all reactivity tables are defined. The maximum number of reactivity tables is 50.

#### 2.9.10 Record: 760XXX, Nodal Point Kinetics - Control Rod Reactivity Data

This record defines data for the nodal point kinetics model. XXX is the node number, *i*. The maximum number of nodes is NRKMAX = 50. This record defines the node-specific values, which for the point kinetics model are defined in the record 760000.

- W-1 (I): Pointer to a Tabular or Control Function that defines the reactivity IREARK(1, i)for the node i = XXX. If the number is positive, the reactivity will be defined by a Tabular Function with the number: IREARK(1). If the number is negative then the reactivity will be defined by a Control Function with the number: |IREARK(1)|. The units obtained from the Tabular or Control Function are assumed to be (\$). Here 1\$ =sum of the global DNP yields for all groups,  $\sum$ [BTDNRK(i)] - section 2.9.12. Acceptable range: must be a valid reference number of a tabular or a Control Function. The "Reactor Kinetics" type CF cannot be used. Default value: 0. W-2(I): IREARK(2, i)Pointer to a Tabular or Control Function that defines the reactivity for the node i = XXX. If the number is positive, the reactivity will be defined by a Tabular Function with the number: IREARK(2). If the number is negative then the reactivity will be defined by a Control Function with the number: | IREARK(2) |. The units obtained from the
  - Tabular or Control Function are assumed to be (\$). Here 1\$ = sum of the<br/>global DNP yields for all groups, ∑[BTDNRK(i)] section 2.9.12.Acceptable range:must be a valid reference number of a tabular or a<br/>Control Function. The "Reactor Kinetics" type CF<br/>cannot be used.Default value:0.
- ... until all reactivity tables are defined. The maximum number of reactivity tables is 50.

#### 2.9.11 Record: 761000, Power Control

This record defines the automatic power control, used to keep the reactor power constant in one of the following situations.

- When the CV/JN/... packages are deactivated, and the constant reactor power option is requested (IRKSL=2 in the record 900XXX).
- When the nodal point kinetics model is used and the initialization option is requested (INONRK=1 in the record 750999).
- When INONRK=2 in the record 750999.

The power control is performed by the Solver by inserting or removing reactivity, according to the following formula:

$$R(t) = CPCVRK \times \left(\frac{Q_{tar} - Q(t)}{Q_{tar}}\right) + CICVRK \times \int_{t_0}^t \left(\frac{Q_{tar} - Q(t')}{Q_{tar}}\right) dt'$$

where R(t) is the control system reactivity, (\$), and  $Q_{tar}$  it the target power, (W), equal to the reactor power at the time when:

- CV/JN/... packages become inactive (when IRKSL=2),
- Start of the calculations (when INONRK=1).

W-1 (I) :	CPCVRK	Constant in the proportional part of the PI reactor power controller. Acceptable range: $10^{-6} \le CPCVRK \le 10^{+1}$ Default value: 1.0
W-2 (I) :	CICVRK	Constant in the integral part of the PI reactor power controller.Acceptable range: $10^{-6} \le CPCVRK \le 10^{+1}$ Default value:1.0

#### 2.9.12 Record: 770XXX, Delayed Neutron Precursor Data

XXX = 001, 002, ..., NDNGRK, is the number of the delayed neutron precursor group. The maximum number of delayed neutron precursor groups is 10. SPECTRA contains data for eight groups of delayed neutrons, which is being used if no data is entered. Thus, by default NDNGRK is equal to 8. If records 770XXX are entered, then the NDNGRK is equal to the largest value of XXX. For XXX = 1 through 8 any of the entries described below may be entered as zero to use the built-in value.

W-1 (R) :	BTDNRK	Yield of the group	XXX, $\beta_{i=XXX}$ , (-).
		Acceptable range:	$10^{-6} \le \text{BTDNRK} \le 10^{-2}$
		Default value:	values for U-235, shown in the example below
W-2 (R) :	DCDNRK	Decay constant of t	he group XXX, $\lambda_{i=XXX}$ , (1/s).
		Acceptable range:	$10^{-4} \le \text{DCDNRK} \le 10^2$
		Default value:	values for U-235, shown in the example below

#### **Example:**

In the example below, the delayed neutron precursors are defined using the data for thermal fission of U-235:

*	DELAYED NEUT	FRON DATA
*	BTDNRK (-)	DCDNRK (1/s)
770001	2.145E-04	1.24667E-02
770002	1.001E-03	2.82917E-02
770003	5.915E-04	4.25244E-02
770004	1.281E-03	1.33042E-01
770005	2.151E-03	2.92467E-01
770006	5.850E-04	6.66488E-01
770007	5.265E-04	1.63478E+00
770008	1.495E-04	3.55460E+00

Using the following inputs, the user may define individual yield fractions, specific to all fissile isotopes in the problem. If the input entries are present, there must be exactly the same values as the number of fissile isotopes (isotopes with positive fission cross section, SFITRK>0.0) present in the RK Package. Zeroes may be entered; in such case the value will be set to the average yield, BTDNRK.

W-3 (R): BIDNRK(1)Individual yield of the group XXX from the first fissile isotope. Acceptable range:  $0.0 \le BIDNRK(1) \le 10^{-2}$ 

*Default value:* BTDNRK

W-4 (R): BIDNRK(2)Individual yield of the group XXX from the first fissile isotope. Acceptable range:  $0.0 \le BIDNRK(2) \le 10^{-2}$ Default value: BTDNRK

[...] until the yields are defined for all fissile isotopes.

#### **Example:**

In the example below, the fission yields of delayed neutron precursors are defined for:

- U-235, Pu-239, and Pu-241.
- Assuming that all default fuel chains are present, the fissile isotopes are:
  - U-233, U-235, U-239, Pu-239, Pu-241.

The following input defines individual yields for U-233 and Pu-239, based on the available data (see Volume 1). It is assumed that the values for U-239 are the same as for U-235 (defined as BTDNRK), while the values for Pu-241 are assumed to be the same as for Pu-239.

*	DELAYED NEUTH	individual	yields	(BIDNRF	K)		
*	BTDNRK (-)	DCDNRK (1/s)	U-233	U-235	U-239	Pu-239	Pu-241
770001	2.145E-04	1.24667E-02	8.580E-05	0	0	6.930E-05	6.930E-05
770002	1.001E-03	2.82917E-02	4.004E-04	0	0	3.234E-04	3.234E-04
770003	5.915E-04	4.25244E-02	2.366E-04	0	0	1.911E-04	1.911E-04
770004	1.281E-03	1.33042E-01	5.122E-04	0	0	4.137E-04	4.137E-04
770005	2.151E-03	2.92467E-01	8.606E-04	0	0	6.951E-04	6.951E-04
770006	5.850E-04	6.66488E-01	2.340E-04	0	0	1.890E-04	1.890E-04
770007	5.265E-04	1.63478E+00	2.106E-04	0	0	1.701E-04	1.701E-04
770008	1.495E-04	3.55460E+00	5.980E-05	0	0	4.830E-05	4.830E-05

The actual yields will be determined based on the current fuel composition, using the values of BIDNRK. The value of BTDNRK is serving only as a definition of the default value. The correctness of input may be checked in the \*.OUT file, where it is printed below the isotope data, in the following block:

=RK=	INDIVIDUAL	FISSION	YIELDS	FOR	8	DELAYED	NEUTRON	PRECURSOR

	GLOBAL	INDIVIDUAL F	OR FISSILE IS	OTOPES, BIDNR	к:	
Group	BTDNRK	U-233	U-235	U-239	Pu-239	Pu-241
Ţ	2.14500E-04	8.58000E-05	2.14500E-04	2.14500E-04	6.93000E-05	6.93000E-05
2	1.00100E-03	4.00400E-04	1.00100E-03	1.00100E-03	3.23400E-04	3.23400E-04
3	5.91500E-04	2.36600E-04	5.91500E-04	5.91500E-04	1.91100E-04	1.91100E-04
4	1.28100E-03	5.12200E-04	1.28100E-03	1.28100E-03	4.13700E-04	4.13700E-04
5	2.15100E-03	8.60600E-04	2.15100E-03	2.15100E-03	6.95100E-04	6.95100E-04
6	5.85000E-04	2.34000E-04	5.85000E-04	5.85000E-04	1.89000E-04	1.89000E-04
7	5.26500E-04	2.10600E-04	5.26500E-04	5.26500E-04	1.70100E-04	1.70100E-04
8	1.49500E-04	5.98000E-05	1.49500E-04	1.49500E-04	4.83000E-05	4.83000E-05
Sum:	6.50000E-03	2.60000E-03	6.50000E-03	6.50000E-03	2.10000E-03	2.10000E-03

Note!

The definition of dollars is always based on the values of BTDNRK; where 1 \$ = sum of the global DNP yields for all groups, [BTDNRK(i)]. The reactivity sources (records 760XXX) and the feedback coefficients (records 784XXX) should always be defined using this value (in the example above it is equal to: 6.78286E-3) - see Volume 3, test cases DNP-1, DNP-2.

## 2.9.13 Records: 780000, Reactivity Feedback Data – Selection of Independent Variable

W-1 (I):	IRFDRK	Indicator determining the independent variable for how the moderator			
		feedback calculation (the moderator feedback data table is defined			
		records 782XXX). The independent variable is:			
=1: Moderator te		=1: Moderator temperature, (K)			
		=2: Moderator density, $(kg/m^3)$			
		Acceptable range: 1 or 2.			
		Default value: 1.			

#### 2.9.14 Records: 781XXX, Reactivity Feedback Data - Fuel Temperatures

The reactivity feedback table is defined in records 781XXX, 782XXX, 783XXX, and 784XXX. Record 781XXX contains fuel temperature coordinate data. XXX is the point number in reactivity feedback data tables. The total number of data points in the reactivity feedback data tables may not exceed a maximum of NRFMAX = 50.

W-1 (R) :	TFTBRK	Fuel temperature c point XXX, $T_{f,T}(XX)$	oordinate value for reactivity feedback table, at the (X), (K).
		Acceptable range:	Values of TFTBRK must increase. Thus the value
			for the point XXX must be greater than the value for
			the point XXX–1.
		Default value:	none.

# 2.9.15 Records: 782XXX, Reactivity Feedback Data - Moderator Temperatures/densities

The reactivity feedback table is defined in records 781XXX, 782XXX, 783XXX, and 784XXX. Record 782XXX contains moderator temperature coordinate data. XXX is the point number. The total number of data points may not exceed a maximum of NRFMAX = 50.

W-1 (R) :TMTBRKModerator temperature or density (depending on the value of IRFDRK<br/>defined in the record 780000) coordinate value for reactivity feedback<br/>table at point XXX,  $T_{m,T}(XXX)$ , (K) or (kg/m<sup>3</sup>).<br/>Acceptable range:Values of TMTBRK must increase. Thus the value<br/>for the point XXX must be greater than the value for<br/>the point XXX-1.<br/>Default value:

## 2.9.16 Record: 783XXX, Reactivity Feedback Data - Void Fractions

The reactivity feedback table is defined in records 781XXX, 782XXX, 783XXX, and 784XXX. Record 783XXX contains void fraction coordinate data. XXX is the point number. The total number of data points may not exceed a maximum of NRFMAX = 50.

W-1 (R) :VFTBRKVoid fraction coordinate value for reactivity feedback table at the point<br/>XXX,  $\alpha_T(XXX)$ , (-).Acceptable range:Values of VFTBRK must increase. Thus the value<br/>for the point XXX must be greater than the value for<br/>the point XXX-1.Default value:none.

#### 2.9.17 Record: 784XXX, Reactivity Feedback Data - Reactivities

The reactivity feedback table is defined in records 781XXX, 782XXX, 783XXX, and 784XXX. Record 784XXX contains reactivity data. XXX is just a record identifying number and does not need to be consecutive. The total number of data points may not exceed a maximum of NRFMAX = 50. If no data is entered, but coordinate values are entered, that means records 781XXX, 782XXX, 783XXX are present in input file, but records 784XXX are not present, then default values are used (see below).

Two formats may be used, namely: independent reactivity table format, with 3 entries per record (Format 2), and full reactivity table format, with four entries per record (Format 1). Data must be entered consistently. Once a given format is chosen, all entries must be given in the same format.

Independent reactivity table format (Format 2):

Using Format 2 three independent reactivity tables are created:

- 1.)  $R_{f,T}(i) = f(T_{f,T}(i)),$
- 2.)  $R_{m,T}(j) = f(T_{m,T}(j)), or f(\rho_{m,T}(j)),$
- 3.)  $R_{\alpha,T}(k) = f(\alpha_T(k)).$

The full reactivity table is then created by the code, as a sum of the individual values:

$$R_{T}(i,j,k) = R_{f,T}(i) + R_{m,T}(j) + R_{\alpha,T}(k).$$

When this format is used reactivity values for all data points must be entered.

W-1 (I): L Indicator of data type: =1: this record contains the fuel temperature reactivity table,  $R_{fT}(T_{fT})$ . =2: this record contains the moderator temperature or density reactivity table,  $R_{m,T}(T_{m,T})$ . this record contains the void fraction reactivity table,  $R_{\alpha,T}(\alpha,T)$ . =3: Acceptable range: 1, 2, 3. Default value: none. Point number, W-2(I): i, j, or kif L = 1: point number in fuel temperature reactivity table, *i*, if L = 2: point number in moderator temperature reactivity table, *j*, if L = 3: point number in void fraction reactivity table, k, Acceptable range: if L = 1: 1, 2, ..., NTFFRK, where NTFFRK is equal to the number of data points entered in record 781XXX. if L = 2: 1, 2, ..., NTMFRK, where NTMFRK is equal to the number of data points entered in record 782XXX. if L = 3: 1, 2, ..., NVFFRK, where NVFFRK is equal to the number of data points entered in record 783XXX.

Default value: none.

W-3 (R): RXTBRK reactivity value (\$). Here 1\$ = sum of the global DNP yields for all groups,  $\sum$ [BTDNRK(i)] - section 2.9.12. if L = 1:  $R_{f,T}(i) = f(T_{f,T}(i))$ , if L = 2:  $R_{m,T}(j) = f(T_{m,T}(j))$ , if L = 3:  $R_{\alpha,T}(k) = f(\alpha_T(k))$ . *Acceptable range:* all real numbers. *Default value:* see below.

#### Full reactivity table format (Format 1):

Using Format 1 the full reactivity table is entered: R(i,j,k), where i = 1, ..., NTFFRK, j = 1, ..., NTMFRK, k = 1, ..., NVFFRK. Using this format it is not necessary to enter reactivity values for all data points. User may leave "gaps" in the reactivity table. These gaps will be filled in by the program, using linear interpolation (see description below).

W-1 (I) :	i	Fuel temperature per Acceptable range: Default value:	oint number. 1,, NTFFRK. none.
W-2 (I) :	j	Moderator tempera Acceptable range: Default value:	ture or density point number. 1,, NTMFRK. none.
W-3 (I) :	k	Void fraction point Acceptable range: Default value:	number. 1,, NVFFRK. none.
W-4 (R) :	RCTBRK	reactivity value at t = $R_T$ ( $T_{f,T}(i)$ , $T_{m,T}(j)$ Acceptable range: Default value:	he point <i>i</i> , <i>j</i> , <i>k</i> : $R_T(i,j,k) =$ ), $\alpha_T(k)$ ). all reals. see below.

#### Default values of reactivity feedback

The default values of reactivity feedback are used if no data is entered in records 784XXX, but coordinate values are entered in records 781XXX, 782XXX, 783XXX. At least one coordinate point must be entered in each of these record types. The entered coordinate values are meaningless, since they will be overwritten by the built-in data. The default values are based on reactivity coefficients shown in [5], table 14-2.

<ul><li>Fuel temperature:</li><li>Moderator temperature:</li><li>Void fraction:</li></ul>	$\begin{array}{l} \partial \rho / \partial T_{\rm fuel} \approx -3.0 \cdot 10^{-5} \ ({\rm K}^{-1}), \\ \partial \rho / \partial T_{\rm mod} \approx -2.5 \cdot 10^{-4} \ ({\rm K}^{-1}), \\ \partial \rho / \partial \alpha \ \approx -1.5 \cdot 10^{-3} \ (\%^{-1}), \end{array}$	$\begin{split} &\partial R/\partial T_{\rm fuel}\approx-5.0\times10^{-3}(\text{\$/K}),\\ &\partial R/\partial T_{\rm mod}\approx-4.0\times10^{-2}(\text{\$/K}),\\ &\partial R/\partial\alpha\approx-2.0\times10^{-1}(\text{\$/\%}). \end{split}$
The built-in tables are:	$\begin{array}{l} T_{fuel} = 0.0 \ K \\ T_{fuel} = 10000.0 \ K \end{array}$	R = 0.0 R = -50.0
	$\begin{split} T_{mod} &= 0.0 \text{ K} \\ T_{mod} &= 10000.0 \text{ K} \end{split}$	R = 0.0 R = -400.0

$\alpha = 0.0$	R = 0.0 \$
$\alpha = 1.0$	R = -20.0 \$

#### "Gaps" in reactivity table

When the full reactivity table format is selected, then gaps may be left in the table, that means not all reactivity values need to be entered. The gaps are filled in by the program, using linear interpolation. The interpolation is performed in each of the three "dimensions", between the two closest defined points, bounding the gap from both sides (Figure 2-48). No extrapolation is performed; the defined points must be bounding the point being filled in from both sides. If such points cannot be found in given direction, then interpolation is skipped in this direction.

Therefore up to 3 interpolations may be performed to fill a gap. If three or two interpolations are performed, then an arithmetic average is calculated, and then assigned to the gap - Figure 2-48 (a) and (b). If one interpolation is performed, then the resulting value is assigned to the gap - Figure 2-48 (c). If no interpolation is performed, then an error message is printed and the execution is stopped - Figure 2-48 (d). Only the user defined points are used for interpolation. The points, for which values have been obtained previously by interpolations, are not used in subsequent interpolations.

The method of calculating average value of independent interpolations is used to fill the gaps rather than a full 3-dimensional interpolation (see description of 3-d interpolation below), because in practice it would be difficult to find 8 defined points bounding the gap from all directions. Thus a full 3-d interpolation scheme would often fail because of lack of data. With the applied scheme the interpolation will fail for the first and the last points: (i=1, j=1, k=1), (i=NTFFRK, j=NTMFRK, k=NVFFRK), so these points must be filled in by the user. But other points, or whole rows of data may be left out and they will be filled in by interpolation.

#### Linear interpolation in 3-D space to obtain reactivity

Once the reactivity table is filled, the program can start calculations. During calculations reactivity is calculated for actual values of fuel temperature,  $T_{fuel}$ , moderator temperature,  $T_{mod.}$ , and void fraction,  $\alpha$  (see sections 2.9.18, 2.9.19, and 2.9.20, for the description how  $T_{fuel}$ ,  $T_{mod.}$  and  $\alpha$  are obtained). This is done by performing linear interpolation in a 3-dimensional "space", using eight tabulated points bounding the ( $T_{fuel}$ ,  $T_{mod.}$ ,  $\alpha$ ) point from all sides - Figure 2-49. No extrapolation is performed. The end point values are kept outside the tabulated space

The interpolations are performed in the following order (see Figure 2-49). First, four interpolations are performed for the fuel temperature direction. Next, two interpolations are performed in the moderator temperature direction. Finally, the last interpolation is performed in the void fraction direction.

Since all interpolations are linear, the order of interpolations is meaningless. The same end value would be obtained by, for example, performing first four interpolations in  $T_{mod.}$ , next two interpolations in  $\alpha$ , and finally one interpolation in  $T_{fuel.}$ 





Figure 2-48 Interpolations to fill gaps in the reactivity feedback table.



Figure 2-49 Calculating reactivity by 3-D linear interpolation in reactivity feedback table.

# 2.9.18 Record: 791XXX, Weighting Factors - Fuel Temperatures

The weighting factors are defined in records 791XXX, 792XXX, and 793XXX. Record 791XXX contains fuel temperature weighting factors. The value of XXX is equal to:

• in case	e of point kin	etics: XXX	= 000,
• in case	e of nodal poi	nt kinetics: XXX	= node number.
W-1 (I) :	ITF1RK	Region indicator 1. = 1: 1-D Solid H for this regio = 2: 2-D Solid H for this region = 3: Control Vol this region. = 4: Control V temperature Acceptable range: Default value:	leat Conductor temperature defines fuel temperature on. leat Conductor temperature defines fuel temperature on. ume pool temperature defines fuel temperature for folume atmosphere temperature defines fuel for this region. 1, 2, 3, 4 for circulating fuel (IFTORK=2): 3 1.
W-2 (I) :	ITF2RK	Region indicator 2. if ITF1RK=1: if ITF1RK=2: if ITF1RK=3: if ITF1RK=4: Acceptable range: Default value:	<ul> <li>Defines SC, TC, or CV number for this region.</li> <li>1-D Solid Heat Conductor number,</li> <li>2-D Solid Heat Conductor number,</li> <li>Control Volume number,</li> <li>Control Volume number.</li> <li>must be a valid reference number of a 1-D, 2-D</li> <li>Solid Heat Conductor, or a Control Volume.</li> <li>none.</li> </ul>
W-3 (I) :	ITF3RK	Region indicator 3. Conductor are with if ITF1RK=1: if ITF1RK=2: if ITF1RK=3: if ITF1RK=4: <i>Acceptable range:</i> if ITF1RK=1: if ITF1RK=2 <i>Default value:</i>	Defines which mesh cells of a 1-D or 2-D Solid Heat in this region. Starting cell number of a 1-D Heat Conductor. Starting cell number of a 2-D Heat Conductor. not used, not used. $1 \le ITF3RK \le NCELSC(ITF2RK).$ $1 \le ITF3RK \le NCELTC(ITF2RK).$ none.
W-4 (I) :	ITF4RK	Region indicator 4. Conductor are with if ITF1RK=1: if ITF1RK=2: if ITF1RK=3: if ITF1RK=4: <i>Acceptable range:</i> if ITF1RK=1: if ITF1RK=2: <i>Default value:</i>	Defines which mesh cells of a 1-D or 2-D Solid Heat in this region. Last cell number of a 1-D Heat Conductor. Last cell number of a 2-D Heat Conductor. not used, not used. ITF3RK $\leq$ ITF4RK $\leq$ NCELSC(ITF2RK). ITF3RK $\leq$ ITF4RK $\leq$ NCETSC(ITF2RK). none.

- W-5 (R) :WTFFRKWeighting factor,  $W_{TF}$ , for the region defined by the words 1 through 4.<br/>The values will be normalized to 1.0 if all factors are positive. If any<br/>factor is negative, then no normalization is performed and all fuel<br/>temperature weighting factors will be used as entered. NOTE: in such<br/>case the value of average fuel temperature (RK-000-Tfue-0000 Table<br/>2-29) will not have a physical meaning.<br/>Acceptable range: WTFFRK  $\neq 0.0$ <br/>for circulating fuel (IFTORK=2): WTFFRK>0.0<br/>Default value:<br/>none.
- W-6 (R): WTCFRK Used only for circulating fuel (IFTORK=2). This word defines fraction of isotopes that are generated in the region defined by the words 1 through 4. The values will be normalized to 1.0. Thioretically this value represents fraction of core power generated in this region. If no value is entered, then WTFFRK will be used for this core region. In such case it is required that all WTFFRK values are positive. *Acceptable range:* WTCFRK > 0.0 *Default value:* WTFFRK.
- W-7 (I):IRegion number. If no value, or zero is entered, then the region data are<br/>read sequentially the first record in the input is interpreted as containing<br/>the first (lower) region data (I=1), then I=2, etc. The total number of<br/>regions is equal to NTFWRK  $\leq$  NWFMAX = 200.<br/>Acceptable range: I = 1, 2, ..., 200<br/>Default value: none

## 2.9.19 Record: 792XXX, Weighting Factors - Moderator Temperatures or Densities

The weighting factors are defined in records 791XXX, 792XXX, and 793XXX. Record 792XXX contains moderator temperature weighting factors. The value of XXX is equal to:

- in case of point kinetics: XXX = 000,
- in case of nodal point kinetics: XXX = node number.

W-1 (I): ITM1RK Region indicator 1.

- = 1: 1-D Solid Heat Conductor temperature defines moderator temperature for this region.
- = 2: 2-D Solid Heat Conductor temperature defines moderator temperature for this region.
- = 3: Control Volume pool temperature or density (depending on IRFDRK – see record 780000) defines moderator temperature for this region.
- = 4: Control Volume atmosphere temperature or density (depending on IRFDRK – see record 780000) defines moderator temperature for this region.
- Acceptable range: 1, 2, 3, and 4. If the moderator density is used (IRFDRK is equal to 2 in record 780000), the acceptable values are 3 and 4.

Default value:

3.

W-2 (I) :	ITM2RK	Region indicator 2. if ITM1RK=1: if ITM1RK=2: if ITM1RK=3: if ITM1RK=4: Acceptable range: Default value:	Defines SC number or CV number for this region. 1-D Solid Heat Conductor number, 2-D Solid Heat Conductor number, Control Volume number, Control Volume number. must be a valid reference number of a 1-D , 2-D Solid Heat Conductor, or a Control Volume. none.
W-3 (I) :	ITM3RK	Region indicator 3. Conductor are with if ITM1RK=1: if ITM1RK=2: if ITM1RK=3: if ITM1RK=4: Acceptable range: if ITM1PK=1:	Defines which mesh cells of a 1-D or 2-D Solid Heat in this region. Starting cell number of a 1-D Heat Conductor. Starting cell number of a 2-D Heat Conductor. not used, not used.
		if ITM1RK=1. <i>Default value:</i>	$1 \le \text{ITM3RK} \le \text{NCELSC(ITM2RK)}.$ $1 \le \text{ITM3RK} \le \text{NCELTC(ITM2RK)}.$ none.
W-4 (I) :	ITM4RK	Region indicator 4. Conductor are with if ITM1RK=1: if ITM1RK=2: if ITM1RK=3: if ITM1RK=4: <i>Acceptable range:</i> if ITM1RK=1: if ITM1RK=2: <i>Default value:</i>	Defines which mesh cells of a 1-D or 2-D Solid Heat in this region. Last cell number of a 1-D Heat Conductor. Last cell number of a 2-D Heat Conductor. not used, not used. ITM3RK ≤ ITM4RK ≤ NCELSC(ITM2RK). ITM3RK ≤ ITM4RK ≤ NCETSC(ITM2RK). none.
W-5 (R) :	WTMFRK	Weighting factor, W The values will be factor is negative, the temperature/density such case the value Tmod-0000 - Table Acceptable range: Default value:	$W_{TM}$ , for the region defined by the words 1 through 4. normalized to 1.0 if all factors are positive. If any hen no normalization is performed and all moderator weighting factors will be used as entered. NOTE: in of average moderator temperature/density (RK-000- e 2-29) will not have a physical meaning. WTMFRK $\neq 0.0$ . none.
W-6 (I) :	Ι	Region number. If read sequentially - t the first (lower) re regions is equal to 1 Acceptable range: Default value:	no value, or zero is entered, then the region data are he first record in the input is interpreted as containing gion data (I=1), then I=2, etc. The total number of NTMWRK $\leq$ NWFMAX = 200 I = 1, 2,, 200 none

# 2.9.20 Record: 793XXX, Weighting Factors - Void Fractions

The weighting factors are defined in records 791XXX, 792XXX, and 793XXX. Record 793XXX contains void fraction weighting factors. The value of XXX is equal to:

• i • i	n case of point kind n case of nodal poi	etics: X nt kinetics: X	XXX = 000, XXX = node number (maximum of 50 nodes)
W-1 (I) :	IVF1RK	Region indica = 1: Local $x$ Solid H = 2: $X_{pool,SC}$ Effective is the u at the p = 3: Local $x$ Solid H = 4: $X_{pool,TC}$ Effective boundar pool. $X$ fraction = 5: Averag = 6: $X_{pool,CV}$ Effective of CV of by atmost	tor 1. void fraction, $\alpha_{SC}$ , in the pool-covered fraction of a 1-D leat Conductor surface. $\alpha_{SC} + X_{atms,SC}$ ve local void fraction at a 1-D Solid Heat Conductor $\alpha_{SC}$ is the fraction of surface covered by pool. $X_{atms,SC}$ incovered fraction of surface. $\alpha_{SC}$ is the local void fraction pool-covered part of the SC surface. void fraction, $\alpha_{TC}$ , in the pool-covered fraction of a 2-D leat Conductor boundary cell. $\alpha_{TC} + X_{atms,TC}$ ve local void fraction at a 2-D Solid Heat Conductor try cell. $X_{pool,TC}$ is the fraction of cell surface covered by $X_{atms,TC}$ is the uncovered fraction. $\alpha_{TC}$ is the local void in at the pool-covered part of the TC cell surface. the void fraction, $\alpha_{CV}$ , in a CV pool. $\alpha_{CV} + X_{atms,CV}$ ve void fraction in a Control Volume. $X_{pool,CV}$ is the fraction occupied by pool. $X_{atms,CV}$ is the fraction of CV occupied ophere. $\alpha_{CV}$ is the average void fraction in the pool of CV. trge: 1, 2, 3, 4, 5, and 6. $\therefore 2.$
W-2 (I) :	IVF2RK	Region indica if IVF1RK=1: if IVF1RK=2: if IVF1RK=3: if IVF1RK=4: if IVF1RK=5: if IVF1RK=6: Acceptable rational Default value:	<ul> <li>tor 2. Defines SC number or CV number for this region.</li> <li>1-D Solid Heat Conductor number,</li> <li>1-D Solid Heat Conductor number,</li> <li>2-D Solid Heat Conductor number,</li> <li>2-D Solid Heat Conductor number,</li> <li>Control Volume number,</li> <li>Control Volume number.</li> <li>mge: must be a valid reference number of a 1-D, 2-D Solid Heat Conductor, or a Control Volume.</li> <li>none.</li> </ul>
W-3 (I) :	IVF3RK	Region indica Conductor, or considered. if IVF1RK=1, if IVF1RK=3, if IVF1RK=5, Acceptable ra	<ul> <li>ator 3. Defines which surface of a 1-D Solid Heat</li> <li>which boundary cells of a 2-D Solid Heat Conductor are</li> <li>,2: IVF3RK = -1: left surface, IVF3RK = +1: right surface.</li> <li>,4: Starting cell number of a 2-D Heat Conductor.</li> <li>,6: not used.</li> <li><i>inge:</i> if IVF1RK=1, 2: -1, or +1. if IVF1RK=3, 4: boundary cell number.</li> </ul>

*Default value:* none.

W-4 (I):IVF4RKRegion indicator 4. Defines which boundary cells of a 2-D Solid Heat<br/>Conductor are within this region.<br/>if IVF1RK=1, 2: not used.<br/>if IVF1RK=3, 4: Last cell number of a 2-D Heat Conductor.<br/>if IVF1RK=5, 6: not used.<br/>Acceptable range:<br/>if IVF1RK=3, 4: IVF3RK  $\leq$  IVF4RK  $\leq$  NCETSC(IVF2RK).<br/>Default value: none.

W-5 (R): WVFMRK Weighting factor,  $W_{VF}$ , for the region defined by the words 1 through 4. The values will be normalized to 1.0 if all factors are positive. If any factor is negative, then no normalization is performed and all void fraction weighting factors will be used as entered. NOTE: in such case the value of average void fraction (RK-000-Void-0000 - Table 2-29) will not have a physical meaning. *Acceptable range:* WVFFRK  $\neq$  0.0. *Default value:* none.

W-6 (I):IRegion number. If no value, or zero is entered, then the region data are<br/>read sequentially - the first record in the input is interpreted as containing<br/>the first (lower) region data (I=1), then I=2, etc. The total number of<br/>regions is equal to NVFWRK  $\leq$  NWFMAX = 200<br/>Acceptable range: I = 1, 2, ..., 200<br/>Default value: none

#### 2.9.21 Example of Reactor Kinetics Input Data

Two examples of Reactor Kinetics input are provided below. In the first example the reactivity feedback is defined through independent tables. In the second example the reactivity feedback is defined through a full table.

In the first example the reactor is 50 m<sup>3</sup> in size, the initial power is 100 MW. The macroscopic fission cross section is calculated as follows. The fuel consists of 5% enriched uranium. The total mass of uranium in the core is 20 t. The mass of U-235 is equal to  $20.0.05 = 1 \text{ t} = 10^3 \text{ kg}$ . The number of kmoles is equal to  $10^3/235 = 4.255$ . The average molar density is equal to  $4.255/50 = 0.0851 \text{ kmol/m}^3$ . The atomic density is obtained using the Avogadro number ( $6.022 \cdot 10^{26}$  atoms/kmol):  $N = 0.0851 \times 6.022 \cdot 10^{26} = 5.12 \cdot 10^{25} \text{ atoms/m}^3$ . The macroscopic fission cross section is equal to:  $\Sigma_f = N \cdot \sigma_f$ , where  $\sigma_f$  is the microscopic fission cross-section for U-235, equal to 505 barn =  $505 \cdot 10^{-28} \text{ m}^2$  (Figure 2-54). The value of  $\Sigma_f$  is equal to:

$$\Sigma_f = N \cdot \sigma_f = 5.12 \cdot 10^{25} \cdot 505 \cdot 10^{-28} = 0.028 \text{ m}^{-1}$$

If there is more than one fissile isotope in the core, then  $\Sigma_f$  is a sum over all individual values, calculated as shown above.

The initial reactivity is zero. Three Tabular Functions (TF-001, TF-002, and TF-003) are used to model three groups of control rods. TF-004 is used to define the external neutron source.

The reactivity feedback is entered using independent reactivity tables input format. Tabular data defining the reactivity feedback from fuel temperature, moderator temperature, and void fraction, are shown in Table 2-33, Table 2-34 and Table 2-35, respectively.

The average fuel temperature is calculated by averaging the Solid Heat Conductor temperatures of SC-001 and SC-002. For both SC-001 and SC-002 mesh cells 1 through 10 are included in average temperature calculation. That means within each of these SC's the average temperature is calculated as cell volume averaged value including cells 1 through 10:

$$T_{SC} = \frac{\sum_{i=1}^{10} V_i T_i}{\sum_{i=1}^{10} V_i}$$

where  $T_{SC}$  is the SC average temperature, while  $T_i$  and  $V_i$  are the temperature and volume respectively of cell *i*. The weighting factors of 0.6 and 0.4 are assigned to SC-001 and SC-002 respectively, therefore the average fuel temperature is calculated as:

$$T_{fuel} = 0.6 \cdot T_{SC-001} + 0.4 \cdot T_{SC-002} = 0.6 \cdot \left(\frac{\sum_{i=1}^{10} V_i T_i}{\sum_{i=1}^{10} V_i}\right)_{SC-001} + 0.4 \cdot \left(\frac{\sum_{i=1}^{10} V_i T_i}{\sum_{i=1}^{10} V_i}\right)_{SC-002} + 0.4 \cdot \left(\frac{\sum_{i=1}^{10} V_i}{\sum_{i=1}^{10} V_i}\right)$$

Table 2-33 Reactivity feedback from fuel temperature.

i	1	2	3	4
$T_{f,T}(i)$ (K)	300	800	1300	1800
$R_{f,T}(i)$ (\$)	1.00	0.90	0.80	0.70

Table 2-34 Reactivity feedback from moderator temperature.

j	1	2
$T_{m,T}(j)$ (K)	300	900
$R_{m,T}(j)$ (\$)	1.00	0.95

Table 2-35 Reactivity feedback from void fraction.

k	1	2
$\alpha_T(k)$ (K)	0.0	1.0
$R_{\alpha,T}(k)$ (\$)	1.00	0.00

The average moderator temperature is calculated from the pool temperatures in Control Volumes CV-002 and CV-005, with the weighting factors of 0.9 and 0.1 respectively. Therefore:

$$T_{\text{mod}} = 0.9 \cdot T_{pool,CV-002} + 0.1 \cdot T_{pool,CV-005}$$

The average moderator void fraction is calculated from the effective local void fraction at the left and right surfaces of SC-001 and SC-002, with the weighting factors of 0.3 at SC-001 surfaces, and 0.2 at SC-002 surfaces. Therefore:

$$\alpha = 0.3 \cdot \alpha_{eff,SC-001-L} + 0.3 \cdot \alpha_{eff,SC-001-R} + 0.2 \cdot \alpha_{eff,SC-002-L} + 0.2 \cdot \alpha_{eff,SC-002-R}$$

$$\alpha = 0.3 \cdot (X_{pool}\alpha_{pool} + X_{atms})_{SC-001-L} + 0.3 \cdot (X_{pool}\alpha_{pool} + X_{atms})_{SC-001-R} + 0.2 \cdot (X_{pool}\alpha_{pool} + X_{atms})_{SC-002-L} + 0.2 \cdot (X_{pool}\alpha_{pool} + X_{atms})_{SC-002-R}$$

where  $X_{pool}$  is the fraction of SC surface covered by pool,  $X_{atms}$  is the uncovered fraction of SC surface, and  $\alpha_{pool}$  is the local bubble fraction at SC surface.

```
* -- FUEL TEMPERATURE TABLE
781001 300.0 * Tfuel(1)
 781002 800.0 * Tfuel(2)
 781003 1300.0 * Tfuel(3)
 781004 1800.0 * Tfuel(4)
            -- MOD. TEMPERATURE TABLE
782001 300.0 * Tmod(1)
782002 900.0 * Tmod(2)
             -- VOID FRACTION TABLE
783001 0.0 * void(1)
783002 1.0 * void(2)
             -- REACTIVITY TABLE - INDEPENDENT REACTIVITY COEFFICIENT INPUT

        --
        REACTIVITI
        TABLE
        -
        INDEPENDENT

        *
        TYPE
        Point
        REACTIVITY

        *
        (1=Tfuel)
        No.
        ($)

        784001
        1
        1
        1.000

        784002
        1
        2
        0.900

        784003
        1
        3
        0.800

        784004
        4
        0.700

        *
        TYPE
        Point
        REACTIVITY

        *
        (2=Tmod)
        No
        ($)

        *
        (2=Tmod.)
        No.
        ($)

        784005
        2
        1
        1.000

        784006
        2
        2
        0.950

        *
        TYPE
        Point
        REACTIVITY

* (3=V.Fr.) No. ($)
784007 3 1 1.000
784008 3 2 0.000
 * - WEIGHTING FACTORS
 +
            -- FUEL TEMPERATURE

      791000 1 1 1 1 0 0.6
      *
      SC-001,
      Temperature in Nodes: 1 - 10,
      W = 0.6

      791000 1 2 1 10 0.4
      *
      SC-002,
      Temperature in Nodes: 1 - 10,
      W = 0.4

            -- MODERATOR TEMPERATURE
792000 3 2 0 0 0.9 * CV-002, Pool temperature,
792000 3 5 0 0 0.1 * CV-005, Pool temperature,
                                                                                                                                                                                                       W = 0.9
                                                                                                                                                                                                       W = 0.1

      792000 3 5 0 0 0.1
      *
      CV-005, Pool temperature,
      W = 0.1

      *
      -- VOID FRACTION

      793000 2 1 -1 0 0.3
      *
      SC-001, Void fraction at left surf., W = 0.3

      793000 2 1 1 0 0.3
      *
      SC-001, Void fraction at right surf., W = 0.3

      793000 2 2 -1 0 0.2
      *
      SC-002, Void fraction at left surf., W = 0.2

      793000 2 2 1 0 0.2
      *
      SC-002, Void fraction at right surf., W = 0.2
```

The second example, shown below, is very similar to the previous one, but in this case only one control rod group is modelled (using TF-001), no external neutron source is present, and the reactivity feedback is defined using full reactivity table format. The data covers a 3-D "space":

300 K  $\leq T_{fuel} \leq 1300$  K, 300 K  $\leq T_{mod.} \leq 900$  K,  $0.0 \leq \alpha \leq 1.0$ .

The same weighting factors are used, so the average fuel temperature, moderator temperature and void fraction, are calculated as described above.

Note that a Control Function, type "Reactor Kinetics" is entered in both examples. The Reactor Kinetics Package is actually activated by a presence of such Control Function in the input deck. If such CF is not present in the input deck, then the Reactor Kinetics Package will not be used, regardless whether any of the RK data has been entered or not. It should also be remembered that only one such function may be present in the input deck, and that the value of this CF will be equal to the current reactor power. Therefore this CF cannot be used as a CF defining control rod reactivity (section 2.9.9), or CF defining external neutron source (section 2.9.7). Such cases are flagged by the program as input errors.

705001 REACTOR KINETICS CONTROL FUNCTION 700001 3 5 1.0 0.0 \* Type: Reactor Kinetics, Scale=1.0, Add=0.0 710001 9 0 1 0 \* Argument: time 750000 0 0.26 \* MACROSCOPIC FISSION CROSS SECTION 751000 50.0 1.0E8 0.0 \* V (m3), POWER (W), REAC. (\$) 760000 001 \* CONTROL ROD REACTIVITY DEFINED BY TF-001 \* - REACTIVITY FEEDBACK DATA -- FUEL TEMPERATURE TABLE 781001 300.0 \* Tfuel(1) 781002 800.0 \* Tfuel(2) 781003 1300.0 \* Tfuel(3) -- MOD. TEMPERATURE TABLE 782001 300.0 \* Tmod(1) 782002 900.0 \* Tmod(2) -- VOID FRACTION TABLE 783001 0.0 \* void(1) 783002 1.0 \* void(2) -- REACTIVITY TABLE - FULL TABLE INPUT Tfuel Tmod. V.Fr. REACTIVITY POINT No. POINT No. POINT No. (\$) (\$) 1.000 
 784001 1
 1
 1

 784002 1
 1
 2

 784003 1
 2
 1

 784004 1
 2
 2
 0.000 0.950 0.050 

 784005
 2
 1

 784006
 2
 1

 784007
 2
 2

 784008
 2
 2

 1 2 1 2 0.900 -0.100 0.850 -0.150 784009 3 1 1 1 2 2 1 0.800 784010 3 2 -0.200 784011 3 0.750 784012 3 2 2 -0.250 \* - WEIGHTING FACTORS -- FUEL TEMPERATURE 

 791001 1 1 1 10 0.6
 \*
 SC-001, Temperature in Nodes: 1 - 10, W = 0.6

 791002 1 2 1 10 0.4
 \*
 SC-002, Temperature in Nodes: 1 - 10, W = 0.4

 -- MODERATOR TEMPERATURE 792001 3 2 0 0 0.9 \* CV-002, Pool temperature, 792002 3 5 0 0 0.1 \* CV-005, Pool temperature, W = 0.9W = 0.1-- VOID FRACTION  $793001 \ 2 \ 1 \ -1 \ 0 \ 0.3$ \*SC-001, Void fraction at left surf., W = 0.3 $793002 \ 2 \ 1 \ 1 \ 0 \ 0.3$ \*SC-001, Void fraction at right surf., W = 0.3 $793003 \ 2 \ 2 \ -1 \ 0 \ 0.2$ \*SC-002, Void fraction at left surf., W = 0.2 $793004 \ 2 \ 2 \ 1 \ 0 \ 0.2$ \*SC-002, Void fraction at right surf., W = 0.2

## 2.9.22 Record: 740000, Isotope Transformation Data - Initial Core Composition

The Isotope Transformation model is a part of the Reactor Kinetics package, and may be used only if the RK package is active.

W-1 (I):	ICITRK	Initial core composition calculation.
		1 = only input values. The user can define the initial concentrations of non-fissile isotopes in records 740XXX (section 2.9.24) and fissile
		isotopes in records 746XXX (section 2.9.24), and fissile
		isotope concentrations should be read from an Initial Condition File
		ICF (see section 2.16.3).
		2 = equilibrium concentrations are calculated for non-fissile isotopes,
		unless the initial values are specified in records /40XXX.
		Concentrations of the isotopes for which there is no removal mechanism
		(such as decay, neutron absorption) are set to zero, because there is no
		equilibrium solution (the "equilibrium" concentration would be infinitely large).
		3 = equilibrium concentrations are calculated for all isotopes, unless the initial values are specified in records 740XXX (non-fissile) or 746XXX
		(fissile) Concentrations of the isotopes for which there is no removal
		mechanism are set to zero
		-1 = suppress the whole isotope transformation model
		$A_{ccentable range} = \frac{1}{2} \frac{2}{3} \text{ or } -1$
		Default value: 2
		Dejuui value. 2.
W-2 (I) :	IDITRK	Request for built-in isotope data (see section 2.9.36). The entry has six-
		digit format: <i>fedcba</i> . For each digit 0 means don't use data.
		$a \neq 0$ : use built-in data for <sup>233</sup> U/ <sup>235</sup> U fuel chain (8 isotopes),
		$b \neq 0$ : use built-in data for <sup>239</sup> U/ <sup>239</sup> Pu/ <sup>241</sup> Pu fuel chain (8 isotopes),
		$c \neq 0$ : use built-in data for <sup>135</sup> Xe chain (3 isotopes),
		$d\neq 0$ : use built-in data for <sup>149</sup> Sm chain (3 isotopes).
		$e \neq 0$ · use built-in data for <sup>157</sup> Gd chain (2 isotopes)
		$f \neq 0$ : use built-in data for 11 decay heat groups
		$f \neq 0$ . Use built-in data for 11 decay heat groups.
		for the gadolinium chain enter 101111
		101  the gauge multiplication of the second state of the secon
		Acceptable range: $IDTIKK \geq 0$ .
		<i>Dejaun vanue:</i> 000000.

## 2.9.23 Records: I05XXX, Isotope Transformation Data - Isotope Names

XXX=001, 002, ..., NIITRK, is the isotope reference number. The isotope reference numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined isotopes must have higher numbers than the built-in isotopes. The recommended numbers are XXX>700. The maximum number of isotopes is 200.

W-1 (A): NMITRK User defined name, length up to 7 characters. The name is read as a 7character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.

Examples of the isotope names are: **U-235**, **Xe-131m**. Note that the name is arbitrary and does not serve as, for example, an indicator of fissile nuclides. Fissile nuclides are identified only by a non-zero fission cross section, entered in record 743XXX (see section 2.9.27). *Acceptable range:* any string of up to 7 characters. *Default value:* 7 "underline" characters: "\_".

## 2.9.24 Records: 740XXX, Isotope Transformation Data - Initial Isotope Concentrations

XXX=001, 002, ..., NIITRK, is the isotope reference number. The isotope reference numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined isotopes must have higher numbers than the built-in isotopes. The recommended numbers are XXX>700. The maximum number of isotopes is 200.

W-1 (R) :	XIITRK	Initial concentration of isotope XXX, $N_{i=XXX}$ , $(1/m^3)$ , or relative concentration of XXX depending on word 2. Only initial concentrations of non-fissile isotopes can be specified here. Fuel initial concentrations are specified in record 746XXX, as mass fractions (see section 2.9.28). If an equilibrium core is specified in record 740000 (see section 2.9.22 above), then the initial concentration entered here overwrites the calculated equilibrium value. In the case of the nodal point kinetics, the concentration defined here is used in <u>all</u> nodes. The nodal-specific values are printed in the ICF file. The initialization of nodal point kinetics is done by selecting initialization option, INONRK=1, in the record 750XXX. When the initialization run is finished, all initial concentrations are available in the ICF file and may be modified by the user, if needed. <i>Acceptable range:</i> XIITRK $\geq 0.0$ . <i>Default value:</i> 0.0.
W-2 (I) :	IIITRK	Reference fissile isotope for definition of initial concentration of isotope XXX. If IIITRK $\leq 0$ , then XIITRK (word 1 above) is interpreted as initial concentration of isotope XXX, in m <sup>-3</sup> . If IIITRK > 0, then XIITRK (word 1 above) is interpreted as initial concentration of isotope XXX relative to the initial concentration of fissile isotope IIITRK. In such case there must exist an isotope IIITRK, with positive fission cross section. <i>Acceptable range:</i> IIITRK $\leq$ NIITRK . <i>Default value:</i> 0.
W-3 (R) :	CRITRK	Multiplier on reactivity effect of isotope XXX, $C_{R, i=XXX}$ , (-). This is a ratio of true reactivity effect of isotope XXX to the value obtained assuming uniform reactor flux distribution (point reactor):

$$CRITRK = \frac{\Delta \rho}{\Delta \rho_{point}}$$

The reactivity change for a point reactor is equal to:

$$\Delta \rho_{point} = -\frac{\Sigma_a}{v \Sigma_f}$$

where  $\Sigma_a$  is the absorption cross section of poison,  $\Sigma_f$  is the fission cross section,  $\nu$  is the number of neutrons produced per fission. For point reactor there is no position independence of cross sections. This is how SPECTRA calculates the reactivity effect. In reality the neutron flux distribution is not uniform, and the cross sections are position dependent. The reactivity effect is approximately given by (see [5], equation 15-35):

$$\Delta \rho = -\frac{\int_{V} \Sigma_{a}(\bar{r}) \Phi^{2}(\bar{r}) d^{3}r}{v \int_{V} \Sigma_{f}(\bar{r}) \Phi^{2}(\bar{r}) d^{3}r}$$

where  $\Phi(\mathbf{r})$  is the neutron flux. Using perturbation theory a reactivity effect for equilibrium poison concentration can be calculated. It may be shown (see [5], section 15.I.D):

$$\Delta \rho \propto -\frac{\int_{V} \Phi^{3}(\bar{r}) d^{3}r}{\int_{V} \Phi^{2}(\bar{r}) d^{3}r}$$

Thus the value of reactivity worth increases with more non-uniform flux distribution.

Acceptable range: $0.0 < CRITRK \le 1000.0$ Default value:1.0

## 2.9.25 Records: 741XXX, Isotope Transformation Data - Decay Data

XXX=001, 002, ..., NIITRK, is the isotope reference number. The isotope reference numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined isotopes must have higher numbers than the built-in isotopes. The recommended numbers are XXX>700. The maximum number of isotopes is 200.

W-1 (R) :	DCITRK	Decay constant, $\lambda$ , record are ignored.	, (1/s). If $\lambda = 0.0$ , the following data words in this
		Acceptable range:	$DCITRK \ge 0.0$ .
		Default value:	Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36).
$\mathbf{W} (\mathbf{D})$ .		Heat concreted nor	decer a (I)

W-2 (R): QDITRK Heat generated per decay, 
$$q_d$$
, (J).  
Acceptable range:  $0.0 \le \text{QDITRK} \le 1.0 \cdot 10^{-9}$ 

		Default value:	(note that 1 MeV= $1.602 \cdot 10^{-13}$ J). Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36).
W-3 (I) :	J1	Isotope number of a Acceptable range: Default value:	the decay product. $J1 \leq NIITRK$ . none.
W-4 (R) :	YDITRK (J1)	Yield fraction of iso This number is inten nuclide of isotope X J1. Acceptable range: Default value:	botope J1 from decay of XXX, (-). erpreted as a probability of the fact that a decay of a KXX will result in production of a nuclide of isotope YDITRK $\geq 0.0$ . Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36). A small number, $<10^{-50}$ , sets the built-in value to 0.0.
W-5 (I) :	J2	Isotope number of t Acceptable range: Default value:	the decay product. $J2 \leq NIITRK$ . none.
W-6 (R) :	YDITRK (J2)	Yield fraction of isotope J2 from decay of XXX, (-).This number is interpreted as a probability of the fact that a decay of a nuclide of isotope XXX will result in production of a nuclide of isotope J2.Acceptable range:YDITRK $\geq 0.0$ .Default value:Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36). A small number, $<10^{-50}$ , sets the built-in value to 0.0.	

... until all decay products are defined.

Note!

If the sum of the decay yield fractions is different than 1.0, then the fractions may be normalized, to give the sum of 1.0. The normalization is requested by the user, through word 1 in record 749000 (section 2.9.34).

## 2.9.26 Records: 742XXX, Isotope Transformation Data - Absorption Data

XXX=001, 002, ..., NIITRK, is the isotope reference number. The isotope reference numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined isotopes must have higher numbers than the built-in isotopes. The recommended numbers are XXX>700. The maximum number of isotopes is 200.

W-1 (R) :	SAITRK	Microscopic cross XXX. If $\sigma_c = 0.0$ , the <i>Acceptable range:</i> <i>Default value:</i>	section for neutron capture, $\sigma_c$ , (barn), for isotope he following data words in this record are ignored. SAITRK $\geq 0.0$ . Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36. Note that the values for U-238 and Th-232 depend on resonance absorption and therefore on the fission cross section and the concentrations of all fissile isotopes, as described in section 2.9.36.
W-2 (I) :	J1	Isotope number of <i>Acceptable range: Default value:</i>	the product of neutron capture by XXX. $J1 \leq NIITRK$ . none.
W-3 (R) :	YAITRK (J1)	Yield fraction of is This number is int neutron by a nucl nuclide of isotope. Acceptable range: Default value:	botope J1 from neutron capture in XXX, (-). terpreted as a probability of the fact that capture of ide of isotope XXX will result in production of a J1. YAITRK $\ge 0.0$ . Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36). A small number, <10 <sup>-50</sup> , sets the built-in value to 0.0.
W-4 (I) :	J2	Isotope number of Acceptable range: Default value:	the product of neutron capture by XXX. $J2 \leq NIITRK$ . none.
W-5 (R) :	YAITRK (J2)	Yield fraction of isotope J2 from neutron capture in XXX, (-).This number is interpreted as a probability of the fact that capture of neutron by a nuclide of isotope XXX will result in production of a nuclide of isotope J2.Acceptable range:YAITRK $\geq 0.0$ .Default value:Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36). A small number, $<10^{-50}$ , sets the built-in value to 0.0.	

... until all products of neutron capture are defined.

# Note!

If the sum of the capture yield fractions is different than 1.0, then the fractions may be normalized, to give the sum of 1.0. The normalization is requested by the user, through word 2 in record 749000 (section 2.9.34).

#### 2.9.27 Records: 743XXX, Isotope Transformation Data - Fission Data

XXX=001, 002, ..., NIITRK, is the isotope reference number. The isotope reference numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined isotopes must have higher numbers than the built-in isotopes. The recommended numbers are XXX>700. The maximum number of isotopes is 200.

W-1 (R) :	SFITRK	Microscopic cross section for fission, $\sigma_f$ , (barn), for isotop $\sigma_f = 0.0$ , the following data words in this record are ignored. <i>Acceptable range:</i> SFITRK $\ge 0.0$ .	
		Default value:	is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36).
W-2 (I) :	J1	Isotope number of a Acceptable range: Default value:	the product of fission of XXX. J1 ≤ NIITRK . none.
W-3 (R) :	YFITRK (J1)	Yield fraction of is This number is inte isotope J1 will be c Acceptable range: Default value:	otope J1 from fission of XXX, (-). erpreted as a probability of the fact that a nuclide of reated from fission of XXX. YFITRK $\geq 0.0$ . Default values are available if built-in isotope data is requested in record 740000. The default values for all built-in isotopes are listed below, in section 2.9.36). A small number, $<10^{-50}$ , sets the built-in value to 0.0.
W-4 (I) :	J2	Isotope number of a Acceptable range: Default value:	the product of fission of XXX. $J2 \leq NIITRK$ . none.
W-5 (R) :	YFITRK (J2)	Yield fraction of isotope J2 from fission of XXX, (-).This number is interpreted as a probability of the fact that a nuclide ofisotope J2 will be created from fission of XXX.Acceptable range:YFITRK $\geq 0.0$ .Default value:Default value:Defau	

... until all fission products are defined.

Note!

If the sum of the fission yield fractions is different than 2.0, then the fractions may be normalized, to give the sum of 2.0. The normalization is requested by the user, through word 3 in record 749000 (section 2.9.34).
#### 2.9.28 Records: 746XXX, Isotope Transformation Data - Fuel Composition

XXX=001, 002, ..., NIITRK, is the isotope number. The maximum number of isotopes is 200. This record specifies initial composition of fuel (mass fractions). At least one positive value must be entered for a fissile isotope. If the sum of all fractions is not equal to 1.0, then the fractions will be normalized, to give the sum of 1.0.

W-1 (R): FIITRK Mass fraction of fissile isotope XXX in the fuel. If equilibrium fuel concentrations are requested (ICITRK=3, record 740000, section 2.9.22), then concentrations of those isotopes for which initial fractions are zero are calculated from the equilibrium condition, and then all fuel fractions are rescaled to give the sum of one. To avoid using equilibrium concentrations for certain fuels, enter positive small number for these fuels, for example 10<sup>-30</sup>.

The initial concentrations, in  $(1/m^3)$ , are calculated using the fissile fractions entered here, and the overall macroscopic fission cross-section,  $\Sigma_f$ , defined in record 750000 (section 2.9.1). To calculate concentrations,  $N_i$ , the following relation is used:

$$\Sigma_f = \sum_i N_i \sigma_{f,i} = C \cdot \sum_i f_i \sigma_{f,i}$$

where  $f_i$  are the fractions entered in this record, and C is a constant, equal to:

$$C = \frac{\sum_{f} \cdot \sum_{i} f_{i}}{\sum_{i} f_{i} \sigma_{f,i}}$$

By including the sum of  $f_i$ , the above formula automatically takes care that the entered fractions should be normalized to 1.0. Finally, all fuel concentrations are obtained from:

 $N_i = C \cdot f_i$ .

Acceptable range:if isotope XXX does not undergo fission ( $\sigma_f$  =<br/>SFITRK = 0.0 - section 2.9.27), then FIITRK must<br/>be equal to zero; if isotope XXX does undergo<br/>fission ( $\sigma_f$  = SFITRK > 0.0 - section 2.9.27), then<br/>FIITRK  $\geq 0.0$ .Default value:0.0.

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#### 2.9.29 Record: 747XXX, Isotope Transformation Data - Fuel Removal/Loading Data

The value of XXX is equal to:

•	in case of point kinetics:	XXX = 000,
•	in case of nodal point kinetics:	XXX = node number (maximum of 50 nodes).

W-1 (I):

IREMRK Pointer to a Tabular or Control Function that defines relative rate of removal of fuel elements from the core,  $R^R = -(1/N_{fe}) \cdot (dN_{fe}/dt)$ , (1/s), where  $N_{fe}$  is the number of fuel elements in the core. Change of concentration of any isotope *i*, due to fuel removal function, is given by:

$$\left(\frac{dN_i}{dt}\right)_{R^R} = -N_i C_i R^R$$

where  $C_i$  is a constant, defined in records 720XXX (section 2.9.30).

If the number is positive then the relative removal rate will be defined by a Tabular Function with the number: IREMRK. If the number is negative then the relative removal rate will be defined by a Control Function with the number: | IREMRK |. The minimum limit of zero, and the maximum limit of  $10^{-3}$  are imposed on the value obtained from Tabular or Control Function.

Acceptable range: must be a valid reference number of a Tabular or a Control Function. The "Reactor Kinetics" type CF cannot be used here. 0.

Default value:

Pointer to a Tabular or Control Function that defines first filling W-2(I): IFILRK function,  $R^{F}(1)$ , that defines a relative rate of fuel elements insertion into (1)the core,  $R^{F}(1) = (1/N_{fe}) \cdot (dN_{fe}/dt)$ , (1/s), where  $N_{fe}$  is the number of fuel elements in the core. Change of concentration of any isotope *i*, due to the *k*-th filling function, is given by:

$$\left(\frac{dN_i}{dt}\right)_{R^F(k)} = N_i^F(k) \cdot R^F(k)$$

where  $N_i^F(k)$  are the isotope concentrations  $(1/m^3)$  in the elements loaded to the core with the k-th loading function. The isotope concentrations  $N_i^F(k)$  are defined through records 72YXXX, and 73YXXX.

If the number is positive then  $R^{F}(1)$  will be defined by a Tabular Function with the number: IFILRK. If the number is negative then  $R^{F}(1)$ will be defined by a Control Function with the number:

| IFILRK |. The minimum limit of  $-1.0 \times 10^{-3}$ , and the maximum limit of  $+1.0 \times 10^{-3}$  are imposed on the value obtained from Tabular or Control Function.

Acceptable range: must be a valid reference number of a Tabular or a Control Function. The "Reactor Kinetics" type CF cannot be used here. 0.

Default value:

W-3 (I):IFILRK<br/>(2)Pointer to a Tabular or Control Function that defines second filling<br/>function  $(R^F(2) - \text{see description of word 2 above}).$ Acceptable range:must be a valid reference number of a Tabular or a<br/>Control Function. The "Reactor Kinetics" type CF<br/>cannot be used here.Default value:0.

... until all filling functions are defined. The maximum number of filling functions is 9.

**EXAMPLE**: The following input (copied from the test case Xe-136-SOL-1) defines loading of U-235 (isotope No. 201) into the core.

\* fuel load data
\* RR RF(1)
747000 0 201 \*
605201 Loading rate U-235 (1/s)
600201 0.0 2.5518E-8

The loading rate is :  $R^F = 2.5518\text{E-8}$  (1/s). The initial U-235 concentration in the core is printed in the output file:

		Input	Multiplier
		Initial	on
		Concentr.	Reactivity
i	Isotope	[1/m3]	[ - ]
108	U-235	1.18812E+25	1.00000E+00

The concentration is  $N^F = 1.8812E+25$  (1/m<sup>3</sup>). Therefore the loading rate of U-235 will be equal to:  $2.5518E-8 \times 1.8812E+25 = 4.8E+17$  (1/m<sup>3</sup>-s). The loading functions and the fuel composition for the loading functions are also printed in the output file:

```
=RK= FUEL LOADING FUNCTIONS
NODE LOADING FUNCTION No.
No. 1
1 TF-201
[...]
Fuel Composition in Assemblies Being Loaded During Transient
Mass Nuclide
Fraction Concentration
i Isotope [-] [1/m3]
108 U-235 1.00000E+00 1.18812E+25
```

### 2.9.30 Records: 720XXX, Isotope Transformation Data - Multipliers for Fuel Removal

XXX=001, 002, ..., NIITRK, is the isotope number. This record specifies multipliers for isotopes that are being removed from the core with the removal function  $R^{R}$ , (see section 2.9.29).

W-1 (R) :	CIITRK	Value of the multiplier for isotope XXX,		
		Acceptable range:	$0.0 \le \text{CIITRK} \le 10.0.$	
		Default value:	1.0 .	

# 2.9.31 Records: 72YXXX, Isotope Transformation Data - Loaded Fuel Data

XXX=001, 002, ..., NIITRK, is the isotope number. The maximum number of isotopes is 200. Y = 1, ..., 9 is the loading function number, k. This record specifies composition of fuel (mass fractions) in assemblies that are being loaded into the core with the loading function k (see section 2.9.29).

W-1 (R): FRITRK Mass fraction of fissile isotope XXX in the fuel being loaded into the core with the loading function k,  $N_{i=XXX}^{F}(k=Y)$  (see section 2.9.29). The fuel concentrations, in  $(1/m^3)$ , are calculated from (see section 2.9.28):  $N_i = C \cdot f_i$ . where  $f_i$  are the fractions entered in this record, and C is a constant, calculated as shown in section 2.9.28 (note that C is defined using the initial fuel fractions, entered in records 746XXX, and not the reload fuel fractions entered here). It is important to note that the fractions entered here are not normalized by the program, so any desired concentrations may be obtained for the loaded fuel. Acceptable range: if isotope XXX does not undergo fission ( $\sigma_f$  = SFITRK = 0.0 - section 2.9.27), then FRITRK must be equal to zero; if isotope XXX does undergo fission ( $\sigma_f$  = SFITRK > 0.0 - section 2.9.27), then FRITRK  $\geq 0.0$ .

Default value:

#### 2.9.32 Records: 73YXXX, Isotope Transformation Data - Loaded Non-fuel Data

XXX=001, 002, ..., NIITRK, is the isotope number. The maximum number of isotopes is 200. Y = 1, ..., 9 is the loading function number, *k*. This record specifies concentrations of non-fuel isotopes in assemblies that are being loaded into the core with the loading function *k* (see section 2.9.29).

0.0.

W-1 (R) :	XRITRK	Reload concentration, $(1/m^3)$ , of isotope XXX being loaded into the core with the loading function <i>k</i> , or relative concentration of XXX, depending on word 2. Only reload concentrations of non-fissile isotopes can be specified here. Fuel concentrations are specified in record 72YXXX, as mass fractions (see section 2.9.31). <i>Acceptable range:</i> XIITRK $\ge 0.0$ . <i>Default value:</i> 0.0.
W-2 (I) :	IRITRK	Reference fuel isotope for definition of reload concentration of isotope XXX. If IRITRK $\leq 0$ , then XRITRK (word 1 above) is interpreted as reload concentration of isotope XXX, in m <sup>-3</sup> . If IRITRK > 0, then XRITRK (word 1 above) is interpreted as reload concentration of isotope XXX relative to the reload concentration of fissile isotope IRITRK. In such case there must exist an isotope IRITRK, with positive fission cross section. <i>Acceptable range:</i> IRITRK $\leq$ NIITRK . <i>Default value:</i> 0.

#### 2.9.33 Record: 748000, Point Kinetics Model for Circulating Fuel

The point kinetics model for circulating fuel is intended for applications such as molten salt reactors (MSR). In MSRs the fissile fuel is dissolved in a fluid (molten salt) which circulates in the primary reactor system.

W-1 (I): IFTORK Fuel type option

1 = solid fuel. In such case, standard point kinetics model is used. The delayed neutron precursors are obtained as in the classical point kinetics equation (Volume 1, section 9.2.1):

$$\frac{dC_i(t)}{dt} = \frac{\beta_i}{\Lambda} n(t) - \lambda_i C_i(t)$$

The isotope concentrations are obtained from the isotope transformation model, as shown in Volume 1, section 9.3.1).

2 = circulating fuel (e.g. molten salt reactor). Allowed only for alternative fluid (IFLDFL > 1). In such case mapping is necessary (IMAPRK>0). The delayed neutrons must be mapped into the RT Package (see Word 2 below). The RK Package calculates the precursor source as (see Volume 1):

$$S_i(t) = \frac{\beta_i}{\Lambda} n(t)$$

The source is provided to the RT Package, which subsequently calculates transport, decay, as well as eventual other mechanisms such as removal in the filters, etc. The total mass of delayed neutron precursors present at any time in the core,  $C_i(t)$ , is obtained as a sum of the masses in all core volumes. The core volumes are recognized as these Control Volumes for which a non-zero weighting factor is specified in the records 791XXX, 792XXX, 793XXX.

The fission products, for example the major decay heat producers (group 6) should also be mapped. The RK Package will calculate the source of these isotopes, as described in Volume 1. The source is provided to the RT Package, which subsequently calculates transport, decay, as well as eventual other mechanisms such as removal by filters, etc.

If IFTORK = 2 (circulating fuel), the core region is defined by the fuel temperature feedback weighting factors (record 791XXX). All fuel regions must be defined as Control Volumes (ITF1RK must be set to 3). The source of isotopes (including the delayed neutron precursors), obtained from the RK package as shown above, will be distributed over all volumes with positive weighting factor (WTFFRK>0), as described in Volume 1.

Acceptable range:1, 2Default value:1

W-2(I): **IMAPRK** Isotope mapping data. The entry has an eight-digit format: hgfedcba. For each digit 0 means don't map the chain. The chains are defined by IDITRK (record 740000, section 2.9.22).

 $a\neq 0$ : map the <sup>233</sup>U/<sup>235</sup>U chain (8 isotopes) into the RT Package

- $b\neq 0$ : map the <sup>239</sup>U/<sup>239</sup>Pu/<sup>241</sup>Pu chain (8 isotopes) into RT
- $c\neq 0$ : map the <sup>135</sup>Xe chain (3 isotopes) into RT
- $d\neq 0$ : map the <sup>149</sup>Sm chain (3 isotopes) into RT
- $e \neq 0$ : map the <sup>157</sup>Gd chain (2 isotopes) into RT
- $f\neq 0$ : map the 11 major decay heat producers chain into RT
- $g \neq 0$ : map the delayed neutron precursors into RT

 $h\neq 0$ : map an additional, user-defined chain (if present) into RT

Acceptable range: IMAPRK  $\geq 0$ , if a chain is not active (appropriate digit in IDITRK is zero), the mapping request must not be used for this chain. Mapping is required (IMAPRK>0) for the circulating fuel (IFTORK = 2). Mapping can be requested for solid fuel (IFTORK=1)but in such case there will be no data transfer (sources of isotopes) from the RK to the RT Package. Note: in case of additional, user-defined chain, the molar weight, as well as the vapor class and the release class are not defined in the RK Package. If such chain is mapped  $(h\neq 0)$ , then those parameters should be defined within the RT Package, using records 880XXY, 885XXY, 886XXY, 0

Default value:

#### W-3 (I): **IDSORK** Initial distribution of isotopes.

= 1: isotope concentrations are initially set only in the core volumes, i.e. Control Volumes with positive fuel weighting factor (WTFFRK>0). The concentrations are proportional to the fuel weighting factors, WTFFRK.

= 2: isotope concentrations are initially set in all Control Volumes belonging to the CV group ICVGRT (Word 4 below). The concentrations are not proportional to the fuel weighting factors. WTFFRK, in the core volumes; the same concentrations are used in all volumes. This option gives best possible approximation of a system that is flowing at the start of the simulation.

= 3: isotope concentrations of fuel ( $\sigma_f > 0$ ) are initially set in all Control Volumes belonging to the CV group ICVGRT (Word 4 below). The concentrations are not proportional to the fuel weighting factors, WTFFRK. All other isotopes (fission products, including delayed neutron precursors) are initially set only in the core volumes, i.e. Control Volumes with positive fuel weighting factor (WTFFRK>0). The concentrations are proportional to the fuel weighting factors, WTFFRK, in the core volumes. This option gives best possible approximation of a system that is stagnant at the start of the simulation.

= 4: very similar to option 3, but all isotopes except for the fuel are initially set to zero. This option represent a "cold" (zero-power) nonflow situation.

=-1: use isotope concentrations from the initial condition file (ICF). Acceptable range: IDSORK = -1, 1, 2, 3, 4

Default value: 3

- W-4 (I): ICVGRK CV group (defined in record 101XXX). Initial concentrations of isotopes are set in all Control Volumes belonging to the CV group ICVGRT, if the initial distribution option (IDSORK) is set to 2 or 3. Acceptable range: ICVGRK  $\ge 0$ Default value: 1
- W-5 (I): IVRERK Pointer to a Tabular or Control Function that defines the reactivity effect caused by changes of the active core volume in case of circulating fuel. In case of solid fuel (IFTORK=1) the core volume is constant and equal to RVOLRK (input record 751000). In case of circulating fuel (IFTORK=2) the core volume is, in general, time dependent. The core volume is equal to the sum of liquid volumes of the Control Volumes that are defined as the core volumes. The core volumes are defined by a positive fuel weighting factors (WTFFRK>0, record 791XXX).

When the core volume changes, reactivity will generally change, for example due to different neutron leakage. This effect is taken into account by the present function. The function defines reactivity (in dollars) as a function of relative core volume:

$$R_{V}[\$] = f\left(\frac{V_{R}(t)}{V_{REF}}\right)$$

 $R_V$  - reactivity effect caused by changes of core volume, (\$) (plot parameter RT-000-ReVo-0000).

 $V_R(t)$  - current core volume, m<sup>3</sup>, (plot parameter RT-000-Rvol-0000).

 $V_{REF}$  - reference core volume, m<sup>3</sup>, (input parameter RVOLRK).

f - function defined by IVRERK. If the number is positive then the reactivity will be defined by a Tabular Function with the number: IVRERK. The argument of this function will be relative volume:  $V_R(t)/V_{REF}$ . If the number is negative then the reactivity will be defined by a Control Function with the number: |IVRERK|. The units obtained from the Tabular or Control Function are assumed to be (\$). *Acceptable range:* must be a valid reference number of a tabular or a

Control Function. The "Reactor Kinetics" type CF cannot be used.

*Default value:* 0.

Note: Typically the reactivity decreases with decreasing core volume. An example of a function defining the reactivity effect is given below:

$V_R(t)/V_{REF}(-)$	$R_V(\$)$
0.0	-1.00
1.0	0.00
1.1	+0.10

W-6 (I) :

IREIRK

Reactivity effect from isotope concentrations.

=1: reactivity feedback from isotope concentrations is taken into account

=2: reactivity feedback from isotope concentrations is <u>not</u> taken into account. In such case changes of concentrations due to for example thermal expansion of fluid is not taken into account. This option is intended mainly for testing calculations.

Acceptable range: 1, 2 Default value: 1

W-8 (I): IRTSRK Source of isotopes defined in the RT Package (non-mapped from RK) in circulating fuel. Typically all isotopes from the RK Package are mapped into the RT Package (see IMAPRK, above; all built-in chains and one user-defined chain may be mapped). However, the user may wish to use the RT chains in the analysis of circulating fuel (see Volume 1, Chapter: Fission Products, section: Isotope Chains). Source of those non-mapped isotopes in the RT Package may be defined for the circulating fuel in a similar way as it is done with the mapped isotopes. The source of isotope *i* is given by:

$$S_i = \gamma_{f,i} \cdot \sum_{k \in fis} \sigma_{f,k} N_k \Phi - \sigma_{a,i} N_i \Phi + \sum_{j \neq i} \sigma_{a,j} N_j \Phi \gamma_{a,j \to i}$$

Here  $\Phi$  is the neutron flux (1/m<sup>2</sup>-s),  $N_k$  is the concentration (1/m<sup>3</sup>) of isotope k,  $\sigma_{f,k}$  is the fission cross section of isotope k,  $\sigma_{a,j}$  is the neutron capture (non-fissile absorption) cross section of isotope j,  $\gamma_{f,i}$  is the average yield fraction of isotope i from fission of all fissile isotopes,  $\gamma_{a,j} \rightarrow i$  is the yield fraction of isotope i due to neutron capture by isotope j. Note!

In the RK Package the fission yields are different for each fissile isotope. In the RT Package, no individual fission yields are defined for the builtin isotopes, shown in section 2.15.111. However, if mapping from the RK chains (section 2.9.36) to the RT Package is requested (IMAPRK>0), and the first two chains (the  $^{233}U / ^{235}U$  fuel chain and the  $^{239}U / ^{239}Pu / ^{241}Pu$  fuel chain) are mapped, then the individual yields are defined for the next three chains:  $^{135}Xe$ ,  $^{149}Sm$ , and  $^{157}Gd$  chains, if they are mapped. The individual yields for those three chains are shown in section 2.9.36. For example, the RK Package defaults for Xe-135 chain are shown in Figure 2-50, left, while the RT Package defaults are shown in Figure 2-50, right.



Figure 2-50 Decay chain  $M_W = 135$ , RK Package see Volume 1, "Description of the Built-in Isotope Library" left: right: RT Package, see Volume 1, "Isotope Chains (Decay Chains)"

> IRTSRK=1 : source of non-mapped isotopes not taken into account IRTSRK=2 : source of the non-mapped isotopes taken into account, as described above. Acceptable range: 1,2 Default value: 2

W-Q

W-9 (I) :	IDEPRK	Option for calculating isotope concentrations in the core of circulating fuel
		IDEPRK = 0: only isotopes in the circulating fuel, i.e. CV pool
		IDEPRK = 1 : pool + adsorbed on adjacent structures (SC/TC)
		IDEPRK = 2: pool + atmosphere (gas space)
		IDEPRK = 3: pool + atmosphere + adjacent structures
		By adding 10 to IDEPRK, isotopes adsorbed on the aerosol particles are added:
		IDEPRK = 10: + isotopes adsorbed on particles in the CV pool
		IDEPRK = 11: + pool + particles deposited on adjacent structures
		IDEPRK = 12: + pool + particles in atmosphere
		IDEPRK = 13: + pool + atmosphere + adjacent structures
		NOTE: the isotopes located in different parts may have different
		reactivity worth. Appropriate multipliers are defined by words 11
		through 13 below.
		Acceptable range: 0, 1, 2, 3,
		10, 11, 12, 13
		Default value: 0
W-10 (R):	RLTVRK	Liquid volume fraction in the reactor, $V_{liq}/(V_{liq} + V_{sol})$ . The reactor core

V of consists of liquid with dissolved fuel and solid (for example graphite moderator in MSRE). RLTVRK represents the ratio between the liquid volume and the total volume occupied by liquid and solid. For example,

in case of MSRE, the ratio is 0.225; the graphite volume fraction is 0.775. The core liquid volume is obtained as a sum of pool volumes for all CV-s with positive power fraction, WTCFRK. The formula is:

$$V_{liq} = \sum_{i=1}^{N} V_{pool}(i)$$

The total core volume (plot parameter RT-000-RVol-0000) is obtained as:

$$V_{core} = \frac{V_{liq}}{RLTVRK} = \frac{1}{RLTVRK} \times \sum_{i=1}^{N} V_{pool}(i)$$

Acceptable range: $0.01 \le \text{RLTVRK} \le 1.0$ Default value:1.0

W-11 (R):	RLITRK	Reactivity worth multiplier for isotopes residing in liquid, including. $\Box$ CV pool (all core volumes), $\Box$ adsorbed on particles suspended in CV pool (all core volumes).Acceptable range: $10^{-2} \le \text{RLITRK} \le 10^{+2}$ Default value:1.0
W-12 (R):	RSITRK	<ul> <li>Reactivity worth multiplier for isotopes residing in solids, including</li> <li>SC/TC (adsorbed on structures adjacent to core volumes),</li> <li>adsorbed on particles deposited on SC/TC surfaces (all structures adjacent to the core volumes).</li> <li>Acceptable range: 10<sup>-2</sup> ≤ RSITRK ≤ 10<sup>+2</sup></li> <li>Default value: 1.0</li> </ul>
W-13 (R):	RGITRK	<ul> <li>Reactivity worth multiplier for isotopes residing in gas, including.</li> <li>CV atmosphere (all core volumes),</li> <li>adsorbed on particles airborne in CV atmosphere (all core volumes).</li> <li>Acceptable range: 0.0 ≤ RGITRK ≤ 10<sup>+2</sup></li> <li>Default value: 0.0</li> </ul>
W-14 (I):	IRSLRK	If positive, this is a number of Tabular Function, defining the ratio of solid worth to liquid worth, (RSITRK/RLITRK), versus the ratio of the solid density to the liquid density ( $N_{SC}/N_{CV}$ ) of isotope JRSLRK, defined below Acceptable range: reference to a Tabular Function, if non-zero Default value: none
W-15 (I) :	JRSLRK	Reference number of the isotope.Acceptable range:must be a valid isotope number if IRSLRK > 0 must be zero if IRSLRK = 0Default value:none.
W-16 (R):	FRSLRK	Ratio of the neutron flux in the solid (graphite) to the liquid (salt).

$$FRSLRK = \frac{\int \Phi \, dV_g}{\int \int \Phi \, dV_s}$$

Used to calculate absorption of isotopes, e.g. Xe-135 in graphite. For any isotope i, present in the solid structures of the core, the neutron absorption term is obtained from:

 $\sigma_{c,i} \cdot N_{s,i} \cdot \Phi \cdot FRSLRK$ 

Here  $\sigma_{c,i}$  is the neutron capture cross section of the isotope *i*,  $N_{s,i}$  is the concentration of the isotope *i* in the solid, and  $\Phi$  is the neutron flux, obtained from the reactot kinetics model. Acceptable range:  $10^{-3} \leq \text{FRSLRK} \leq 10^{+3}$ Default value: 1.0

W-17 (I): ICVURK CV number of the upper plenum. Isotopes that are present in the core are obtained as a sum of all isotopes present in volumes for which positive fuel weighting factor is given. If ICVURK>0 then this number indicates the upper plenum volume. A fraction (FCVURK) of the isotopes present in the upper plenum will affect the core reactivity. This fraction is added to the sum mentioned above. The main purpose on this and the next entry is to take into account the possibility of delayed neutron precursors in the upper plenum affecting the core reactivity. Acceptable range: must be a valid reference to a Control Volume, if positive Default value: none. W-18 (R): FCVURK Fraction of the isotopes present in the upper plenum volume (ICVURK) that are added to the total mass of isotopes present in the core. The main purpose on this and the previous entry is to take into account

the possibility of delayed neutron precursors in the upper plenum affecting the core reactivity. *Acceptable range:*  $0.0 \le \text{FCVURK} \le 1.0$ 

*Default value:* 0.167 (=1/6, an average fraction that is directed back towards the core)

# EXAMPLE OF THE USE OF RLITRK, RSITRK:

In case of MSRE core with fuel salt and graphite moderator, the effective Xe concentration is ([55], sec. 7.2)

$$N = \frac{\int N_s \Phi_2^* \Phi_2 dV_s + \int N_g \Phi_2^* \Phi_2 dV_g}{\int \Phi_2^* \Phi_2 dV_s + \int \Phi_2^* \Phi_2 dV_g}$$

Here N is the importance-averaged concentration per unit reactor volume,  $N_s$  and  $N_g$  are the local concentrations per unit volumes of salt and graphite respectively,  $\Phi_2$  is the thermal neutron flux. N is the uniform equilibrium concentration of xenon in the reactor, which produces the same reactivity effect as the actual distribution.

This is approximated in SPECTRA by introducing reactivity worth multipliers. The isotope concentrations in liquid (CV pools) are multiplied by RLITRK, while the concentrations in solids (SC/TC) are multiplied by RSITRK:

$$N = \frac{\sum_{CV \in core} N_{CV} \times RLITRK \times V_{CV} + \sum_{SC \in core} N_{SC} \times RSITRK \times V_{SC}}{\sum_{CV \in core} RLITRK \times V_{CV} + \sum_{SC \in core} RSITRK \times V_{SC}}$$

Here  $N_{CV}$  and  $N_{SC}$  are the isotope concentrations in the core CV pools and core SCs respectively. The theoretical values of the reactivity worth multipliers are:

$$RLITRK = \int_{CV \in core} \Phi_{CV} \Phi_{CV} dV_{CV}$$
$$RSITRK = \int_{SC \in core} \Phi_{SC}^* \Phi_{SC} dV_{SC}$$

Additionally, if there is a gas space in the reactor (for example, fuel salt disappears because of fuel dump, etc.) then the last parameter may be used:

$$RGITRK = \int_{CV \in core} \Phi_{CV}^* \Phi_{CV} \, dV_{CV,atms}$$

An additional problem with using the formula for N, shown above, is the definition of the volume of solids,  $V_{SC}$ . The concentration of isotopes on SCs is defined in SPECTRA per unit surface area,  $N_{S,SC}$  (atoms/m<sup>2</sup>). The total number of atoms of given isotope is therefore given as:

$$\sum_{SC \in core} N_{S,SC} \times A_{SC}$$

Here  $A_{SC}$  is the surface area of SC (m<sup>2</sup>). The adsorbed isotopes may be stored at the surface or diffuse inside the material. Calculations performed with MSRE model showed that in case of Xe-135 the diffusion depth is of order of centimeters.

Therefore in case of thick structures it might be better to define an effective volume of SC, which is equal to the surface area times the expected penetration depth. In the current code version the volume of solid structures in the core is defined by means of the user-defined parameter RLTVRK (input record 748000). According to the definition of this parameter, the total volume of solid structures in the core is:

$$V_{sol} = \frac{1 - RLTVRK}{RLTVRK} \times \sum_{CV \in core} V_{CV}$$

For convenience, in the notation applied here  $V_{CV}$  is the pool volume in CV, so the sum is the same as in the description of RLTVRK:

$$\sum_{i=1}^{N} V_{pool}(i) \equiv \sum_{CV \in core} V_{CV}$$

# 2.9.34 Record: 749000, Isotope Transformation Data - Normalization Indicators

W-1 (I) :	NDITRK	Indicator for normalization of decay yield fractions (see section 2.9.25). If the sum of the decay yield fractions is different than 1.0, then the fractions may be normalized, to give the sum of 1.0. 1 = normalize fractions if the sum is greater than 1.0 2 = normalize fractions if the sum is smaller than 1.0 3 = always normalize the decay yield fractions to 1.0 4 = never normalize the decay yield fractions <i>Acceptable range:</i> 1, 2, 3, 4 <i>Default value:</i> 4
W-2 (I) :	NAITRK	Indicator for normalization of absorption yield fractions (see section 2.9.26). If the sum of the absorption yield fractions is different than 1.0, then the fractions may be normalized, to give the sum of 1.0. 1 = normalize fractions if the sum is greater than 1.0 2 = normalize fractions if the sum is smaller than 1.0 3 = always normalize the absorption yield fractions to 1.0 4 = never normalize the absorption yield fractions <i>Acceptable range:</i> 1, 2, 3, 4 <i>Default value:</i> 4
W-3 (I) :	NFITRK	Indicator for normalization of fission product yield fractions (see section 2.9.27). If the sum of the fission product yield fractions is different than 2.0, then the fractions may be normalized, to give the sum of 2.0. Note: a single fission process creates two products, not one as in the decay process or the neutron absorption process, so if ALL fission products are tracked (which is rare), the sum of yield fractions is 2.0. 1 = normalize fractions if the sum is greater than 2.0 2 = normalize fractions if the sum is smaller than 2.0 3 = always normalize the fission yield fractions to 2.0 4 = never normalize the fission yield fractions Acceptable range: 1, 2, 3, 4 Default value: 4

# 2.9.35 Examples of Isotope Transformation Input Data

Three examples are given below, to illustrate input for Isotope Transportation model.

#### Example 1. Simplified Xenon Chain

This example shows how to prepare input data for a certain isotope chain. The Xenon chain is chosen for this example input. It should be noted however that in practice there is no need to prepare data for the Xenon chain, since this chain is present in the built-in isotope transformation library (see section 2.9.36) and need only to be activated as shown in section 2.9.22

The example defines isotope data for the analysis of poison material - Xenon-135. <sup>135</sup>Xe has an extremely large absorption cross section, and therefore is important in reactor analyses. The example input provides data for a simplified <sup>135</sup>Xe chain. The simplified chain is shown in Figure 2-52. (For comparison, a full <sup>135</sup>Xe chain is shown in Figure 2-51).

The half-lives of <sup>135</sup>I and <sup>135</sup>Xe are equal to 6.58 hr and 9.17 hr respectively ([5], figure 15-1). That means:  $\lambda_I = 2.93 \cdot 10^{-5} \text{ s}^{-1}$ , and  $\lambda_{Xe} = 2.01 \cdot 10^{-5} \text{ s}^{-1}$ . The yield fractions from fission of <sup>235</sup>U are:  $\gamma_I = 6.32\%$ , and  $\gamma_{Xe} = 0.26\%$  [17]. The absorption cross-section for <sup>135</sup>Xe is 2.772 \cdot 10^6 barn [17]. The fission cross-section of <sup>235</sup>U is 505 barn [17]. The input defines six isotopes:



Figure 2-51 Full decay scheme for <sup>135</sup>Xe ([5], figure 15-1).



Figure 2-52 Simplified decay scheme for <sup>135</sup>Xe ([5], figure 15-2).

1.)  $^{235}$ U (note that at least one fissile isotope must be present), 2.)  $^{238}$ U,

3.) <sup>135</sup>I,
4.) <sup>135</sup>Xe,
5.) <sup>135</sup>Cs,
6.) <sup>136</sup>Xe.

There is only one fissile nuclide -  $^{235}$ U. The fuel is assumed to be composed of  $^{235}$ U and  $^{238}$ U, with enrichment of e = 2%. This means the ratio of  $^{238}$ U to  $^{235}$ U is equal to:

$$\frac{N_{U-238}}{N_{U-235}} = \frac{1-e}{e} = \frac{1-0.02}{0.02} = 49.0$$

The isotopes <sup>238</sup>U, <sup>135</sup>Cs, <sup>136</sup>Xe, are included here only to make the example input more instructive. In the present example these isotopes neither absorb neutrons ( $\sigma_c$ =0.0), nor decay ( $\lambda$ =0.0). Therefore they have no effect on reactivity or decay heat production, and they could as well be skipped. In such case no yield fractions from decay of <sup>135</sup>Xe, and from neutron absorption in <sup>135</sup>Xe, would be specified. That means record 741004 would contain only two words, and record number 742004 would contain only one word.

```
_____
      ISOTOPES DATA
*_____
         Isotope names

      IO50001 U-235
      *
      Isotope No. 1

      I05002 U-238
      *
      Isotope No. 2

      I05003 I-135
      *
      Isotope No. 3

      I05004 Xe-135
      *
      Isotope No. 4

      I05005 Cs-135
      *
      Isotope No. 5

I05006 Xe-136 * Isotope No. 6
         Decay data
                       Decay Yield fractions
         Decay
         constant heat
* (1/s) (W)
741003 2.93E-5 0.0
                                   Isotope Yield
                                   4 1.0 * I-135 -> Xe-135
5 1.0 * Xe-135 -> Cs-135
741004 2.107E-5 0.0
         Absorption data
         Absorption
cross section
(barn) Isotope Yield
50006 6 1.0
                             Yield fractions
         Absorption
*
                                          1.0 * Xe-135 -> Xe-136
742004 2.722E6
         Fission data
                           Yield fractions
         Fission

        (barn)
        (1)
        (2)

        505.0
        3
        0.0632
        4

         cross section (1)
                                                      Isotope Yield
4 0.0026
                                                                     0.0026 * U-235
743001 505.0
*
         Initial core composition - Uranium, enrichment: e = 2%
746001 1.0 * mass fraction of U-235 = 100% (no other fissionable nuclides)
740002 49.0 1 * U-238/U-235 = (1 - e)/e = (1 - 0.02)/0.02 = 49
```

#### Example 2. Continuous Fuel Reload

In example 2 the built-in isotope library is used (see section 2.9.36). The initial enrichment (at the start of the calculations) of the fuel is assumed to be equal to  $e_{core} = 4.7\%$ . This means the ratio of <sup>238</sup>U and <sup>235</sup>U concentrations in the fuel present in the core is equal to:

$$\left[\frac{N_{U-238}}{N_{U-235}}\right]_{core} = \frac{1-e}{e} = \frac{1-0.047}{0.047} = 20.3$$

Fuel is continuously reloaded. Fresh fuel, which is being loaded into the core, has the enrichment of  $e_{fresh} = 8.1\%$ . This means the ratio of <sup>235</sup>U concentration in the fresh fuel to the <sup>235</sup>U concentration in the fuel present in the core is equal to:

$$\frac{[N_{U-235}]_{fresh}}{[N_{U-235}]_{core}} = \frac{e_{fresh}}{e_{core}} = \frac{0.081}{0.047} = 1.723$$

The ratio of <sup>238</sup>U and <sup>235</sup>U concentrations in the fresh fuel is equal to:

$$\left[\frac{N_{U-238}}{N_{U-235}}\right]_{fresh} = \frac{1 - e_{fresh}}{e_{fresh}} = \frac{1 - 0.081}{0.081} = 11.3$$

Fuel is being loaded to and removed from the core with the same rate - use is made of a Control Function, in this example it is CF-029. This CF is built to control the fuel reloading rate in order to keep constant power. Volume 3 shows examples how to build such a function.

Suppose further that only fuel that has reached a specified burn-up is being removed from the core (such procedure is applied in PBMR reactors). In the present example, which is based on PBMR plant specification, the reactor target burn-up is: B = 80,000 MWd/t. The corresponding enrichment of the spent fuel is, according to the specification, equal to about 1.3%. If the neutron flux is known, then this value may be also estimated from the following simple calculation. For the reactor fission power of  $Q_f$ =252 MW, and the heavy metal mass of M=2.97 t, the time needed to reach the target burn-up is equal to:  $t = BM/Q_f = 80,000 \cdot 2.970/252 = 943$  days =8.15  $\cdot 10^7$  s. The concentration of U-235 in this fuel is estimated from the formula:

$$\frac{dN_{U-235}}{dt} = -\sigma_f N_{U-235} \Phi$$

Solution of this differential equation gives:

$$N/N_0 = \exp(-\sigma_f \Phi t) = \exp(-505 \cdot 10^{-28} \, 4.5 \cdot 10^{17} \, 8.15 \cdot 10^7) = 0.157.$$

where  $\Phi$  is the neutron flux. The concentration of U-235 in the fuel which reached the target burn-up is therefore equal to the initial concentration times 0.157. This is approximately equal to the enrichment ratio, so the enrichment of the spent fuel is  $0.157 \cdot 8.1\% \approx 1.3\%$ , in agreement with the plant specification.

Finally, the ratio of U-235 concentration in the spent fuel to the concentration of the fuel initially present in the core is equal to:

$$\frac{[N_{U-235}]_{spent}}{[N_{U-235}]_{core}} = \frac{e_{spent}}{e_{core}} = \frac{0.013}{0.047} = 0.277$$

#### 2.9.36 Built-In Isotope Transformation Data

The built-in isotope chains are described subsequently below. The built-in data is requested in record 740000 (section 2.9.22). The following built-in data is available in the code:

- Isotope chain for  $^{233}U / ^{235}U$  fuel (8 isotopes).
- Isotope chain for  $^{239}$ U /  $^{239}$ Pu /  $^{241}$ Pu fuel (8 isotopes).
- Isotope chain for <sup>135</sup>Xe poison (3 isotopes).
- Isotope chain for <sup>149</sup>Sm poison (3 isotopes).
- Isotope chain for <sup>157</sup>Gd poison (2 isotopes).
- 11 groups of main isotopes responsible for the decay heat generation.

# - Isotope chain for ${}^{233}U/{}^{235}U$ fuel (isotopes 101 ÷ 108)

The isotope chain for  $^{233}$ U /  $^{235}$ U fuel is shown in Figure 2-53 (reproduced from [8]). The chain implemented in the SPECTRA built-in isotope library is somewhat simplified - the isotopes beyond  $^{235}$ U are not taken into account. The isotope chain for  $^{233}$ U /  $^{235}$ U fuel, as implemented in SPECTRA, is shown in Figure 2-54. The decay constants were taken from [8]. The decay constant for  $^{234}$ Pa was taken from reference [6]. Decay heats were taken from [13]. One-group cross-sections are used; the fission and the capture cross-sections were obtained from [17].



Figure 2-53 The isotope chain for <sup>233</sup>U / <sup>235</sup>U fuel ([8], figure 6.2).



Figure 2-54 The isotope chain for <sup>233</sup>U / <sup>235</sup>U fuel, as implemented in SPECTRA.

# Isotope chain for $^{239}U/^{239}Pu/^{241}Pu$ fuel (isotopes 201 ÷ 208)

The isotope chain for  $^{239}$ U /  $^{239}$ Pu /  $^{241}$ Pu fuel is shown in Figure 2-55 (reproduced from [8]). The chain implemented in the SPECTRA built-in isotope library is somewhat simplified - the isotopes beyond  $^{241}$ Pu are not taken into account. The isotope chain for  $^{239}$ U /  $^{239}$ Pu /  $^{241}$ Pu fuel, as implemented in SPECTRA, is shown in Figure 2-56. Decay data were taken from [8] and [13]. One-group cross-sections are used; the fission and the capture cross-sections were obtained from [17].



Figure 2-55 The isotope chain for <sup>239</sup>U / <sup>239</sup>Pu / <sup>241</sup>Pu fuel ([8], figure 6.1).



Figure 2-56 The isotope chain for <sup>239</sup>U / <sup>239</sup>Pu / <sup>241</sup>Pu fuel, as implemented in SPECTRA.

# Correction for resonance capture by $^{232}$ Th and $^{238}U$

In case of <sup>232</sup>Th and <sup>238</sup>U there is a significant neutron capture in resonances. To take that into account, the neutron capture cross sections for those two nuclides are modified. The "effective" cross sections are calculated from (compare [11], equation 7.119):

$$\sigma_{c,i} = \sigma_{c,i}^{true} \left( 1 + (1 - p_i) \varepsilon v P_{FNL} \frac{\sum_{j} \sigma_{f,j} N_j}{\sigma_{c,i}^{true} N_i} \right)$$

where: $\sigma_{c,i}$ effective cross section for isotope i, i=1 (232Th) or =9 (238U), $p_i$ probability of escaping resonance absorption in isotope  $i, \varepsilon$  $\varepsilon$ fast fission factor,vnumber of neutrons generated per fission, $P_{FNL}$ fast non-leakage probability, $\sigma_{f,j}$ fission cross section for isotope j, (barn), $N_b,N_j$ concentrations of isotopes i, j, (1/m3).

In the above equation the true capture cross section is given with the superscript "*true*", and the sum is taken over all fissile isotopes. The resonance escape probability is given by ([11], equation 6.119):

$$p_i = \exp\left(-c_i I_i N_i\right)$$

where  $I_i$  is the resonance integral for isotope *i* and *c* is certain constant, the value of which varies for different reactors. The resonance integral is given by ([11], equation 6.120):  $I_i = A_i + C_i/(r\rho)^{1/2}$ , where *r* is rod diameter (cm),  $\rho$  is fuel density (kg/cm<sup>3</sup>), and  $A_i$ ,  $C_i$  are constants, equal to ([11], table 6.5):

-	$i = {}^{238}$ U (metal)	$A_i = 2.8$	$C_i = 38.3,$
-	$i = {}^{238}\text{UO}_2$	$A_i = 3.0$	$C_i = 39.6,$
-	$i = {}^{232}$ Th (metal)	$A_i = 3.9$	$C_i = 20.9,$
-	$i = {}^{232}\text{ThO}_2$	$A_i = 3.4$	$C_i = 24.5.$

It is assumed that resonance absorption occurs only in <sup>232</sup>Th and <sup>238</sup>U. Therefore the individual resonance escape probabilities,  $p_i$ , are related to the overall resonance escape probability, p, by:  $p_1p_9=p$ . The value of p is a user input (see section 2.9.1). After easy transformations one obtains the following expressions for  $p_1$ ,  $p_9$ :

$$p_1 = \exp\left(\ln(p)\frac{I_1N_1}{I_1N_1 + I_9N_9}\right) \qquad p_9 = \exp\left(\ln(p)\frac{I_9N_9}{I_1N_1 + I_9N_9}\right)$$

The following values are assumed for calculations: r=1.0,  $\rho=19.1$ ,  $A_{i_b}$ ,  $C_i$  for dioxides. These gives  $I_1 = 9.0$ ,  $I_9 = 12.1$ . The effective cross sections are calculated based on initial concentrations, and are not modified during the transient. It must be remembered that the effective cross sections are calculated as described above only if the built-in library is being used (IDITRK $\geq$ 3, section 2.9.22), and if the capture cross sections for <sup>232</sup>Th, <sup>238</sup>U are not modified in the input data. Thus, the user can calculate his own resonance integrals, and enter the effective capture cross sections in the input data, overwriting the default values.

# • Isotope chain for $^{135}$ Xe poison (isotopes 301 ÷ 303)

The isotope chain for <sup>135</sup>Xe fission product poison is shown in Figure 2-57. A simplified chain is used, and the short life isotopes, <sup>135</sup>Sb, <sup>135</sup>Te, are neglected. The yield fraction of <sup>135</sup>I is taken as a sum of the yield fractions for <sup>135</sup>Sb, <sup>135</sup>Te, and <sup>135</sup>I. The decay constants were taken from reference [5] (figure 15-1). The decay heats were taken from [13]. The fission product yields were taken from reference [17] (table 8). One-group cross-sections are used; the fission and the capture cross-sections were obtained from [17].



Figure 2-57 The isotope chain for <sup>135</sup>Xe fission product poison, as implemented in SPECTRA.

# - Isotope chain for $^{149}$ Sm poison (isotopes 401 ÷ 403)

The isotope chain for <sup>149</sup>Sm fission product poison is shown in Figure 2-58. The decay constants were taken from reference [8] (figure 6.3). The decay heats were taken from [13]. The fission product yields were taken from reference [17] (table 8). One-group cross-sections are used; the fission and the capture cross-sections were obtained from [17].



Figure 2-58 The isotope chain for <sup>149</sup>Sm fission product poison, as implemented in SPECTRA.

# - Isotope chain for $^{157}$ Gd poison (isotopes 501 ÷ 502)

The isotope chain for <sup>157</sup>Gd fission product poison is shown in Figure 2-59. The decay constants were taken from reference [17] (table 6). The decay heats were taken from [13]. The fission product yields were taken from reference [17] (table 8). One-group cross-sections are used; the fission and the capture cross-sections were obtained from [17].



Figure 2-59 The isotope chain for <sup>157</sup>Gd fission product poison, as implemented in SPECTRA.

#### - Isotope groups of main decay heat producers (isotopes 601 ÷ 611)

The decay heat producers are represented by 11 groups of "isotopes", similarly as in [15]. The decay constants and fission yields of these groups were established based on data from [15] and comparisons with ANS standard [2]. Detailed description and comparisons with ANS standard are presented in Volumes 1 and 3.

For all decay heat groups the values of the decay constant,  $\lambda_i$ , and the decay heat,  $q_{d,i}$  are positive. The neutron absorption is neglected, thus the neutron capture cross section,  $\sigma_{c,i}$ , as well as fission cross section,  $\sigma_{f,i}$ , are equal to zero. Therefore, for the decay heat groups, the general isotope balance equation (see Volume 1) reduces to:

$$-\frac{dN_i}{dt} = -\lambda_i N_i + \sum_j \lambda_j N_j \gamma_{d,j \to i} + \sum_j \sigma_j N_j \Phi \gamma_{f,j \to i}$$

where:	$N_i$ -	concentration of nuclides from group <i>i</i> , $(1/m^3)$ ,
	$\lambda_i$ -	decay constant of group $i$ , (1/s),
	$y_{d, j \rightarrow i}$ -	decay yield fractions (probability that a decay of nuclide from group <i>j</i> will result in creation of nuclide in group <i>i</i> )
	$\mathcal{Y}_{f, j \rightarrow i}$ -	fission yield fractions (probability that a fission of nuclide from a fissile group <i>i</i> will result in creation of nuclide in group <i>i</i> )
	Φ-	neutron flux, $(1/m^2/s)$ .

The value of decay heat of each group is calculated as:

$$Q_{d,i} = \lambda_i N_i q_{d,i}$$

where:	$Q_{d, i}$ -	decay heat density, group i, $(W/m^3)$ ,
	$q_{d,i}$ -	heat release per decay, group i, (W/decay).

The values of the decay constants,  $\lambda_i$ , the fission yield fractions,  $y_{f, k \to i}$ , the decay yield fractions,  $y_{d, j \to i}$ , as well as the energy per decay,  $q_{d, i}$ , are shown in Table 2-36 and Figure 2-60. Detailed description of how these values were derived is presented in Volume 1.

Group	Isotope	Decay constant,	Decay yields	U fission yields	Pu fission yields
No.	i	$\lambda_i$ , (1/s)	$y_{d, i \to i+1}, (-)$	У <sub>f, U→i</sub> , (-)	<i>y</i> <sub>f, Pu→i</sub> , (-)
1	601	1.77	1.000	0.2392	0.1600
2	602	0.577	1.000	0.4208	0.3000
3	603	6.74×10 <sup>-2</sup>	1.000	0.5800	0.5800
4	604	6.21×10 <sup>-3</sup>	0.602	0.3080	0.3080
5	605	4.74×10 <sup>-4</sup>	0.554	0.0000	0.0000
6	606	4.81×10 <sup>-5</sup>	0.358	0.0000	0.0000
7	607	5.34×10 <sup>-6</sup>	0.710	0.0000	0.0000
8	608	5.73×10 <sup>-7</sup>	0.700	0.0000	0.0000
9	609	1.04×10 <sup>-7</sup>	0.506	0.0000	0.0000
10	610	2.96×10 <sup>-8</sup>	1.000	0.0000	0.0000
11	611	7.59×10 <sup>-10</sup>		0.0000	0.0000

Table 2-36 Decay heat group constants.



Figure 2-60 Decay heat group constants.

### 2.10 Material Property Input Data

# 2.10.1 Records: 801XXX, Thermal Conductivity Data

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100. Thermal conductivity is assumed to be a function of temperature and is defined by pairs, giving the temperature and the thermal conductivity for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. Total number of data pairs for a material may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.10.8).

W-1 (R) :	TCSMDX	Temperature, (K). Acceptable range:	Temperature values must increase. Thus the value must be greater than the value of TCSMDX for the previous point.
		Default value:	none.
W-2 (R) :	TCSMDY	Thermal conductive Acceptable range: Default value:	ity, (W/m/K). $0.0 < \text{TCSMDY} \le 10^{10}$ . none.

#### 2.10.2 Records: 802XXX, Density Data

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100. Density is assumed to be a function of temperature and is defined by pairs, giving the temperature and the density for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. Total number of data pairs for a material may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.10.8).

W-1 (R) :	RHSMDX	Temperature, (K). <i>Acceptable range:</i>	Temperature values must increase. Thus the value must be greater than the value of RHSMDX for the previous point.			
		Default value:	none.			
W-2 (R) :	RHSMDY	Density, (kg/m <sup>3</sup> ). Acceptable range: Default value:	$0.0 < \text{RHSMDY} \le 10^{10}$ . none.			

# 2.10.3 Records: 803XXX, Specific Heat Data

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100. Specific heat is assumed to be a function of temperature and is defined by pairs, giving the temperature and the specific heat for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. Total number of data pairs for a material may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.10.8).

W-1 (R) :	CPSMDX	Temperature, (K). <i>Acceptable range:</i>	Temperature values must increase. Thus the value must be greater than the value of CPSMDX for the previous point.
		Default value:	none.
W-2 (R) :	CPSMDY	Specific heat, (J/kg Acceptable range: Default value:	/K). $0.0 < CPSMDY \le 10^{10}$ . none.

#### 2.10.4 Records: 804XXX, Diffusion Coefficients for Fission Product Vapors

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100. The diffusion coefficients are used only if sorption of fission products is calculated. In such case they are used to calculate diffusion of the sorbed fission products into the SC or TC materials. The diffusion coefficient is calculated from:

$$D_{CS} = D_0 \cdot \exp\left(-\frac{A_D}{T}\right)$$

Limits are applied:

$$D_{\min} \leq D_{CS} \leq D_{\max}$$

W-1 (R) :	IVAP	Fission product vap Acceptable range: Default value:	por class number. must be one of the existing fission product vapor classes. none.
W-2 (R) :	DCS0MP	Coefficient $D_0$ , (m <sup>2</sup> vapor class IVAP entered for this mat	$^{2}$ /s), in the correlation for $D_{CS}$ of the fission product in the solid material XXX. If zero or no value is terial, the diffusion will not be calculated.

Acceptable range:  $0.0 \le DCSOMP \le 1.0 \times 10^{+6}$ Default value: 0.0

W-3 (R) :	ADCSMP	Coefficient <i>A</i> <sub>D</sub> , (K) vapor class IVAP ir <i>Acceptable range:</i> <i>Default value:</i>	), in the correlation for $D_{CS}$ of the fission product in the solid material XXX. $0.0 \le \text{ADCSMP} \le 1.0 \times 10^{10}$ 0.0
W-4 (R) :	DMINMP	Lower limit, $D_{\min}$ , (1 vapor class IVAP ir Acceptable range: Default value:	m <sup>2</sup> /s), in the correlation for $D_{CS}$ of the fission product a the solid material XXX. $0.0 \le \text{DMINMP} \le 1.0 \times 10^{-6}$ 0.0
W-5 (R) :	DMAXMP	Upper limit, $D_{max}$ , (1 vapor class IVAP ir Acceptable range: Default value:	m <sup>2</sup> /s), in the correlation for $D_{CS}$ of the fission product in the solid material XXX. DMINMP $\leq$ DMAXMP $\leq 1.0 \times 10^{-6}$ $1.0 \times 10^{-6}$

#### 2.10.5 Records: 805XXX, Material Name

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100.

 W-1 (A): NAMESM User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.
 Acceptable range: any string of up to 50 characters. Default value: 50 "underline" characters: "\_".

# 2.10.6 Records: 806XXX, Materials Composed of Different Materials

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100.

Using this record, the user may specify a material that is composed from several (up to 10) different materials. The average thermophysical properties of such material are obtained from:

$$\overline{\rho \cdot c_p} = \sum_i x_i \cdot \rho_i \cdot c_{p,i} \qquad \overline{k} = \sum_i x_i \cdot k_i \qquad or \qquad \overline{1/k} = \sum_i x_i / k_i$$

 $x_i$  = volumetric fraction of the material *i* in the mixture, (-)  $\rho_i$  = density of the material *i*, (kg/m<sup>3</sup>)  $c_{p,i}$  = specific heat of the material *i*, (J/kg-K)  $k_i$  = conductivity of the material *i*, (W/m<sup>2</sup>-K)

An example of the situation where this record is useful, is the fuel of high temperature reactor, consisting of graphite and TRISO particles, which in turn consist of fuel kernel and several coating layers.

W-1 (R) :	CCOMMP	Option to calculate  CCOMMP  = 1.0:  CCOMMP  = 2.0: < CCOMMP  < 2.0:	average thermal conductivity, (see Figure 2-61): use average thermal conductivity: $k = \Sigma(x_ik_i)$ use average thermal resistance: $1/k = \Sigma(x_i/k_i)$ interpolate between the first and the second formula: $k = (2- CCOMP ) \times \Sigma x_i k_i + ( CCOMP -1) \times \Sigma x_i/k_i$
		Furthermore, this	entry determines if the composition is defined by
		volume fractions or	r by mass fractions:
		CCOMMP>0.0: X	COMMP are interpreted as volume fractions
		CCOMMP<0.0:  X	COMMP are interpreted as mass fractions
		Acceptable range:	1.0 <  CCOMMP  < 2.0
		Default value:	2.0 (conservative: gives the lowest conductivity)
W-2 (I) :	ICOMMP	Material number of	f the first material in the composition.
	(1)	Acceptable range:	This must be a single material, i.e. it cannot be a another composed material.
		Default value:	none.
W-3 (R) :	XCOMMP	Volumetric fractic material in the com	on (mass fraction if CCOMMP<0.0) of the first aposition.
	(1)	Acceptable range:	$0.0 \leq \text{XCOMMP} < 1.0$
	(-)	Default value:	none.
W-4 (I) ·	ICOMMP	Material number of	f the second material in the composition
	(2)	Acceptable range:	This must be a single material, i.e. it cannot be a another composed material.
		Default value:	none.
W-5 (R) :	XCOMMP	Volumetric fractio	n (mass fraction if CCOMMP<0.0) of the second
		Acceptable range	$0.0 \leq \text{XCOMMP} < 1.0$
		Default value:	none.

... etc. until all materials are defined. The maximum number of materials is 10.





# 2.10.7 Records: 800XXX, Constant Multipliers on the Material Properties

XXX is the material reference number. The material reference numbers need not be consecutive. The maximum number of materials is 100.

W-1 (R) :	TCMLMP	Multiplier on the thermal conductivity data, TCSMDY (defined i 801XXX).	in
		Acceptable range: $0.01 < \text{TCMLMP} \le 100.0$	
		Default value: 1.00	
W-2 (R) :	RHMLMP	Multiplier on the density data, RHSMDY (defined in 802XXX).	
		Acceptable range: $0.01 < \text{RHMLMP} \le 100.0$	
		Default value: 1.00	
W-3 (R) :	CPMLMP	Multiplier on the specific heat data, CPSMDY (defined in 803XXX).	
		Acceptable range: $0.01 < \text{CPMLMP} \le 100.0$	
		Default value: 1.00	

# 2.10.8 Examples of Material Property Input Data

The input shown below defines material property for concrete (Stone 1-2-4 mix), stainless steel SS 304 and carbon steel SA533B1. The values for concrete are based on [9] (table A-3) and are valid for temperature of 20 °C. The values for stainless steel and carbon steel are based on graphs shown in [16] and define material properties valid for the temperature ranges:

- for - for	stainless steel: carbon steel:	from 300 K to 1300 from 300 K to 1000	K, K.
*	Definition of	material No. 001;	Concrete
805001 *	Concrete Temperature	Thermal conducti	vity
801001 *	(K) 293.0 Temperature	(W/M/K) 1.37 Density	*
* 802001 *	(K) 293.0 Temperature	(kg/m3) 2300.0 Specific heat	*
* 803001 *	(K) 293.0	(J/kg/K) 880.0	*
* * *	Definition of	material No. 002;	
* 805002 *	Stainless stee Temperature	el, SS-304 Thermal conducti	vity
*	(K)	(W/m/K)	
801002	300.0	13.5	*
801002	800.0	23.0	*
801002	1300.0	32.0	*
*	Temperature	Density	
*	(K)	(kg/m3)	
802002	300.0	7800.0	*
802002	800.0	7600.0	т Т
*	1300.0	/35U.U	^
*	Temperature	Specific heat	
003003	300 0	(J/KG/K) 410 0	*
803002	500.0	410.0	*
803002	800.0	400.0 500.0	*
803002	1300.0	550.0	*
*	1000.0	000.0	
*			
* *	Definition of	material No. 003;	SA533B1 ======
805003	Carbon steel,	SA533B1	
*	Temperature	Thermal conduction	vity
*	(K)	(W/m/K)	т
801003	300.0	52.0	т Т
801003	600.0	44.0	^ +
001003	1000.0	30.0	*
*	Temperature	Density	
*	(K)	(kg/m3)	
802003	300 0	7850 0	*
802003	500.0	7790.0	*
802003	700.0	7720.0	*
*	Temperature	Specific heat	
*	(K)	(J/kg/K)	
803003	300.0	450.0	*
803003	600.0	600.0	*
803003	800.0	700.0	*
803003	1000.0	950.0	*

\* \_\_\_\_\_

The same input may be defined by specifying multiple data pairs in a single data record:

~										
805001	Concrete	9								
*	T (K)	Value								
801001	293.0	1.37	* Tł	nermal c	conductiv	/ity (W/	m/K)			
802001	293.0	2300.0	* De	ensity (	(kq/m3)					
803001	293.0	880.0	* Sp	pecific	heat (J	/kq/K)				
*			-			<u> </u>				
*										
805002	Stainles	s steel	, SS-3	304						
*	T (K)	Value	T (K)	Value	T (K)	Value	T (K)	Value		
801002	300.0	13.5	800.0	23.0	1300.0	32.0			*	Thermal conductivity
802002	300.0	7800.0	800.0	7600.0	1300.0	7350.0			*	Density
803002	300.0	410.0	500.0	450.0	800.0	500.0	1300.0	550.0	*	Specific heat
*										
805003	Carbon s	steel,	SA533B1	1						
*	T (K)	Value	T (K)	Value	T (K)	Value	T (K)	Value		
801003	300.0	52.0	600.0	44.0	800.0	38.0	1000.0	30.0	*	Thermal conductivity
802003	300.0	7850.0	500.0	7790.0	700.0	7720.0			*	Density
803003	300.0	450.0	600.0	600.0	800.0	700.0	1000.0	950.0	*	Specific heat

The following records illustrates how to re-define material property data:

* T (K)	k (W/m/K)	
801002 300.0	13.5	* old data point 1
801002 800.0	23.0	* old data point 2
801002 0		* start re-defining the k data
801002 273.0	125.0	* new data point 1
801002 973.0	225.0	* new data point 2

The following records illustrates how to define a material composed of several materials. The example defines TRISO particles in graphite matrix with packing factor of 0.25 (volumetric fraction of TRISO particles is 25%): It is assumed that the properties of graphite and TRISO particles are defined as:

- Material 502 graphite
- Material 111 fuel kernel
- Material 122 PyC (buffer)
- Material 123 iPyC
- Material 121 SiC
- Material 124 oPyC

Volume fractions of the fuel and coatings in a single TRISO particle were calculated assuming the following dimensions: fuel kernel diameter 500  $\mu$ m, buffer 95  $\mu$ m, iPyC 40  $\mu$ m, SiC 35  $\mu$ m, oPyC 40  $\mu$ m. The input deck defining such material is shown below.

805572	Gr	aphite	e-Fuel										
*		Grap	phite	Fue	el	but	ffer	iPyC	2	Si	2	oP	уC
*	k	Mat.	Vol.fr.	Mat.	Vol.fr.	Mat.	Vol.fr.	Mat.	Vol.fr.	Mat.	Vol.fr.	Mat.	Vol.fr.
806572	0	502	0.7500	111	0.04013	122	0.06534	123	0.04110	121	0.04372	124	0.05971

# 2.11 User-Defined Gas Data

The SPECTRA code contains six built-in gases:

- H<sub>2</sub> hydrogen
- He helium
- H<sub>2</sub>O steam
- N<sub>2</sub> nitrogen
- O<sub>2</sub> oxygen
- CO<sub>2</sub> carbon dioxide

These gases are treated as real gases. For all the gases except for the steam, the virial equation of state is used. The properties are tabulated versus temperature and pressure - see Volume 1.

On top of the built-in gases, user-defined gases are available. The total number of gases (built-in + user-defined) is 20. The user-defined gases are treated as semi-perfect gases. The perfect gas equation of state is used. The specific heat, the viscosity, and the thermal conductivity, are assumed to be functions of temperature.

The user has to define the following parameters:

- Molar weight,  $M_w$ , (kg/kmol)
- Molecular diffusion volume,  $\Sigma$ , (-)
- Specific heat,  $c_p(T)$ , (J/kg-K)
- Viscosity,  $\eta(T)$ , (kg/m-s)
- Thermal conductivity, *k*(*T*), (W/m-K)

# 2.11.1 Record: G05XXX, Name of the User-Defined Gas

XXX is the user-defined gas number. The gas numbers must start at 007 (because there are six builtin gases) and be consecutive. The maximum number of gases is equal to: NGMXFL = 20.

Default value: 50 "underline" characters: " ".

# 2.11.2 Record: 830XXX, Molar Weight, Diffusion Volume, Reference Energy

XXX is the user-defined gas number. The gas numbers must start at 007 (because there are six builtin gases) and be consecutive. The maximum number of gases is equal to: NGMXFL = 20.

W-1 (R): WMOLFL Molar weight,  $M_w$  (kg/kmol), of the user-defined gas XXX. Used to calculate the individual gas constant, R, (needed for the perfect gas equation of state):

$$R = \frac{R_u}{M_w}$$

 $R_u$ universal gas constant (=8314.51), (J/kmol-K)Rindividual gas constant, (J/kg-K) $M_w$ gas molar weight, (kg/kmol)The molar weights of some elements and compounds are given in<br/>Table 2-37.Acceptable range: $10^{-1} < WMOLFL < 10^3$ Default value:none

W-2 (R): DVGSFL Molecular diffusion volume, Σ, of the user-defined gas XXX. Used to calculate the diffusion coefficients for a gas mixture. The molecular diffusion volume of some elements and compounds are given in Table 2-37.

Element	$M_W$	Σ	Compound	$M_W$	Σ
С	12.01	15.90	H <sub>2</sub>	2.02	6.12
Н	1.01	2.31	$D_2$	4.03	6.84
0	16.00	6.11	$N_2$	28.00	18.50
Ν	14.00	5.43	$O_2$	32.00	16.30
F	19.00	14.70	Air	28.01	19.70
Cl	35.45	21.00	CO	28.80	18.0
Br	79.90	21.90	$CO_2$	44.01	26.90
Ι	126.90	29.80	$N_2O$	44.00	35.90
S	32.06	22.90	$NH_3$	16.02	20.70
He	4.00	2.67	$H_2O$	18.02	13.10
Ne	20.18	5.98	$SF_4$	108.06	71.30
Ar	39.95	16.20	$Cl_2$	70.91	38.40
Kr	83.80	24.50	$Br_4$	159.80	69.00
Xe	131.30	32.70	$SO_2$	64.06	41.80

Table 2-37 Molar weights [39] (page 1-7) and molecular diffusion volumes, [43] (table 11-1).

none

For other materials the value may be estimated from the following correlations:

elements:  $\Sigma \sim 1.3 \cdot M_w^{0.66}$ compounds:  $\Sigma \sim 2.5 \cdot M_w^{0.66}$ Results obtained with the above correlations are shown in Figure 2-62. *Acceptable range:*  $0.0 < \text{DVGSFL} < 10^3$ 

a warning message is issued if the value is outside the range:  $1.3 \cdot M_w^{0.66} \times 0.5 \div 2.5 \cdot M_w^{0.66} \times 2.0$ 

Default value:



Figure 2-62 Diffusion volumes - data and correlations:  $\Sigma = 1.3 \cdot M_w^{0.66}$ ,  $\Sigma = 2.5 \cdot M_w^{0.66}$ .

W-3(R):

UREFFL Value of the internal energy,  $u_{ref}$  (J/kg), at the reference point,  $T_0$ . The reference point is assumed to be the first point in the specific heat data table (the first value of XCPGFL in the record 831XXX). The internal energy of gas XXX at this temperature will be equal to UREFFL. For other temperatures the internal energy is calculated by integrating the specific heat data provided by the user in the record 831XXX, as:

$$u(T) = u_{ref} + \int_{T_0}^{T} [c_p(T') - R] dT'$$

Here *R* is the gas constant.

Acceptable range:UREFFL  $\geq 0.0$ Default value:0.0

# 2.11.3 Record: 831XXX, Specific Heat

XXX is the user-defined gas number. The gas numbers must start at 007 (because there are six builtin gases) and be consecutive. The maximum number of gases is equal to: NGMXFL = 20. Specific heat is assumed to be a function of temperature and is defined by pairs, giving the temperature and the specific heat for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. The total number of data pairs for a single gas may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.11.6).

W-1 (R) :	XCPGFL	Temperature, T (K).		
		Acceptable range:	$0.0 < T < 10^4$ . Temperature values must increase.	
			Thus the value must be greater than the value of T	
			for the previous point. The first value is set as a	
			reference temperature, $T_{ref}$ , and cannot be larger	
			than 270 K. The recommended value is 0.0.	
		Default value:	none.	
W-2 (R) :	YCPGFL	PGFL Specific heat at the temperature $T$ , $c_p(T)$ (J/kg-K).		
		Acceptable range:	$2 \times R < \text{YCPGFL} < 10^5$ ( <i>R</i> is the gas constant)	
		Default value:	none	

# 2.11.4 Record: 832XXX, Dynamic Viscosity

XXX is the user-defined gas number. The gas numbers must start at 007 (because there are six builtin gases) and be consecutive. The maximum number of gases is equal to: NGMXFL = 20. Viscosity is assumed to be a function of temperature and is defined by pairs, giving the temperature and the viscosity for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. The total number of data pairs for a single gas may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.11.6).

W-1 (R) :	XVSGFL	Temperature, T (K).		
		Acceptable range:	$0.0 < T < 10^4$ . Temperature values must increase.	
			Thus the value must be greater than the value of T	
			for the previous point.	
		Default value:	none.	
W-2 (R) :	YVSGFL	Viscosity at the ten	nperature T, $\eta(T)$ (kg/m-s).	
		Acceptable range:	$10^{-10} < YVSGFL < 10^{+1}$	
		Default value:	none	
# 2.11.5 Record: 833XXX, Thermal Conductivity

XXX is the user-defined gas number. The gas numbers must start at 007 (because there are six builtin gases) and be consecutive. The maximum number of gases is equal to: NGMXFL = 20. Thermal conductivity is assumed to be a function of temperature and is defined by pairs, giving the temperature and the thermal conductivity for that temperature. Each record contains one or several data pairs. Records are read sequentially - the first record in the input is interpreted as containing the first set of data pairs. The total number of data pairs for a single gas may not exceed 100. To re-define the data, enter a record with a single entry of zero, followed by the new data table (see example in section 2.11.6).

W-1 (R) :	XTCGFL	Temperature, T (K)	).
		Acceptable range:	$0.0 < T < 10^4$ . Temperature values must increase.
			Thus the value must be greater than the value of T
			for the previous point.
		Default value:	none.
W-2 (R) :	YTCGFL	Thermal conductiv	ity at the temperature $T$ , $k(T)$ (W/m-K).
		Acceptable range:	$10^{-10} < \text{YTCGFL} < 10^{+1}$
		Default value:	none

### 2.11.6 Examples of the User-Defined Gas Data

The input below defines carbon monoxide, argon, and neon, as user-defined gases number 7, 8, 9.

```
= User-defined gas data, Data for CO, Ar, Ne
      Ref.
      (Lide, 1992) - D.R. Lide, et al., ""CRC Handbook of Chemistry and Physics,
A Ready-Reference Book of Chemical and Physical Data",
72-nd edition, ISBN-0-8493-0472-5, CRC Press Inc., 1991-1992.
G05007 CO , Carbon monoxide
*
             Molar
                            Diffusion
                                                U-ref
                              volume
                                                (J/kg)
0.0
              weight
830007
                             18.0
              28.8
*
    * T Value T Value T Value T Value T Value
    * Cp (J/kg-K) ((Lide, 1992), p. 8-50)
    * Cp (J/kg-K) ((Lide, 1992), p. 6-154)
    * S3007 300.0 1.78E-5 400.0 2.21E-5 500.0 2.58E-5 600.0 2.91E-5 * Visc, (kg/m-s) ((Lide, 1992), p. 6-154)
    * S3007 300.0 0.0250 400.0 0.0323 500.0 0.0392 600.0 0.0457 * k, (W/m-K) ((Lide, 1992), p. 6-162)

G05008
            Ar , Argon
*
             Molar
                        Diffusion U-ref
             weight
39.95
                            volume (J/kg)
16.2 0.0
830008
           T Value
0.0 520.0
300.0 2.29E-5
300.0 0.0179
                                       T Value
                                                                   T Value
                                                                                              T Value
                                                                                                                   * Cp (J/kg-K)
                                                                                                                                             ((Lide, 1992), p. 6-68)
831008
                                   400.0 2.88E-5
400.0 0.0226
                                                               500.0 3.42E-5 600.0 3.90E-5 * Visc, (kg/m-s) ((Lide, 1992), p. 6-154)
500.0 0.0268 600.0 0.0306 * k, (W/m-K) ((Lide, 1992), p. 6-162)
832008
833008
G05009 Ne , Neon
*
             Molar
                            Diffusion U-ref
             weight 20.18
                           volume (J/kg)
5.98 0.0
830009
                                    T Value
          T Value
                                                                                              T Value
                                                                                                                  * Cp (J/kg-K)
                                                                                           * Cp (J/kg-K) ((Lide, 1992), p. 5-68)
600.0 5.08E-5 * Visc, (kg/m-s) ((Lide, 1992), p. 6-154)
600.0 0.0787 * k, (W/m-K) ((Lide, 1992), p. 6-162)
831009
832009
                                                                  500.0 4.50E-5
833009
                                                                  500.0 0.0699
```

#### The following records illustrates how to re-define the gas property data:

831008 832008 833008	0.0 300.0 300.0	520.0 2.29E-5 0.0179	400.0 400.0	2.88E- 0.0226	5 500.0 500.0	3.42E-5 0.0268	600.0 600.0	3.90E-5 0.0306	* Cp ( 5 * Visc * k, (	J/kg-K) , (kg/m-s) W/m-K)	((Lide, ((Lide, ((Lide,	1992), p. 1992), p. 1992), p.	6-68) 6-154) 6-162)
833008 833008	0 * 300.0	start re- 0.179	-defining 400.0	the k d	ata 500.0 (	0.268	600.0 0.	306 * 1	<pre>&lt; values</pre>	increased	x 10 fo:	r sensitiv	itv

### 2.12 Alternative Fluid (Liquid Metal, Molten Salt, etc.) Property Data

The alternative fluid may be specified in SPECTRA instead of water. In such case water properties are replaced by the properties of the alternative fluid, defined in these records. This option is included primarily for analyzing liquid metal and molten salt reactors.

Note that when the alternative fluid) is defined, it is used in all Control Volumes and therefore liquid water is not available. If the user wishes to run a model in which both liquid metal and water are needed, then the model must be split into two parts, one containing liquid metal and one containing water. The two models may then be run in parallel using the synchronized option in the EDF Package (section 2.18). An example of such synchronized run with liquid metal on the primary side and water on the secondary side is shown in Volume 3.

The alternative fluid is only used as a liquid. Any evaporation is prohibited. This is done by deactivating the bubble collapse model and setting the multipliers on the Sherwood number correlations to zero (see section 2.1.25, records 155XXX, and section 2.1.3.2, record 810020):

$$XBCMCV(i) = -1, \qquad i = 1, 2, 3$$
$$XSHPHT = XSHDHT = XSHBHT = 0$$

Boiling is prevented by limiting the maximum liquid temperature to a value of DTSBFL below saturation.

$$T \leq T_{sat}(p) - DTSBFL$$

The critical mass flow in SPECTRA is appropriate for water as liquid. Therefor the critical flow must be defined using the user-defined critical flow (see record 262000).

#### 2.12.1 Record: 840000, Alternative Fluid Activator

W-1 (I) :	IFLDFL	Alternative fluid activator:
		= 1: No alternative fluid (built-in water properties are used).
		= 2: Alternative fluid is used. Tabulated fluid properties are supplied by
		the user in the records 841000 and 842000. The properties are tabulated
		versus temperature in Kelvins (K). During the calculations the
		parameters (temperature, pressure) in any Control Volume must be
		within the tabulated range.
		= 3: Alternative fluid is used. Tabulated fluid properties are supplied by
		the user in the records 841000 and 842000. The properties are tabulated
		versus temperature in degrees Celsius (°C). During the calculations the
		parameters (temperature, pressure) in any Control Volume must be
		within the tabulated range.
		Acceptable range: 1, 2, 3
		Default value: 1

W-2 (R): DTSBFL Minimum subcooling for alternative fluid. Used only if IFLDFL > 1. In order to avoid saturated and subcooled boiling of the alternative fluids, calculations are stopped when the subcooling in any CV is below the value of DTSBFL:  $T > T_{sat}(p) - DTSBFL$ . Acceptable range:  $0.1 \le DTSBFL \le 10.0$ Default value: 1.0

## 2.12.2 Record: A05000, Name of the Alternative Fluid

W-1 (A): NAMEFL User-defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* 50 "underline" characters: "\_".

### 2.12.3 Records: 841000, Thermodynamic Properties of the Alternative Fluid

Each record defines data for one temperature point. The record is repeated as many times as needed to define the fluid properties for the desired temperature range. The temperature values must be in ascending order. The maximum number of data points is 1000.

W-1 (R) :	TTABFL	Temperature for the thermodynamic property data tables, $T_i$ , (K or °C). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then <u>all tables</u> of the thermodynamic properties are filled using the built-in steam-water property data (in other words, all data that may follow in this record is ignored). Acceptable range: $0 \le T_i \le 10^9$ $T_{i-1} < T_i < T_{i-1} \times 10$ Default value: none
W-2 (R) :	PTABFL	Saturation pressure at the temperature $T_i$ , $p_{sat}(T_i)$ , (Pa). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 < p_{sat}(T_i) \le 10^9$ $p_{sat}(T_{i-1}) < p_{sat}(T_i) < 10 \times p_{sat}(T_{i-1})$ Default value: none
W-3 (R) :	HFTBFL	Saturated liquid enthalpy at the temperature $T_i$ , $h_f(T_i)$ , (J/kg). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le h_f(T_i) \le 10^9$ $h_f(T_{i-1}) < h_f(T_i) < 10 \cdot \times h_f(T_{i-1})$ Default value: none

W-4 (R) :	HGTBFL	Saturated vapor enthalpy at the temperature $T_i$ , $h_g(T_i)$ , (J/kg). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le h_g(T_i) \le 10^9$ , $h_g(T_{i-1}) / 10 < h_g(T_i) < 10 \times h_g(T_{i-1})$ Default value: none
W-5 (R) :	RFTBFL	Saturated liquid density at the temperature $T_i$ , $\rho_f(T_i)$ , (kg/m <sup>3</sup> ). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le \rho_f(T_i) \le 10^9$ , $\rho_f(T_{i-1}) / 10 < \rho_f(T_i) < \rho_f(T_{i-1})$ Default value: none
W-6 (R) :	RGTBFL	Saturated vapor density at the temperature $T_i$ , $\rho_g(T_i)$ , (kg/m <sup>3</sup> ). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le \rho_g(T_i) \le 10^9$ , $\rho_g(T_{i-1}) < \rho_g(T_i) < 10^9$ , Default value: none
W-7 (R) :	SFTBFL	Saturated liquid entropy at the temperature $T_i$ , $s_f(T_i)$ , $(J/kg \cdot K)$ . The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le s_f(T_i) \le 10^9$ $s_f(T_{i-1}) < s_f(T_i) < 10 \cdot \times s_f(T_{i-1})$ Default value: none
W-8 (R) :	SGTBFL	Saturated vapor entropy at the temperature $T_i$ , $s_g(T_i)$ , $(J/kg \cdot K)$ . The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le s_g(T_i) \le 10^9$ , $s_g(T_{i-1}) / 10 < s_g(T_i) < s_g(T_{i-1}) \times 10$ Default value: none
W-9 (I) :	Ι	Data point number. If no value, or zero is entered, then the data are read sequentially - the first record in the input is interpreted as containing the first data set (lowest temperature, I=1), then I=2, etc. Acceptable range: $0 < I \le 1000$ Default value: none.

## 2.12.4 Records: 842000, Thermo-Physical Properties of the Alternative Fluid

Each record defines data for one temperature point. The record is repeated as many times as needed to define the fluid properties for the desired temperature range. The temperature values must be in ascending order. The maximum number of data points is 1000.

W-1 (R) :	TTBTFL	Temperature for the thermo-physical property data tables, $T_i$ , (K or °C). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then <u>all tables</u> of the thermo-physical properties are filled using the built-in steam-water property data (in other words, all data that may follow in this record is ignored). Acceptable range: $0 \le T_i \le 10^9$ $T_{i-1} < T_i < T_{i-1} \times 10$ Default value: none.
W-2 (R) :	VFTBFL	Saturated liquid viscosity at the temperature $T_i$ , $\eta_f(T_i)$ , (kg/m·s). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le \eta_f(T_i) \le 10^9$ , $\eta_f(T_{i-1}) / 10 < \eta_f(T_i) < \eta_f(T_{i-1})$ Default value: none
W-3 (R) :	VGTBFL	Saturated vapor viscosity at the temperature $T_i$ , $\eta_g(T_i)$ , (kg/m·s). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le \eta_g(T_i) \le 10^9$ , $\eta_g(T_{i-1}) < \eta_g(T_i) < \eta_g(T_{i-1}) \times 10$ Default value: none
W-4 (R) :	TFTBFL	Saturated liquid thermal conductivity at temperature $T_i$ , $k_f(T_i)$ , (W/m·K) The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le k_f(T_i) \le 10^9$ , $k_f(T_{i-1}) / 10 < k_f(T_i) < k_f(T_{i-1}) \times 10$ Default value: none
W-5 (R) :	TGTBFL	Saturated vapor thermal conductivity at temperature $T_i$ , $k_g(T_i)$ , (W/m·K) The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le k_g(T_i) \le 10^9$ , $k_g(T_{i-1}) < k_g(T_i) < 10^9$ , $k_g(T_{i-1}) < k_g(T_i) < 10$ Default value: none

W-6 (R) :	PFTBFL	Saturated liquid Prandtl number at temperature $T_i$ , $Pr_f(T_i)$ , (-). The entered values must be positive for all data points or zero for all data points. Acceptable range: $0 \le Pr_f(T_i) \le 10^9$ , $Pr_f(T_{i-1}) / 10 < Pr_f(T_i) < Pr_f(T_{i-1}) \times 10$ Default value: $Pr_f = c_{pf} \times \eta_f / k_f$ where: $\eta_f = \text{viscosity value: VFTBFL}$ $k_f = \text{thermal conductivity value: TFTBFL}$ $c_{pf} = \text{specific heat} = dh_f/dT$ , with $h_f = \text{HFTBFL}$ A warning message is issued if the entered value is more than 1% different from the default value.
W-7 (R) :	PGTBFL	Saturated vapor Prandtl number at temperature $T_i$ , $Pr_g(T_i)$ , (-). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le Pr_g(T_i) \le 10^9$ , $Pr_g(T_{i-1}) / 10 < Pr_g(T_i) < Pr_g(T_{i-1}) \times 10$ Default value: none
W-8 (R) :	STTBFL	Surface tension at temperature $T_i$ , $\sigma_{fg}$ , (N/m). The entered values must be positive for all data points or zero for all data points. If zeroes are entered, then this table is filled using the built-in steam-water property data. Acceptable range: $0 \le \sigma_{fg}(T_i) \le 10^9$ , $\sigma_{fg}(T_{i-1}) / 10 < \sigma_{fg}(T_i) < \sigma_{fg}(T_{i-1}) \times 10$ Default value: none
W-9 (I) :	Ι	Data point number. If no value, or zero is entered, then the data are read sequentially - the first record in the input is interpreted as containing the first data set (lowest temperature, I=1), then I=2, etc. Acceptable range: $0 < I \le 1000$ Default value: none

# 2.12.5 Record: 843000, Heat Transfer Option

W-1 (R) :	IHTCFL	Heat transfer option:
		=1: use only the forced convection correlations, defined in the records
		843XXX, below.
		=2: use the forced convection correlations, defined in the records
		843XXX below, as well as the natural convection correlations, the same
		as in case of the standard fluid.
		Acceptable range: 1 or 2
		Default value: 1

#### 2.12.6 Record: 843XXX, Heat Transfer Correlations for Alternative Fluid

XXX is the correlation number. The correlation numbers must be consecutive (starting with 1). The maximum number of correlations is 99:  $001 \le XXX \le 099$ .

The alternative fluid model is intended mainly for liquid metal coolants. A generally applicable correlation is available in SPECTRA that may be used to represent forced convective heat transfer. The correlation is:

$$Nu = \left[A_0 + A_1 \cdot Re^{B_1} \cdot Pr^{C_1} \cdot \left(1 + A_2 \cdot Re^{B_2} \cdot Pr^{C_2}\right)^{D_2} \cdot \left(1 + A_3 \cdot Re^{B_3} \cdot Pr^{C_3}\right)^{D_3}\right] \times \left(\frac{\mu_f}{\mu_w}\right)^x$$

The value obtained from the correlation may be multiplied by a viscosity ratio:  $(\mu_f/\mu_w)^x$ , where *x* is the user-defined multiplier (XVISFL). Furthermore, if the multiplier  $X_{RB}$  (words XRBLSC, XRBRSC, XRBBTC) is used and the flow is defined as internal (IFCLSC, IFCRSC, IFCBTC = -1), then the value obtained from the above correlation is multiplied by  $X_{RB}$ .

The user should provide an appropriate correlation for every configuration in the analyzed problem. The total number of user-defined correlations is NHCAFL≤100. Selection of correlation is performed for each boundary surface using the input parameters IHCLSC, IHCRSC, IHCBTC (defined in records 321XXX, 322XXX, 420XXX, respectively).

If no correlation is selected in these records, the default selection is: the first correlation (record 843001) is applied for the rectangular geometry, the second (843002) for the cylindrical geometry, and the third correlation (843003) for the spherical geometry. If the number of correlations defined by the user is <3, then additional correlations will be defined automatically, so that there is always at least three correlations available to be used with rectangular, cylindrical, and spherical geometries.

The default values, listed below, are assigned if zeroes are entered or no data is entered for all input words in this record. The default values are applicable for liquid lead internal flow (see Volume 1, description of forced convection correlations).

W-1 (R) :	A0HCFL	$A_0$ in the user-defined	ned correlation.
		Acceptable range:	$-10^{10} \le A0HCFL \le 10^{10}$
		Default value:	4.8 for XXX=1, value from XXX-1 for XXX>1
W-2 (R) :	A1HCFL	$A_1$ in the user-defined	ed correlation.
		Acceptable range:	$0.0 \le A1HCFL \le 10^{10}$
		Default value:	0.0156 for XXX=1, value from XXX-1 for XXX>1
W-3 (R) :	B1HCFL	$B_1$ in the user-defined	ed correlation.
		Acceptable range:	$-100.0 \le B1HCFL \le 100.0$
		Default value:	0.85 for XXX=1, value from XXX-1 for XXX>1
W-4 (R) :	C1HCFL	$C_1$ in the user-defined	ned correlation.
		Acceptable range:	$-100.0 \le C1HCFL \le 100.0$
		Default value:	0.93 for XXX=1, value from XXX-1 for XXX>1

W-5 (R) :	A2HCFL	$A_2$ in the user-defined correlation.Acceptable range: $-10^{10} \le A2HCFL \le 10^{10}$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-6 (R) :	B2HCFL	$B_2$ in the user-defined correlation.Acceptable range: $-100.0 \le B2HCFL \le 100.0$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-7 (R) :	C2HCFL	$C_2$ in the user-defined correlation.Acceptable range: $-100.0 \le C2HCFL \le 100.0$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-8 (R) :	D2HCFL	$D_2$ in the user-defined correlation. Acceptable range: $-100.0 \le \text{D2HCFL} \le 100.0$ Default value: 0.0 for XXX=1, value from XXX-1 for XXX>1
W-9 (R) :	A3HCFL	$A_3$ in the user-defined correlation.Acceptable range: $-10^{10} \le A3HCFL \le 10^{10}$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-10 (R) :	B3HCFL	$B_3$ in the user-defined correlation.Acceptable range: $-100.0 \le B3HCFL \le 100.0$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-11 (R) :	C3HCFL	$C_3$ in the user-defined correlation.Acceptable range: $-100.0 \le C3HCFL \le 100.0$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-12 (R) :	D3HCFL	$D_3$ in the user-defined correlation.Acceptable range: $-100.0 \le D3HCFL \le 100.0$ Default value:0.0 for XXX=1, value from XXX-1 for XXX>1
W-13 (R) :	XVISFL	Power in viscosity ratio. If a non-zero value is specified, the correlation is multiplied by a viscosity ratio to the power of XVISFL:

$$\left(\frac{\mu_f}{\mu_w}\right)^x$$

Here  $\mu_f$  is the fluid viscosity obtained at the bulk fluid temperature, while  $\mu_w$  is the fluid viscosity obtained at the wall surface temperature. The power *x* is the input parameter XVISFL. *Acceptable range:* -100.0  $\leq$  XVISFL  $\leq$  100.0 *Default value:* 0.0

## 2.12.7 Record: 843YYY, Heat Transfer Correlation Sets for Alternative Fluid

YYY is the correlation set number. The correlation sets starts at 101 and must be consecutive. The maximum number of correlation sets is 99:  $101 \le YYY \le 199$ .

If a single heat transfer correlation is needed, then it may be defined using the records 843XXX. Such correlation is valid for the entire range of Reynolds numbers. If multiple correlations are needed, then a set of correlations may be defined in the present record. Up to ten correlations may be used in a single set. All correlations must be defined in the records 843XXX.

## **Correlation 1**

W-1 (I):	ICORFL(1) Correlation 1.
	Acceptable range: must be one of the correlations defined in the records 843XXX
	Default value: none
W-2 (R) :	RELLFL(1) Lower limit of the Reynolds number to apply Correlation 1. Typically this should be zero. If a positive value is used, the value of heat transfer correlation for Re smaller than the minimum value, will be constant and equal to the value for Re = RELLFL(1). Acceptable range: RELLFL(1) $\geq 0.0$ . Default value: 0.0
W-3 (R) :	REULFL(1)Upper limit of the Reynolds number to apply Correlation 1. <i>Acceptable range:</i> REULFL(1) > 0.0 <i>Default value:</i> none
	Correlation 2
W-4 (I) :	ICORFL(2) Correlation 2. Acceptable range: must be one of the correlations defined in the records 843XXX Default value: none
W-5 (R) :	$\begin{array}{llllllllllllllllllllllllllllllllllll$
W-6 (R) :	REULFL(2)Upper limit of the Reynolds number to apply Correlation 2. Acceptable range: REULFL(2) > RELLFL(2) × 1.1 Default value: none
	() until all correlations are defined. Maximum number of correlations is 10.

#### 2.12.8 Example of the Alternative Fluid Data - Data for Liquid Lead

The input below defines liquid lead as the alternative fluid. The recommended heat transfer correlations are used (see Volume 1). The data fields for the spherical geometry are left empty; therefore the cylindrical geometry correlation will be used for the spherical geometry.

The file LEAD-K.ATT contains properties of liquid lead tabulated versus temperature in Kelvins. The method to create such file is discussed in Volume 3. Below some parts of this file are listed

*								
* PR(	OPERTIES OF L	IQUID LEAD						
A05000 *	LIQUID LEA	١D						
840000 *	2 * DA	TA TABLES IN	KELVINS					
* * 1.)	THERMODYNAMI	C DATA OF THE	LEAD					
*	т (К)	P (Pa)	Hf (J/kg)	Hg (J/kg)	Rf (kg/m3)	Rg (kg/m3)	Sf (J/kg-K)	Sg (J/kg-K)
841000 841000 841000	6.00000E+02 6.10000E+02 6.20000E+02	5.38066E-07 9.52207E-07 1.71474E-06	6.45682E+04 6.60983E+04 6.77231E+04	0.00000E+00 0.00000E+00 0.00000E+00	1.06496E+04 1.06384E+04 1.06265E+04	0.00000E+00 0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00 0.00000E+00
841000	6.40000E+02	5.26237E-06	7.09638E+04	0.00000E+00	1.06026E+04	0.00000E+00	0.00000E+00	0.00000E+00
841000 841000 841000	1.98000E+03 1.99000E+03 2.00000E+03	8.66948E+04 9.17306E+04 9.70040E+04	2.67839E+05 2.69210E+05 2.70579E+05	0.00000E+00 0.00000E+00 0.00000E+00	9.00209E+03 8.99014E+03 8.97820E+03	0.00000E+00 0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00 0.00000E+00
841000 841000 *	2.01000E+03 2.02000E+03	1.02524E+05 1.05957E+05	2.71949E+05 2.72770E+05	0.00000E+00 0.00000E+00	8.96626E+03 8.95909E+03	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00
* 2.) *	THERMO-PHYSI	CAL DATA OF I	HE LEAD					
*	T (K)	Vf (kg/m-s)	Vg (kg/m-s)	Tf (W/m−K)	Tg (W/m−K)	Prf (-)	Prg (-)	ST (N/m)
842000 842000 842000 842000 842000	6.00000E+02 6.10000E+02 6.20000E+02 6.30000E+02 6.40000E+02	2.69778E-03 2.62479E-03 2.55164E-03 2.48275E-03 2.41779E-03	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	1.58066E+01 1.59100E+01 1.60200E+01 1.61300E+01 1.62400E+01	0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.00000E+00	2.52231E-02 2.43592E-02 2.34947E-02 2.26818E-02 2.19163E-02	0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.00000E+00	4.51132E-01 4.50070E-01 4.48940E-01 4.47810E-01 4.46680E-01
842000 842000 842000 842000 842000	1.98000E+03 1.99000E+03 2.00000E+03 2.01000E+03 2.02000E+03	7.80704E-04 7.78589E-04 7.76501E-04 7.74438E-04 7.73214E-04	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	3.09800E+01 3.10900E+01 3.12000E+01 3.13100E+01 3.13760E+01	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	3.47789E-03 3.45739E-03 3.43718E-03 3.41726E-03 3.40544E-03	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	2.95260E-01 2.94130E-01 2.93000E-01 2.91870E-01 2.91192E-01

#### 2.13 Heat Transfer Model Coefficients

The heat transfer model coefficients are applied for all 1-D and 2-D Solid Heat Conductors.

#### 2.13.1 Records: 810010, CHF Model Data

Typically the CHF increases with decreasing diameter. The dependency is well represented by:

$$CHF \sim \left(\frac{D}{D_0}\right)^n$$

where  $D_0$  is a reference diameter (equal to 0.008 m) and *n* is between -1/3 and -1/2. This relation holds for diameters larger than a certain critical diameter,  $D_{crit}$ . Below the critical diameter, CHF decreases with decreasing diameter. Measurement data indicate that the critical diameter depends on subcooling. For large subcooling (55 K) the critical diameter is smaller than 0.3 mm [46]. For subcooling of about 20 K it is about 1 - 2 mm [47]. For saturated liquid it is as large as 7 mm [48]. This data is approximated in SPECTRA by the following correlation:

$$D_{crit} = D_c \cdot \exp[-A_c X]$$

Here X is quality and  $D_c$  and  $A_c$  are constants. The data points are shown in Figure 2-63. The following constants are selected:  $D_c = 0.007$  m and  $A_c = 30.0$ . The line obtained with the correlation is shown in Figure 2-63. The coefficients  $D_c$  and  $A_c$  may be redefined in this record.



Figure 2-63 Critical diameter for CHF

- W-1 (R): DCHFHT Coefficient  $D_c$ , (m). Critical diameter for saturated liquid. Acceptable range:  $0.0 \le \text{DCHFHT} \le 0.01$ Default value: 0.007
- W-2 (R) :ACHFHTCoefficient  $A_c$ , (-).<br/>Acceptable range: $0.0 \le \text{ACHFHT} \le 1000.0$ <br/>negative or small positive value sets ACHFHT=0.0<br/>Default value:30.0

The Zuber critical heat flux correlation is used for pool boiling CHF calculation (see Volume 1):

$$CHF_{Zub} = C_{Zub}\rho_{gas}h_{l-\nu}\left(\frac{\sigma g(\rho_{liq} - \rho_{gas})}{\rho_{gas}^2}\right)^{0.25} \left(\frac{\rho_{liq}}{\rho_{liq} + \rho_{gas}}\right)^{0.5}$$

The value of coefficient  $C_{Zub}$  in the correlation is  $0.13 \div 0.18$ . For pool boiling in narrow channels, Monde-Mitsutake experiments [49] indicated that:

$$CHF_{M-M} = \frac{0.16}{1 + C_{LD}(L/D)} \rho_{gas} h_{l-\nu} \left(\frac{\sigma g(\rho_{liq} - \rho_{gas})}{\rho_{gas}^2}\right)^{0.25}$$

Here L/D is the ratio of length to heated equivalent diameter and  $C_{LD}$  is a constant, equal to 0.025 for tubes and 0.075 for annular channel with inner tube heated [49]. At low pressures, the density ratio  $(\rho_{liq} + \rho_{vap})^{0.5}$  is practically equal to 1.0. Calculations performed for pressures between 1.0 and 4.0 bar show that the value is between 0.999 and 1.0, so the error introduced be neglecting this term is below 0.1%. This means that the Monde and Mitsutake correlation may be defined in SPECTRA by defining the input parameter CZUBHT equal to:

$$CZUBHT = \frac{0.16}{1 + C_{LD}(L/D)}$$

For example, for L/D = 200, we have:

•	tube ( $C_{LD} = 0.025$ ), with $L/D = 200$ :	$C_{Zub} = \text{CZUBHT} = 0.16/(1+0.025\times200) = 0.0267$
•	annulus ( $C_{LD} = 0.075$ ), with $L/D = 200$ :	$C_{Zub} = \text{CZUBHT} = 0.16/(1+0.075 \times 200) = 0.01$

W-3 (R) :	CZUBHT	Coefficient in Zub entered, the value The value obtained of: $1.0 \times 10^{-4} - 1.0 \times$	er CHF correlation, $C_{Zub}$ , (-). If a negative value is is computed from the Control Function  CZUBHT . I from the Control Function is restricted to the range $10^2$ .
		Acceptable range:	$1.0 \times 10^{-4} \le CZUBHT \le 1.0 \times 10^{2}$ or reference to a Control Function
		Default value:	0.13
W-4 (R) :	COIMHT	Constant in Ivey-N	Iorris correction for subcooling, C <sub>0</sub> ,  C0IMHT .
		$ C0IMHT  < 10^{-10}$ :	Ivey-Morris correction deactivated.
		C0IMHT < 0.0:	Multiplier $(1-X)$ in pool boiling CHF deactivated.
		Acceptable range:	$-10.0 \le \text{COIMHT} \le 10.0$
		Default value:	0.1

#### 2.13.2 Records: 810020, Heat and Mass Transfer Model Data

This record allows to modify the heat and mass transfer correlations used for condensation or evaporation from pool surface, droplet surface, and bubble surface.

• Heat transfer

The heat transfer coefficient, h (W/m<sup>2</sup>-K), at gas-liquid interfaces is obtained from the Nusselt number (see Volume 1, Heat and Mass Transfer Correlations):

$$h = Nu \cdot \frac{k}{d}$$

Here k is the thermal conductivity and d is the characteristic dimension. The Nusselt number is obtained from appropriate correlations as shown in Volume 1. Using this record, the user may modify the Nusselt number obtained from the correlations by defining a constant multiplier on the Nusselt number,  $X_{Nu}$ :

$$h = X_{Nu} \cdot Nu \cdot \frac{k}{d}$$

• Mass transfer

The mass transfer coefficient,  $K_M$ , (kg/m2-s), at gas-liquid interfaces is obtained using the Sherwood number (see Volume 1, Heat and Mass Transfer Correlations):

$$K_M = Sh \cdot \frac{D_C}{d}$$

Here  $D_C$  is the diffusion coefficient and d is the characteristic dimension. The Sherwood number is obtained from appropriate correlations as shown in Volume 1. Using this record, the user may modify the Sherwood number obtained from the correlations by defining a constant multiplier on the Sherwood number,  $X_{Sh}$ :

$$K_m = X_{Sh} \cdot Sh \cdot \frac{D_C}{d}$$

W-1 (R) :	XNUPHT	Nusselt number multiplier, $X_{Nu}$ , heat transfer on the pool surface. Acceptable range: $0.0 \le \text{XNUPHT} \le 100.0$		
		Default value:	1.0 (a small number, $<10^{-50}$ , sets the value to 0.0)	
W-2 (R) :	XNUDHT	Nusselt number mu Acceptable range: Default value:	Itiplier, $X_{Nu}$ , heat transfer on the droplet surface. $0.0 \le \text{XNUDHT} \le 100.0$ $1.0$ (a small number, $< 10^{-50}$ , sets the value to 0.0)	
W-3 (R) :	XNUBHT	Nusselt number mu Acceptable range: Default value:	altiplier, $X_{Nu}$ , heat transfer on the bubble surface. $0.0 \le \text{XNUBHT} \le 100.0$ $1.0$ (a small number, $<10^{-50}$ , sets the value to 0.0)	

W-4 (R) :	XSHPHT	Sherwood number Acceptable range: Default value:	multiplier, $X_{Sh}$ , mass transfer on the pool surface. $0.0 \le \text{XSHPHT} \le 100.0$ 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0) 0.0 if an alternative fluid is used (see section 2.12). In such case any mass transfer must be avoided. The same effect may be obtained by setting the model activators to +2: MINGCV(IPLAT) section 2.1.38, MINTCV(IPLAT) section 2.1.39.
W-5 (R) :	XSHDHT	Sherwood number Acceptable range: Default value:	multiplier, $X_{Sh}$ , mass transfer on the droplet surface. $0.0 \le XSHDHT \le 100.0$ 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0) 0.0 if an alternative fluid is used (see section 2.12). In such case any mass transfer must be avoided. The same effect may be obtained by setting the model activators to +2: MINGCV(IDPAT) section 2.1.38, MINTCV(IDPAT) section 2.1.39.
W-6 (R) :	XSHBHT	Sherwood number Acceptable range: Default value:	multiplier, $X_{Sh}$ , mass transfer on the bubble surface. $0.0 \le XSHBHT \le 100.0$ 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0) 0.0 if an alternative fluid is used (see section 2.12). In such case any mass transfer must be avoided. The same effect may be obtained by setting the model activators to +2: MINGCV(IBBPL) section 2.1.38, MINTCV(IBBPL) section 2.1.39.
W-7 (R) :	XRBLHT	Default value of the left surface of 1-D record 321XXX. <i>Acceptable range:</i> <i>Default value:</i>	e convective heat transfer multiplier, $X_{RB}$ , used on the O Solid Heat Conductors: XRBLSC, defined in the $0.0 \le  \text{XRBLHT}  \le 10^6$ 0.0
W-8 (R) :	XRBRHT	Default value of the right surface of 1-J record 322XXX. Acceptable range: Default value:	e convective heat transfer multiplier, $X_{RB}$ , used on the D Solid Heat Conductors: XRBRSC, defined in the $0.0 \le  \text{XRBRHT}  \le 10^6$ 0.0
W-9 (R) :	XRBBHT	Default value of the boundary surface of the record 420XXX Acceptable range: Default value:	te convective heat transfer multiplier, $X_{RB}$ , used on the of 2-D Solid Heat Conductors: XRBBTC, defined in X. $0.0 \le  \text{XRBBHT}  \le 10^6$ 0.0

### 2.13.3 Records: 810030, BDC and CHF/MFB Model Data

#### • BDC

The Bubble Detachment Criterion (BDC) determines if bubbles produced during subcooled boiling will be entrained in the liquid. The value is calculated and printed in the output and plot files for informative purposes but is not used in the calculations. The BDC heat flux is obtained from the following correlation [53]:

$$BDC = \frac{v_{liq}(T_{sat} - T_{liq})}{\eta_C}$$

where: *BDC* heat flux at bubble detachment,  $(W/m^2)$ ,

- $v_{liq}$  liquid velocity, (m/s),
- $T_{sat}$  saturation temperature, (K),

 $T_{liq}$  liquid temperature in the bulk fluid, (K),

 $\eta_C$  critical value of the BDC parameter

The value of  $\eta_C$  is obtained from [53]:

$$\eta_C = A_{BDC} + B_{BDC} \cdot v_{liq}$$

Here:  $A_{BDC}$  is the first constant, (J/m<sup>3</sup>-K);  $B_{BDC}$  is the second constant, (J-s/m<sup>4</sup>-K).

W-1 (R) :	ABDCHT	Coefficient <i>A</i> <sub>BDC</sub> , (J Acceptable range: Default value:	$M/m^{3}$ -K). $0.0 \le ABDCHT \le 1.0 \times 10^{-3}$ $32.0 \times 10^{-6}$
W-2 (R) :	BBDCHT	Coefficient $B_{BDC}$ , (J Acceptable range: Default value:	$J/m^3$ -K). $0.0 \le BBDCHT \le 1.0 \times 10^{-3}$ $1.64 \times 10^{-6}$

#### Boiling curve hysteresis parameters

The boiling curve hysteresis is defined following the observation of Ramilison and Lienhard (see Volume 1). If the hysteresis is used, then the transition boiling curve is different when the wall temperature increases and different when it decreases. With increasing wall temperature, the transition boiling curve leads from the Critical Heat Flux (CHF) point to the Minimum Film Boiling (MFB) point. When the temperature decreases the transition boiling curve leads from MFB to  $q_{\text{max}}$ , defined as follows:

$$q_{\text{max}} = Min(q_{CHF}, q_{MFB} \times C_{hyst})$$

Here  $C_{hyst}$  is a constant, defined by Words 3 - 5 below. The effect of  $C_{hyst}$  is shown in Figure 2-64. Calculations shown in the figures were performed using 1 bar pressure and different values of  $C_{hyst}$ . The wall temperature was increased and then decreased and the resulting heat flux was plotted as a function of wall temperature. As can be seen, for this test, the value of  $C_{hyst} = 50$ . In order to eliminate the boiling hysteresis at all conditions, the user should define a large value of  $C_{hyst}$ .



Figure 2-64 Boiling hysteresis, effect of Chyst (CBH0HT)

W-3 (R) :	CBH0HT	Boiling curve, hyste Acceptable range: Default value:	eresis coefficient, $C_{hyst}$ , (-), vertical surfaces. $1.0 \le \text{CBH0HT} \le 1.0 \times 10^{10}$ 5.0
W-4 (R) :	CBH1HT	Boiling curve, hyste down. Acceptable range: Default value:	eresis coefficient, $C_{hyst}$ , (-), horizontal surfaces, facing $1.0 \le \text{CBH1HT} \le 1.0 \times 10^{10}$ CBH0HT
		. <b>J</b>	
W-5 (R) :	CBH2HT	Boiling curve, hyste	eresis coefficient, $C_{hyst}$ , (-), horizontal surfaces, facing
		Acceptable range: Default value:	$1.0 \le CBH2HT \le 1.0 \times 10^{10}$ CBH0HT

### • Void fraction-dependent multiplier for film boiling

The full film boiling correlation is used when the void fraction is below the critical value,  $\alpha_1$ , defined below. For larger void fractions a 3-rd order interpolation is performed to a mist flow at high void fraction ( $\alpha = 0.99$ ). The heat transfer coefficient obtained from the film boiling correlation is multiplied by the following void fraction-dependent factor:

$$F = (3 - 2 \cdot X) \cdot X^2$$

where:

$$X = \frac{1 - \alpha}{1 - \alpha_1}$$

Here  $\alpha$  is the void fraction and  $\alpha$ 1 is the critical value, above which the convective part of the heat transfer coefficient correlation is reduced. The interpolation is performed for  $\alpha_1 \le \alpha, \le \alpha_2$ , where  $\alpha_2$ , = 0.99. In order to eliminate the interpolation (*F* = 1.0 = const.), set  $\alpha_1$  to 1.0. The multiplier, *F*, is plotted in Figure 2-65.

W-6 (R) :	VFL0HT	Critical void fraction for film boiling, $\alpha_1$ , vertical surfaces. <i>Acceptable range:</i> $0.1 \le \text{VFLOHT} \le 1.0$ <i>Default value:</i> $0.80$
W-7 (R) :	VFL1HT	Critical void fraction for film boiling, $\alpha_1$ , horizontal surfaces, facing down. <i>Acceptable range:</i> $0.1 \le VFL1HT \le 1.0$ <i>Default value:</i> VFL0HT
W-8 (R) :	VFL2HT	Critical void fraction for film boiling, $\alpha_1$ , horizontal surfaces, facing up. <i>Acceptable range:</i> 0.1 $\leq$ VFL2HT $\leq$ 1.0

**VFL0HT** 



Default value:



# 2.14 Material Oxidation Data

Material oxidation is activated for each 1-D or 2-D Solid Heat Conductor in records 381XXX, 382XXX, and 480XXX. Several oxidation models are built-in - see Volume 1. The user may define his own oxidation model using the data specified in these records.

#### 2.14.1 Records: 8500XX, Oxidation Reaction Definition

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

The oxidation reaction is assumed to have the following general form:

$$Mt + n_1 Gs_1 \rightarrow MtOx + n_2 Gs_2 + n_3 Gs_3$$

Mt	oxidized material
MtOx	material oxide
$Gs_1$	gas 1 (oxidizing gas, for example steam, oxygen
$Gs_2$	gas 2 (product of reaction, for example hydrogen)
$Gs_3$	gas 3 (optional second product of reaction)
$n_1$	reaction ratio 1 - moles of gas $Gs_1$ per one mole of oxidized material
$n_2$	reaction ratio 2 - moles of gas $Gs_2$ per one mole of oxidized material
$n_3$	reaction ratio 3 - moles of gas $Gs_3$ per one mole of oxidized material

The reaction kinetics is assumed to have the following general form:

$$\frac{dm^{x}}{dt} = \left(\frac{1}{K_{T}(T) \cdot C_{T}(T, p_{i})} + \frac{1}{K_{v}(v, T)}\right)^{-1} \cdot K_{p}(p_{1}) \cdot M(B, ...)$$

m	mass of reacted material per unit surface area (kg/m <sup>2</sup> ),
x	exponent, (-) ( $x=2$ for a parabolic oxidation rate)
t	time (s),
Κ	reaction rate $((kg/m^2)^{x/s})$ ,
Т	temperature, (K),
v	velocity of the oxidizing gas, (m/s),
$p_i$	partial pressure of the gas <i>i</i> , (Pa),
$p_1$	partial pressure of the oxidizing gas, (Pa),
$K_T$	temperature-dependent term (defined in record 8510XX)
$C_T$	correction to the temperature-dependent term (defined in record 8511XX)
$K_{\nu}$	velocity-dependent term (defined in record 8520XX)
$K_p$	temperature-dependent term (defined in record 8530XX)
M(B,)	multiplier to account for the effect of burn-off

W-1 (I):	IGS1OX	Identifier of gas 1 >6=user defined ga	, $Gs_1$ . (1= H <sub>2</sub> , 2=He, 3=H <sub>2</sub> O, 4=N <sub>2</sub> , 5=O <sub>2</sub> , 6=CO <sub>2</sub> , as).
		<i>Acceptable range:</i> <i>Default value:</i>	property data base.
W-2 (I) :	IGS2OX	Identifier of gas 2, user defined gas).	<i>Gs</i> <sub>2</sub> . (1= H <sub>2</sub> , 2=He, 3=H <sub>2</sub> O, 4=N <sub>2</sub> , 5=O <sub>2</sub> , 6=CO <sub>2</sub> , >6=
		Acceptable range:	must be one of the gases in SPECTRA fluid property data base.
W-3 (R) :	RRT1OX	Reaction ratio 1, $n_1$	- number of moles of gas 1 per one mole of oxidized
		material Acceptable range: Default value:	$0.01 \le \text{RRT1OX} \le 100.0.$ none.
W-4 (R) :	RRT2OX	Reaction ratio 2, $n_2$ material	- number of moles of gas 2 per one mole of oxidized
		Acceptable range: Default value:	$0.0 \le \text{RRT2OX} \le 100.0.$ 0.0.
W-5 (R) :	XOX	Exponent in the rea Acceptable range: Default value:	action rate, x, (x=2.0 for parabolic reaction). $0.1 \le XOX \le 10.0.$ 2.0.
W-6 (R) :	QOXIOX	Reaction heat per u Acceptable range: Default value:	mit mass of oxidized material, $Q_{ox}$ , (J/kg). -10 <sup>10</sup> $\leq$ QOXIOX $\leq$ 10 <sup>10</sup> . none.
W-7 (R) :	OEXPOX	Volumetric growth $V(MtO_n)$ , to the volis a ratio of the thickness of an un- Acceptable range: Default value:	h ratio, $\sigma_{ox}$ . Ratio of the material oxide volume, lume of the material only $V(Mt)$ . In other words, this ickness of a fully oxidized material to the original oxidized material. $10^{-10} \le \text{OEXPOX} \le 100.0.$ none.
W-8 (R) :	RHMTOX	Density $\rho_{Mt}$ , of the Acceptable range: Default value:	material being oxidized, $Mt$ , (kg/m <sup>3</sup> ). 10.0 $\leq$ RHMTOX $\leq$ 50,000.0. none.
W-9 (R) :	WMMTOX	Molecular weight, Acceptable range: Default value:	$M_{Mt}$ , of the material being oxidized, $Mt$ , (kg/kmole). 1.0 $\leq$ WMMTOX $\leq$ 1000.0. none.

W-10 (R):XWATOXOxidation indicator for water-covered surfaces.<br/>> 0.0: if water-covered fraction of SC or TC surface exceeds XWATOX,<br/>the oxidation will not be calculated.<br/>< 0.0: if water-covered fraction of SC or TC surface exceeds<br/>|XWATOX|, oxidation by water will be calculated (steam/water<br/>oxidation model).<br/>Acceptable range:  $-1.0 \le XWATOX \le 1.0$ . Negative values allowed<br/>only for steam oxidation (IGS1OX = 3)<br/>Default value:  $1.0 \times 10^{-2}$ .

Optional second reaction product:

The data below is optional and should be entered only if there is more than one gaseous product of the oxidation reaction. For example graphite oxidation by steam:

 $C + H_2 O \rightarrow H_2 + CO$ 

In such case:  $Gs_1 = H_2O$ ,  $Gs_2 = H_2$ ,  $Gs_3 = CO$  (or  $Gs_2 = CO$ ,  $Gs_3 = H_2$ ,  $Gs_2$  and  $Gs_3$  can be reversed).

W-11 (I) :	IGS3OX	Identifier of gas 3, 0 user defined gas).	$Gs_2$ . (1=H <sub>2</sub> , 2=He, 3=H <sub>2</sub> O, 4=N <sub>2</sub> , 5=O <sub>2</sub> , 6=CO <sub>2</sub> , >6=	
		Acceptable range:	must be one of the gases in SPECTRA fluid property data base, if non-zero	
		Default value:	none.	
W-12 (R) :	RRT3OX	Reaction ratio 3, $n_3$ material	- number of moles of gas 3 per one mole of oxidized	
		Acceptable range: Default value:	$0.0 \le \text{RRT3OX} \le 100.0.$ none.	

## 2.14.2 Records: O050XX, Oxidation Reaction Name

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

 W-1 (A) NAMEOX User defined name, length up to 50 characters. The name is read as a 50-character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier.
 Acceptable range: any string of up to 50 characters. Default value: 50 "underline" characters: "\_".

# 2.14.3 Records: 8510XX, Temperature-Dependent Reaction Rate

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

The temperature-dependent oxidation rate is assumed to have the following general form:

$$K_T(T) = \begin{cases} A_1 \exp\left[-B_1/T\right] & for: T < T_1 \\ A_2 \exp\left[-B_2/T\right] & for: T > T_2 \end{cases}$$

$egin{array}{c} K_T \ A_1 \ B_1 \ T_1 \ A_2 \ B_2 \ T_2 \ T \end{array}$	temj coef coef max coef coef mini curre	perature-dependent reaction rate, $((kg/m^2)^x/s)$ , ficient determining the reaction rate at low temperatures, $((kg/m^2)^x/s)$ , ficient determining the reaction rate at low temperatures, $(K)$ , imum temperature limit to apply the low temperature kinetics, $(K)$ , ficient determining the reaction rate at high temperatures, $((kg/m^2)^x/s)$ , ficient determining the reaction rate at high temperatures, $(K)$ , imum temperature limit to apply the high temperature kinetics, $(K)$ , ent temperature, $(K)$ .
W-1 (R) :	A1OX	First coefficient in the low temperature kinetics equation, $A_1$ , $((kg/m^2)^x/s)$ . Acceptable range: $10^{-50} \le A1OX \le 10^{50}$ . Default value: none.
W-2 (R) :	B1OX	Second coefficient in the low temperature kinetics equation, $B_1$ , (K). Acceptable range: $0.0 \le B1OX \le 10^{10}$ . Default value: none.
W-3 (R) :	T1OX	Upper temperature limit to apply the low temperature kinetics equation, $T_1$ (K). Acceptable range: $273.0 \le T1OX \le 10,000$ Default value: 9999.0
W-4 (R) :	A2OX	First coefficient in the high temperature kinetics equation, $A_2$ , $((kg/m^2)^x/s)$ . Acceptable range: $0.0 \le A2OX \le 10^{50}$ . Default value: $0.0$
W-5 (R) :	B2OX	Second coefficient in the high temperature kinetics equation, $B_2$ , (K). Acceptable range: $0.0 \le B2OX \le 10^{10}$ . Default value: $0.0$
W-6 (R) :	T2OX	Lower temperature limit to apply the high temperature kinetics equation, $T_2$ (K). Acceptable range: T1OX + 1.0 $\leq$ T2OX $\leq$ 10,000 Default value: 10,000.0
W-7 (R) :	TMINOX	Minimum temperature for oxidation, $T_{\min}$ , (K). Oxidation rate is set to zero for $T < T_{\min}$ . A linear interpolation from zero to a full value is performed between $T_{\min}$ and $T_{\min}$ +10.0 K.

Acceptable range: $273.0 \le \text{TMINOX} \le 1000.0.$ Default value:600.0.

W-8 (R): TMAXOX Maximum temperature for oxidation,  $T_{max}$ , (K). For temperatures higher than  $T_{max}$ , the oxidation rate is calculated using  $T=T_{max}$ . Acceptable range:  $2000.0 \le \text{TMAXOX} \le 10,000.0$ . Default value: 10,000.0.

#### Post-breakaway reaction

The following input defines additional reaction coefficients for a post-breakaway reaction. The breakaway reaction is observed in case of air oxidation of Zircaloy, for example in case of loss of water in Spent Fuel Pool. In absence of other factors,  $C_T$ ,  $K_\nu$ ,  $K_p$ , M(B,...), the reaction rate is calculated from:

$$\frac{dm^{y}}{dt} = K_{T}(T)$$

$$K_T(T) = \begin{cases} A_3 \exp\left[-B_3/T\right] & for: T < T_3 \\ A_4 \exp\left[-B_4/T\right] & for: T > T_4 \end{cases}$$

- YOX W-9 (R): Exponent in the reaction rate, *y*, applied in the post-breakaway regime. Acceptable range:  $0.1 \le \text{YOX} \le 10.0$ . Default value: none W-10(R): A3OX First coefficient in the low temperature post-breakaway kinetics equation,  $A_3$ ,  $((kg/m^2)^x/s)$ . Acceptable range:  $0.0 \le A3OX \le 10^{50}$ . Default value: 0.0 W-11 (R): B3OX Second coefficient in the low temperature post-breakaway kinetics equation,  $B_3$ , (K). Acceptable range:  $0.0 \le B1OX \le 10^{10}$ . Default value: 0.0 W-12 (R): T3OX Upper temperature limit to apply the low temperature kinetics equation,  $T_{3}(K)$ . Acceptable range:  $273.0 \le T3OX \le 10,000$ Default value: 9999.0
- W-13 (R):A4OXFirst coefficient in the high temperature post-breakaway kinetics<br/>equation,  $A_4$ ,  $((kg/m^2)^y/s)$ .<br/>Acceptable range:  $0.0 \le A4OX \le 10^{50}$ .<br/>Default value: 0.0

W-14 (R) :	B4OX	Second coefficient in the high temperature post-breakaway kinetics equation, $B_4$ , (K).Acceptable range: $0.0 \le B4OX \le 10^{10}$ .Default value: $0.0$
W-15 (R) :	T4OX	Lower temperature limit to apply the high temperature kinetics equation, $T_4$ (K).
		Acceptable range: $T3OX + 1.0 \le T4OX \le 10,000$
		Default value: 10,000.0

The point of breakaway is calculated in one of two ways, using a critical time to breakaway or a critical oxidation depth at breakaway, both temperature-dependent.

 Option 1: critical time to breakaway: A time to breakaway function is tabulated versus temperature, τ(*T*). For a transient conditions a cumulative damage approach is used:

$$CD = \int_{0}^{t} \frac{dt'}{\tau(T)}$$

Breakaway occurs when CD = 1.0. For CD < 1.0 pre-breakaway reaction coefficients are used. For CD > 1.0 + BINTOX (default=0.5), post-breakaway reaction coefficients are used. For 1.0 < CD < 1.0 + BINTOX, a linear interpolation is performed between the pre- and the post-breakaway reaction kinetics.

• Option 2: critical oxidation depth at breakaway: A critical oxidation depth at breakaway is tabulated versus temperature,  $\delta_1(T)$ . This is the upper limit of the pre-breakaway reaction. For  $\delta < \delta_1(T)$  pre-breakaway reaction coefficients are used. For  $\delta > \delta_1(T) \times (1.0 + \text{BINTOX})$ , post-breakaway reaction coefficients are used. For  $\delta_1(T) < \delta < \delta_1(T) \times (1.0 + \text{BINTOX})$ , a linear interpolation is performed between the pre- and the post-breakaway reaction kinetics.

W-16 (I) :	I1OX	Pointer to a Tabul tabulated versus function, $\delta_1(T)$ (m)	ar Function defining time to breakaway function is temperature, $\tau(T)$ or the critical oxidation depth .
		Data is interpreted	as $\tau(T)$ if all tabulated points are within the range 0.0
		$\div$ 1.0. An error met condition.	ssage is issued if not all values of the table fulfill this
		Data is interpreted	as $\delta_1(T)$ if all tabulated points are within the range
		$100 \div 10^{20}$ . An erro	or message is issued if not all values of the table fulfill
		this condition.	
		Acceptable range:	reference to a Tabular Function. If the catalyst model is present (ICATOX>0), then the Option 1, cumulative damage function, should be used.
		Default value:	none.

W-17 (R) :	BINTOX	Interpolation zone for breakaway reaction. Interpolation between pre- breakaway and post-breakaway reaction is performed in the range: Option 1 (cumulative damage) $1.0 < CD < 1.0 + BINTOX$ Option 2 (critical depth): $\delta_1(T) < \delta < \delta_1(T) \times (1.0 + BINTOX)$ Acceptable range: $0.1 \le BINTOX \le 10.0$ Default value: $0.5$
W-18 (I) :	ICATOX	Indicator for catalyst needed for breakaway. =0: no catalyst is needed > 0: catalyst is needed for breakaway. The catalyst is a gas number ICATOX. The critical time to breakaway (cumulative damage) is calculated only if the concentration of the gas ICATOX exceeds the minimum limit of XCATOX.
		Acceptable range:0 or a gas numberDefault value:0
W-19 (R) :	XCATOX	Minimum concentration of catalyst gas needed for breakaway (used if ICATOX>0). Breakaway will only be possible when the volume fraction of gas ICATOX exceeds the value of XCATOX. Acceptable range: $0.0 \le \text{XCATOX} \le 1.0$ Default value: $0.0$

## 2.14.4 Records: 8511XX, Corrector for Temperature-Dependent Reaction Rate

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

The corrector to the temperature-dependent oxidation rate is assumed to have the following general form:

$$C_T(T, p_i) = \frac{1}{1 + A_C \exp[B_C / T] \cdot p_1^{X_1} \cdot p_2^{X_2} \cdot p_3^{X_3}}$$

$C_T$	со	rrection to the temperature-dependent reaction rate, (-),
$A_C$	fir	st coefficient, (-),
$B_C$	sec	cond coefficient, (K),
$p_1$	pa	rtial pressure of the gas $Gs_1$ (oxidizing gas), (Pa),
$p_2$	pa	rtial pressure of the gas Gs <sub>2</sub> (first reaction product), (Pa),
$p_3$	pa	rtial pressure of the gas Gs <sub>3</sub> (second reaction product), (Pa),
$X_1$	ex	ponent for the gas $Gs_1$
$X_2$	ex	ponent for the gas $Gs_2$
$X_3$	ex	ponent for the gas $Gs_3$
W-1 (R):	ACOX	First coefficient, $A_C$ , (-).
		Acceptable range: $0.0 \le AC3OX \le 10^{50}$
		Default value: 0.0
W-2 (R) :	BCOX	Second coefficient, $B_C$ , (K).
		Acceptable range: $-10.0 \le BCOX \le 10^{10}$

		Default value:	0.0
W-3 (R) :	X1OX	First exponent, X <sub>1</sub> , Acceptable range: Default value:	(-). $-10.0 \le X1OX \le 10.0$ 0.0
W-4 (R) :	X2OX	Second exponent, 2 Acceptable range: Default value:	$X_2$ , (-). -10.0 $\leq$ X2OX $\leq$ 10.0 0.0
W-5 (R) :	X3OX	Second exponent, 2 Acceptable range: Default value:	$X_{3}$ , (-). -10.0 $\leq$ X3OX $\leq$ 10.0 0.0

# 2.14.5 Records: 8520XX, Velocity-Dependent Reaction Rate

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

The velocity-dependent reaction rate is defined by:

$$K_{v}(v,T) = C \cdot v^{D} \cdot T^{E}$$

K <sub>v</sub> v T C D E	velo gas temj coef first seco	wity-dependent term, $((kg/m^2)^x/s)$ , velocity, (m/s) perature, (K) ficient determining the reaction rate, ( $kg^x m^{-2x-D} s^{-1+D} K^E$ ) exponent, (-) ond exponent, (-)
W-1 (R) :	CKVOX	Coefficient, <i>C</i> , $(kg^{x} m^{-2x-D} s^{-1+D} K^{E})$ . If the value is zero or not entered, then the velocity-dependent term is not used. <i>Acceptable range:</i> $0.0 \le CKVOX \le 10^{10}$ . <i>Default value:</i> none.
W-2 (R) :	DKVOX	First exponent in the velocity-dependent term, $D$ , (-).Acceptable range: $0.0 \le DKVOX \le 10.0.$ Default value:none.
W-3 (R) :	EKVOX	Second exponent in the velocity-dependent term, $E$ , (-).Acceptable range: $0.0 \le \text{EKVOX} \le 10.0.$ Default value:none.
W-4 (R) :	VMINOX	Minimum velocity, $v_{\min}$ , (m/s). For velocities lower than $v_{\min}$ the oxidation rate is calculated using $v=v_{\min}$ . Acceptable range: $0.001 \le \text{VMINOX} \le 999.0$ Default value: 0.01.

W-5 (R): VMAXOX Maximum velocity,  $v_{max}$ , (m/s). For velocities higher than  $v_{max}$  the oxidation rate is calculated using  $v=v_{max}$ . Acceptable range: VMINOX+1.0  $\leq$  VMAXOX  $\leq$  1000.0. Default value: 1000.0.

### 2.14.6 Records: 8530XX, Pressure-Dependent Reaction Rate

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

The pressure-dependent coefficient is defined by:

$$K_p(p) = \left(\frac{p}{p_{ref}}\right)^F$$

p Pref F	parti refer expo	al pressure of the oxidizing gas ( $Gs_1$ - see section 2.14.1), (Pa) ence pressure, (Pa) nent, (-)
W-1 (R) :	FKPOX	Exponent, <i>F</i> , (-).If the value is zero or not entered, then the pressure- dependent term is not used. <i>Acceptable range:</i> $0.0 \le \text{FKPOX} \le 10.0$ . <i>Default value:</i> none.
W-2 (R) :	PREFOX	Reference pressure, $p_{ref}$ , (Pa).Acceptable range: $1.0 \le PREFOX \le 1.0 \times 10^7$ .Default value: $1.0$
W-3 (R) :	PMINOX	Minimum pressure, $p_{\min}$ , (Pa). Oxidation rate is set to zero for $p < p_{\min}$ . A linear interpolation from zero to a full value is performed between $p_{\min}$ and $p_{\min} \times 2.0$ . Acceptable range: $1.0 \le \text{PMINOX} \le 1.0 \times 10^3$ . Default value: 1.0.
W-4 (R) :	PMAXOX	Maximum pressure, $p_{\text{max}}$ , (Pa). For pressures higher than $p_{\text{max}}$ the oxidation rate is calculated using $p=p_{\text{max}}$ . Acceptable range: $1.0 \times 10^4 \le \text{PMAXOX} \le 1.0 \times 10^7$ . Default value: $1.0 \times 10^7$ .

#### 2.14.7 Records: 8540XX, Burn-off Factor

XX is the number of the user-defined oxidation model. The maximum number of user-defined oxidation models is 10. The oxidation models must be numbered consecutively, XX=01, 02, 03, ...

W-1 (I): IBOFOX Pointer to a Tabular or Control Function that defines the burn-off factor, M(B,...).

	$001 \le \text{IBOFOX} \le$ with the reference r the depth of oxidize $001 \le -\text{IBOFOX} \le$ with the reference Tabular or Contro BMINOX, BMAX IBOFOX = 1001 correlation, defined be restricted to the P Acceptable range: Default value:	999: $M(B,)$ will be defined by a Tabular Function number: IBOFOX. The argument to this TF is always ed material: $M(B,) = \text{TF}(d_{ox})$ . (999: $M(B,)$ will be defined by a Control Function e number:  IBOFOX . The value obtained from 1 Function will be restricted to the limit given by OX, defined below. : $M(B,)$ will be calculated from the built-in below. The value obtained from the correlation will limit given by BMINOX, BMAXOX, defined below. must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-2 (R) : BMINOX	Minimum value of Acceptable range: Default value:	M(B,). $10^{-10} \le BMINOX \le 2.0$ $10^{-2}$
W-3 (R) : BMAXOX	Maximum value of Acceptable range: Default value:	M(B,). BMINOX $\leq$ BMAXOX $\leq 10^{10}$ $10^{+2}$

## Built-in correlation

The built-in correlation, developed within the ARCHER project, has the following form (see Volume 3, 3.11.9, Graphite Oxidation by Steam - Validation Calculations):

$$M(B,P) = f_B(B) \cdot [f_{P,\infty}(P) - f_{P,0}(P)] + f_{P,0}(P)$$

where:

$$f_B(B) = \begin{cases} 1 - \left(\frac{B}{B_{\infty}} - 1\right)^2 & \text{if } B < B_{\infty} \\ 1 & \text{if } B > B_{\infty} \end{cases}$$
$$f_{P,0}(P) = A_0 \cdot \exp(B_0 P)$$
$$f_{P,\infty}(P) = A_1 \cdot \exp(B_1 P)$$

 $B_{\infty} = 0.3 \times 10^{-3}$  m. The pressure range for the correlations is limited to  $P < 55 \times 10^{5}$  Pa.

W-4 (R) :	A0FPOX	Coefficient $A_0$ in the built-in correlation for burn-off factor.Acceptable range: $10^{-3} \le A0FPOX \le 10^3$ Default value: $0.35$
W-5 (R) :	B0FPOX	Coefficient $B_0$ in the built-in correlation for burn-off factor. Acceptable range: $-10^{-6} \le B0FPOX \le 10^{-6}$ Default value: $-7.0 \times 10^{-8}$
W-6 (R) :	A1FPOX	Coefficient $A_1$ in the built-in correlation for burn-off factor. Acceptable range: $10^{-3} \le A1FPOX \le 10^3$ Default value: 1.7

W-7 (R) :	B1FPOX	Coefficient $B_1$ in th Acceptable range: Default value:	e built-in correlation for burn-off factor. $-10^{-6} \le B1FPOX \le 10^{-6}$ $-1.8 \times 10^{-7}$
W-8 (R) :	BINFOX	Coefficient $B_{\infty}$ in the <i>Acceptable range: Default value:</i>	the built-in correlation for burn-off factor. $10^{-6} \le \text{BINFOX} \le 10^{-2}$ $0.3 \times 10^{-3}$
W-9 (R) :	PMNBOX	Minimum pressure Acceptable range: Default value:	to be applied in the correlation for $f_{P,0}$ and $f_{P,\infty}$ . $0.0 \le \text{PMNBOX} \le 10^{10}$ 0.0  Pa
W-10 (R) :	PMXBOX	Maximum pressure Acceptable range: Default value:	to be applied in the correlation for $f_{P,0}$ and $f_{P,\infty}$ . $0.0 \le \text{PMXBOX} \le 10^{10}$ $5.5 \times 10^6 \text{ Pa}$

#### 2.14.8 Records: 855000, Options for Insufficient Oxidant

In case there is not enough oxidant available for the reaction, the oxidation reaction rate is decreased. This decrease is referred to here as the oxidant starvation limit. The parameters determining how the reaction rate decreases with decreasing oxidant fraction are defined in this record.

W-1 (R) :	C1OX	Critical concentration, $c_1$ . If the concentration (volume fraction) of the oxidizing gas is above this limit, there is no restriction for oxidation rate and the reaction proceeds according to the defined reaction kinetics. If the concentration is below $c_1$ , the reaction rate is interpolated to reach zero at the concentration value of $c_0$ . The value of $c_0$ is constant and set to $c_0 = 0.1 \times c_1$ . Figure 2-66 illustrates the interpolation and the values of $c_0$ and $c_1$ . Acceptable range: $10^{-6} \le C1OX \le 10^{-2}$ Default value: $10^{-4}$
W-2 (I) :	INTPOX	Type of interpolation. = 1: linear interpolation: $x_1 = (c - c_0) / (c_1 - c_0)$ = 2: third order interpolation: $x_2 = (3 - 2x_1) x_1^2$ = 3: sixth order interpolation: $x_3 = x_2^2 = ((3 - 2x_1) x_1^2)^2$ The three interpolation types are shown in Figure 2-66. The interpolation is important in case of very intensive oxidation, when the oxidizing gas is consumed as soon as it enters the Control Volume. This may lead to numerical instabilities and time step reductions. Test calculations showed that the best results are obtained with sixth order interpolation. Therefore this option is set as default. <i>Acceptable range:</i> 1, 2, 3 <i>Default value:</i> 3



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Figure 2-66 Interpolation performed in case of oxidant starvation

# 2.14.9 Built-in Oxidation Models

Data for three steam oxidation reactions is built into the code, as the reactions number -01, -02, and -03. These are:

- -01 Zr oxidation by steam, Cathcart + Urbanic-Heidrich model.
- -02 Zr oxidation by steam, Urbanic-Heidrich model.
- -03 Steel oxidation by steam, White model.

The data for these reactions is shown in Table 2-38.

Data for two  $O_2$  oxidation reactions is built into the code, as the reactions number -04 and -05. These are:

- -04 Zr oxidation by O<sub>2</sub>, Benjamin et al. model.
- -05 Graphite oxidation by  $O_2$ , Roes model.

The data for these reactions is shown in Table 2-39.

	Reaction				
	$Zr+2H_2O \rightarrow ZrO_2+2H_2$ ,	$Zr+2H_2O \rightarrow ZrO_2+2H_2$ ,	$Fe+H_2O\rightarrow FeO+H_2$ ,		
Coefficient	Cathcart (low T),	Urbanic-Hedrich	$2Cr+3H_2O\rightarrow Cr_2O_3+3H_2$ ,		
	Urbanic-Hedrich (high T)		White		
$n_1$	2.0	2.0	1.1		
<i>n</i> <sub>2</sub>	2.0	2.0	1.1		
x	2.0	2.0	2.0		
$Q_{ox}$	$6.45 \times 10^{6}$	$6.45 \times 10^{6}$	$0.477 \times 10^{6}$		
$\sigma_{ox}$	1.5	1.5	3.92		
$ ho_{ox}$	$\rho(Zr) = 6490.0$	$\rho(Zr) = 6490.0$	$\rho(Fe) = 8020.0$		
Mox	M(Zr) = 91.22	M(Zr) = 91.22	M(St) = 51.70		
$A_1$	$2 \times 16.8 \times (M_{Zr}/M_{O2})^2 = 273.0$	29.6	2.51×10 <sup>9</sup>		
$B_1$	20,060.0	16,820.0	42,428.0		
$T_1$	1783.0	1783.0	full temperature range		
$A_2$	$2 \times 5.41 \times (M_{Zr}/M_{O2})^2 = 87.9$	87.9	-		
$B_2$	16,610.0	16,610.0			
$T_2$	1853.0	1853.0			
С	0.0	0.0	0.0		
D	-	-	-		
Ε	-	-	-		
F	0.0	0.0	0.0		
$p_{\it ref}$	-	-	-		
Tmin / Tmax	600.0 / 10,000.0	600.0 / 10,000.0	600.0 / 10,000.0		

T-1-1- 0.00	D: 14 1.4			data fan		and deathers.
1 able 2-38	Buiit-in	oxidation	reaction	data for	steam	oxidation.

Table 2-39 Built-in oxidation reaction data for oxidation by  $O_{2}$ .

	Reaction				
Coefficient	$Zr+O_2 \rightarrow ZrO_2$ ,	C+O₂→CO₂,			
	Benjamin et al.	Roes			
$n_1$	1.0	1.0			
$n_2$	0.0	1.0			
x	2.0	1.0			
$Q_{ox}$	$12.1 \times 10^{6}$	$32.8 \times 10^{6}$			
$\sigma_{ox}$	1.5	0.01			
$\rho_{ox}$	$\rho(Zr) = 6490.0$	$\rho(C) = 2250.0$			
Mox	M(Zr) = 91.22	M(C) = 12.01			
$A_1$	50.4	7.5×10 <sup>3</sup>			
$B_1$	14,630.0	16,140.0			
$T_1$	full temperature range	full temperature range			
$A_2$	-	-			
$B_2$					
$T_2$					
С	0.0	8.03×10 <sup>-4</sup>			
D	-	0.65			
Ε	-	0.34			
F	0.0	1.0			
$p_{\it ref}$	-	1.0×10 <sup>5</sup>			
Tmin / Tmax	600.0 / 10,000.0	600.0 / 10,000.0			
vmin / vmax	-	0.01 / 1000.0			
p <sub>min</sub> / p <sub>max</sub>	-	$1.0 \times 10^1 / 1.0 \times 10^7$			

#### 2.14.10 Examples of the User-Defined Oxidation Models

The inputs shown below define four oxidation models. The first model is exactly the same as the builtin Cathcart model for the <u>steam-Zr oxidation</u>, i.e. the reaction:

$$Zr + 2H_2O \rightarrow ZrO_2 + 2H_2$$

O05001 Steam-Zr Reaction, Cathcart Model \* Gs1 Gs2 n1 n2 x Q V RHO MW 850001 3 1 2.0 2.0 2.0 6.45E6 1.5 6490.0 91.22 \* \* T coefficients: \* A1 B1 T1 A2 B2 T2 T-min T-max 851001 273.0 20060.0 1783.0 87.9 16610.0 1853.0 600.0 10000.0

The second model defines chromium oxidation by steam:

or:

$$2Cr+3H_2O \rightarrow Cr_2O_3+3H_2$$

$$Cr + 1.5H_2O \rightarrow 0.5Cr_2O_3 + 1.5H_2$$

using only one (lower) set of coefficients. The reaction kinetics coefficients and the reaction heat are taken from reference [35].

O05002 Steam-Cr Reaction \* Gs1 Gs2 n1 n2 x Q V RHO MW 850002 3 1 1.5 1.5 2.0 2.442E6 1.5 2000.0 26.98 \* \* T coefficients: \* A1 B1 T1 A2 B2 T2 T-min T-max 851002 2.42E9 42400.0 9998.0 1.0 1.0 9999.0 600.0 10000.0

The third model defines steel oxidation by  $O_2$ . It is assumed that only Fe is oxidized, therefore the reaction considered is:

$$Fe + \frac{1}{2}O_2 \rightarrow FeO$$

The reaction kinetics is based on data from Nanni et al. [37]. The data is correlated by:

$$\frac{dm^2}{dt} = K_T(T) = 2.34 \times 10^{10} \exp\left[-45,350.0/T\right]$$

The reaction heat,  $4.9 \times 10^6$  (W/kg), is obtained from [39]. Other parameters are assumed to be the same as for steam oxidation. Listing of the oxidation model is shown below (listing of a full input deck for a test case involving this oxidation reaction is shown in Volume 3).

O05003 Steel-Oxygen reaction, Nanni et al. data \* Gs1 Gs2 n1 n2 x Q V RHO MW 850003 5 1 0.5 0.0 2.0 4.9E6 3.92 8020.0 51.7 \* \* T coefficients: \* A1 B1 T1 A2 B2 T2 T-min T-max 851003 2.34E10 45350.0 9998.0 1.0 1.0 9999.0 600.0 10000.0 The fourth model is exactly the same as the built-in model for the graphite oxidation by O<sub>2</sub>, i.e.:

```
C + O_2 \rightarrow CO_2
```

```
O05004 Graphite-Oxygen reaction, Roes Model

* Gsl Gs2 nl n2 x Q V RHO MW

850004 5 6 1.0 1.0 1.0 32.8E6 0.01 2250.0 12.01

*

* T coefficients:

* Al Bl Tl A2 B2 T2 T-min T-max

851004 7.5E3 16140.0 9998.0 1.0 1.0 9999.0 600.0 10000.0

*

* v coefficients:

* C D E v-min v-max

852004 8.03E-4 0.65 0.34 0.01 1000.0

*

* p-coefficients

* F p-ref p-min p-max

853004 1.0 1.0E5 1.0 1.0E+7
```

The fifth model defines graphite oxidation by steam. The reaction is:

$$C + H_2O \rightarrow H_2 + CO$$

The reaction kinetics is defined following by Kubaschewski-Heinrich [38]:

$$\frac{dm}{dt} = \frac{6.4 \cdot 10^{11} \cdot \exp\left[-\frac{256,000}{8.315 \cdot T}\right] \cdot p_{H20}^{0.44}}{1 + 7.5 \cdot 10^{-5} \cdot \exp\left[\frac{121,000}{8.315 \cdot T}\right] \cdot p_{H2}^{0.9} \cdot p_{H20}^{-0.4}}$$

Here pressure is in (bar), and reaction rate in (mg/cm<sup>2</sup>-hr). First, the formula is converted to SI units:

$$\frac{dm}{dt} = \frac{1.78 \cdot 10^{6} \cdot \exp\left[-\frac{256,000}{8.315 \cdot T}\right] \cdot \left(\frac{p_{H20}}{10^{5}}\right)^{0.44}}{1 + 7.5 \cdot 10^{-5} \cdot \exp\left[\frac{121,000}{8.315 \cdot T}\right] \cdot \left(\frac{p_{H2}}{10^{5}}\right)^{0.9} \cdot \left(\frac{p_{H20}}{10^{5}}\right)^{-0.4}}$$

Here pressure is in (Pa), reaction rate in (kg/m<sup>2</sup>-s) and temperature in (K). Furthermore, the formula is rearranged as follows:

$$\frac{dm}{dt} = \frac{1.12 \cdot 10^4 \cdot \exp\left[-\frac{30788}{T}\right] \cdot (p_{H2O})^{0.44}}{1 + 2.37 \cdot 10^{-7} \cdot \exp\left[\frac{14552}{T}\right] \cdot (p_{H2})^{0.9} \cdot (p_{H2O})^{-0.4}}$$

The reaction rate is defined using the temperature-dependent factor  $K_T(T)$ , the correction to the temperature-dependent factor  $C_T(T,p_i)$ , and the pressure-dependent factor,  $K_p(p_1)$ :

$$\frac{dm}{dt} = K_T(T) \cdot C_T(T, p_i) \cdot K_p(p_{H2O})$$

• Temperature-dependent factor,  $K_T(T)$ :

$$K_T = 1.12 \cdot 10^4 \cdot \exp\left[-\frac{30788}{T}\right]$$

• Correction to temperature-dependent factor,  $C_T(T, p_i)$ :

$$C_{T} = \frac{1}{1 + 2.37 \cdot 10^{-7} \cdot \exp\left[\frac{14552}{T}\right] \cdot (p_{H2})^{0.9} \cdot (p_{H2O})^{-0.4}}$$

а

• Pressure-dependent factor,  $K_p(p_i)$ 

$$K_p = \left(p_{H2O}\right)^{0.44}$$

The reaction heat,  $131.3 \text{ kJ/mol} = 131.3 \times 10^6 \text{ (J/kmol)} = 10.9 \times 10^6 \text{ (J/kg_C)}$ . Input defining this reaction is shown below.

```
O05005 Graphite-steam reaction, Kubaschewski-Heinrich

* Gsl Gs2 nl n2 x Q V RHO MW XW Gs3 n3

850005 3 l 1.0 l.0 l.0 l0.9E6 0.01 2250.0 l2.0l 0 7 l.0

* K-T coefficients:

* Al Bl Tl A2 B2 T2 T-min T-max

851005 l.12E+4 30788.0 9998.0 l.0 l.0 9999.0 600.0 l0000.0

*

* C-T coefficients:

* A3 B3 X1 X2 X3

851105 2.37E-7 l4552.0 -0.4 0.9 0.0

*

* K-p coefficients

* F p-ref p-min p-max

853005 0.44 0.0 l.0 l.0E+7
```

The sixth model defines graphite oxidation by steam using the correlation of Kubaschewski-Heinrich and the best estimate multiplier  $M_{BE}(B,P)$ , described in detail in Volume 3. The correlation of Kubaschewski-Heinrich is already shown above. Here the multiplier is shown. The simplest way to activate the best estimate multiplier is to use default values of Words 4 through 10 on record 8540XX. Below an alternative way is shown, where the multiplier is defined as a general 2-D Tabular Function. The applied function will give the same results as setting IBOFOX=1001 in the record 8540XX. The tabulated data is shown below.

	B [m]:	0.00E+00	6.00E-05	1.20E-04	1.80E-04	2.40E-04	3.00E-04
	B/B∞ [-]:	0.00	0.20	0.40	0.60	0.80	1.00
	f(B/B∞) [-]:	0.00	0.36	0.64	0.84	0.96	1.00
P [Pa]	1.00E+05	0.35	0.82	1.19	1.46	1.62	1.67
	5.00E+05	0.34	0.78	1.12	1.36	1.51	1.55
	1.00E+06	0.33	0.72	1.03	1.24	1.38	1.42
	1.50E+06	0.32	0.67	0.94	1.14	1.26	1.30
	2.00E+06	0.30	0.62	0.87	1.04	1.15	1.19
	2.50E+06	0.29	0.58	0.80	0.96	1.05	1.08
	3.00E+06	0.28	0.54	0.74	0.88	0.96	0.99
	3.50E+06	0.27	0.50	0.68	0.80	0.88	0.91
	4.00E+06	0.26	0.47	0.62	0.74	0.80	0.83
	4.50E+06	0.26	0.44	0.58	0.68	0.74	0.76
	5.00E+06	0.25	0.41	0.53	0.62	0.67	0.69
	5.50E+06	0.24	0.38	0.49	0.57	0.62	0.63

Best estimate multiplier  $M_{BE}(B,P)$  (see Volume 3)

#### The input deck defining this 2-D table is:

705901	M(B,P) Be	est Estimate	
*	Group Numb	oer Fac	ct. Const.
700901	1 5	, 1.	0 0.0 * Type : General TF
*	yl y	<sup>7</sup> 2 y3	у4 у5 уб
708901	0.0E+00 6.0	)E-5 1.2E-4	1.8E-4 2.4E-4 3.0-4 * y-coordinate data points (B)
*	Arguments		
* Point	ters: (1) (2)	(3) (4) Fact	Const.
710901	1 102	2 13 1 1.0	0.0 * x-argument: CV-102, total pressure
710901	6 901	. 1 0 1.0	0.0 * uses TF-901 for $y = y1$ (B = 0.0E+0)
710901	6 902	2 1 0 1.0	0.0 * uses TF-902 for $y = y2$ (B = 6.0E-5)
710901	6 903	1 0 1.0	0.0 * uses TF-903 for $y = y3$ (B = 1.2E-4)
710901	6 904	1 0 1.0	0.0 * uses TF-904 for $y = y4$ (B = 1.8E-4)
710901	6 905	1 0 1.0	0.0 * uses TF-905 for $y = y5$ (B = 2.4E-4)
710901	6 906	5 1 0 1.0	0.0 * uses TF-906 for $y = y6$ (B = 3.0E-4)
710901	3 102	30 1 -1.0	0.001 * y-argument: SC-102, oxidized depth
*			
*			
605901	f(P) for	B = 0.0	
*	P (Pa)	f(P)	
600901	1.00E+05	0.35	
600901	5.00E+05	0.34	
600901	1.00E+06	0.33	
600901	1.50E+06	0.32	
600901	2.00E+06	0.30	
600901	2.50E+06	0.29	
600901	3.00E+06	0.28	
600901	3.50E+06	0.27	
600901	4.00E+06	0.26	
600901	4.50E+06	0.26	
600901	5.00E+06	0.25	
600901 *	5.50E+06	0.24	
 605902	f(P) for	B = 6.0E-5)	
*	P (Pa)	f(P)	
600902	1.00E+05	0.82	
600902	5.00E+05	0.78	

600902 600902 600902 600902 600902 600902 600902 600902 600902 600902	1.00E+06 1.50E+06 2.00E+06 3.00E+06 3.50E+06 4.00E+06 4.50E+06 5.00E+06 5.50E+06	0.72 0.67 0.52 0.58 0.54 0.50 0.47 0.44 0.41 0.38
* 605903 * 600903 600903 600903 600903 600903 600903 600903 600903 600903 600903 600903 600903 600903 *	f(P) for P (Pa) 1.00E+05 5.00E+05 1.00E+06 2.00E+06 2.50E+06 3.00E+06 3.50E+06 4.00E+06 5.00E+06 5.50E+06	B = 1.2E-4 f(P) 1.19 1.12 1.03 0.94 0.87 0.80 0.74 0.68 0.62 0.58 0.53 0.49
605904 * 600904 600904 600904 600904 600904 600904 600904 600904 600904 600904 600904 600904	f(P) for P (Pa) 1.00E+05 5.00E+05 1.00E+06 2.00E+06 2.50E+06 3.00E+06 3.50E+06 4.00E+06 5.00E+06 5.50E+06	B = 1.8E-4 f(P) 1.46 1.36 1.24 1.14 0.96 0.88 0.80 0.74 0.68 0.62 0.57
^ 605905 * 600905 600905 600905 600905 600905 600905 600905 600905 600905 600905 600905 600905 600905 600905	f(P) for P (Pa) 1.00E+05 5.00E+05 1.00E+06 2.00E+06 2.50E+06 3.00E+06 3.50E+06 4.00E+06 5.00E+06 5.50E+06	B = 2.4E-4 f(P) 1.62 1.51 1.38 1.26 1.15 1.05 0.96 0.88 0.80 0.74 0.67 0.62
<pre>605906 * 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 600906 *</pre>	f(P) for P (Pa) 1.00E+05 5.00E+05 1.00E+06 2.00E+06 2.50E+06 3.00E+06 3.50E+06 4.00E+06 5.00E+06 5.50E+06	B = 3.0E-4 f(P) 1.67 1.55 1.42 1.30 1.19 1.08 0.99 0.91 0.83 0.76 0.69 0.63
## 2.15 Radioactive Particle Transport Data

## 2.15.1 Record: 860000, RT Package Global Activators, Main Aerosol Data

W-1 (I) :	MGACRT	<ul> <li>Global activator of the Radioactive Particle Transport (RT) Package.</li> <li>=0: the RT calculations are by default inactive in all Control Volumes, Junctions, 1-D Solid Heat Conductors, and 2-D Solid Heat Conductors. Individual Control Volumes, Junctions and Heat Conductors can be included in the RT calculations, using the records 170XXX, 270XXX, 370XXX, 470XXX.</li> <li>=1: the RT calculations are by default active in all Control Volumes, Junctions, 1-D Solid Heat Conductors, and 2-D Solid Heat Conductors. Individual Control Volumes, Junctions and Heat Conductors can be excluded from the RT calculations, using the records 170XXX, 270XXX, 270XXX, 370XXX, 470XXX.</li> <li>=2: the RT calculations are by default active in all Control Volumes and Junctions.</li> <li>=3: the RT calculations are by default active in all Control Volumes. <i>Acceptable range:</i> 0, 1, 2, 3.</li> </ul>
W-2 (I) :	IJNART	Global activator of the Solid Heat Conductors (SC/TC) and JN associations (for details see records 371XXX, 471XXX). =-1: The global activator is off. The associations may be specified individually for each SC and TC in the records 371XXX, 471XXX. = 1: Each boundary surface of a SC and TC is associated with this junction connected to the boundary Control Volume, which has the largest flow area. These associations may be changed individually for each SC and TC in the records 371XXX, 471XXX. = 2: Each boundary surface of a SC and TC is associated with this junction connected to the boundary Control Volume, which has the smallest flow area. These associations may be changed individually for each SC and TC in the records 371XXX, 471XXX. = 11 or 12: Same as 1 and 2 above, but additionally the junction area reduction calculation is automatically activated for all junctions. The default width is equal to the square root of the junction flow area, and may be redefined using the records 371XXX, 471XXX. <i>Acceptable range:</i> -1, 1, 2, 11, 12. <i>Default value:</i> -1.
W-3 (I) :	IGRVRT	Global selection of the gravity factors GRV1RT, GRV2RT. =-1: the global activator is off. All gravity factors are equal to zero, unless specified otherwise in the records 372XXX, 472XXX. Setting IGRVRT to -1 is an easy way to globally deactivate the gravitational deposition on all surfaces. =+1: Rectangular geometry: the default value of the gravity factors is: +1 for horizontal, up-facing surfaces, -1 for horizontal, down-facing surfaces, and 0.0 for vertical surfaces. Cylindrical and spherical geometry: one half of the theoretical value for the upper half of a

	د 2 1 5 5 5 5 6 6	cylinder or sphere (see discussion of GRV1RT, GRV2RT in sections 2.15.14, 2.15.15). The values are: norizontal cylinders: $1/\pi = 0.3183$ . spheres: $\pi/8 = 0.3927$ . =+2: Rectangular geometry: as above, i.e. +1 for horizontal, up-facing surfaces, -1 for horizontal, down-facing surfaces, and 0.0 for vertical surfaces. Cylindrical and spherical geometry: zero (therefore there is no gravitational deposition on these surfaces). The gravity factors are entered individually for each SC and TC in the records 372XXX,
	2 F 1	472XXX. Acceptable range: 1, 2. Default value: 1.
W-4 (R) : D	DENART I	Density of aerosol particles, $\rho_p$ , (kg/m <sup>3</sup> ). Acceptable range: $0.01 \le \text{DENART} \le 22,600.0$ (density of iridium) Default value: 1000.0.
W-5 (R) : T	CONRT 7	Thermal conductivity of aerosol particles, $k_p$ , (W/m/K). Acceptable range: $0.01 \le \text{TCONRT} \le 500.0$ . Default value: 10.0.
W-6 (R) : P	ORSRT I	Porosity of the deposited layer, $\varepsilon_{dep}$ , (-). The thickness, $t_{dep}$ , and the effective thermal conductivity of the deposited aerosol layer, $k_{dep}$ are calculated as: $\frac{m_{dep}}{m_{dep}} = k_{ee} \cdot (1 - \varepsilon_{ee})$
	° dep	$A\rho_{dep}(1-\varepsilon_{dep}) \qquad \qquad$
	2   	where $m_{dep}$ is the deposited mass (kg) and <i>A</i> is the deposition area (m <sup>2</sup> ). Acceptable range: $0.0 \le \text{PORSRT} \le 0.9$ . Default value: 0.5.
W-7 (R) : F	JNMRT M ( r	Minimum area fraction for junctions blocked by the deposited aerosols (see records 370XXX, 470XXX), (-). The junction open fraction will never be smaller than this value:
		$A_{JN}(t) \ge FJNMRT \cdot A_0$
	N 2 1	where $A_0$ is the total flow area of the junction. Acceptable range: $0.0 \le \text{FJNMRT} \le 1.0$ . Default value: 0.01.
W-8 (I) : II	RMGRT ( = s 2 7 2 i i <i>A</i>	Global activator of a resuspension model on all surfaces of Solid Heat Conductors (SC/TC). = 0: The global activator is off. The resuspension models may be specified individually for each SC and TC in the records 377XXX, 477XXX. $\neq$ 0: The resuspension model number IRMGRT is activated globally for all SC/TC surfaces. The resuspension model may be changed ndividually for each SC and TC in the records 377XXX, 477XXX. <i>Acceptable range:</i> 0 or a number of an existing resuspension model

Default value: 0

- W-9(R): VFMXRT Maximum volumetric fraction of aerosols in a Control Volume. Calculations are stopped and an error message is printed if the volume of aerosols divided by the total volume of a control volume exceeds this number. *Acceptable range:*  $0.001 \le VFMXRT \le 1.0$ Default value: 0.1
- W-10(R): DTMXRT Maximum deposited layer thickness, (m), on a Solid Heat Conductor surface. Calculations are stopped and an error message is printed if the deposited layer thickness exceeds this number. Acceptable range:  $10^{-3} \le \text{DTMXRT} \le 10^{3}$ Default value: 1.0
- W-11 (R): VMINRT Minimum velocity for transport of aerosol particles or fission product isotopes through a junction. If the calculated velocity is smaller than this value, it is set to zero. This prevents transport of extremely small quantities of particles or fission product isotopes, which could lead to numerical problems. Acceptable range:  $10^{-7} \le \text{VMINRT} \le 10^{-3}$  $0^{-5}$

W-12(I): ILBORT Option for Langmuir-Blodgett correlation (see Volume 1). = 1: Use the unmodified L-B correlation:

$$\eta = \eta_{\max} \cdot \frac{Stk^2}{(Stk + C_{LB})^2}$$

= 2: Use the modified L-B correlation:

$$\eta = \eta_{\max} \cdot \begin{cases} \frac{0.25}{C_{LB}} \cdot Stk & for \quad Stk < C_{LB} \\ \frac{Stk^2}{(Stk + C_{LB})^2} & for \quad Stk > C_{LB} \end{cases}$$
Acceptable range: 1 or 2
Default value: 2

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

W-1 (I): MICVRT Individual activator of the RT Package in a Control Volume. <0: the RT package is inactive in the Control Volume XXX. >1: the RT package is active in the Control Volume XXX. =0: the RT package is inactive when the global activator MGACRT is equal to 0 (record 860000), or active when MGACRT=1, 2, 3. Acceptable range: if two Control Volumes are connected by a junction, then the RT package must be either active or inactive in both Control Volumes.

*Default value:* 0.

#### 2.15.3 Records: 270XXX, Junction Activators

XXX is the Junction reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	MIJNRT	Individual activator	r of the RT Package in a Junction.
		<0: the RT package	e is inactive in the Junction XXX.
		>0: the RT package	e is active in the Junction XXX.
		=0: the RT packag	e is inactive when the global activator MGACRT is
		equal to 0 (record 8	860000), or active when MGACRT=1, 2.
		Acceptable range:	if the RT package is active in a Junction, then it must
			also be active in both Control Volumes it connects.
		Default value:	0.

#### 2.15.4 Records: 370XXX, 1-D Solid Heat Conductor Activators

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I): MISCRT Individual activator of the RT Package in a 1-D Solid Heat Conductor.
<0: the RT package is inactive in the 1-D Solid Heat Conductor XXX.</li>
>1: the RT package is active in the 1-D Solid Heat Conductor XXX.
=0: the RT package is inactive when the global activator MGACRT is equal to 0 (record 860000), or active when MGACRT=1.
Acceptable range: if any of the boundary surfaces of the heat conductor is transferring heat to a Control Volume with an active RT package, then a warning message is produced if the RT package is inactive in the heat conductor.
Default value: 0.

#### 2.15.5 Records: 470XXX, 2-D Solid Heat Conductor Activators

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I): MITCRT Individual activator of the RT Package in a 2-D Solid Heat Conductor.
<0: the RT package is inactive in the 2-D Solid Heat Conductor XXX.</li>
>1: the RT package is active in the 2-D Solid Heat Conductor XXX.
=0: the RT package is inactive when the global activator MGACRT is equal to 0 (record 860000), or active when MGACRT=1.
Acceptable range: if any of the boundary cells of the heat conductor is transferring heat to a Control Volume with an active RT package, then a warning message is produced if the RT package is inactive in the heat conductor.
Default value: 0.

#### 2.15.6 Records: 171000, Control Volume - Pool Related Data

Using this record one may specify the parameters described in record 171XXX for all Control Volumes in the model - see description of record 171XXX below.

#### 2.15.7 Records: 171XXX, Control Volume – Pool Related Data

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

- W-1 (R):FRFCRTFriction factor for turbulent deposition calculation on the pool surface.<br/>If zero or no value is entered, then the turbulent deposition will not be<br/>calculated for the pool surface. If a positive value is entered, then the<br/>turbulent deposition will be calculated for the pool surface assuming<br/>the friction factor is equal to FRFCRT.<br/>Acceptable range:  $0.001 \leq \text{FRFCRT} \leq 1.0$ .<br/>Default value: 0.1.
- W-2 (R): CRAPRT Critical ratio for aerosol to pool mass, to start resuspending deposited aerosols. When a water pool is evaporated, the aerosols deposited in the pool will be resuspended. The model is set up in such a way that the resuspension is gradual, to avoid sudden resuspension of all mass when the pool becomes empty. The resuspension starts when the aerosol mass exceeds the pool mass multiplied by CRAPRT. *Acceptable range:*  $0.001 \leq CRAPRT \leq 0.1$ . *Default value:* 0.01.
- W-3 (R): VINPRT(1) vertical velocity (m/s) of a size 1 particle in stagnant pool,  $v_{\infty}$ . Positive velocity means the particles will flow up, towards the pool surface. | VINPRT  $| \le 100$ : use constant velocity, equal to VINPRT VINPRT > 100: use the correlation:

$$v_{\infty} = \left(\frac{4/3}{C_D} \cdot \frac{Dg(\rho_f - \rho_p)}{\rho_f}\right)^{1/2}$$

- g gravity constant, =  $9.81 \text{ (m/s^2)}$
- $\rho_p$  particle density, (kg/m<sup>3</sup>)
- $\rho_f$  fluid density, (kg/m<sup>3</sup>)
- *D* particle diameter, (m)
- $C_D$  drag coefficient

VINPRT<1000: drag coefficient:  $C_{D,Re\to\infty} = \text{VINPRT} - 100$ VINPRT>1000: constant drag coeff.:  $C_D = \text{const.} = \text{VINPRT} - 1000$ The velocity will be positive (upwards) if the particle density ( $\rho_p = \text{DENART}$ ) is smaller than the fluid density ( $\rho_f = \text{current pool density}$ ). Acceptable range:  $-100.0 \le \text{VINPRT}(1) \le +100.0$ , or  $+100.0 \le \text{VINPRT}(1) \le +200.0 (0.0 \le C_{D,Re\to\infty} \le 100.0)$ 

= VINPRT(1) for size sections > 1

W-4 (R): VINPRT(2) vertical velocity (m/s) of a size 2 particle in stagnant pool

(...) until VINPRT is defined for all size sections

#### NOTE!

- If the aerosol particle field is used to represent very light particles (for example gas bubbles), which can be transported to the pool surface (VINPRT>0) then the deposition mechanism should be disabled. This is done by setting IDEPRT(1) to -1, record 865002. Otherwise the light particles may be transported back to the liquid phase due to gravitational settling, turbulent impaction, etc.
- The option ISVBCV may be needed to prevent the transport to pool surface (in favor of transport to the volume above) when CV is full of liquid Figure 2-3.
- If the correlation is used (VINPRT > 100), then the correlation for small particles may be activated using  $C_{small}$  (CSMLCV, record 161000). The correlation for small particles is:

$$v_{\infty} = \frac{1}{18} \cdot \frac{D_p^2 g(\rho_f - \rho_p)}{\eta_f} \cdot C_{small}$$

#### 2.15.8 Records: 172000, Option for Pool-Gas Transport of Particles – Global

Using this record one may specify the parameter described in record 172XXX for all Control Volumes in the model - see description of record 172XXX below.

#### 2.15.9 Records: 172XXX, Option for Pool-Gas Transport of Particles – Individual

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

W-1 (I) : KPATRT Pool-gas transport of aerosol particles. =1 : transport occurs on the pool-atmosphere surface =2: transport occurs on the bubble-pool surface. =3 : transport occurs on droplet-atmosphere surface. NOTE: with option 2, fission products are transported from one CV to another with bubble flow. With option 3, fission products are not transported with droplets from one CV to another. Therefore the droplet to and from CV is automatically disabled: IDFAJN is set to 1. Acceptable range: KPATRT = 1, 2, 3 Default value: 1 W-2(R): YPATRT Multiplier for the pool-gas transport of aerosol particles. The pool-gas transport calculated by the model described in record 171XXX, is multiplied by this value. This parameter is used for any transport defined by KPATRT. It may be used for example to model sticking fraction in case of pool-bubble transport. Acceptable range:  $0.0 \le \text{YPATRT} \le 10.0$ 1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0). Default value:

K6223/24.277594 MSt-2402

W-3 (I):KSVBCVIndicator for aerosol transport from pool to atmosphere. The meaning is<br/>the same as in case of bubble transport: ISVBCV - see Figure 2-3.<br/>Acceptable range:  $0 \le \text{KSVBRT} \le 100$ <br/>Default value:ISVBCV

#### 2.15.10 Records: 271000, Aerosol Transport Through Junctions

Using this record one may specify the parameters described in record 271XXX for all Junctions in the model - see description of record 271XXX below.

#### 2.15.11 Records: 271XXX, Aerosol Transport Through Junctions

XXX is the Junction reference number,  $001 \le XXX \le 999$ . <u>NOTE: if XXX = 000</u>, then the parameters defined in this record are applied to all Junctions.

W-1 (R): SLFART (1)

Slip factor,  $S_A$ , for aerosols size section 1 flow with the atmosphere. The slip factor is defined as the ratio of the aerosol particle velocity to that of the carrier gas. The particle transport through a junction is calculated using the particle velocity,  $v_p$ , defined as:

$$v_p = S_A \cdot v_g - J_{JN} \cdot v_{d,grav}$$

where:

$S_A$	-	slip factor, SLFART(1), (-)
$v_g$	-	gas velocity, (m/s)
Vd,grav	-	deposition velocity due to gravitational settling, (m/s)
$J_{JN}$	-	junction direction indicator (IVERJN, record 200XXX):
		= $-1$ : if the positive flow direction is down
		= 0: if the junction flow is horizontal
		= +1: if the positive flow direction is up

If -1.0 is entered, then the slip factor is calculated using the diffusiophoretic theory, as:

$$S_A = \sqrt{\frac{M_1}{M_2}} = \sqrt{\frac{R_2}{R_1}}$$

where:

 $M_1$ -molecular weight of gas in the upstream CV, (kg/kmole) $M_2$ -molecular weight of gas in the downstream CV, $R_1$ -gas constant in the upstream CV, (J/kg/K) $R_2$ -gas constant in the downstream CV

Acceptable range: $0.0 \le \text{SLFART}(1) \le 10.0$ , or  $\text{SLFART}(1) \le -1.0$ .<br/>(a small number,  $<10^{-50}$ , sets the value to 0.0).Default value:1.0.

W-2 (I): SLFPRT Slip factor,  $S_A$ , for aerosols size section 1 flow with the pool. (1) The slip factor is defined as the ratio of the aerosol particle velocity to that of the carrier liquid. The particle transport through a junction is calculated using the particle velocity,  $v_p$ , defined as:

$$v_p = S_P \cdot v_l + J_{JN} \cdot v_{\infty}$$

where:

$S_P$	-	slip factor, SLFPRT(1), (-)
$v_l$	-	liquid velocity, (m/s)
$J_{JN}$	-	junction direction indicator, described above
$\mathcal{V}_{\infty}$	-	vertical velocity (m/s) of a single particle in stagnant pool
Accep	table r	<i>ange:</i> $0.0 \le \text{SLFPRT}(1) \le 10.0$ .
1		(a small number, $<10^{-50}$ , sets the value to 0.0).
Defau	lt valu	e: 1.0.

W-3 (I): VINFRT(1) vertical velocity (m/s) of a size 1 particle in stagnant pool,  $v_{\infty}$ . Positive velocity means the particles will flow vertically up.

| VINFRT  $| \le 100$ : use constant velocity, equal to VINFRT

VINFRT > 100: use the correlation:

$$v_{\infty} = \left(\frac{4/3}{C_D} \cdot \frac{Dg(\rho_f - \rho_p)}{\rho_f}\right)^{1/2}$$

- g gravity constant, =  $9.81 \text{ (m/s^2)}$
- $\rho_p$  particle density, (kg/m<sup>3</sup>)
- $\rho_f$  fluid density, (kg/m<sup>3</sup>)
- *D* particle diameter, (m)
- $C_D$  drag coefficient

VINFRT<1000: dr	ag coefficient:	$C_{D,Re\to\infty} = \text{VINFRT} - 100$
VINFRT>1000: co	instant drag coeff.:	$C_D = \text{const.} = \text{VINFRT} - 1000$
The velocity will	be positive (upwar	ds) if the particle density ( $\rho_p =$
DENART) is small	ler than the fluid der	nsity ( $\rho_f$ = current pool density).
Acceptable range:	-100.0≤VINFRT(	1)≤+100.0, or
	+100.0 <vinfrt(< td=""><td><math>1) \leq +200.0 \ (0.0 &lt; C_{D,Re \to \infty} \leq 100.0)</math></td></vinfrt(<>	$1) \leq +200.0 \ (0.0 < C_{D,Re \to \infty} \leq 100.0)$
	+1000.0 <vinfrt< td=""><td><math>(1) \leq +1100.0 \ (0.0 &lt; C_D \leq 100.0)</math></td></vinfrt<>	$(1) \leq +1100.0 \ (0.0 < C_D \leq 100.0)$
Default value:	= 0.0 for size secti	on 1
	= VINFRT(1) for	size sections $> 1$

The three words described above are repeated for all size sections (defined in record 861000). Thus the number of entries in this record should be  $3 \times N$ , where N is the number of aerosol size sections.

Note that if the correlation is used (VINFRT > 100), then the correlation for small particles may be activated using  $C_{small}$  (CSMLCV, record 161000). The correlation for small particles is:

$$v_{\infty} = \frac{1}{18} \cdot \frac{D_p^2 g(\rho_f - \rho_p)}{\eta_f} \cdot C_{small}$$

#### 2.15.12 Records: 371XXX, 1-D Solid Heat Conductors - Junctions Associations

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IJN1RT (1)	Reference number of = 0: No association using the gas veloce (Word 3). > 0: Left surface of IJN1RT(1). Turbulor velocity, or the gas indicator IVTDRT multiplied by XVT Acceptable range: Default value:	of a junction associated with the SC left surface. In with junction. Turbulent deposition is calculated ity at the SC left surface, multiplied by XVT1RT(1) of this SC is associated with the junction number ent deposition is calculated using either the junction is velocity at the SC left surface, depending on the (word 15 in the record 865000). The velocity is 1RT(1) (Word 3). the junction must be connected to the Control Volume that is a boundary volume for the left surface of the SC. The default value depends on the global activator IJNART (record 860000): if UNART(= 0: 0
			if IJNAR1 $\leq$ 0: 0 if IJNART=1 or 11: JN with the smallest flow area if IJNART=2 or 12: JN with the largest flow area.
W-2 (R) :	WJN1RT (1)	Representative wid If $-1.0$ is entered the not affect the flow a entered, then the d junction flow area a	th, $W$ , of the junction defined by IJN1RT(1), above. nen the deposition on the left surface of the SC will area of the junction IJN1RT(1). If a positive value is eposition on the surface of the SC will reduce the as (see Figure 2-67):
		A(t) = A	$A_0 - W D(t)$
		$A_0$ junction $W$ junction $D(t)$ thickness $A(t)$ current	on total flow area, (m <sup>2</sup> ) on width, (m) less of the deposited layer, (m) at open area of the junction (m <sup>2</sup> )
◀	W		
	JN		
		D(t)	

Figure 2-67 Junction area reduction in case of deposition on a 1-D conductor.

SC

Note that if the SC has a multiplicity not equal to 1.0 (for example, it represents multiple plates), then the deposit thickness, D(t), will be multiplied by the SC multiplicity. Therefore the width entered here should represent in such case the width of a <u>single plate</u>.

Several SC-s can be associated with a single junction. In this case the total area reduction of the junction will be given by:

$$A(t) = A_0 - \sum_{SC} W_{SC} D_{SC}(t)$$

The total reduction of the flow area is internally limited by the code, so the junction area will never be smaller than FJNMRT× $A_0$ , where FJNMRT is the minimum area fraction, entered in the record 860000.

If the user does not want to have junction area reduction, but at the same time wants to calculate the turbulent deposition, then the junction number should be specified using IJN1RT(1), while the area reduction should be deactivated by setting WJN1RT(1) to -1.0.

Acceptable range:	$0.01 \le WJN1RT(1) \le 10.0$ , or $WJN1RT(1) \le -1.0$ .
	Area reduction due to deposition cannot be
	calculated for a valve junction. The default value
	depends on the global activator IJNART=0 (record
	860000):
Default value:	if IJNART<10: 0.0
U	if IJNART>10: $A_0^{1/2}$ ( $A_0$ is the junction total flow
	area).

W-3 (I) :XVT1RTGas velocity multiplier for turbulent deposition calculation on the left<br/>surface (see description of IJN1RT - word 1 above).Acceptable range: $0.0 < XVTDRT \le 1000.0$ .<br/>Default value:1.0.

W-4 (I): IJN1RT Reference number of a junction associated with the SC right surface. = 0: No association with junction. Turbulent deposition is calculated (2)using the gas velocity at the SC right surface, multiplied by XVT1RT(2) (Word 6). > 0: Right surface of this SC is associated with the junction number IJN1RT(2). Turbulent deposition is calculated using either the junction velocity, or the gas velocity at the SC right surface, depending on the indicator IVTDRT (word 15 in the record 865000). The velocity is multiplied by XVT1RT(2) (Word 6). Acceptable range: the junction must be connected to CV that is a boundary volume for the right surface of the SC. The default value depends on the global activator Default value: IJNART (record 860000): if LINART<0: 0 if IJNART=1 or 11: JN with the smallest flow area if IJNART=2 or 12: JN with the largest flow area.

# W-5 (R):WJN1RT<br/>(2)Representative width, W, of the junction defined by IJN1RT(2), above.<br/>Meaning, as described above, at WJN1RT(1) description, but in relation<br/>to the right surface of the SC.<br/>Acceptable range: $0.01 \le WJN1RT(2) \le 10.0$ , or WJN1RT(2) $\le -1.0$ .

			Area reduction due to deposition cannot be calculated for a valve junction. The default value depends on the global activator IJNART=0 (record
		Default value:	860000): if IJNART<10: 0.0 if IJNART>10: $A_0^{1/2}$ ( $A_0$ is the junction flow area).
W-6 (I) :	XVT1RT (2)	Gas velocity multi right surface (see c Acceptable range: Default value:	plier for turbulent deposition calculation on the description of IJN1RT(2) - word 4 above). $0.0 < XVTDRT(2) \le 1000.0.$ 1.0.

#### 2.15.13 Records: 471XXX, 2-D Solid Heat Conductors – Junctions Associations

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	I1	Boundary cell number. Using I1 and I2 (below) the user specifies the cell range for association with junction. The junction association, defined by Word 3, will be applied for the boundary cells I, $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. <i>Default value:</i> none.
W-2 (I) :	I2	Boundary cell number. Using I2 and I1 (above) the user specifies the cell range for association with junction. The junction association, defined by Word 3, will be applied for the boundary cells I, $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. I2 $\ge$ I1. <i>Default value:</i> none.
W-3 (I) :	IJN2RT (I)	Reference number of a junction associated with the boundary cells, I: I = I1 through I2. = 0: No association with junction. Turbulent deposition is calculated using the gas velocity at the cell I surface, multiplied by XVT2RT(I) (Word 4). > 0: Cell I surface of this TC is associated with the junction number IJN2RT(I). Turbulent deposition is calculated using either the junction velocity, or the gas velocity at the cell I surface, depending on the indicator IVTDRT (word 15 in the record 865000). The velocity is multiplied by XVT2RT(2) (Word 4). <i>Acceptable range:</i> the junction must be connected to CV that is a boundary volume for the right surface of the SC. <i>Default value:</i> The default value depends on the global activator IJNART (record 860000): if IJNART=0: 0 if IJNART=1 or 11: JN with the smallest flow area if IJNART=2 or 12: JN with the largest flow area.
W-4 (R) :	WJN2RT (I)	Representative width, <i>W</i> , of the junction defined by IJN2RT(I), above. If zero or no value is entered then the deposition on cell I of the TC will not affect the flow area of the junction IJN2RT(I). If a positive value is

entered, then the deposition on cell IBC of the TC will reduce the junction flow area by:  $W_k \times D_k(t)$ . The total area reduction of the junction will be equal to the sum of reductions due to deposit on individual cell (see Figure 2-68):

$$A(t) = A_0 - \sum_k W_k D_k(t)$$

$A_0$	junction total flow area, (m <sup>2</sup> )
$W_k$	width related to cell $k$ , (m)
$D_k(t)$	thickness of the deposited layer on the cell $k$ , (m)
A(t)	current open area of the junction, (m <sup>2</sup> )



Figure 2-68 Junction area reduction in case of deposition on 2-D conductor.

Note that if the TC has a multiplicity not equal to 1.0 (for example, it represents multiple plates), then the deposit thickness,  $D_k(t)$ , will be multiplied by the TC multiplicity. Therefore the width entered here should represent in such case the width of a <u>single plate</u>.

Several TC-s (and SC-s) can be associated with a single junction. In this case the total area reduction of the junction will be given by:

$$A(t) = A_0 - \sum_{SC} W_{SC} D_{SC}(t) - \sum_{TC} \sum_{k} W_{TC,k} D_{TC,k}$$

The total reduction of the flow area is internally limited by the code, so the junction area will never be smaller than FJNMRT× $A_0$ , where FJNMRT is the minimum area fraction, entered in the record 860000.

If the user does not want to have junction area reduction, but at the same time wants to calculate the turbulent deposition, then the junction number should be specified using IJN2RT(I), while the area reduction should be deactivated by setting WJN2RT(I) to -1.0.

 Acceptable range:
 0.01 ≤ WJN2RT(I) ≤ 10.0, or WJN2RT(I) ≤-1.0.

 Area reduction due to deposition cannot be calculated for a valve junction. The default value depends on the global activator IJNART=0 (record 860000):

 Default value:
 if IJNART<10: 0.0</td>

if IJNART>10:  $A_0^{1/2}$  ( $A_0$  is the junction flow area).

The data set consisting of the five words described above is repeated until the junctions are defined for all desired boundary cells. The data may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 5.

#### 2.15.14 Records: 372XXX, 1-D Solid Heat Conductors Gravity Factors

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

- W-1 (R): GRV1RT SC left surface orientation related to the gravity vector.
  - (1)

=-1.0: horizontal surface, facing down

= 0.0: vertical surface

=+1.0: horizontal surface, facing up

Other values:  $GRV1RT(1) = sin(\alpha)$ , where  $\alpha$  is the angle between the normal to the surface and the horizontal direction.

The gravitational deposition velocity is multiplied by GRV1RT. In case of vertical surfaces the gravitational deposition does not contribute to the total deposition. In case of horizontal surfaces facing up the gravitational deposition has a positive effect (i.e. the gravitational deposition is added to the other velocities to obtain the total deposition velocity). In case of horizontal surfaces facing down the gravitational deposition has a negative effect (i.e. the gravitational deposition has a negative effect (i.e. the gravitational deposition is subtracted from the other velocities to obtain the total deposition velocity).

For rectangular structures the default values are based on the SC vertical orientation parameter (IVERSC). For cylindrical and spherical structures the default values depend on the global activator IGRVRT (see record 860000). If the user models a horizontal pipe, then the best way is to divide it into two parts, the lower half and the upper half (each half can be modelled for example using cylindrical SC with a multiplicity factor of 0.5).

The gravity indicator should then be specified as, for example: +1.0 for the SC representing the lower half of the pipe and -1.0 for the SC representing the upper half of the pipe.

Strictly speaking, the gravity indicator on the surface of the half-pipe should be equal to the average  $sin(\alpha)$  of the surface angle. This is obtained as:



Therefore, for the SC representing the lower half of the pipe GRV1RT(1) will be equal to 0.637, while for the SC representing the upper half of the pipe GRV1RT(1) will be equal to -0.637. Similarly the average gravity factors can be calculated for the lower (and the upper) half of a sphere:

$$GRV1RT(1) = \frac{\int_{0}^{\pi/2} 2\pi r \sin^{2}(\alpha) \, d\alpha}{\int_{0}^{\pi/2} 2\pi r \sin(\alpha) \, d\alpha} = \frac{\pi/4}{1.0} = 0.785$$

Acceptable range:  $-1.0 \leq \text{GRV1RT}(1) \leq +1.0$ 

(a small number,  $<10^{-50}$ , sets the value to 0.0). rectangular geometry (IGEOSC=1): Default value: equal to the natural convection indicator, INCLSC: vertical (IVERSC=0): 0.0, horizontal down (IVERSC=-1): -1.0. horizontal up (IVERSC=+1): +1.0,cylindrical and spherical geometry: if the global selector, IGRVRT (section 2.15.1), is equal to 2, then GRV1RT is 0.0 (no gravitational deposition). If the global selector equal to 1, then GRV1RT is set to one half of the theoretical value for the upper half of the structure. This means  $1/\pi = 0.3183$  for horizontal cylinders, and  $\pi/8 = 0.3927$  for the spheres. If fins/spines are present, then the default value is 0.0 if IGRVRT=2 or the upwards area fraction if IGRVRT=1. The upwards area fraction is:  $1.0/A_I$  for horizontal walls (vertical fins),  $0.5 \times (1.0 - 1.0/A_l)$  for vertical walls (horizontal fins),  $0.3183/A_{I}$ , for horizontal cylinders (vertical fins).  $(A_I$  is the surface area increase ratio due to fins).

W-2(R):

(2)

GRV1RT SC right surface orientation related to the gravity vector. =-1.0: horizontal surface, facing down

- = 0.0: vertical surface.

=+1.0: horizontal surface, facing up.

Other values:  $GRV1RT(2) = sin(\alpha)$ , where  $\alpha$  is the angle between the normal to the surface and the horizontal direction.

For a SC representing lower half of a pipe GRV1RT(2) will be equal to -0.637, while for a SC representing upper half of the pipe GRV1RT(2) will be equal to 0.637.

Acceptable range:	$-1.0 \le \text{GRV1RT}(2) \le +1.0.$
	(a small number, $<10^{-50}$ , sets the value to 0).
Default value:	rectangular geometry (IGEOSC=1):
	equal to the natural convection indicator, INCRSC:
	- vertical (IVERSC=0): 0.0,
	- horizontal down (IVERSC=-1): +1.0,
	- horizontal up (IVERSC=+1): -1.0,
	cylindrical and spherical geometry: if the global
	selector, IGRVRT (section 2.15.1), is equal to 2,
	then GRV1RT is 0.0 (no gravitational deposition).
	If the global selector is equal to 1, then GRV1RT is
	set to one half of the theoretical value for the upper
	half of the structure. This means $1/\pi = 0.3183$ for
	horizontal cylinders, and $\pi/8 = 0.3927$ for the
	spheres.
	If fins/spines are present, then the default value is
	0.0 if IGRVRT=2 or the upwards area fraction if
	IGRVRT=1. The upwards area fraction is:
	$1.0/A_I$ for horizontal walls (vertical fins),
	$0.5 \times (1.0 - 1.0/A_I)$ for vertical walls (horizontal fins),
	$0.3183/A_I$ , for horizontal cylinders (vertical fins).
	$(A_I$ is the surface area increase ratio due to fins).

### 2.15.15 Records: 472XXX, 2-D Solid Heat Conductors Gravity Factors

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	II	Boundary cell number. Using I1 and I2 (below) the user specifies the cell range for gravity vector definition. The gravity vector, defined by Word 3, will be applied for the boundary cells I, $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. <i>Default value:</i> none.
W-2 (I) :	I2	Boundary cell number. Using I2 and I1 (above) the user specifies the cell range for gravity vector definition. The gravity vector, defined by Word 3, will be applied for the boundary cells I, $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. I2 $\ge$ I1. <i>Default value:</i> none.
W-3 (R) :	GRV2RT (I)	TC, boundary cell I, surface orientation related to the gravity vector. =-1.0: horizontal surface, facing down = 0.0: vertical surface =+1.0: horizontal surface, facing up Other values: GRV2RT(I) = $sin(\alpha)$ , where $\alpha$ is the angle between the normal to the surface and the horizontal direction. <i>Acceptable range:</i> -1.0 ≤ GRV2RT(I) ≤ +1.0.

(a small number,  $<10^{-50}$ , sets the value to 0). *Default value:* (a small number,  $<10^{-50}$ , sets the value to 0). rectangular geometry (IGEOSC=1): equal to the natural convection indicator, INCBTC. cylindrical geometry: if the global selector, IGRVRT (section 2.15.1), is equal to 2, then GRV2RT is 0.0 (no gravitational deposition). If the global selector is equal to 1, then for the horizontal cylindrical walls GRV2RT is set to one half of the theoretical value for the upper half of the cylinder:  $1/\pi = 0.3183$ .

The data set consisting of the three words described above is repeated until the gravity factors are defined for all desired boundary cells. The data may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 3.

#### 2.15.16 Records: 361XXX, Electric Field Strength at 1-D Solid Heat Conductors

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	EFS1RT(1)Electric field strength towards the left surface of the 1-D Solid Heat Conductor, (V/m). Used to calculate the electrophoretic deposition.  Acceptable range: $-1.0 \times 10^{10} \le \text{EFS1RT}(1) \le 1.0 \times 10^{10}$  Default value: 0.0
W-2 (R) :	EFS1RT(2)Electric field strength towards the right surface of the 1-D Solid Heat Conductor, (V/m). Used to calculate the electrophoretic deposition.  Acceptable range: $-1.0 \times 10^{10} \le \text{EFS1RT}(2) \le 1.0 \times 10^{10}$  Default value: 0.0

#### 2.15.17 Records: 461XXX, Electric Field Strength at 2-D Solid Heat Conductors

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	II	Boundary cell number. Using I1 and I2 (below) the user specifies the cell range for the electric field strength definition. The electric field strength, defined by Word 3, will be applied for the boundary cells I, I1 $\leq$ I $\leq$ I2. <i>Acceptable range:</i> must be an existing boundary cell number. <i>Default value:</i> none.
W-2 (I) :	I2	Boundary cell number. Using I2 and I1 (above) the user specifies the cell range for the electric field strength definition. The electric field strength, defined by Word 3, will be applied for the boundary cells I, I1 $\leq$ I2. <i>Acceptable range:</i> must be an existing boundary cell number. I2 $\geq$ I1. <i>Default value:</i> none.

W-3 (R) :EFS2RT(I)Electric field strength towards the boundary surfaces I,  $I1 \le I \le I2$  of the<br/>2-D Solid Heat Conductor, (V/m). Used to calculate the electrophoretic<br/>deposition.<br/>Acceptable range:  $-1.0 \times 10^{10} \le EFS2RT(I) \le 1.0 \times 10^{10}$ <br/>Default value: 0.0

The data set consisting of the three words described above is repeated until the electric force strengths are defined for all desired boundary cells. The data may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 3.

#### 2.15.18 Record: 861000, Aerosol Size Sections

W-1 (R) :	DASCRT (1)	Representative equ Acceptable range: Default value:	ivalent diameter of the aerosol size section 1, (m). $1.0 \times 10^{-8} \le \text{DASCRT}(1) \le 1.0 \times 10^{-2}$ . $1.0 \times 10^{-6}$ .
W-2 (R) :	DASCRT (2)	Representative equ Acceptable range:	ivalent diameter of the aerosol size section 2, (m). DASCRT(i–1) < DASCRT(i) $\leq 1.0 \times 10^{-2}$ . The diameter ratio, DASCRT(i)/DASCRT(i–1), must be at least equal to 0.5 times the previous ratio DASCRT(i–1)/DASCRT(i-2), for i $\geq$ 3.
		Default value:	3.0×10 <sup>-6</sup> .

..., until all diameters are entered. The number of aerosol size sections, NSIZRT, will be equal to the number of input entries in this record. The maximum number of the aerosol size sections is 20.

The default aerosol size sections include 5 sections, with the following representative diameters:

Sec. number	1	2	3	4	5
Diameter, (m)	1.0×10 <sup>-6</sup>	3.0×10 <sup>-6</sup>	$1.0 \times 10^{-5}$	3.0×10 <sup>-5</sup>	$1.0 \times 10^{-4}$

It is recommended that for each the size sections i>1 the diameter is at least 1.25 times the diameter of the previous section:

 $DASCRT(i) \ge 1.25 \times DASCRT(i-1)$ 

This condition approximately corresponds to:

 $V_i \geq 2V_{i-1}$ 

(the exact value that leads to  $V_i = 2 V_{i-1}$  is  $D_i = 1.2599 D_{i-1}$ ). The default size sections are set in such way that the ratios of the section volumes are approximately 30:  $V_i \sim 30 V_{i-1}$ .

#### 2.15.19 Record: 861001, Aerosol Surface Areas

The surface area of aerosol particles is used for sorption calculations if the sorption model is activated (records 898001 through 898004). For the sorption model to work properly the surface area of aerosol

particles must be preserved during coagulation. Therefore the surface area based on a sphere with the size section representative diameter:

$$A_i = \pi \cdot D_i^2$$

cannot be used, since it would lead to decrease of the overall surface area of aerosol particles during coagulation. The formula that is applied in SPECTRA is:

$$A_i = A_{base} \cdot \frac{V_i}{V_{base}}$$

 $A_i$  - surface area of a single aerosol particle of the size section *i*, (m<sup>2</sup>)

 $A_{base}$  - surface area of a base particle, (m<sup>2</sup>)

- volume of a single aerosol particle of the size section i, (m<sup>3</sup>)

 $V_{base}$  - volume of a base particle, (m<sup>3</sup>)

By default the base particle is a spherical particle of the smallest aerosol size section:

$$A_{base} = \pi \cdot D_1^2$$

Physically this means that with the default treatment the particles of the smallest size section are assumed to be spherical, while the particles of the larger size sections are assumed to be conglomerates, consisting of multiple spherical particles of the smallest size section.

A user defined multiplier is available for the base particle area calculation. The base particle area is calculated from:

$$A_{base} = X_{base} \cdot \pi \cdot D_1^2$$

*X*<sub>base</sub> - user-defined multiplier, (-)

The value of  $X_{base}$  equal to 1.0 results in spherical particles of the smallest size section. Using a value larger than 1.0 the user may account for non-spherical shapes of the smallest size section particles.

W-1 (R): XBASRT User-defined multiplier for the base particle area calculation,  $X_{base}$ , (-). Acceptable range:  $10^{-10} \le \text{XBASRT} \le 10^{10}$ Default value: 1.0

#### 2.15.20 Records: 173XXX, Initial Airborne Aerosol Masses

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	XAIRRT (1)	Initial mass of aero Acceptable range: Default value:	sols size section 1 in the CV atmosphere, (kg). XAIRRT(1) $\ge$ 0.0, the total volume of aerosols of all size sections in both atmosphere and pool must not exceed the total volume of the CV multiplied by a maximum aerosol fraction, given by VFMXRT (record 860000).
		Dejuuti vutue.	0.0.

osphere, (kg).
ume of aerosols of
nere and pool must
e CV multiplied by
iven by VFMXRT
i

..., until the initial masses are specified for all size sections.

#### 2.15.21 Records: 174XXX, Initial Masses of Aerosols Deposited in the Pool

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

W-1 (R):	XWATRT	Initial mass of aero	sols size section 1 in the pool of the CV, (kg).
	(1)	Acceptable range:	XWATRT(1) $\ge$ 0.0, the total volume of aerosols of
			all size sections in both atmosphere and pool must
			not exceed the total volume of the CV multiplied by
			a maximum aerosol fraction, given by VFMXRT
			(record 860000).
		Default value:	0.0.
W-2 (R) :	XWATRT	Initial mass of aero	sols size section 2 in the pool of the CV, (kg).
	(2)	Acceptable range:	XWATRT(2) $\ge$ 0.0, the total volume of aerosols of
		1 0	all size sections in both atmosphere and pool must
			not exceed the total volume of the CV multiplied by
			a maximum aerosol fraction, given by VFMXRT
			(record 860000).
		Default value:	0.0.

..., until the initial masses are specified for all size sections.

#### 2.15.22 Records: 373XXX, Initial Deposition on the Left Surface of a SC

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	XDP1RT	Initial mass of aero	sols size section 1 on the left surface of SC, (kg).
	(1)	Acceptable range:	$XDP1RT(1) \ge 0.0$ , the initial thickness of the
			deposited aerosols must not exceed the maximum
			aerosol thickness, given by DTMXRT (record
			860000).
		Default value:	0.0.
W-2 (R) :	XDP1RT	Initial mass of aero	sols size section 2 on the left surface of SC, (kg).
	(2)	Acceptable range:	$XDP1RT(2) \ge 0.0$ , the initial thickness of the
			deposited aerosols must not exceed the maximum
			aerosol thickness, given by DTMXRT (record
			860000).

*Default value:* 0.0.

..., until the initial masses are specified for all size sections.

#### 2.15.23 Records: 374XXX, Initial Deposition on the Right Surface of a SC

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	XDP1RT	Initial mass of aero	sols size section 1 on the right surface of SC, (kg).
	(1)	Acceptable range:	XDP1RT(1) $\ge$ 0.0, the initial thickness of the deposited aerosols must not be bigger than $10^{-3}$ m.
		Default value:	0.0.
W-2 (R) :	XDP1RT	Initial mass of aero	osols size section 2 on the right surface of SC, (kg).
	(2)	Acceptable range:	XDP1RT(2) $\ge 0.0$ , the initial thickness of the deposited aerosols must not be bigger than $10^{-3}$ m.
		Default value:	0.0.

..., until the initial masses are specified for all size sections.

## 2.15.24 Records: 474XXX, Initial Deposition on the Boundary Surfaces of a TC

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	11	Boundary cell num cell range for initia by Word 3, will be <i>Acceptable range:</i> <i>Default value:</i>	aber. Using I1 and I2 (below) the user specifies the l deposited mass definition. The initial mass, defined applied for the boundary cells I, $I1 \le I \le I2$ . must be an existing boundary cell number. none.
W-2 (I) :	12	Boundary cell num cell range for initia by Word 3, will be <i>Acceptable range:</i> <i>Default value:</i>	aber. Using I2 and I1 (above) the user specifies the l deposited mass definition. The initial mass, defined applied for the boundary cells I, $I1 \le I \le I2$ . must be an existing boundary cell number. I2 $\ge$ I1. none.
W-3 (R) :	XDP2RT (1)	Initial mass of aero Acceptable range: Default value:	sols size section 1 on the cell I surface, (kg). XDP2RT(1) $\geq 0.0$ , the initial thickness of the deposited aerosols of all size sections must not be bigger than $10^{-3}$ m. 0.0.
W-4 (R) :	XDP2RT (2)	Initial mass of aero Acceptable range: Default value:	sols size section 2 on the cell I surface, (kg). XDP2RT(2) $\ge 0.0$ , the initial thickness of the deposited aerosols of all size sections must not be bigger than $10^{-3}$ m. 0.0.

 $\ldots$ , until the initial masses are specified for all size sections. Several records with the same number may be entered, each record containing data for different boundary cells.

#### 2.15.25 Records: 175XXX, External Sources of Aerosols

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	ZSRCRT	Elevation of the sou Acceptable range: Default value:	arce above bottom of the CV, (m). $0.0 \le \text{ZSRCRT} \le \text{HEIGCV}$ (CV height). 0.0.
W-2 (I) :	ISRCRT (1)	Indicator defining to If the number is po Function with the negative, then the so reference number: or Control Function Acceptable range: Default value:	the aerosol source for the size section 1 in the CV. sistive, then the source will be defined by a Tabular reference number: ISRCRT(1). If the number is ource will be defined by a Control Function with the  ISRCRT(1) $ $ . The units obtained from the Tabular are assumed to be (kg/s). must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-3 (I) :	ISRCRT (2)	Indicator defining to If the number is por Function with the negative, then the sereference number: or Control Function Acceptable range: Default value:	the aerosol source for the size section 2 in the CV. sitive, then the source will be defined by a Tabular reference number: ISRCRT(2). If the number is ource will be defined by a Control Function with the  ISRCRT(2) $ $ . The units obtained from the Tabular are assumed to be (kg/s). must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.

..., until the sources are specified for all size sections.

#### 2.15.26 Records: 375XXX, External Sources of Aerosols Deposited on 1-D Surfaces

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	IBC	Surface indicator. =1: left surface, =2: right surface Acceptable range: 1 or 2 Default value: none	
W-2 (I) :	ISC1RT(1)	Indicator defining the ae on the surface IBC of t number is positive, then the with the reference number source will be defined by	rosol source for the size section 1, deposited he 1-D Solid Heat Conductor XXX. If the le source will be defined by a Tabular Function r: ISC1RT. If the number is negative, then the a Control Function with the reference number:

		ISC1RT   . The un assumed to be (kg/s Acceptable range:	its obtained from the Tabular or Control Function are s). must be a valid reference number of a Tabular or a Control Function, if non-zero.
		Default value:	0.
W-3 (I) :	ISC1RT(2)	2) Indicator defining the aerosol source for the size section 2, deposite on the surface IBC of the 1-D Solid Heat Conductor XXX. If the number is positive, then the source will be defined by a Tabular Function with the reference number: ISC1RT. If the number is negative, then the source will be defined by a Control Function with the reference number  ISC1RT . The units obtained from the Tabular or Control Function a assumed to be (kr/s)	
		Acceptable range:	must be a valid reference number of a Tabular or a
			Control Function, if non-zero.
		Default value:	0.

..., until the sources are specified for all size sections.

#### 2.15.27 Records: 475XXX, External Sources of Aerosols Deposited on 2-D Surfaces

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R):	IBC	Boundary cell num	ber. $1 < IPC < NPCI TC$
		<i>Default value:</i>	none
W-2 (I) :	ISC2RT(1)	Indicator defining on the surface IB number is positive, with the reference is source will be define ISC2RT  . The un assumed to be (kg/s Acceptable range: Default value:	the aerosol source for the size section 2, deposited C of the 2-D Solid Heat Conductor XXX. If the then the source will be defined by a Tabular Function number: ISC2RT. If the number is negative, then the ted by a Control Function with the reference number: its obtained from the Tabular or Control Function are s). must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.
W-3 (I) :	ISC2RT(2)	Indicator defining on the surface IB number is positive, with the reference is source will be defin  ISC2RT . The un assumed to be (kg/s Acceptable range: Default value:	the aerosol source for the size section 2, deposited C of the 2-D Solid Heat Conductor XXX. If the then the source will be defined by a Tabular Function number: ISC2RT. If the number is negative, then the red by a Control Function with the reference number: its obtained from the Tabular or Control Function are s). must be a valid reference number of a Tabular or a Control Function, if non-zero. 0.

..., until the sources are specified for all size sections.

#### 2.15.28 Records: 275XXX, Aerosol Filter Model

XXX is the Junction reference number,  $001 \le XXX \le 999$ . The default values of parameters are appropriate for a glass fibre filter (reference [34], table 9.1).

W-1 (I) :	IFLTRT	Filter type. =0: No filter. =1: Filter type 1 – v =2: Filter type 2 – g Acceptable range: Default value:	user defined efficiency. glass fibre filter. 0, 1, 2. 0.
		FILTER T	TYPE 1 DATA
W-2 (R) :	JFLTRT(1)	Reference number efficiency for the a <i>Acceptable range:</i>	of a Tabular or a Control Function that defines filter erosol size section 1, (-). must be a valid reference number of a Tabular or Control Function, if nonzero
		Dejuuti vatue.	0.0.
W-3 (R) :	JFLTRT(2)	Reference number efficiency for the a <i>Acceptable range:</i>	of a Tabular or a Control Function that defines filter erosol size section 2, (-). must be a valid reference number of a Tabular or Control Function, if nonzero
		Default value:	0.0.
, until the ef	ficiencies are	e specified for all siz	e sections.
		FILTER T	TYPE 2 DATA
W-2 (R) :	ALPFRT	Packing density or equal to one minus	solidity of the filter, $\alpha$ , (-). The packing density is the porosity, $\varepsilon$ , of the filter:
		$\alpha$ =	$=1-\varepsilon$
		Acceptable range: Default value:	0.01 ≤ ALPFRT ≤ 0.99. 0.10 [34].
W-3 (R) :	THCFRT	Thickness of the fil Acceptable range: Default value:	lter, $t_f$ , (m). $1.0 \times 10^{-5} \le \text{ALPFRT} \le 1.0 \times 10^{-2}$ . $2.3 \times 10^{-4}$ [34].
W-4 (R) :	DPNFRT	Pressure drop at the value or zero is en fiber diameter, $d_f$ (n	e velocity of 0.27 m/s for a new filter, $\Delta p$ , (Pa). If no tered, then the pressure drop is calculated using the n) (Word 5 below), from ([34], Chapter 9):
		$\Delta p = \frac{\eta}{2}$	$rac{dt_f U_0 f(lpha)}{d_f^2}$

where:

- $\eta$  gas viscosity (equal to the air viscosity:  $1.8 \times 10^{-5}$  kg/m/s),
- T gas temperature (equal to 300 K),
- $U_0$  face velocity (equal to 2.7×10<sup>-1</sup> m/s),
- and:

 $f(\alpha) = 64\alpha^{1.5} (1+56\alpha^3)$  for: 0.006 <  $\alpha$  < 0.3

<u>Note</u>! The forward and reverse loss coefficients, FLCFJN and FLCRJN, entered in the record 210XXX, are checked for consistency with the filter data. The minimum loss factor is calculated from:

$$K_{\min} = \frac{2\Delta p}{\rho v^2} = \frac{2\Delta p}{1.2 \cdot 0.27^2}$$

where 1.2 is the air density at normal conditions. If the value of the loss coefficient is smaller than  $K_{\min}$ , then a warning message is printed and the loss coefficient is re-set to the value of  $K_{\min}$ . Acceptable range:  $1.0 \times 10^2 \le \text{DPNFRT} \le 1.0 \times 10^5$ , if non-zero. Default value:  $2.0 \times 10^3$  [34].

W-5 (R): DSFFRT Diameter of a single fiber,  $d_{f_i}$  (m). If no value or zero is entered, then the fiber diameter is calculated using the pressure drop  $\Delta p$ , (Pa) (Word 4 above):

$$d_f = \sqrt{\frac{\eta t_f U_0 f(\alpha)}{\Delta p}}$$

Acceptable range:  $1.0 \times 10^{-8} \le \text{DFSFRT} \le 1.0 \times 10^{-4}$ , if non-zero. Default value:  $1.0 \times 10^{-6}$  (the range  $0.1 - 4 \ \mu\text{m}$  is given in [34]).

#### 2.15.29 Records: 276XXX, Pool Scrubbing Model

XXX is the Junction reference number,  $001 \le XXX \le 999$ . When a stream of gas enters a pool region of the receiving Control Volume, then it forms bubbles in the pool. The gas is assumed to quickly reach equilibrium at the entrance to the pool (the equilibrium conditions are calculated by the Bubble Collapse Model). At the end of the bubble collapse the mass flow of gas entering the pool,  $W_B$ , is divided into the mass flow of gas,  $W_G$ , and condensed liquid,  $W_L$ . The flow  $W_G$  forms bubbles in the pool, while  $W_L$  remains in the pool. The aerosols entering the pool with the stream of gas are divided as follows:

- The part  $W_L/W_B$  remains in the pool.
- The part  $W_G / W_B$  is transported partly to the atmosphere and partly remains in the pool, depending on the pool scrubbing efficiency.

Therefore the division of aerosol particles is:

•	Fraction remaining in the pool:	$\frac{W_G}{W_B}E_{PS} + \frac{W_L}{W_B}$
•	Fraction reaching the atmosphere:	$\frac{W_G}{W_B}(1-E_{PS})$

In the above formulae  $E_{PS}$  is the pool scrubbing efficiency, defined in this record.

W-1 (I) :	IPLSRT	Pool scrubbing model.	
		=1: Model 1 – user defined scrubbing efficience	cy.
		=2: Model 2 - theoretical model.	
		Acceptable range: 1, 2.	
		Default value: 1.	

#### MODEL 1 DATA

W-2 (R) :	JPLSRT(1)	Reference number	of a Tabular or a Control Function that defines pool
		scrubbing efficience	y, $E_{PS}$ , for the aerosol size section 1, (-).
		Acceptable range:	must be a valid reference number of a Tabular or
			Control Function, if nonzero
		Default value:	0.1.
W-3 (R) :	JPLSRT(2)	Reference number	of a Tabular or a Control Function that defines pool

W-3 (R): JPLSR1(2) Reference number of a Tabular or a Control Function that defines pool scrubbing efficiency,  $E_{PS}$ , for the aerosol size section 2, (-). Acceptable range: must be a valid reference number of a Tabular or Control Function, if nonzero Default value: 0.1.

..., until the efficiencies are specified for all size sections.

#### MODEL 2 DATA

A correlation is available in to calculate the pool scrubbing efficiency. The correlation is:

$$E_{PS} = A \cdot (1 - \exp[-B \cdot D_p])$$

W-2 (R) :	APLSRT	Coefficient <i>A</i> in the pool scrubbing correlation, (-). Default value provides a conservative (too low) estimation for the pool scrubbing efficiency. The best-estimate value is close to 1.0 (see Volume 1) Acceptable range: $0.0 \le \text{APLSRT} \le 1.0$ Default value: 0.5.
W-3 (R) :	BPLSRT	Coefficient <i>B</i> in the pool scrubbing correlation, (-). Acceptable range: $0.0 \le \text{BPLSRT} \le 1.0 \times 10^{10}$

## 2.15.30 Record: 376XXX, Inertial Impaction Model for 1-D Solid Heat Conductors

*Default value:*  $0.5 \times 10^6$ 

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I): MII1RT(1) Inertial impaction model on the left surface of the 1-D Solid Heat Conductor number XXX.

= 0: no model

< 0: collection efficiency is defined by a Control Function |MII1RT|. The values obtained from the Control Function are limited to the range between 0.0 and 1.0.

0 < MII1RT <1000: collection efficiency is calculated from a general correlation as a function of Stokes number, *Stk*:

$$\eta = f(Stk)$$

The function f is defined using a Tabular Function number MII1RT. The independent variable for the function is the Stokes number.

= 1001: collection efficiency is calculated from the Ciemat correlation [41], appropriate for tube bundle:

$$\eta = \frac{\eta_{\max}}{1 + c_1 \cdot \exp(-c_2 \cdot Stk^{c_3})}$$

Here  $\eta_{\text{max}}$ ,  $c_1$ ,  $c_2$ ,  $c_3$  are user defined coefficients with the default values of 0.75, 29.31, 3.85, and 0.5 respectively. The values are defined in the record 865000. *Stk* is the Stokes number, defined as:

$$Stk = \frac{C_m \cdot \rho_p \cdot d_p^2 \cdot v_g}{18 \cdot \mu_g \cdot D_i}$$

- $C_m$  Cunningham correction factor, (-)
- $\rho_p$  particle desity, (kg/m<sup>3</sup>)
- $d_p$  particle diameter, (m)
- $v_g$  gas velocity at the vicinity of the impactor, (m/s)
- $\mu_g$  gas viscosity, (kg/m/s)

 $D_i$  impactor dimension, (m)

= 1002: collection efficiency is calculated from the correlation appropriate for a tube bend [42]:

$$\eta = \eta_{\max} \cdot (1 - 10^{-c_1 \cdot Stk})$$

Here  $\eta_{\text{max}}$ ,  $c_1$ , are user defined coefficients with the default values of 1.0 and 0.963 respectively. The values are defined in the record 865000.

*Acceptable range:* 1001, 1002, or a valid reference to a TF or a CF. *Default value:* 0

W-2 (I): JII1RT(1) Junction association for the inertial impaction on the left surface. This word determines whether the gas velocity is taken from the CV next to the SC surface or from a junction.

= 0: no junction association, the gas velocity,  $v_{g0}$  (needed to compute the velocity  $v_g$  that is used to calculate the Stokes number), is equal to the gas velocity in the Control Volume next to the SC.

< 0: use junction association defined in the record 371XXX. The gas velocity,  $v_{g0}$  (needed to compute the velocity  $v_g$  that is used to calculate the Stokes number) is taken from the associated junction. If no association is specified in the records 371XXX, the local gas velocity at the SC surface is used.

> 0: reference number of the associated junction. The gas velocity,  $v_{g0}$  is taken from the associated junction.

Acceptable range: $\leq 0$  ar a valid reference to a JNDefault value:0

W-3 (R): FJI1RT(1) Jet energy dissipation factor,  $F_{jet}$ . Used to calculate the gas velocity at the impactor surface. The gas velocity is equal to:

$$v_g = v_{g0} \cdot F_{jet}$$

The jet dissipation factor may be used to account for the decrease of the gas velocity when the impactor is located in some distance from the source.

Acceptable range: $0.0 < FJI1RT(1) \le 10.0$ Default value:1.0

- W-4 (R): DII1RT(1) Impactor dimension,  $D_i$ , (m). The value of  $D_i$  is used to calculate the Stokes number, *Stk. Acceptable range:* DII1RT(1) > 0.0 *Default value:* rectangular: square root of the surface area other: diameter
- W-5 (R) : FRI1RT(1) Fraction of the total inertial impaction deposition caused by the jet coming from the associated junction that is deposited on the left surface of the 1-D Solid Heat Conductor,  $F_{R,i}$ . This input entry allows the user to associate multiple surfaces with the same junction and distribute the total impaction among them. The sum of fractions for a given junction must be not larger than 1.0. *Acceptable range:*  $0.0 < FRI1RT(1) \le 1.0$ *Default value:* 1.0
- W-6 (I): MII1RT(2) Inertial impaction model on the right surface of the 1-D Solid Heat Conductor number XXX. See the description of MII1RT(1) above. *Acceptable range:* 1001, 1002, or a valid reference to a TF or a CF. *Default value:* 0
- W-7 (I):JII1RT(2)Junction association for the inertial impaction on the right surface. See<br/>the description of JII1RT(1) above.<br/>Acceptable range:  $\leq 0$  ar a valid reference to a JN<br/>Default value: 0
- W-8 (R): FII1RT(2) Jet energy dissipation factor,  $F_{jet}$ . See the description of FJI1RT(1) above.

Acceptable range: $0.0 < FJI1RT(2) \le 10.0$ Default value:1.0

W-9 (R) :	FRI1RT(2)	Fraction of the to coming from the surface of the 1-D FRI1RT(1) above.	tal inertial in associated j Solid Heat	mpaction deposition caused by the unction that is deposited on the Conductor, $F_{R,i}$ . See the description	ne jet right on of
		Acceptable range: Default value:	0.0 < FRI11 1.0	$RT(1) \leq 1.0$	
W-9 (R) :	DII1RT(2)	DII1RT(2) Impactor dimension, $D_i$ , (m). Acceptable range: DII1RT(1)		ee the description of DII1RT(1) a > 0.0	bove.
		Default value:	rectangular: other:	: square root of the surface area diameter	

## 2.15.31 Record: 476XXX, Inertial Impaction Model for 2-D Solid Heat Conductors

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	11	Boundary cell num cell range for the in defined by Words $I$ $I1 \le I \le I2$ . Acceptable range: Default value:	aber. Using I1 and I2 (below) the user specifies the nertial impaction model. The inertial impaction data, 3 through 7, will be applied for the boundary cells I, must be an existing boundary cell number. none.
W-2 (I) :	I2	Boundary cell num cell range for the in defined by Words $I$ $I1 \le I \le I2$ . Acceptable range: Default value:	aber. Using I2 and I1 (above) the user specifies the nertial impaction model. The inertial impaction data, 3 through 6, will be applied for the boundary cells I, must be an existing boundary cell number. I2 $\geq$ I1. none.
W-3 (I) :	MII2RT(I)	Inertial impaction Heat Conductor m records 376XXX. Acceptable range: Default value:	model on the boundary surface I of the 2-D Solid umber XXX. See description of MII1RT(1) in the 1001, 1002, or a valid reference to a TF or a CF. 0
W-4 (I) :	JII2RT(I)	Junction association I of the 2-D Solid I records 376XXX. Acceptable range: Default value:	on for the inertial impaction on the boundary surface Heat Conductor. See description of JII1RT(1) in the $\leq 0$ ar a valid reference to a JN 0
W-5 (R) :	FJI2RT(I)	Jet energy dissipat the records 376XX Acceptable range: Default value:	ion factor, $F_{jet}$ . See the description of FJI1RT(1) in X. $0.0 < FJI2RT(I) \le 10.0$ 1.0

W-6 (R) :	DII2RT(I)	Impactor dimension, $D_i$ , (m). See the description of DII1RT(1) in therecords 376XXX.Acceptable range:DII2RT(I) > 0.0Default value:smaller of the cell dimensions
W-7 (R) :	FRI2RT(I)	Fraction of the total inertial impaction deposition caused by the jet coming from the associated junction that is deposited on the boundary surface I of the 2-D Solid Heat Conductor, $F_{R,i}$ . See the description of FRI1RT(1) in the records 376XXX. Acceptable range: $0.0 < \text{FRI2RT(I)} \le 1.0$ Default value: $1.0$

## 2.15.32 Record: 862000, Agglomeration Shape Factors

W-1 (R) :	YSHFRT (1)	Agglomeration sha Acceptable range: Default value:	the factor, $\gamma$ , for aerosols section 1, (-). 1.0 $\leq$ YSHFRT(1) $\leq$ 100.0. 1.0.
W-2 (R) :	YSHFRT (2)	Agglomeration sha Acceptable range: Default value:	the factor, $\gamma$ , for aerosols section 2, (-). $1.0 \leq \text{YSHFRT}(2) \leq 100.0.$ 1.0.

..., until the agglomeration shape factors are specified for all size sections.

#### 2.15.33 Record: 863000, Dynamic Shape Factors

W-1 (R) :	XSHFRT (1)	Dynamic shape factor, $\chi$ , for aerosols section 1, (-). Acceptable range: $1.0 \leq \text{XSHFRT}(1) \leq 100.0$ . Default value: 1.0.
W-2 (R) :	XSHFRT (2)	Dynamic shape factor, $\chi$ , for aerosols section 2, (-). Acceptable range: $1.0 \leq \text{XSHFRT}(2) \leq 100.0$ . Default value: 1.0.

..., until the dynamic shape factors are specified for all size sections.

#### 2.15.34 Record: 864000, Cunningham Slip Correction Factor Model Data

This record defines the coefficients in the Cunningham slip correction factor correlation:

$$C_m = 1 + Kn \cdot [A_1 + A_2 \exp(-A_3 / Kn)]$$

where *Kn* is the Knudsen number.

W-1 (R): A1CMRT Coefficient  $A_1$  in the Cunningham slip correction factor:

*Acceptable range:*  $0.0 \le A1CMRT \le 2.0$ . *Default value:* 1.257.

W-2 (R) :	A2CMRT	Coefficient $A_2$ in the Cunningham slip correction factor:		
		Acceptable range:	$0.0 \le A2CMRT \le 1.0.$	
		Default value:	0.4.	

W-3 (R): A3CMRT Coefficient  $A_3$  in the Cunningham slip correction factor: Acceptable range:  $0.0 \le A3CMRT \le 2.0$ . Default value: 1.1.

#### 2.15.35 Record: 865000, Deposition Model Data

W-1 (I): ITMSRT Thermophoresis model selection:  
=1: use Brock correlation.  
=2: use Ha and Ahmadi correlation.  
=3: use Brock correlation for 
$$Kn \le 0.1$$
, Ha and Ahmadi for  $Kn \ge 0.2$   
(linear interpolation is performed for  $0.1 < Kn < 0.2$ ).  
=4: do not use the thermophoretic deposition model.  
*Acceptable range:* 1, 2, 3, or 4  
*Default value:* 3

W-2 (I): IBLDRT Model selection for the diffusion boundary layer calculation: =-1: use input value TBLDRT (Word 3 below) =+1: use the model based on Sherwood number, *Sh*, correlation. *Sh* is related to  $\delta_{BL}$  by:

$$\delta_{BL} = \frac{D_{hyd}}{Sh}$$

where:

 $D_{hyd}$  - characteristic dimension (assumed equal to the hydraulic diameter, i.e. the forced convection characteristic dimension,  $D_{FC}$  – see sections 2.3.11 word DFCLSC, section 2.3.12 word DFCRSC, and section 2.4.13 word DFCBTC).

The Sherwood number is calculated using the heat and mass transfer analogy ( $Nu \rightarrow Sh, Pr \rightarrow Sc$ ), from the laminar and the turbulent flow correlations:

$$Sh = \begin{cases} C_{lam} & (laminar) \\ C_{tur} Re^{a} Sc^{b} & (turbulent) \end{cases}$$

where *Re*, *Sc*, *Sh* are Reynolds number, particle Schmidt number, and Sherwood number respectively. The constants,  $C_{laun}$ ,  $C_{tur}$ , *a*, *b*, are defined by the words 9, 10, 11, 12, below.

The formula for  $\delta_{BL}$  comes from an assumption that the deposition velocity equals the mass transfer coefficient,  $v = K_m$ , (m/s), calculated for the particle Schmidt number:

$$K_m = \frac{Sh \cdot D_C}{D_{hyd}}$$

where  $D_C$  is the diffusion coefficient (m<sup>2</sup>/s). Therefore:

$$v = K_m = \frac{Sh \cdot D_C}{D_{hyd}} = \frac{D_C}{(D_{hyd} / Sh)}$$

The deposition velocity is equal to  $v=D_C / \delta_{BL}$  (see for example [31], page 8) and therefore  $\delta_{BL} = D_{hyd} / Sh$ . The Reynolds number is taken from the Junction data (with a limit in the RT package the same as in the JN package: *Re<sub>min</sub>*=100.0), while the *Sc* number is calculated from:

$$Sc = \frac{3\pi \ \mu_g^2 \ D_p \ \chi}{k_B \ \rho_g \ T \ C_m}$$

where:

		where:		
		$\mu_g$ gas viscosity	v, (kg/m/s)	
		$D_p$ particle dian	neter, (m)	
		$\chi$ dynamic sha	pe factor, (-)	
		$k_B$ Boltzman co	$(=1.38 \times 10^{-23} (J/K))$	
		$\rho_g$ gas density,	(kg/m <sup>3</sup> )	
		T gas temperat	ture, (K)	
		<i>C</i> <sub>m</sub> Cunningham	n correction factor, (-)	
		The boundary layer thickness, calculated as described above, is limited to by a minimum value of $1.0 \times 10^{-7}$ m, and a maximum value of $1.0 \times 10^{-3}$ m.		
		Acceptable range:	IBLDRT = $-1$ or 1. The value of 1 (correlation) is in effect only for those surfaces which are associated with junctions (see records 371XXX, 471XXX). For surfaces not associated with junctions TBLDRT will be used.	
		Default value:	-1.	
W-3 (R) :	TBLDRT	Diffusion boundary Acceptable range: Default value:	y layer thickness, (m). Used if IBLDRT=-1. $1.0 \times 10^{-7} \le \text{TBLDRT} \le 1.0 \times 10^{-3}$ . $1.0 \times 10^{-5}$ .	
W-4 (I) :	IBLTRT	Model selection fo =-1: use input valu =+1: use the mode	r the thermophoretic boundary layer calculation: the TBLTRT (Word 5 below) l:	
		$\delta_{\scriptscriptstyle B}$	$k_L = \frac{k}{h}$	

where k is the gas thermal conductivity, and h is the heat transfer coefficient. The formula comes from the assumption that the convected

heat, q, is transported through the boundary layer of thickness  $\delta_{BL}$ , through gas conduction:

$$q = \frac{k}{\delta_{BL}} (T - T_{wall})$$

where *T* is the gas temperature and  $T_{wall}$  is the wall surface temperature. The convective heat flux is of course equal to:

$$q = h(T - T_{wall})$$

Therefore the boundary layer thickness is given by  $\delta_{BL} = k/h$ . The heat transfer coefficient is taken from the SC/TC data, with an internal limit imposed by the RT package:  $h_{min}=1.0 \text{ W/m}^2/\text{K}$ . Acceptable range: IBLTRT = -1 or 1. Default value: 1. W-5 (R): TBLTRT Thermophoretic boundary layer thickness, (m). Used if IBLTRT=-1. Acceptable range:  $1.0 \times 10^{-4} \leq \text{TBLDRT} \leq 1.0 \times 10^{-2}$ . 2.0×10<sup>-3</sup>. Default value: W-6 (R): **FSLPRT** Slip correction factor,  $F_{slip}$ , used by the thermophoresis model, Brock correlation. Acceptable range:  $0.0 \leq \text{FSLPRT} \leq 2.0$ . Default value: equal to the coefficient  $A_1$  in the Cunningham slip correction factor (A1CMRT in the record 864000) Thermal accommodation coefficient,  $C_t$ , used by the thermophoresis W-7 (R): CTCORT model, Brock correlation. Acceptable range:  $1.0 \leq \text{CTCORT} \leq 5.0$ . *Default value:* 2.5. W-8 (R): CSCORT Thermal exchange coefficient,  $C_s$ , used by the thermophoresis model, Brock correlation. Acceptable range:  $0.0 \leq \text{CSCORT} \leq 5.0$ . Default value: 1.17. W-9 (R): CSLBRT Constant  $C_{lam}$  in the Sherwood number correlation used to calculate diffusion boundary layer thickness (used when IBLDRT=1). Acceptable range:  $10^{-3} \leq \text{CSLBRT} \leq 10^{3}$ . Default value: 3.656 [14]. W-10(R): CSTBRT Constant  $C_{tur}$  in the Sherwood number correlation used to calculate diffusion boundary layer thickness (used when IBLDRT=1). Acceptable range:  $10^{-3} \leq \text{CSTBRT} \leq 10^3$ . Default value: 0.023 [30]. W-11 (R): ASTBRT Constant a in the Sherwood number correlation used to calculate diffusion boundary layer thickness (used when IBLDRT=1). Acceptable range:  $0.1 \leq \text{ASTBRT} \leq 2.0$ .

*Default value:* 0.8 [30].

- W-12 (R): BSTBRT Constant b in the Sherwood number correlation used to calculate diffusion boundary layer thickness (used when IBLDRT=1). Acceptable range:  $0.1 \leq BSTBRT \leq 2.0$ . Default value: 0.4 [30]. W-13 (I): **IDMSRT** Diffusiophoresis model selection: =1: use differential molecular impact effect in both evaporation and condensation. =2: use differential molecular effect only in case of condensation (MELCOR model, see [35] RN Reference Manual, section 2.4.2.2). =3: do not use the diffusiophoretic deposition model. Acceptable range: 1, 2, or 3.
  - Default value: 1.
- W-14 (R): ATDVRT Constant *A* in the correlation for the turbulent deposition velocity (see Volume 1):

$$v_{D,2}^+ = A \cdot \left(\tau_p^+\right)^2$$

Acceptable range: $0.0 \le \text{ATDVRT} \le 1.0 \times 10^{-3}$ .<br/>(a small number,  $<10^{-50}$ , sets the value to 0).Default value: $4.5 \times 10^{-4}$ .

- IVTDRT W-15 (I): Gas velocity calculation for turbulent deposition. =1: Use the gas velocity at the surface of 1-D or 2-D Solid Heat Conductor. The obtained gas velocity is multiplied by the factor XVT1RT (SC - see records 371XXX) or XVT2RT (TC - see records 471XXX). =2: Use gas velocity in a junction associated with the surface of 1-D or 2-D Solid Heat Conductor if such association exists (see records 371XXX, 471XXX), otherwise use the gas velocity at the surface of 1-D or 2-D Solid Heat Conductor (same as 1). The obtained gas velocity is multiplied by the factor XVT1RT (SC - see records 371XXX) or XVT2RT (TC - see records 471XXX). Acceptable range: 1, 2. Default value: 1
- W-16 (R): EMCIRT Constant  $\eta_{max}$  in the tube bundle (CIEMAT) correlation for the inertial impaction. The inertial impaction model is selected in the records 376XXX and 476XXX. The correlation is:

$$\eta = \frac{\eta_{\max}}{1 + c_1 \cdot \exp(-c_2 \cdot Stk^{c_3})}$$

*Acceptable range:*  $0.0 < \text{EMCIRT} \le 1.0$ *Default value:* 0.75

W-17 (R): C1CIRT Constant  $c_1$  in the tube bundle (CIEMAT) correlation for the inertial impaction.

Acceptable range: $0.0 < C1CIRT \le 1000.0$ Default value:29.31

W-18 (R) :	C2CIRT	Constant $c_2$ in the tube bundle (CIEMAT) correlation for the inertialimpaction.Acceptable range: $0.0 < C2CIRT \le 100.0$ Default value: $3.85$
W-19 (R) :	C3CIRT	Constant $c_3$ in the tube bundle (CIEMAT) correlation for the inertialimpaction.Acceptable range: $0.0 < C3CIRT \le 10.0$ Default value: $0.5$
W-20 (R) :	EBIIRT	Constant $\eta_{\text{max}}$ in the pipe bend correlation for the inertial impaction. The inertial impaction model is selected in the records 376XXX and 476XXX. The correlation is:
		$\eta = \eta_{\max} \cdot (1 - 10^{-c_1 \cdot Stk})$
		Acceptable range: $0.0 < \text{EBIIRT} \le 1.0$ Default value: $1.0$
W-21 (R) :	C1BIRT	Constant $c_1$ in the pipe bend correlation for the inertial impaction.Acceptable range: $0.0 < C1CIRT \le 100.0$ Default value: $0.963$
W-22 (R) :	SFIIRT(1)	Slip factor, <i>S</i> , for aerosol size section 1. Used for the inertial impaction. Used only if there is no association with junction. The associations are specified for each deposition surface in the records 376XX, 476XX (JII1RT, JII2RT). The slip factor is used to calculate the deposition velocity (see Volume 1):
		$v_D = \eta \cdot S \cdot v_g$
		where:Sslip factor SFIIRT(1), (-) $v_g$ gas velocity, (m/s) $\eta$ collection efficiency for the inertial impaction $v_D$ deposition velocity for the inertial impaction:Acceptable range: $0.0 \le SFIIRT(1) \le 10.0$ Default value: $1.0$
W-23 (R) :	SFIIRT(2)	Slip factor, S, for aerosol size section 2. Used for the inertial impaction.See the description above.Acceptable range: $0.0 \le \text{SFIIRT}(2) \le 10.0$ Default value: 1.0

•••

until the slip factors are defined for all aerosol size sections.

#### 2.15.36 Record: 865001, Electrophoretic Deposition - Particle Charge

W-1 (R) : CQEDRT(1) Constant  $C_q$  in the formula for the electric charge, q, of the particle size section 1. The electric charge is calculated from:

$$q = C_q \cdot (D_p \times 10^6)^{x_q}$$

Here  $D_p$  is the particle diameter (m).

An equilibrium (minimum) charge may be approximated by (see Volume 1):

$$q = 3.8 \times 10^{-19} \cdot \sqrt{D_p \times 10^6}$$

This is achieved by setting CQEDRT =  $3.8 \times 10^{-19}$ , XQEDRT = 0.5. An maximum charge may be approximated by (see Volume 1):

$$q = 4.5 \times 10^{-14} \cdot (D_n \times 10^6)^2$$

This is achieved by setting CQEDRT =  $4.5 \times 10^{-14}$ , XQEDRT = 2.0. Acceptable range:  $0.0 \le CQEDRT(1) \le 1.0 \times 10^{6}$ Default value: 0.0

- W-2 (R): XQEDRT(1) Constant  $x_q$  in the formula for the electric charge, q, of the particle size section 1. Acceptable range:  $0.0 \le \text{XQEDRT}(1) \le 10.0$ Default value: 0.0
- W-3 (R) : CQEDRT(2) Constant  $C_q$  in the formula for the electric charge, q, of the particle size section 2. Acceptable range:  $0.0 \le \text{CQEDRT}(2) \le 1.0 \times 10^6$ Default value: 0.0
- W-4 (R): XQEDRT(2) Constant  $x_q$  in the formula for the electric charge, q, of the particle size section 2. Acceptable range:  $0.0 \le \text{XQEDRT}(2) \le 10.0$ Default value: 0.0

•••

until the data is defined for all aerosol size sections.

#### 2.15.37 Record: 865002, Global Activators of Deposition Processes

The aerosol deposition may be deactivated in this record.

W-1 (I): IDEPRT(1) Activator of the aerosol deposition models on the pool surface in all Control Volumes. = -1: Model inactive. No deposition is allowed on the pool in any CV

= +1: Model active. Deposition is allowed on the pool in every CV. *Acceptable range:* -1, +1 *Default value:* +1

- W-2 (I): IDEPRT(2) Activator of the aerosol deposition models on the surface in all 1-D Solid Heat Conductors.
  = -1: Model inactive. No deposition is allowed on any SC.
  = +1: Model active. Deposition is allowed on every SC.
  Acceptable range: -1, +1
  Default value: +1
  W-3 (I): IDEPRT(3) Activator of the aerosol deposition models on the surface in all 2-D Solid
- W-3 (I): IDEPRT(3) Activator of the aerosol deposition models on the surface in all 2-D Solid Heat Conductors.
  = -1: Model inactive. No deposition is allowed on any TC.
  = +1: Model active. Deposition is allowed on every TC.
  Acceptable range: -1, +1
  Default value: +1

#### 2.15.38 Record: 866000, Coagulation Model Data

W-1 (I) :	ICEMRT	Collision efficiency model selection: =1: use Fuchs model, approximate formula ([32], section 4.3). =2: use Fuchs model, exact formula ([32], section 4.3). =3: use Pruppacher and Klett model ([32], section 4.3). <i>Acceptable range:</i> 1, 2, or 3. <i>Default value:</i> 1.
W-2 (I) :	ICBMRT	<ul> <li>Brownian coagulation model selection:</li> <li>=1: use diffusion model ([32], section 4.2.1). The diffusion model is valid for large particles and is therefore not recommended.</li> <li>=2: use slip flow model ([32], section 4.2.3).</li> <li>=3: use Fuchs model ([32], section 4.2.4).</li> <li>Acceptable range: 1, 2, or 3.</li> <li>Default value: 2.</li> </ul>
W-3 (R) :	ETDRRT	Turbulence dissipation rate, applied in the turbulent flow range, $\varepsilon_{TT}$ . The value is used by the turbulent coagulation model. The actual turbulence dissipation rate is calculated from: • Laminar flow, $Re < Re_{lam}$ $\varepsilon_T = 0.0$
		• Turbulent flow, $Re > Re_{tur}$ $\varepsilon_T = \varepsilon_{TT}$

• Transition flow,  $Re_{lam} < Re < Re_{tur}$
$$\varepsilon_{T} = \varepsilon_{TT} \left( 3 - 2 \frac{Re - Re_{lam}}{Re_{tur} - Re_{lam}} \right) \cdot \left( \frac{Re - Re_{lam}}{Re_{tur} - Re_{lam}} \right)^{2}$$

In the transition region the value is calculated using a smooth, third order interpolation. The limiting Reynolds numbers are defined by words 4 and 5 below.

*Acceptable range:*  $0.0 \le \text{ETDRRT} \le 1.0$ . *Default value:* 0.001.

- W-4 (R): RELART Limiting Reynolds number for laminar flow,  $Re_{lam}$ . If a negative number is entered, then the turbulence dissipation rate,  $\varepsilon_T$ , will be constant, and equal to ETDRRT ( $\varepsilon_{TT}$ ) independently of the Reynolds number (as it is in the MELCOR code). The value is used also for the multiplier on the turbulent deposition velocity correlation. *Acceptable range:* 100.0 ≤ RELART ≤ 10,000.0 if positive. *Default value:* 2200.0 ([14], page 7-27).
- W-5 (R): RETURT Limiting Reynolds number for turbulent flow,  $Re_{tur}$ . The value is used for the turbulence dissipation rate and the turbulent deposition velocity calculation. Acceptable range:  $2.0 \times \text{RELART} \le \text{RETURT} \le 50,000.0$ . Default value: 10,000.0 ([14], page 7-27).
- W-6 (R):CSTCRTParticle sticking coefficient. The coagulation kernel, as calculated by<br/>the correlations, is multiplied by this value. The value of CSTCRT may<br/>be set to zero by entering a negative number. CSTCRT of zero will<br/>disable the coagulation model.Acceptable range: $0.0 \le$  CSTCRT  $\le 10.0$ , or CSTCRT < 0.0.<br/>Default value:1.0.
- W-7 (I): ICD1RT Model selection for coagulation of particles deposited on 1-D Solid Heat Conductor surfaces (this coagulation is important in case of resuspension).
  =1: no coagulation of deposited particles.
  =2: coagulation of deposited particles is estimated using the deposited layer thickness and the input parameter XCD1RT (see below).
  Acceptable range: 1 or 2.
  Default value: 2.
- W-8 (R): XCD1RT If coagulation of particles deposited on 1-D Solid Heat Conductor surfaces is selected (ICD1RT=2), than the deposited particles whose size is smaller than the product of the deposited layer thickness and this parameter are transferred to the first size section whose size is larger than this product. The meaning of XCD1RT is illustrated in Figure 2-69. Coagulation into the size section *i* is initiated when the deposited layer thickness, *t*, is larger than XCD1RT ×  $d_i$ :

 $t \ge d_i \times XCD1RT$ 

Here  $d_i$  is the diameter of the section *i*. Coagulation then proceeds with the user-defined rate,  $R_c$  (word RCD1RT, below). Acceptable range:  $0.1 \le \text{XCD1RT} \le 100.0$ . Default value: 1.0.







W-9 (R):

RCD1RT Coagulation rate of particles deposited on 1-D Solid Heat Conductor surfaces,  $R_c$  (1/s). If the condition determined by XCD1RT is fulfilled, the transfer rate from a given size section *i* due to coagulation is calculated from:

$$\frac{dm_i}{dt} = -R_c m_i$$

Acceptable range: $1.0 \times 10^{-10} \le \text{RCD1RT} \le 1.0$ , and<br/> $R_c \ \Delta t \le 100.0$  where  $\Delta t$  is the maximum time stepDefault value: $1.0 \times 10^{-3}$ .

W-10 (I) :	ICD2RT	<ul> <li>Model selection for coagulation of particles deposited on 2-D Solid Heat Conductor surfaces (this coagulation is important in case of resuspension).</li> <li>1: no coagulation of deposited particles.</li> <li>2: coagulation of deposited particles is estimated using the deposited layer thickness and the input parameter XCD2RT (see below).</li> <li>Acceptable range: 1 or 2.</li> <li>Default value: 2.</li> </ul>
W-11 (R) :	XCD2RT	If coagulation of particles deposited on 2-D Solid Heat Conductor surfaces is selected (ICD2RT=2), than all deposited particles whose size is smaller than the product of the deposited layer thickness and this parameter are transferred to the first size section whose size is larger than this product (see description of XCD1RT, above). Acceptable range: $0.1 \leq \text{XCD2RT} \leq 100.0$ . Default value: 1.0.
W-12 (R) :	RCD2RT	Coagulation rate of particles deposited on 2-D Solid Heat Conductor surfaces, $R_c$ (1/s) (see description of RCD1RT, above). Acceptable range: $1.0 \times 10^{-10} \le \text{RCD1RT} \le 1.0$ , and $R_c \Delta t \le 100.0$ where $\Delta t$ is the maximum time step Default value: $1.0 \times 10^{-3}$ .

# 2.15.39 Records: 377XXX, 1-D Solid Heat Conductors Resuspension Model Selection

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	IRM1RT (1)	SC left surface resuspension model. =-2: no resuspension model applied on the left surface. =-1: parametric resuspension model (defined in the records 867000, 868XXX, and 868XXX) is applied on the left surface. > 0: mechanistic model number IRM1RT(1) (defined in the records 8700XX through 8793XX) is applied on the left surface. Acceptable range: $-2 \le \text{IRM1RT}(1) \le +10$ . Default value: IRMGRT (global activator of the resuspension	
		model, record 860000)	
W-2 (R) :	IRM1RT (2)	SC right surface resuspension model. =-2: no resuspension model applied on the right surface. =-1: parametric resuspension model (defined in the records 867000, 868XXX, and 868XXX) is applied on the right surface. > 0: mechanistic model number IRM1RT(2) (defined in the records 8700XX through 8793XX) is applied on the right surface. Acceptable range: $-2 \le IRM1RT(2) \le +10$ . Default value: IRMGRT (global activator of the resuspension model, record 860000)	

# 2.15.40 Records: 477XXX, 2-D Solid Heat Conductors Resuspension Model Selection

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	К	Boundary cell number for the data described by the word 2 below.Acceptable range: $1 \le K \le NBCLTC$ (number of boundary cells).Default value:none.		
W-2 (R) :	IRM2RT	TC, boundary cell K, surface resuspension model.		
	(K)	=-2: no resuspension model applied on the boundary cell K.		
		=-1: parametric resuspension model (defined in the records 867000,		
		868XXX, and 868XXX) is applied on the boundary cell K.		
		> 0: mechanistic model IRM2RT(K) (defined in the records 8700XX)		
		through 8793XX) number is applied on the boundary cell K.		
		Acceptable range: $-2 \leq \text{IRM2RT}(\text{K}) \leq +10$ .		
		Default value: IRMGRT (global activator of the resuspension		
		model, record 860000)		

The data set consisting of the two words described above is repeated until the resuspension model is defined for all desired boundary cells. The data may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 2.

#### 2.15.41 Record: 867000, Parametric Resuspension Model - Main Data

The parametric resuspension model with user-defined coefficients is selected in this record. The resuspension model is selected for each surface of a 1-D Solid Heat Conductor, and each boundary cell of a 2-D Solid Heat Conductor in the records 377XXX and 477XXX respectively. The model coefficients are defined in the records 868XXX and 869XXX, below.

The resuspension can be calculated as a result of:

- Large velocity of the gas flowing along the surface with deposited aerosols. •
- Fast depressurization. •
- A combination of both gas velocity and depressurization rate. •

The resuspension rate is calculated for each process from a linear and power function.

• Velocity-dependent resuspension:

$$R_{v}(t) = C_{1}(v - v_{0}) + C_{2}(v - v_{0})^{x}$$

Depressurization-dependent resuspension: •

$$R_{p}(t) = C_{1} \left(\frac{dp}{dt} - \left(\frac{dp}{dt}\right)_{0}\right) + C_{2} \left(\frac{dp}{dt} - \left(\frac{dp}{dt}\right)_{0}\right)^{x}$$

where:	$R_i$	-	resuspension rate due to process i, (1/s). $R_i = (1/m)(dm/dt)$ , where m is the
			deposited mass (kg).
	v	-	fluid velocity parallel to the deposition surface, (m/s).
	$\mathcal{V}_0$	-	minimum fluid velocity for resuspension, (m/s).
	dp/d	lt -	depressurization rate, (Pa/s) (positive when pressure decreases).
	(dp/d)	$(dt)_0$ -	minimum depressurization rate for resuspension, (Pa/s).
	$C_i$	-	model coefficients, an internal limit is imposed:
			$0.0 \le C_i \le 1.0$ in case of velocity-dependent resuspension,
			$0.0 \le C_i \le 1.0 \times 10^{-3}$ in case of depressurization-dependent resuspension.
	х	-	exponent, $(0.1 < x < 10.0)$ , (-).

The total resuspension rate is obtained from:

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$$R(t) = \left[1.0 - (1.0 - R_{v}(t)) \cdot (1.0 - R_{p}(t))\right] \cdot f(\Delta t, B)$$

1

The term:  $f(\Delta t, B)$  gives decay of the resuspension rate with time, and is approximately proportional to ~  $R_0 \exp(-Bt)$ . The model coefficients can be defined for all size sections, or separately for each aerosol size section, as described in the records 868XXX, 869XXX below.

W-1 (I) :	IRSMRT	Resuspension model selection.
		=0: No resuspension is calculated
		=1: Resuspension is calculated based on gas velocities.
		=2: Resuspension model is calculated based on depressurization rates.

		<ul> <li>=3: Resuspension model is calculated based on both velocities and depressurization rates.</li> <li>Acceptable range: 0, 1, 2, 3.</li> <li>Default value: 0.</li> </ul>
W-2 (I) :	IVELRT	Gas velocity calculation for resuspension. =1: Use the fluid velocity at the surface of 1-D or 2-D Solid Heat Conductor. The obtained fluid velocity is multiplied by the factor XVELRT (next word). =2: Use gas velocity in a junction associated with the surface of 1-D or 2-D Solid Heat Conductor if such association exists (see records 371XXX, 471XXX), otherwise use the fluid velocity at the surface of 1-D or 2-D Solid Heat Conductor (same as 1). The obtained fluid velocity is multiplied by the factor XVELRT (next word). <i>Acceptable range:</i> 1, 2. <i>Default value:</i> 1.
W-3 (I) :	XVELRT	Multiplier for the gas velocity.Acceptable range: $0.0 < \text{XVELRT} \le 1000.0.$ Default value: $1.0.$
W-4 (I) :	IHUMRT	<ul> <li>Option to calculate the relative humidity for resuspension calculation.</li> <li>=1: Use current gas relative humidity at the surface.</li> <li>=2: Use RHUMRT (word 3 below).</li> <li>=3: Use the maximum relative humidity recorded over the calculated time period.</li> <li>=4: Use maximum value of RHUMRT and the maximum relative humidity recorded over the calculated time period.</li> <li>=5: Use time averaged relative humidity over the calculated time period.</li> <li>=6: Use maximum value of RHUMRT and the time averaged relative humidity over the calculated time period.</li> <li>=6: Use maximum value of RHUMRT and the time averaged relative humidity over the calculated time period.</li> <li>Acceptable range: 1, 2, 3, 4, 5, 6.</li> <li>Default value: 5.</li> </ul>
W-5 (R) :	RHUMRT	Relative humidity for resuspension calculation. The use of this word depends on the option specified by IHUMRT, above.Acceptable range: $0.0 \le \text{RHUMRT} \le 1.0$ .Default value: $0.0$ .
W-6 (I) :	IRMTRT	Indicator for calculating decay of the resuspension rate with time. If the gas velocity (or depressurization rate) is constant over a certain period of time, <i>t</i> , then the velocity-induced resuspension rate changes as: $R \sim R_0 \exp(-Bt)$ -1: No model, $R = R_0$ . +1: Model 1, $R \leq R_0$ (see Figure 2-70) +2: Model 2, $R \leq R_0$ ; $R = R_0$ for increasing $R_0$ (see Figure 2-71) <i>Acceptable range:</i> -1, +1 or +2. <i>Default value:</i> +1.

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W-7 (I): BRMTRT Exponent *B* for calculating decay of the resuspension rate with time, (1/s) (see Volume 1) Acceptable range:  $0.0 \le BRMTRT \le 1.0$ . If the model is applied (IRMTRT>0), then BRMTRT>0.0. Default value: 0.1.

**Resuspension Versus Time** Model 1  $R_0 = f(v)$ 0.8 ---*R* for *B*=0.01 *R* for *B*=0.10 R for B=1.00R, [1/s] 0.4 0.2 10 30 40 20*t*, [s]





Figure 2-71 Resuspension versus exposure time – model 2.

#### 2.15.42 Records: 868XXX, Parametric Resuspension Model - V-Coefficients

The model coefficients for the velocity-dependent resuspension are entered in these records. XXX is the aerosol size section number. If XXX > 000, then the set of coefficients defined below is valid for the size section XXX. If XXX = 000, then the set of coefficients defined below is valid for all size sections. The user can define first the set of coefficients for all size sections using the record 868000, and then re-define the coefficients for selected size sections using records 868XXX, with XXX>000.

Note that the re-defining records 868XXX must be placed in the input file below the record 868000. (The data entered in 868000 is immediately assigned to all size sections, so if any previous data for individual size sections were entered, they would be overwritten by the data in the record 868000.)

The minimum velocity for resuspension and the coefficients are obtained as follows:

$$v_{0} = v_{00} + v_{0h}H + v_{0n}n + v_{0T}T$$
  

$$C_{1} = C_{10} + C_{1h}H + C_{1n}n + C_{1T}T$$
  

$$C_{2} = C_{20} + C_{2h}H + C_{2n}n + C_{2T}T$$

where:	H	-	relative humidity, (-)
	n	-	concentration of airborne particles, $(1/m^3)$
	Т	-	temperature, (K)

The resuspension coefficients as well as the limiting velocity depend on the relative humidity gas pressure and temperature. The influence of humidity was observed in resuspension experiments [33]. Mono-layer particles subject to air currents can be resuspended by impaction of other particles [34]. Therefore the influence of airborne particles concentration, n, is present. The resuspension measurements indicate temperature dependency [34], T, which is therefore included. The resuspension behaviour depends on a long term humidity rather than an instantaneous humidity at the moment of resuspension. The user can choose the humidity definition in the record 867000.

W-1 (R) :	VV00RT	$v_{00}$ , (m/s) in the formula for the minimum velocity, $v_0$ .Acceptable range: $0.0 \le VV00RT \le 1000.0$ .Default value: $0.0$ .
W-2 (R) :	VV0HRT	$v_{0h}$ , (m/s) in the formula for the minimum velocity, $v_0$ . <i>Acceptable range:</i> $0.0 \le VV0HRT \le 1000.0$ . <i>Default value:</i> 0.0.
W-3 (R) :	VV0NRT	$v_{0n}$ , (m <sup>4</sup> /s) in the formula for the minimum velocity, $v_0$ . Acceptable range: $-1.0 \times 10^{-3} \le \text{VV0NRT} \le 0.0$ . Default value: 0.0.
W-4 (R) :	VV0TRT	$v_{0T}$ , ((m/s)/K) in the formula for the minimum velocity, $v_0$ . Acceptable range: $-1.0 \le VV0TRT \le 1.0$ . Default value: 0.0.
W-5 (R) :	CV10RT	$C_{10}$ , ((1/s)/(m/s))=(m <sup>-1</sup> ), in the formula for the coefficient $C_1$ . <i>Acceptable range:</i> $0.0 \le \text{CV10RT} \le 1.0 \times 10^{-1}$ . <i>Default value:</i> 0.0.
W-6 (R) :	CV1HRT	$C_{1h}$ , $((1/s)/(m/s))=(m^{-1})$ , in the formula for the coefficient $C_1$ . Acceptable range: $-1.0 \times 10^{-1} \le \text{CV1HRT} \le 0.0$ . Default value: 0.0.
W-7 (R) :	CV1NRT	$C_{1n}$ , $((m^3/s)/(m/s))=(m^2)$ , in the formula for the coefficient $C_1$ . <i>Acceptable range:</i> $0.0 \le \text{CV1NRT} \le 1.0 \times 10^{-7}$ . <i>Default value:</i> 0.0.

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W-8 (R) :	CV1TRT	$C_{1T}$ , ((1/s K)/(m/s))=(m <sup>-1</sup> K <sup>-1</sup> ), in the formula for the coefficient $C_1$ . Acceptable range: $-1.0 \times 10^{-4} \le \text{CV1TRT} \le 1.0 \times 10^{-4}$ . Default value: 0.0.
W-9 (R) :	CV20RT	$C_{20}$ , $((1/s)/(m/s)^x)$ in the formula for the coefficient $C_2$ . Acceptable range: $0.0 \le \text{CV20RT} \le (1.0 \times 10^{-1})^x$ . Default value: 0.0.
W-10 (R) :	CV2HRT	$C_{2h}$ , $((1/s)/(m/s)^x)$ in the formula for the coefficient $C_2$ . Acceptable range: $-(1.0 \times 10^{-1})^x \le \text{CV2HRT} \le 0.0$ . Default value: 0.0.
W-11 (R) :	CV2NRT	$C_{2n}$ , $((m^3/s)/(m/s)^x)$ in the formula for the coefficient $C_2$ . Acceptable range: $0.0 \le \text{CV2NRT} \le 1.0 \times 10^{-6} \times (1.0 \times 10^{-1})^x$ . Default value: 0.0.
W-12 (R) :	CV2TRT	$C_{2T}$ , $((1/s \text{ K})/(\text{m/s})^x)$ in the formula for the coefficient $C_2$ . Acceptable range: $-10^{-3} \times (10^{-1})^x \leq \text{CV2TRT} \leq 10^{-3} \times (10^{-1})^x$ . Default value: 0.0.
W-13 (R) :	XV00RT	x, exponent in the formula for resuspension.Acceptable range: $0.001 \le XV00RT \le 10.0.$ Default value: $3.0.$

### 2.15.43 Records: 869XXX, Parametric Resuspension Model - P-Coefficients

The model coefficients for the depressurization-dependent resuspension are entered in these records. XXX is the aerosol size section number. If XXX > 000, then the set of coefficients defined below is valid for the size section XXX. If XXX = 000, then the set of coefficients defined below is valid for all size sections. The user can define first the set of coefficients for all size sections using the record 869000, and then re-define the coefficients for selected size sections using records 869XXX, with XXX>000. Note that the re-defining records 869XXX must be placed in the input file below the record 869000.

The minimum depressurization rate for resuspension and the coefficients are obtained as follows:

$$\left(\frac{dp}{dt}\right)_0 = \left(\frac{dp}{dt}\right)_{00} + \left(\frac{dp}{dt}\right)_{0h} H + \left(\frac{dp}{dt}\right)_{0n} n + \left(\frac{dp}{dt}\right)_{0T} T$$
$$C_1 = C_{10} + C_{1h} H + C_{1n} n + C_{1T} T$$
$$C_2 = C_{20} + C_{2h} H + C_{2n} n + C_{2T} T$$

where: H - relative humidity, (-) n - concentration of airborne particles, (1/m<sup>3</sup>) T - temperature, (K)

The resuspension coefficients as well as the limiting depressurization rate depend on the relative humidity gas pressure and temperature. The influence of humidity was observed in resuspension

experiments [33]. Mono-layer particles subject to air currents can be resuspended by impaction of other particles [34]. Therefore the influence of airborne particles concentration, n, is present. The resuspension measurements indicate temperature dependency [34], T, which is therefore included. The resuspension behavior depends on a long term humidity rather than an instantaneous humidity at the moment of resuspension. The user can choose the humidity definition in the record 867000.

W-1 (R) :	DP00RT	$(dp/dt)_{00}$ , (Pa/s) in the formula for the minimum depressurization rate, $(dp/dt)_{0.}$ Acceptable range: $0.0 \le \text{DP00RT} \le 1.0 \times 10^6$ .
W-2 (R) :	<b>DP0HRT</b>	<i>Default value:</i> 0.0. $(dp/dt)_{0h}$ , (Pa/s) in the formula for the minimum depressurization rate,
		$(dp/dt)_{0}$ . Acceptable range: $0.0 \le \text{DP0HRT} \le 1.0 \times 10^{6}$ . Default value: $0.0$ .
W-3 (R) :	DPONRT	$(dp/dt)_{0p}$ , $((Pa/s) \cdot m^3)$ in the formula for the minimum depressurization rate, $(dp/dt)_{0}$ . Acceptable range: $-1.0 \le DPONRT \le 0.0$ . Default value: 0.0.
W-4 (R) :	DP0TRT	$(dp/dt)_{0T}$ , ((Pa/s)/K)), in the formula for the minimum depressurization rate, $(dp/dt)_{0}$ . Acceptable range: $-1.0 \times 10^{3} \le \text{DP0TRT} \le 1.0 \times 10^{3}$ . Default value: 0.0.
W-5 (R) :	CP10RT	$C_{10}$ , ((1/s)/(Pa/s))=(Pa <sup>-1</sup> ), in the formula for the coefficient $C_1$ . Acceptable range: $0.0 \le \text{CP10RT} \le 1.0 \times 10^{-3}$ . Default value: 0.0.
W-6 (R) :	CP1HRT	$C_{1h}$ , ((1/s)/(Pa/s))=(Pa <sup>-1</sup> ), in the formula for the coefficient $C_1$ . Acceptable range: $-1.0 \times 10^{-3} \le \text{CP1HRT} \le 0.0$ . Default value: 0.0.
W-7 (R) :	CP1NRT	$C_{1n}$ , ((m <sup>3</sup> /s)/(Pa/s))=(m <sup>3</sup> /Pa), in the formula for the coefficient $C_1$ . <i>Acceptable range:</i> $0.0 \le \text{CP1NRT} \le 1.0 \times 10^{-9}$ . <i>Default value:</i> 0.0.
W-8 (R) :	CP1TRT	$C_{1T}$ , ((1/s K)/(Pa/s))=(Pa <sup>-1</sup> K <sup>-1</sup> ), in the formula for the coefficient $C_1$ . Acceptable range: $-1.0 \times 10^{-6} \le \text{CP1TRT} \le 1.0 \times 10^{-6}$ . Default value: 0.0.
W-9 (R) :	CP20RT	$C_{20}$ , $((1/s)/(Pa/s)^x)$ in the formula for the coefficient $C_2$ . <i>Acceptable range:</i> $0.0 \le CP20RT \le (1.0 \times 10^{-3})^x$ . <i>Default value:</i> 0.0.
W-10 (R) :	CP2HRT	$C_{2h}$ , $((1/s)/(Pa/s)^x)$ in the formula for the coefficient $C_2$ . Acceptable range: $-(1.0 \times 10^{-3})^x \le CP2HRT \le 0.0$ . Default value: 0.0.
W-11 (R) :	CP2NRT	$C_{2n}$ , $((m^3/s)/(Pa/s)^x)$ in the formula for the coefficient $C_2$ .

Acceptable range:  $0.0 \le \text{CP2NRT} \le 10^{-6} \times (1.0 \times 10^{-3})^x$ . Default value: 0.0.

W-12 (R) :	CP2TRT	C <sub>2T</sub> , ((1/s K)/(Pa/s) Acceptable range: Default value:	(x) in the formula for the coefficient $C_2$ . -10 <sup>-3</sup> × (10 <sup>-3</sup> ) <sup>x</sup> ≤ CP2TRT ≤ $10^{-3}$ × (10 <sup>-3</sup> ) <sup>x</sup> . 0.0.
W-13 (R) :	XP00RT	<i>x</i> , exponent in the <i>t</i> <i>Acceptable range:</i> <i>Default value:</i>	formula for resuspension. 0.001 < XP00RT < 10.0. 3.0.

#### 2.15.44 Records: 8700XX, Mechanistic Resuspension - Main Data

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). The resuspension model is selected for each surface of a 1-D Solid Heat Conductor, and each boundary cell of a 2-D Solid Heat Conductor in the records 377XXX and 477XXX respectively.

W-1 (R): CFORRT Coefficient  $C_{f0}$ , (-), in the formula for the frequency of vibration,  $f_0$ :

$$f_0 = C_{f0} \frac{f}{8} \frac{\rho_g V_g^2}{\mu_g}$$

If a negative value of  $C_{f0}$  is entered, then  $f_0$  will be constant and equal to:

 $f_0 = |C_{f0}|$  if  $C_{f0} < 0.0$ 

Acceptable range:	$1.0 \times 10^{-6} \le CFORRT \le 1.0 \times 10^{1}$	if CF0RRT>0.0
	$1.0 \times 10^{-3} \le -CF0RRT \le 1.0 \times 10^{3}$	if CF0RRT<0.0
Default value:	3.33×10 <sup>-3</sup> .	

W-2 (R): XFRRT Power  $x_F$ , (-), in the formula for the resuspension rate,  $R_m(t)$ :

$$R_m(t) = f_0 \exp\left[-\left(\frac{F_{a\tau}}{F_d}\right)^{x_F}\right]$$

Acceptable range:  $0.1 \le \text{CFORRT} \le 100.0$ . Default value: 1.33.

W-3 (R) :

: CHIRRT Constant  $C_{\chi}$ , (-), in the formula for the equivalent spring stiffness  $\chi$ :

$$\chi = C_{\chi} \cdot K^{2/3} \cdot D_{eff,0}^{1/3} \cdot F_a^{1/3}$$

Acceptable range: $0.1 \le \text{CHIRRT} \le 10.0.$ Default value:1.13.

W-4 (R): VIPRRT Poisson's ratio for the particles  $v_p$ , (-). Used to calculate K:

$$K = \frac{4}{3} \left( \frac{1 - v_p^2}{E_p} + \frac{1 - v_s^2}{E_s} \right)^{-1}$$

Acceptable range: $0.1 \le \text{VIPRRT} \le 1.0.$ Default value:0.3.

- W-5 (R): EYPRRT Young modulus for the particles  $E_p$ , (Pa). Used to calculate K: Acceptable range:  $1.0 \times 10^5 \le \text{EYPRRT} \le 1.0 \times 10^{18}$ . Default value:  $1.0 \times 10^{11}$ .
- W-6 (R): VISRRT Poisson's ratio for the surface  $v_s$ , (-). Used to calculate *K*: Acceptable range:  $0.1 \le VISRRT \le 1.0$ . Default value: 0.3.
- W-7 (R): EYSRRT Young modulus for the surface  $E_s$ , (Pa). Used to calculate K: Acceptable range:  $1.0 \times 10^5 \le \text{EYSRRT} \le 1.0 \times 10^{18}$ . Default value:  $1.0 \times 10^{11}$ .
- W-8 (R): CFARRT Constant  $C_{Fa}$ , (-), in the formula for the tangential pull-off force,  $F_{a\tau}$ :

$$F_{a\tau} = C_{Fa} \cdot \frac{F_a^{3/2}}{D_{eff,0}^{1/2} \cdot \chi^{1/2}}$$

The formula is used if a positive value of  $C_{Fa}$  is entered. In such case the ratio between the  $F_{a\tau}$  and the adhesion force,  $F_a$ , is further limited by the input parameters TMNRRT, TMXRRT (records 8791XX), so that:

$$TMNRRT \leq \left(\frac{F_{a\tau}}{F_{a}}\right) \leq TMXRRT$$

If a negative value of  $C_{Fa}$  is entered, then a scaled adhesion force,  $F_a$ , will be used with the scaling factor equal to the absolute value of  $C_{Fa}$ :

$$F_{a\tau} = \left| C_{Fa} \right| \cdot F_a \qquad if \ C_{Fa} < 0.0$$

W-9 (I) :

IVELRT Gas velocity calculation for resuspension.

=1: Use the fluid velocity at the surface of 1-D or 2-D Solid Heat Conductor. The obtained fluid velocity is multiplied by the factor XVELRT (next word).

=2: Use gas velocity in a junction associated with the surface of 1-D or 2-D Solid Heat Conductor if such association exists (see records 371XXX, 471XXX), otherwise use the fluid velocity at the surface of

		<ul> <li>1-D or 2-D Solid Heat Conductor (same as 1). The obtained fluid velocity is multiplied by the factor XVELRT (next word).</li> <li><i>Acceptable range:</i> 1, 2.</li> <li><i>Default value:</i> 1.</li> </ul>
W-10 (I) :	XVELRT	Multiplier for the gas velocity.Acceptable range: $0.0 < \text{XVELRT} \le 1000.0.$ Default value: $1.0.$
W-11 (I) :	IAFRRT	<ul> <li>Adhesion force or surface asperity distribution selection.</li> <li>1: Adhesion force distribution, φ(F<sub>a</sub>), is specified in the records 87YYXX.</li> <li>2: Surface asperity distribution, φ<sub>as</sub>(r<sub>as</sub>), is specified in the records 87YYXX.</li> <li><i>Acceptable range:</i> 1 or 2.</li> <li><i>Default value:</i> 1.</li> </ul>
W-12 (I) :	IDTRRT	Adhesion force distribution type.1:Lognormal distribution2:Tabular distributionAcceptable range:1 or 2.Default value:1.
W-13 (I) :	IDORRT	<ul> <li>Adhesion force distribution option.</li> <li>1: Particle balance separately for each F<sub>a</sub>-section. Adhesion force distribution is used only during deposition, to distribute the newly deposited particles in the appropriate F<sub>a</sub>-sections. During resuspension a balance of particles is considered for each F<sub>a</sub>-section, so the resuspension from a given F<sub>a</sub>-section stops when there are no particles left in this section.</li> <li>2: The same distribution is kept constant throughout the transient. This option is not recommended for general application. It is included mainly for test calculations for comparisons with analytical solutions obtained assuming a fixed adhesion force distribution.</li> <li>Acceptable range: 1 or 2.</li> <li>Default value: 1.</li> </ul>
W-14 (I) :	NSCRRT	Number of $F_a$ -sections (if IAFRRT=1), or $r_{as}$ -sections (if IAFRRT=2), $N_{sec}$ (see Figure 2-72).Acceptable range: $1 \le NSCRRT \le 99$ . The total number of integration points, equal to $NSCRRT \times NJSRRT+1$ , must be not smaller than 3 and not larger than 500.Default value:51 if the adhesive spread, Max(SAMRRT), is $\le 10$ . 99 if the adhesive spread, Max(SAMRRT), is $> 10$ . Note: an uneven number of sections has the advantage of having a middle section with the $F_a$ (or $r_{as}$ ) equal to the mean value.

W-15 (I): NJSRRT Number of integration intervals per single  $F_a$ -section or  $r_{as}$ -section,  $N_i$ , (see Figure 2-72). Acceptable range:  $1 \le NJSRRT \le 5$ . The total number of integration points, equal to NSCRRT×NJSRRT+1, must be not smaller than 3 and not larger than 500. Default value: 1. W-16(R): CUTRRT Cut-off limit for high negative exponents (low resuspension rates). The resuspension rates are proportional to  $R \sim \exp(-Y)$ , where Y is equal to  $(F_{a\tau}/F_d)^{X_F}$ . CUTRRT is the maximum value of Y that is considered in the resuspension calculations. The resuspension rates is set to 0.0 for

those  $F_a$ -sections for which Y > CUTRRT. The value of 20 means practically no cut-off (only the terms  $R < \exp(-20) \sim 10^{-10}$  s are eliminated). The value of 10 means that the terms  $R < \exp(-10) \sim 10^{-5}$ s are eliminated. Those terms give resuspension times of  $\sim 10^5$  s. According to experimental observations such slow resuspension rates are not realistic. CUTRRT is a convenient parameter that can filter out the slow resuspension rates. A discussion of this parameter is found in Volume 3.

*Acceptable range:*  $10.0 \le \text{CUTRRT} \le 20.0$ . *Default value:* 15.0.



Figure 2-72 Lognormal distribution of adhesion forces.

#### 2.15.45 Records: 87YYXX, Mechanistic Resuspension - Adhesion Force Distribution

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). YY is the particle size section. The data entered in these records depend on the value of the indicator IDTRRT (record 8700XX). If the lognormal distribution is used (IDTRRT=1), then only the first two words need to be entered. If the tabular distribution is used (IDTRRT=2), then all words must be entered.

W-1 (I) :	FAMRRT	Mean value of the mean asperity rad distribution for pa equal to zero, th correlations, based <i>Acceptable range:</i> <i>Default value:</i>	a adhesion force $\langle F_a \rangle$ , (N), (if 1 lius $\langle r_a \rangle$ , (m) (if IAFRRT=2) rticles of size section YY. If the mean value is calculated on coefficients entered in the re $0.0 \leq \text{FAMRRT} \leq 1.0$ $1.0 \times 10^{-10} \leq \text{FAMRRT} \leq 1.0$ $0.0 \text{ for } \langle F_a \rangle$ , none for $\langle r_{as} \rangle$ .	IAFRRT=1), or the ) in the lognormal he entered value is from the built-in ecord 8792XX. for $\langle F_a \rangle$ for $\langle r_{as} \rangle$
W-2 (I) :	SAMRRT	Adhesive spread f IAFRRT=1) or the particles of size sec Acceptable range: Default value:	actor in the adhesion force dist e asperity distribution, $\sigma_{as}$ , (-), ction YY. 1.1 $\leq$ SAMRRT $\leq$ 20.0. With SAMRRT=10, the min./r 10 <sup>3</sup> . Thus the adhesive force sp magnitude! For such large sprea $F_a$ -sections is necessary. The number of 99 $F_a$ -sections is se SAMRRT (maximum of all siz (larger than 10.0 - see descri record 8700XX). 4.0.	tribution, $\sigma_a$ , (-), (if (if IAFRRT=2) for max. range is 10 <sup>-3</sup> / pread is 6 orders of ad a large number of refore a maximum elected by default if ze sections) is large ption of NSCRRT,

• <u>If IDTRRT = 2</u>: <u>Tabular distribution</u>

If the tabular distribution is used, the values of  $\langle F_a \rangle$  (or  $\langle r_a \rangle$ ) and  $\sigma_a$ , (or  $\sigma_{as}$ ), defined above, are still used but only to define the  $F_a$ -section (or  $r_{as}$ -section) boundaries and the representative values. The relationships between the section boundaries *A*, *B* (see Figure 2-73) and  $\langle F_a \rangle$ ,  $\sigma_a$ , are:

$$A = \frac{\langle F_a \rangle}{\sigma_a^3} \qquad B = \langle F_a \rangle \cdot \sigma_a^3$$
$$\langle F_a \rangle = (AB)^{1/2} \qquad \sigma_a = \left(\frac{B}{A}\right)^{1/6}$$

The section interval width is equal to:

$$D_{\rm sec} = \exp\left(\frac{\ln(B/A)}{N_{\rm sec}}\right)$$



Figure 2-73 Tabulated distribution of adhesion forces.

Section boundaries:

$$F_{a,\text{sec}}(i+1) = F_{a,\text{sec}}(i) \cdot D_{\text{sec}} = A \cdot D_{\text{sec}}^{i}$$

Representative forces:

$$F_a(i) = \sqrt{F_{a,\text{sec}}(i) \cdot F_{a,\text{sec}}(i+1)}$$

Integration interval:

$$D_{j} = \exp\left(\frac{\ln(B/A)}{N_{\text{sec}} \cdot N_{j}}\right)$$

Integration points:

$$F_{a,j}(j+1) = F_{a,j}(j) \cdot D_j = F_{a,sec}(i) \cdot D_j^{j}$$

For example, if  $\sigma_a = 4.64$ , then  $\sigma_a^3 = 100.0$  and  $A = \langle F_a \rangle \times 10^{-2}$ ,  $B = \langle F_a \rangle \times 10^{+2}$ . If the number of  $F_a$ -sections is assumed as 4,  $N_{sec} = 4$ , then:

- The relative section boundaries,  $F_{a,sec}(i)/\langle F_a \rangle$ , will be equal to:  $10^{-2}$ ,  $10^{-1}$ , 1.0,  $10^{+1}$ ,  $10^{+2}$ .
- The section representative forces,  $F_a(i)/\langle F_a \rangle$ : 3.162×10<sup>-2</sup>, 3.162×10<sup>-1</sup>, 3.162, 3.162×10<sup>+1</sup>.

If the number of integration intervals per  $F_a$ -section is assumed as 3, then:

• The integration point interval "length",  $D_j$ , is equal to 2.154. The integration points,  $F_{aj}(i)/\langle F_a \rangle$ , are: 10<sup>-2</sup>, 2.154×10<sup>-2</sup>, 4.640×10<sup>-2</sup>, 10<sup>-1</sup>, 2.154×10<sup>-1</sup>, ..., etc.

Such distribution is illustrated in Figure 2-73. Values of the distribution function,  $\varphi$ , must be specified in these points as the table FASRRT. The total number of points must be equal to

 $N_{sec} \times N_j + 1$ , in the considered example 13. The value of the function in the boundary points is zero, but it does not necessarily have to be the case.

For the tabulated distribution the value of  $\langle F_a \rangle$  (FAMRRT) is the reference adhesion force.  $\langle F_a \rangle$  and  $\sigma_a$  are used to determine the  $F_a$ -section boundaries and representative values. The value itself is may not be equal to the mean force, since the distribution shape is now determined by the user and in general the mean force for the distribution tabulated by the user will not be identical to the mean force for the lognormal distribution.

W-3 (I) :	FAIRRT (1)	Value of the distribution function at the first point, $\varphi_{a,j}(1) = \varphi(A)$ , N <sup>-1</sup> , (if IAFRRT=1), or $\varphi_{as,j}(1) = \varphi_{as}(A)$ , m <sup>-1</sup> , (if IAFRRT=2) in the tabulated distribution. The distribution is normalized so the values may be scaled by any factor. Acceptable range: $0.0 \leq \text{FAIRRT}(1) \leq 100.0$ . Default value: none.
W-4 (I) :	FAIRRT (2)	Value of the distribution function at the second point, $\varphi_{a,j}(2)$ , N <sup>-1</sup> , (if IAFRRT=1), or $\varphi_{as,j}(2)$ , m <sup>-1</sup> , (if IAFRRT=2) in the tabulated distribution. The distribution is normalized so the values may be scaled by any factor. Acceptable range: $1.0 \times 10^{-10} \le \text{FAIRRT}(2) \le 100.0$ . Default value: none.

... until the full distribution,  $N_{sec} \times N_j + 1$  data points, is entered. Note that the acceptable range starts at 0.0 for the first and the last point only. For all other points the value must be positive, at least  $1.0 \times 10^{-10}$ . The maximum number of data points (array size) is 500, because the maximum  $N_{sec}$  has a maximum of 99 while  $N_j$  a maximum of 5.

#### 2.15.46 Records: 8791XX, Mechanistic Resuspension - Asperity Size Distribution

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01).

W-1 (R): RASRRT Mean asperity radius,  $\langle r_{as} \rangle$ . Used only if the mean adhesion force distribution,  $\varphi_a(F_a)$ , is selected (IAFRRT=1, record 8700XX). If the asperity distribution,  $\varphi_{as}(r_{as})$ , is selected (IAFRRT=2, record 8700XX), then the asperity size radius is defined individually for each size section, in the records 87YYXX. If RASRRT  $\geq 0.0$  then r is assumed to have a lognormal distribution

If RASRRT > 0.0, then  $r_{as}$  is assumed to have a lognormal distribution, with the mean value  $\langle r_{as} \rangle =$  RASRRT and the spread of  $\sigma_{as} =$  SASRRT (Word 7 below). The individual values,  $r_{as}(i)$ , are obtained as follows:

A

Boundaries:

$$=\frac{\langle r_{as}\rangle}{\sigma_{as}^3} \qquad B=\langle r_{as}\rangle\cdot\sigma_{as}^3$$

Section interval width: D

 $D_{\rm sec} = \exp\left(\frac{\ln(B/A)}{N_{\rm sec}}\right)$ 

Section boundaries:

$$r_{as,\text{sec}}(i+1) = r_{as,\text{sec}}(i) \cdot D_{\text{sec}}$$

Representative values of  $r_{as}(i)$ :  $r_{as}(i) = \sqrt{r_{a,sec}(i) \cdot r_{as,sec}(i+1)}$ 

If RASRRT < 0.0, then  $r_{as}$  a single value is used for all  $F_a$ -sections:  $r_{as}(i) = |\text{RASRRT}|.$ 

Acceptable range:  $|RASRRT| \leq 1.0 \times 10^{-4}$ . Default value:

use a small value (  $\leq 10^{-50}$ ) to set RASRRT to zero.  $1.\times10^{-7}$  (based on Reeks and Hall, f'=0.027,  $D_p=10$  $\mu$ m,  $f' \times D_p = 0.027 \times 10 \times 10^{-6}/2$  m).

- W-2 (R): SASRRT Spread factor for the asperity radius distribution,  $\sigma_{as}$ . Used only if the mean adhesion force distribution,  $\varphi_a(F_a)$ , is selected (IAFRRT=1, record 8700XX) and if the mean asperity radius, RASRRT (Word 6 above), is positive value. Acceptable range:  $1.1 \leq \text{SASRRT} \leq 20.0$ . Default value: 4.0.
- Constant  $x_{p,0}$  in the formula for the effective diameter,  $D_{eff,0}$ , (note that W-3 (R): **XPORRT**  $D_{eff,0}$ , is used to calculate the "spring" stiffness and finally the tangential pull-off force - see record 8700XX, W-8: CFARRT):

$$D_{eff,0} = \frac{1}{\frac{1}{x_{p,0}D_p} + \frac{1}{x_{as,0}2r_{as}}}$$

Acceptable range:  $0.1 \leq \text{XPORRT} \leq 1.0 \times 10^{10}$ . *Default value:* 1.0.

- W-4 (R): **XAORRT** Constant  $x_{as,1}$  in the formula for the effective diameter,  $D_{eff,0}$ . Acceptable range:  $0.1 \leq XA0RRT \leq 1.0 \times 10^{10}$ . Default value: 3.0 (a particle typically rests on three asperities)
- W-5 (R): TMNRRT Minimum ratio of the tangential pull-off force,  $F_{a\tau}$ , and the adhesion force,  $F_a$ . Used only if the tangential pull-off force is obtained from the Vainshtein's expression (CFARRT>0.0 - records 8700XX). The ratio of  $F_{a\tau}$  to  $F_a$ , depends on the effective "spring" stiffness, therefore the user must be very careful changing the parameters (CHIRRT, XPORRT, XAORRT). The minimum limit is set to avoid unreasonable values of the pull-off force for some combination of these input parameters. The ratio of the tangential pull-off force and the adhesion force is limited by:

$$TMNRRT \leq \left(\frac{F_{a\tau}}{F_a}\right) \leq TMXRRT$$

Acceptable range:  $1.0 \times 10^{-5} \leq \text{TMNRRT} \leq 5.0$ .  $1.0 \times 10^{-3}$ . Default value:

W-6 (R): TMXRRT Maximum ratio of the tangential pull-off force,  $F_{a\tau}$ , and the adhesion force,  $F_a$ .

Acceptable range:  $2.0 \times \text{TMNRRT} \le \text{TMXRRT} \le 10.0$ . Default value: 1.0.

#### 2.15.47 Records: 8792XX, Mechanistic Resuspension - Adhesion Force Calculation

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). The data specified in this record is used to calculate the mean adhesion forces for each particle size section if they are not given by the user in the record 87YYXX (FAMRRT  $\leq 0.0$ )

W-1 (R): A1ARRT Constant  $A_1$  in the formula for the adhesion force,  $F_{a,1}$ :

*Default value:* 

$$F_{a,1} = \frac{A_1}{R^{x_1}} D_{eff,1}$$

Note that the value of  $A_1$  that gives the same adhesion force as the Vainshtein model for a smooth surface is a function of the parameter  $\Delta \gamma$ (adhesive surface energy,  $J/m^2$ ):

$$A_{1} = \frac{3}{4}\pi \cdot 10^{-9} \cdot \Delta \gamma = 2.356 \times 10^{-9} \cdot \Delta \gamma$$

Reference [33] gives values of  $\Delta \gamma = 0.15$  for graphite particles and 0.56 for alumina particles. The corresponding values of  $A_1$  are  $3.53 \times 10^{-10}$  and  $1.32 \times 10^{-9}$  respectively.

Acceptable range:  $0.0 \le A1ARRT \le 1.0 \times 10^{10}$ . If a negative value is entered, A1ARRT is set to zero. 5.0×10<sup>-10</sup>.

W-2 (R) :X1ARRTConstant 
$$x_1$$
 in the formula for the adhesion force,  $F_{a,1}$ .  
Acceptable range: $0.0 \le X1ARRT \le 10.0$ .  
If a negative value is entered, X1ARRT is set to 0.  
Default value:W-3 (R) :RGHRRTSurface roughness,  $R$ , in the formula for the adhesion force,  $F_{a,1}$ .  
Acceptable range:RGHRRT  $\le 1.0 \times 10^{-4}$ .  
If RGHRRT  $\le 1.0 \times 10^{-4}$ .  
If RGHRRT  $\le 10^{-10}$ , then RGHRRT is set to zero  
(smooth). Smooth surface is recommended if the  
asperity distribution option is used (IAFRRT = 2,  
record 8700XX)  
Default value: $10^{-5}$  if IAFRRT=1 (adhesion force correlations)  
 $0.0$  if IAFRRT=2 (asperity distribution)

W-4 (R) : XP1RRT Constant  $x_{p,1}$  in the formula for the effective diameter,  $D_{eff,1}$ , in the formula for the adhesion force,  $F_{a,1}$ :

$$D_{eff,1} = \frac{1}{\frac{1}{x_{p,1}D_p} + \frac{1}{x_{as,1}2r_{as}}}$$

		Acceptable range: Default value:	$0.1 \le 1.0$ $10^{10}$	XP1RRT $\leq 1.0 \times 10^{10}$ . if IAFRRT=1 (adhesion force correlations) if IAFRRT=2 (asperity distribution)	
W-5 (R) :	XA1RRT	Constant $x_{as,1}$ in the formula for the added <i>Acceptable range: Default value:</i>	the formation $0.1 \le 10^{10}$ 1.0	mula for the effective diameter, $D_{eff,1}$ , in the force, $F_{a,1}$ . XA1RRT $\leq 1.0 \times 10^{10}$ . if IAFRRT=1 (adhesion force correlations) if IAFRRT=2 (asperity distribution)	•
W-6 (R) :	A2ARRT	Constant $A_2$ in the	formu	la for the adhesion force, $F_{a,2}$ :	
		$F_{a,2} = A_2 \cdot j$	f(H)	$\cdot \sigma \cdot D_{_{e\!f\!f,2}}$	
		Acceptable range:	0.0≤ A2AF	A2ARRT $\leq 100.0$ if IAFRRT=1RRT = 0if IAFRRT=2	
		Default value:	If a no 6.28 0.0	egative value is entered, A2ARRT is set to 0. if IAFRRT=1 (adhesion force correlations) if IAFRRT=2 (asperity distribution)	
W-7 (R) :	RHUMRT	Relative humidity, Acceptable range: Default value:	$H, in = 0.0 \le 0.0.$	the formula for the adhesion force, $F_{a,2}$ . RHUMRT $\leq 1.0$ .	
W-8 (R) :	SIGRRT	Surface tension, <i>σ</i> , <i>Acceptable range:</i> <i>Default value:</i>	in the 0.0 ≤ 6.0×1	formula for the adhesion force, $F_{a,2}$ . SIGRRT $\leq 1.0$ . $0^{-2}$ .	
W-9 (R) :	XP2RRT	Constant $x_{p,2}$ in the formula for the add	e form nesion	nula for the effective diameter, $D_{eff,2}$ , in the force, $F_{a,2}$ :	9
		$D_{eff,2} = \frac{1}{x_{p,2}}$	$\frac{1}{\frac{1}{2D_p}}$ +	$\frac{1}{\frac{1}{x_{as,2}2r_{as}}}$	
		Acceptable range: Default value:	0.1 ≤ 1.0.	$XP2RRT \le 1.0 \times 10^{10}.$	
W-10 (R) :	XA2RRT	Constant $x_{as,2}$ in the formula for the adh Acceptable range: Default value: Default value:	the form nesion $0.1 \le 1.0.$ 1.0	mula for the effective diameter, $D_{eff,2}$ , in the force, $F_{a,2}$ . XA2RRT $\leq 1.0 \times 10^{10}$ .	•

W-11 (R): A3ARRT Constant  $A_3$  in the formula for the adhesion force,  $F_{a,3}$ :

$$F_{a,3} = K_E \cdot \frac{A_3 q^2}{[\min(x_E R, D_p)]^2}$$

Acceptable range:
$$0.0 \le A3ARRT \le 1.0$$
if IAFRRT=1A3ARRT = 0if IAFRRT=2Default value: $0.0$ 

- W-12 (R): XE3RRT Constant  $x_E$  in the formula for the adhesion force,  $F_{a,3}$ . Acceptable range:  $0.1 \le XE3RRT \le 10.0$ . Default value: 0.5.
- W-13 (R): CQ3RRT Constant  $C_q$  in the formula for the electric charge, q.

$$q = C_q \cdot (D_p \times 10^6)^{x_q}$$

Here  $D_p$  is the particle diameter (m).

A minimum charge may be approximated by (see Volume 1): CQ3RRT =  $3.8 \times 10^{-19}$ , XQ3RRT = 0.5. A maximum charge may be approximated by: CQ3RRT =  $4.5 \times 10^{-14}$ , XQ3RRT = 2.

If positive CQ3RRT is entered, CQ3RRT and XQ3RRT are used for all size sections. Particle charge may be also defined in the record 865001 where  $C_q$  and  $x_q$  are defined independently for each size section. The section-dependent data from record 865001 is used if CQ3RRT is set to zero.

Acceptable range:  $0.0 \le CQ3RRT \le 1.0 \times 10^6$ . Default value: 0.0

- W-14 (R): XQ3RRT Constant  $x_q$  in the formula for the electric charge, q. If positive CQ3RRT is entered, CQ3RRT and XQ3RRT are used for all size sections. Particle charge may be also defined in the record 865001 where  $C_q$  and  $x_q$  are defined independently for each size section. The section-dependent data from record 865001 is used if CQ3RRT is set to zero. Acceptable range:  $0.0 \le XQ3RRT \le 10.0$ . Default value: 0.0
- W-15 (R): GRVRRT Surface orientation related to the gravity vector,  $\delta_{grav}$ , in the formula for the adhesion force,  $F_{a,4}$ :

$$F_{a,4} = C_4 \cdot \rho_p D_p^3 \cdot \delta_{grav}$$

=-1.0: horizontal surface facing down = 0.0: vertical surface =+1.0: horizontal surface facing up Acceptable range:  $-1.0 \le \text{GRVRRT} \le 1.0$ . Default value: 0.0.

#### 2.15.48 Records: 8793XX, Mechanistic Resuspension - Drag Force Calculation

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01).

W-1 (R): XDRRT Multiplier  $X_d$ , (-), in the formula for the drag force,  $F_d$ :

~

$$F_d = X_d \cdot F_d' = X_d \cdot 8.0 \cdot \frac{\mu_g^2}{\rho_g} \cdot (D_p^+)^2$$

Acceptable range: $0.0 < \text{XDRRT} \le 1000.0$ .Default value:0.3.

W-2 (R): XLRRT Multiplier  $X_L$ , (-), in the formula for the lift force,  $F_L$ . Note that the lift force is not used in the Vainshtein model. In the present resuspension model the lift force may be used if it is activated by the option IDRRT (Word 3 below).

$$F_{L} = X_{L} \cdot \begin{cases} F_{L,Soluni}^{'} = 0.975 \cdot \frac{\mu_{g}^{2}}{\rho_{g}} \cdot (D_{p}^{+})^{3.0} & \text{if} \quad D_{p}^{+} < 8.34 \\ F_{L,Hall}^{'} = 4.215 \cdot \frac{\mu_{g}^{2}}{\rho_{g}} \cdot (D_{p}^{+})^{2.31} & \text{if} \quad D_{p}^{+} > 8.34 \end{cases}$$

Acceptable range: $0.0 < \text{XLRRT} \le 1000.0$ .Default value:1.0.

W-3 (I): IDRRT Option for calculation of  $F_d$  in the resuspension model: =1: Use the drag force,  $F_d$  (calculated with the multiplier XDRRT)  $R_m(t) = f_0 \exp\left[-\left(\frac{F_{a\tau}}{F_d}\right)^{x_F}\right] = f_0 \exp\left[-\left(\frac{F_{a\tau}}{(X_d F_d)}\right)^{x_F}\right]$ =2: Use the lift force,  $F_L$  (calculated with the multiplier XLRRT)  $R_m(t) = f_0 \exp\left[-\left(\frac{F_{a\tau}}{F_L}\right)^{x_F}\right] = f_0 \exp\left[-\left(\frac{F_{a\tau}}{(X_L F_L)}\right)^{x_F}\right]$ =3: Use the sum of  $F_d$  and  $F_L$ :  $R_m(t) = f_0 \exp\left[-\left(\frac{F_{a\tau}}{F_d + F_L}\right)^{x_F}\right] = f_0 \exp\left[-\left(\frac{F_{a\tau}}{(X_d F_d) + (X_L F_L)}\right)^{x_F}\right]$ Acceptable range:  $1 < \text{IDRRT} \le 3$ . Default value: 1.

#### 2.15.49 Records: 8794XX, Mechanistic Resuspension, C1 and C2, All Sections

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). This record defines constants  $C_1$  and  $C_2$  for all size sections. These constants may be defined section-by-section in records 8795XX and 8796XX.

W-1 (R): C1ERRT Constant  $C_1$ , (-), in the extended resuspension model:

$$R_m = f_0 \exp\left[-C_1 \left(\frac{F_{a\tau} - C_2 F_d}{F_d}\right)^{x_F}\right]$$

A limit is imposed on the difference, such that it never becomes negative ( $F_{a\tau} - C_2 \ F_d \ge 0.0$ ). Therefore if  $C_2 \ F_d \ge F_{a\tau}$  the result is independent on the forces and is always equal to:  $f_0 \exp(0) = f_0$ *Acceptable range:*  $1.0 \times 10^{-6} < \text{C1ERRT} \le 1.0 \times 10^{6}$ . *Default value:* 1.0.

W-2 (R): C2ERRT Constant  $C_2$ , (-), in the extended resuspension model. Acceptable range:  $0.0 < C2ERRT \le 1.0 \times 10^6$ . Default value: 0.0.

#### 2.15.50 Records: 8795XX, Mechanistic Resuspension, C1 Per Size Section

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). This record defines constants  $C_1$  section-by-section.

W-1 (R) :	C1ERRT(1)Constant $C_1$ , (-), in the extended resuspension model. Valid for size section 1. Acceptable range: $1.0 \times 10^{-6} < C1ERRT(1) \le 1.0 \times 10^{6}$ .
	Default value: 1.0.
W-2 (R) :	C1ERRT(2)Constant $C_1$ , (-), in the extended resuspension model. Valid for size section 2.
	Acceptable range: $1.0 \times 10^{-6} < \text{C1ERRT}(2) \le 1.0 \times 10^{6}$ . Default value: C1ERRT(1)

until C1ERRT is defined for all size sections. The default value for all size sections > 1 is the value for the size section 1: C1ERRT(1).

#### 2.15.51 Records: 8796XX, Mechanistic Resuspension, C2 Per Size Section

The mechanistic resuspension model data is specified in these records. XX is the model number. Up to 20 models may be used. The model numbers, XX, must be consecutive (starting with 01). This record defines constants  $C_2$  section-by-section.

W-1 (R) :	C2ERRT(1)Constant $C_2$ , (-), in the extended resuspension model. Valid for size section 1.
	Acceptable range: $0.0 < C2ERRT(1) \le 1.0 \times 10^6$ .
	Default value: 0.0.
W-2 (R) :	C2ERRT(2)Constant $C_2$ , (-), in the extended resuspension model. Valid for size section 2.
	Acceptable range: $0.0 < C2ERRT(2) \le 1.0 \times 10^6$ .
	<i>Default value:</i> C2ERRT(1)

. . .

until C2ERRT is defined for all size sections. The default value for all size sections > 1 is the value for the size section 1: C2ERRT(1).

An example input for the resuspension model with tabulates distribution is shown below. The adhesive force distribution corresponds to the one shown in Figure 2-73, with 4  $F_a$ -sections and 3 integration intervals per section. The mean value for each of the 5 particle size sections is calculated internally by the code. The adhesive spread factor is 4.64 for each size section.

MECHANISTIC RESUSPENSION MODEL No. 01 Distribution Cf0 XF Chi Vp Ep Vs Es CFa Ivel 0 0 0 0 0 0 0 0 0 0 Fa Log Opt Nsec Nj 1 2 1 4 3 870001 0 0 Adhesion force distribution Table 

 \*
 Table

 \*
 <Fa> sigma
 1
 2
 3
 4
 5
 6
 7
 8
 9
 10
 11
 12
 13

 870101
 0.0
 4.64
 0.0
 1.0
 5.0
 10.0
 15.0
 15.0
 13.0
 9.0
 4.0
 2.0
 0.0
 \* size section
 1

 870201
 0.0
 4.64
 0.0
 1.0
 5.0
 10.0
 15.0
 15.0
 13.0
 9.0
 4.0
 2.0
 0.0
 \* size section
 1

 870301
 0.0
 4.64
 0.0
 1.0
 5.0
 10.0
 15.0
 15.0
 13.0
 9.0
 4.0
 2.0
 0.0
 \* size section

 870401
 0.0
 4.64
 0.0
 1.0
 5.0
 17.0
 15.0
 13.0
 9.0
 4.0
 2.0
 0.0
 \* size section

 870501 0.0 4.64 0.0 1.0 5.0 10.0 15.0 17.0 15.0 15.0 13.0 9.0 4.0 2.0 0.0 \* size section 5 xp0 xa0 0.0 0.0 \* <Ras> sigma 879101 0.0 4.64 Tmn 0.0 Tmx 0.0 Adhesion force mean value <Fa> calculation - model constants 
 \*
 Van der Waals
 Adsorbed liquid
 Elecrostatic

 \*
 Al
 x1
 R
 xp1
 xa1
 A2
 H
 sig
 xp2
 xa2
 A3
 xE3
 Cq3
 Xq3

 879201
 5.0E-10
 0.0
 1.0E-6
 0.0
 0.0
 0.0
 0.0
 0.0
 9.0E9
 0.5
 3.8E-16
 0.5
 Gravity 0.0 Drag force calculation \* Xd XL ID 879301 0.3 1.0 1 \*\*\*\*\*

Further examples of resuspension models, including the Rock'n Roll Model, the quasi static on/off models (NRG3, NRG4) are discussed in Volume 3.

### 2.15.52 Record: 880000, Fission Product Main Data

The fission product chains considered by the Radioactive Particle Transport (RT) Package are very similar to the isotope chains, used by the Reactor Kinetics (RK) Package. In some cases the fission product chains may duplicate the chains from the RK package (for example the Xe-135 chain). In general, the RK chains include only those isotopes which are important for the reactivity (Xe-135, Sm-149, etc.), while the fission product chains include those isotopes which may be released from the core and thus pose a radioactive threat to the environment. In short, the difference between the isotopes which are used by the RK package and the RT package is that the former are never released from the core, while the latter do not affect the reactivity.

It was decided to adopt this modelling approach, and treat the fission product isotopes separately from the isotopes present within the RK Package for the following reason. The isotopes from the RK Package need to be solved all at once (large matrix), since they are all interconnected through the fission product yields. Only few isotopes are important for the reactivity, therefore the total size of the matrix remains relatively small. The RT package on the other hand considers large amount of short chains, with only the members of one particular chain interacting through the decay process. Therefore each short chain can be solved separately using a small matrix. If those chains were put into the common matrix together with the isotopes affecting the reactivity, a very large matrix would be created.

W-1 (I) :	IMFPRT	Indicator for the initial mass of fission products in the core. =1 : Initial masses are calculated outside SPECTRA (for example by the ORIGEN code) and defined in records 880XXY. =2 : Initial masses are calculated internally by the code, using a user- defined fuel burn-up (Word 6 below). <i>Acceptable range:</i> 1 or 2. <i>Default value:</i> 2.
W-2 (I) :	IBFPRT	Request for built-in isotope data (see section 2.15.111). The entry has ten-digit format: <i>jihgfedcba</i> . For each digit 0 means don't use data. $a\neq 0$ : use built-in data for the 131 isotope chain, (6 isotopes), $b\neq 0$ : use built-in data for the 132 isotope chain (3 isotopes), $c\neq 0$ : use built-in data for the 133/134 isotope chain (9 isotopes), $d\neq 0$ : use built-in data for the 135/136 isotope chain (5 isotopes), $e\neq 0$ : use built-in data for the 137 isotope chain (5 isotopes), $f\neq 0$ : use built-in data for the 138 isotope chain (2 isotopes), $f\neq 0$ : use built-in data for the 85 isotope chain (5 isotopes), $h\neq 0$ : use built-in data for the 90 isotope chain (6 isotopes), $i\neq 0$ : use built-in data for the 106 isotope chain (6 isotopes), $i\neq 0$ : use built-in data for the 106 isotope chain (10 isotopes), $i\neq 0$ : use all built in data for the 1111111111; to use all data except for the 132 chain, enter 11111111111; $Acceptable range: IDITRK \ge 0$ . Default value: 000000000 (10 decay chains are used, NDCHRT=10)
W-3 (R) :	TICMRT	Indicator for the transient calculation of the in-core fission product

masses.

>0.0 : The in-core isotope masses are constant, and equal to the initial masses specified in records 880XXY until the time of scram. The value of TICMRT specifies the time of scram in seconds. After scram (t > TICMRT), the isotope decay is calculated, according to the decay chain data, specified in the records 881XXY. Use of this option means that the reactor is assumed to operate at the full power for t < TICMRT (in-core isotopes are at their equilibrium) and is instantaneously shutdown at t = TICMRT (the isotope production and capture ceases at that time, and only the decay mechanism remains). This option is always available, independently whether the reactor kinetics model is used or not.

 $\leq 0.0$ : The in-core isotope masses are calculated according to the (variable) reactor fission power, obtained from the reactor kinetics model. The source from fission, the radioactive decay, and the neutron capture are taken into account in solving the mass balance. The source from fission is obtained from the Reactor Kinetics Package. This option is available only if the reactor kinetics model is used.

Acceptable range:all real numbers if the reactor kinetics is used.Positive numbers if the reactor kinetics is not used.Default value:0.0 if the reactor kinetics model is used.10<sup>10</sup> if the reactor kinetics model is not used.

W-4 (I): NDFPRT Indicator for normalization of decay yield fractions (see section 2.15.55). If the sum of the decay yield fractions is larger than 1.0, then the fractions will always be normalized, to give the sum of 1.0. If the sum of yield fractions is smaller then 1.0, then the fractions will, or will not be normalized to 1.0, depending on the value of this word.
1 = do not normalize fractions if sum is smaller than 1.0,
2 = normalize fractions if sum is smaller than 1.0.
Acceptable range: 1, 2.
Default value: 1.

- W-5 (I): NCFPRT Indicator for normalization of neutron capture yield fractions (see section 2.15.56). If the sum of the yield fractions is larger than 1.0, then the fractions will always be normalized, to give the sum of 1.0. If the sum of yield fractions is smaller then 1.0, then the fractions will, or will not be normalized to 1.0, depending on the value of this word.
  1 = do not normalize fractions if sum is smaller than 1.0,
  2 = normalize fractions if sum is smaller than 1.0.
  Acceptable range: 1, 2.
  Default value: 1.
- W-6 (R): BNUPRT Fuel burn-up, *B*, (MWd/kg). Used if the initial masses of the fission products need to be calculated by the code (IMFPRT=2 see Word 1 above). The initial masses of fission product masses are calculated by integrating the isotope balance equation over the burn-up time,  $t_B$ , equal to:

$$t_B = \frac{m_{fuel}}{e} \frac{B \cdot 8.64 \times 10^{10}}{Q_R}$$

- $Q_R$  reactor fission power, (W) (PINIRK, see record 751000, section 2.9.5).
- *e* fuel enrichment, (-) (ENRFRT Word 6 below)
- $m_{fuel}$  total mass of fuel (fissile isotopes) in the core, (kg), calculated based on the data from the RK Package, equal to:

$$m_{fuel} = \frac{V_R M_{wf}}{A_v} \cdot \sum_{i \in fis} (N_{f,i})$$

$V_R$	reactor volume, (m <sup>3</sup> ) (RVOLRK, see record 751000,
	section 2.9.5)
$M_{w,f}$	average molar weight of the fuel (AMWFRT -Word 7)
$A_{v}$	Avogadro number (= $6.022 \times 10^{26}$ ), (1/kmol)
$\sigma_{f,,j}$	fission cross section for fissile material $j$ (from the RK
	Package), (barn)
N <sub>f,i</sub>	concentration of fissile material <i>i</i> (from the RK Package),
	$(m^{-3})$
	0.0 < DM

Acceptable range:  $0.0 \le BNUPRT \le 155.0$  [56] Default value: 80.0.

Note: there is an internal limit on  $t_B = 1.0$  s. Therefore reducing BNUPRT below the values corresponding to  $t_B = 1.0$  s will not have any effect on the results. The value of  $t_B$  is printed in the SPECTRA output file below the value of BNUPRT, as BTIMRT:

Reducing the value of BNUPRT further will not have any effect, because with the current value of BNUPRT, BTIMRT is already smaller than 1.0 s.

W-7 (R) :	ENRFRT	Fuel enrichment, e,	, (-). Used if the initial masses of the fission products
		need to be calculate	ed by the code (see Words 1 and 6 above).
		Acceptable range:	$0.01 \leq \text{ENRFRT} \leq 0.99.$
		Default value:	0.05.

- W-8 (R) : AMWFRT Average molar weight of fuel,  $M_{f_i}$  (-). Used if the initial masses of the fission products need to be calculated by the code (see Words 1 and 6 above). *Acceptable range:* 200.0  $\leq$  AMWFRT  $\leq$  250.0. *Default value:* 235.0.
- W-9 (I):ISRGRTGlobal activator of a sorption model on all surfaces of Solid Heat<br/>Conductors (SC/TC).<br/>= 0: The global activator is off. The sorption sorption model may be<br/>specified individually for each SC and TC in the records 395XXX,<br/>495XXX.<br/> $\neq$  0: The sorption set number ISRGRT is activated globally for all SC/TC<br/>surfaces. The sorption model may be changed individually for each SC<br/>and TC in the records 395XXX, 495XXX.<br/>Acceptable range: 0 or a number of an existing sorption set<br/>Default value: 0

W-10 (I) :	IMEART	Acceptance of mass error for Solid Heat Conductors (SC/TC). = 1: Mass error not accepted. Time step reduction is performed. = 2: Mass error is accepted. No time step reduction. Acceptable range: 1 or 2 Default value: 1
W-11 (R) :	AMFPRT	End-of-time-step error correction for fission product masses. $\leq 0.0$ : End-of-time-step error correction is not performed. > 0.0: End-of-time-step error correction is performed. If at the end of time step the relative mass error of fission products is smaller than AMFPRT, then all masses are rescaled to eliminate the mass error made during time step. If the mass error is larger than AMFPRT, an error message is printed and calculations are stopped. Note: mass conservation is possible only if: (1) fission products cannot flow to/from time-dependent CVs (2) there is no sorption on surfaces linked to time-dependent CVs (3) all daughter products of radioactive decay are tracked (full radioactive chains) If (1), (2), or (3) is not fulfilled, AMFPRT should be set to $\leq 0.0$ . Acceptable range: AMFPRT $\leq 1.0$ Default value: 0.0 if (1), (2), or (3) is not fulfilled $10^{-2}$ otherwise
W-12 (I) :	IDESRT	<ul> <li>Indicator on desorption calculations on gas-covered surfaces.</li> <li>= 1: Full calculations. Desorbed masses are taken into account in the fluid flow solution.</li> <li>= 2: Desorbed masses are not taken into account in the fluid flow solution. When large time steps are used, desorption may cause numerical problems. This option may be useful in obtaining fast results if desorption is small and can be neglected.</li> <li>Acceptable range: 1 or 2</li> <li>Default value: 1</li> </ul>

## 2.15.53 Records: F05XXY, Fission Product Data - Isotope Names

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined chains must have higher numbers than the mapped chains. The recommended numbers are XX>20. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (A): NMFPRT User defined name, length up to 7 characters. The name is read as a 7-character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. Examples of the isotope names are: I-131, Xe-131m.
Acceptable range: any string of up to 7 characters.
Default value: 7 "underline" characters: "\_".

# 2.15.54 Records: 880XXY, Fission Product Data – Initial Masses, Molar Weights, etc.

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined chains must have higher numbers than the mapped chains. The recommended numbers are XX>20. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (R) :	XMFPRT	Initial mass of the masses are not cal 880000).	isotope XXY, (kg) in the core. Used if the initial culated by the code, i.e. $IMFPRT = 1$ (see record
		Acceptable range: Default value:	$XMFPRT \ge 0.0.$ 0.0.
W-2 (R) :	WMFPRT	Molar weight of th Acceptable range: Default value:	e isotope XXY, (kg/kmol). $1.0 \leq WMFPRT \leq 250.0.$ available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91).
W-3 (R) :	EBFPRT	Fraction of the dec Acceptable range: Default value:	ay energy carried by the beta particle, $E_{\beta}$ , (-). $0.0 \le \text{EBFPRT} \le 1.0$ . 1.0 - EGFPRT, where EGFPRT is the fraction of energy carried by the gamma radiation, defined below.
W-4 (R) :	EGFPRT	Fraction of the dec Acceptable range: Default value:	ay energy carried by the gamma radiation, $E_{\gamma}$ , (-). $0.0 \le \text{EGFPRT} \le 1.0$ . available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). Each of the built- in isotopes has its default energy fractions. In case of beta decay ( $\beta^-$ ) both beta and gamma fractions are assumed to be 0.5, following [35]. In case of Isomeric Transition (IT) the gamma fraction is of course equal to 1.0. If more than one decay mode is possible (for example Te-131m - Figure 2-83), then the average energy fraction is calculated using the decay yields as weighting factors. For example, Te- 131m experiences $\beta^-$ decay with the yield of $\gamma_d =$ 77.8%, and Isomeric Transition, with the yield of $\gamma_d = 22.2\%$ (Figure 2-83). The average energy fraction is obtained from: $E_{\gamma} = 0.778 \times 0.5 +$ $0.222 \times 1.0 = 0.611$ .
W-5 (R) :	YFFPRT	Average yield of yields are not used external calculation Acceptable range: Default value:	the isotope XXY from fission, $\gamma_f$ , (-). The fission l if the initial masses of isotopes are specified from is (IMFPRT = 1 – see section 2.15.52). $0.0 \le \text{YFFPRT} \le 2.0$ . available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). The built-in fission yields are those for fission of U-235.

#### **Example:**

The following input defines one average yield, appropriate for U-235 (3.513%):

F05371 Kr-88 \* M-core MW beta gamma fission yield 880371 0 88 0.159 0.841 3.513E-02

Using the following inputs, the user may define individual yield fractions, specific to all fissile isotopes in the problem. If the input entries are present, there must be exactly the same values as the number of fissile isotopes (isotopes with positive fission cross section, SFITRK>0.0) present in the RK Package. Zeroes may be entered; in such case the value will be set to the average yield, YFFPRT.

	n the first fissile isotope in the
Reactor Kinetics Package.	
Acceptable range: $0.0 \le \text{YIFPRT}(1) \le 1$	1.0.
Default value: YFFPRT	
W-7 (R): YIFPRT(2) Individual yield of the isotope XXY from	m the second fissile isotope in
W-7 (R): YIFPRT(2) Individual yield of the isotope XXY from the Reactor Kinetics Package.	m the second fissile isotope in
W-7 (R): YIFPRT(2) Individual yield of the isotope XXY from the Reactor Kinetics Package. Acceptable range: $0.0 \le$ YIFPRT(2) $\le 1$	m the second fissile isotope in 1.0.

[...] until the yields are defined for all fissile isotopes.

#### **Example:**

In the example below, the fission yields of Kr-88 are defined. The yields of Kr-88 are equal to:

- U-235: 3.513%
- Pu-239: 1.272%
- Pu-241: 0.9765%

Assuming that all default fuel chains are present, the fissile isotopes are:

• U-233, U-235, U-239, Pu-239, Pu-241.

The following input defines individual yields for the Pu fuels.

 F05371
 Kr-88
 individual fission yields

 \*
 M-core
 MW
 beta
 gamma
 fission yield
 U-233
 U-235
 U-239
 Pu-239
 Pu-241

 880371
 0
 88
 0.159
 0.841
 3.513E-02
 0
 0
 1.272E-02
 9.765E-3

In this case the fission yields for all Uranium isotopes is 3.513E-2. The actual fission yield will be determined based on the current fuel composition, using the values of YIFPRT. The value of YFFPRT is serving only as a definition of the default value. The correctness of input may be checked in the \*.OUT file, where it is printed in the following block:

=RT= INDIVIDUAL FISSION YIELDS FOR 5 DECAY CHAINS

	GLOBAL YFFPRT	INDIVIDUAL F U-233	OR FISSILE I U-235	SOTOPES, YIFPR U-239	T: Pu-239	Pu-241
371 Kr-88	3.51300E-02	3.51300E-02	3.51300E-02	3.51300E-02	1.27200E-02	9.76500E-03

# 2.15.55 Records: 881XXY, Fission Product Data - Decay Data

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined chains must have higher numbers than the mapped chains. The recommended numbers are XX>20. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (R) :	DCFPRT	Decay constant, $\lambda$ , $W$ -3,, to overwribe entered. A zero entries below are out <i>Acceptable range: Default value:</i>	(1/s). NOTE: if the user wishes to define words W-2, te the built-in values, a positive decay constant must entry means this isotope is not radioactive and all the mitted. DCFPRT $\ge 0.0$ available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91).
W-2 (R) :	QSFPRT	Specific decay heat Acceptable range: Default value:	t - heat generated per single decay, $q_d$ , (J). $0.0 \le \text{QSFPRT} \le 1.0 \cdot 10^{-11}$ (note that 1 MeV = $1.602 \cdot 10^{-13}$ J) available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91)
W-3 (I) :	J1	Reference number Acceptable range: Default value:	of the decay product. must be one of the isotopes in the chain XX. none
W-4 (R) :	YDFPRT (J1)	Yield fraction of the This number is internuclide of the isoto a nuclide of the isoto <i>Acceptable range:</i> <i>Default value:</i>	e isotope J1 from decay of XXY, (-). erpreted as a probability of the fact that a decay of a ope Y from the chain XX will result in production of tope J1 from the same chain. YDFPRT $\ge 0.0$ available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). A small number, <10 <sup>-50</sup> , sets the built-in value to 0.0.
W-5 (I) :	J2	Reference number Acceptable range: Default value:	of the decay product. must be one of the isotopes in the chain XX. none.
W-6 (R) :	YDFPRT (J2)	Yield fraction of th This number is inte- nuclide of the isoto a nuclide of the isoto <i>Acceptable range:</i> <i>Default value:</i>	e isotope J2 from decay of XXY, (-). erpreted as a probability of the fact that a decay of a pe Y from the chain XX will result in production of tope J2 from the same chain. YDFPRT $\ge 0.0$ . available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). A small number, <10 <sup>-50</sup> , sets the built-in value to 0.0.

... until all decay products are defined.

Note!

If the sum of all yield fractions is larger than 1.0, then the yield fractions will be normalized, to give

the sum of 1.0. If the sum of all yield fractions is smaller than 1.0, then the yield fractions will not be normalized, unless the normalization is requested by the user, through word 4 in record 880000 (section 2.15.52).

Note!

No individual fission yields are defined for the built-in isotopes, shown in section 2.15.111. However, if mapping from the RK chains (section 2.9.36) to the RT Package is requested (IMAPRK>0), and the first two chains (the <sup>233</sup>U / <sup>235</sup>U fuel chain and the <sup>239</sup>U / <sup>239</sup>Pu / <sup>241</sup>Pu fuel chain) are mapped, then the individual yields are defined for the next three chains: <sup>135</sup>Xe, <sup>149</sup>Sm, and <sup>157</sup>Gd chains, if they are mapped. The individual yields for those three chains are shown in section 2.9.36.

#### 2.15.56 Records: 882XXY, Fission Product Data – Neutron Capture Data

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive, however, if the mapping from RK package is requested (IMAPRK>0), then the user-defined chains must have higher numbers than the mapped chains. The recommended numbers are XX>20. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01). Neutron capture data is not used if the initial masses of isotopes are specified from external calculations (IMFPRT = 1 – see section 2.15.52).

W-1 (R) :	SCFPRT	Microscopic cross isotope XXY. Acceptable range: Default value:	s section for neutron capture, $\sigma_c$ , (barn), for the SCFPRT $\geq 0.0$ . available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91).
W-2 (I) :	J1	Reference number Acceptable range: Default value:	of the capture product. must be one of the isotopes in the chain XX. none.
W-3 (R) :	YCFPRT (J1)	Yield fraction of th This number is int capture by a nuclic production of a nucl Acceptable range: Default value:	e isotope J1 from neutron capture in XXY, (-). terpreted as a probability of the fact that a neutron le of the isotope Y from the chain XX will result in clide of the isotope J1 from the same chain. YCFPRT $\ge 0.0$ . available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). A small number, <10 <sup>-50</sup> , sets the built-in value to 0.0.
W-4 (I) :	J2	Reference number Acceptable range: Default value:	of the capture product. must be one of the isotopes in the chain XX. none.
W-5 (R) :	YCFPRT (J2)	Yield fraction of the isotope J2 from neutron capture in XXY, (-). This number is interpreted as a probability of the fact that a neutron capture by a nuclide of the isotope Y from the chain XX will result in production of a nuclide of the isotope J2 from the same chain. <i>Acceptable range:</i> YCFPRT $\geq 0.0$ .	

```
Default value:
```

available if the built-in isotope data is requested (see Figure 2-83 through Figure 2-91). A small number,  $<10^{-50}$ , sets the built-in value to 0.0.

... until all decay products are defined.

Note!

If the sum of all yield fractions is larger than 1.0, then the yield fractions will be normalized, to give the sum of 1.0. If the sum of all yield fractions is smaller than 1.0, then the yield fractions will not be normalized, unless the normalization is requested by the user, through word 5 in record 880000 (section 2.15.52).

#### 2.15.57 Record: 883000, Definition of Fuel Regions for FP Release

The maximum number of fuel regions is NLOMRT = 200. The total mass of fission products, as specified in the records 880XXY, or calculated internally by the code, is assumed to be located within solid structures – 1-D or 2-D Solid Heat Conductors, representing the fuel. The properties of the fuel regions as well as the distribution (mass fraction) of fission products is specified in this record. This record must be specified if the reactor kinetics is not used. If the reactor kinetics is used and this record is not present, then the mass fractions are assumed to be the same as the fuel temperature weighting factors, defined in the record 791XXX (section 2.9.18).

W-1 (I) :	L1FPRT	Fuel region indicator 1.			
		=1: this fuel region	is represented by a 1-D Solid Heat Conductor,		
		=2: this fuel region is represented by a 2-D Solid Heat Conductor.			
		Acceptable range:	1 or 2 .		
		Default value:	if the reactor kinetics model is used, the default values are equal to the regions indicators ITF1RK, specified for the fuel temperature weighting factor in record 791XXX. In this case the region indicator ITF1RK must refer to a 1-D or 2-D Heat Conductor (=1 or 2).		
W-2 (I) :	L2FPRT	Fuel region indicator 2. Equal to:			
		Reference number of a 1-D Solid Heat Conductor, if $L1FPRT = 1$ ,			
		Reference number of a 2-D Solid Heat Conductor, if $L1FPRT = 2$ .			
		Acceptable range:	Must be a valid reference number of a 1-D or a 2-D Solid Heat Conductor.		
		Default value:	if the reactor kinetics model is used, the default values are equal to the regions indicators ITF2RK, specified for the fuel temperature weighting factor in record 791XXX.		
W-3 (R) :	FRFPRT	Fraction of total m by L1FPRT and L2	ass of fission products present in the region defined 2FPRT.		
		Acceptable range:	$0.0 \le \text{FRFPRT} \le 1.0.$		
		Default value:	if the reactor kinetics model is used, the default values are equal to the fuel temperature weighting factors, WTFRRK, specified in record 791XXX. In		

this case the region indicator ITF1RK must refer to a 1-D or 2-D Heat Conductor (=1 or 2).

W-4 (R): SOVFRT Value of the surface to volume ratio (S/V) for release calculation. The release rates calculated by the CORSOR-M or ARSAP model are multiplied by this value, and divided by the CORSOR-M reference value (see record 890000) or ARSAP reference value (see record 891000). A negative value will disable the use of (S/V) for release calculation (i.e. the CORSOR-M and ARSAP model will be used). Acceptable range:  $10.0 \le \text{SOVFRT} \le 10000.0$ , or SOVFRT < 0.0. Default value:  $2.0/R_f$  for rectangular and cylindrical geometry.  $3.0/R_f$  for spherical geometry, where  $R_f$  is the fuel radius, obtained as the outer radius of the cell: NGFRSC-1, if the gap model is present, or NCELSC-1, if no gap model is present W-5 (I): N1FPRT Boundary cell indicator for cladding failure calculation (see record 883101). The cladding temperature for failure criterion will be taken from the cell N1FPRT of the SC with a reference number L2FPRT (if L1FPRT=1), or from the boundary cell number N1FPRT of the TC with a reference number L2FPRT (if L1FPRT=2). Acceptable range: Must be a boundary cell of a 1-D or a 2-D Solid Heat Conductor. This means: =1 (left) or 2 (right), in case of SC  $=1 \div NBCLTC$ , in case of TC *Default value:* =2, in case of SC (L2FPRT=1), =NBCLTC, in case of TC (L2FPRT=2).

The set of five words defined above is repeated until all fuel regions are described. The total number of entries in this record must be a multiple of 5. If the Reactor Kinetics Package is used, the total number of core regions must be the same as the number of the weighting factors in the Reactor Kinetics Package.

## 2.15.58 Record: 883101, Definition of Cladding Failure Criteria

This record defines the cladding failure criteria to be used for each fuel region, defined in the record 883000. If a cladding failure criterion is used for a given region, then the released fission products are kept within the fuel until the cladding fails. Afterwards they are released to the atmosphere of the Control Volume adjacent to the 1-D or 2-D Solid Heat Conductor representing this fuel region. If a cladding failure criterion is not used for a given region, then the released fission products are instantaneously released to the atmosphere of the Control Volume adjacent to the atmosphere of the Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Control Volume adjacent to the 1-D or 2-D Solid Heat Conductor representing this fuel region.

W-1 (I): ICFCRT(1) Indicator defining the cladding failure criterion for the fuel region 1 (fuel regions are defined in the record 883000).

=0: no cladding failure criterion is used for this region

>0: cladding failure criterion is defined using a Tabular Function with the reference number equal to ICFCRT. The Tabular Function must be defined as to give a failure temperature (K), as a function of an oxidized cladding fraction (-). For example, the following TF:

Oxidized frac.(-)	Failure Temp. (K)
0.00	1300.0
0.50	1000.0
1.00	300.0

defines the failure temperature as equal to 1300 K for un-oxidized cladding, decreasing to 1000.0 K in case of 50% oxidation, and further to 300.0 K in case of full oxidation.

Acceptable range: Must be a valid reference number of a Tabular Function, if non-zero.

Default value: none.

W-2 (I): ICFCRT(2) Indicator defining the cladding failure criterion for the fuel region 2. Acceptable range: Must be a valid reference number of a Tabular Function, if non-zero. Default value: none.

. . until the cladding failure criteria are defined for all fuel regions. (Fuel regions are defined in the record 883000.)

# 2.15.59 Record: 883102, Initial Cladding State

This record defines the initial cladding state for each fuel region, defined in the record 883000. If a cladding failure criterion is used for a given region, then the cladding may be initially intact or failed, depending on the data entered in this record. Typically the cladding is initially intact, however it may be initially failed for example in case of continuation of an earlier calculation (when the initial condition file, \*.ICF, from a previous run is used, the initial cladding state is taken from this file).

W-1 (I): ICFLRT(1) Cladding initial state for the fuel region 1 (fuel regions are defined in the record 883000). =0: intact

=1: failedAcceptable range: 0 or 1.Default value: 0.

### W-2 (I): ICFCRT(2) Cladding initial state for the fuel region 2. *Acceptable range:* 0 or 1. *Default value:* 0.

. . until the cladding initial state is defined for all fuel regions. (Fuel regions are defined in the record 883000.)

## 2.15.60 Record: 8832XX, Definition of Common Fuel Regions for Cladding Failure

XX is the common fuel region for cladding failure (single fuel rod). The region numbers must be consecutive (starting with 01). The common regions are introduced for the following reason. If a fuel rod is represented by several Solid Heat Conductors (there is an axial division of the fuel rods), then cladding failure in only one of these Solid Heat Conductors is needed to release the fission products present in the gap of all other Solid Heat Conductors. Therefore the common fuel regions must reflect the axial nodalization of the fuel rods.

If the SC gap model is used, and the SC fuel regions are defined in the record 340000, the common fuel regions for gap calculations in the SC Package (records 3402XX) must be consistent with the common fuel regions for cladding failure in the RT Package, defined in this record. The maximum number of fuel regions is NLOMRT = 200.

W-1 (I) :	IICFRT(1)	Fuel region number to the common fue belonging to the coregions belonging to <i>Acceptable range:</i> <i>Default value:</i>	r IICFRT(1) (defined in the record 883000) belongs el region XX. Cladding failure in any of the regions mmon region XX results in gap release from all fuel to the common region XX. must be one of the core regions defined in records 883000. XX.
W-2 (I) :	IICFRT(2)	Fuel region number to the common fue belonging to the coregions belonging to <i>Acceptable range:</i> <i>Default value:</i>	r IICFRT(2) (defined in the record 883000) belongs el region XX. Cladding failure in any of the regions mmon region XX results in gap release from all fuel to the common region XX. must be one of the core regions defined in records 883000. none.
W-3 (I) :	IICFRT(3)	Fuel region number to the common fuer belonging to the corregions belonging to <i>Acceptable range:</i> <i>Default value:</i>	r IICFRT(3) (defined in the record 883000) belongs el region XX. Cladding failure in any of the regions mmon region XX results in gap release from all fuel to the common region XX. must be one of the core regions defined in records 883000. none.
$\dots$  until all members of the common fuel regions are defined. The maximum number of fuel regions per a single common fuel region is NLOMRT = 200.

#### 2.15.61 Record: 884XXY, Initial Fractions of Released (Gap) Fission Products

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (R) :	RFRAC(1)	Mass fraction of the fuel region 1.	is e isotope XXY that is initially outside fuel (gap) in $(2 + 2) = (2 + 2)$
		Acceptable range:	$0.0 \leq \text{RFRAC}(1) \leq 1.0.$
		Default value:	0.0.
W-2 (R) :	RFRAC(2)	Mass fraction of th the fuel region 2.	e isotope XXY that is initially outside fuel (gap) in
		Acceptable range:	$0.0 \le \operatorname{RFRAC}(2) \le 1.0.$

... until the released fractions for all fuel regions are defined. (Fuel regions are defined in the record 883000.)

#### 2.15.62 Record: 885000, Release Model Indicator

W-1 (I) :	MFPRRT	Release model indicator.
		= 0: do not apply any release model
		= 1: CORSOR-M model (LWR reactors)
		= 2: ARSAP model (LWR reactors)
		= 3: HTR-FPR model (HTR reactors)
		Acceptable range: 0, 1, 2, 3.
		Default value: 0
W-2 (R) :	CFPRRT	Constant in the HTR-FPR model. Used only if MFPRRT = 3. Acceptable range: $1.0 \le CFPRRT \le 5.0$ Default value: $3.0$

#### 2.15.63 Record: 885XXY, Release Classes

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (I): KFPRRT Release class indicator for the isotope XXY.
=0: do not apply any release model for this isotope.
>0: release class number. A built-in release model, defined in the record 885000 will be used, with the coefficient set applicable for the release class number KFPRRT.
<0: use Control Function number |KFPRRT| to determine the release rate, *R*, (1/s). The release rate is defined as a fraction of the mass that is released per second:

$$R = \frac{1}{m} \frac{dm}{dt}$$

Acceptable range:	must be a valid release class if positive, or a valid
	reference number of a Control Function if negative.
Default value:	available if the built-in isotope data is requested (see
	Figure 2-83 through Figure 2-91).

#### 2.15.64 Record: 886000, Fission Product Condensation

W-1 (I) :	IFPCRT	Fission product vapor condensation indicator. = -1 or 1: inactive. = 2: active. Condensation occurs when vapor pressure exceeds saturation pressure, defined for each vapor class in the records 886XXY. <i>Acceptable range:</i> -1, 1, 2 <i>Default value:</i> 2
W-2 (I) :	IASCRT	Condensation of fission product vapors creates aerosols of the size section IASCRT. Acceptable range: 1, 2,, NSIZRT (see record 861000) Default value: NSIZRT
W-3 (I) :	JASCRT	Coagulation of aerosols created by condensation (section IASCRT). = $-1$ or 1: section IASCRT does not coagulate with other sections = 2: section IASCRT does coagulate with other sections <i>Acceptable range:</i> $-1$ , 1, 2 <i>Default value:</i> $-1$
W-4 (I) :	ISATRT	Saturation pressure calculation option. = 1: saturation pressure, as defined in records 8930XX, is used for every isotope of a given vapor class. For example, suppose the vapor class 4 consists of I-131 and Br-83. With this option the vapor pressure of <u>each</u> <u>isotope</u> may be as high as the saturation pressure for the vapor class 4. This is correct because I-131 and Br-83 are different chemical elements.

Since their properties are considered similar, they are grouped into the same vapor class, thus have the same saturation pressure, defined in 893004. However, the partial pressure of each of these elements is independent and may increase up to the saturation pressure. = 2: saturation pressure, as defined in records 8930XX, is used for total vapor class. For example, suppose the vapor class 4 consists of I-131 and I-133. With this option the total vapor pressure of <u>both isotopes</u> may be as high as the saturation pressure for the vapor class 4. This is correct because I-131 and I-133 are both the same chemical element. *Acceptable range:* 1, 2

Default value:

Note: clealy the saturation pressure treatment is not completely general. For example, neither option would be exactly correct if the vapor calss 4 consisted of I-131, I-133, and Br-83. The default value was chosen to maximize the amount of vapor, which in general is more conservative. If the user wishes to have more appropriate treatment in such case, the best is to create a new vapor class, with properties such as saturation pressure and release coefficient, the same as the vapor class 4, and move Br-83 into this new class.

#### 2.15.65 Record: 886XXY, Fission Product Vapor Pressure and Diffusion Volume

XX is the isotope chain reference number,  $01 \le XX \le 99$ . The chain numbers need not be consecutive. The maximum number of chains is 24. Y is the isotope number within the chain XX. The isotope numbers must be consecutive (starting with 01).

W-1 (I) :	KFPVRT	Indicator defining a =0: do not apply ar will form solid (o become gas. >0: use vapor pres number KFPVRT, Table 2-40. Acceptable range: Default value:	the vapor pressure for the isotope XXY. by vapor pressure model for this isotope. This isotope r liquid) aerosols, but will never be evaporated to ssure coefficient set appropriate for the vapor class defined in the record 8930XX (XX=KFPVRT), see must be a number of an existing release class, defined in the records 8930XX. available if the built-in isotope data is requested.
W-2 (R) :	SGFPRT	Diffusion volume, then the diffusion of atmosphere gas of method, applicable particular element correlations are rea 1):	$\Sigma$ , of the isotope XXY. If a positive value is used, coefficient for fission product vapor diffusion in the E a Control Volume is calculated from the general e for any gas mixture. If the diffusion volume for a or compound is not available, then the following commended to calculate the value of $\Sigma$ (see Volume
		Elements: Compounds: A is the atomic nur The diffusion volue if the diffusion model 256XXX). Acceptable range:	$\Sigma = 2.4 \cdot A^{0.66}$ $\Sigma = 4.2 \cdot A^{0.66}$ mber of the isotope XXY. me is used to calculate diffusion coefficients, needed del is activated for junction flows (IDIFJN=2, record $0.0 \le \text{SGFPRT} \le 1000.0$

*Default value:* 0.0

#### 2.15.66 Record: 8900XX, Fission Product Release Coefficients – CORSOR-M Model

XX is the release class number,  $01 \le XX \le 20$ . The class numbers, XX, must be consecutive. These records define coefficients for the CORSOR-M [35] fission product release model.

Each fission product, which can be released from the fuel and whose release is not determined by a user-defined Control Function, needs to be associated with one of the release class (the associations are specified in the records 883XXX), defined in these records (and 8910XX) as well as one of the fission product vapor class, defined in the records 8930XX. The release classes and the vapor classes are independent, and therefore the same isotope may be associated with a release class and a vapor class with different numbers. The fission product classes are shown in Table 2-40. The coefficients shown in Table 2-42 and Table 2-45 are specified based on reference [35]. For some classes the coefficients were modified, as described in Volume 1. The class numbering from reference [35] was preserved, therefore the release class and the vapor class for a given isotope have the same number. The CORSOR-M release rate given by:

$$R = A \cdot \exp\left(-\frac{B}{T}\right)$$

where: R - release rate, (1/s) A - fractional release rate coefficient, (1/s) B - release constant, (K)

Note that [35] uses somewhat different formulation and units:

$$R = k_0 \cdot \exp\left(-\frac{Q}{RT}\right)$$

where:	R	-	release rate, (1/min)
	$k_0$	-	fractional release rate coefficient, (1/min)
	Q	-	release constant, (kcal/mol)
	R	-	gas constant, equal to 1.987×10 <sup>-3</sup> (kcal/mol/K)

Conversion to the SI units (used by SPECTRA) is quite simple:  $A = k_0 / 60.0$ ,  $B = Q / R = Q / 1.987 \times 10^{-3}$ . The release coefficients from [35] and the conversion to the SI units is shown in Table 2-41. The release rate equations, as applied in SPECTRA (SI units) for 12 release classes, defined following [35], are shown in Table 2-42.

W-1 (R) :	AFPRRT	Fractional release rate, $A$ , (1/s), for the CORSOR-M model, release class XX.				
		Acceptable range: Default value:	$0.0 \le \text{AFPRRT} < 1.0 \times 10^{10}$ . available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default CORSOR-M model coefficients are shown in Table 2-41 and Table 2-42.			
W-2 (R) :	BFPRRT	Release constant, E Acceptable range: Default value:	B, (K), for the CORSOR-M model, release class XX. $0.0 \le BFPRRT < 1.0 \times 10^5$ . available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default			

CORSOR-M model coefficients are shown in Table 2-41 and Table 2-42.

#### W-3 (R): RMINRT Minimum release rate for the release class XX, $R_{min}$ , (1/s). Acceptable range: $0.0 \le \text{RMINRT} \le 1.0 \times 10^{-5}$ . Default value: 0.0.

Delesseries	Marshan damaré farma farma [25]	Default
Release class	Member elements from reference [35]	in SPECTRA
1	<b>Xe</b> , He, Ne, Ar, Kr, Rn, H, N	Xe, Kr
2	<b>Cs</b> , Li, Na, K, Rb, Fr, Cu	Cs, Rb
3	Ba, Be, Mg, Ca, Sr, Ra, Es, Fm	Ba, Sr
4	I, F, CI, Br, At	I, Br
5	<b>Te</b> , O, S, Se, Po	Te, Se
6	Ru, Rh, Pd, Re, Os, Ir, Pt, Au, Ni	Ru, Rh, Pd
7	Mo, V, Cr, Fe, Co, Mn, Nb, Tc, Ta, W	-
8	<b>Ce</b> , Ti, Zr, Hf, Th, Pa, Np, Pu, C	Zr
9	La, Al, Sc, Y, Ac, Pr, Nd, Pm, Sm, Eu, Gd, Tb,	Y
	Dy, Ho, Er, Tm, Yb, Lu, Am, Cm, Bk, Cf	-
10	U	-
11	Cd, Hg, Zn, As, Sb, Pb, Tl, Bi	Sb
12	Sn, Ga, Ge, In, Ag	-

Table 2-40 SPECTRA default fission product classes.

Table 2-41 Built-in release coefficients, CC	RSOR-M modified.
--	------------------

Release class	Member Elements	$A$ , (s <sup>-1</sup> ), (= $k_0 / 60.0$ )	B, (K), (=Q / R)
1	Xe, Kr	$2.00 \times 10^5 / 60.0 = 3.333 \times 10^3$	63.8 / <i>R</i> = 32108.7
2	Cs, Rb	$2.00 \times 10^5 / 60.0 = 3.333 \times 10^3$	63.8 / <i>R</i> = 32108.7
3	Ba, Sr	$9.50 \times 10^6 / 60.0 = 1.583 \times 10^5$	100.2 / <i>R</i> = 50427.8
4	I, Br	$2.00 \times 10^5 / 60.0 = 3.333 \times 10^3$	63.8 / <i>R</i> = 32108.7
5	Te, Se	$2.00 \times 10^5 / 60.0 = 3.333 \times 10^3$	63.8 / <i>R</i> = 32108.7
6	Ru, Rh, Pa	$2.00 \times 10^{10} / 60.0 = 3.333 \times 10^{8}$	152.8 / <i>R</i> = 76899.8
7	(Mo)	$3.00 \times 10^4 / 60.0 = 5.000 \times 10^2$	65.0 / <i>R</i> = 32712.6
8	Zr	$2.67 \times 10^8 / 60.0 = 4.450 \times 10^6$	188.2 / <i>R</i> = 94715.7
9	Y	$1.46 \times 10^7 / 60.0 = 2.433 \times 10^5$	143.1 / <i>R</i> = 72018.1
10	(U)	$1.46 \times 10^7 / 60.0 = 2.433 \times 10^5$	143.1 / <i>R</i> = 72018.1
11	Sb	$7.90 \times 10^3 / 60.0 = 1.317 \times 10^1$	61.4 / <i>R</i> = 30900.9
12	(Ag)	$7.90 \times 10^3 / 60.0 = 1.317 \times 10^1$	61.4 / <i>R</i> = 30900.9

Table 2-42 Release rate formulae, CORSOR-M model, SI units.

Class			A				В			
1:	R	=	3.333E+03	exp	(	-	32108.7	/	Т	)
2:	R	=	3.333E+03	exp	(	-	32108.7	/	Т	)
3:	R	=	1.583E+05	exp	(	-	50427.8	/	Т	)
4:	R	=	3.333E+03	exp	(	-	32108.7	/	Т	)
5:	R	=	3.333E+03	exp	(	-	32108.7	/	Т	)
6:	R	=	3.333E+08	exp	(	-	76899.8	/	Т	)
7:	R	=	5.000E+02	exp	(	-	32712.6	/	Т	)
8:	R	=	4.450E+06	exp	(	-	94715.7	/	Т	)
9:	R	=	2.433E+05	exp	(	-	72018.1	/	Т	)
10:	R	=	2.433E+05	exp	(	-	72018.1	/	Т	)
11:	R	=	1.317E+02	exp	(	-	30900.9	/	Т	)
12:	R	=	1.317E+03	exp	(	_	30900.9	/	Т	)

#### 2.15.67 Record: 890000, CORSOR-M Model Constants

W-1 (R): SOVCRT Reference value for surface to volume ratio  $(S/V)_{CORSOR-M}$  for the CORSOR-M model. The release rates calculated by the CORSOR-M model are multiplied by the actual (S/V) (see record 883000), and divided by the reference value:

 $R = R_{CORSOR-M} \times (S/V) / (S/V)_{CORSOR-M}$ 

Acceptable range: $10.0 \le \text{SOVCRT} \le 10000.0.$ Default value:422.5 [35].

W-2 (I): ITCCRT This word defines how the temperature *T* (needed for the CORSOR-M model release calculation) is obtained.
=1: always use maximum cell temperature of the SC or TC of a given fuel region (SC/TC are assigned to fuel regions in record 883000).
=2: always use cell average temperature of the SC or TC of a given fuel region (SC/TC are assigned to fuel regions in record 883000).
=2: always use cell average temperature of the SC or TC of a given fuel region (SC/TC are assigned to fuel regions in record 883000). *Acceptable range:* 1 or 2. *Default value:* 1.

#### 2.15.68 Record: 8910XX, Fission Product Release Coefficients – ARSAP Model

XX is the release class number,  $01 \le XX \le 20$ . The class numbers, XX, must be consecutive. These records define coefficients for the ARSAP (Advanced Reactor Severe Accident Program) [36] fission product release model.

The ARSAP model is used [36], with the release rate given by:

$$R = \frac{C}{R_g} \cdot \exp\left(-\frac{c_1}{T}\right)$$

R	-	release rate, (1/s)
$C$ , $c_1$	-	coefficients
$R_g$	-	grain size, (m) (RGARRT, record 891000)
Т	-	minimum of the current temperature the FCI temperature, (K)
$T_{FCI}$	-	fuel-cladding interaction (FCI) temperature, (K) (TFCIRT, record 891000)
	R C,c <sub>1</sub> R <sub>g</sub> T T <sub>FCI</sub>	$R - C, c_1 - R_g - T - T_{FCI} - T_{FCI}$

Note that [36] uses somewhat different formulation:

$$R = \frac{1}{R_g} \cdot \exp\left(-\frac{c_1}{T} + c_2\right)$$

In order to be consistent with the formulation of the CORSOR-M model, the above equation has been transformed in SPECTRA. The transformation is simple:  $C = \exp(c_2)$ . The release coefficients from [36] and the conversion to the SI units is shown in Table 2-43. The class numbering scheme from the CORSOR-M model (from [35]) was preserved here to avoid confusion. Therefore the elements shown in Table 2-43 are not in the same order as they are appearing in reference [36]. The release rate equations, as applied in SPECTRA for the 12 release classes, are shown in Table 2-44.

The principal differences between the ARSAP and CORSOR-M models are (apart from different values of coefficients): the use of grain size and the FCI temperature in ARSAP.

W-1 (R) :	CCARRT	Coefficient <i>C</i> , (K), <i>Acceptable range:</i> <i>Default value:</i>	for the ARSAP model, release class XX. $0.0 \le \text{CCARRT} < 1.0 \times 10^{15}$ . available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq$ 0). The default ARSAP model coefficients are shown in Table 2-43
		Confficient (K)	and Table 2-44.
W-2 (K) :	CIARRI	Coefficient <i>c</i> <sub>1</sub> , ( <b>K</b> ), Acceptable range: Default value:	for the ARSAP model, release class XX. $0.0 \le C2ARRT < 1.0 \times 10^6$ . available if at least one chain from the built-in isotope data is requested (IBFPRT $\ne 0$ ). The default ARSAP model coefficients are shown in Table 2-43 and Table 2-44.
W-3 (R) :	RMINRT	Minimum release r Acceptable range: Default value:	ate for the release class XX, $R_{min}$ , (1/s). $0.0 \le \text{RMINRT} \le 1.0 \times 10^{-5}$ . 0.0.

Release class	Elements, [36]	C, (s <sup>-1</sup> ), (=exp(c <sub>2</sub> ))	<b>c</b> <sub>1</sub> , (K)
1	Krypton, Kr	exp(-1.49D+00) = 2.254E-01	37300.0
2	Cesium, Cs	exp( 1.34D+00) = 3.819E+00	43000.0
3	Barium, Ba	exp( -2.20D+00 ) = 1.108E-01	45900.0
4	Iodine, I	exp( 9.36D-01) = 2.550E+00	42100.0
5	Tellurium, Te	exp( 1.19D+00 ) = 3.287E+00	44500.0
6	-	0.0	0.0
7	Molybdenum, Mo	exp( -4.94D+00 ) = 7.155E-03	34900.0
8	Cerium, Ce	exp( 20.20D+00 ) = 5.926E+08	119000.0
9	Neodymium, Nd	exp( 24.00D+00 ) = 2.649E+10	130000.0
10	-	0.0	0.0
11	Antimony, Sb	exp( -1.19D+00 ) = 3.042E-01	41500.0
12	-	0.0	0.0

Table 2-43 Built-in release coefficients, ARSAP [36].

Table 2-44 Release rate formulae, ARSAP model,  $T = Min(T_{fuel}, T_{MCl})$ .

Class			С	c1	
1:	R	= (	2.254E-01 /	Rg ) exp ( - 37300.0 / T	)
2:	R	= (	3.819E+00 /	Rg ) exp ( - 43000.0 / T )	)
3:	R	= (	1.108E-01 /	Rg ) exp ( - 45900.0 / T )	)
4:	R	= (	2.550E+00 /	Rg ) exp ( - 42100.0 / T )	)
5:	R	= (	3.287E+00 /	Rg ) exp ( - 44500.0 / T )	)
6:	R	= (	0.000E+00 /	Rg) exp ( - 0.0 / T )	)
7:	R	= (	7.155E-03 /	Rg ) exp ( - 34900.0 / T )	)
8:	R	= (	5.926E+08 /	Rg ) exp ( -119000.0 / T )	)
9:	R	= (	2.649E+10 /	Rg ) exp ( -130000.0 / T )	)
10:	R	= (	0.000E+00 /	Rg) exp ( - 0.0 / T )	)
11:	R	= (	3.042E-01 /	Rg ) exp ( - 41500.0 / T )	)
12:	R	= (	0.000E+00 /	Rg ) exp ( - 0.0 / T )	)

#### 2.15.69 Record: 891000, ARSAP Model Constants

This record defines constants for the alternative fission product release correlation – ARSAP (Advanced Reactor Severe Accident Program) [36].

W-1 (R): SOVART Reference value for surface to volume ratio  $(S/V)_{ARSAP}$  for the ARSAP model. The release rates calculated by the ARSAP model are multiplied by the actual (S/V) (see record 883000), and divided by the reference value:

 $R = R_{ARSAP} \times (S/V) / (S/V)_{ARSAP}$ 

Acceptable range: $10.0 \le \text{SOVART} \le 10000.0.$ Default value:422.5.

W-2 (R): RGARRT Equiaxed grain size  $R_g$ , (m), for the ARSAP model, all release classes. Acceptable range:  $1.0 \times 10^{-6} \le \text{RGARRT} \le 1.0 \times 10^{-3}$ .

		Default value:	$3.0 \times 10^{-5}$ based on VI and VECTORS tests (see Volume 3), [36] recommends $10^{-5}$ .
W-3 (R) :	TFCIRT	Fuel-cladding inter model, all release c Acceptable range: Default value:	action (FCI) temperature, $T_{FCI}$ , (K), for the ARSAP lasses. 2000.0 $\leq$ TFCIRT $\leq$ 3000. 2500.0 based on VI and VECTORS tests (see Volume 3), [36] recommends 2000.0.
W-2 (I) :	ITCART	This word defines h release calculation) =1: always use ma fuel region (SC/TC =2: always use cell region (SC/TC are Acceptable range: Default value:	how the temperature $T$ (needed for the ARSAP model is obtained. ximum cell temperature of the SC or TC of a given are assigned to fuel regions in record 883000). average temperature of the SC or TC of a given fuel assigned to fuel regions in record 883000). 1 or 2. 1.

#### 2.15.70 Record: 892XXX, Fission Product Release Coefficients – HTR-FPR Model

XXX is the fuel region number,  $001 \le XXX \le 200$ . These records define coefficients for the HTR (High Temperature Reactor) fission product release model. The model is applicable to TRISO particles in graphite matrix, either in pebble bed, or in prismatic block reactors.

W-1 (R):	BTRIRT	Relative burn-up, <i>B</i> , (-). <i>B</i> =0.0: fresh fuel, <i>B</i> =1.0: maximum burn-up, equal to 80,000 MWh/t. Acceptable range: $0.0 \le BTRIRT \le 2.0$ . A warning message is issued if the value is > 1.0.
		Default value: 0.0
W-2 (I) :	ITRIRT	Model determining the failed fraction of TRISO particles. Acceptable range: 1 or a reference to a Control Function Default value: 0.0 = 1 : use built-in correlation, which provides the failed fraction, <i>F</i> , as a function of temperature, <i>T</i> , and fuel burn-up, <i>B</i> (see Volume 1) < 0 : Failed fraction is given by Control Function with the number   ITRIRT  . It must be a 2-D Tabular Function with the first arguments being the temperature ( <i>T</i> ) and the second argument being the the relative burnup ( <i>B</i> ). The values of <i>T</i> and <i>B</i> are those for the fuel region XXX, therefore the same CF may be used for multiple fuel regions. The actual arguments entered for the CF are not used for failed fraction calculation (they will only be used to calculate the value of CF printed in the CF block output). The following limits are set internally on the value obtained from the Control Function: $0.0 \le F(T,B) \le 1.0$ Acceptable range: 1 or reference to a CF Default value: 1

An example of the failure function is shown below.

```
885000 3 * FP release model: HTR-FPR
+
       BTRIRT ITRIRT
               -100 *
892001 1.0
                         Use CF-100 for the fuel region number 1
705100 2-D Tabular Function Defining Failure fraction F(T,B)
       Group Number Fact. Const.
                                  * Type : General TF
700100 1
             5
                     1.0 0.0
       B=0.0 B=0.5 B=1.0
708100 0.0
                0.5
                         1.0
                                   * y-coordinate data points (relative burn-up)
* Arguments
* s : (1)(2)(3)(4) Fact. Const.
                           0.0 * x-argument: dummy argument, for the F\left( T,B\right) calculation it
710100 9 000 1 0 1.0
                                  will be replaced by the temperature of the fuel region
710100 6 101 1 0 1.0
                           0.0 * \text{ uses TF-101 for } y = 0.0
                           0.0 * \text{ uses TF-102 for } y = 0.5
710100 6 102 1 0 1.0
710100 6 103 1 0 1.0
710100 9 000 1 0 1.0
                           0.0 * \text{ uses TF-103 for y} = 1.0
                           0.0 * y-argument: dummy argument, for the F(T,B) calculation it
                                  will be replaced by the relative burn-up in the fuel region
605101 FF(T,B=0.0)
        T (C)
                   FF
600101
        1171.6
                  2.62E-04
600101 1471.2
                                   10<sup>-3</sup>
                  2.64E-04
600101
        1500.4
                  2.77E-04
600101 1537.6
                  2.98E-04
600101 1569.1
                  3.19E-04
        1598.3
600101
                  3.42E-04
                                     5
600101
        1626.6
                  3.69E-04
                                                                    1 .
600101
        1658.1
                  4.03E-04
600101
        1695.3
                  4.48E-04
600101 1728.5
                  4.99E-04
                                FRACTION
                                                                    2
                                                                                    З
600101
        1761.6
                  5.51E-04
        1790.7
600101
                  6.09E-04
                                     2
                  6.72E-04
600101
        1819.8
600101
        1849.8
                  7.39E-04
600101 1878.9
                  8.17E-04
                                              Irradiation-Induced
600101 1916.1
                  9.27E-04
                                PARTICLE
                                              particle failure
(proportional to
                                   10^{-4}
                                              burnup)
605102
        FF(T,B=0.5)
        T (C)
                   FF
600102
        1171.8
                  1.63E-04
600102
                  1.64E-04
        1473.1
                  1.89E-04
600102
        1515.1
                                AILED
                                     5
                                                                   FUEL ELEMENT WITH MAX BURNUP
FUEL ELEMENT WITH MEAN BURNUP
NEW FUEL ELEMENT
600102
        1559.6
                  2.22E-04
        1600.8
600102
                  2.59E-04
600102
       1648.5
                  3.07E-04
600102
        1689.7
                  3.54E-04
                                              Uncoated unanlum due
600102
        1733.4
                  4.19E-04
                                              to manufacturing
        1771.4
                                              defects
600102
                  4.82E-04
                                     2
600102
        1813.4
                  5.65E-04
        1845.8
                  6.26E-04
600102
600102
        1884.6
                  7.08E-04
600102
        1916.1
                  7.79E-04
                                   10^{-5}
                                              1000
                                                                                       1600°C
605103 FF(T,B=1.0)
                                                           1200
                                                                         1400
        T (C)
                   도도
                                                         FUEL TEMPERATURE
600103 1173.1
                  6.12E-05
                  6.12E-05
600103
        1472.7
600103
        1506.6
                  7.70E-05
        1531.6
                  9.13E-05
600103
600103
        1560.7
                  1.10E-04
600103 1588.1
                  1.33E-04
600103
        1613.2
                  1.56E-04
        1645.5
600103
                  1.88E-04
600103
        1676.2
                  2.27E-04
600103
        1701.2
                  2.59E-04
600103 1726.3
                  2.96E-04
```

600103 1753.7 600103 1777.2 3.39E-04 3.80E-04

600103	1807.9	4.37E-04
600103	1838.6	4.98E-04
600103	1866.9	5.56E-04
600103	1891.1	6.14E-04
600103	1917.8	6.76E-04
*		

If the following input parameters are not defined, no diffusion through the intact layer is calculated and the release will be only due to failure fraction. If they are defined, diffusion through the SiC layer will be calculated for the intact particles and will contribute to the total release. The release due to diffusion is calculated as follows:

$$\left(\frac{dM_{FP}}{dt}\right)_{diff} = -\frac{C_{FPR}}{R_{TRISO}} \cdot \frac{M_{FP}}{R_{diff}}$$

The diffusion resistance,  $R_{diff}$ , is given by:

$$R_{diff} = \frac{X_{ker}}{D_{ker}} + \frac{X_{SiC}}{D_{SiC}} + \frac{X_{PyC}}{D_{PyC}}$$

 $C_{FPR}$  constant, (=CFPRRT, record 885000)

- $M_{FP}$  mass of fission product isotope in the kernel of all TRISO particles, (kg)
- $R_{TRISO}$  radius of the kernel of a TRISO particle, (m)
- $D_{ker}$  diffusion coefficient in the fuel kernel, (m<sup>2</sup>/s)
- $X_{ker}$  effective thickness of the kernel, (m) (equal to <sup>1</sup>/<sub>4</sub> of the kernel radius RTRIRT)
- $D_{SiC}$  diffusion coefficient in the SiC layer, (m<sup>2</sup>/s)
- $X_{SiC}$  thickness of the SiC layer, (m), input parameter TTRIRT(1)
- $D_{PyC}$  diffusion coefficient in the PyC layer, (m<sup>2</sup>/s)
- $X_{PyC}$  thickness of the PyC layer, (m), input parameter TTRIRT(2)

W-3 (R) :	RTRIRT	Radius of the kernel of TRISO particle, $R_{TRISO}$ (m).			
		Default value:	250×10 <sup>-6</sup>		
W-4 (I) :	MTRIRT(0)	Material number fo	r the kernel.		
		Acceptable range: Default value:	must be a reference to a material if non-zero none		
W-5 (R) :	TTRIRT(1)	Thickness of the Si	C layer, $X_{TRISO}$ , (m).		
		Acceptable range:	$0.0 < \text{RTRIRT}(1) \le 10^{-3} \text{ m}$		
		Default value:	$35 \times 10^{-6}$ (based on the GEMINI+ design)		
W-6 (I) :	MTRIRT(1)	Material number fo	r the SiC layer.		
		Acceptable range: Default value:	must be a reference to a material if non-zero none		
W-7 (R) :	TTRIRT(2)	Thickness of the Py	$VC$ layer, $X_{PyC}$ , (m).		
		Acceptable range:	$0.0 < \text{RTRIRT}(2) \le 10^{-3} \text{ m}$		
		Default value:	$175 \times 10^{-6}$ (based on the GEMINI+ design)		
W-8 (I) :	MTRIRT(2)	Material number fo	r the PyC layer.		
		Acceptable range: Default value:	must be a reference to a material if non-zero none		

#### 2.15.71 Record: 8930XX, Fission Product Vapor Pressure Coefficients

XX is the vapor class number,  $01 \le XX \le 40$ . The class numbers, XX, must be consecutive. These records define coefficients for the fission product vapor model.

Each fission product, defined in records 880XXY, 881XXX, must be associated with one of the vapor class (the associations are specified in the records 884XXX), specified in these records and one of the fission product release class, specified in the records 8900XX. The vapor classes and the release classes are independent, and therefore the same isotope may be associated with a vapor class and a release class with different numbers. The default release classes and vapor classes, shown in Table 2-42 and Table 2-45, are specified based on reference [35]. The class numbering from reference [35] was preserved; therefore the release class and the vapor class for a given isotope have the same number.

The general formula used to compute the fission product vapor pressure is [35]:

$$\log_{10}(P) = -\frac{A}{T} + B + C \log_{10}(T)$$

P - saturation pressure, (Pa) A, B, C coefficients, T - temperature, (K)

Note that [35] uses pressure in mm Hg:

$$\log_{10}(P'[mmHg]) = -\frac{A'}{T} + B' + C' \log_{10}(T)$$

Conversion to the SI units is quite simple:  $B = B' + \log_{10}(10^5/750) = B' + 2.125$  (A and C remain unchanged: A=A', C=C'). The fission product vapor equations, as applied in SPECTRA (SI units) for 13 vapor classes (first 12 the same as the release classes – see record 8900XX, and the Class 13 - CsI), are shown in Table 2-45.

W-1 (R) :	AFPVRT	Coefficient <i>A</i> , vapor above the temperat	or class XX, coefficient set 1, applied for temperatures ure limit specified by Word 4 below.
		Acceptable range: Default value:	$0.0 \le AFPVRT < 1.0 \times 10^5$ . available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq$ 0). The default model coefficients are shown below.
W-2 (R) :	BFPVRT	Coefficient <i>B</i> , vapor above the temperat	or class XX, coefficient set 1, applied for temperatures ure limit specified by Word 4 below.
		Acceptable range:	$0.0 \le \text{BFPRRT} < 1.0 \times 10^2.$
		Default value:	available if at least one chain from the built-in
			isotope data is requested (IBFPRT $\neq$ 0). The default model coefficients are shown below.

W-3 (R) :	CFPVRT	Coefficient <i>C</i> , vapor above the temperat <i>Acceptable range:</i> <i>Default value:</i>	or class XX, coefficient set 1, applied for temperatures ure limit specified by Word 4 below. $-10.0 < CFPVRT \le 0.0.$ available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default model coefficients are shown below.
W-4 (R) :	TFPVRT	Temperature limit words. This is a lot the coefficients of t the lower limit of the Acceptable range: Default value:	for the coefficient set given by the three preceding wer limit. For the temperatures lower than this limit the previous set are used. For the temperatures below he first set the vapour pressure is equal to zero. $0.0 \le \text{TFPVRT} < 10,000.0.$ available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default model coefficients are shown below.

Up to three sets of coefficients may be entered. The number of entries in this record must be 4 (single set), 8 (two sets), or 12 (three sets). The temperature limit for a given set must be at least 50 K higher than the limit for the previous set.

Class				A		в		с		<b>T-lim</b>
1:	log(P)	=	-	0.0 / T	+	10.00	-	0.00 log(T)	,	T > 273.0
2:	log(P)	=	-	9400.0 / T	+	23.71	-	3.75 log(T)	,	T > 390.0
	log(P)	=	-	6870.8 / T	+	10.12	-	0.00 log(T)	,	т > 1553.0
3:	log(P)	=	-	7836.0 / T	+	8.57	-	0.00 log(T)	,	T > 422.0
4:	log(P)	=	-	3578.0 / T	+	19.84	-	2.51 log(T)	,	T > 273.0
	log(P)	=	-	3205.0 / T	+	25.79	-	5.18 log(T)	,	T > 387.0
	log(P)	=	-	2176.9 / T	+	9.77	-	0.00 log(T)	,	T > 457.0
5:	log(P)	=	-	13940.0 / т	+	25.63	-	3.52 log(T)	,	T > 534.0
6:	log(P)	=	-	33200.0 / т	+	12.73	-	0.00 log(T)	,	T > 1460.0
7:	log(P)	=	-	32800.0 / Т	+	11.80	-	0.00 log(T)	,	т > 1504.0
8:	log(P)	=	-	21570.0 / т	+	10.87	-	0.00 log(T)	,	T > 1032.0
9:	log(P)	=	-	21800.0 / T	+	10.80	-	0.00 log(T)	,	T > 1046.0
10:	log(P)	=	-	32110.0 / Т	+	14.00	-	0.00 log(T)	,	T > 1338.0
11:	log(P)	=	-	13730.0 / т	+	10.55	-	0.00 log(T)	,	T > 666.0
12:	log(P)	=	-	15400.0 / т	+	10.28	-	0.00 log(T)	,	T > 758.0
13:	log(P)	=	-	10420.0 / т	+	21.82	-	3.02 log(T)	,	T > 436.0
	log(P)	=	-	9678.0 / T	+	22.48	-	3.52 log(T)	,	T > 894.0
	log(P)	=	-	7303.9 / T	+	9.71	-	0.00 log(T)	,	т > 1553.0

Table 2-45 Fission product vapour pressures, SI units.

#### 2.15.72 Record: 8931XX, Minimum Half-Life for Vapor Class Isotopes

XX is the vapor class number,  $01 \le XX \le 40$ . The class numbers, XX, must be consecutive. These records define a minimum isotope half-life for a given vapor class.

W-1 (R) :T12MRTThe absolute value T12MRT gives the minimum half-life,  $T_{1/2,min}$  (s), for<br/>vapor class XX. All isotopes that have a half-life shorter than  $T_{1/2,min}$  are<br/>excluded from this class. These isotopes are indicated in the code output<br/>as the class 0. The vapor models, such as adsorption/desorption,<br/>condensation, etc., do not apply to these isotopes. Only the radioactive<br/>decay takes place. If the value is negative then the stable isotopes are<br/>also eliminated from the vapor class XX and moved to the class 0.<br/>
<br/>
Acceptable range:  $-1.0 \times 10^{10} \leq T12MRT < 1.0 \times 10^{10} s$ <br/>
The maximum time step used for an analysis should<br/>not be larger than |T12MRT| (the smallest value of<br/>all vapor classes)<br/>
<br/>
Default value:  $1.0 \times 10^4$  s

For example, let's consider the decay chain 133/134, shown in Figure 2-74. If the default value of  $T12MRT = 10^5$  s (about 1.1 day) is used, then five isotopes are coming into the vapor classes :

• Xe-133m, Xe-133, Cs-133, Cs-134, Ba-134 If T12MRT is set to  $-10^5$  s, then on top of the isotopes for which  $T_{1/2,\min} < 10^5$  s, the stable isotopes, Cs-133 and Ba-134, are also eliminated. The following three isotopes are coming into the vapor classes:



• Xe-133m, Xe-133, Cs-134



#### 2.15.73 Record: 8932XX, Particle Size and Density of Vapor Class Isotopes

XX is the vapor class number,  $01 \le XX \le 40$ . The class numbers, XX, must be consecutive. By default, the fission product isotopes are transported in molecular form, until they are attached to aerosol particles (typical size of aerosol particles is >10<sup>-6</sup> m). With these records the user may define an alternative way of fission product transport, namely they will be transported as small particles (typical size <10<sup>-6</sup> m). The main difference is possibility of sedimentation of particles in the pool and different models for transport to bubbles and aerosol particles (use of Brownian force and inertial impaction rather than use of a Sherwood number correlation - see Volumes 1, 3).

W-1 (R) :	DPFPRT	Particle size of particles of the vapor class XX, (m) Acceptable range: $1.0 \times 10^{-15} \le \text{DPFPRT} < 1.0 \times 10^{-6}$ , if non-zero DPFPRT and RHFPRT must be both zero or both positive. Default value: 0.0 (transport in molecular form)
W-2 (R) :	RHFPRT	Density of particles of the vapor class XX, (kg/m <sup>3</sup> ). Acceptable range: $0.01 \le \text{RHFPRT} < 22,600.0$ , if non-zero DPFPRT and RHFPRT must be both zero or both positive. Default value: $0.0$
W-3 (I) :	VIFPRT	Vertical velocity (m/s) in a stagnant pool, $v_{\infty}$ . Positive velocity means the particles will flow vertically up.   VIFPRT   $\leq 100$ : use constant velocity, equal to VIFPRT VIFPRT> 100: use the correlation:
		$v_{\infty} = \left(\frac{4/3}{C_D} \cdot \frac{Dg(\rho_f - \rho_p)}{\rho_f}\right)^{1/2}$
		g gravity constant, = 9.81 (m/s <sup>2</sup> ) $\rho_p$ particle density, (kg/m <sup>3</sup> )

- $\rho_f$  fluid density, (kg/m<sup>3</sup>)
- *D* particle diameter, (m) =DPFPRT
- $C_D$  drag coefficient

VIFPRT<1000: drag coefficient:  $C_{D,Re\to\infty}$ = VIFPRT-100 VIFPRT=1000: constant drag coeff.:  $C_D$  = const. = VIFPRT-1000 The velocity will be positive (upwards) if the particle density ( $\rho_p$  = RHFPRT) is smaller than the fluid density ( $\rho_f$  = current pool density). Acceptable range: -100.0 $\leq$ VIFPRT(1) $\leq$ +100.0, or +100.0<VIFPRT(1) $\leq$ +200.0 (0.0<C<sub>D,Re $\rightarrow\infty$ </sub> $\leq$ 100.0) +1000.0<VIFPRT(1) $\leq$ +1100.0 (0.0<C<sub>D</sub> $\leq$ 100.0)

*Default value:* = 0.0

Note that if the correlation is used (VIFPRT > 100), then the correlation for small particles may be activated using  $C_{small}$  (CSMLCV, record 161000). The correlation for small particles is:

$$v_{\infty} = \frac{1}{18} \cdot \frac{D_p^2 g(\rho_f - \rho_p)}{\eta_f} \cdot C_{small}$$

#### 2.15.74 Record: 8941XX, Chemical Reactions of Fission Product Vapors – Element A

Fission product chemistry is not implemented in the current code version. The equations shown below will be implemented in a future version.

XX is the vapor class number,  $01 \le XX \le 40$ . These records define combination of masses due to chemical reaction between elements during their release.

The chemical reaction is:

$$nA + mB \leftrightarrow A_n B_m$$

The elements A and B are reacting to form the compound  $A_nB_m$ . All isotopes of the element A and B should be taken into account in defining the reaction. This record defines the isotopes of the element A, as well as the number of moles n, for the reaction that gives source to the class XX.

W-1 (R) :	XACVRT	Number of moles according to the real	of the element $A$ per one mole of the compound, $n$ , action shown above.		
		Acceptable range:	$0.1 \le \text{XACVRT} \le 10.0.$		
		Default value:	available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default model coefficients are shown below.		
			model coefficients are shown below.		
W-2 (I) :	IACVRT(1)	) Reference number release is to be cor class XX.	of the first isotope of the element $A$ , which upon nbined with isotopes of the element $B$ and enter the		
		Acceptable range:	must be a valid reference number XXY, of an isotope, defined in records 880XXY through 884XXY.		
		Default value:	available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq$ 0). The default model coefficients are shown below.		
W-3 (I) :	IACVRT(2	) Reference number release is to be cor class XX.	of the second isotope of the element $A$ , which upon nbined with isotopes of the element $B$ and enter the		
		Acceptable range:	must be a valid reference number XXY, of an isotope, defined in records 880XXY through 884XXY.		
		Default value:	available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq 0$ ). The default model coefficients are shown below.		

..., etc. until all isotopes of the element *A* are defined.

#### 2.15.75 Record: 8942XX, Chemical Reaction of Fission Product Vapors – Element B

Fission product chemistry is not implemented in the current code version. The equations shown below will be implemented in a future version.

XX is the vapor class number,  $01 \le XX \le 40$ . These records define combination of masses due to chemical reaction between elements during their release.

The chemical reaction is:

$$nA + mB \leftrightarrow A_n B_m$$

The elements *A* and *B* are reacting to form the compound  $A_nB_m$ . All isotopes of the element *A* and *B* should be taken into account in defining the reaction. This record defines the isotopes of the element *B*, as well as the number of moles *m*, for the reaction that gives source to the class XX.

W-1 (R) :	XBCVRT	Number of moles of according to the real	of the element <i>B</i> per one mole of the compound, <i>m</i> , action shown above. $0.1 \le \text{VPCVPT} \le 10.0$
		Acceptable range.	$0.1 \ge ADC \vee K1 \ge 10.0$ .
		Dejuun vanue.	isotope data is requested (IBFPRT $\neq$ 0). The default
			model coefficients are shown below.
W-2 (I) :	IBCVRT(1)	Reference number release is to be cor class XX.	of the first isotope of the element $B$ , which upon nbined with isotopes of the element $A$ and enter the
		Acceptable range:	must be a valid reference number XXY, of an
			isotope, defined in records 880XXY through 884XXY.
		Default value:	available if at least one chain from the built-in isotope data is requested (IBFPRT $\neq$ 0). The default model coefficients are shown below.
W-3 (I) :	IBCVRT(2)	Reference number	of the second isotope of the element $B$ , which upon which with isotopes of the element $A$ and enter the
		class XX.	notified with isotopes of the element A and enter the
		Acceptable range:	must be a valid reference number XXY, of an isotope, defined in records 880XXY through 884XXY.
		Default value:	available if at least one chain from the built-in
			isotope data is requested (IBFPRT $\neq$ 0). The default model coefficients are shown below.

 $\ldots$ , etc. until all isotopes of the element *B* are defined.

As an example the following chemical reaction is defined:

$$Cs + I = CsI$$

The reaction is defined for all built-in isotopes of Cs and I:

Cs: Cs-133, Cs-135, Cs-137
I: I-131, I-132, I-133, I-134, I-135

The input data defining this reaction is shown in Table 2-46. The reference numbers for all built-in isotopes are listed in Table 2-47.

Table 2-46 Input defining class combination for CsI, for the built-in isotopes.

```
* Class 13, element A:
                          Cs-131 Cs-133 Cs-135
                     n
894113
                     1.0
                            037
                                   054
                                          072
                          I-131 I-132 I-133
* Class 13, element B:
                     m
                                               T-134
                                                        T-135
894213
                     1.0
                            014
                                   022
                                          034
                                                 042
                                                        051
```

#### 2.15.76 Record: 8943XX, Chemical Reaction Kinetics

Fission product chemistry is not implemented in the current code versions. The equations shown below will be implemented in the future version.

XX is the vapor class number,  $01 \le XX \le 40$ . The class numbers, XX, must be consecutive. These records define the kinetics of the chemical reaction, defined in the records 8941XX and 8942XX. The reaction kinetics is given by:

$$\frac{d[A_n B_m]}{dt} = R_{for}(T) \cdot [A] \cdot [B] - R_{rev}(T) \cdot [A_n B_m]$$

- (A) concentration of the element A,  $(\text{kmol/m}^3)$
- (B) concentration of the element B, (kmol/m<sup>3</sup>)
- $(A_n B_m)$  concentration of the compound  $A_n B_m$ ,  $(\text{kmol/m}^3)$
- $R_{for}$  forward reaction rate, (m<sup>3</sup>/(kmol·s))
- $R_{rev}$  reverse reaction rate, (1/s)

$$R_{for}(T) = R_{0,for} \cdot \exp\left(-\frac{A_{R,for}}{T}\right)$$
$$R_{rev}(T) = R_{0,rev} \cdot \exp\left(-\frac{A_{R,rev}}{T}\right)$$

 $R_{0,for}$  forward reaction first coefficient, (m<sup>3</sup>/kmol-s)

 $A_{R,for}$  forward reaction second coefficient, (K) (activation energy divided by the gas constant)  $R_{0,rev}$  reverse reaction first coefficient, (m<sup>3</sup>/kmol-s)

 $A_{R, rev}$  reverse reaction second coefficient, (K) (activation energy divided by the gas constant)

W-1 (R) :	R0FCRT	Forward reaction fi If a negative value  R0FCRT  is used for the Tabular Fun Acceptable range: Default value:	irst coefficient, $R_{0, for}$ , (m <sup>3</sup> /kmol-s) ue is entered then the Tabular Function number instead of the analytical expression. The argument nction is the gas temperature. $0.0 \le \text{ROFCRT} \le 1.0 \times 10^{10}$ or a valid reference to a Tabular Function none
W-2 (R) :	ARFCRT	Forward reaction s $> 0.0$	econd coefficient, $A_{R, for}$ , (K). Used only if R0FCRT
		Acceptable range: Default value:	$-1.0 \times 10^{10} \le \text{ARFCRT} \le 1.0 \times 10^{10}$ 0.0
W-3 (R) :	RMFCRT	Lower limit on <i>R</i> <sub>for</sub>	$r_{r}(T)$ :
		$RMFCRT \leq R$	$_{for}(T) \leq RXFCRT$
		Acceptable range: Default value:	$0.0 \le \text{RMFCRT} \le 10^{-1}$ 0.0
W-4 (R) :	RXFCRT	Upper limit on <i>R<sub>for</sub></i> Acceptable range: Default value:	( <i>T</i> ). RMFCRT $\leq$ RXFCRT $\leq$ 1.0 1.0
W-5 (R) :	RORCRT	Reverse reaction fir If a negative valu  R0RCRT  is used for the Tabular Fun Acceptable range: Default value:	rst coefficient, $R_{0, rev}$ , (1/s) ue is entered then the Tabular Function number instead of the analytical expression. The argument nction is the gas temperature. $0.0 \le \text{RORCRT} \le 1.0 \times 10^{10}$ or a valid reference to a Tabular Function none
W-6 (R):	ARRCRT	Reverse reaction so $> 0.0$ .	econd coefficient, $A_{R, rev}$ , (K). Used only if RORCRT
		Acceptable range: Default value:	$-1.0 \times 10^{10} \le \text{ARRCRT} \le 1.0 \times 10^{10}$ 0.0
W-7 (R) :	RMRCRT	Lower limit on $R_{re}$	$_{\nu}(T)$ :
		$RMRCRT \leq R$	$P_{rev}(T) \leq RXRCRT$
		Acceptable range: Default value:	$0.0 \le \text{RMRCRT} \le 10^{-1}$ 0.0
W-8 (R) :	RXRCRT	Upper limit on <i>R<sub>rev</sub></i> Acceptable range: Default value:	p(T). RMRCRT $\leq$ RXRCRT $\leq$ 1.0 1.0

#### 2.15.77 Records: 895YXX, Sorption of Fission Product Vapors on Surfaces

This record defines the reaction model and coefficients for the sorption process number YXX. The sorption models are defined as up to nine sets, with models for all fission product vapor classes within each set. Y is the set number, XX is the vapor class number. Different sets are applied on different surfaces. Selection of the sorption model set on the surface is done in records 395XXX and 495XXX. The set numbers, Y, must be consecutive (starting with 1). Three sorption models are available (see Volume 1):

- Sorption model 0 User-defined sorption rate
- Sorption model 1 SPECTRA model
- Sorption model 2 PATRAS/SPATRA model
- W-1 (I): ISORRT Model selection,

< 0: User-defined model,  $\left| \text{ISORRT} \right|$  is the reference number of a Control Function that determines the adsorption rate in (kg/m²-s) on the surface. The following limits are imposed internally on the value obtained from the Control Function:

$$-10^{-3} \le CF \le 10^{-3}$$
  
if  $C < C_{\min} = 10^{-30}$ , then:  $(dC_S / dt) = CF \cdot (C / C_{\min})$ 

Here *C* is the vapor concentration in the gas space (for *CF*>0) or inside the wall (*CF*<0) (kg/m<sup>3</sup>)

= 1: Sorption model 1
= 2: Sorption model 2
Acceptable range: 1, 2, or reference to a Control Function.
Default value: none.

The following words depend on the model selected by Word 1.

#### ISORRT < 0: User-defined sorption rate

If ISORRT < 0, the sorption rate is defined by the user as a Control Function:

$$\left(\frac{dC_s}{dt}\right)_{total} = CF$$

The availability of sorbed species is checked by the code, so the sorption rate is automatically reduced if insufficient amount is present. However, if a positive sorption rate is defined (CF>0.0) at zero concentration of the sorbed species, a mass error may be encountered. To avoid this error, CF should be defined such that the value approaches zero when the concentration approaches zero. The model may be applied for either gas-covered or liquid-covered surfaces, depending on the selector ISRLRT, W-2 below.

W-2(I): ISRLRT Selection of sorption on liquid-covered surfaces - Figure 2-75. ISRLRT = 1: sorption only on gas-covered surface ISRLRT = 2: sorption only on liquid-covered surface Acceptable range: ISRLRT = 1, 2 Default value: 1

#### ISRLRT = 1 (input record 895YXX) Sorption on gas-covered surfaces



ISRLRT = 2 (input record 895YXX) Sorption on liquid-covered surfaces









- (2) sorption on liquid-covered surfaces, applicable models: 0, 1

#### ISORRT = 1: Sorption Model 1 (SPECTRA Model)

If ISORRT = 1 the words 2 - 25 define the model constants of the Sorption Model 1. The full equation is:

$$\left(\frac{dC_s}{dt}\right)_{total} = \begin{cases} A_s(T) \cdot C_V^{x_A} & -B_s(T) \cdot C_d & \text{for } C_V \leq C_{sat}(T) \\ A_s(T) \cdot C_V^{x_{nd}} \cdot \left(\frac{C_{sat}}{C_{sat}^{x_{nd}}}\right) - B_s(T) \cdot C_d & \text{for } C_V > C_{sat}(T) \end{cases}$$

The adsorption coefficient,  $A_S(T)$  and the desorption coefficient,  $B_S(T)$ , and  $C_{sat}(T)$  are calculated from Tabular Functions or the following analytical expressions:

$$A_{S}(T) = A_{0} \cdot \exp\left(-\frac{A_{A}}{T}\right)$$
$$B_{S}(T) = B_{0} \cdot \exp\left(-\frac{A_{B}}{T}\right)$$
$$C_{sat}(T) = C_{0} \cdot \exp\left(-\frac{A_{C}}{T}\right)$$

All coefficients for the Sorption Model 1 are defined by the Words 2 - 16 below. The model may be applied for either gas-covered or liquid-covered surfaces, depending on the selector ISRLRT, see W-17 below.

W-2 (R): A0SRRT Constant  $A_0$  in the expression for the adsorption coefficient,  $A_s(T)$ :

$$A_{S}(T) = A_{0} \cdot \exp\left(-\frac{A_{A}}{T}\right)$$

If a negative value is entered then the Tabular Function number |A0SRRT| is used instead of the analytical expression. The argument for the Tabular Function is the wall temperature.

Acceptable range:  $0.0 \le AOSRRT \le 1.0 \times 10^{20}$  or a valid reference to a Tabular Function

- Default value: 0.0
- W-3 (R): AASRRT Constant  $A_A$  in the expression for the adsorption coefficient,  $A_S(T)$ . Used only if AOSRRT > 0.0. Acceptable range:  $-1.0 \times 10^{10} \le AASRRT \le 1.0 \times 10^{10}$ Default value: 0.0
- W-4 (R) :XASRRTConstant  $x_A$  in the sorption model 1.Acceptable range: $0.3 \le XASRRT \le 3.0$ Default value:1.0

W-5 (R) : AMSRRT Lower limit on  $A_{S}(T)$ :

 $AMSRRT \leq A_{S}(T) \leq AXSRRT$ 

Acceptable range:  $0.0 \le \text{AMSRRT} \le 10^{-1}$ Default value: 0.0

- W-6 (R) : AXSRRT Upper limit on  $A_s(T)$ . Acceptable range: AMSRRT  $\leq$  AXSRRT  $\leq$  1.0 Default value: 1.0
- W-7 (R): BOSRRT Constant  $B_0$  in the expression for the desorption coefficient,  $B_s(T)$ :

$$B_{S}(T) = B_{0} \cdot \exp\left(-\frac{A_{B}}{T}\right)$$

If a negative value is entered then the Tabular Function number |B0SRRT| is used instead of the analytical expression. The argument for the Tabular Function is the wall temperature.

Acceptable range: $0.0 \le B0SRRT \le 1.0 \times 10^{20}$  or a valid reference to a<br/>Tabular FunctionDefault value:0.0

- W-8 (R): ABSRRT Constant  $A_B$  in the expression for the desorption coefficient,  $B_S(T)$ . Used only if B0SRRT > 0.0. Acceptable range:  $-1.0 \times 10^{10} \le \text{ABSRRT} \le 1.0 \times 10^{10}$ Default value: 0.0
- W-9 (R) : BMSRRT Lower limit on  $B_S(T)$ :

 $BMSRRT \leq B_{S}(T) \leq BXSRRT$ 

Acceptable range: $0.0 \le BMSRRT \le 10^{-6}$ Default value:0.0

W-10 (R) : BXSRRT Upper limit on  $B_S(T)$ . Acceptable range: BMSRRT  $\leq$  BXSRRT  $\leq$  1.0 Default value: 1.0

W-11 (I) :	IDSRRT	Indicator for negat	ive sorption and $C_d$ interpretatio	n
		IDSRRT  = 1:	negative sorption allowed,	$dC_{s}/dt <> 0.0$
		IDSRRT  = 2:	negative sorption not allowed,	$dC_{s}/dt \ge 0.0$
		IDSRRT < 0:	$C_d$ = surface concentration (kg/n	m <sup>2</sup> )
		IDSRRT > 0:	$C_d$ = volumetric concentration (	kg/m <sup>3</sup> )
		Acceptable range:	IDSRRT = -2, -1, 1, 2	-
		Default value:	1	

W-12 (R): COSRRT Constant  $C_0$  in the expression for  $C_{sat}(T)$ :

$$C_{sat}(T) = C_0 \cdot \exp\left(-\frac{A_C}{T}\right)$$

If a negative value is entered then the Tabular Function number |C0SRRT| is used instead of the analytical expression. The argument for the Tabular Function is the wall temperature.

Acceptable range: $0.0 \le \text{COSRRT} \le 1.0 \times 10^{20}$  or a valid reference to a<br/>Tabular FunctionDefault value:0.0

- W-13 (R): ACSRRT Constant  $A_C$  in the expression for the parameter  $C_{sat}(T)$ .Used only if COSRRT > 0.0. Acceptable range:  $-1.0 \times 10^{10} \le \text{CASRRT} \le 1.0 \times 10^{10}$ Default value: 0.0
- W-14 (R): XRSRRT Reduced exponent,  $x_{red}$ , valid for high vapor concentrations,  $C_V > C_{sat}(T)$ . If zero is used then the adsorption term is independent on the vapor concentration,  $C_V$ , and equal to:

 $A_{S}(T_{w}) \cdot C_{sat}^{x_{A}}(T)$ 

If a positive value is entered then the adsorption term increases with the vapor concentration,  $C_V$ , but the increase is slower. The adsorption term is given by:

$$A_{S}(T_{w}) \cdot C_{V}^{x_{red}} \cdot \left(\frac{C_{sat}^{x_{A}}(T)}{C_{sat}^{x_{red}}(T)}\right)$$

The term in brackets ensures continuity of the function at  $C_V = C_{sat}(T)$ Acceptable range:  $0.0 \le \text{XRSRRT} < \text{XASRRT}$ Default value: 0.0

W-15 (R): CMSRRT Lower limit on  $C_{sat}(T)$ :

 $CMSRRT \le C_{sat}(T) \le CXSRRT$ 

Acceptable range:  $0.0 \le \text{CMSRRT} \le 10^{-1}$ Default value: 0.0

- W-16 (R) : CXSRRT Upper limit on  $C_{sat}(T)$ . Acceptable range: CMSRRT  $\leq$  CXSRRT  $\leq$  1.0 Default value: 1.0
- W-17 (I): ISRLRT Selection of sorption on liquid-covered surfaces Figure 2-75. ISRLRT = 1: sorption only on gas-covered surface ISRLRT = 2: sorption only on liquid-covered surface Acceptable range: ISRLRT = 1, 2 Default value: 1

W-18 (R): DCSRRT Diffusion coefficient in liquid,  $D_C$ , (m<sup>2</sup>/s). Used only for sorption in liquids. i.e. if ISRLRT = 2. If no value or zero is entered, then the adsorption coefficient is obtained from the user-defined constants  $A_0$  (A0SRRT),  $A_A$  (AASRRT) and the temperature-dependent formula:  $A_S = A_0 \exp(-A_A/T)$ .

If the diffusion coefficient,  $D_C$ , is defined, then the adsorption flux is computed using the heat and mass transfer analogy, where:  $Nu \rightarrow Sh$ ,  $Pr \rightarrow Sc$ . The Sherwood number is:  $Sh = A_S \times D_{FC}/D_C$ , where  $D_{FC}$  is the characteristic dimension for forced convection (hydraulic diameter),  $D_C$ , is the diffusion coefficient, DCSRRT. The mass transfer correlation is defined by the following words, and has the form:

$$Sh = A_{Sh} + B_{Sh} \frac{Re^{C_{Sh}} Sc^{D_{Sh}}}{1 + E_{Sh} Re^{F_{Sh}} Sc^{G_{Sh}}}$$

For example, in case of internal forced convection, Dittus-Boelter correlation is:

$$Sh = 0.023 Re^{0.8} Sc^{0.4}$$

To apply this correlation, one needs to set  $B_{Sh} = 0.023$ ,  $C_{Sh} = 0.8$ ,  $D_{Sh} = 0.4$ , other coefficients being equal to zero. If a positive value is entered,  $D_C = \text{DCSRRT}$ If a negative value is entered,  $D_C = \text{TF}$  number |DCSRRT|. The argument for the TF is the fluid temperature. Acceptable range:  $0.0 \le \text{DCSRRT} \le 1.0$  or a valid reference to a Tabular Function Default value: 0.0

- W-19 (R): ASSRRT  $A_{Sh}$  in the user-defined Sherwood number correlation Acceptable range:  $-10^{10} \le \text{ASSRRT} \le 10^{10}$ Default value: 0.0
- W-20 (R) : BSSRRT  $B_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le BSSRRT \le 10^{10}$ Default value: 0.0
- W-21 (R): CSSRRT  $C_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le CSSRRT \le 10.0$ Default value: 0.0
- W-22 (R): DSSRRT  $D_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le DSSRRT \le 10.0$ Default value: 0.0
- W-23 (R): ESSRRT  $E_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le \text{ESSRRT} \le 10^{10}$ Default value: 0.0
- W-24 (R): FSSRRT  $F_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le FSSRRT \le 10.0$ Default value: 0.0
- W-25 (R): GSSRRT  $G_{Sh}$  in the Sherwood number correlation:

*Acceptable range:*  $0.0 \le \text{GSSRRT} \le 10.0$ *Default value:* 0.0

The next two words are used only if fission products are transported as particles (particle diameter DPFPRT>0.0 and density RHFPRT>0.0) and transport on liquid-covered surfaces is active ISRLRT=2. If that is the case, the Sh number correlation described above may be replaced by an alternative way of calculating the pool-gas transport (aerosol particles represent gas bubbles in this case), which uses Brownian diffusion and inertial impaction models on the surface of aerosol particles in the pool:

$$\mathcal{G}_{pool-gas} = v_{Brown} + v_{inertial}$$

where:

$$v_{Brown} = \frac{D_C}{\delta_{BL}}$$
$$v_{inertial} = v_{\infty} \cdot \eta \cdot A_{h,bubb} / A_{bubb} = v_{\infty} \cdot \eta / 4$$

*v*<sub>Brown</sub> Brownian deposition velocity, (m/s)

*v*<sub>inertial</sub> inertial impaction deposition velocity, (m/s)

 $D_C$  diffusion coefficient, (m<sup>2</sup>/s)

 $\delta_{BL}$  diffusion boundary layer thickness, (m) (=10<sup>-5</sup>)

 $A_{h,bubb}$  horizontal cross section area of a "bubble", (m<sup>2</sup>),  $= \pi \times D_{bubb}^2 / 4$ 

 $A_{bubb}$  total surface area of a "bubble", (m<sup>2</sup>),  $= \pi \times D_{bubb}^2$ 

 $v_{\infty}$  particle-to-"bubble" relative velocity, (m/s)

 $\eta$  collection efficiency, calculated from one of three correlations, described below.

Langmuir and Blodgett (L-B) correlation - Figure 2-76

$$\eta = \eta_{\max} \cdot \frac{Stk^2}{\left(Stk + C_{LB}\right)^2}$$

 $C_{LB}$  constant (=0.25, see [54], eq. 3)

 $\eta_{max}$  maximum value of collection efficiency (=1.0)

*Stk* Stokes number, (-), see Volume 1 for detailed description.

Modified Langmuir and Blodgett correlation - Figure 2-77

$$\eta = \eta_{\max} \cdot \begin{cases} \frac{0.25}{C_{LB}} \cdot Stk & for \quad Stk < C_{LB} \\ \frac{Stk^2}{\left(Stk + C_{LB}\right)^2} & for \quad Stk > C_{LB} \end{cases}$$

Correlation developed based on data of Yoon & Lutrell and Afruns & Kitchener - Figure 2-78

$$\eta = Min\left(\eta_{\max}, A \cdot \frac{d_p^2}{D_b}\right)$$



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Figure 2-76 Langmuir and Blodgett correlation



Figure 2-77 Modified versus original Langmuir and Blodgett correlation

In order to activate the model, non-zero values must be supplied for at least two out of the following three input entries:

W-26 (R): TBL2RT Diffusion boundary layer thickness,  $\delta_{BL}$ , (m). Acceptable range:  $1.0 \times 10^{-7} \le \text{TBL2RT} \le 1.0 \times 10^{-3}$ . Default value: none If the model is used, the recommended value is  $5.0 \times 10^{-5}$ .



Figure 2-78 Data of Yoon & Lutrell and Afruns & Kitchener and correlation

W-27 (R): CLB2RT Constant in the correlation for inertial impaction. CLB2RT  $\leq$  10: *C*<sub>*LB*</sub>, in the L-B or modified L-B correlation (depending on ILBORT, record 860000) CLB2RT > 1000: A in the correlation developed based on data of Yoon & Lutrell and Afruns & Kitchener Acceptable range:  $10^{-2} \le \text{CLB2RT} \le 10^{+1} C_{LB}$ , in L-B, modified L-B  $10^{+3} \le \text{CLB2RT} \le 10^{+5} A$  in YLAK correlation Default value: none For L-B and modified L-B, the recommended value is 0.25. For YLAK, the recommended values are 9,000 - 13,000. Maximum efficiency  $\eta_{max}$ , in the correlation for inertial impaction. W-28 (R): ELB2RT Acceptable range:  $10^{-3} \le \text{ELB2RT} \le 10^{+3}$ Default value: 1.0 if the model is used (if TBL2RT>0.0, CLB2RT>0.0)

#### ISORRT = 2: Sorption Model 2 (PATRAS/SPATRA model)

If ISORRT = 2 the words 2 - 29 define the model constants of the Sorption Model 2. The model is applicable for gas phase only. In case of liquid-covered surfaces, only desorption of the reversibly-bound particles is possible (when APSRRT > 0.0, see W-27 below). The equations are:

$$\left(\frac{dC_s}{dt}\right)_{total} = \alpha \cdot (1-\theta) \cdot u \cdot C_{\delta} - \vartheta \cdot C_{rev} - \eta \cdot C_d$$
$$\left(\frac{dC_s}{dt}\right)_{diff} = \alpha \cdot (1-\theta) \cdot u \cdot C_{\delta} \cdot (1-\beta) - \eta \cdot C_d$$

- W-2 (R) :ALSRRTSticking factor,  $\alpha$ , (-).Acceptable range: $0.0 \le ALSRRT \le 1.0$ Default value:1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0)
- W-3 (R): CMSRRT Maximum number of adsorption sites per unit surface area,  $C_{max}$ , (m<sup>-2</sup>). The value may be applied for each vapor individually or as a global value for all vapors, depending on the selector ICSRRT (Word 29 beow). If a global value is used, then CMSRRT must be specified as the same for all vapors. Acceptable range:  $10^5 \leq \text{CMSRRT} \leq 10^{50}$

Default value:  $1.0 \times 10^{18}$ 

W-4 (R): SGSRRT Diffusion volume,  $\Sigma$ , of the fission product class XX. If a positive value is used, then the diffusion coefficient for fission product vapor diffusion in the atmosphere gas of a Control Volume is calculated from the general method, applicable for any gas mixture. If the diffusion volume for a particular element or compound is not available, then the following correlations are recommended to calculate the value of  $\Sigma$ (see Volume 1):

Elements:
$$\Sigma = 2.4 \cdot A^{0.66}$$
Compounds: $\Sigma = 4.2 \cdot A^{0.66}$ A is the atomic number.Acceptable range: $0.0 \leq \text{SGSRRT} \leq 1000.0$ ,  
either SGSRRT or ADSRRT must be positiveDefault value: $0.0$ 

W-5 (R): ADSRRT If the diffusion volume,  $\Sigma$  (SGSRRT), is equal to zero, then a Chapman-Enskog correlation is applied to calculate the diffusion coefficient:

$$D_C = A_D \cdot \frac{T_g^{B_D}}{p}$$

- $A_D$  user-defined coefficient
- $B_D$  user-defined coefficient
- $T_g$  gas temperature, (K)
- p gas pressure, (Pa)
- $D_C$  diffusion coefficient, (m<sup>2</sup>/s)

		ADSRRT is the correlation is valid the gas composition helium is replaced <i>Acceptable range:</i> <i>Default value:</i>	coefficient $A_D$ in this correlation. Note that this only for given gas and should not be applied when on may change during calculations, for example if by air. $0.0 \le \text{ADSRRT} \le 1.0 \times 10^3$ either SGSRRT or ADSRRT must be positive 0.0
W-6 (R) :	BDSRRT	Coefficient $B_D$ in diffusion volume, $T$ Acceptable range: Default value:	the Chapman-Enskog correlation. Used only if the $\Sigma$ (SGSRRT), is equal to zero. $0.0 \le BDSRRT \le 10.0$ 0.0
W-7 (R) :	B0SRRT	$(1-\beta_0)$ in the formu	la for the penetration factor, $(1-\beta)$ :
		$1 - \beta = (1 - \beta)$	$(\beta_0) \cdot \exp\left(\frac{A_{\beta}}{T_w}\right)$
		Acceptable range:	$0.0 \le BOSRRT \le 1.0$ for wall surfaces
		Default value:	$10^{-5}$ for wall surfaces, 0.0 for aerosol surfaces (a small number, $<10^{-50}$ , sets the value to 0.0)
W-8 (R) :	ABSRRT	$A_{\beta}$ in the formula for $Acceptable range: Default value:$	for the penetration factor, $(1-\beta)$ . $0.0 \le ABSRRT \le 1.0 \times 10^{10}$ 0.0
W-9 (R) :	BMSRRT	Lower limit on (1- Acceptable range: Default value:	$(-\beta), (1-\beta)_{\min}.$ $0.0 \le BMSRRT \le 1.0$ 0.0
W-10 (R) :	BXSRRT	Upper limit on (1– Acceptable range: Default value:	$\beta$ ), $(1-\beta)_{max}$ . BMSRRT $\leq$ BXSRRT $\leq$ 1.0 1.0
W-11 (R) :	A0SRRT	$\mathcal{G}_0$ in the formula f	for the desorption coefficient, $\mathcal{G}$ :
		$\mathcal{G}=\mathcal{G}_0\;\cdot\;$	$\exp\!\!\left(-\frac{A_g}{T_w}\right)$
		Acceptable range: Default value:	$0.0 \le A0SRRT \le 1.0 \times 10^{20}$ 0.0
W-12 (R) :	AASRRT	$A_{\mathcal{G}}$ in the formula	for the desorption coefficient, $\mathcal S$ .
		Acceptable range: Default value:	$\begin{array}{l} 0.0 \leq AASRRT \leq 1.0 \times 10^{10} \\ 0.0 \end{array}$
W-13 (R) :	AMSRRT	Lower limit on $\mathcal{G}$ ,	$artheta_{\min}$ .

Acceptable range: $0.0 \le AMSRRT \le 1.0$ Default value:0.0

- W-14 (R) :AXSRRTUpper limit on  $\mathcal{G}, \mathcal{G}_{max}$ .Acceptable range:AMSRRT  $\leq$  AXSRRT  $\leq$  1000.0Default value:10.0
- W-15 (R) : E0SRRT  $\eta_0$  in the formula for the evaporation coefficient,  $\eta$ :

$$\eta = \eta_0 \cdot \exp\left(-\frac{A_g}{T_w}\right)$$

Acceptable range: $0.0 \le E0SRRT \le 1.0 \times 10^{20}$ Default value:0.0

- W-16 (R): AESRRT  $A_{\eta}$  in the formula for the evaporation coefficient,  $\eta$ . Acceptable range:  $0.0 \le \text{AESRRT} \le 1.0 \times 10^{10}$ Default value: 0.0
- W-17 (R): EMSRRT Lower limit on  $\eta$ ,  $\eta_{min}$ . Acceptable range:  $0.0 \le \text{EMSRRT} \le 1.0$ Default value: 0.0
- W-18 (R) : EXSRRT Upper limit on  $\eta$ ,  $\eta_{max}$ . Acceptable range: EMSRRT  $\leq$  EXSRRT  $\leq$  1.0 Default value: 1.0
- W-19 (R): ASSRRT  $A_{Sh}$  in the user-defined Sherwood number correlation:

$$Sh = A_{Sh} + B_{Sh} \frac{Re^{C_{Sh}} Sc^{D_{Sh}}}{1 + E_{Sh} Re^{F_{Sh}} Sc^{G_{Sh}}}$$

This correlation is used if  $A_{Sh} > 0$  or  $B_{Sh} > 0$  (Word 12 below). If  $A_{Sh}$  is negative, then the Gnielinski correlation is used:

$$Sh = \frac{r \cdot (Re - 1000) \cdot Sc}{1 + 12.7 \cdot \sqrt{r} \cdot (Sc^{2/3} - 1)} \cdot \left(1 + \left(\frac{d}{x}\right)^{2/3}\right) \cdot \left(\frac{T_{gas}}{T_{wall}}\right)^{r}$$

where:

 $r = (1/8) \cdot (1.82 \cdot \log_{10}(Re) - 1.64)^{-2}$ 

 $T_{gas}$ ,  $T_{wall}$  are the gas and wall temperature, d is the hydraulic diameter and x is the distance from tube entrance. The value of x is equal to the absolute value of ASSRRT: x = |ASSRRT|. The value of x may be specified individually for each SC/TC on the records 396XXX and 496XXX. The value of y is defined by YGNIRT, Word 28, below. If both  $A_{Sh}$  and  $B_{Sh}$  are equal to zero, then the mass transfer coefficient is calculated from the heat and mass transfer analogy, using the same correlations as are being used for natural and forced convective heat transfer. For example, in case of internal flow forced convection this is Dittus-Boelter correlation, which is:

$$Sh = 0.023 Re^{0.8} Sc^{0.4}$$

Suppose the user wishes to apply this correlation in natural as well as forced convective regime. This may be done applying the user-defined Sherwood number correlation, with:  $B_{Sh} = 0.023$ ,  $C_{Sh} = 0.8$ ,  $D_{Sh} = 0.4$ , other coefficients being equal to zero. Acceptable range:  $-10^{10} \le \text{ASSRRT} \le 10^{10}$ Default value: 0.0

- W-20 (R) : BSSRRT  $B_{Sh}$  in the Sherwood number correlation:  $Acceptable \ range: 0.0 \le BSSRRT \le 10^{10}$  $Default \ value: 0.0$
- W-21 (R): CSSRRT  $C_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le CSSRRT \le 10.0$ Default value: 0.0
- W-22 (R): DSSRRT  $D_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le DSSRRT \le 10.0$ Default value: 0.0
- W-23 (R): ESSRRT  $E_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le \text{ESSRRT} \le 10^{10}$ Default value: 0.0
- W-24 (R): FSSRRT  $F_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le FSSRRT \le 10.0$ Default value: 0.0
- W-25 (R): GSSRRT  $G_{Sh}$  in the Sherwood number correlation: Acceptable range:  $0.0 \le \text{GSSRRT} \le 10.0$ Default value: 0.0
- W-26 (R): XLSRRT Limiting factor in the number of adsorption sites per unit surface area that may be taken by a single vapor during a time step,  $X_{lim}$ , (m<sup>-2</sup>). Acceptable range:  $0.90 \le XLSRRT \le 1.00$ Default value: 0.99
- W-27 (R): APSRRT Desorption coefficient for pool-covered surfaces,  $\mathcal{P}_{pool}$ . On the poolcovered surfaces only desorption of the reversibly bound molecules (that had been adsorbed when the surface was uncovered) may occur. No adsorption, penetration, or evaporation is calculated during the period when the surface is covered by liquid. The mass transfer is:

$$\left(\frac{dC_{rev}}{dt}\right)_{total} = -\mathcal{G}_{pool} \cdot C_{rev}$$

		Acceptable range: Default value:	$0.0 \le \text{APSRRT} \le 1.0$ 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0)
W-28 (R) :	YGNIRT	The value of y in the value of y in the Acceptable range: Default value:	he Gnielinski correlation. 0.001 YGNIRT ≤ 1.00 0.015
W-29 (R) :	ICSRRT	Method of calculat ICSRRT = 1: ICSRRT = 2: Acceptable range: Default value:	tion of CMSRRT (Word 3 above). CMSRRT is independent for each vapor CMSRRT is a global value for all vapors 1 or 2. ICSRRT must be entered consistently for all vapors within a sorption set (i.e. the same value must be applied for all vapors). 1

## 2.15.78 Records: 395XXX, Selection of Sorption Processes on SC Surfaces

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	I1SRRT(1)	Sorption set number surface of the 1-D deactivates the sorp <i>Acceptable range:</i> <i>Default value:</i>	er (defined in records 895YXX) to be used on the left O Solid Heat Conductor XXX. A negative number obtion model. must be one of existing sorption sets, if positive -1 if ISRGRT (global activator of the sorption model, record 880000) is 0, ISRGRT otherwise.
W-2 (R) :	Y1SRRT(1)	Multiplier for the s Solid Heat Conduc calculated by the multiplied by this v Acceptable range: Default value:	orption model applied on the left surface of the 1-D etor XXX. The adsorption or desorption rate that is sorption model selected by the previous word, is value when applied to the left surface of this SC. $0.0 \le \text{Y1SRRT}(1) \le 10.0$ . For the sorption model 2 (see 895YXX) only 1.0 and 0.0 may be used. 1.0.
W-3 (I) :	I1SRRT(2)	Sorption set numbe surface of the 1-D deactivates the sorp <i>Acceptable range:</i> <i>Default value:</i>	r (defined in records 895YXX) to be used on the right O Solid Heat Conductor XXX. A negative number otion model. must be one of existing sorption sets, if positive -1 if ISRGRT (global activator of the sorption model, record 880000) is 0, ISRGRT otherwise.
W-4 (R) :	Y1SRRT(2)	Multiplier for the so Solid Heat Conduc calculated by the multiplied by this v	orption model applied on the right surface of the 1-D ctor XXX. The adsorption or desorption rate that is sorption model selected by the previous word, is value when applied to the right surface of this SC.

Acceptable range: $0.0 \le Y1SRRT(2) \le 10.0$ . For the sorption model 2<br/>(see 895YXX) only 1.0 and 0.0 may be used.Default value:1.0.

#### 2.15.79 Records: 495XXX, Selection of Sorption Processes on TC Surfaces

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	I1	Boundary cell num cell range for sorpt by Word 3, will be <i>Acceptable range:</i> <i>Default value:</i>	aber. Using I1 and I2 (below) the user specifies the ion process definition. The sorption process, defined applied for the boundary cells I: $I1 \le I \le I2$ . must be an existing boundary cell number. none.
W-2 (I) :	I2	Boundary cell num cell range for sorpt by Word 3, will be <i>Acceptable range:</i> <i>Default value:</i>	aber. Using I2 and I1 (above) the user specifies the ion process definition. The sorption process, defined applied for the boundary cells I: $I1 \le I \le I2$ . must be an existing boundary cell number. $I2 \ge I1$ . none.
W-3 (I) :	I2SRRT(I)	Sorption set numb boundary cell I, I1 negative number de <i>Acceptable range:</i> <i>Default value:</i>	er (defined in records 895YXX) to be used on the $\leq I \leq I2$ , of the 2-D Solid Heat Conductor XXX. A eactivates the sorption model. must be one of existing sorption sets, if nonzero -1 if ISRGRT (global activator of the sorption model, record 880000) is 0, ISRGRT otherwise.
W-4 (R) :	Y2SRRT(I)	Multiplier for the $I1 \le I \le I2$ , of the 2 desorption rate that previous word, is m cell I of this TC. <i>Acceptable range: Default value:</i>	sorption model applied on the boundary cell I, 2-D Solid Heat Conductor XXX. The adsorption or t is calculated by the sorption model selected by the nultiplied by this value when applied to the boundary $0.0 \le Y2SRRT(I) \le 10.0$ . For the sorption model 2 (see 895YXX) only 1.0 and 0.0 may be used. 0.0.

The data set consisting of the four words described above is repeated until sorption reactions are defined for all desired boundary cells. The data sets may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 4.

#### 2.15.80 Records: 396XXX, Sorption Related Parameters for SC Surfaces

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

- W-1 (I): XGN1RT(1) Parameter x in the Gnielinsky correlation (see description of record 895YXX, Word 19, ASSRRT) to be used on the left surface of the 1-D Solid Heat Conductor XXX. Acceptable range: 0.001 ≤ XGN1RT(1) ≤ 1000.0 Default value: |ASSRRT|
  W-2 (I): XGN1RT(2) Parameter x in the Gnielinsky correlation (see description of record 895YXX, Word 19, ASSRRT) to be used on the right surface of the 1-
- w-2 (1): XGN1R1(2) Parameter x in the Gnielinsky correlation (see description of record 895YXX, Word 19, ASSRRT) to be used on the right surface of the 1-D Solid Heat Conductor XXX. Acceptable range:  $0.001 \le XGN1RT(2) \le 1000.0$ Default value: |ASSRRT|

#### 2.15.81 Records: 496XXX, Sorption Related Parameters for TC Surfaces

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	I1	Boundary cell number. Using I1 and I2 (below) the user specifies the cell range for sorption process definition. The sorption process, defined by Word 3, will be applied for the boundary cells I: $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. <i>Default value:</i> none.
W-2 (I) :	I2	Boundary cell number. Using I2 and I1 (above) the user specifies the cell range for sorption process definition. The sorption process, defined by Word 3, will be applied for the boundary cells I: $I1 \le I \le I2$ . <i>Acceptable range:</i> must be an existing boundary cell number. I2 $\ge$ I1. <i>Default value:</i> none.
W-3 (R) :	XGN2RT(	I) Parameter i in the Gnielinsky correlation (see description of record 895YXX, Word 19, ASSRRT) to be used on the boundary cell I, $I1 \le I \le I2$ , of the 2-D Solid Heat Conductor XXX. Acceptable range: $0.001 \le XGN2RT(I) \le 1000.0$ Default value: $ ASSRRT $

The data set consisting of the four words described above is repeated until sorption reactions are defined for all desired boundary cells. The data sets may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 3.

#### 2.15.82 Records: 191XXX, Initial Masses of Isotopes in CV Atmosphere and Pool

XXX is the CV reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	KKI	Reference number number and I is the <i>Acceptable range:</i> <i>Default value:</i>	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-2 (R) :	XMACRT	Initial mass of the is XXX, (kg).	sotope KKI in the atmosphere of the Control Volume
		Acceptable range:	$0.0 \leq \text{XMACRT} \leq 0.1 \times M_{atms}$
		1 0	Here $M_{atms}$ is the mass of atmosphere in CV
		Default value:	0.0
W-3 (R) :	XMPCRT	Initial mass of the i (kg).	sotope KKI in the pool of the Control Volume XXX,
		Acceptable range:	$0.0 \le \text{XMPCRT} \le 0.1 \times M_{pool}$
			Here $M_{pool}$ is the mass of pool in CV
		Default value:	0.0

The data set consisting of the three words described above is repeated until initial masses of all desired isotopes are defined. The data sets may be entered in several records with the same number. The number of entries in a single record must be always a multiple of 2.

#### 2.15.83 Records: 391XXX, Initial Masses of Isotopes in SC

This record defines initial masses of isotopes that have penetrated into 1-D solid structures due to the sorption processes. XXX is the SC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	KKI	Reference number number and I is the <i>Acceptable range:</i> <i>Default value:</i>	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-2 (R) :	XM1FRT	Initial mass of the i (kg). This is a tot distribution may b 392XXX. If the dist the mass of XM1FF cells, i.e. with unifo <i>Acceptable range:</i> <i>Default value:</i>	sotope KKI in the 1-D Solid Heat Conductor XXX, tal mass in all cells of the SC. The cell-to-cell e specified for each vapor class in the records ribution is not specified in the record 392XXX, then RT is assumed to be uniformly distributed among the rm material density (kg/m <sup>3</sup> ). $0.0 \le XM1FRT \le 0.001 \times M_{SC}$ Here $M_{SC}$ is the mass of the SC material 0.0

The set of two words is repeated until initial masses of all desired isotopes are defined. Several records with the same number may be used.
### 2.15.84 Records: 491XXX, Initial Masses of Isotopes in TC

This record defines initial masses of isotopes that have penetrated into 2-D solid structures due to the sorption processes. XXX is the TC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	KKI	Reference number number and I is the <i>Acceptable range:</i> <i>Default value:</i>	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-2 (R) :	XM2FRT	Initial mass of the kine (kg).	isotope KKI in the 2-D Solid Heat Conductor XXX,
		Acceptable range:	$0.0 \le \text{XM2FRT} \le 0.001 \times M_{\text{TC}}$
			Here $M_{\rm TC}$ is the mass of the TC material
		Default value:	0.0

The set of two words is repeated until initial masses of all desired isotopes are defined. Several records with the same number may be used.

## 2.15.85 Records: 192XXX, External Sources of Isotopes

This record specifies any external sources of isotopes for a Control Volume. The term external sources is used to mean sources other than release from the core (calculated by one of the available release models - records 890000, 891000). XXX is the CV reference number,  $001 \le XXX \le 999$ .

W-1 (R) :	ZFSCRT	Elevation of the source related to the bottom of CV. The value i used as an indicator for a replacement of data - see the comment b the W-3 description.	
		Acceptable range: Default value:	$0.0 \le \text{ZFSCRT} \le \text{HEIGCV}$ (see record 110XXX) 0.0
W-2 (I) :	KKI	Reference number number and I is the <i>Acceptable range:</i> <i>Default value:</i>	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-3 (I) :	IFSCRT	Pointer to a Tabula isotope KKI in the of the source will be number: IFSCRT. defined by a Contr If the current value 0.0, the source will be set to 10 <sup>3</sup> . The u <i>Acceptable range:</i> <i>Default value:</i>	ar or Control Function that defines the source of the Control Volume XXX. If the number is positive, then defined by a Tabular Function with the reference If the number is negative, then the source will be of Function with the reference number:  IFSCRT . e of the Tabular or Control Function is smaller than be set to 0.0. If it is larger than 10 <sup>3</sup> , the source will nits are: (kg/s). must be a valid reference number of a Tabular or Control Function if nonzero none

The data set consisting of the two words described above is repeated until all desired sources are defined. The data sets may be entered in several records with the same number and the same elevation of the source. If the elevation of the source is different than the elevation entered in previous record or records with the same number, then this record is treated as a replacement and replaces any previous data that has been entered in records 192XXX. The number of entries minus one in a single record must be always a multiple of 2.

#### 2.15.86 Records: 392XXX, Initial Distribution of Vapors on the Surfaces of SC

This record defines initial distribution of the isotopes that are reversibly bound to the surface of 1-D solid structures. XXX is the SC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IVAP	Vapor class number. <i>Acceptable range:</i> must be a valid class number if nonzero <i>Default value:</i> none.
W-2 (R) :	CR1FRT	(1) Surface concentration of the reversibly bound molecules on the left surface of the 1-D Solid Heat Conductor XXX, $(kg/m^2)$ . The total mass of the reversibly bound molecules on both left and right surface of SC cannot exceed the total mass that is initially present in the SC, determined in the record 391XXX. If the mass of the reversibly bound molecules on both left and right surfaces is smaller than the total mass in the SC, then the remaining part is assumed to be penetrated inside the SC. If the mass of the reversibly bound molecules on both left and right surfaces is larger than the total mass in the SC, then the reversibly bound molecules on both left and right surfaces is larger than the total mass. In such case there is no penetrated molecules. <i>Acceptable range:</i> CR1FRT(1) $\geq$ 0.0 <i>Default value:</i> 0.0
W-3 (R) :	CR1FRT	(2) Surface concentration of the reversibly bound molecules on the right surface of the 1-D Solid Heat Conductor XXX. (kg/m <sup>2</sup> ).

surface of the 1-D Solid Heat Conductor XXX,  $(kg/m^2)$ . Acceptable range: CR1FRT(2)  $\geq 0.0$ Default value: 0.0

# 2.15.87 Records: 492XXX, Initial Distribution of Vapors on the Surfaces of TC

This record defines initial distribution of the isotopes that are reversibly bound to the surface of 2-D solid structures. XXX is the TC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	I1	Boundary cell num cell range for the d distribution defined cells I: $I1 \le I \le I2$ . <i>Acceptable range:</i> <i>Default value:</i>	aber. Using I1 and I2 (below) the user specifies the listribution of vapors on the boundary surfaces. The l by Words 3 and 4 will be applied for the boundary must be an existing boundary cell number. none.
W-2 (I) :	I2	Boundary cell num cell range for the distribution defined cells I: $I1 \le I \le I2$ . Acceptable range: Default value:	aber. Using I2 and I1 (above) the user specifies the distribution of vapors on the boundary surfaces. I by Words 3 and 4 will be applied for the boundary must be an existing boundary cell number. I2 $\geq$ I1. none.
W-3 (I) :	IVAP	Vapor class numbe Acceptable range: Default value:	r. must be a valid class number if nonzero none.
W-4 (R) :	CR2FRT(I)	Surface concentration boundary cell I, II (kg/m <sup>2</sup> ). The total m of TC cannot excert determined in the molecules on all bot TC, then the remained in the mass of the mission of the mass of the mission of the mass of the ma	tion of the reversibly bound molecules on the $I \le I \le I2$ , of the 2-D Solid Heat Conductor XXX, hass of the reversibly bound molecules on all surfaces ed the total mass that is initially present in the SC, record 491XXX. If the mass of the reversibly bound bundary surfaces is smaller than the total mass in the ning part is assumed to be penetrated inside the TC. eversibly bound molecules on all boundary surfaces tal mass in the TC, then the reversibly bound masses r the correct total mass. In such case there is no es. CR2FRT(I) $\ge 0.0$ 0.0

Several records with the same number may be used to define distributions of different fission product vapors.

# 2.15.88 Records: 393XXX, Initial Distribution of Vapor Classes Inside SC

This record defines initial distribution of the masses of isotopes that have penetrated into 1-D solid structures due to the sorption processes (the masses are defined in record 391XXX). XXX is the SC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IVAP	Vapor class numbe Acceptable range: Default value:	r. must be a valid class number if nonzero none.
W-2 (R) :	CD1FRT(	1) Relative density, va normalized and ma Acceptable range: Default value:	apor class IVAP, in the cell number 1. The values are by therefore be scaled by any factor. $CD1FRT(1) \ge 0.0$ 0.0
W-3 (R) :	CD1FRT(	2) Relative density, va Acceptable range: Default value:	apor class IVAP, in the cell number 2. $CD1FRT(2) \ge 0.0$ 0.0

... until all cells are defined

The last word is repeated until density in all cells are defined. Several records with the same number may be used to define distributions of different fission product vapors.

### 2.15.89 Records: 493XXX, Initial Distribution of Vapor Classes Inside TC

This record defines initial distribution of the masses of isotopes that have penetrated into 2-D solid structures due to the sorption processes (the masses are defined in record 391XXX). XXX is the TC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IVAP	Vapor class number.Acceptable range:must be a valid class number if nonzeroDefault value:none.
W-2 (I) :	L	Row number in <i>y</i> -direction. The following data must specify NCLXTC values of internal power for all cells in the <i>y</i> -row number L. Acceptable range: $1 \le L \le NCLYTC$ . Default value: none.
W-3 (R) :	CD2FRT (1,L)	Relative density, vapor class IVAP, cell (1,L), ( <i>x</i> -row 1, <i>y</i> -row L), (-). The values are normalized and may therefore be scaled by any factor. The values will be normalized during the input processing so that the total mass of the vapor class IVAP is always equal to the sum of the initial masses of all isotopes, specified in the record 491XXX, that belong to the class IVAP. <i>Acceptable range:</i> CD2FRT(1,L) $\ge$ 0.0 <i>Default value:</i> 0.0

The last word is repeated NCLXTC times density in all cells of row L are defined. Several records with the same number may be used to define distributions of different fission product vapors.

# 2.15.90 Records: 194XXX, Decay Heat Distribution Parameters for CV

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . This record, together with the records 394XXX and 494XXX, describes how the decay heat of the isotopes that are released from the core is distributed among the gas and liquid spaces of a Control Volume and solid structures. The default modelling is based on the following assumptions:

- $\beta$ -radiation is absorbed by the gas in the atmosphere of a Control Volume.
- $\gamma$ -radiation passes through the gas and is absorbed by solid structures and water pool.

Division of the decay heat of isotopes present in the atmosphere and pool of a Control Volume are discussed in this section.

W-1 (R) :	XATBRT	Fraction of $\beta$ -radiation absorbed in the gas space of the Control Volume XXX, $x_{atms, \beta}$ , (-). Acceptable range: $0.0 \le \text{XATBRT} \le 1.0$
		Default value: 1.0
W-2 (R) :	XATGRT	Fraction of $\gamma$ -radiation absorbed in the gas space of the Control VolumeXXX, $x_{atms, \gamma}$ , (-).Acceptable range:0.0 $\leq$ XATGRT $\leq$ 1.0Default value:0.0

#### 2.15.91 Records: 394XXX, Decay Heat Distribution Parameters for SC

XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record, together with the records 194XXX and 494XXX, describes how the decay heat of the isotopes that are released from the core is distributed among the gas and liquid spaces of a Control Volume and solid structures. The default modelling is based on the following assumptions:

- $\beta$ -radiation is completely absorbed by the solid structures.
- *y*-radiation is completely absorbed by the solid structures.

Division of the decay heat of isotopes present in the 1-D Solid Heat Conductors are discussed in this section.

W-1 (R) :	XS1BRT	Fraction of $\beta$ -radiation absorbed in the solid material of the Heat Conductor XXX, $x_{solid, \beta}$ , (-). Currently only default value is allowed. Acceptable range: $1.0 \le \text{XS1BRT} \le 1.0$ Default value: $1.0$
W-2 (R) :	XS1GRT	Fraction of $\gamma$ -radiation absorbed in the solid material of the Heat Conductor XXX, $x_{solid, \gamma}$ , (-). Currently only default value is allowed. Acceptable range: $1.0 \leq XS1GRT \leq 1.0$ Default value: $1.0$
W-3 (R):	WFSCRT	Weighting factor, $w_{SC}$ , (-), applied for the left surface in calculating the division of decay heat. The radiation emitted from the surface of an SC

is distributed among all surfaces present in a given enclosure based on the absorption fractions, defined as:

$$F_{abs,SC} = \frac{A_{SC} \cdot |w_{SC}|}{\sum_{L} A_{L} \cdot |w_{L}|}$$

 $A_{SC}$  - surface area of the solid heat conductor

 $w_{SC}$  - weighting factor of the surface SC

The summation is performed over all structures (1-D as well as 2-D) that are in contact with the boundary CV. Therefore the index L stands for any SC as well as TC in contact with the CV.

The values of  $F_{abs,SC}$  are pre-computed during the input processing and are printed next to the weighting factors for CV related data of the RT Package, as a "CV enclosure data for decay heat calculations".

If  $w_{SC}$ , is negative, the generating surface is not included in the distribution of the radiation emitted from its surface. Physically it means that the structure cannot radiate to itself. In such case the structure absorbs only half of the radiation generated at its surface. The other half is distributed among other structures of the enclosure, gas or pool. This means the fraction of the generated decay heat that the source structure receives is equal to:

$$\frac{1}{2}(\beta + \gamma)$$

If  $w_{SC}$ , is positive, the generating surface is included in the distribution of the radiation emitted from its surface. Physically it means that the structure can radiate to itself. The total fraction of the generated decay heat that the source structure receives is equal to:

$$\frac{1}{2}(\beta+\gamma) + \frac{1}{2}[\beta(1-x_{atms,\beta})+\gamma(1-x_{atms,\gamma})] \cdot (1-X_{pool,SC} \cdot w_{pool,CV}) \cdot F_{abs,SC}$$

Acceptable range:  $10^{-6} \le |WFSCRT| \le 10^{6}$ Default value: -1.0.

W-4 (R): WFSCRT Weighting factor,  $w_i$ , (-), applied for the right surface in calculating the division of decay heat. Acceptable range:  $10^{-6} \le |WFSCRT| \le 10^6$ Default value: 1.0.

### 2.15.92 Records: 494XXX, Decay Heat Distribution Parameters for TC

XXX is the 2-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ . This record, together with the records 194XXX and 394XXX, describes how the decay heat of the isotopes that are released from the core is distributed among the gas and liquid spaces of a Control Volume and solid structures. The default modelling is based on the following assumptions:

- $\beta$ -radiation is completely absorbed by the solid structures.
- *γ*-radiation is completely absorbed by the solid structures.

Division of the decay heat of isotopes present in the 2-D Solid Heat Conductors are discussed in this section.

W-1 (R) :	XS2BRT	Fraction of $\beta$ -radiation absorbed in the solid material of the Heat Conductor XXX, $x_{solid, \beta}$ , (-). Currently only default value is allowed. Acceptable range: $1.0 \le XS2BRT \le 1.0$ Default value: $1.0$
W-2 (R) :	XS2GRT	Fraction of $\gamma$ -radiation absorbed in the solid material of the Heat Conductor XXX, $x_{solid, \gamma}$ , (-). Currently only default value is allowed. Acceptable range: $1.0 \leq XS2GRT \leq 1.0$ Default value: $1.0$
W-3 (R) :	WFTCRT	Weighting factor, $w_i$ , (-), applied for all boundary cells in calculating the division of decay heat. <i>Acceptable range:</i> $10^{-3} \le \text{WFTCRT} \le 10^3$ <i>Default value:</i> 1.0.

### 2.15.93 Records: 295XXX, Vapor Filter Model

XXX is the Junction reference number,  $001 \le XXX \le 999$ ..

W-1 (I) :	IFLVRT	Filter type:
		=-1: no filter.
		= 1: vapor filter, filter efficiency defined for each vapor class.
		= 2: isotope filter, filter efficiency defined for each isotope.
		Acceptable range: -1, 1, 2
		Default value: -1

# $\underline{\text{If IFLVRT} = 1}$

W-2 (I) :	JFLVRT(1)	Reference number	of a Tabular or a Control Function that defines filter
		efficiency for the v	apor class 1.
		Acceptable range:	must be a valid reference number of a Tabular or
			Control Function, if nonzero
		Default value:	none
W-3 (I) :	JFLVRT(2)	Reference number	of a Tabular or a Control Function that defines filter
		efficiency for the v	apor class 2.
		Acceptable range:	must be a valid reference number of a Tabular or
			Control Function, if nonzero
		Default value:	none

..., until the efficiencies are specified for all vapor classes.

#### If IFLVRT = 2

W-2 (I): I1 Isotope number

W-3 (I) :	JFLVRT(1)	Reference number efficiency for the is <i>Acceptable range:</i> <i>Default value:</i>	of a Tabular or a Control Function that defines filter sotope I1 must be a valid reference number of a Tabular or Control Function, if nonzero none
W-4 (I) :	I2	Isotope number	
W-5 (I) :	JFLVRT(1)	Reference number efficiency for the is <i>Acceptable range:</i> <i>Default value:</i>	of a Tabular or a Control Function that defines filter sotope I2 must be a valid reference number of a Tabular or Control Function, if nonzero none

..., until the efficiencies are specified for all isotopes

### 2.15.94 Records: 296XXX, Pool Scrubbing Model for Fission Product Vapors

XXX is the Junction reference number,  $001 \le XXX \le 999$ . When a stream of gas enters a pool region of the receiving Control Volume, then it forms bubbles in the pool. The gas is assumed to quickly reach equilibrium at the entrance to the pool (the equilibrium conditions are calculated by the Bubble Collapse Model). At the end of the bubble collapse the mass flow of gas entering the pool,  $W_B$ , is divided into the mass flow of gas,  $W_G$ , and condensed liquid,  $W_L$ . The flow  $W_G$  forms bubbles in the pool, while  $W_L$  remains in the pool. The FP vapors entering the pool with the stream of gas are divided as follows:

- The part  $W_L/W_B$  remains in the pool.
- The part  $W_G / W_B$  is transported partly to the atmosphere and partly remains in the pool, depending on the pool adsorption efficiency.

Therefore the division of aerosol particles is:

• F	raction remaining in	n the pool:	$\frac{W_G}{W_B}E_{PV} + \frac{W_L}{W_B}$
• F	raction reaching the	e atmosphere:	$\frac{W_G}{W_B}(1-E_{PV})$
W-1 (R) :	JPLVRT(1)	Reference number adsorption efficience Acceptable range: Default value:	of a Tabular or a Control Function that defines pool cy, $E_{PV}$ , for the vapor class 1, (-). must be a valid reference number of a Tabular or Control Function, if nonzero none
W-2 (R) :	JPLVRT(2)	Reference number adsorption efficience Acceptable range: Default value:	of a Tabular or a Control Function that defines pool cy, $E_{PV}$ , for the vapor class 2, (-). must be a valid reference number of a Tabular or Control Function, if nonzero none

..., until the efficiencies are specified for all vapor classes.

#### 2.15.95 Records: 195000, Pool-Gas Transport of FP Vapors - Global

This record contains global transport coefficient,  $\mathcal{G}_{pool-atms}$ , for the vapor classes (detailed description is provided in record 195XXX, containing individual activators).

W-1 (R) :	DCPGRT(1) Global transport coefficient for the vapor class 1.			
	Acceptable range:	$0.0 \le \text{DCPGRT}(1) \le 10.0$		
	Default value:	0.0		
W-2 (R) :	DCPGRT(2) Global transport c	coefficient for the vapor class 2.		

Acceptable range: $0.0 \le \text{DCPGRT}(2) \le 10.0$ Default value:0.0

... until coefficients are defined for all vapor classes.

#### 2.15.96 Records: 195XXX, Pool-Gas Transport of FP Vapors - Individual

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . If fission product vapors are present in the pool, they may be transported to the pool-atmosphere (or pool-bubble) surface and enter the atmosphere of the Control Volume. The effect is calculated using a transport coefficient, defined below. the transfer process is calculated only if the pool-gas transport is activated in records 196000, 196XXX.

W-1 (R) : DCPART(1) Mass transfer coefficient (net velocity of FP molecules towards the pool surface or bubble surface) for the vapor class 1 isotopes present in the pool,  $\mathcal{G}_{pool-gas}$ , (m/s). The mass transfer rate is:

$$\frac{dm}{dt} = \mathcal{G}_{pool-gas} \cdot \rho_{pool} \cdot A_{pool} = \mathcal{G}_{pool-gas} \cdot \frac{M_{pool}}{V_{pool}} \cdot A_{pool}$$

 $\rho_{pool}$  - density of the fission product in the pool, (kg/m<sup>3</sup>)  $A_{pool}$  - surface area (m<sup>2</sup>) (depending on IPATRT this may be poolatmosphere, bubble-surface or both)

- $V_{pool}$  volume of the pool, (m<sup>3</sup>),
- $M_{pool}$  mass of the fission product in the pool, (kg)

The rate of change of the fission product vapor mass in the pool is:

$$\left(\frac{dM_{pool}}{dt}\right) = \begin{cases} -\mathcal{P}_{pool-gas} \cdot \frac{M_{pool}}{V_{pool}} \cdot A_{pool} & \text{if } p_{atms} < p_{sat} \\ 0.0 & \text{if } p_{atms} > p_{sat} \end{cases}$$

If a negative number is entered, then the Sherwood number correlation is used, defined in the record 8960XX, where XX is the set number, equal to -DCPART

Acceptable range:0.<DCPART(1)<10. or set number with minus sign</th>Default value:DCPGRT(1) - see record 195000

... until coefficients are defined for all vapor classes.

#### 2.15.97 Records: 196000, Option for Pool-Gas Transport of FP Vapors – Global

Using this record one may specify the parameter described in record 196XXX for all Control Volumes in the model - see description of record 196XXX below.

#### 2.15.98 Records: 196XXX, Option for Pool-Gas Transport of FP Vapors – Individual

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ . If fission product vapors are present in the pool, they may be transported to the pool-atmosphere (or pool-bubble) surface and enter the atmosphere of the Control Volume. This record defines where the transport is occurring.

W-1 (I) :	IPATRT	<ul> <li>Pool-gas transport of fission products.</li> <li>=0: no pool-gas transport of fission product occurs</li> <li>=1 : transport occurs on the pool-atmosphere surface</li> <li>=2 : transport occurs on the bubble-pool surface.</li> <li>=3 : transport occurs on droplet-atmosphere surface.</li> <li>NOTE: with option 2, fission products are transported from one CV to another with bubble flow. With option 3, fission products are not transported with droplets from one CV to another. Therefore the droplet to and from CV is automatically disabled: IDFAJN is set to 1.</li> <li><i>Acceptable range:</i> IPATRT = 0, 1, 2, 3</li> <li><i>Default value:</i> 0</li> </ul>
W-2 (R) :	XPATRT	Multiplier for the pool-gas transport. The pool-gas transport calculated by the model described in record 8960XX, is multiplied by this value. This parameter is used for any transport defined by IPATRT. It may be used for example to model sticking fraction in case of pool-bubble transport.

Acceptable range:  $0.0 \le \text{XPATRT} \le 10.0$ 

*Default value:* 1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0).

W-3 (I):ISVBRTIndicator for FP transport from pool to atmosphere. The meaning is the<br/>same as in case of bubble transport: ISVBCV - see Figure 2-3.<br/>Acceptable range:  $0 \le ISVBRT \le 100$ <br/>Default value:ISVBCV

#### 2.15.99 Records: 8960XX, Pool-Gas Transport of FP Vapors Sh Correlation

XX is the set number.  $01 \le XX \le 99$ . The set number is selected for a given fission product vapor class in the records 195000 and 195XXX. If fission product vapors are present in the pool, they may be transported to the pool surface and/or bubble surface. The transport velocity is obtained using the Sherwood number correlation.

$$Sh = A_{Sh} + B_{Sh} \frac{Re^{C_{Sh}} Sc^{D_{Sh}}}{1 + E_{Sh} Re^{F_{Sh}} Sc^{G_{Sh}}}$$

Here *Sh* is the Sherwood number, *Re* is the Reynolds number, *and Sc* is the Schmidt number. The coefficients,  $A_{Sh}$ ,  $B_{Sh}$ ,  $C_{Sh}$ ,  $D_{Sh}$ ,  $E_{Sh}$ ,  $F_{Sh}$ ,  $G_{Sh}$ , are defined below. The mass transfer coefficient (net velocity of vapor flow towards the pool surface or bubble surface) is obtained from:

$$\mathcal{G}_{pool-gas} = Sh \frac{D_C}{D_{hvd}}$$

Here  $D_{hyd}$  is the hydraulic diameter (m), and  $D_C$  is the diffusion coefficient (m<sup>2</sup>/s).

W-1 (R) :	DXPART	Diffusion coefficient in liquid, $D_C$ , $(m^2/s)$ . If a positive value is entered, $D_C = DXPART$ If a negative value is entered, $D_C = TF$ number $ DXPART $ . The argument for the TF is the liquid temperature. Acceptable range: $0.0 < DXPART \le 1.0$ or a valid reference to Tabular Function
		Default value: 0.0
W-2 (R) :	ASPART	$A_{Sh}$ in the user-defined Sherwood number correlation: $Acceptable range: -10^{10} \le ASPART \le 10^{10}$ $Default value: 0.0$
W-3 (R) :	BSPART	$B_{Sh}$ in the Sherwood number correlation:Acceptable range: $0.0 \le BSPART \le 10^{10}$ Default value: $0.0$
W-4 (R) :	CSPART	$C_{Sh}$ in the Sherwood number correlation:Acceptable range: $0.0 \le \text{CSPART} \le 10.0$ Default value: $0.0$
W-5 (R) :	DSPART	$D_{Sh}$ in the Sherwood number correlation: <i>Acceptable range:</i> $0.0 \le \text{DSPART} \le 10.0$ <i>Default value:</i> $0.0$

W-6 (R) :	ESPART	$E_{Sh}$ in the Sherwood Acceptable range: Default value:	d number correlation: $0.0 \le \text{ESPART} \le 10^{10}$ 0.0
W-7 (R) :	FSPART	$F_{Sh}$ in the Sherwood Acceptable range: Default value:	d number correlation: $0.0 \le \text{FSPART} \le 10.0$ 0.0
W-8 (R) :	GSPART	<i>G<sub>sh</sub></i> in the Sherwoo <i>Acceptable range:</i> <i>Default value:</i>	d number correlation: 0.0 ≤ GSPART ≤ 10.0 0.0

The next two words are used only if fission products are transported as particles. i.e. if the particle diameter (DPFPRT) and density (RHFPRT) is specified in the record 8932XX and transport on bubble surface is active IPATRT=2. If that is the case, the Sh number correlation described above may be replaced by an alternative way of calculating the pool-gas transport, which uses Brownian diffusion and inertial impaction models on the surface of bubbles in the pool:

$$\mathcal{G}_{pool-gas} = v_{Brown} + v_{inertial}$$

where:

$$v_{Brown} = \frac{D_C}{\delta_{BL}}$$
$$v_{inertial} = v_{\infty} \cdot \eta \cdot A_{h,bubb} / A_{bubb} = v_{\infty} \cdot \eta / 4$$

*v*<sub>Brown</sub> Brownian deposition, (m/s)

*v*<sub>inertial</sub> inertial impaction deposition, (m/s)

 $D_C$  diffusion coefficient, (m<sup>2</sup>/s)

 $\delta_{BL}$  diffusion boundary layer thickness, (m) (=10<sup>-5</sup>)

 $A_{h,bubb}$  horizontal cross section area of a bubble, (m<sup>2</sup>), =  $\pi \times D_{bubb}^2 / 4$ 

 $A_{bubb}$  total surface area of a bubble, (m<sup>2</sup>),  $= \pi \times D_{bubb}^2$ 

 $v_{\infty}$  particle-to-bubble relative velocity, (m/s)

 $\eta$  collection efficiency, calculated from one of three correlations, described below.

*Langmuir and Blodgett (L-B) correlation - Figure 2-79* 

$$\eta = \eta_{\max} \cdot \frac{Stk^2}{\left(Stk + C_{LB}\right)^2}$$

 $C_{LB}$  constant (=0.25, see [54], eq. 3)

 $\eta_{max}$  maximum value of collection efficiency (=1.0)

Stk Stokes number, (-), see Volume 1 for detailed description.

Modified Langmuir and Blodgett correlation - Figure 2-80

$$\eta = \eta_{\max} \cdot \begin{cases} \frac{0.25}{C_{LB}} \cdot Stk & for \quad Stk < C_{LB} \\ \frac{Stk^2}{\left(Stk + C_{LB}\right)^2} & for \quad Stk > C_{LB} \end{cases}$$



Figure 2-79 Langmuir and Blodgett correlation



Figure 2-80 Modified versus original Langmuir and Blodgett correlation

Correlation developed based on data of Yoon & Lutrell and Afruns & Kitchener - Figure 2-81

$$\eta = Min\left(\eta_{\max}, A \cdot \frac{d_p^2}{D_b}\right)$$

In order to activate the model, non-zero values must be supplied for at least two out of the following three input entries:

W-9 (R): TBL1RT Diffusion boundary layer thickness,  $\delta_{BL}$ , (m).

Acceptable range:  $1.0 \times 10^{-7} \le \text{TBL1RT} \le 1.0 \times 10^{-3}$ . Default value: none If the model is used, the recommended value is  $5.0 \times 10^{-5}$ . W-10 (R) : CLB1RT Constant in the correlation for inertial impaction,  $C_{LB}$ . CLB1RT  $\leq$  10: *C*<sub>*LB*</sub>, in the L-B or modified L-B correlation (depending on ILBORT, record 860000) CLB1RT > 1000: A in the correlation developed based on data of Yoon & Lutrell and Afruns & Kitchener Acceptable range:  $10^{-2} \le \text{CLB1RT} \le 10^{+1} C_{LB}$ , in L-B, modified L-B  $10^{+3} \le \text{CLB1RT} \le 10^{+5} A$  in YLAK correlation none Default value: If the model is used, the recommended value is 0.25.

W-11 (R): ELB1RT Maximum efficiency  $\eta_{max}$ , in the correlation for inertial impaction Acceptable range:  $10^{-3} \le \text{ELB1RT} \le 10^{+3}$ Default value: 1.0 if the model is used (if TBL1RT>0.0, CLB1RT>0.0)



Figure 2-81 Data of Yoon & Lutrell and Afruns & Kitchener and correlation

### 2.15.100 Records: 385XXX, Leaching Input Parameters for SC

This record defines leaching parameters. XXX is the 1-D Solid Heat Conductor reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	LILCRT	Leaching model indicator. = 0 : no leaching is applied, = 1 : leaching is applied on the left boundary surface = 2 : leaching is applied on the right boundary surface = 3 : leaching is applied on both boundary surfaces Acceptable range: 0, 1, 2, 3 Default value: 0
W-2 (I) :	KKI	Reference number of the isotope, where KK is the chain reference number and I is the isotope number within the chain KK. This isotope is being leached from the boundary surface of SC. <i>Acceptable range:</i> must be a valid reference number <i>Default value:</i> none.
W-3 (R) :	CALCRT	Average initial concentration (mass fraction) of the isotope KKI, (-). The initial mass of the isotope of KKI is equal to the total mass of the material in the SC node multiplied by this number. The initial mass is set only in the cells with the same material as in the boundary cell (the leached alloy). If LLILCRT=3, then the material in both left and right boundary cells must be the same. The same concentration is applied in all nodes with the leached material, unless the concentrations are defined differently in the records $393XXX$ . <i>Acceptable range:</i> 0.0 < CALCRT< 0.5 <i>Default value:</i> none.
W-4 (R) :	TOLCRT	Characteristic time (s) for the surface concentration to reach zero (Stage I).Acceptable range: $10^2 \le \text{TOLCRT} \le 10^6$ Default value: $10^3$

#### NOTE!

A sorption model must be activated on the surface on which the leaching model is applied. Furthermore, the parameter ISRLRT must be set to 2 (sorption in liquid). The sorption model must be a CF type. Two methods are available:

• If the diffusion coefficient of the surface material is defined, then the diffusion model is used and the Control Function is a dummy and the value of the CF is not important. In that case a fine nodalization must be used.

0	size of the nodes close to the boundary:	$10^{-6} - 10^{-5} \text{ m} (1 - 10 \ \mu\text{m}),$
0	applied for at least:	$5 \times 10^{-4}$ m (50 µm) depth.

• If the diffusion coefficient of the surface material is not defined, then the value of surface mass flux is equal to the value of the CF. In lack of diffusion, the material will be leached from the boundary cell only. Therefore the boundary cell must be large enough. The following limits are set by the input procedures:

 $\circ$  minimum required size of the boundary node:  $10^{-4}$  m (100 µm)

 $10^{-3} \text{ m} (1000 \ \mu\text{m})$ 

• recommended size of the boundary node:

The following limits are internally imposed on the value obtained from the CF:

- $\circ \quad CF \leq 0.0$
- $\circ$  CF  $\geq -1.0 \times 10^{-6}$

Example:

The following example defines chromium leaching on the left surface of SC-991.

```
* ---- Leaching model
* LEACRT KKI CALCRT TOLCRT
385991 1 191 0.07 1.0E3
* ---- Define stable isotope Cr-52, Isotope 191, member of vapor class 7
F05191 Cr-52
* M-core MW beta gamma yield
880191 0.0 52 0.0 0.0 0.0
885191 07 * release class
886191 07 * vapor class
*
* ---- Sorpion definition
* LEFT RIGHT
*
   SET MULT. SET MULT.
395991 1 0.0 0 0.0
*Vap-7: model ISRLRT
895107 -100 2 * cf-100, ISRLRT=2 (LIQUID)
705100 SORPTION CF (dummy)
* Group Number Fact. Const.
700100 1 1 1.0 0.0
* Arguments
* Pointers: (1) (2) (3) (4) Fact. Const
710100 9 000 1 0 1.0 0.0 * time
```

#### 2.15.101 Records: 386000, Leaching Model General Parameters

W-1 (R) :	TMLCRT	Minimum temperature (K) for the reaction. The reaction is not proceeding if the surface temperature is smaller than TMLCRT. An interpolation zone of DTLCRT is assumed. The diffusion-controlled reaction reaches full speed if the temperature exceeds TMLCRT+DTLCRT. Acceptable range: $273.0 \le \text{TMLCRT} \le 10,000.0$
W-2 (R) :	DTLCRT	Interpolation temperature range (K) for the reaction. The diffusion- controlled reaction reaches full speed if the temperature exceeds TMLCRT+DTLCRT.

Acceptable range: $10.0 \le \text{DTLCRT} \le 100.0$ Default value:50.0

### 2.15.102 Records: 8970XX, List of RT Isotopes Mapped to CV Gases

XX is the list number. Usually isotopes are treated as trace species; the isotope mass is not considered in the CV Package. Using this list, the user may link the RT isotope masses to the CV gas masses for the cases when the effect of gas pressurization is considered non-negligible. A mass source referring to this list must be specified in the records 13YXXX. The maximum number of lists is 20 (=NGMXFL).

W-1 (I) :	Ι	Gas number The H 3=steam, $4=N_2$ , $5=0$ Acceptable range: Default value:	built-in gases are: 0=water (liquid), 1=H <sub>2</sub> , 2=He, D <sub>2</sub> , 6=CO <sub>2</sub> . $1 \le I \le NGASCV \le NGMXFL = 20$ none.
W-2 (I) :	KKI(1)	Reference number of reference number an Acceptable range: Default value:	of the first isotope on this list, where KK is the chain and I is the isotope number within the chain KK. must be an existing isotope none.
W-3 (I) :	KKI(2)	Reference number chain reference num Acceptable range: Default value:	of the second isotope on this list, where KK is the aber and I is the isotope number within the chain KK. must be an existing isotope none.

... until all isotopes are defined. The maximum number of isotopes on one list is 20.

An example is shown below. The example shows how to link Xenon and Krypton isotopes in the RT Package to Xenon and Krypton gases in the FL Package.

```
* Xe isotopes -> Xe gas (user-defined gas number 11)
* Gas Xe-131m Xe-131 Xe-132 Xe-133m Xe-134 Xe-135m Xe-135 Xe-137
897001 11 015 016 023 035 043 052 053 061
*
* Kr isotopes -> Kr gas (user-defined gas number 10)
* Gas Kr-85m Kr-85 Kr-90
897002 10 083 084 091
```

The gases must be defined in the FL input. An example of such input is shown in:

\Z-INPUTS\FL\GAS\CO-Ar-Ne-Kr-Xe-H2.ATT

The example above is valid if all built-in isotope chains are used (see 2.15.111). If additional isotopes are defined in the RT input, the list above must be appended accordingly. An example of additional isotope inputs for Xe and Kr isotopes is shown in:

\Z-INPUTS\RT\DECAY-CHAINS

#### 2.15.103 Records: 898000, Selection of Sorption Processes on Aerosol Particles

The sorption on aerosol particles, defined in this record, is applied for all aerosol particles, including the particles deposited on structures.

W-1 (I): IASRRT(1) Number of sorption set (defined in records 895YXX) to be used on the surface of the aerosol particles in a Control Volume, either atmosphere

	or pool of CV. The input parameter ISRLRT (record 895YXX) determines if sorption occurs in the gas or the liquid phase. <i>Acceptable range:</i> must be one of existing sorption sets, if nonzero <i>Default value:</i> 0
W-2 (R) :	YASRRT(1) Multiplier for the sorption model applied on the aerosol particles in a Control Volume. The sorption rate that is calculated by the sorption model selected by the previous word, is multiplied by this value. <i>Acceptable range:</i> $0.0 \le$ YASRRT(1) $\le 10.0$ . For the sorption model 2 (see 895YXX) only 1.0 and 0.0 may be used. Zero may be used to disable the sorption model but keep track of the penetrated and reversibly-bound molecules (the latter may for example be washed by water pool).
	<i>Default value:</i> 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0).
W-3 (I) :	IASRRT(2) Number of sorption set (defined in records 895YXX) to be used on the surface of the aerosol particles deposited on the surfaces of 1-D Solid Heat Conductors, either on the uncovered or on the pool-covered surface. The input parameter ISRLRT (record 895YXX) determines if sorption occurs in the gas or the liquid phase. It is recommended to use the same set on all aerosol particles, IASRRT(2) = IASRRT(1). <i>Acceptable range:</i> must be one of existing sorption sets, if nonzero <i>Default value:</i> 0
W-4 (R) :	YASRRT(2) Multiplier for the sorption model applied on the aerosol particles deposited on the surfaces of 1-D Solid Heat Conductors. The sorption rate that is calculated by the sorption model selected by the previous word, is multiplied by this value.
	Acceptable range: $0.0 \le \text{YASRRT}(2) \le 10.0$ . For the sorption model 2 (see 895YXX) only 1.0 and 0.0 may be used. Zero may be used to disable the sorption model but keep track of the penetrated and reversibly-bound molecules (the latter may for example be washed by water pool).
	<i>Default value:</i> 1.0 (a small number, $<10^{-50}$ , sets the value to 0.0).
W-5 (I) :	<ul> <li>IASRRT(3) Number of sorption set (defined in records 895YXX) to be used on the surface of the aerosol particles deposited on the surfaces of 2-D Solid Heat Conductors, either on the uncovered or on the pool-covered surface. The input parameter ISRLRT (record 895YXX) determines if sorption occurs in the gas or the liquid phase. It is recommended to use the same set on all aerosol particles, IASRRT(3) = IASRRT(2) = IASRRT(1).</li> <li>Acceptable range: must be one of existing sorption sets, if nonzero Default value: 0</li> </ul>
	Degana rame. 0
W-6 (R) :	YASRRT(3) Multiplier for the sorption model applied on the aerosol particles deposited on the surfaces of 2-D Solid Heat Conductors. The sorption rate that is calculated by the sorption model selected by the previous word, is multiplied by this value.

		Acceptable range:	$0.0 \le \text{YASRRT}(3) \le 10.0$ . For the sorption model 2 (see 895YXX) only 1.0 and 0.0 may be used. Zero may be used to disable the sorption model but keep track of the penetrated and reversibly-bound molecules (the latter may for example be washed by water pool).
		Default value:	1.0 (a small number, $<10^{-50}$ , sets the value to 0.0).
W-7 (I) :	IAFPRT	Apply adjustment of =1: Adjustment is a is set to the total m vapor classes for (PATRAS/SPATR =2: Adjustment is n Acceptable range: Default value:	of fission products adsorbed on aerosol particles: applied. At the end of a time step, the penetrated mass mass and the reversible mass is set to zero for those or which model other than the Model 2 A model) is applied. not applied. 1 or 2 1

### 2.15.104 Records: 197XXX, Initial Masses of Isotopes on Aerosol Particles

XXX is the CV reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	ITP	Data type indicator, 1=airborne aerosol particles, 2=particles deposited in the pool. The data specified by the Words below is applied for either airborne or pool-deposited particles depending on ITP <i>Acceptable range:</i> 1 or 2 <i>Default value:</i> none.
W-2 (I) :	KKI	Reference number of the isotope, where KK is the chain reference number and I is the isotope number within the chain KK. <i>Acceptable range:</i> must be a valid reference number if nonzero <i>Default value:</i> none.
	<u>If ITP = 1</u>	<u>.</u>
W-3 (R) :	YN5CRT(	1) Initial mass fraction of the isotope KKI (both reversibly-bound and penetrated) present in the aerosol particles of the size section 1 in the

W-4 (R): YP5CRT(1) Initial fraction of the penetrated mass of the isotope KKI present in the aerosol particles of the size section 1 in the Control Volume XXX, (-). Used only if the sorption model 2 is used for the aerosol particles (sorption set is selected in the record 898001).

Acceptable range: $YP5CRT(1) \le YN5CRT(1)$  for sorption model 2YP5CRT(1) = YN5CRT(1) for other modelDefault value:0.0

- W-5 (R) :YN5CRT(2) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 2, present<br/>in the Control Volume XXX, (-).<br/>Acceptable range:  $0.0 \leq \text{YN5CRT}(2) \leq 1.0$ <br/>Default value: 0.0
- W-6 (R) :YP5CRT(2) Initial fraction of the penetrated mass of the isotope KKI present in the<br/>aerosol particles of the size section 2 in the Control Volume XXX, (-).<br/>Used only if the sorption model 2 is used for the aerosol particles<br/>(sorption set is selected in the record 898001)<br/>Acceptable range:<br/>YP5CRT(2)  $\leq$  YN5CRT(2) for sorption model 2<br/>YP5CRT(2) = YN5CRT(2) for other model<br/>Default value:

... until data for all size sections is specified.

# <u>If ITP = 2:</u>

- W-3 (R) :YN6CRT(1) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 1,<br/>deposited in the pool of Control Volume XXX, (-).<br/>Acceptable range:  $0.0 \leq$  YN6CRT(1)  $\leq$  1.0<br/>Default value: 0.0
- W-4 (R) :YP6CRT(1) Initial fraction of the penetrated mass of the isotope KKI present in the<br/>aerosol particles of the size section 1 deposited in the pool of Control<br/>Volume XXX, (-). Used only if the sorption model 2 is used for the<br/>aerosol particles (sorption set is selected in the record 898001).<br/><br/>Acceptable range:YP6CRT(1)  $\leq$  YN6CRT(1) for sorption model 2<br/>YP6CRT(1) = YN6CRT(1) for other model<br/>Default value:
- W-5 (R) :YN6CRT(2) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 2,<br/>deposited in the pool of Control Volume XXX, (-).<br/><br/>Acceptable range:  $0.0 \leq \text{YN6CRT}(2) \leq 1.0$ <br/>Default value: 0.0
- W-6 (R) :YP6CRT(2) Initial fraction of the penetrated mass of the isotope KKI present in the<br/>aerosol particles of the size section 2, deposited in the pool of the Control<br/>Volume XXX, (-). Used only if the sorption model 2 is used for the<br/>aerosol particles (sorption set is selected in the record 898001).<br/>Acceptable range:<br/>YP6CRT(2)  $\leq$  YN6CRT(2) for sorption model 2<br/>YP6CRT(2) = YN6CRT(2) for other model<br/>Default value:

... until data for all size sections is specified.

The data sets for different isotopes should be entered in different records with the same number. For each aerosol size sections the sum of fractions entered in these records must be smaller than or equal to 1.0.

# 2.15.105 Records: 397XXX, Initial Masses of Isotopes on Particles Deposited on SC

XXX is the SC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IBC	Boundary surface specified by the We initially deposited of <i>Acceptable range:</i> <i>Default value:</i>	number, 1=left surface, 2=right surface. The data ords below is applied for the aerosol particles that are on the boundary surface IBC. 1 or 2 none.
W-2 (I) :	KKI	Reference number number and I is the <i>Acceptable range:</i> <i>Default value:</i>	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-3 (R) :	YN7FRT(1)	) Initial mass fracti penetrated) presen deposited on the bo XXX, (-). Acceptable range: Default value:	on of the isotope KKI (both reversibly-bound and t in the aerosol particles of the size section 1, undary surface IBC of the 1-D Solid Heat Conductor $0.0 \le \text{YN7FRT}(1) \le 1.0$ 0.0
W-4 (R) :	YP7FRT(1)	Initial fraction of th aerosol particles of IBC of the 1-D Soli model 2 is used for record 898001). Acceptable range: Default value:	The penetrated mass of the isotope KKI present in the the size section 1, deposited on the boundary surface d Heat Conductor XXX, (-). Used only if the sorption r the aerosol particles (sorption set is selected in the YP7FRT(1) $\leq$ YN7FRT(1) for sorption model 2 YP7FRT(1) = YN7FRT(1) for other model 0.0
W-5 (R) :	YN7FRT(2	) Initial mass fracti penetrated) presen deposited on the bo XXX, (-). <i>Acceptable range:</i> <i>Default value:</i>	on of the isotope KKI (both reversibly-bound and t in the aerosol particles of the size section 2, undary surface IBC of the 1-D Solid Heat Conductor $0.0 \le \text{YN7FRT}(2) \le 1.0$ 0.0
W-6 (R) :	YP7FRT(2)	Initial fraction of th aerosol particles of IBC of the 1-D Soli model 2 is used for record 898001). Acceptable range: Default value:	The penetrated mass of the isotope KKI present in the the size section 2, deposited on the boundary surface d Heat Conductor XXX, (-). Used only if the sorption r the aerosol particles (sorption set is selected in the YP7FRT(2) $\leq$ YN7FRT(2) for sorption model 2 YP7FRT(2) = YN7FRT(2) for other model 0.0

... until data for all size sections is specified. The data sets for different boundary surfaces and different isotopes should be entered in different records with the same number. For each aerosol size section the sum of fractions entered in these records must be smaller than or equal to 1.0.

#### 2.15.106 Records: 497XXX, Initial Masses of Isotopes on Particles Deposited on TC

XXX is the TC reference number,  $001 \le XXX \le 999$ .

W-1 (I) :	IBC	Boundary cell num for the aerosol part boundary cell IBC. <i>Acceptable range:</i> <i>Default value:</i>	ber. The data specified by the Words below is applied icles that are initially deposited on the surface of the 1 or 2 none.
W-2 (I) :	KKI	Reference number number and I is the Acceptable range: Default value:	of the isotope, where KK is the chain reference isotope number within the chain KK. must be a valid reference number if nonzero none.
W-3 (R) :	YN8FRT(1	) Initial mass fracti penetrated) presen deposited on the su Conductor XXX, (- Acceptable range: Default value:	on of the isotope KKI (both reversibly-bound and the in the aerosol particles of the size section 1, rface of the boundary cell IBC of the 2-D Solid Heat -). $0.0 \le \text{YN8FRT}(1) \le 1.0$ 0.0
W-4 (R) :	YP8FRT(1)	) Initial fraction of th aerosol particles of IBC of the 2-D Soli model 2 is used for record 898001). Acceptable range: Default value:	The penetrated mass of the isotope KKI present in the f the size section 1, deposited on the boundary cell d Heat Conductor XXX, (-). Used only if the sorption r the aerosol particles (sorption set is selected in the YP8FRT(1) $\leq$ YN8FRT(1) for sorption model 2 YP8FRT(1) = YN8FRT(1) for other model 0.0
W-5 (R) :	YN8FRT(2	) Initial mass fracti penetrated) presen deposited on the su Conductor XXX, (- Acceptable range: Default value:	on of the isotope KKI (both reversibly-bound and t in the aerosol particles of the size section 2, rface of the boundary cell IBC of the 2-D Solid Heat -). $0.0 \le \text{YN8FRT}(2) \le 1.0$ 0.0
W-6 (R) :	YP8FRT(2	) Initial fraction of the aerosol particles of IBC of the 2-D Soli model 2 is used for record 898001). Acceptable range: Default value:	The penetrated mass of the isotope KKI present in the f the size section 2, deposited on the boundary cell d Heat Conductor XXX, (-). Used only if the sorption r the aerosol particles (sorption set is selected in the YP8FRT(2) $\leq$ YN8FRT(2) for sorption model 2 YP8FRT(2) = YN8FRT(2) for other model 0.0

. . . until data for all size sections is specified. The data sets for different boundary surfaces and different isotopes should be entered in different records with the same number. For each aerosol size section the sum of fractions entered in these records must be smaller than or equal to 1.0.

## 2.15.107 Records: 198XXX, Isotopes on External Sources of Aerosols

XXX is the CV reference number,  $001 \le XXX \le 999$ . The external sources of aerosols are specified in records 175XXX. The present records may be used to define the isotopes that are present in the aerosols coming from the external sources.

- W-1 (I): KKI Reference number of the isotope, where KK is the chain reference number and I is the isotope number within the chain KK. *Acceptable range:* must be a valid reference number if nonzero *Default value:* none.
- W-2 (R):YNSCRT(1) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 1, coming<br/>from the external source defined in the record 175XXX into the Control<br/>Volume XXX, (-).<br/><br/>Acceptable range:  $0.0 \leq \text{YNSCRT}(1) \leq 1.0$ <br/>Default value: 0.0
- W-3 (R): YPSCRT(1) Initial fraction of the penetrated mass of the isotope KKI present in the aerosol particles of the size section 1, coming from the external source defined in the record 175XXX into the Control Volume XXX, (-). Used only if the sorption model 2 is used for the aerosol particles (sorption set is selected in the record 898001).

Acceptable range: $YPSCRT(1) \le YNSCRT(1)$  for sorption model 2YPSCRT(1) = YNSCRT(1) for other modelsDefault value:0.0

- W-4 (R) :YNSCRT(2) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 2, coming<br/>from the external source defined in the record 175XXX into the Control<br/>Volume XXX, (-).<br/><br/>Acceptable range:  $0.0 \leq \text{YNSCRT}(2) \leq 1.0$ <br/>Default value: 0.0
- W-3 (R): YPSCRT(2) Initial fraction of the penetrated mass of the isotope KKI present in the aerosol particles of the size section 2, coming from the external source defined in the record 175XXX into the Control Volume XXX, (-). Used only if the sorption model 2 is used for the aerosol particles (sorption set is selected in the record 898001).
   Acceptable range: YPSCRT(2) ≤ YNSCRT(2) for sorption model 2 YPSCRT(2) = YNSCRT(2) for other models

*Default value:* 0.0

 $\dots$  until data for all size sections is specified. The data sets for different isotopes should be entered in different records with the same number. For each aerosol size section the sum of fractions entered in these records must be smaller than or equal to 1.0.

### 2.15.108 Records: 398XXX, Isotopes on External Sources of SC-Deposited Aerosols

XXX is the SC reference number,  $001 \le XXX \le 999$ . The external sources of aerosols are specified in records 375XXX. The present records may be used to define the isotopes that are present in the aerosols coming from the external sources.

- W-1 (I): KKI Reference number of the isotope, where KK is the chain reference number and I is the isotope number within the chain KK. *Acceptable range:* must be a valid reference number if nonzero *Default value:* none.
- W-2 (R):YNS7RT(1) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 1, coming<br/>from the external source defined in the record 375XXX onto the surfaces<br/>of 1-D Solid Heat Conductor XXX, (-).<br/>Acceptable range:  $0.0 \le$  YNS7RT(1)  $\le$  1.0<br/>Default value: 0.0
- W-3 (R) :YPS7RT(1) Initial fraction of the penetrated mass of the isotope KKI present in the<br/>aerosol particles of the size section 1, coming from the external source<br/>defined in the record 375XXX onto the surfaces of 1-D Solid Heat<br/>Conductor XXX, (-). Used only if the sorption model 2 is used for the<br/>aerosol particles (sorption set is selected in the record 898001).<br/>Acceptable range:<br/>YPS7RT(1)  $\leq$  YNS7RT(1) for sorption model 2<br/>YPS7RT(1)  $\leq$  YNS7RT(1) for other models<br/>Default value:
- W-4 (R) :YNS7RT(2) Initial mass fraction of the isotope KKI (both reversibly-bound and<br/>penetrated) present in the aerosol particles of the size section 2, coming<br/>from the external source defined in the record 375XXX onto the surfaces<br/>of 1-D Solid Heat Conductor XXX, (-).<br/>Acceptable range:  $0.0 \le$  YNS7RT(2)  $\le$  1.0<br/>Default value: 0.0
- W-3 (R) :YPS7RT(2) Initial fraction of the penetrated mass of the isotope KKI present in the<br/>aerosol particles of the size section 2, coming from the external source<br/>defined in the record 375XXX onto the surfaces of 1-D Solid Heat<br/>Conductor XXX, (-). Used only if the sorption model 2 is used for the<br/>aerosol particles (sorption set is selected in the record 898001).<br/>Acceptable range:<br/>YPS7RT(2)  $\leq$  YNS7RT(2) for sorption model 2<br/>YPS7RT(2) = YNS7RT(2) for other models<br/>Default value:

 $\dots$  until data for all size sections is specified. The data sets for different isotopes should be entered in different records with the same number. For each aerosol size section the sum of fractions entered in these records must be smaller than or equal to 1.0.

#### 2.15.109 Records: 498XXX, Isotopes on External Sources of TC-Deposited Aerosols

XXX is the TC reference number,  $001 \le XXX \le 999$ . The external sources of aerosols are specified in records 475XXX. The present records may be used to define the isotopes that are present in the aerosols coming from the external sources.

W-1 (I) :	KKI	Reference number of the isotope, where KK is the chain reference number and I is the isotope number within the chain KK. <i>Acceptable range:</i> must be a valid reference number if nonzero <i>Default value:</i> none.
W-2 (R) :	YNS8RT(	1) Initial mass fraction of the isotope KKI (both reversibly-bound and penetrated) present in the aerosol particles of the size section 1, coming from the external source defined in the record 475XXX onto the surfaces of 2-D Solid Heat Conductor XXX, (-). Acceptable range: $0.0 \leq \text{YNS8RT}(1) \leq 1.0$ Default value: 0.0
W-3 (R) :	YPS8RT(	) Initial fraction of the penetrated mass of the isotope KKI present in the aerosol particles of the size section 1, coming from the external source defined in the record 475XXX onto the surfaces of 2-D Solid Heat Conductor XXX, (-). Used only if the sorption model 2 is used for the aerosol particles (sorption set is selected in the record 898001). Acceptable range: $YPS8RT(1) \le YNS8RT(1)$ for sorption model 2 YPS8RT(1) = YNS8RT(1) for other models Default value: 0.0
W-4 (R) :	YNS8RT(	2) Initial mass fraction of the isotope KKI (both reversibly-bound and penetrated) present in the aerosol particles of the size section 2, coming from the external source defined in the record 475XXX onto the surfaces of 2-D Solid Heat Conductor XXX, (-). Acceptable range: $0.0 \le \text{YNS8RT}(2) \le 1.0$ Default value: 0.0
W-3 (R) :	YPS8RT(	2) Initial fraction of the penetrated mass of the isotope KKI present in the aerosol particles of the size section 2, coming from the external source defined in the record 475XXX onto the surfaces of 2-D Solid Heat Conductor XXX, (-). Used only if the sorption model 2 is used for the aerosol particles (sorption set is selected in the record 898001). Acceptable range: YPS8RT(2) $\leq$ YNS8RT(2) for sorption model 2 YPS8RT(2) = YNS8RT(2) for other models Default value: 0.0

 $\dots$  until data for all size sections is specified. The data sets for different isotopes should be entered in different records with the same number. For each aerosol size section the sum of fractions entered in these records must be smaller than or equal to 1.0.

#### 2.15.110 Records: 199XXX, Radiation Exposure and Dose Parameters

XXX is the Control Volume reference number,  $001 \le XXX \le 999$ .

\_

W-1 (R): CG1DRT Multiplier  $C_{\gamma,1}$  (-), in the formula for the  $\gamma$ -radiation flux. The full formula is (see Volume 1 for detailed explanation):

$$\varphi_{\gamma,i} = C_{\gamma,1} \cdot \frac{0.620}{V_{CV}^{2/3}} \cdot S_{i,CV} + C_{\gamma,2} \cdot \frac{0.207}{V_{CV}^{2/3}} \cdot \left(S_{i,CV-pool} + \sum_{SC \in CV} S_{i,SC} + \sum_{TC \in CV} S_{i,TC}\right)$$

Acceptable range:  $10^{-6} \le \text{CG1DRT} \le 10^{6}$ Default value: 1.0

- W-2 (R): CG2DRT Multiplier  $C_{\gamma,2}$  (-), in the formula for the  $\gamma$ -radiation flux. Acceptable range:  $10^{-6} \le \text{CG2DRT} \le 10^{6}$ Default value: 1.0
- W-3 (R): CB1DRT Multiplier  $C_{\beta,1}$  (-), in the formula for the  $\gamma$ -radiation flux. The full formula is (see Volume 1 for detailed explanation):

$$\varphi_{\beta,i} = C_{\beta,1} \cdot \frac{S_{i,CV} \cdot \rho}{(\mu_{a,\beta} / \rho)} \cdot \left(1 - \exp[-(\mu_{a,\beta} / \rho) \cdot (\rho R)]\right) + C_{\beta 2} \cdot \frac{0.207}{V_{CV}^{2/3}} \left(S_{i,CV-pool} + \sum_{SC \in CV} S_{i,SC} + \sum_{TC \in CV} S_{i,TC}\right) \cdot \exp[-(\mu_{a,\beta} / \rho) \cdot (\rho R)]$$

Acceptable range:  $10^{-6} \le CB1DRT \le 10^{6}$ Default value: 1.0

- W-4 (R): CB2DRT Multiplier  $C_{\beta,2}$  (-), in the formula for the  $\gamma$ -radiation flux. Acceptable range:  $10^{-6} \le \text{CB2DRT} \le 10^{6}$ Default value: 1.0
- W-5 (R): QFGMRT Quality factor for the  $\gamma$ -radiation,  $Q_{\gamma}$ . Used to calculate the dose equivalent, *H*:

$$H = D_{\gamma} \cdot Q_{\gamma} + D_{\beta} \cdot Q_{\beta}$$

Acceptable range:  $10^{-6} \le \text{QFGMRT} \le 10^{6}$ Default value: 1.0

W-6 (R): QFBTRT Quality factor for the  $\beta$ -radiation,  $Q_{\beta}$ . Acceptable range:  $10^{-6} \le \text{QFBTRT} \le 10^{6}$ Default value: 1.0

### 2.15.111 Built-in Fission Product Chains (Decay Chains)

The built-in decay chains are shown in Figure 2-83 through Figure 2-92. Isotopes are shown in colours depending on their decay half-life time, T. The red colour is used for the short-life isotopes (T of order of minutes). The stable isotopes are shown in blue. The applied colour scale is shown in Figure 2-82. List of all built-in isotopes and their reference numbers is given in Table 2-47.







Figure 2-83 Decay chain,  $M_w = 131$ .



Figure 2-84 Decay chain,  $M_w = 132$ .



Figure 2-85 Decay chain,  $M_w = 133$ .



Figure 2-86

Decay chain,  $M_w = 134$ .



Figure 2-87 Decay chain,  $M_w = 135 / 136$ .



Figure 2-88 Decay chain,  $M_w = 136$ .



Figure 2-89 Decay chain,  $M_w = 138$ .









Figure 2-92

Decay chain,  $M_w = 106$ .

### Table 2-47 List of all built-in isotopes, reference numbers, names, and nuclear data.

	Fission Yield	Capture Cross-sec	Capture Cross-sec			Fission Yield	Capture Cross-sec	Captur Cross-s
i Isotope	(-)	(barn)	(m2)	i	Isotope	(-)	(barn)	(m2)
11 Sb-131	2.60000E-02	0.00000E+00	0.00000E+00	061	I-136	3.10000E-02	0.00000E+00	0.00000E
12 Te-131m	4.00000E-03	0.00000E+00	0.00000E+00	062	Xe-136	3.40000E-02	0.00000E+00	0.00000E
13 Te-131	0.00000E+00	0.00000E+00	0.00000E+00					
14 I-131	2.90000E-02	6.00000E-01	6.00000E-29	071	Xe-137	6.00000E-02	0.00000E+00	0.0000E-
15 Xe-131m	0.00000E+00	7.55000E+01	7.55000E-27	072	Cs-137	1.50000E-03	1.10000E-01	1.10000E-
16 Xe-131	0.00000E+00	7.55000E+01	7.55000E-27	073	Ba-137m	0.00000E+00	5.10000E+00	5.10000E-
				074	Ba-137	0.00000E+00	5.10000E+00	5.10000E-
21 Te-132	4.70000E-02	0.00000E+00	0.00000E+00					
22 I-132	0.00000E+00	0.00000E+00	0.00000E+00	081	Se-85	1.10000E-02	0.00000E+00	0.0000E+
23 Xe-132	0.00000E+00	0.00000E+00	0.00000E+00	082	Br-85	0.00000E+00	0.00000E+00	0.0000E+
				083	Kr-85m	0.00000E+00	1.70000E+00	1.70000E-
31 Sb-133	4.00000E-02	0.00000E+00	0.00000E+00	084	Kr-85	3.00000E-03	1.70000E+00	1.70000E-
32 Te-133m	9.00000E-03	0.00000E+00	0.00000E+00	085	Rb-85	0.00000E+00	9.60000E-01	9.60000E-
33 Te-133	0.00000E+00	0.00000E+00	0.00000E+00					
34 I-133	2.00000E-02	0.00000E+00	0.00000E+00	091	Kr-90	5.00000E-02	0.00000E+00	0.0000E+
35 Xe-133m	0.00000E+00	1.68000E+02	1.68000E-26	092	Rb-90m	0.00000E+00	0.00000E+00	0.0000E+
36 Xe-133	0.00000E+00	1.68000E+02	1.68000E-26	093	Rb-90	0.00000E+00	0.00000E+00	0.0000E+
37 Cs-133	0.00000E+00	2.59000E+01	2.59000E-27	094	Sr-90	7.70000E-03	9.00000E-01	9.00000E-
				095	Y-90	0.00000E+00	6.50000E+00	6.50000E-
41 Te-134	6.90000E-02	0.00000E+00	0.00000E+00	096	Zr-90	0.00000E+00	5.31000E+00	5.31000E-
42 I-134	9.00000E-03	0.00000E+00	0.00000E+00					
43 Xe-134	3.00000E-03	2.60000E-01	2.60000E-29	101	Ru-106	3.80000E-03	1.50000E-01	1.50000E-
				102	Rh-106	0.00000E+00	0.00000E+00	0.0000E+
51 I-135	6.30000E-02	2.00000E-01	2.00000E-29	103	Pd-106	0.00000E+00	5.71000E+00	5.71000E-
52 Xe-135m	0.00000E+00	2.72000E+06	2.72000E-22					
53 Xe-135	2.00000E-03	2.72000E+06	2.72000E-22					
54 Cs-135	0.00000E+00	8.00000E+00	8.00000E-28			5.23000E-01		
55 Ba-135	0.00000E+00	0.00000E+00	0.00000E+00					

### 2.16 Transient Solution and Output Frequency Parameters

### 2.16.1 Record: 900000, Initial Time

W-1 (R): TSTART Start time for the analysis, (s) Acceptable range:  $-10^{10} \le \text{TSTART} \le +10^{10}$ . Default value: 0.0.

# 2.16.2 Records: 900XXX, Time Step Data

XXX = 001, 002, ..., NTSMAX, is the number of the time step domain. The maximum number of time step domains is 999. The maximum and minimum time steps, print and plot frequency are controlled by the data on these records. The data are valid for times smaller than the domain end time, entered as the last word in these records. The first domain is in effect from the time equal to zero to the end time for the first domain. The next domains are active for times larger than the end time for the previous domain and smaller or equal to the end time of the current domain.

W-1 (R) :	DTMAX	Maximum time step, (s). The maximum time step can be redefined during calculations, using the SPECTRA Stop File, "* <b>.STP</b> " (see section 3.8). This is done as follows. The stop file has to be put in the directory where the run is performed. The program will (among others) ask for the new maximum time step. If zero is entered the current value will be unchanged. If a positive value is entered, it will be used provided that it is not smaller than the minimum time step and not larger than 10 times the then current maximum time step. <i>Acceptable range:</i> $10^{-10} \le \text{DTMAX} \le 10^{10}$ . <i>Default value:</i> 0.1.
W-2 (R) :	DTMIN	Minimum time step, (s). The minimum time step can be redefined during calculations, using the SPECTRA Stop File, " <b>*.STP</b> " (see section 3.8). This is done as follows. The stop file has to be put in the directory where the run is performed. The program will (among others) ask for the new minimum time step. If zero is entered the current value will be unchanged. If a positive value is entered, it will be used provided that it is not smaller than $10^{-20}$ and not larger than current minimum time step. <i>Acceptable range:</i> $10^{-20} \le \text{DTMIN} \le \text{DTMAX}$ . <i>Default value:</i> $10^{-6}$ .
W-3 (R) :	DTPRT	$\begin{array}{llllllllllllllllllllllllllllllllllll$

W-4 (R) :	DTPLT	Plot frequency, (s). A negative value results in plot point being written every time step.Acceptable range:DTMAX $\leq$ DTPLT $\leq 10^{10}$ or DTPLT<0.0 (TENDI(i) - TSTART)/200, if i=1, (TENDI(i) - TENDI(i-1))/200, if i>1, where i is the time step domain number.
W-5 (R) :	TENDI	<ul> <li>End time for this domain, (s). The end time for the last domain determines the time when the transient calculations are terminated. Calculations can also be terminated at any time using the SPECTRA Stop File, "*.STP" (see section 3.8). This is done as follows. The stop file has to be put in the directory where the run is performed. The program will (among others) ask for the new end time. If zero is entered the current value will be unchanged. If a positive value is entered, it will be used provided that it is not smaller the current time and not larger than the end of the next time step domain (if exists).</li> <li>Acceptable range: End time values must increase. Thus the value must be greater than the value of TENDI for the previous domain.</li> <li>Default value: none.</li> </ul>
W-6 (I) :	IOPSL	<ul> <li>Solver options valid for this domain. Using this input entry the user can deactivate the thermal-hydraulic packages, such as CV, JN, etc. This means the conditions in all Control Volumes, Junctions, etc. will be frozen during the whole time domain. This option is useful if the thermal-hydraulic packages require a lot of computing time (for example small Courant Limit), while the user needs a long calculation, with quasi-stationary thermal-hydraulic conditions. This may be the case if for example the user wishes to calculate a long term behavior (days, months, or even years) with practically constant thermal-power (long term operation with nominal power). In such run the parameters of interest may be:</li> <li>Reactor Kinetics related parameters: <ul> <li>depletion of fuel,</li> <li>accumulation of fission product poisons following start-up</li> <li>re-loading rate,</li> </ul> </li> <li>Radioactive Particle Transport Related parameter: <ul> <li>accumulation of dust particles in various parts of the system during normal operation,</li> <li>accumulation of radioactive isotopes in various parts of the system</li> </ul> </li> </ul>

during normal operation

The meaning of IOPSL is as follows:

- IOPSL = 0: normal calculations (all packages active)
- IOPSL = 1: deactivate CV/JN/H2 package.
- IOPSL = 2 : deactivate CV/JN/H2 and SC/TC/TR/OX packages

IOPSL = 3 : deactivate CV/JN/H2 and SC/TC/TR/OX and TF/CF packages. Only the TF-YYY or the CF-YYY (see below) is recalculated. IOPSL = 1YYY: the option is defined by a Tabular Function TF-YYY, where YYY = IOPSL-1000. The value of TF-YYY is rounded to the nearest integer and set to the range between 0 and 3. If the value is 3, then the TF/CF packages are deactivated with the exception of TF-YYY.

IOPSL = 2YYY: the option is defined by a Control Function CF-YYY, where YYY = IOPSL-2000. The value of CF-YYY is rounded to the nearest integer and set to the range between 0 and 3. If the value is 3, then the TF/CF packages are deactivated with the exception of CF-YYY and any TF that is being used by the CF-YYY.

Acceptable range:0, 1, 2, or reference to a Tabular FunctionDefault value:0

W-7 (I): IRKSL Additional action for the reactor kinetics model in case of deactivated thermal-hydraulic packages. This input entry determines the behavior of the Reactor Kinetics Package in case when IOPSL > 0.

1: the RK is active; the reactivity is kept constant.

2: the RK is active; the reactor total power is kept constant by using a power controller. If this option is used, the constants in the PI power controller are defined in the record 761000. This option is not recommended. If the power is to be kept constant it is recommended to use option 1 or 4.

3: the RK is active; no specific actions are taken to ensure constant power or reactivity.

4: the RK is inactive; the reactor fission power is kept constant. However, changes in the isotope concentrations are calculated. The macroscopic fission cross section (RK-000-SigF-0000) and, consequently, the neutron density and the neutron flux (RK-000-Neut-0000, RK-000-Flux-0000) as well as the DNP concentrations (RK-000-Cpre-00nn) are updated to obtain the stationary state values corresponding to the current SigF.

In the case of circulating fuel (IFTORK=2) two chains, DNP and DHG, are excluded from the solution (the concentrations are kept constant). This is because these chains contain short living isotopes. The flow solution for these isotopes would not be accurate for time steps significantly larger than the Courant limit.

Acceptable range: 1, 2, 3, 4 Default value: 4

W-8 (I): ICVSL Additional action for the Control Volumes with time dependent conditions in case of deactivated thermal-hydraulic packages. This input entry determines the behavior of Control Volumes for which ITYPCV  $\neq 0$  (record 100XXX) and parameters are defined by Tabular or Control Functions (record 125XXX).

1 : do not recalculate conditions in these Control Volumes (keep the parameters constant) when IOPSL > 0.

2: recalculate conditions in these Control Volumes (use the Tabular or Control Function Values) when IOPSL > 0.

Acceptable range: 1, 2 Default value: 1

W-9 (R) :DTRSTRestarting frequency, (s).<br/>Acceptable range:<br/>Default value:DTMAX  $\leq$  DTRST  $\leq$  1010.<br/>(TENDI(i) - TSTART)/2 for i=1<br/>(TENDI(i) - TENDI(i-1))/2 for i>1<br/>where i is the time step domain number. If the value<br/>obtained from the above formulae is smaller than<br/>1000×DTMAX, it is se to 1000×DTMAX. This is<br/>done to avoid excessive restarts when for short time<br/>domains.

Example inputs with the use of non-standard Solver options is presented below: In the first run a PBMR fuel reloading rate needed at nominal power is being determined. The computation time was set at 1 month  $(2.6 \times 10^6 \text{ s})$ . In the second run transport and deposition of radioactive isotopes during normal operation is analysed. The analysis time is 1 year  $(3.2 \times 10^7 \text{ s})$ .

* 1	Max.dt	Min.dt	Print	Plot	End time	Solver	optio	ons	
*	(s)	(s)	(s)	(s)	(s)	IOPSL	IRKSL	ICVSL	
900001	0.1	1.0E-6	0.0	0.0	1000.0	0	0	0 *	1000 s to get stable conditions
900002	1000.	1.0E-6	0.0	0.0	2.6E+6	1	3	0 *	1 month analysis, keep feedback
*								*	from SC (fuel temperatures),
*								*	do not control power -
*								*	the fuel reloading will keep
*								*	the power constant
* 1	Max.dt	Min.dt	Print	Plot	End time	Solver	optio	ons	
* I *	Max.dt (s)	Min.dt (s)	Print (s)	Plot (s)	End time (s)	Solver IOPSL	optio	ons ICVSL	
* 1 * 900001	Max.dt (s) 0.1	Min.dt (s) 1.0E-6	Print (s) 0.0	Plot (s) 0.0	End time (s) 1000.0	Solver IOPSL 0	optio IRKSL 0	ons ICVSL 0 *	1000 s to get stable conditions
* N * 900001 900002	Max.dt (s) 0.1 1000.	Min.dt (s) 1.0E-6 1.0E-6	Print (s) 0.0 0.0	Plot (s) 0.0 0.0	End time (s) 1000.0 3.2E+7	Solver IOPSL 0 2	optio IRKSL 0 4	ons ICVSL 0 * 0 *	1000 s to get stable conditions 1 year simulation with large dt
* M * 900001 900002 *	Max.dt (s) 0.1 1000.	Min.dt (s) 1.0E-6 1.0E-6	Print (s) 0.0 0.0	Plot (s) 0.0 0.0	End time (s) 1000.0 3.2E+7	Solver IOPSL 0 2	optio IRKSL 0 4	ons ICVSL 0 * 0 * *	1000 s to get stable conditions 1 year simulation with large dt and deactivated CV/JN/
* M 900001 900002 *	Max.dt (s) 0.1 1000.	Min.dt (s) 1.0E-6 1.0E-6	Print (s) 0.0 0.0	Plot (s) 0.0 0.0	End time (s) 1000.0 3.2E+7	Solver IOPSL 0 2	c optic IRKSL 0 4	ons ICVSL 0 * * *	1000 s to get stable conditions 1 year simulation with large dt and deactivated CV/JN/ to compute fission product
* N 900001 900002 * *	Max.dt (s) 0.1 1000.	Min.dt (s) 1.0E-6 1.0E-6	Print (s) 0.0 0.0	Plot (s) 0.0 0.0	End time (s) 1000.0 3.2E+7	Solver IOPSL 0 2	optic IRKSL 0 4	ons ICVSL 0 * 0 * * *	1000 s to get stable conditions 1 year simulation with large dt and deactivated CV/JN/ to compute fission product transport and accumulation
* 1 900001 900002 * * *	Max.dt (s) 0.1 1000.	Min.dt (s) 1.0E-6 1.0E-6	Print (s) 0.0 0.0	Plot (s) 0.0 0.0	End time (s) 1000.0 3.2E+7	Solver IOPSL 0 2	optio IRKSL 0 4	DNS ICVSL 0 * * * *	1000 s to get stable conditions 1 year simulation with large dt and deactivated CV/JN/ to compute fission product transport and accumulation during normal operation

#### 2.16.3 Record: 905000, Read Initial Conditions from a File

W-1 (A): ICFILE File name containing initial conditions. The extension (default: ".ICF") must be included in the name.
 Every time a calculation is finished, the program writes the current conditions (pressures, temperatures, fluid velocities, etc.) to a file with extension ".ICF" . This file may be used to overwrite the initial conditions entered in the input deck.

Typically an input model of a power plant is prepared, and then steady state calculations are performed until all parameters are stable. If the steady state calculations are long, then it is convenient to store the calculated parameters, and use them as a starting point for subsequent accident analyses. Then, to perform the accident analysis, user has to:

- attach the base model (see ATTACH statement, page 1-1),
- use this record to read initial conditions from a file, and
- define accident specific records.

In an example shown below, the base model of a NPP is stored as a file "BASE". Example of the steady state input deck is shown below.

The analyzed accident is a leak from the primary system (CV-001) to the environment (CV-030). The leak is defined by adding one Junction (JN-051). The input deck is shown below.

It is important to note the principal differences between using restart (see section 2.20), and using the initial condition file. Those differences are listed below.

1.) Restart

With restart all variables from all program data bases are saved and then read in binary format. When calculations are stopped and then restarted, then, unless the time steps are altered on restart, the results obtained after the restart are identical to those which would be obtained if the job proceeded without stopping. Very few numbers can be altered on restart (time step size, end time, diagnostics printout). The restart option is intended to allow continuation of a run that for some reason has been stopped. When a job is restarted no input processing is performed.

2.) Initial Condition File (ICF)

With ICF only the initial conditions are saved and read from a file. The file is in text format, thus the initial conditions can be altered by the user. When a job is stopped and then started again using ICF, the results are slightly different from those which would be obtained without stopping, because data is stored in formatted file, and not all data base is stored. With ICF the user can change practically anything in his input deck. Node numbers should not be changed because the values stored on ICF would then fall into wrong nodes. A limited re-nodalization with number changes is possible, but the user has then to manually fix the ICF, to make it appropriate for the new nodalization. When ICF is
used, the whole input processing is performed as usually. At the end of the input processing phase ICF is read, and the initial conditions for CVs, JNs, SCs, CFs, and isotopes, stored in the ICF, replace those present in the input deck. The values stored in ICF are used only for those nodes for which the option "use entered values" is selected. The appropriate options for JNs, SCs, CFs, and isotopes are read in records 201XXX, 301XXX, 701XXX, 740000 respectively. The value of 2 in records 201XXX, 301XXX, 701XXX, and the value of 1 in the record 740000 mean "use enter value". In such cases the value entered in input file or read from ICF is used. *Acceptable range:* any string of up to 50 characters.

Default value: none.

Example of a (steady state) run with the base model stored in a file "BASE"

= Input file for steady state run (file: STEADY)
\*
ATTACH BASE \* Attach base model of NPP
\*
\* Define time steps
\* Maximum dt Minimum dt Print dt Plot dt End time
\* (s) (s) (s) (s) (s)
900001 0.1 0.0001 100.0 10.0 1000.0 \* 1000 s of steady state run

Example input of a simple accident scenario (LOCA), using the base model BASE.

Input file for accident analysis (LOCA from CV-001 to CV-030) \* ATTACH BASE Attach base model of NPP 905000 STEADY.ICF \* Read initial conditions calculated in staedy state run Define time steps \* Maximum dt Minimum dt Print dt Plot dt End time (s) \* (s) (s) (s) (s) 0.0001 500.0 5000.0 \* 5000 s of transient run 900001 0.1 10.0 \* Define leak (note that the initial condition data for this JN is not present in ICF) 205051 Leak model \* From To Area Elevation Length 200051 001 030 0.01 2.5 1.0 2.5

#### 2.16.4 Record: 910000, Advancement Message Frequency, Extended Diagnostics

W-1 (R): DTSCR Screen (terminal) message frequency, (s). The information about current model time, time step and the CPU time used so far is written to the screen approximately every DTSCR seconds of the processor time. If not entered, or the entered value is out of the acceptable range it is automatically reset to the default value. Acceptable range:  $1.0 \le \text{DTSCR} \le 600.0$ Default value: 1.0

W-2 (I): NADIA Advancement message frequency, (-). At the end of each time step advancement, the information is available what time step (s) was used and how many iterations were performed. This information may be written to the diagnostics file. NADIA is the number of advancements between messages written to the diagnostics file. If not entered, or the entered value is out of the acceptable range it is automatically reset to the default value.

Acceptable range:	$1 \le N$	$ADIA \le 100,000$	
Default value:	1	for analysis times:	$t \le 10^4  { m s}$
	10	for analysis times:	$10^4 \text{ s} < t \le 10^6 \text{ s}$
	100	for analysis times:	$10^6 \text{ s} < t \le 10^8 \text{ s}$
	1000	for analysis times:	$10^8 \text{ s} < t \le 10^{10} \text{ s}$
	10000	) for analysis times:	$10^{10}  \mathrm{s} < t$

W-3 (I): IEXDIA Request for extended SOLVER diagnostics output. If a number different than zero is entered, then the following information is written to the diagnostics file in case of non-convergent iterations: the values of those variables that didn't converge, including values assumed and calculated for the last two iterations.

The extended diagnostics can also be requested during the run using the SPECTRA Stop File, "**\***.**STP**" (see section 3.8). This is done as follows. The stop file has to be put in the directory where the run is performed. The program will (among others) ask if the extended diagnostics should be activated in the next part of the run. If the answer is "Y" then the extended diagnostics will be activated. Any other answer will result in suppressing the extended diagnostics. The extended diagnostics can only be requested if the diagnostics file is not suppressed (see section 2.16.7, below).

*Acceptable range:* all integers. *Default value:* 0

W-4 (I): XDEBUG Request for debug print-out. If XDEBUG is greater than zero then the debug printout is written to the diagnostics file. The debug printout consists of the values of all iterated variables, controlled by the SOLVER. Values assumed and calculated in each iteration are printed for all iterations, for times greater than TDEBUG (s), where TDEBUG is defined as: TDEBUG = XDEBUG –  $1.0 \times 10^6$ .

The debug printout writes large amount of data to the diagnostics file and thus should be used with care.

The debug printout can also be requested during the run using the SPECTRA Stop File, "**\*.STP**" (see section 3.8). This is done as follows.

The stop file has to be put in the directory where the run is performed. The program will ask if the user wishes to terminate the calculation. The user should answer 'N' (no). Then the program will (among others) ask if the debug printout should be activated in the next part of the run. If the answer is "Y" then the debug printout will be activated. Any other answer will result in suppressing the debug printout. The debug printout can only be requested if the diagnostics file is not suppressed (see section 2.16.7, below). Acceptable range: XDEBUG >  $0.9 \times 10^6$  if non-zero. Thus the debug printout can be activated for the times greater than: -100,000 (s). 0

Default value:

W-5 (I) :	IMESAG	Message write option. Messages on changes of valve status, pump status
		may be written to a message file (*.MES) and the screen.
		=1: messages are written to the message file
		=2: messages are writted to the message file and the screen
		Acceptable range: 1, 2
		Default value: 1

## 2.16.5 Record: 920000, Iteration Parameters

The parameters listed below control the numerical solution procedure. All of them have their default values. Any change in those parameters should be done with caution, since it may result in slowing down the solution or even causing the code to crash.

W-1 (I) :	MAXITR	Number of iterations to cut the time step. If the solution does not converge in MAXITR iterations then SOLVER repeats the advancement with a reduced time step. The value of the new, reduced time step, is determined by the time step reduction factor, DTREDN, (Word 3, below). Acceptable range: $10 \le MAXITR \le 200$ Default value: 50
W-2 (I) :	MINITR	Number of iterations to increase the time step. If, due to non-convergent iterations or failure, the time step has been reduced below the maximum value (DTMAX, section 2.16.2) in previous advancements, then during subsequent advancements SOLVER tries to increase the time step to reach again DTMAX. This increase is attempted only if the last advancement has been solved in less than MINITR iterations. Acceptable range: $10 \le MINITR \le 50$ , MINITR $\le MAXITR$ , MINITR $\ge ITMNSL$ (Word 14) Default value: 20
W-3 (R) :	DTREDN	Time step reduction ratio in case of non-convergent iterations. If the solution does not converge in MAXITR (Word 1 above) iterations, then SOLVER attempts to repeat the advancement with a new, reduced time step. The reduced time step is obtained as: $\Delta t' = \Delta t/\text{DTREDN}$ , where $\Delta t$ is the time step for which the solution did not converge. If DTREDN is

too large, then time step reduction may be unnecessarily too severe, thus increasing the execution time.

Acceptable range:  $2.0 \le \text{DTREDN} \le 16.0$ Default value: 4.0

W-4 (R): DTREDF Time step reduction ratio in case of failure. Failure may occur for a number of reasons. For example, water property routines may be called with temperatures beyond the data range, a linear equation solver may fail (singular matrix), etc. If such failure occurs, then a recovery from the failure is possible. On recovery, the advancement is repeated with a new, reduced time step. The reduced time step is obtained as:  $\Delta t' = \Delta t/DTREDF$ , where  $\Delta t$  is the time step for which the failure occurred. Because the number of recoveries is limited (see Word 7, below), the time step reduction should be significant, to limit the possibility that the failure will occur again, forcing to use more recovery processes.

Acceptable range: $4.0 \le \text{DTREDF} \le 32.0$ Default value:8.0

W-5 (R): DTINC Maximum time step increase factor, (-). If, due to non-convergent iterations or failure, the time step had been reduced below the maximum value (DTMAX) in previous advancements then during subsequent advancements SOLVER tries to increase the time step to reach again DTMAX. This increase is attempted only if the last advancement was solved in less than MINITR (Word 2, above) iterations, and is limited to the ratio defined by DTINC. Thus the new time step is obtained as:  $\Delta t' = \Delta t^*$ DTINC, where  $\Delta t$  is the time step at which solution converged in less than MINITR iterations.

The DTINC is not used in case the code runs with maximum time step and a new time step domain is reached. In that case SOLVER tries to use the new maximum time step, no matter how different it might be from the previous maximum time step. When this attempt is unsuccessful, it will try to reduce the time step.

Acceptable range:  $1.001 \le \text{DTINC} \le 10^6$ Default value: 1.30278... This partic

1.30278... This particular value was selected to allow the code to come back to the same end-ofadvancement time points after a reduction of the time step by a factor of 2 (or multiple factors of 2). For example: suppose the maximum time step is 1.0. The end-of-advancement time points are: 1.0, 2.0, 3.0, etc. At certain moment, say 3.0 s, SOLVER cuts the time step by half. Then, if it increases the time step using the default value of DTINC, the following end-of-advancements time points will be: 3.5, 4.1514, 5.0, 6.0, etc. Thus when the maximum time step is re-reached (5.0 s), then the end-ofadvancement time points will be exactly the same as if the reduction of time step did not occur. The exact value is defined by the positive root of the following quadratic equation:

 $DTINC^2 + DTINC - 3.0 = 0.0$ 

IACTFL W-6(I): Action to be taken on failure. The value determines the kind of action that will be taken in case a failure occurs during calculations. IACTFL=1: write output, plot, and diagnostics edits, restart file, and terminate the run. IACTFL=2: continue calculations with reduced time step. The new time step is defined by the factor DTREDF (Word 4, above). Acceptable range:  $1 \leq \text{IACTFL} \leq 2$ Default value: 1 W-7 (I): LSTACK Limit in recovery from failure. If the value of IACTFL (Word 6, above) is equal to 2, then in case of failure the recovery procedure is applied, and the run is continued with reduced time step. This recovery procedure is invoked only up to LSTACK times. If failure occurs more than LSTACK times then the run is terminated. Increased value of LSTACK will allow more error recoveries. However, the number of error recoveries is also limited by the FORTRAN stack limit. If LSTACK is made too large, then the program may stop on the stack limit. If the stack is exceeded, then the FORTRAN run-time error message is printed: "Program stack exceeded", and the run is immediately terminated. This should be avoided, because if this happens neither the diagnostics message nor the output and plot edits from SPECTRA are available at the time of the crash. The acceptable range and the default value were set based on experience with the Lahey FORTRAN compiler [12], and may be different for other compilers. Acceptable range:  $10 \le \text{LSTACK} \le 20$ Default value: 15 IACSFL W-8 (I): Action to be taken on failure during initial state calculations. Sometimes convergence failure may occur during the initial state calculations, when SC or TC temperatures need to be initialized (INTSC=1 - section 2.3.3, or INTTC=1 - section 2.4.3) in a steady-state step. One solution is to initialize SCs manually (set INTSC, INTTC to 2 and provide the initial temperatures in the input deck). Other solution is to ignore the failure, and start the transient calculations from the obtained conditions. Ignoring the failure is often the best choice, since even un-converged calculated SC temperatures are typically better than can be obtained by

IACSFL=1:	write output edit and terminate the run.
IACSFL=2:	ignore the failure and continue.
Acceptable range:	$1 \leq IACSFL \leq 2$
Default value:	1

manual initialization.

**Solver Convergence Criteria** 

- It is not recommended to change the Solver convergence criteria.
- If frequent time step cuts are observed, but the values of un-converged parameters (printed if the extended diagnostic option is used record 910000, Word 3) do not change much from iteration to iteration, then an increase of the convergence criteria may be considered as a method of speeding up the calculations.

W-9 (R) :	CCCASL	Solver convergence calculated value. ' between the param during this iteration Acceptable range: Default value:	e criterion on the difference between the assumed and The criterion is satisfied if the relative difference heter value assumed for the iteration and calculated h, is smaller than CCCASL. $10^{-5} \le CCCASL \le 10^{-1}$ $10^{-3}$
W-10 (R) :	CCAASL	Solver convergence previously assume difference between the value assumed <i>Acceptable range:</i> <i>Default value:</i>	e criterion on the difference between the assumed and ed value. The criterion is satisfied if the relative the parameter value assumed for the last iteration and for the previous iteration, is smaller than CCAASL. $10^{-6} \le \text{CCAASL} \le 10^{-2}$ $10^{-4}$
W-11 (R) :	ABSLSL	Absolute limit on a defined by Words if the absolute valu Acceptable range: Default value:	a parameter value. The Solver convergence criteria, 9 and 10 above, are bypassed for a given parameter, e of the parameter is smaller than ABSLSL. $10^{-20} \le ABSLSL \le 1.0$ $10^{-10}$
W-12 (R) :	CMCASL	Multiplier on CCC Acceptable range: Default value:	ASL for the reactor kinetics model. $1.0 \le CMCASL \le 100.0$ 1.0
W-13 (R) :	CMAASL	Multiplier on CCA Acceptable range: Default value:	ASL for the reactor kinetics model. 1.0 ≤ CMAASL ≤ 100.0 1.0
W-14 (I) :	ITMNSL	Minimum number Acceptable range: Default value:	of iterations to accept the solution. 1 ≤ ITMNSL ≤ 20 3 5 if decay chains are used, i.e. if NDCHRT > 0 9 if LFM is used, i.e. if MSFMJN = 2
W-15 (I) :	DISTIN	Initial disturbance Acceptable range: Default value:	(relative) to start the solution procedure. $10^{-10} \le \text{DISTIN} \le 10^{-1}$ $10^{-2}$

Solver Convergence Criteria for FP Masses

- The accuracy of the FP solution is judged by a global mass balance for fission products. If the mass error becomes large, the calculations are stopped. In such case it is best to eliminate the mass error using the AMFPRT > 0 option. The user may also try to reduce time step or decrease the convergence criteria. The recommended values are given in the descriptions below and summarized in Table 2-48.
- The default values were set to provide fast but less accurate solutions. The values were successfully tested for time steps up to 10<sup>5</sup> s.

W-16 (R) :	FCCASL	Solver convergence gas space of Contro for fission product : Acceptable range: Default value:	e criterion applied for fission product masses in the ol Volumes. Same as CCCASL (Word 9) but applied masses. $10^{-4} \le \text{FCCASL} \le 10^{+10}$ $10^{+1}$ . If a large mass error is encountered, then it is recommended to use $10^{-1}$ . This will increase accuracy at the expense of computing time.
W-17 (R) :	FCAASL	Solver convergence gas space of Contro for fission product <i>Acceptable range</i> : <i>Default value</i> :	e criterion applied for fission product masses in the d Volumes. Same as CCAASL (Word 10) but applied masses. $10^{-5} \le \text{FCAASL} \le 10^{+10}$ $10^{0}$ . If a large mass error is encountered, then it is recommended to use $10^{-2}$ . This will increase accuracy at the expense of computing time.
W-18 (R) :	FABLSL	Absolute limit on a in the gas space of applied for fission p Acceptable range: Default value:	a parameter value applied for fission product masses Control Volumes. Same as ABSLSL (Word 11) but product masses. $10^{-40} \le FABLSL \le 1.0 \times 10^{-10}$ $10^{-30}$
W-19 (I) :	ITMXSL	Maximum number Acceptable range: Default value:	of iterations to accept the fission product solution. ITMNSL < ITMXSL $\leq$ MAXITR 15. If a large mass error is encountered, then it is recommended to use 40. This will increase accuracy at the expense of computing time.
W-20 (I) :	IFPESL	Indicator for fission = 0: calculations are > 0: calculations are < 0: calculations are Note that FP mass (input record 88000 Note: mass conserv (1) fission products (2) there is no sorpt (3) all daughter radioactive chains) If (1), (2), or (3) is a Acceptable range:	n product (FP) mass error treatment. e stopped when the FP mass error exceeds 10%, e stopped when the error exceeds IFPESL %, e never stopped because of FP mass error. error may be eliminated by using the AMFPRT > 0 00). It is usually best to use the AMFPRT > 0 option. vation is possible only if: c cannot flow to/from time-dependent CVs tion on surfaces linked to time-dependent CVs products of radioactive decay are tracked (full not fulfilled, IFPESL should be set to < 0. all integers

Default value: -1 if (1), (2), or (3) is not fulfilled 0 otherwise

Table 2-48 Recommended convergence criteria for fission product mass

	Parameter			
Calculation type	FCCASL	FCAASL	ITMXSL	
Fast but less accurate	10 <sup>1</sup>	100	15	
Accurate but slow	10-1	10 <sup>-2</sup>	40	

#### 2.16.6 Record: 925000, Reduction of Solid Material Specific Heat for Steady State

Calculations are often started with an approach to steady state. Such approach may be significantly accelerated by reducing the volumetric heal capacity ( $\rho \times c_p$ ) of materials present in the model. Using this record, the user may reduce the volumetric heat capacity of all solid materials (used by SC and TC). The fluid properties in Control Volumes remain unaltered.

W-1 (R) :	CREDSL	Reduction factor, (-). The reduction factor is applied if a positive valueis entered.Acceptable range: $0.001 \le CREDSL \le 1.0$ , if non-zeroDefault value:none
W-2 (R) :	TREDSL	End-time, (s), to apply the reduction factor CREDSL. For times greater than TREDSL the reduction is not applied (the reduction factor is set to 1.0). <i>Acceptable range:</i> TREDSL > TSTART (start time, record 900000) <i>Default value:</i> none

#### 2.16.7 Record: 930000, Suppressing the Diagnostics File

W-1 (I):	IDIAFL	Indicator defining whether the warning and error messages are printed into the diagnostics file.
		If IDIAFL=0 then warning and error messages are printed into the
		diagnostics file. In some cases this may result in very large diagnostics
		file.
		If IDIAFL≠0 then warning and error messages suppressed. No
		information is printed to the diagnostics file during the calculations. The
		diagnostics file is closed at the end of input processing phase. This
		option saves the disk space and speeds up the calculations. The
		disadvantage of using this option is the lack of diagnostics messages in case of severe numerical problems.
		If IDIAFL≠0 then the extended diagnostics and the debug printout are
		automatically suppressed (IEXDIA and XDEBUG are set to zero - see section 2.16.4)
		Acceptable range: any integer.
		Default value: 0.

#### 2.16.8 Record: 931000, Adjusting Time Step at the End of Time Domain

W-1 (I): ITSNSL Indicator defining whether the time step should be adjusted at the end of each time step domain to finish each domain at exactly the specified time point.

1: Do not adjust time step. In the example shown in section 2.16.11 the first time step domain ends at 100.0 s. If the code is at 99.3 s and runs with the maximum time step of 1.0 s, then it will finish this domain and proceed to the next one at the time of 100.3 s.

2: Adjust the time step to finish each time step domain at exactly the specified time point. In the example shown in section 2.16.11 the first time step domain ends at 100.0 s. If the code is at 99.3 s and runs with the maximum time step of 1.0 s, then it will automatically reduce this time step to 0.7 s, in order to finish this time step domain and proceed to the next one at exactly 100.0 s. This option may be important if certain events (for example break opening, control system actions) need to occur at precisely the start of certain time domain.

Acceptable range: 1 or 2 Default value: 1

#### 2.16.9 Record: 940000, Interactive Simulation Activation

W-1 (I): ISIMUL Activator of an interactive simulation run. In a non-interactive run, the computations are entirely determined by the input deck.. The results may be viewed using the plot file \*.PLT (or the output file, \*.OUT), when the calculations are finished. In an interactive run the values of all Tabular Functions that are defined as interactive may be changed (by the simulation program, which writes appropriate commands to the \*.TFD file). The results maybe viewed during the calculations because SPECTRA writes every plot point separately (file \*.SIM). Additionally SPECTRA writes the headers (variable names) in the file \*.SIN. The simulation program (VISOR) reads a single plot point, displays the current conditions on the screen, sends eventual signal to the \*.TFD file and sends signal to SPECTRA to proceed (this signal is simply a removal of the \*.SIM file with the current plot point). The full plot file, \*.PLT, is produced as usual, so that the results can be viewed in the usual post-processing mode, after the run is finished.

0: Interactive simulation inactive.

1: Interactive simulation active, fast mode. Actions take effect with a delay of up to the time step between plots. Run is faster because SPECTRA proceeds to the next plot point without waiting for eventual signals from VISOR.

2: Interactive simulation active, slow mode. Actions take effect immediately. Run may be slower because SPECTRA waits for eventual signals from the simulator before proceeding to the next plot point.

*Acceptable range:* 0, 1, or 2. *Default value:* 0.

### 2.16.10 Record: 950000, Scrambling Input Files

If an input file needs to be distributed to a non-licensed user (for example as a model that has to serve as demo, a simulator, etc.) the input file may be scrambled to prevent the non-licensed user from making changes in the model.

W-1 (I): ISCRMB Scrambling indicator.
=0: scrambling is not needed.
=1: scrambling is needed. The scrambled file \*.SCR is generated. The file \*.SCR should be renamed into \*.SPE and distributed to a non-licensed user.
Acceptable range: 0 or 1 Default value: 0

#### 2.16.11 Example of Transient Solution and Output Frequency Data

The input shown below defines the SOLVER data, including the start time for the run and time step data for three domains. The start time of the analysis is -10.0 s. The first time domain is active from the start time to 100 seconds. The second domain is active for times between 100 s and 500 s. The third domain is active for times between 500 s and 10,000 s. The transient calculations are terminated at 10,000 seconds. The time steps, the print- and the plot-points, are more frequent at the beginning of the transient. The maximum time step size is used for plot edits (zeroes are entered). The advancement message frequency and the iteration parameters are not entered, thus default values are used.

*	Definition of time steps				
*					
*					
*	Start Time				
930000 *	-10.0				
*	Maximum dt	Minimum dt	Print dt	Plot dt	End time
*	(s)	(s)	(s)	(s)	(s)
900001	1.0	0.001	10.0	0.0	100.0
900002	2.0	0.001	50.0	0.0	500.0
900003	10.0	0.001	500.0	0.0	10000.0

## 2.17 Exporting Input Data to Other Programs

SPECTRA allows to export data to other system codes. The export option creates a file \*.EXP, which contains geometry and initial conditions for the following elements of an input model:

- CV Control Volumes
- JN Junctions
- FL Fluid Property Data
- SC 1-D Solid Heat Conductors
- MP Material Property Data
- TF Tabular Functions
- CF Control Functions

The data can be exported to one of the following formats:

- Generic format. With this format all data such as volumes, flow areas, loss coefficients, etc, are exported in a general format, as columns of numbers with headers. This format may provide a significant help in producing an input decks for computer codes which have similar structure as SPECTRA (.i.e. free nodalization, modeling based on interconnected fluid volumes convecting heat to solid structures), for example: MELCOR, RELAP, WAVCO, CONTAIN, etc.
- MELCOR format. This option produces MELCOR input. Note that the input is restricted to:
  - o CV Control Volumes
  - FL Flow Paths
  - NCG Non-Condensable Gases
  - HS Heat Structures
  - o MP Material Properties
  - TF Tabular Functions
  - CF Control Functions

Other elements of the model, such as time steps, modeling assumptions (for example hydrogen models, aerosol models, fission product models, etc.), boundary conditions (for example sources of hydrogen, aerosol, fission products, etc.), must be prepared manually.

- RELAP format. This option produces RELAP5 input. Note that the input is restricted to:
  - Control Volumes (set of single volumes are created, no pipes, branches, etc.)
  - Junctions (set of single junctions are created)
  - Heat Structures
  - Material Properties
  - General Tables
  - Control Variables

Other elements of the model, such as time steps, modeling assumptions, boundary conditions, must be prepared manually.

#### 2.17.1 Record: 960000, Request for Exporting Data to Other Programs

W-1 (I) :	IEXPSL	Request for exporting data.IEXPSL=0: No data exportingIEXPSL=1: Data is exported to generic formatIEXPSL=2: Data is exported to MELCOR input formatIEXPSL=3: Data is exported to RELAP input formatAcceptable range: $0 \le IEXPSL \le 3$ Default value: $0$
W-2 (I) :	IEXTSL	Time of exporting data. The data can be exported at the start or at the end of the run. This affects the transient parameters, such as pressures, temperatures, velocities, etc., that are written to the exported file IEXTSL=0: Data is exported at the start of the run. The transient parameters are those defined in the SPECTRA input file or in the SPECTRA ICF file used to start the run.
		IEXTSL=1: Data is exported at the end of the run. The transient parameters are those calculated at the end of the SPECTRA run, i.e. the same as those present in the ICF file produced by the run. Acceptable range: $0 \le IEXTSL \le 1$ Default value: 0

<u>If IEXTRT = 2 (exporting to MELCOR)</u>

W-3 (I): IRADSL Option for exporting the net enclosure thermal radiation model into MELCOR format. Used only is IEXPSL = 2. In general there is no good way to convert a net enclosure model into MELCOR. Simple enclosures, consisting of two radiating surfaces only, can be modeled in MELCOR using the structure-to-structure radiation input record HSRDCCCCCO. This is not done automatically and must be done manually. More complex enclosures, with multiple participating surfaces, cannot be modeled in MELCOR. To a certain extend this can be remedied by applying a surface-to-gas radiation model. Note that in such case radiation-absorbing gases, for example H<sub>2</sub>O, CO<sub>2</sub>. There are two options for treating the net enclosures when exporting data to MELCOR:

- IRADSL=0: Thermal radiation on the surfaces involved in the net enclosures is ignored and the radiation data is not exported. Simple two-surface enclosures can be defined manually in the records HSRDCCCCC0.
- IRADSL=1: Surfaces involved in the net enclosure thermal radiation model are assigned a simple surface-to-gas radiation model: GRAY GAS, with the beam length of 1000.0 m to maximize the radiation heat transfer.

Acceptable range: $0 \leq IRADSL \leq 1$ Default value:0

W-4 (R): TFRCSL MELCOR input parameter TFRAC, determining time fraction of burn before propagation is allowed. SPECTRA calculates flame propagation based on flame speed (code-calculated) and propagation distance (input

parameter PRPDH2). In MELCOR propagation is a user-defined parameter, with default value of 0.0 (instantaneous propagation through Control Volumes). A positive value will slow down the propagation. *Acceptable range:*  $0.0 \le \text{TFRCSL} \le 1.0$ *Default value:* 0.7 (ratio between the burn propagation PRPDH2, and burn dimension DIMH2)

W-5 (R): IFRMSL MELCOR input parameter IFRMAT, format flag for temperature node location data.
IFRMSL=1: Node location data is exported according to IFRMAT=1; location of a temperature node and the number of this node.
IFRMSL=2: Node location data is exported according to IFRMAT=2; length and the number of consecutive mesh intervals with this length. *Acceptable range:* TFRCSL = 1 or 2 *Default value:* 2

#### If IEXTRT = 3 (exporting to RELAP)

- W-3 (I): IRADSL Option for exporting the vertical orientation of Control Volumes. Used only is IEXPSL = 3. In general there is no good way to convert elevations of CV and JN into RELAP. There are two options for automatic definition of vertical orientation of CV when exporting data to RELAP:
  - IRADSL=-1: All CV-s will be defined as horizontal (inclination angle will be set to 0.0, elevation change will be set to zero). The input deck will run but the vertical angles will not be correct and will have to be redefined manually.
  - IRADSL=+1: All CV-s will be defined as vertical (inclination angle will be set to +90.0, elevation change will be set to volume height). All vertical-up junctions will be connected to the outlet of the "from" CV to the inlet of the "to" CV. All horizontal JN will be defined as cross-flow JN. All vertical-down junctions will be connected to the inlet of the "from" CV to the outlet of the "to" CV. Input deck will be OK provided that in SPECTRA model the junctions are:
    - vertical JN: connected at the top or bottom of the Control Volumes it connects.
    - horizontal JN: connected at the middle of the Control Volumes it connects.

If these conditions are not fulfilled, the inclination angles will not be correct and will have to be redefined manually. It should be noted that in RELAP JN are connected to inlet, outlet, or middle (cross-flow) of a CV. Therefore unless JN elevation is at the bottom, top, or middle of CV, a one-to-one conversion to RELAP is not possible. In such cases re-nodalization of the model will be necessary.

Acceptable range:  $-1 \le IRADSL \le +1$ Default value: +1

## 2.18 Requests for External Data Files

The External Data File (EDF) Package serves as a utility in SPECTRA to communicate with external data files. SPECTRA has two external data files:

- "Write-EDF", and
- "Read-EDF"

The EDF written by SPECTRA may be used by another program as a source of data (e.g. as boundary conditions, etc.). The EDF read by SPECTRA may be used to supply data (e.g. boundary conditions, etc.) to SPECTRA. Such data could be generated by another program, spreadsheet, hand-calculations, etc.

Using the "Write-EDF" a set of variables from the SPECTRA data base may be sent to the EDF. Any variable in from the SPECTRA data base may be used. The full list of SPECTRA variables is provided in Table 2-23 through Table 2-32.

Using the "Read-EDF" a set of Tabular Function values may be read by SPECTRA. The reason why only Tabular Functions are read is the following. Other variables, such as for example Control Volume temperature or pressure, are being calculated by the SOLVER Package, and they cannot be redefined outside the SOLVER. If a user wishes to use a Control Volume with fixed, or time-specified pressure, then he has to use the time-specified CV (see section 2.1.14), where CV temperature, pressure, etc. are defined using either Tabular or Control Function. Therefore reading TF values is sufficient to provide every kind of boundary condition that the SPECTRA user may wish to define in his calculations.

There are two main options of using EDF:

- Normal run with EDF
- Synchronized run with EDF

If the first option is used, then the Write-EDF is created during the calculations (it is very similar to the plot file; the main difference is lack of variable identifiers (headers) in the EDF file (compare section 3.3 and 2.18.6). The Read-EDF must be present when SPECTRA is started, and the values from the Read-EDF are read during the run and assigned to the appropriate tabular functions. At the end of calculations both files contain full information from the run.

The second option is provided to allows <u>interactively</u> read/write EDF. With this option on, SPECTRA may run parallel with another program (or another model run by the SPECTRA code itself) and exchange information with selected data exchange time step.

In case of synchronized run each EDF contains data for a single (current) time step only. The following procedure is used. Once SPECTRA comes to the point when EDF must be written, it first checks if the EDF that has been written at the previous step still exists. If it does, then it waits until it disappears. Thus, the non-existence of the file is treated as a sign from the other program that the information has been successfully received and the other program is ready to receive new information.

Similarly, once SPECTRA comes to the point when EDF must be read, it first checks if it exists. If so, it reads the information and then deletes the file. Thus it gives the signal to the other code that the information has been successfully received and SPECTRA is ready to receive new information.

During both normal run and synchronized run the EDF information is written/read using the data exchange step not smaller than the maximum time step DTMAX, specified in the records 900XXX (see section 2.16.2). Therefore the maximum time step must selected as not larger than the data exchange step for all time step domains.

## 2.18.1 Record: 9800000, EDF Main Data

W-1 (I) :	IEDFED	EDF option: = 1: Normal run without EDF (EDF Package inactive). = 2: Normal run with Write EDF used. = 3: Normal run with Read EDF used. = 4: Normal run with both Read and Write EDF used. = 5: Synchronized run with both Read and Write EDF, explicit coupling. = 6: Synchronized run with both Read and Write EDF, implicit coupling. Note: In the case of implicit coupling, data is exchanged every time step. Sub-cycling (time step reduction) is not possible. The minimum time step must be set as equal to the maximum time step: DTMIN(i) = DDTMAX(i). The data exchange time step (Word 5 below) must be equal to the maximum time step: DTEXED = DTMAX(i). Acceptable range: 1, 2, 3, 4, 5, 6. Default value: 1.
W-2 (I) :	IROPED	Error handling for the Read-EDF: = 1: Write a diagnostic and stop if errors are encountered in the Read-EDF (for example loss of time synchronism, improper data fields, insufficient data, etc.). = 2: Ignore the errors and continue calculations. However do not assign the erroneously read values to the Tabular Functions. <i>Acceptable range:</i> 1 and 2. <i>Default value:</i> 1.
W-3 (I) :	NNFMED	Data format indicator for the Write-EDF. The number of data fields in a single line of the Write-EDF will be restricted to NNFMED. The data is written to the EDF using the format: N(1X,ES16.9), where N is equal to NNFMED. A negative number indicates CSV format, with maximum number of data columns equal to -NNFMED. The total number of variables in the Write EDF (NVAWED) cannot exceed -NNFMED A value of 1 or -1 will result in a free format, without leading spaces. If NNFMED = 1, numbers will be separated by a single space, if NNFMED = -1, numbers will be separated by a single comma. Acceptable range: $1 \le NNFTED \le 1000$ if positive NNFTED $\ge -20$ if negative Default value: 5.

W-4 (R): ERRSED Maximum acceptable time mismatch in synchronized runs, explicit coupling. This is a fraction of the data exchange time step. If the time mismatch is smaller than the product: ERRSED × DTEXED, then the data is exchanged without any time step modification. If the mismatch is larger, the time step is reduced (Figure 2-93). A small increase of time step (10%) is also permitted, in order to avoid severe  $\Delta t$  reduction in the subsequent step. Decreasing ERRSED will result in more accurate timing of data exchange, at the expense of time step reductions. The number of time step reductions and the mismatch in data exchange timings are printed in the output and the message file, if requested by IMESED, below.

Acceptable range:  $0.0 < \text{ERRSED} \le 1.0$ Default value: 0.1



Figure 2-93 Effect of ERRSED (synchronized run, explicit coupling.

W-5 (R): DTEXED Time step for data exchange, (s).

Acceptable range:  $DTMAX(i) \le DTEXED \le 1.0E10$ , or 0.0 Note: In the case of implicit coupling (IEDFED=6), data is exchanged every time step. Sub-cycling (time step reduction) is not possible. The minimum time step must be set as equal to the maximum time step: DTMIN(i) = DDTMAX(i). The data exchange time step (Word 5 below) must be equal to the maximum time step: DTEXED = DTMAX(i). Default value: DTMAX(i) Note: if zero or no value is entered, the data exchange time step will be equal to DTMAX(i), so in general, it will be different in each time step domain. When a positive value is entered, a single value will be used throughout the run and it must be not smaller than the maximum value of DTMAX(i), i=1.N.

W-6 (I) :	IMESED	Option to write message about EDF transfers to the message file. = 0: do not write messages about EDF data transfers = 1: write a message whenever data is transferred through EDF = 2: write a message whenever time step is adjusted due to EDF = 3: write a message in both cases (EDF transfer or $\Delta t$ adjustment) = 4: as above, additionally write the values of transferred data <i>Acceptable range:</i> IMESED = 0, 1, 2, 3, 4 <i>Default value:</i> 0
W-7 (I) :	INITED	Option to transfer data during initialization. = 1: Single data exchange, at the end of the iterations, is performed during initialization. This option may be required when a synchronized run is performed with another program. = 2: Two data exchanges are performed, first at the start of iterations and second at the end of iterations. Some data e.g. initial pressures, temperatures, etc. are available at the start of iteration and if these data are transferred it helps to pass them on to the other program already at the start of iterations. Other data, e.g. heat transfer coefficients, heat fluxes, etc., are available at the end of iterations, therefore the second data transfer is mandatory in order to achieve a complete data transfer. <i>Acceptable range:</i> IMESED = 1, 2 <i>Default value:</i> 2
W-8 (R) :	EMICED	Acceptable relative error in implicit coupling. Iterations continue until the relative errors of all exchanged parameters are smaller than EMICED. The relative error in iteration <i>i</i> is defined as: $ V_i - V_{i-1}  /  V_i $ if $V_i \neq 0$ , $ V_i - V_{i-1}     V_{i-1} $ if $V_{i-1} \neq 0$ , 0.0 otherwise. Here $V_i$ is the value in iteration <i>i</i> , $V_{i-1}$ is the value in iteration <i>i</i> -1. EMICED<10 <sup>-50</sup> means that the convergence is not checked within this run. In such case it must be checked by the other run. Acceptable range: $0.0 \leq \text{EMICED} \leq 10^{-1}$ Default value: $10^{-3}$ (a small number, $<10^{-50}$ , disables convergence check in the current run)
W-9 (I) :	MIICED	Maximum number of iterations. To avoid excessive number of iterations, a limit may be set here. If zero is entered, no limit is imposed. Acceptable range: $0 \le MIICED \le 100$ Default value: 50
W-10 (R) :	XIMPED	Implicit solution factor. In the case of implicit solution, the end-of time step value is multiplied by this factor. The applied value is set to: $V_{act} = V \times XIMPED + V_0 \times (1.0 - XIMPED)$ . If a negative value is entered, the general Solver procedure is used to control the convergence of the parameter being sent to the Write-EDF. EMICED is still used, but somewhat differently and the iteration is a bit more complex. While with XIMPED = 1 two values are kept (the last and the previous iteration), Solver (XIMPED < 0) keeps four values: the assumed and the calculated values from the last two iterations. Based on these values, it determines a new assumed value for the next iteration.

The convergence criterion, EMICED, is applied on the calculated values, while EMICED×0.1 is applied on the assumed values. Acceptable range: XIMPED  $\leq 1.0$ Default value: -1.0 (a small number,  $<10^{-50}$ , sets the value to 0.0).

#### 2.18.2 Record: E0500X, File Name of the Write-EDF

X is the EDF process number, XX = 0, 1, 2, ... Maximum number of EDF processes is 10.

W-1 (A): WRFILE User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* \*.EDF, where \* is the name of the input file.

## 2.18.3 Record: D0500X, File Name of the Read-EDF

X is the EDF process number, X = 0, 1, 2, ... Maximum number of EDF processes is 10.

W-1 (A): RDFILE User defined name, length up to 50 characters. The name is read as a 50 character string, starting from the first non-blank character after the record identifier. There must be at least one blank character, separating the name from the record identifier. *Acceptable range:* any string of up to 50 characters. *Default value:* none (must be specified if IEDFED  $\geq$  3).

#### 2.18.4 Records: 981000X, Definition of Variables Present in the Write-EDF

X is the EDF process number, X = 0, 1, 2, ... Maximum number of EDF processes is 10. Several records with the same number may be entered. Each record should contain a number of sets of six numbers, which in a unique way define the variable from SPECTRA data base.

W-1 (I) :	IVW1ED	First pointer for the first variable request.		
	(1)	The value of this po	pinter defines the data base. The values are:	
		IVW1ED = 1:	Control Volume Data Base.	
		IVW1ED = $2$ :	Junction Data Base.	
		IVW1ED = 3:	1-D Solid Conductor Data Base.	
		IVW1ED = 4:	2-D Conductor Data Base.	
		IVW1ED = 5:	Thermal Radiation Data Base.	
		IVW1ED = 6:	Tabular Function Data Base.	
		IVW1ED = 7:	Control Function or Reactor Kinetics Data Base.	
		IVW1ED = 8:	Radioactive Particle Data Base	
		IVW1ED $= 9$ :	SOLVER Data Base.	
		Acceptable range:	$1 \leq IVW1ED \leq 9.$	
		Default value:	none.	

W-2 (I) :	IVW2ED (1)	Second pointer for the first variable request. This pointer defines the component number that holds the data to be plotted. The following values should be used: IVW2ED = CV number, if $IVW1ED = 1$ , IVW2ED = JN number, if $IVW1ED = 2$ , IVW2ED = SC number, if $IVW1ED = 3$ , IVW2ED = TC number, if $IVW1ED = 4$ , IVW2ED = TR number, if $IVW1ED = 5$ , IVW2ED = TF number, if $IVW1ED = 6$ , IVW2ED = CF number or 0 for RK, if $IVW1ED = 7$ , IVW2ED = CV, JN, SC, TC number, or 0, if $IVW1ED = 8$ , IVW2ED = 0, if $IVW1ED = 9$ . Exceptions are the "summed quantities" (giving mass, energy, etc., summed for all Control Volumes). If a summed quantity is requested then this pointer must be entered as zero. Acceptable range: must be a valid reference number. Default value: none.
W-3 (I) :	IVW3ED (1)	Third pointer for the first variable request. This pointer defines the type of variable in the data base. The values of IVW3ED and their interpretation are the same as in case of the Control Function argument pointer IARG3C, which are shown in Table 2-23 through Table 2-32. For example, if IVW1ED = 1 (Control Volume Data Base) then IVW3ED = 14 points to the CV temperatures (see Table 2-23). Acceptable range: $1 \le IVW3ED \le 131$ ; if IVW1ED = 1, $1 \le IVW3ED \le 47$ ; if IVW1ED = 2, $1 \le IVW3ED \le 43$ ; if IVW1ED = 3, $1 \le IVW3ED \le 59$ ; if IVW1ED = 4, $1 \le IVW3ED \le 59$ ; if IVW1ED = 5, $IVW3ED \le 1$ ; if IVW1ED = 6, $1 \le IVW3ED \le 25$ ; if IVW1ED = 7, $1 \le IVW3ED \le 323$ ; if IVW1ED = 8, $1 \le IVW3ED \le 8$ ; if IVW1ED = 9. Default value: none.
W-4 (I) :	IVW4ED (1)	Fourth pointer for the first variable request. For example, if the Control Volume temperature is needed (IARG1C = 1, IARG3C = 14; see Table 2-23) then this pointer specifies whether the temperature of the atmosphere gas (IARG4C =1), atmosphere droplets (=2), pool liquid (=3), or pool bubbles (=4), is used. If the Solid Heat Conductor Temperature is needed (IARG1C = 3, IARG3C = 16; see Table 2-23) then this pointer specifies the node number. The values of IARG4C, their interpretation and acceptable range, are shown in Table 2-23 through Table 2-32. <i>Acceptable range:</i> indicated in Table 2-23 through Table 2-32. <i>Default value:</i> none.

Additional pointers for the Radioactive Particle Transport Package

W-5 (I) :	IVW5ED (1)	Fifth pointer for the first variable request. This pointer is used for some parameters in the Radioactive Particle
		Transport Package - Table 2-28. For example, if the gravitational
		deposition velocity of aerosol particles is needed (IARG1C = 8,
		IARG3C = 53 or 74, see Table 2-28) then this pointer specifies the
		aerosol size section number. (Note that in this case the fourth pointer
		specifies the boundary cell number). The values of IARG5C, their
		interpretation and acceptable range, are shown in Table 2-28.
		Acceptable range: indicated in Table 2-28.
		Default value: none.
W-6 (I) :	IVW6ED	Sixth pointer for the first variable request.
	(1)	This pointer is used for some parameters in the Radioactive Particle
		Transport Package - Table 2-28. For example, if the deposited fractions
		in given $F_a$ -section (adhesion force section) is needed (IARG1C = 8,
		IARG3C = 65 or 86, see Table 2-28) then this pointer specifies $F_a$ -
		section number. (Note that in this case the fifth pointer specifies the
		aerosol size section number and the fourth pointer specifies the boundary
		cell number). The values of IARG6C, their interpretation and acceptable
		range, are shown in Table 2-28.
		Acceptable range: indicated in Table 2-28.
		Default value: none.

The six words described above may be repeated. An arbitrary amount of sets of six words may be entered. Several records with the same number may be used but sets should not be split between records.

## 2.18.5 Records: 982000X, Definition of Variables Present in the Read-EDF

X is the EDF process number, X = 0, 1, 2, ... Maximum number of EDF processes is 10. Several records with the same number may be entered. Each record should contain reference number of the Tabular Functions that need to be read from the Read-EDF.

W-1 (I) :	IVR2ED	Second pointer for the first variable request.
	(1)	IVR2ED = reference number of a Tabular Function,
		Note that for the Read-EDF the first pointer is always equal to 6 (TF),
		the third pointer always equal to 1 (value of TF), and the fourth pointer
		always equal to 0 (un-used)
		Acceptable range: must be a valid reference number of a Tabular
		Function, if non-zero.
		Default value: none.
W-2 (I)	IVR2ED	Second pointer for the second variable request. Meaning as above.
	(2)	an arbitrary amount of data words may be entered. Several records with
		the same number may be used.

#### 2.18.6 Examples of EDF Input and Output

#### • Write EDF

The input shown below defines Write EDF data file which sends for plot parameters to the Write EDF ED-W.

```
* EDF ERROR NNFMED SYNCH DT

9800000 2 1 5 0.0 0.25

E05000 ED-W

9810000 1 1 13 1 0 0 1 2 13 1 0 0 1 1 14 1 0 0 7 900 1 0 0 0
```

The EDF file ED-W is shown below.

```
        4

        0.00000000E+00
        1.00000000E+05
        1.0000000E+05
        3.00000000E+02
        0.00000000E+00

        0.00000000E+00
        1.00000000E+05
        1.0000000E+05
        3.00000000E+02
        -1.00000000E+00

        0.0000000E+01
        1.00000000E+05
        9.992427113E+04
        3.0000000E+02
        -7.50000000E+01

        0.0000000E+01
        1.0000000E+05
        9.99408216E+04
        3.0000000E+02
        -5.0000000E+01

        1.00000000E+01
        1.0000000E+05
        9.994139694E+04
        3.0000000E+02
        -2.50000000E+01

        1.00000000E+00
        1.00000000E+05
        9.994138699E+04
        3.0000000E+02
        -2.20446049E-16

        1.250000000E+00
        1.00000000E+05
        9.994157405E+04
        3.0000000E+02
        2.50000000E-01

        1.50000000E+00
        1.00000000E+05
        9.994157405E+04
        3.0000000E+02
        2.50000000E-01

        1.750000000E+00
        1.00000000E+05
        9.994157405E+04
        3.00000000E+02
        5.00000000E-01

        1.750000000E+00
        1.00000000E+05
        9.994192356E+04
        3.0000000E+02
        7.50000000E+01

        2.00000000E+00
        1.00000000E+05
        9.994192356E+04
        3.00000000E+02
        1.000000000E+02
```

• Write EDF, CSV format

The input shown below defines Write EDF data file which sends for plot parameters to the Write EDF ED-W.CSV, using the csv (comma-separated values) format (readable for excel).

EDF ERROR NNFMED SYNCH DT 9800000 2 1 -5 0.0 0.25 \* negative NNFMED defines CSV format E05000 ED-W-CSV.CSV 9810000 1 1 13 1 0 0 1 2 13 1 0 0 1 1 14 1 0 0 7 900 1 0 0 0

The EDF (CSV) file is shown below.

```
TIME,CV-001-Pres-atms,CV-002-Pres-atms,CV-001-Temp-atms,CF-900-Valu-0000
0.00000000E+00, 1.00000000E+05, 1.00000000E+05, 3.00000000E+02, 0.00000000E+00
2.50000000E+01, 1.00000000E+05, 9.992427113E+04, 3.00000000E+02,-7.50000000E+01
5.00000000E-01, 1.0000000E+05, 9.994008216E+04, 3.00000000E+02,-5.00000000E+01
7.500000000E-01, 1.0000000E+05, 9.994139694E+04, 3.00000000E+02,-2.50000000E+01
1.00000000E+00, 1.0000000E+05, 9.99412899E+04, 3.00000000E+02, 2.220446049E+01
1.250000000E+00, 1.0000000E+05, 9.99412899E+04, 3.00000000E+02, 2.50000000E+01
1.5000000E+00, 1.0000000E+05, 9.99417405E+04, 3.00000000E+02, 5.0000000E+01
1.5000000E+00, 1.0000000E+05, 9.99417405E+04, 3.00000000E+02, 7.50000000E+01
2.0000000E+00, 1.0000000E+05, 9.994192356E+04, 3.00000000E+02, 7.50000000E+01
```

The variables are written using fixed format (with a space for sign). On order to obtain the CSV file without spaces, the value of NNFMED should be set to -1:

	EDF	ERROR	NNFMED	SYN	СН	DT													
9800000	2	1	-1	0.0	0	.25	*	ne	egat	iv	е	NNFMED	0	defir	nes	5 (	CSV	7 f	format
E05000	ED-V	J-CSV.CSV																	
9810000	1 1	13 1 0 0	1 2	2 13	1 0	0	1	1	14	1	0	0	7	900	1	0	0	0	

#### In this case the EDF (CSV) file is shown below.

TIME, CV-001-Pres-atms, CV-002-Pres-atms, CV-001-Temp-atms, CF-900-Valu-0000 .00000000, 100000.0000, 100000.0000, 300.000000, .00000000 .250000000, 100000.0000, 99924.2711, 300.000000, -.750000000 .50000000, 100000.0000, 99940.0822, 300.000000, -.500000000 .750000000, 100000.0000, 99941.3969, 300.000000, -.250000000 1.00000000, 100000.0000, 99941.2890, 300.000000, .222044605E-15 1.25000000, 100000.0000, 99941.4306, 300.000000, .250000000 1.50000000, 100000.0000, 99941.5741, 300.000000, .500000000 1.75000000, 100000.0000, 99941.7476, 300.000000, .750000000 2.0000000, 100000.0000, 99941.9236, 300.000000, .750000000

#### • Synchronic run

The input shown below defines EDF data for a synchronic run, where SPECTRA-calculated data will be sent out in the EDF file called "SPECTRA.DAT", while simultaneously an external data, calculated by other program (PANTHER) will be read from the file "PANTHER.DAT".

The following variables will be written to the SPECTRA.DAT file:

- Atmosphere temperature in CV-150.
- Atmosphere temperature in CV-160.
- Atmosphere pressures in CV-150.
- Atmosphere pressures in CV-160.

The following variables are read from the PANTHER.DAT file:

- Value of TF-151.
- Value of TF-152
- Value of TF-161.
- Value of TF-162.

```
_____
           EDF Input Data
            _____
                   Main data
                   Type(synch.) Read option
                                                                     Format
9800000
                                           1
                                                                      5
E05000 SPECTRA.DAT * Write-EDF name
* Write-EDF data:
* Pointers: (1) (2) (3) (4) * (1) (2) (3) (4)

9810000 1 150 13 1 * CV data base, CV-150, Temperature, Atmosphere

9810000 1 160 13 1 * CV data base, CV-160, Temperature, Atmosphere

        9810000
        1
        100
        13
        1
        CV data base, CV-150, Pressure, Atmosphere

        9810000
        1
        160
        14
        1
        * CV data base, CV-160, Pressure, Atmosphere

        9810000
        1
        160
        14
        1
        * CV data base, CV-160, Pressure, Atmosphere

D05000 PANTHER.DAT
                                                    * Read-EDF name
9820000 151 152 161 162 * Read-EDF data: reference numbers of TF
            _____
```

An example of a Write-EDF file is presented below. It is important to note that the Write-EDF contains always:

• N integer number, defining the total number of variables, equal to NVAWED,

- Time the current time,
- User-specified variables, NVAWED total.

An example of such file is shown below. The current time is in the file equal to 1.0 (s). The file SPECTRA.DAT for this time is:

1.00000E+00 2.93125D+02 2.93125D+02 1.01295D+05 1.01295D+05

The above example shows the EDF for a synchronized run, i.e. for a single time point. In case of a normal run, the file will contain all time dependent look something like:

110.0000E+002.93125D+022.93125D+021.01295D+051.01295D+051.00000E+002.93125D+022.93125D+021.01295D+051.01295D+052.00000E+002.93125D+022.93125D+021.01295D+051.01295D+053.00000E+002.93125D+022.93125D+021.01295D+051.01295D+054.00000E+002.93125D+022.93125D+021.01295D+051.01295D+05

SPECTRA expects the Read-EDF to have the same structure. The first number in the read EDF must determine the number of variables. This number must be equal to NVARED (record 9820000). If it is not, the run will be terminated unless ignoring read error is requested by setting IROPED to 2 (record 9800000). The next number is expected to be time. The time must be the same as the SPECTRA time. If it is not, the run will be terminated unless ignoring read error is requested by setting IROPED to 2 (record 9800000). Next, NVARED data fields are expected, providing data for the NVARED tabular functions, specified in the records 9920000. If the number of data fields is different or if any kind of read error is encountered, the run will be terminated unless ignoring read error is requested by setting IROPED to 2 (record 9800000).

Note that the Read-EDF is read by SPECTRA using the free format, so the number of data fields in a single line of the Read-EDF may be arbitrary. For example the Read-EDF file may look :

4 1.00 1.23 2.34 3.45 4.56

Alternatively in may have a form, for example:

4 1.00 1.23 2.34 3.45 4.56

This file will result in assigning the following values to tabular functions: TF-151 = 1.23 TF-152 = 2.34 TF-161 = 3.45 TF-162 = 4.56

Again, the above example is for a synchronized run, i.e. it gives data for a single time point. In case of a normal run, the Read-EDF file should contain data for all time steps, and should look something like:

4				
0.00	1.23	2.34	3.45	4.56
1.00	1.23	2.34	3.45	4.56
2.00	1.23	2.34	3.45	4.56
3.00	1.23	2.34	3.45	4.56
4.00	1.23	2.34	3.45	4.56
5.00	12.3	23.4	34.5	45.6
6.00	12.3	23.4	34.5	45.6

л

The values in the first column represent the time, t. The values in the next columns define the values of the tabular functions at the time t. In the example presented above, during the first 4 second the tabular functions will be equal to:

 $TF-151 = 1.23 \\ TF-152 = 2.34 \\ TF-161 = 3.45 \\ TF-162 = 4.56 \\ TF-162 = 4.5$ 

During the next second (between t = 4.0 s and t = 5.0 s) the values will increase (linearly) to:

 $TF-151 = 12.3 \\ TF-152 = 23.4 \\ TF-161 = 34.5 \\ TF-162 = 45.6 \\ TF-162 = 45.$ 

These values are kept constant for the next second, that means until t = 6.0 s.

#### • Multiple EDFs

Below an example of multiple EDF processes. The data exchanged are the same as in the example above, but the data concerning CV-150, TF-151, TF-152 are going to/from the first EDF process, while the data concerning CV-160, TF-161, TF-162 are going to/from the second EDF process. In general, one job may exchange data interactively with several (up to 10) other jobs.

```
*
           _____
          EDF Input Data for multiple EDF processes
+
                 Main data
                  Type(synch.) Read option
                                                                 Format
9800000 5
                                          1
                                                                  5
E05000 SPECTRA-1.DAT * Write-EDF name
* Write-EDF data:

      * Pointers: (1) (2) (3) (4) * (1)
      (2) (3) (4)

      9810000
      1
      150
      13
      1
      * CV data base, CV-150, Temperature, Atmosphere

      9810000
      1
      150
      14
      1
      * CV data base, CV-150, Pressure, Atmosphere

E05001 SPECTRA-2.DAT * Write-EDF name
                                             * Write-EDF data:
* Pointers: (1) (2) (3) (4) * (1) (2) (3) (4)

9810001 1 160 13 1 * CV data base, CV-160, Temperature, Atmosphere

9810001 1 160 14 1 * CV data base, CV-160, Pressure, Atmosphere
D05000PANTHER-1.DAT* Read-EDF name9820000151152* Read-EDF data: reference numbers of TF
D05001PANTHER-2.DAT* Read-EDF name9820001161162* Read-EDF data: reference numbers of TF
```

#### 2.19 Requests for Plot Variables

By default all plottable data is dumped into the plot file every time the plot edit is written (every DTPLT seconds). This may result in a very large size of the plot file produced during the run. Not only it creates the danger of filling the whole disk space, but also it increases the overall run time, since the I/O operations are relatively slow. The user can reduce the size of the plot file by two methods: reducing the plot frequency (thus making intervals between plot points - DTPLT - larger), or selecting only certain amount of variables he is interested in. The selection of plot variables is done using the records described in this section.

#### 2.19.1 Record: 9900000, Full Plot File Option

W-1 (I) :	IPLOT	Full plot file indic missing, then the f present in the plot 992000, 993000 b suppressed (IPLOT record). If IPLOT is different records 991000, 9 requests are present <i>Acceptable range:</i> <i>Default value:</i>	ator. If the value is equal to zero, or this record is full plot file is written (all plottable variables will be file). However, if the plot requests (records 991000, elow) are entered, then the full plot file option is T is set to 1 independently of the value entered in this ent than zero, then only the requested variables (via 92000, 993000) are written to the plot file. If no t then the plot file is empty. all integers. 0 (by default all plottable variables are dumped into the plot file if no requests are present, and only the requested variables if the requests are present)
			requested variables if the requests are present).

#### 2.19.2 Record: 9910000, Requests for Specific Component

These records may be used to request <u>all plottable data for a specific component</u>, for example all plottable data may be selected for one or several Control Volumes, one or several Solid Conductors, etc. Multiple records with the same number may be entered.

Note that the "summed quantities" (giving mass, energy, etc., summed for all components) are not obtained using these records. These records request all data related to a specific component (for example, specific Control Volume), while "summed quantities" are related to all components in the problem (for example all Control Volumes).

Each record should contain a number of pairs of data, defining the component for which all plottable variables need to be dumped into the plot file.

W-1 (I):	IPLC1(1)	First pointer for the first component request. The value of this pointer				
		defines the data base. The values are:				
		IPLC1 = 1: Control Volume Data Base.				
		IPLC1 = 2: Junction Data Base.				
IPLC1 = 3: 1-D So		IPLC1 = 3: 1-D Solid Conductor Data Base.				
		IPLC1 = 4: $2$ -D Conductor Data Base.				

		$IPLC1 = 5$ :Thermal Radiation Data Base $IPLC1 = 6$ :Tabular Function Data Base. $IPLC1 = 7$ :Control Function or Reactor I $IPLC1 = 8$ :Radioactive Particle Data Base $Acceptable range: 1 \le IPLC1 \le 7$ . $Default value:$ none.	e. Kinetics Data Base. se
W-2 (I) :	IPLC2(1)	Second pointer for the first component req component number, which holds the data values should be used: IPLC2 = CV number IPLC2 = JN number IPLC2 = SC number IPLC2 = TC number IPLC2 = TC number IPLC2 = TR number IPLC2 = TF number IPLC2 = CF number IPLC2 = CV, JN, SC, TC number, or 0 Acceptable range: must be a valid referent Default value: none.	uest. This pointer defines the to be plotted. The following if IPLC1 = 1, if IPLC1 = 2, if IPLC1 = 3, if IPLC1 = 4, if IPLC1 = 5, if IPLC1 = 6, if IPLC1 = 7, if IPLC1 = 8, ice number in nonzero.
W-3 (I)	IPLC1(2)	First pointer for the second component req	uest. Meaning as above.
W-4 (I)	IPLC2(2)	Second pointer for the second component	request. Meaning as above.
		an arbitrary number of pairs may be enter same number may be used, but pairs should	red. Several records with the not be split between records.

### 2.19.3 Record: 9920000, Requests for Specific Variable

These records may be used to request a <u>single variable for all components</u>, for example the atmosphere pressure can be selected for all Control Volumes, the left surface temperature for all Solid Conductors, etc.

Note that the "summed quantities" (giving mass, energy, etc., summed for all components) cannot be requested by these records. These records are used to request multiple data (for example, pressures in all Control Volumes), while "summed quantities" give a single data, summed over all components in the problem (for example, atmosphere mass summed over all Control Volumes). Therefore summed quantities should be requested using single plot variable requests (section 2.19.4 - Requests for Specific Component and Variable).

Several records with the same number may be entered. Each record should contain a number of sets of three numbers, defining the variable dumped to the plot file for all components.

W-1 (I) :	IPLV1(1)	First pointer for the first variable request. The value of this pointer
		defines the data base. The values are:
		IPLV1 = 1: Control Volume Data Base.
		IPLV1 = 2: Junction Data Base.
		IPLV1 = 3: 1-D Solid Conductor Data Base.
		IPLV1 = 4: $2$ -D Conductor Data Base.

- $$\begin{split} \text{IPLV1} &= 5: \quad \text{Thermal Radiation Data Base.} \\ \text{IPLV1} &= 6: \quad \text{Tabular Function Data Base.} \\ \text{IPLV1} &= 7: \quad \text{Control Function or Reactor Kinetics Data Base.} \\ \text{IPLC1} &= 8: \quad \text{Radioactive Particle Data Base} \\ \text{Acceptable range:} \quad 1 \leq \text{IPLV1} \leq 7. \\ \text{Default value:} \qquad \text{none.} \end{split}$$
- W-2 (I): IPLV2(1) Second pointer for the first variable request. This pointer defines the type of variable in the data base. The values of IPLV2 and their interpretation are the same as in case of the Control Function argument pointer IARG3C, which are shown in tables Table 2-23 through Table 2-32. For example, if IPLV1 = 1 (Control Volume Data Base) then IPLV2 = 14 points to the CV temperatures (see Table 2-23).

Acceptable range:

$1 \leq IPLV3 \leq 131$	if $IPLV1 = 1$ ,
$1 \leq IPLV3 \leq 47$	if $IPLV1 = 2$ ,
$1 \leq IPLV3 \leq 43$	if $IPLV1 = 3$ ,
$1 \leq IPLV3 \leq 59$	if $IPLV1 = 4$ ,
$1 \leq IPLV3 \leq 8$	if $IPLV1 = 5$ ,
IPLV3 = 1	if $IPLV1 = 6$ ,
$1 \leq IPLV3 \leq 25$	if $IPLV1 = 7$ ,
$1 \leq IPLV2 \leq 323$	if $IPLV1 = 8$ ,
$1 \leq IPLV3 \leq 8$	if $IPLV1 = 9$ .
Default value:	none.

- W-3 (I): IPLV3(1)Third pointer for first variable request. This is an additional pointer, needed sometimes to specify for which material the data is needed. The values of IPLV3 and their interpretation are the same as in case of the Control Function argument pointer IARG4C, which are shown in Table 2-23 through Table 2-32. For example, if the Control Volume temperature is needed (IPLV1 = 1, IPLV2 = 14; see Table 2-23) then this pointer specifies whether the temperature of the atmosphere gas (IPLV3 = 1), atmosphere droplets (IPLV3 = 2), pool liquid (IPLV3 = 3), or pool bubbles (IPLV3 = 4), is used. The values of IPLV3, their interpretation and acceptable ranges, are shown in tables Table 2-23 through Table 2-32 (as IARG4C). Acceptable range: indicated in Table 2-23 through Table 2-32. Default value: none.
- W-4 (I) IPLV1(2) First pointer for the second component request. Meaning as above.
- W-5 (I) IPLV2(2) Second pointer for the second component request. Meaning as above.
- W-6 (I) IPLV3(2) Third pointer for the second component request. Meaning as above.
- ... an arbitrary amount of sets of three words may be entered. Several records with the same number may be used but sets should not be split between records.

### 2.19.4 Record: 9930000, Individual Requests (Specific Component and Variable)

These records may be used to request single plot variables. Those requests are also called "individual requests". For example the atmosphere pressure can be selected for Control Volume No. 015, the left surface temperature for the Solid Conductor No. 125, etc. Several records with the same number may be entered. Each record should contain a number of sets of four numbers, defining the component number and the variable.

W-1 (I) :	IPLCV1(1)	First pointer for the first individual request. defines the data base. The values are: IPLCV1 = 1: Control Volume Data Base. IPLCV1 = 2: Junction Data Base. IPLCV1 = 3: 1-D Solid Conductor Data Base IPLCV1 = 4: 2-D Conductor Data Base. IPLCV1 = 5: Thermal Radiation Data Base. IPLCV1 = 6: Tabular Function Data Base. IPLCV1 = 7: Control Function Data Base. IPLCV1 = 8: Radioactive Particle Data Base IPLCV1 = 9: SOLVER Data Base. Acceptable range: $1 \le IPLCV1 \le 9$ .	The value of this pointer
		Default value: none.	
W-2 (I) :	IPLCV2(2)	Second pointer for first individual request. component number that holds the data to ivalues should be used: IPLCV2 = CV number, IPLCV2 = JN number, IPLCV2 = SC number, IPLCV2 = TC number,	This pointer defines the be plotted. The following if IPLCV1 = 1, if IPLCV1 = 2, if IPLCV1 = 3, if IPLCV1 = 4,

IPLCV2 = TR number, if IPLCV1 = 5. IPLCV2 = TF number, if IPLCV1 = 6, IPLCV2 = CF number, or 0 for RK, if IPLCV1 = 7, IPLCV2 = CV, JN, SC, TC number, or 0, if IPLCV1 = 8. IPLCV2 = 0.if IPLCV1 = 9. Exceptions are the "summed quantities" (giving mass, energy, etc., summed for all Control Volumes). If a summed quantity is requested then this pointer must be entered as zero.

Acceptable range: must be a valid reference number, if nonzero. Default value: none.

W-3 (I): IPLCV3(1) Third pointer for the first individual request. This pointer defines the type of variable in the data base. The values of IPLCV3 and their interpretation are the same as in case of the Control Function argument pointer IARG3C, which are shown in Table 2-23 through Table 2-32. For example, if IPLCV1 = 1 (Control Volume Data Base) then IPLCV3 = 14 points to the CV temperatures (see Table 2-23). Acceptable range:  $1 \leq IPLCV3 \leq 131$  if IPLCV1 = 1,  $1 \leq IPLCV3 \leq 47$  if IPLCV1 = 2,  $1 \leq IPLCV3 \leq 43$  if IPLCV1 = 3,  $1 \leq IPLCV3 \leq 59$  if IPLCV1 = 4,

$$\begin{split} 1 &\leq \text{IPLCV3} \leq 8 \quad \text{if IPLCV1} = 5, \\ \text{IPLCV3} = 1 \quad \text{if IPLCV1} = 6, \\ 1 &\leq \text{IPLCV3} \leq 25 \quad \text{if IPLCV1} = 7, \\ 1 &\leq \text{IPLCV2} \leq 323 \quad \text{if IPLCV1} = 8, \\ 1 &\leq \text{IPLCV3} \leq 8 \quad \text{if IPLCV1} = 9. \\ Default value: \qquad \text{none.} \end{split}$$

- W-4 (I) : IPLCV4(1) Fourth pointer for the first individual request. This is an additional pointer, needed sometimes to specify for which material the data is needed. The values of IPLCV4 and their interpretation are the same as in case of the Control Function argument pointer IARG4C, which are shown in Table 2-23 through Table 2-32. For example, if the Control Volume temperature is needed (IPLCV1 = 1, IPLCV3 = 14; see Table 2-23) then this pointer specifies whether the temperature of the atmosphere gas (IPLCV4 = 1), atmosphere droplets (IPLCV4 = 2), pool liquid (IPLCV4 = 3), or pool bubbles (IPLCV4 = 4), is used. The values of IPLCV4, their interpretation and acceptable ranges, are shown in Table 2-23 through Table 2-32 (as IARG4C). *Acceptable range:* indicated in Table 2-23 through Table 2-32. *Default value:* none.
- W-5 (I) IPLCV1(2) First pointer for the second individual request. Meaning as above.
- W-6 (I) IPLCV2(2) Second pointer for the second individual request. Meaning as above.
- W-7 (I) IPLCV3(2) Third pointer for the second individual request. Meaning as above.
- W-8 (I) IPLCV4(2) Fourth pointer for the second individual request. Meaning as above.
- ... an arbitrary amount of sets of four words may be entered. Several records with the same number may be used but sets should not be split between records.

#### 2.19.5 Example of Plot Requests Data

The input shown below requests for the following variables to be written to the plot file:

- All plottable variables for the Control Volume No. 003.
- Atmosphere pressures, for all Control Volumes.
- Atmosphere temperatures, for all Control Volumes.
- Heat transfer coefficient, for wall-atmosphere heat transfer on the left surface, for all Solid Conductors.
- Pool and bubble temperatures for the Control Volume No. 005.

```
_____
*
         1.) Component requests
         ------
               Request for all plottable data for CV-003.
* Pointers: (1) (2) * (1) (2)
9910000 1 3 * CV data base, CV No. 003
         2.) Variable requests
                ------
                Request for atmosphere pressures and temperatures
                for all Control Volumes, and heat transfer coefficient
                from the left surface to the atmosphere for all Solid Conductors.
* Pointers: (1) (2) (3) * (1) (2) (3)

9920000 1 13 1 * CV data base, Pressure, Atmosphere

9920000 1 14 1 * CV data base, Temperature, Atmosphere

9920000 3 4 -1 * SC data base, H.T.C., Left surface, atmosphere
        3.) Individual requests
*
               Request for temperature of liquid pool and pool bubbles
               in Control Volume No. 005.
* Pointers: (1) (2) (2) (3) * (1) (2) (3) (4)
9930000 1 005 14 3 * CV data base, CV No. 005, Temperature, Pool
9930000 1 005 14 4 * CV data base, CV No. 005, Temperature, Bubbles
```

### 2.20 Restarting

The concept of restarting a terminated job is very simple and user convenient in the SPECTRA code. A restart file is written with specific frequency (by default 10 restart points per single time step domain - see section 2.16.2). Additionally a restart point is written every time a job is finished, either due to normal end, or terminated by the stop file, or terminated due to failure. Calculations may be resumed from any of these points. The restart point is not written if the job has crashed, for example when it's terminated by CTRL-C, in case of abnormal shutdown of the computer, for instance caused by operating system failure, power failure etc. This is one of the reasons why the user should avoid stopping a run with CTRL-C, and use the stop file instead (see section 3.8).

Restarting a job is interactive, and no input preparation is necessary. To restart a terminated job, one has to simply run the code in the directory where the results of the previous calculations exist, and, when prompted by the program, answer that restarting the previous run is indeed what he wishes to do. The program then reads the restart file, and interactively asks the user what changes he wants to make in the time step data (minimum, maximum time step, end time for the restarted run, see section 2.20.1 below). Next, the program lists sequentially the time points when restarts are available, and in each case asks if the user wants to restart from a given point (see section 3.4). Calculations are resumed at the requested restart point.

An input file (\*.SPE) may be used on restart. If an input file is not present, then all data is read from the restart file (\*.RST) and interactively (section 2.20.1). If an input file (\*.SPE) is present, the Solver data (see section 2.16) and the Tabular Function data (see section 2.7) are read from the input file. The Solver data read from the input file replaces the Solver data read from the restart file. Thus all input parameters described in section 2.16 may be redefined on restart, using the SPECTRA input file (\*.SPE). The TF data read from the input file replaces the TF data read from the restart file. New data points may be added to a Tabular Function or the existing data points may be replaced. However, no new TF can be defined on restart - only the data points for the existing Tabular Functions may be modified on restart using the SPECTRA input file (\*.SPE). Currently only the TF data and the Solver data may be re-defined in the SPECTRA input file upon restart.

The output file and the diagnostics file, \*.OUT, \*.DIA, are appended when a job is restarted, so they contain all the information for the original run, followed by the information from the restarted job. The plot file, \*.PLT, is appended from the restart point, so that the time argument in the plot file is increasing (eventual overlapping point are removed). If any of the files: \*.OUT, \*.DIA, \*.PLT is not present, then the information prior to the restart will not be available in this file. The \*.OUT and \*.DIA files will start at the time of restart. The data in the \*.PLT file will also start at the time of the restart, after the number of plot points and the headers (variable names) are written to it.

An example of using the restart option is shown in chapter 3, section 3.4. Interactive input entries for restart are described below, in section 2.20.1. Input entries read from an input file (\*.SPE) on restart are described in section 2.16 and section 2.7.

### 2.20.1 Interactive Input on Restart

The following five values may be changed interactively on restart. The first three values may always be changed. The last two values may be changed only if the current status is "yes". The first three values are valid for the "current" time step domain, that means the time step domain in which the restart had been written.

W-1 (R) :	DTMAX	Maximum time step, (s).	
		Acceptable range:	$DTMIN_R \leq DTMAX \leq 10 \cdot DTMAX_R$ (values with subscript "R" mean the old values, read from the restart file)
		Default value:	$DTMAX_R$ (old value, read from the restart file).
W-2 (R) :	DTMIN	Minimum time step Acceptable range: Default value:	p, (s). $10^{-10} \le \text{DTMIN} \le \text{DTMIN}_{\text{R}}$ . $\text{DTMIN}_{\text{R}}$ (old value, read from the restart file).
W-3 (R) :	DTPRT	Printout (main edit) Acceptable range: Default value:	) frequency, (s). DTMAX $\leq$ DTPRT $\leq$ 10 <sup>10</sup> . ( TENDI(i) - TSTART ) / 10 , if i=1, ( TENDI(i) - TENDI(i-1) ) / 10 , if i>1, where i is the time step domain number.
W-4 (R) :	DTPLT	Plot frequency, (s). Acceptable range: Default value:	$\begin{array}{ll} DTMAX \leq DTPLT \leq 10^{10}. \\ (\mbox{ TENDI(i)} - \mbox{TSTART}) / 300 , & \mbox{if } i=1, \\ (\mbox{ TENDI(i)} - \mbox{TENDI(i-1)}) / 300 , & \mbox{if } i>1, \\ where i \mbox{ is the time step domain number.} \end{array}$
W-5 (R) :	TENDI	End time for this de <i>Acceptable range:</i> <i>Default value:</i>	$\begin{array}{l} \text{Domain, (s).} \\ \text{TIME (current time)} \leq \text{TENDI} < \text{TENDI}_{R}^{\text{next}} \text{ (next time step domain)} - 1.0 \text{ . If the time step domain at the restart is the last one, then there is no upper limit for the end time.} \\ \text{TENDI}_{R} \text{ (old value, read from the restart file).} \end{array}$
W-6 (I) :	IEXDIA	If extended diagnostics had been previously requested then it may be switched off on the restart. The extended diagnostics can be switched on during the run, using the "SPECTRA Stop File" (see sections 2.16.4, 3.8). <i>Acceptable range:</i> "Y", "y", "N", "n". <i>Default value:</i> "N".	
W-7 (I) :	XDEBUG	If the debug printers witched off on the the run, using the " <i>Acceptable range: Default value:</i>	out had been previously requested then it may be restart. The debug printout can be switched on during SPECTRA Stop File" (see sections 2.16.4, 3.8). "Y", "y", "N", "n". "N".

## 2.21 Maximum Problem Size – Summary

The problems that are to be analyzed with the present SPECTRA version must be restricted according to the following limits.

٠	Thermal-hydraulics				
	Control volumes (CV):	550 (999 in LINUX version)			
	Junctions (JN):	600 (999 in	LINUX version)	50 in single CV	
	1-D solid heat conductors (SC):	500 (999)	Cells/SC:	100	
	2-D solid heat conductors (TC):	$20 (\text{or } 2)^{(*)}$	Cells/TC:	$51 \times 51 = 2601$	
			Boundary Cells / TC:	$4 \times 50 = 200$	
	Radiating systems (TR):	9	Surfaces / system:	90	
	Solid materials:	100	Data points / material:	100	
	Number of gases	20	Data points / gas:	100	
	Alternative fluids (liquid metals):	1	Data points / fluid:	1000	
			heat transfer correlations	::100	
•	Material Oxidation (OX)				
	Oxidation models:	10 + 5 built	-in models		
•	Reactor Kinetics (RK)				
	Delayed neutron precursor groups:	10	Reactivity functions:	50	
	Reactivity feedback data points:	50	2		
	Weighting factors data points:	200	Core isotopes (IT):	200	
	Number of nodes in nodal point kin.	50	<b>A</b>		
•	Radioactive Isotope Transport (RT)				
	Aerosol (dust) size sections:	20			
	Resuspension models:	20	Adhesion force sections:	99	
	Inertial impaction surfaces per JN:	10			
	Isotope chains:	24	Isotopes/chain:	11	
	Fission product release classes:	20	Isotopes/class:	100	
	Fission product vapor classes:	20	Isotopes/class:	100	
	Sorption models/class:	9			
•	General Functions				
	Tabular functions (TF):	999	Data pairs / TF:	20,000	
	Control functions (CF):	999	Arguments / CF:	100	
•	External Data Files				
	Max. number of EDF processes:	10	Data channels / EDF:	200	
•	Solver data (SL)				
	Time step domains:	999			

 $^{(*)}$  Note that when the RT Package is used, the maximum number of TC-s is restricted to 2

## 2.22 Applicability Restrictions

The code can be delivered with restrictions, i.e. not all input parameters described in the previous sections can be used. The applicability restrictions are defined by the applicability code AppC. The parameter AppC has the format of four digits: *abcd*, determining restrictions for any of the four main types of nuclear reactors:

$\operatorname{AppC}(1) = a$	-	Light Water Reactors (LWR)
$\operatorname{AppC}(2) = b$	-	High Temperature Reactors (HTR)
$\operatorname{AppC}(3) = c$	-	Liquid Metal Reactors (LMR)
$\operatorname{AppC}(4) = d$	-	Molten Salt Reactors (MSR)

A value of zero means no restriction. A value of one means that the code version has restrictions for a particular reactor type. For example:

AppC = 0000	means no restrictions
AppC = 1000	means restrictions for LWR analyses

The applicability code AppC is printed in the output and diagnostics file, directly below the code version identifier - see section 3.1.1. Details on particular restrictions are described below.

## • *a* = 1: LWR restrictions

In this case the following LWR-specific models are disabled:

- $\circ~$  Fission product release models specific to LWRs: CORSOR-M (MFPRRT = 1) and ARSAP (MFPRRT = 2).
- $\circ$  Oxidation models specific to LWRs: Cathcart model (IOXLSC/IOXRSC/IOXBTC = -1) , Urbanic-Heidreich model (IOXLSC/IOXRSC/IOXBTC = -2), Benjamin model (IOXLSC/IOXRSC/IOXBTC = -4).

## • b = 1: HTR restrictions

In this case the following HTR-specific models are disabled:

- Fission product release model specific to HTRs: HTR-FPR model (MFPRRT = 3).
- $\circ$  Oxidation model specific to HTRs: Roes model (IOXLSC/IOXRSC/IOXBTC = -5).

## • *c* = 1: LMR restrictions

In this case the following LMR-specific model is disabled:

 $\circ$  Alternative fluid availability (IFLDFL > 1).

## • d = 1: MSR restrictions

In this case the following MSR-specific model is disabled:

• Point kinetics model for circulating fuel (IFTORK =2).

# 3 Description of the Output Files

During calculations the SPECTRA program produces the following output files:

- \*.OUT Printed output. The printouts are made with user-requested time intervals.
- \*.PLT Plot file, used for graphs or visualization. The plot points are made with user-requested time intervals.
- \*.DIA Diagnostics file. Contains all warning and error messages.
- \*.RST Restart file. The restart is written only at the end of the calculations.

Additionally several files may optionally be used during calculations:

- \*.ICF "Initial Condition File". It contains values of all time dependent parameters in the model. This file provides an easy way to start computations from earlier calculated conditions. The \*.ICF file, like the \*.RST file, is being written only at the end of the calculations.
- \*.MES Message File contains messages about certain events, for example valve opening/closing, pump startup/shutdown, etc. see input parameter IMESAG, input record 910000.
- \*.TFD Tabular Function Data file may be used to change interactively a value of any Tabular Function that is defined as interactive (see section 2.7.5).
- \*.EDF External data files (section 2.18).
- \*.EXP Export of the model to Generic, MELCOR, or RELAP format (section 2.17).
- \*.SIN \*.SIM Interactive simulator files (section 2.16.9).
- \*.SCR Scrambled input file (section 2.16.10).
- \*.STP The SPECTRA Stop file (see section 3.8) may be used to interactively terminate the calculations.

# 3.1 Description of the Printed Output (\*.OUT)

This section describes the main output file, "\*.OUT", produced by SPECTRA during calculations. The file is arranged in several parts, described below:

- Part 1 Echo of the input file.
- Part 2 Printout of all input data. It contains code interpretation of all input parameters. Keyword to find the header of this part is "=SPE=".
   The printout contains data for each package, keyword to find the header of each package is the package abbreviation within = signs, for example =CV= for Control Volumes. Within each package the data is written for each component, keyword to find the header of each component is the component number preceded by = sign, for example =CV-123 for control volume number 123.

• Part 3 Printout at user defined frequency. The printout contains all transient parameters at given time point. Keyword to find the header of this part is "=**SPE**=". The printout contains data for each package, keyword to find the header of each package is the package abbreviation within = signs, for example =**CV**= for Control Volumes. Within each package the data is written for each component, keyword to find the header of each component is the component number preceded by = sign, for example =**CV-123** for control volume number 123.

An output that is given within the Part 2 (input processing) and the Part 3 (transient) from each Package is discussed separately in the subsequent sections.

#### 3.1.1 SPECTRA Main Program Output

Control Volume outputs may be easily found in the output file by searching for the string: **=SPE=**. This output provides the code version (number and date) and the operating system platform (Windows or Linux). Furthermore, restrictions (if any) of this code version are given, including:

- Validity time limit: MM/YYYY
- Applicability code: AppC. The AppC has the format of four digits: *abcd*, determining restrictions for any of the four main types of nuclear reactors
  - *a* Light Water Reactors (LWR)
  - *b* High Temperature Reactors (HTR)
  - *c* Liquid Metal Reactors (LMR)
  - *d* Molten Salt Reactors (MSR)

A value of zero means no restriction. A value of one means that the code version has restrictions for a particular reactor type. For example:

AppC = 0000 means no restrictions

AppC = 1000 means restrictions for LWR analyses

Details on particular restrictions are described in section 2.22.

Typically the code is delivered without any restrictions (AppC = 0000). A restriction may be placed for a particular country or customer.

Example of printout is shown below:

=SPE= SPECTRA Version 3.61, Jan. 2020, Windows
Sophisticated
Plant
Evaluation
Code for
Thermal-hydraulic
Response
Assessment
Validity: 06/2021, Applicability: AppC = 0000
#### 3.1.2 Control Volume Output

Control Volume outputs may be easily found in the output file by searching for the string: =**CV**=. The first CV printout brings the input data printout. An example of the input printout for a Control Volume is shown below. The printout mainly reflects the data entered in the input file and is quite self-explanatory.

```
=CV= =====CV-001===== Example_problem,_volume_1_
=CV= TYPE
                     : NORMAL CV
      BOTTOM ELEVATION= 0.00000E+00 m
      TOP ELEVATION1.00000E+01 mTOTAL HEIGHT1.00000E+01 mTOTAL VOLUME1.00000E+01 m3HORIZONTAL AREA1.00000E+00 m2
      VERTICAL AREA = 1.00000E+01 m2
      POOL SURF.C.DIM.= ( POOL SURF.AREA ) ** (1/2)
      NO DENSITY STRATIFICATION OF ATMOSPHERE
      NO THERMAL STRATIFICATION OF ATMOSPHERE
      NO THERMAL STRATIFICATION OF POOL
=CV= CV-001,
               SEGMENT DATA
      ELEV-BOTTOM ELEV-TOP
                                HEIGHT
                                                AREA
                                                            VOLUME
SEG.
          (m)
                       (m)
                                    (m)
                                                 (m2)
                                                              (m3)
      0.00000E+00 1.00000E+01 1.00000E+01
                                             1.00000E+00
                                                          1.00000E+01
  1
=CV= CV-001, MASS SOURCES
     Elevation
               Area
                             Diameter
                                         Source Temper. Pressure
                   (m2)
                                                    Table Table
No.
       (m)
                                (m)
                                           Table
 1 0.00000E+00 1.00000E-03 1.00000E-02
                                           TF-001
                                                    TF-002
                                                              TF-003
 2 1.00000E+01 1.00000E-03 1.00000E-02 TF-001 TF-005 TF-003
      MASS SOURCES - OVERALL COMPOSITION
No.
     Water
                Gas
    Water Gas
0.0000E+00 1.0000E+00
 1
 2 1.0000E+00 0.0000E+00
      MASS SOURCES - GAS COMPOSITION
             Не Н2О
No.
      H2
                                         N2
                                                     02
                                                               CO2
 1
    0.0000E+00 0.0000E+00 0.0000E+00 1.0000E+00 0.0000E+00 0.0000E+00
 2 0.0000E+00 0.0000E+00 1.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00
      PLUME MODEL FOR MASS SOURCES
      Atmosphere Pool
No.
 1
      No
                   No
 2
      No
                   No
=CV= CV-001, ENERGY SOURCES
No. Elevation Source
        (m)
                   Table
 1 1.00000E+00 TF-006
      PLUME MODEL FOR ENERGY SOURCES
      Atmosphere Pool
No.
 1
      No
                   No
=CV= CV-001, DROP AND BUBBLY FLOW REGIME MODEL PARAMETERS
                                                          Bubbles
                                 Droplets
                           vertical horizontal
                                                  vertical horizontal
_____ _
                           _____
                                       _____
                                                               _____
Drift flux constant CO
                          0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00
Terminal velocity v-inf 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00
```

0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 Exponent х De-entrainment D 1.00000E+00 0.00000E+00 =CV= CV-001, Surface area for droplet vertical de-entrainment is always equal to the actual pool surface area Surface area for bubble vertical de-entrainment is always equal to the actual pool surface area =CV= CV-001, ANNULAR FLOW MODEL: DEFAULT =CV= CV-001, BUBBLE COLLAPSE MODEL At Junction mass sources : active At SC boiling surfaces  $% (M_{\rm e})$  : active, off at: DTBCCV= 1.00000E+00 K At tabular mass sources  $% (M_{\rm e})$  : active =CV= CV-001, DROPLET AND BUBBLE ACTIVATORS Droplets creation at Junctions : inactive Bubbles creation at Junctions : active Boiling bubbles are created not deeper than: DMBLCV = 5.00000E+00 m Non-eq. bubbles are created not deeper than: DMNBCV = 2.00000E+00 m Droplet diameter at Junctions and TMS : Taylor instability model Limits on diameter of droplets and bubbles created at Junctions and TMS: DMIN (m) DMAX (m) Droplets : 1.00000E-03 2.00000E-02 Bubbles : 1.00000E-03 9.00000E-02 =CV= CV-001, VELOCITY CHANGE LIMITS dVatms/dt = 1.00000E+02 Atms : 

 Image: An and a state of the state of t =CV= CV-001, CV DISPERSED COMPONENT OPTION: IWATCV = 3 
 Droplet diameter
 (m) : 1.00000E-02

 Bubble diameter
 (m) : 1.60000E-02

 Droplet position
 (-) : 7.00000E-01
 Bubble position (-) : 8.00000E-01 Alpha-1 bubb.-annu. (-) : 7.50000E-01 Alpha-2 bubb.-annu. (-) : 8.00000E-01 =CV= CV-001, DISTRIBUTION PARAMETER, CO, MODEL: ZUBER AND FINDLAY =CV= CV-001, NON-EQUILIBRIUM MASS TRANSFER MODEL CONSTANT IN N-E BOILING MODEL : Cbb = 5.00000E-03 CONSTANT IN N-E CONDEN. MODEL : Cbc = 5.00000E-03 STEAM FROM N-E BOILING IS PLACED IN THE POOL AS BUBBLES WATER FROM N-E CONDEN. IS PLACED AT THE INTERPHASE N-E MASS TRANSFER IN DROPLETS : INACTIVE N-E MASS TRANSFER IN BUBBLES : INACTIVE =CV= CV-001, INTERPHASE HEAT AND MASS TRANSFER MODEL AT POOL-ATMS INTERPHASE : ACTIVE AT DROP-ATMS INTERPHASE : ACTIVE AT BUBB-POOL INTERPHASE : ACTIVE =CV = CV - 0.01. DE-ENTRAINMENT CALCULATION DROPLET DE-ENTRAINMENT : IMPLICIT

BUBBLE DE-ENTRAINMENT : IMPLICIT

Below the individual Control Volume printouts, the total volume is printed (sum of the volumes for all CVs present in the model), as well as the volume data for the three largest volumes in the model. In the presented example the largest volume is CV-005 with 10,000 m<sup>3</sup>. The volume of the remaining CVs is 8,020 m<sup>3</sup>. The next in size is CV-003, with 5,000 m<sup>3</sup>. The volume of the remaining CVs (excluding CV-005 and CV-003) is 3,020 m<sup>3</sup>. The third in size is CV-004, with 3,000 m<sup>3</sup>. The volume of the remaining CVs (excluding CV-005, CV-003, CV-004) is 20 m<sup>3</sup>.

At the bottom of the CV input printout the internal CV numbering scheme is given. All printouts, diagnostic messages, plots, etc., are made using the reference numbers, which are chosen by the user. The calculations are performed using the internal, consecutive numbers. The user typically does not need to know the internal numbers. They might be helpful in case of some debugging sessions. The internal numbers are printed at the bottom of the input data printouts for every package.

=CV= ALL CONTROL VOLUMES ------TOTAL VOLUME = 1.80200E+04 (m3) DATA FOR 3 LARGEST CVs : VOL. OF REMAINING CV VOLUME CVs 1.0000E+04 8.0200E+03 CV-005 Environment CV-003 Larger\_building\_\_\_\_\_5.0000E+03 3.0200E+03 CV-004 Smaller building 3.0000E+03 2.0000E+01 \_\_\_\_\_ =CV= CONTROL VOLUME INTERNAL NUMBERING SCHEME \_\_\_\_\_ 
 Int. Ref.
 Int. Ref.
 Int. Ref.
 Int. Ref.
 Int. Ref.

 No.
 No.
 No.
 No.
 No.
 No.
 No.

 1
 CV-001
 2
 CV-002
 3
 CV-003
 4
 CV-004
 5
 CV-005
 \_\_\_\_\_

An example of the transient printout for a Control Volume is shown below. The printout consists of several blocks. The discussion of the data printed in each block is given below the printout.

Pressure, Pa

1.10120E+05 1.10120E+05 1.10120E+05 1.20355E+05

Temper Sat. 1 Sat. 1 Volum Mass 1 Volume Mass Energy Vert. Horiz	rature, Temp., Pressure Fraction Fraction Velocity Velocity	K Fa - m3 kg J m/s -	3.1926 3.0373 1.0205 9.9999 4.7555 5.6058 1.6525 -3.5327 8.0185	57E+02 30E+02 54E+04 91E-01 31E-01 53E+00 31E+00 52E+06 74E-02 50E-03	3.4664 3.75410 3.63342 9.45900 7.76873 4.49833 4.38912 1.35010 6.37433 8.01850	1E+02 DE+02 3E+04 4E-06 2E-03 2E-05 1E-02 DE+04 5E+00 DE-03	3.15027F 3.75410F 8.21047F 9.53471F 9.99937F 5.00041F 4.95750F 8.69274F 2.19100F 0.00000F	E+02 E+02 E+03 E-01 E-01 E+00 E+03 E+08 E-02 E+00	3.14969E+02 3.03825E+02 8.18488E+03 4.65287E-02 6.25613E-05 2.44016E-01 3.10167E-01 9.26118E+04 3.02792E-01 0.00000E+00
=CV=	CV-001,	FLUID PRO	OPERTY	DATA A	r time	: 5.10	)000E+00	(s)	
Quant:	ity 	Units	Atms-	-Gas	Atms-1	Drop 	Pool-Li	Lq	Pool-Bub
Speci: Densit Intern Enthal Viscos Conduc Cp Cv Prandt Expans Diffus Surfac	fic Volume by hal Energy py sity ctivity cl Number sion coef. sion coef. ce tension	m3/kg kg/m3 J/kg kg/m/s W/m/K J/kg/K J/kg/K - 1/K m2/s N/m	8.4832 1.1788 2.9478 3.8820 1.8937 2.7193 1.0371 7.4433 7.2228 3.1321 2.6826	22E-01 30E+00 37E+05 55E+05 76E-05 31E-02 15E+03 39E+02 33E-01 17E-03 53E-05	1.0248 9.7571 3.0760 3.0771 3.8589 6.6571 4.1892 4.1876 2.4283 5.9648	9E-03 8E+02 2E+05 5E+05 5E-04 3E-01 1E+03 7E+03 3E+00 4E-04 5E-02	1.00866E 9.91419E 1.75345E 1.75456E 6.30334E 6.30334E 4.18204E 4.18204F 4.16376E 4.03462E 6.92942E	E-03 E+02 E+05 E+05 E-04 E-01 E+03 E+03 E+00 E-04 E-02	7.86725E-01 1.27109E+00 2.98587E+05 3.93266E+05 1.81697E-05 2.67289E-02 1.06371E+03 7.62893E+02 7.23085E-01 3.17491E-03 2.38757E-05
=CV=	CV-001,	ATMOSPHEI	re gas	COMPOS	ITION A	r time	: 5.100	)00E+(	00 (s)
GAS No.	3 Id.	MASS kg		MASS FRACT	3 Lon	PRESS Pa	SURE a	VOI FRAC	JUME CTION
 3 4 5	H2O N2 O2	1.44357F 4.21256F 1.24889F	 E-01 E+00 E+00	2.57513 7.51464 2.22785	3E-02 4E-01 5E-01	4.4057 8.3937 2.1777	75E+03 71E+04 71E+04	4.000	233E-01 58E-01
Tota	als:	5.605811	E+00	1.00000	)E+00	1.1012	20E+05	1.000	00E+00
Rela	ative humi	dity (-)	:	4.31709	9E-01				
=CV=	CV-001,	POOL BUBE	BLE GAS	S COMPOS	SITION 2	AT TIME	E : 5.10	)000E+	-00 (s)
GAS No.	3 Id.	MASS kg		MAS: FRACT	5 Lon	PRESS Pa	SURE a	VOI FRAC	JUME CTION
3 4	H2O N2	7.55277E 3.02614E	E-03 E-01	2.4350 9.7564	7E-02 9E-01	4.4318	33E+03 23E+05	3.682 9.631	29E-02 77E-01
Tota	als:	3.10167	E-01	1.00000	)E+00	1.2035	55E+05	1.000	000E+00
Rela	ative humio	dity (-)	:	5.41465	5E-01				
=CV=	CV-001,	PARTICLE	DATA A	AT TIME	: 5.1	0000E+0	)0 (s)		
Quant	ity	Units	Dropl	lets	Bubb	les			
No. of Avera Avera Avera	f particle: ge position ge diamete: ge volume	s – n m r m m3	8.5941 3.3319 1.0000 5.2360	L6E+01 96E+00 )0E-02 )7E-07	1.1174 4.1920 1.6000 2.1446	9E+05 5E+00 0E-02 9E-06			
=CV=	CV-001,	MASS SOUR	RCE DAI	TA AT T	IME :	5.10000	)E+00 (s)		
Quant	ity	Units	Atms-	-Gas	Atms-1	Drop	Pool-Li	Lq	Pool-Bub
1) JN 2) SC,	flows: Wm Hm /TC: Wm Hm	kg/s - W - kg/s - W -	-5.0432 -1.8139 -1.4802 -3.5913	22E-02 - 91E+04 - 23E-04 36E+02	-6.44212 -1.9823 0.0000 0.0000	2E-04 4E+02 0E+00 0E+00	0.00000E 0.00000E 1.48023E 1.08455E	E+00 E+00 E-04 E+01	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00

3) No	on-equil:Wm	kg/s	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
<i>л</i> ) т,	Hm htorph • Wm	W ka/a	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00 2.05230E-03
4) 11	Hm	Kg/S W	1.65598E+03	-1.75618E+02	-2.11194E-03	2.03239E-03 5.28847E+03
5) De	e-entrnm:Wm	kq/s	4.46211E-02	-9.89443E-02	9.89443E-02	-4.46211E-02
	Hm	W	1.75480E+04	-3.04466E+04	3.04466E+04	-1.75480E+04
6) Má	ass Src.:Wm	kg/s	0.00000E+00	1.00000E-01	-1.02918E-03	1.01029E-01
	Hm	W	0.00000E+00	3.21779E+04	-1.80468E+02	3.65650E+04
7) H2	2 burn: Wm	kg/s	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
0) 0-	HM	W lræ (a	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
0) 02	Hm	NG/5 W	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
=CV=	CV-001,	ENERGY :	SOURCE DATA AT	TIME : 5.10	)000E+00 (s)	
Ouant	titv	Units	Atms-Gas	Atms-Drop	Pool-Lig	Pool-Bub
1) SC	C/TC: Qn	W	-3.68093E+01	0.00000E+00	-2.71160E+00	0.00000E+00
2) Tł	n.Rad.: Qn	W	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
3) Ir	nerph.: Qn	W	6.80487E+01	-1.39926E+03	-4.22855E+03	-8.38738E+02
4) Bi	ıb.co⊥l.:Qn	W	U.UUUU00E+00	U.UUUU00E+00	3.62667E+03	U.UUUUUE+00
5) Er	hergy s.:Qn	W M	U.UUUUUE+00	0.00000E+00	1.00000E+05	0.0000E+00
ひ) H2 7) 中・	rp/Comp.Op	VV TAT	0.000008+00	0.000008+00	0.000008+00	0.000008+00
/) [\]/	arb,comp.yn ark: p*dV/d+	W	-4.79847E+03	-1.79734E-02	1.18542E+01	4.78664E+03
**(	p av/at		1., 901/11/03	1		
=CV=	CV-001,	MASS SO	URCE DATA FROM	M INDIVIDUAL S	SOURCES	
=CV=	CV-001,	JUNCTIO	N FLOW DATA AT	TIME : 5.10	)000E+00 (s)	
JN	Quantity	Units	Atms-Gas	Atms-Drop	Pool-Liq	Pool-Bub
001	Flow (in)	kg/s	-5.04322E-02	-6.44212E-04	0.00000E+00	0.00000E+00
	Elevation	m	-1.81391E+04	-1.98234E+02	5 24442E+00	5 24442E+00
	Rel Elev	_	-1 30838E-01	-1 30838E-01	-5 00000E-01	-5 00000E-01
	Part dia.	m	1.500501 01	1.00000E-02	5.000001 01	0.00000E+00
	Part.vol.	m.3		5.23607E-07		0.00000E+00
	Part. src	1/s		-1.26096E+00		0.00000E+00
Indiv	vidual gas m	ass sou	rces (kg/s),	NT.		
No	AS Td	ATMOSPI ka/s	HERE POC	)L (s		
3	Н2О	-6.5733	3E-04 0.0000	)0E+00		
4	N2	-3.8383	6E-02 0.0000	00E+00		
5	02	-1.1391	3E-02 0.0000	)0E+00		
=CV=	CV-001,	SOLID C	ONDUCTOR DATA	AT TIME : 5.	.10000E+00 (s)	
SC	Quantity	Units	Atms-Gas	Atms-Drop	Pool-Liq	Pool-Bub
011L	Mass tr.	kg/s	-7.40114E-05	7.40114E-05	U.U0000E+00	U.UUU00E+00
	Enthalpy	W	-1./9568E+02	5.42273E+00	U.UUUUUE+00	U.UUUUUE+00
	Elevation	m —	3.UUUUUE+UU	4./3358E+00	U.UUUUUE+00	U.UUUUUE+UU 5 000007 01
	Net. Liev.	- m	-1.30030E-01	-J.UUUUUE-UI	J.00000E-01	0.000008-01
	Part vol	m.3		6.52182E-08		0.00000E+00
	Part. src	1/s		1.14005E+00		0.00000E+00
SC	Ouantity	Units	Atms-Gas	Atms-Drop	Pool-Lia	Pool-Bub
	~					
012L	Mass tr.	kg/s	-7.40114E-05	7.40114E-05	0.00000E+00	0.00000E+00
	Enthalpy	W	-1.79568E+02	5.42273E+00	0.00000E+00	0.00000E+00
	Elevation	m	1.00000E+00	4.75558E+00	0.00000E+00	0.00000E+00
	Rel. Elev.	-	2.89721E-01	-5.00000E-01	5.00000E-01	5.00000E-01
	Vart dia	m		4.99407E-03		U.00000E+00
	Dart. 1			C F0100- 00		~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~
	Part.vol.	m3 1/c		6.52182E-08		0.00000E+00
	Part.vol. Part. src	m3 1/s		6.52182E-08 1.14005E+00		0.00000E+00 0.00000E+00

Quantity	Units	Atms-Gas	Atms-Drop	Pool-Liq	Pool-Bub
Volumo		4 75553 <u><u></u>+00</u>	1 10030E-05	5 000/1 TT+00	2 44016E-01
Volume Maga transfor	1113	4.73333E+00	4.49032E-03	0.00041E+00	2.44010E-01
Fass transfer	M/m3	0.00000E+00	0.0000000000000000000000000000000000000	0.00000E+00	0.00000E+00
Elemetion	W/IIIS	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00
Deletine Elen	111	0.0000000000000000000000000000000000000	0.0000000000000000000000000000000000000	0.00000E+00	0.00000E+00
Relative Elev.	-	0.00000E+00	0.000005+00	0.00000E+00	0.000005+00
Part, diameter		0.00000E+00		0.00000E+00	
Part. Volume	1/2/22	0.00000E+00		0.00000E+00	
Part. Source	1/5/103	0.000008+00		0.00000E+00	
=CV= CV-001,	INTERPHA	SE MASS TRANS	FER DATA AT T	IME : 5.1000	)E+00 (s)
Quantity	Units	Atms-Pool	Atms-Drop	Pool-Bub	
Area	m2	1 00000E+00	2 69993E-02	8 98737E+00	
Mass tr. coeff.	m/s	2.51628E-03	9.10617E-02	9.81888E-03	
Mass transfer	ka/m2/s	5.95570E-05	2.11433E-02	2.28363E-04	
Enthalpy - gas	W/m2	1.53463E+02	5.56500E+04	5.88433E+02	
Enthalpy gub	W/m2	1 04435E+01	6 50452E+03	4 00444E+01	
Conv HTC	W/m2/K	1 01679E+00	9 79059E+01	7 85572E+03	
Conv heat flux	W/m2	-4 31159E+00	2 68008E+03	4 55065E+02	
Mass tr heat fl	W/m2	1 43019E+02	4 91455E+04	5 48389E+02	
Liquid temperat	K	3 15027E+02	3 46641E+02	3 15027E+02	
Gas temperat.	ĸ	3 192671-02	3 192678+02	3 149698+02	
Gas volume fract	ions	J.1720/ETUZ	J • 1 J 2 U / LT U 2	2.1100000002	
Gas vorume rract	ц20	4 000868-02	4 000868-02	3 682298-02	
	N2	4.00080E-02	4.00080E-02	9.63177E-01	
	02	1.97758E-01	1.97758E-01	0.00000E+00	
	02	1.077002 01	1.077002 01	0.00002.00	
=CV= CV-001,	DE-ENTRA	INMENT DATA A	T TIME : 5.10	0000E+00 (s)	
Quantity	Units	Drop ver	Drop hor	Bubble ver	
Mass transfer	kg/s	9.89443E-02	0.00000E+00	4.46211E-02	
Enthalpy	W	3.04466E+04	0.00000E+00	1.75480E+04	
Elevation	m	4.75558E+00	0.00000E+00	5.24442E+00	
Relative Elev.	-	-5.00000E-01	0.00000E+00 -	-5.00000E-01	
Volume fraction	-	1.57989E-05	0.00000E+00	1.15936E-01	
=CV= CV-001,	TABULAR	MASS SOURCE D	ATA AT TIME :	5.10000E+00	(s)
M	1				
Mass source No.:					
Quantity	Units	Atms-Gas	Atms-Drop	Pool-Liq	Pool-Bub
Mass flux	kg/s	0.00000E+00	0.00000E+00	0.00000E+00	1.00000E-01
Temperature	K	0.00000E+00	0.00000E+00	0.00000E+00	3.74000E+02
Pressure	Pa	0.00000E+00	0.00000E+00	0.00000E+00	1.00000E+05
Enthalpy	W	0.00000E+00	0.00000E+00	0.00000E+00	4.00112E+04
Elevation	m	4.75558E+00	4.75558E+00	0.00000E+00	0.00000E+00
Relative Elev.	-	-5.00000E-01	-5.00000E-01	5.00000E-01	5.00000E-01
Part. diameter	m		0.00000E+00		2.00000E-02
Part. volume	m3		0.00000E+00		4.18885E-06
Part. source	1/s		0.00000E+00		1.66983E+04
Bubble collapse	paramete	rs			
Collapse time	s	0.00000E+00			
Bubble flow time	s	2.00000E+01			
Pool bypas frac.	_	0.00000E+00			
Heat transfer c.	W/m2/K	7.24499E+03			
Heat flux	W/m2	-2.28236E+06			
Heat to pool	W	3.62667E+03			
	TT 1	D. C	7 Chan and 1		
Quantity	Units	Before coll.	AITER COLL.		
Gas flow	kg/s	1.00000E-01	1.01029E-01		
Liquid flow	kg/s		-1.02918E-03		
Gas enthalpy	W	4.00112E+04	3.65650E+04		
Liquid enthalpy	W		-1.80468E+02		
Bubble diameter	m	2.00000E-02	1.89838E-02		
Bubble temperat.	K	3.74000E+02	3.15027E+02		
Gas volume fract	ions, (-	):			

			H2 He H2O N2 O2 CO2		0.00000E+ 0.00000E+ 0.00000E+ 1.00000E+ 0.00000E+ 0.00000E+	00 00 00 00 00 00	0.0000 0.0000 1.018 9.898 0.0000 0.0000	00E+00 00E+00 70E-02 13E-01 00E+00 00E+00				
Mass Quan	source tity	No.	.: Uni	2 ts	Atms-Gas		Atms-	-Drop	1	Pool-Liq	P	ool-Bub
Mass Temp Pres Enth Elev Rela Part Part Part	flux erature sure alpy ation tive El . diame . volum . sourc	ev. ter e	kg/: K Pa W m - m m3 1/s		0.00000E+ 0.00000E+ 0.00000E+ 0.00000E+ 0.00000E+ 5.00000E-	00 00 00 00 00 00 00	1.0000 3.5000 1.0000 3.217 0.0000 5.0000 1.2380 9.9359 1.0336	00E-01 00E+02 00E+05 79E+04 00E+00 00E-01 04E-02 90E-07 52E+02	0 0 0 5 -5	00000E+00 00000E+00 00000E+00 00000E+00 24442E+00 .00000E-01	0. 0. 0. 5. -5. 0. 0.	00000E+00 00000E+00 00000E+00 24442E+00 00000E-01 00000E+00 00000E+00 00000E+00
=CV=	CV-00	1,	ENER	GY S	OURCE DATA	FRO	M IND	IVIDUAL	S	DURCES		
=CV=	CV-00 Side Q	1 <b>,</b> uant	SC C tity	ONVE Uni	CTION DATA ts Atms-	AT Gas	TIME : At	: 5.10 cms-Dro	000 p	)E+00 (s) Pool-Liq		Pool-Bub
001 002 003 004 005 006 007 008 009 010 011 012 =CV=	Left H Left H	eat eat eat eat eat eat eat eat eat eat	flux flux flux flux flux flux flux flux	W W W W W W W W LAR	0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 -2.4251 -1.8283 -1.8283 ENERGY SOU	00E+0 00	0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 0 0.0 1 0.0 1 0.0 1 0.0 1 0.0	00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+ 00000E+			01 01 01 01 01 01 01 01 01 00 00 00	C.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 (s)
ES	Quanti	ty	Uni	ts	Atms-Gas	;	Atms-	-Drop	]	Pool-Liq	P	ool-Bub
001	Heat f	lux	- <u>-</u>		0.00000E+	00	0.000	)0E+00	1	.00000E+05	0.	00000E+00

The first block contains the data related to the <u>pool surface</u>, including elevation (above bottom of CV), velocity (upwards), area, characteristic dimension, volumes above and below the pool surface, vertical cross section area above and below the pool surface, and volume fractions of bubbles and droplets at the pool surface.

The second block contains the current values of the <u>stratification</u> parameters: DSP, TSP, PSP. If there is a thermal stratification of atmosphere or pool then the temperatures at the bottom and at the top of atmosphere or pool are printed.

The third block contains printout of <u>thermodynamic data</u> for all components that may be present in a Control Volume: atmosphere (gas), droplets, pool (liquid), and bubbles. If a given component is currently not present in the Control Volume then its column is filled with zeroes. **The volume and the mass fractions, printed in this block, always refer to the sum of the continuous and the corresponding discontinuous component**. For example, the bubble volumetric fraction  $(4.65287 \times 10^{-2})$  is equal to the volume of bubbles  $(2.44016 \times 10^{-1} \text{ m}^3)$  divided by the sum of the volume of water in the pool  $(5.00041 \text{ m}^3)$  and the volume of bubbles. The droplet volumetric fraction

 $(9.45904 \times 10^{-6})$  is equal to the volume of droplets  $(4.4983250 \times 10^{-5} \text{ m}^3)$  divided by the sum of volumes of the atmosphere  $(4.75553 \text{ m}^3)$  and the droplets.

It is important to note that the positive direction for the vertical velocities is always towards the atmosphere-pool interphase. Thus for pool and bubbles positive velocity means upwards, for atmosphere and droplets positive velocity means downwards.

The next block contains <u>fluid property data</u> for all components present in a Control Volume: atmosphere (gas), droplets, pool (liquid), and bubbles. If a given component is currently not present in the Control Volume then its column is filled with zeroes.

The fourth block contains the data on the <u>atmosphere gas composition</u>. The atmosphere is assumed to be composed of a mixture of gases. This block gives masses, mass fractions, partial pressures, and volume fractions, for all gases in the atmosphere, as well as the relative humidity for the atmosphere. This block is printed only if atmosphere is present in the Control Volume.

The next block contains the data on the <u>bubble gas composition</u>. The bubbles are assumed to be composed of a mixture of gases. This block gives masses, mass fractions, partial pressures, and volume fractions, for all gases in the bubbles, as well as the relative humidity for the bubble gas. This block is printed only if bubbles are present in the Control Volume.

The next block contains <u>particle data</u>, including number of particles, position, diameter and volume of the average particle. Note that the position inside the Control Volume is defined differently for droplets and bubbles: **In case of bubbles the average position is measured from the bottom of CV, in case of droplets the average position is measured from the top of CV**. In case particles are not present in a CV their average position is assumed to be zero.

The next block contains <u>mass source data</u> for CV, including mass fluxes and corresponding enthalpy fluxes for all components. In the example case there is a mass source due to Junction flows, evaporation or condensation on Solid Conductors, interphase mass transfer, de-entrainment, and tabular mass sources. The values printed there are explained in the paragraph discussing the printout of individual mass sources, below.

The next block contains data on <u>energy sources</u> in CV, including energy fluxes for all components. In the example case there is an energy transfer due to convection from Solid Conductors, interphase energy transfer, bubble collapse, and tabular energy sources.

The following blocks contain data on <u>individual mass sources</u>. The first block in this group contains data on <u>Junction flows</u>. This block contains mass sources for all components (atmosphere, droplets, pool and bubbles) caused by the Junction flows. Note that the values printed in this block are positive if the flow is into the CV, regardless what is the positive Junction direction. In the example case JN-001 is the only Junction connected to the Control Volume. Consequently the mass flow printed in this block is equal to the JN mass source,  $W_m$ , printed under point 1.) in the block "mass source data". If more Junctions were connected to the CV then the value  $W_m$ , printed in the "mass source data", would be equal to the sum of the mass flows for all Junctions connected to a given CV.

Apart from the mass and enthalpy sources the block contains data on the source absolute and relative "elevations". The definitions of those "elevations" are given in Volume 1. In case of pool and bubbles, the absolute elevations are defined as the distances from the bottom of a CV to a given place in the pool. in case of atmosphere and droplets, the absolute elevations are defined as the distances from the top of a CV to a given place in the atmosphere. The relative elevations are

defined as the distances from the center of the continuous component (atmosphere, pool) to a given place in CV, divided by the height of the continuous component.

In the example case only gas flows through the Junction, thus there is a non-zero source only for the atmosphere. Total height of the CV is 10.0 m and the center point of the Junction is located at 7.0 m above the floor of the CV. Thus, for atmosphere and droplets the absolute elevation of the source is 3.0 m. The pool surface level is 5.24442 m, thus the height of the atmosphere is 10.0 - 5.24442 = 4.75558 m. The relative elevations for atmosphere and droplet, which are measured from the atmosphere center point, are equal to:  $(4.75558/2.0 - 3.0)/4.75558 = -1.30838 \times 10^{-1}$ .

In case of pool and bubble there is no mass source since the Junction is located in the atmosphere space. Nevertheless the values of the elevations are still printed. The absolute elevation is set to the elevation of the pool surface (5.24442 m). Note that if the pool level was somewhat above the lowermost point of the Junction (6.9 m), say at 6.96 m, then the source location would be in the center of the water cover area: (6.9+6.96)/2 = 6.93 m. If the pool level was above the uppermost point of the Junction (7.1 m), then the source location would be always at the Junction center point (7.0 m) which would then be the same as the center of the water covered area. Thus the source elevation is a continuous function of the pool level. Relative elevations are obtained in the same manner as above, but this time they are related to the center point of the pool: (5.24442/2.0 - 5.24442) / 5.24442 = -0.50. Note that the relative elevations are always within the range: (-0.5, +0.5).

The next part of this block contains data on the diameters and volumes of a single particle (bubbles, droplets), and the source strength (number of particles created per second). In the present case the source is negative, that means droplets are transported out of CV through the Junction. The following part gives the gas composition in case of gas sources (atmosphere, bubbles).

At the bottom of the Junction mass source printout the bubble collapse parameters are printed if bubble collapse occurs. In this case bubble collapse does not occur (there is no positive gas mass source below the pool level) and the bubble collapse data is not printed (an example of bubble collapse printout is given below, in the Tabular Mass Source output description).

The following blocks contain data on <u>Solid Conductor sources</u>, belonging to the group of the individual mass sources. These blocks contain mass transfer (boiling / condensation) on Solid Conductors. In the example case there is a mass transfer (condensation) on the left surfaces of SC-011 and SC-012. There is a negative mass source for the atmosphere gas and a positive mass source for the droplets. Note that in the block "mass source data" the value of mass source, W<sub>m</sub>, printed under point 2.) is equal to the sum of the individual values for SC-011 and SC-012, printed here. This block contains the usual information on the absolute and relative elevations. The way those are defined is discussed in the description of the Junction flows block, above. Note that in case of atmosphere the elevation of the droplet mass source is equal to the elevation of the lowermost point of the Conductor. Again it should be noted that in case of pool and bubbles the absolute elevations are measured from the bottom of CV, in case of atmosphere and droplets the absolute elevations are measured from the top of CV.

In the presented example the center points are: SC-011: 7.0 m, SC-012: 9.0. The height of both surfaces is 1.0 m. Thus the absolute elevations, for atmosphere and droplet sources, measured from the top of CV, are equal to, for the center points: 3.0 m, and 1.0 m; for the lowermost points: 3.5 m, and 1.5 m, for SC-011 and SC-012 respectively. In the present example however the elevations of the droplet sources are not equal to 3.5 and 1.5 m. This is because the default value of the condensate drainage parameter (CFDLSC) is used, which results in depositing droplets from condensing surfaces directly in the pool (see description of CFDLSC in sections 2.3.11 and 2.3.12). The droplet source

elevation is therefore set to the pool level, measured from the top of CV: 10.0 - 5.24442 = 4.75558. To obtain a mechanistic treatment of droplets falling from the condensing surfaces one would have to set CFDLSC to the height of the SC (1.0 m). Then the droplet source elevation would indeed be equal to 3.5 m and 1.5 m for SC-011 and SC-012 respectively.

The next part of this block contains data on the diameters and volumes of a single particle (bubbles, droplets), and the source strength (number of particles created per second). In the presented example the condensate forms droplets of the diameter of about half centimeter, at the rate of about one droplet per second. In the present example those droplets are not suspended in the atmosphere but deposited directly in the pool, because of the default value of the CFDLSC parameter, mentioned above. This particular choice of the default value of the CFDLSC and CFDRSC parameters was motivated by the observation that typically calculations are faster, without any practical difference in the results. Therefore mechanistic treatment of droplets from condensing surface is an option that must be activated by the user, if he wishes to use it.

At the bottom of the Solid Conductor mass source printout the bubble collapse parameters are printed if the bubble collapse occurs. In this case the bubble collapse does not occur (there is no boiling) and the bubble collapse data is not printed.

The following block contains data on <u>Non-equilibrium mass transfer</u>, belonging to the group of the individual mass sources. In the presented example there is no non-equilibrium mass transfer and the only non-zero values are the component volumes.

The following block contains data on <u>Interphase mass transfer</u>, belonging to the group of the individual mass sources. The data is printed for the three inter-phases: pool-atmosphere, atmosphere-droplet, and pool-bubble. The data include: interphase areas, mass fluxes, corresponding enthalpy fluxes, and the heat fluxes: convective heat flux and mass transfer heat flux. The mass transfer heat flux is simply the difference between the gas enthalpy flux and the liquid enthalpy flux (approximately equal to the latent heat of evaporation multiplied by the mass transfer rate). The following comments can be made in relation to the interphase mass transfer data for the presented example.

In case of pool-atmosphere interphase there is a small negative (atmosphere-to-pool) convective heat flux. It is caused by the fact that the atmosphere temperature  $(3.19267 \times 10^2 \text{ K})$  is slightly higher than the pool surface temperature  $(3.15027 \times 10^2 \text{ K})$ . The mass transfer rate (as well as the mass transfer heat flux) is positive indicating that evaporation takes place. This evaporation is caused by the fact that the atmosphere is relatively dry (relative humidity of about  $4.31709 \times 10^{-1}$ ).

In case of atmosphere-droplet interphase there is a positive (droplet-to-atmosphere) convective heat flux, and mass transfer flux, caused by the fact that droplets (created at the tabular mass source) are relatively warm ( $3.46641 \times 10^2$  K). In case of bubbles there is positive mass flux (evaporation into bubbles). The bubbles, injected by Tabular Mass Source, are initially dry (pure nitrogen bubble source).

The relation between the heat and mass transfer rates printed in this block and the values printed in the mass source data and heat source data, printed above, is not trivial and is shortly explained here. The values of interphase heat and mass transfer are discussed below sequentially for: droplets, bubbles, atmosphere, and pool.

#### Droplets

The total mass transfer for droplet-atmosphere transfer, printed in the mass source data for droplets,  $W_m$ , in point 4), is equal to:

 $W_m = -Area (2.69993 \times 10^{-2} \text{ m}^2) \cdot Mass \text{ transfer rate} (2.11433 \times 10^{-2} \text{ kg/m}^2/\text{s}) = -5.70856 \cdot 10^{-4} \text{ kg/s}.$ 

The minus sign comes from the convention that positive interphase mass transfer means evaporation. Therefore, when the mass transfer is positive, the droplet mass decreases.

The corresponding enthalpy source for the droplets, H<sub>m</sub>, in point 4) is equal to:

 $H_m = -Area (2.69993 \times 10^{-2} \text{ m}^2) \cdot Enthalpy-liq (6.50452 \times 10^3 \text{ W/m}^2) = -1.75618 \times 10^3 \text{ W}.$ 

The heat source, printed in the energy source data for droplets, Q<sub>n</sub>, in point 3), is equal to:

$$\begin{split} Q_n &= - \text{Area} \; (2.69993 \times 10^{-2} \; \text{m}^2) \cdot \text{Convective heat flux} \; (2.68008 \times 10^3 \; \text{W/m}^2) - \\ &- \text{Area} \; (2.69993 \times 10^{-2} \; \text{m}^2) \cdot \{\text{Enthalpy-gas} \; (5.56500 \times 10^4 \; \text{W/m}^2) - \\ &- \text{Enthalpy-liq} \; (6.50452 \times 10^3 \; \text{W/m}^2) \} = -1.39926 \times 10^3 \; \text{W} \end{split}$$

The first term represents the true heat transfer at the droplet surface, the second term represents the heat consumed during evaporation (enthalpy of the created steam minus enthalpy of the disappearing liquid). The minus sign in the first term comes from the convention that positive interphase heat transfer means heat from liquid to gas.

#### **Bubbles**

The total mass transfer for bubble-atmosphere transfer, printed in the mass source data for bubbles,  $W_m$ , in point 4), is equal to:

 $W_m = +$ Area (8.98737 m<sup>2</sup>) · Mass transfer rate (2.28363×10<sup>-4</sup> kg/m<sup>2</sup>/s) = 2.05239×10<sup>-3</sup> kg/s.

The plus sign comes from the convention that positive interphase mass transfer means evaporation. Therefore, when the mass transfer is positive, the bubble mass increases.

The corresponding enthalpy source for the bubbles, H<sub>m</sub>, in point 4) is equal to:

 $H_m = Area (8.98737 m^2) \cdot Enthalpy-gas (5.88433 \times 10^2 W/m^2) = 5.28847 \times 10^3 W.$ 

The heat source, printed in the energy source data for bubbles, Q<sub>n</sub>, in point 3), is equal to:

 $\begin{aligned} Q_n &= + Area \; (8.98737 \; m^2) \cdot Convective \; heat \; flux \; (4.55065 \times 10^2 \; W/m^2) - \\ &- Area \; (8.98737 \; m^2) \cdot \{ \; Enthalpy-gas \; (5.88433 \times 10^2 - Enthalpy-liq \; (4.00444 \times 10^1) \; \} = \\ &= -8.38738 \times 10^2 \; W \end{aligned}$ 

The first term represents true heat transfer at the bubble surface; the second term represents the heat consumed during evaporation (enthalpy of the created steam minus enthalpy of the disappearing liquid). The plus sign in the first term comes from the convention that positive interphase heat transfer means heat from liquid to gas.

#### Atmosphere

The total mass transfer, printed in the mass source data for atmosphere,  $W_m$ , in point 4), is the sum of pool-atmosphere (p-a) and droplet-atmosphere (d-a) mass transfers, and is equal to:

$$\begin{split} W_m &= + \operatorname{Area}_{p\text{-}a} (1.0 \text{ m}^2) \cdot \text{Mass transfer rate}_{p\text{-}a} (5.95570 \times 10^{-5} \text{ kg/m}^2/\text{s}) + \\ &+ \operatorname{Area}_{d\text{-}a} (2.69993 \times 10^{-2} \text{ m}^2) \cdot \text{Mass transfer rate}_{d\text{-}a} (2.11433 \times 10^{-2} \text{ kg/m}^2/\text{s}) = \\ &= 6.30413 \times 10^{-4} \text{ kg/s} \end{split}$$

The plus sign comes from the convention that positive interphase mass transfer means evaporation. Thus when mass transfer is positive the atmosphere mass increases.

The corresponding enthalpy source for atmosphere, H<sub>m</sub>, in point 4) is equal to:

$$\begin{split} H_m &= Area_{p\text{-}a} \ (1.0 \ m^2) \cdot Enthalpy\text{-}gas_{p\text{-}a} \ (1.53463 \times 10^2 \ W/m^2) + \\ &+ Area_{d\text{-}a} \ (2.69993 \times 10^{-2} \ m^2) \cdot Enthalpy\text{-}gas_{d\text{-}a} \ (5.56500 \times 10^4 \ W/m^2) = 1.65598 \times 10^3 \ W \end{split}$$

The heat source, printed in the energy source data for droplets,  $Q_n$ , in point 3), is the sum of poolatmosphere (p-a) and droplet-atmosphere (d-a) heat transfers, and is equal to:

 $\begin{aligned} Q_n &= + \text{Area}_{p\text{-}a} \ (1.0 \ \text{m}^2) \cdot \text{Convective heat flux}_{p\text{-}a} \ (-4.31159 \ \text{W/m}^2) + \\ &+ \text{Area}_{d\text{-}a} \ (2.69993 \times 10^{-2} \ \text{m}^2) \cdot \text{Convective heat flux}_{d\text{-}a} \ (2.68008 \times 10^3 \ \text{W/m}^2) = 6.80487 \times 10^2 \ \text{W} \end{aligned}$ 

The minus signs come from the convention that positive interphase heat transfer means heat from liquid to gas.

Pool

The total mass transfer, printed in the mass source data for pool,  $W_m$ , in point 4), is the sum of poolatmosphere (p-a) and pool-bubble (p-b) mass transfers, and is equal to:

$$\begin{split} W_{m} &= -Area_{p-a} \; (1.0 \; m^{2}) \cdot Mass \; transfer \; rate_{p-a} \; (5.95570 \times 10^{-5} \; kg/m^{2}/s) - \\ &- Area_{p-b} \; (8.98737 \; m^{2}) \cdot Mass \; transfer \; rate_{p-b} \; (2.28363 \times 10^{-4} \; kg/m^{2}/s) = -2.11194 \times 10^{-3} \; kg/s \end{split}$$

The minus sign comes from the convention that positive interphase mass transfer means evaporation. Thus when mass transfer is positive the pool mass decreases.

 $\begin{array}{l} \mbox{The corresponding enthalpy source for pool, $H_m$, in point 4$) is equal to: $$ $H_m$ = $-Area_{p-a}$ (1.0 m^2) $\cdot$ Enthalpy-liq_{p-a}$ (1.04435 \times 10^1 $W/m^2$) $-$ $- $Area_{b-p}$ (8.98737 m^2$) $\cdot$ Enthalpy-liq_{b-p}$ (4.00444 \times 10^1 $W/m^2$) $= $-3.70337 \times 10^2 $W$. } \end{array}$ 

The heat source, printed in the energy source data for droplets,  $Q_n$ , in point 3), is the sum of poolatmosphere (p-a) and droplet-atmosphere (d-a) heat transfers, as well as the heat consumed during evaporation from the pool surface, and is equal to:

 $\begin{aligned} Q_n &= -Area_{p\text{-}a} \; (1.0 \; m^2) \cdot Convective \; heat \; flux_{p\text{-}a} \; (-4.31159 \; W/m^2) - \\ &- Area_{p\text{-}b} \; (8.98737 \; m^2) \cdot Convective \; heat \; flux_{p\text{-}b} \; (4.55065 \times 10^2 \; W/m^2) - \\ &- Area_{p\text{-}a} \; (1.0 \; m^2) \cdot \{ \; Enthalpy\text{-}gas_{p\text{-}a} \; (1.53463 \times 10^2 \; W/m^2) - \\ &- \; Enthalpy\text{-}liq_{p\text{-}a} \; (1.04435 \times 10^1 \; W/m^2) \; \} = -4.22855 \times 10^3 \; W \end{aligned}$ 

The minus sign in the first two terms come from the convention that positive interphase heat transfer means heat from liquid to gas.

The following block contains data on <u>De-entrainment</u>, belonging to the group of the individual mass sources. Three de-entrainment processes may be taken into account. For droplets these are vertical de-entrainment (when droplets hit the pool surface or CV floor) and horizontal de-entrainment (when droplets hit a wall). For bubbles only vertical de-entrainment is modelled (when bubbles hit the pool surface). In the presented example the droplet horizontal de-entrainment model is not used, thus zeroes are printed in the second column of this block. Droplet vertical de-entrainment mass transfer is  $9.89443 \times 10^{-2}$  kg/s. This is a negative mass source for the droplets and a positive mass source for the

pool (see mass source data printout,  $H_m$ , point 5). The bubble vertical de-entrainment is equal to  $4.46211 \times 10^{-2}$  kg/s. This is a negative source of mass for the bubbles and a positive mass source for the atmosphere (see mass source data printout,  $H_m$ , point 5).

The following blocks contain data on <u>Tabular mass sources</u>, belonging to the group of the individual mass sources. The tabular mass sources are treated quite similarly to the Junction flow sources and the printout is the same as in case of the Junction flow sources, discussed above. In the presented example there are two tabular sources.

The first tabular source is a source of gas, placed at the bottom of the CV. This gas constitutes a source for the pool bubbles. The mass flow is 0.1 kg/s. The injected stream breaks into bubbles of the diameter of  $2.00000 \times 10^{-2}$  m. The bubble source strength is equal to about  $1.66983 \times 10^{+4}$  bubbles per second.

At the bottom of the printout bubble collapse parameters are printed if the bubble collapse occurs. During the "bubble collapse" phase the bubble temperature  $(3.74000 \times 10^{+2} \text{ K})$  equilibrates with the pool temperature  $(3.15027 \times 10^{+2} \text{ K})$ . Simultaneously some water is evaporated into the bubble. After bubble collapse, the bubble diameter is reduced from  $2.00000 \times 10^{-2} \text{ m}$  to  $1.89838 \times 10^{-2} \text{ m}$ ).

The second tabular source is a source of liquid, placed at the top of the CV. This liquid constitutes a source for the atmosphere droplets. The mass flow is  $1.00000 \times 10^{-1}$  kg/s. The injected stream breaks into droplets of the diameter of  $1.23804 \times 10^{-2}$  m. The droplet source strength is equal to  $1.03362 \times 10^{2}$  droplets per second.

Next hydrogen burn and oxidation data may be printed. Since neither of these processes occurs in the present example, these blocks are not printed and zeroes are printed in the mass source data,  $H_m$ , points 7) and 8), and energy source data  $Q_n$ , point 6).

The following blocks contains data on <u>individual energy sources</u>. The first block in this group contains data on <u>Solid Conductor convection</u>. This block contains heat fluxes from all SC surfaces present in the CV. In the presented example nine SCs (SC-001 - SC-009) convect heat to the pool. One SC (SC-010) is partly immersed in pool and convects heat to both pool and atmosphere. Two SCs (SC-011, SC-012) convect heat to the atmosphere gas.

The following block contains data on <u>Tabular energy sources</u>, belonging to the group of the individual energy sources. In the presented example there is a single tabular energy source, placed below the pool surface in the CV.

At the bottom of the CV output the "summed quantities" (data summed for all Control Volumes) are printed. The example output is given below.

=CV= DATA SUMMED FOR ALL CV M & E SOURCES AT TIME : 5.10000E+00 (s)											
Quantit	-у	Units	Atms-Gas	Atms-Drop	Pool-Liq	Pool-Bub					
Mass Energy Energy	(M Src.) (M Src.) (E Src.)	kg J J	0.00000E+00 0.00000E+00 0.00000E+00	4.05000E-01 1.30320E+05 0.00000E+00	0.00000E+00 0.00000E+00 5.10000E+05	4.05000E-01 1.62045E+05 0.00000E+00					
Quantit	су 	Units	Total Value	_							
Mass Energy Energy Energy	(M Src.) (M Src.) (E Src.) (M&E S.)	kg J J J	8.1000000E-0 2.9236565E+0 5.1000000E+0 8.0236565E+0	1 5 5 5							

\_\_\_\_\_ =CV= DATA SUMMED FOR ALL CONTROL VOLUMES AT TIME : 5.10000E+00 (s) \_\_\_\_\_ Summed mass of gases in atmosphere and pool bubbles 
 GAS
 MASS, ATMS.
 MASS, POOL
 MASS, TOTAL

 No. Id.
 kg
 kg
 kg

 ------ ------ ------ 
 3
 H2O
 1.77702E+00
 7.55277E-03
 1.78457E+00

 4
 N2
 1.01171E+04
 3.02614E-01
 1.01174E+04

 5
 O2
 2.58999E+00
 0.00000E+00
 2.58999E+00
 Quantity Units Atms-Gas Atms-Drop Pool-Liq Pool Quantity Pool-Bub Volumem39.00976E+034.49832E-059.01000E+032.44016E-01Masskg1.01214E+044.38911E-028.93278E+063.10167E-01EnergyJ2.49218E+091.35010E+041.56531E+129.26118E+04 Total values: \* Current = at time: 5.10000E+00 (s) \* C-I = current value minus initial value \* C-I-M&E = current minus initial minus M&E, H2 burn, and Oxidation sources \* C-I-M&E-SC = current minus initial minus M&E, H2 burn, and Oxidation sources minus total integrated heat flux from all 1-D and 2-D SCs Quantity Units Current C - I C-I-M&E C-I-M&E C-I-M&E-SC 
 Volume
 m3
 1.80200E+04
 -3.63798E-12

 Mass
 kg
 8.94290E+06
 8.10000E-01
 5.21541E-10

 Energy
 J
 1.56780E+12
 8.00420E+05
 -1.94526E+03
 -9.72949E-05
 If there are no flows to or from inactive CVs (CVs in which conditions are held constant) then C-I-M&E and C-I-M&E-SC can be used to check M&E balance: Relative mass error = C-I-M&E / Current Relative energy error = C-I-M&E-SC / Current Typically relative errors are ~1E-14 (governed by round-off error of double precision numbers, which is ~1E-15). When Thermal Radiation model is active the energy error depends on the accuracy in view factors and thus may be relatively large: up to ~1E-6 (TR package requires view factor inaccuracy to be not bigger than 1E-7). \_\_\_\_\_

This data contains two parts. The first part gives summed quantities for all mass and energy sources. The second part gives summed quantities for the whole system.

#### Summed quantities for mass and energy sources

This output consists of the following two blocks:

First block. For all components: atmosphere, droplets, pool, and bubbles, the following summed quantities are given:

- integrated mass (kg) from all mass sources,
- integrated energy (J) accompanying mass sources, from all mass sources,
- integrated energy (J), from all energy sources.

Second block. The following summed quantities are given:

- total integrated mass from all mass sources (kg),
- total integrated energy (J) accompanying mass sources, from all mass sources,
- total integrated energy from all energy sources (J).
- total integrated energy (J), all mass and energy sources.

The first three values are equal to their corresponding values in the first block, summed over all components. The last value is equal to the sum of the second and the third value.

#### Summed quantities for all Control Volumes

This output consists of the following three blocks:

First block. For all gases, which are present in atmosphere and bubbles, the mass of each individual gas, summed over all Control Volumes is printed in this block.

Second block. For all components: atmosphere, droplets, pool, and bubbles, the following summed quantities are given: volume, mass, and energy. Note that the atmosphere mass printed in this block is equal to the sum of the atmosphere individual masses printed in the first block, and the bubble mass printed in this block is equal to the sum of the individual bubble masses, printed in the first block.

Third block. The following summed quantities are given: volume, mass, and energy. The printed values are:

- Current values. Note that in the column "Current" each quantity is equal to the sum over all components of the same quantity printed in the second block.
- Current minus initial.
- Current minus initial minus integrated mass and energy sources. This column contains data for mass and energy. The value of mass in this column represents the "**mass error**".
- Current minus initial minus integrated mass and energy sources minus integrated heat flux from all 1-D and 2-D Solid Heat Conductors. This column contains data for energy only. The value represents the "energy error".

The values printed in this block can be considered as the mass and energy errors only in case when there are no flows to or from inactive Control Volumes (CVs in which conditions are held constant -ITYPCV $\neq$ 0, see section 1.1.1). Typically relative errors (the value of error, divided by the "Current" value) are of order of 10<sup>-14</sup> (governed by round-off error of double precision numbers). When the Thermal Radiation model is active the energy error depends on the accuracy in view factors and thus may be relatively large: up to 10<sup>-6</sup> (the TR package requires view factor inaccuracy to be smaller than 10<sup>-7</sup>).

#### 3.1.3 Junction Output

The Junction outputs may be easily found in the output file by searching for the string: =JN=. The first JN printout brings the input data printout. An example of the input printout for a Junction is shown below. The printout mainly reflects the data entered in the input file and is quite self-explanatory.

=JN= =====JN-001====== Example\_problem,\_Junction\_1\_(CV-001\_->\_CV-002)\_\_\_\_

CONNECTION	:	FROM CV-001	L TO CV-002	2
AREA	m2:	1.00000E+00		
ELEVATION	m:	5.00000E+00		
LENGTH (MOM)	m:	5.00000E+00		
EDGES INDICAT	OR :	0.00000E+00		
DIAMETER	m:	1.12838E+00		
HEIGHT	m:	1.12838E+00		
FLOW DIRECTIO	N :	HORIZONTAL		
ELEVATIONS		IN CV-001	IN CV-002	
TOP	m:	5.56419E+00	5.56419E+00	)

BOTTOM m: 4.43581E+00 4.43581E+00 INITIAL VELOCITIES: INPUT VALUES ARE USED =JN= JN-001. Vatms = 0.00000E+00 (m/s)Vpool = 0.00000E+00 (m/s) =JN= JN-001, FRICTION DATA AND COEFFICIENTS 
 FR. LENGTH
 m:
 5.00000E+00

 ROUGHNESS
 m:
 1.00000E-05

 FK.
 Mail

 ROUGHNESS
 m:
 1.000002

 DTAMETER
 m:
 1.12838E+00

 1
 00000E+00
 FORM LOSS (F) -: 1.00000E+00 FORM LOSS (R) -: 1.00000E+00 
 Rf (2-ph, F)
 -:
 1.00000E+00

 Rf (2-ph, R)
 -:
 1.00000E+00

 CMOODY
 -:
 7.00000E-01
 1-PHASE MODEL : COLEBROOK-WHITE 2-PHASE MODEL : HANCOX-NICOLL =JN= JN-001, VALVE DATA MOTOR VALVE : TF-006 (1/A) \* (dA/dt): 1.00000E+00 CHECK VALVE : NONE INITIAL FR.OPEN : 0.00000E+00 MIN OPEN (LEAK) : 0.00000E+00 MAX OPEN (LIMIT): 1.00000E+00 VALVE COEFF. CV : 5.00000E+00 =JN= JN-001, FLOW CONTROL GAS : MOMENTUM EQ. LIQUID : MOMENTUM EQ. =JN= JN-001, FLOW COMPOSITION PARAMETER (FCP) DATA GAS: 1 FCP: 1.00000E+00 GAS: 2 FCP: 1.00000E+00 GAS: 3 FCP: TF-004 GAS: 3 FCP: TF-004 GAS: 4 FCP: 1.00000E+00 GAS: 5 FCP: 1.00000E+00 GAS: 6 FCP: 1.00000E+00 =JN= JN-001, ENTRAINMENT INDICATORS E-atms : 0.00000E+00 E-drop : 1.00000E+00 E-pool : 0.00000E+00 E-bubb : 1.00000E+00 =JN= JN-001, DROP AND BUBBLY FLOW REGIME MODEL PARAMETERS Droplets Bubbles vertical horizontal vertical horizontal 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 Drift flux constant CO 
 Terminal velocity
 v-inf
 0.00000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0.0000E+00
 0 =JN= JN-001, ANNULAR FLOW MODEL: DEFAULT =JN= JN-001, COUNTER-CURRENT FLOW MODEL CONSTANTS Vertical flow: CCFVJN = 1.00000E-01 Horizontal flow: CCFHJN = 1.00000E+01

Below the individual Junction printouts, several blocks are printed containing data valid for all Junctions. Next the Junction connectivity data is printed, which lists all Junctions connected to every Control Volume. This output helps the user to verify the correctness of his model. Finally, the internal numbering scheme for Junctions is printed. The example printout is given below.

=JN= JUNCTION OPTIONS: VELOCITIES AND ELEVATIONS

\_\_\_\_\_ MINIMUM VELOCITY FOR CRITICAL FLOW TEST: 1.00000E+01 m/s JUNCTION ELEVATIONS ARE CHECKED WHETHER THEY ARE TOO CLOSE TO CV BOTTOM OR TOP THIS IS DEFAULT OPTION, USED FOR TWO-PHASE SYSTEMS \_\_\_\_\_ =JN= JUNCTION PACKAGE FLOW SOLUTION JUNCTION FLOW MATRIX IS SOLVED USING: - LU DECOMPOSITION, IF NUMBER OF ACTIVE JN. <=1000 - BICONJUGATE GRADIENT M., IF NUMBER OF ACTIVE JN. >=1001 JUNCTION MATRIX IS RE-SOLVED DURING ITERATIONS MAX. NO. OF MATRIX SOLUTIONS PER TIME STEP: 2 MIN.VELOCITY FOR Cf, XCFMJN = 1.00000E-03 COURANT L. GAS COMP. CLCMJN = 1.00000E-01 COURANT LIMIT, ATMS, CLMAJN = 5.00000E-01 COURANT LIMIT, POOL, CLMPJN = 5.00000E-01 COURANT L. ENERGY S. CLCEJN = 1.00000E-01COURANT L. PUMPS/CM. CLCPJN = 5.00000E-01 VELOCITY LIMIT MULT. CVCLJN = 5.00000E-01 VELOCITY LIMIT VVCLJN = 1.00000E+01 GAS COMPOSITION CALCULATION : EXPLICIT \_\_\_\_\_ =JN= JN REFERENCE DATA FOR 2 CONTROL VOLUMES \_\_\_\_\_ =JN= Connect. of: CV-001 Example\_problem,\_volume\_1\_ JN-001 Example\_problem, Junction\_1\_(CV-001\_->\_CV-002)\_\_\_ leads to CV-002 Example\_problem,\_volume\_2\_ =JN= Connect. of: CV-002 Example problem, volume 2 JN-001 Example\_problem, Junction\_1\_(CV-001\_->\_CV-002)\_\_ leads from CV-001 Example\_problem,\_volume\_1\_ =JN= MAXIMUM DSP DATA FOR 2 CONTROL VOLUMES CV-001 : DSPmax = 9.28468E-01 , SET BY JN-001 CV-002 : DSPmax = 9.28468E-01 , SET BY JN-001 \_\_\_\_\_ =JN= JUNCTION INTERNAL NUMBERING SCHEME \_\_\_\_\_ Int. Ref. No. No. \_\_\_\_ \_\_\_ 1 JN-001 \_\_\_\_\_ =JN= END OF JUNCTION DATA

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### An example of the transient printout for a Junction is shown below.

=JN=	====JN	-001==== Ex	ample_problem,_	_Junction_1_(CV-(	)01>_CV-002)
=JN=	JN-001,	CONNECTION DAT	A : CV-001 -	> CV-002	
=JN=	JN-001,	COMPONENT DATA	AT TIME : 5.1	L0000E+00 (s)	
Quant	ity	Units Atms	-Gas Atms-I	Drop Pool-Liq	Pool-Bub
Veloc Mass Area, Tempe Densi Entha Cv Cp	ity, flow, rature, ty, lpy,	m/s 7.134 kg/s 5.504 m2 4.983 K 3.797 kg/m3 1.548 J/kg 4.190 J/kg 7.308 J/kg 1.024	55E-01 7.13455 93E-01 5.9182 39E-01 8.50670 41E+02 3.47634 32E+00 9.75140 62E+05 3.11940 38E+02 4.18774 77E+03 4.19014	5E-01 2.49976E-0 7E-02 1.24306E-0 9E-05 5.01576E-0 1E+02 3.15024E+0 9.91420E+0 9.91420E+0 1.75510E+0 1.75510E+0 1.7785E+0 1.17785E+0 1.18204E+0	04 0.00000E+00 01 0.00000E+00 02 0.00000E+00 02 0.00000E+00 05 0.00000E+00 03 0.00000E+00 03 0.00000E+00
=JN=	JN-001,	ATMOSPHERE AND	BUBBLE GAS CON	IPOSITION AT TIME	E : 5.10000E+00 (s)
GA No. 3 4 5	S Id. H2O N2 O2	ATMOSPHER MASS FRAC. 8.97921E-03 8.73394E-01 1.17627E-01	E GAS VOL. FRAC. 1.38889E-02 8.82148E-01 1.03963E-01	POOL BUBBLE           MASS FRAC.         V           0.00000E+00         0           0.00000E+00         0	GAS 70L. FRAC. 00000E+00 00000E+00 00000E+00
=JN=	JN-001,	OVERALL DATA A	T TIME : 5.100	000E+00 (s)	
Gas Liqui Total	Area, : 4.983 d: 5.016 : 1.000	(m2) Flow,(k 39E-01 5.50493 61E-01 1.83489 00E+00 7.33981	g/s) Enth.(J/} E-01 4.19062E+ E-01 2.19514E+ E-01 3.69177E+	kg) Velocity (m, +05 7.13455E-01 +05 3.70915E-04 +05	(s)
Atms Pool	P-up : 1.745 : 1.773	, (Pa) P-down, 57E+05 1.74554 14E+05 1.77313	(Pa) dP, (Pa E+05 3.85425E+ E+05 1.36456E+	a) Reynolds No. 5.84932E+04 600 4.43942E+02	Friction F. 2.02134E-02 1.44163E-01
Pool Cp/Cv Densi	level, for gas, ty of gas,	(m) : 5. (-) : 1. (kg/m3) : 1.	00178E+00 40219E+00 54832E+00		
=JN=	JN-001,	OVERALL GAS CO	MPOSITION AT TI	IME : 5.10000E+0	00 (s)
No. 3 4 5	Id. H2O N2 O2	MASS FRACTION 8.97921E-03 8.73394E-01 1.17627E-01			
=JN=	JN-001,	VALVE DATA AT	TIME : 5.10000	)E+00 (s)	
TF/CF 006	A(full) (m2) 1 00000E+	A(actual) (m2)	Frac.open (-)	K-for (-)	K-rev (-) 1 00000E+00

The printout consists of the following blocks.

The first block contains printout of <u>component data</u>. Current values are printed in four columns, for the four components that may share the same flow path: atmosphere (gas), droplets, pool (liquid), and bubbles.

The second block contains printout of the <u>atmosphere and bubble gas composition</u>, including mass fractions and volumetric fractions.

The third block contains the <u>overall data</u>. The overall data output consists of three parts. The first part gives flow area, mass flow and enthalpy, for the gas, liquid and the total flow. The overall values of the areas and flows are defined as the sums of the individual component data. For example, the overall gas flow,  $W_{gas}$ , is equal to the sum of the atmosphere flow,  $W_{atms}$  and the bubble flow,  $W_{bubb}$ :

$$W_{gas} = W_{atms} + W_{bubb}$$

The overall enthalpies are defined as the averages of the component values, weighted by the component mass flows. For example, the overall gas enthalpy,  $h_{gas}$ , is equal to:

$$h_{gas} = \frac{W_{atms}h_{atms} + W_{bubb}h_{bubb}}{W_{atms} + W_{bubb}}$$

where  $h_{atms}$  and  $h_{bubb}$  are the enthalpies of the atmosphere and the bubbles respectively.

The second part gives pressures upstream and downstream the Junction, pressure differences, Reynolds numbers, and friction factors, for both atmosphere flow and pool flow. Pressure differences are calculated by the program always for both atmosphere and pool, even if the flow of one of those components is zero. These values are needed in case a counter-current flow should occur.

The third part of this block gives the pool level in the Junction, the ratio of specific heats,  $(c_p/c_v)_{gas}$ , for gas, as well as the gas density,  $\rho_{gas}$ . Those values are calculated as the averages of the component values, weighted by the absolute values of the component flows, as shown below.

Ratio of specific heats:

$$\left(\frac{c_p}{c_v}\right)_{gas} = \frac{|W_{atms}|c_{p,atms} + |W_{bubb}|c_{p,bubb}}{|W_{atms}|c_{v,atms} + |W_{bubb}|c_{v,bubb}}$$

 $c_{p, atms}$  specific heat at constant pressure for the atmosphere gas,  $c_{v, atms}$  specific heat at constant volume for the atmosphere gas,  $c_{p, bubb}$  specific heat at constant pressure for the bubble gas,  $c_{v, bubb}$  specific heat at constant volume for the bubble gas.

Gas density:

$$\rho_{gas} = \frac{\left|W_{atms}\right|\rho_{atms} + \left|W_{bubb}\right|\rho_{bubb}}{\left|W_{atms}\right| + \left|W_{bubb}\right|}$$

 $\begin{array}{ll} \rho_{atms} & \text{density of atmosphere,} \\ \rho_{bubb} & \text{density of bubbles.} \end{array}$ 

The values of  $(c_p/c_v)_{gas}$  and  $\rho_{gas}$  are used by the program for the critical flow calculations.

The fourth block contains overall gas composition (mass fractions) defined as:

$$c_{i,gas} = \frac{\left|W_{atms}\right|c_{i,atms} + \left|W_{bubb}\right|c_{i,bubb}}{\sum\left(\left|W_{atms}\right|c_{i,atms} + \left|W_{bubb}\right|c_{i,bubb}\right)}$$

where:  $c_{i, atms}$  - concentration (mass fraction) of the gas No. i, in the atmosphere,  $c_{i, bubb}$  - concentration of the gas No. i, in the bubbles.

The summation is performed over all gases.

The fifth block contains <u>valve data</u>: the total open area and open fraction, as well as the actual friction coefficient (which depends on the open area), are given. This block is printed only if the valve option is used for a given Junction.

If the flow is critical then an informational message is printed at the bottom of the printout for the given Junction.

#### 3.1.4 1-D Solid Heat Conductor Output

The 1-D Solid Heat Conductor outputs may be easily found in the output file by searching for the string: =SC=. The first SC printout brings the input data printout. An example of the input printout for a 1-D Solid Heat Conductor is shown below. The printout mainly reflects the data entered in the input file and is quite self-explanatory.

```
=SC= ======SC-001====== Rectangular, fins on left side, spines on right
       SC GROUP NUMBER :
                                 1
       GEOMETRY TYPE : RECTANGULAR
CONDUCTOR SIZE : 1.00000E+00
       CONDUCTOR SIZE : 1.00000E+00
LEFT COORDINATE : 0.00000E+00
       THICKNESS (m) : 2.00000E-02
ELEVATION (m) : 5.00000E+00
VERTICAL ORIENT.: VERTICAL
       POWER SOURCE : 0.00000E+00
NO.OF CONDUCTORS: 1.00000E+00
INITIAL TEMP. : INPUT VALUES
TRANSIENT TEMP. : CONDUCTION EQUATION
SOLUTION SCHEME : TEMPERATURE NODES AT CELL CENTERS (NIMISC = 1)
          WIDTH
                         VOLUME
                                            MASS
                                                         MATERIAL
                         [m3]
CELL
           [m]
                                           [kg]
                                                          NUMBER
  1 1.0000E-03 1.2000E-05 5.7600E-02
2 2.0000E-03 2.40000E-05 1.15200E-01
                                                           MP-001
                                                          MP-001
  3 2.00000E-03 2.40000E-05 1.15200E-01
4 2.00000E-03 2.40000E-05 1.15200E-01
                                                          MP-001
                                                           MP-001
  5 1.00000E-03 1.20000E-05 5.76000E-02 MP-001
      REL.POWER
                           POWER
CELL
       DENSITY
                        FRACTION
  1 0.00000E+00 0.00000E+00
  2 0.00000E+00 0.00000E+00
  3 0.00000E+00 0.00000E+00
  4 0.00000E+00 0.00000E+00
  5 0.00000E+00 0.00000E+00
       NODE POS. TEMPERATURE
NODE
           [m]
                            [K]
  1 0.00000E+00 3.00000E+02
  2 2.00000E-03 3.00000E+02
  3 4.00000E-03 3.00000E+02
```

4 6.00000E-03 3.00000E+02 5 8.00000E-03 3.00000E+02 TOTAL THICK. OF SC, [m] : 8.00000E-03 TOTAL VOLUME OF SC, [m3]: 9.60000E-05 TOTAL INITIAL MASS, [kg]: 4.60800E-01 BOUNDARY CONDITIONS RIGHT LEFT \_ \_ \_ \_ \_ \_ \_ -----Heat transfer area, m2 : 1.20000E-02 1.20000E-02 

 Area per single SC, m2:
 1.20000E-02
 1.20000E-02

 Height of surface, m:
 1.09545E-01
 1.09545E-01

 Elevation of center, m:
 0.00000E+00
 0.00000E+00

 Lowest point elev. m:
 -5.47723E-02
 -5.47723E-02

 Highest point elev. m:
 5.47723E-02
 5.47723E-02

 Control Volume No. CV-001 None : Tabular Heat Transfer C.: Tabular Temperature Non-convective Heat Flux: TF-001 TF-003 TF-002 None None None Natural conv. config. : VERTICAL WALL VERTICAL WALL Natural conv. dim., m : 1.09545E-01 2.00000E-02 Forced conv. config. : INTERNAL INTERNAL Forced conv. dim., m : 1.09545E-01 1.20000E-02 INTERNAL ACTIVE ACT CHEN CHEN CHEN CHEN 1.30000E-02 Boiling model:ACTIVEACTIVENucl. boiling model:CHENCHENNucl. boiling, Csf:1.30000E-021.30000E-02CHF model:ZUBER-U.A.S.ZUBER-U.A.S.Film boiling config.:VERTICAL WALLVERTICAL WALLFilm boiling dim.,m:1.09545E-012.00000E-02 Condensation config. : VERTICAL VERTICAL Condensation dim., m : 1.09545E-01 2.00000E-02 Noncondensables model : MODIFIED OGG MODIFIED OGG Condensate film drain. : POOL OR RAIN POOL OR RAIN Edge elev./Edge SC no. : 0.0000E+00 -1.00000E+00 CV horizontal flow is:PARALLELPARALLELContact angledeg:9.6000E+019.60000E+01Rod bundle multiplier:0.0000E+000.00000E+00Oxidation model:NoneNone PARALLET RIGHT SIDE FIN/SPINE DATA 
 Type
 : FINS

 Half thickness,
 m : 1.00000E-03

 Length,
 m : 2.00000E-02
 FINS Distance (effective) m : 1.20000E-02 Thermal conduct. W/m/K : MP-001 Area increase - : 4.33333E+00 Volume increase - : 4.3333E+00 =SC= SC-001, BOUNDARY FLUID TEMPERATURE USED FOR POOL: T(fluid) = T(CV, pool)=SC= SC-001, VELOCITY MULTIPLIER: 1.00000E+00 =SC= SC-001, Maximum fraction of surface area covered by pool to allow simultaneous heat transfer to pool and atmosphere: - LEFT SURFACE, PMXLSC: 0.00000E+00 - RIGHT SURFACE, PMXRSC: 0.00000E+00 =SC= SC-001, FAILURE: NOT CALCULATED =SC= SC-001, AXIAL HEAT TRANSFER: NOT CALCULATED

At the bottom of the 1-D Solid Conductor data printout the data valid for all heat conductors are printed. Next the SC reference data is printed for all Control Volumes, which are used as boundary conditions for SC. Finally, the internal numbering scheme is printed.

=SC= ALL 1-D SOLID HEAT CONDUCTORS \_\_\_\_\_ CHF AND MINIMUM FILM BOILING PARAMETERS: - MINIMUM VALUE OF T(CHF)-T(MFB): TFMNSC = 5.00000E+00 - MAXIMUM VALUE OF T(CHF)-T(MFB): TFMXSC = 1.00000E+03 - MAXIMUM VALUE OF SLIP FOR CHF : SMAXSC = 1.00000E+02 - MULTIPLIER FOR COUNTER-FLOW TA: CMN1SC = 1.00000E-02 : CMN2SC = 1.00000E+00- MULTIPLIER FOR CO-FLOW TA =SC= SC REFERENCE DATA FOR 2 CONTROL VOLUMES =SC= SC surfaces in CV-001 Room SC-001 right side 1-D finned wall, Aluminum SC-002 right side 1-D finned wall, Stainless Steel SC-003 right side 1-D NON-finned wall, Aluminum =SC= ALL 1-D SOLID HEAT CONDUCTORS \_\_\_\_\_ SC-S IN SEQUENTIAL ORDER LEFT AREA RIGHT AREA [m2] [m2] SC-001 1-D finned wall, Aluminum 1.2000E-02 1.2000E-02 SC-002 1-D finned wall, Stainless Steel 1.2000E-02 1.2000E-02 SC-003 1-D NON-finned wall, Aluminum 1.2000E-02 1.2000E-02 SC-S SORTED BY THE RIGHT SURFACE SIZE : LEFT AREA RIGHT AREA [m2] [m2] SC-003 1-D NON-finned wall, Aluminum 1.2000E-02 1.2000E-02 1.2000E-02 1.2000E-02 SC-002 1-D finned wall, Stainless Steel SC-001 1-D finned wall, Aluminum 1.2000E-02 1.2000E-02 LEFT RIGHT TOTAL TOTAL AREA, SURFACES CONNCTED TO CV : 0.0000E+00 3.6000E-02 3.6000E-02 TOTAL AREA, SURFACES NOT CONNCTED TO CV: 3.6000E-02 0.0000E+00 3.6000E-02 =SC= SOLID HEAT CONDUCTORS OF GROUP : 1 \_\_\_\_\_ SC-S IN SEQUENTIAL ORDER LEFT AREA RIGHT AREA [m2] [m2] SC-001 1-D finned wall, Aluminum 1.2000E-02 1.2000E-02 SC-002 1-D finned wall, Stainless Steel 1.2000E-02 1.2000E-02 1.2000E-02 1.2000E-02 SC-003 1-D NON-finned wall, Aluminum LEFT RIGHT TOTAL 
 TOTAL AREA, SURFACES CONNCTED TO CV
 0.0000E+00
 3.6000E-02
 3.6000E-02

 TOTAL AREA, SURFACES NOT CONNCTED TO CV:
 3.6000E-02
 0.0000E+00
 3.6000E-02
 =SC= TOTAL VOLUME AND MASS TOTAL VOLUME = 2.8800E-04 [m3] TOTAL MASS = 1.6704E+00 [kg] V [%] No. Material V [m3] 1.9200E-04 66.7 2 9.6000E-05 33.3 No. Material M [kq] M [%] 9.2160E-01 1 55.2 \_\_\_\_\_ 7.4880E-01 2 44.8 =SC= TOTAL VOLUME AND MASS FOR SC GROUP : 1 \_\_\_\_\_

	TOTAL VOLUME = 2.8800E-04 [m3] TOTAL MASS = 1.6704E+00 [kg]		
No. 1 2	Material	V [m3] 1.9200E-04 9.6000E-05	V [%] 66.7 33.3
No. 1 2	Material	M [kg] 9.2160E-01 7.4880E-01	M [%] 55.2 44.8
==========	1-D SOLID HEAT CONDUCTOR INTERNAL NUMBERING SCHEME		
	Int. Ref. No. No.  1 SC-001		
====== =SC=	END OF 1-D SOLID HEAT CONDUCTOR DATA		

An example of the transient printout for a Solid Conductor is shown below.

=SC=		====S(	2-001======	Rectangular,_	fins_on_left_	side,_spines_	on_right_
=SC= Node 1 2	SC-I Po	001, ositio 0.0000 2.0000	NODE TEMPERA on, (m) T, 00E+00 3.88 00E-02 3.78	ATURES AT TIME , (K) 3156E+02 3728E+02	: 5.00000E+	01 (s)	
=SC=	SC-0 Vol	001,	BOUNDARY CON H.T.Area Fractions	NDITIONS AT TI Twall (K)	ME : 5.00000 Tfluid (K)	E+01 (s) h (W/m2/K)	H.T. Mode
Left :	001	atms pool repr	1.00000E+00 0.00000E+00 1.00000E+00	3.88156E+02 3.88156E+02 3.88156E+02	3.89768E+02 0.00000E+00 3.89768E+02	1.16412E+04 0.00000E+00 1.16412E+04	CONDEN
Right:	002	atms pool repr	4.99983E-01 5.00017E-01 1.00000E+00	3.78728E+02 3.78728E+02 3.78728E+02	3.70262E+02 3.70005E+02 3.70008E+02	5.70140E+01 4.27029E+03 2.16372E+03	FC-LAM NUC-B
=SC=	SC-	001,	BOUNDARY HEA q(conv) (W/m2)	AT FLUXES AT T Q(conv) (W)	IME : 5.0000 q(rad) (W/m2)	0E+01 (s) Q(rad) (W)	
Left :	001	atms pool repr	-1.87579E+04 0.00000E+00 -1.87579E+04	-1.87579E+04 0.00000E+00 -1.87579E+04	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00	
Right:	002	atms pool repr	4.82693E+02 3.72528E+04 1.88684E+04	2.41338E+02 1.86270E+04 1.88684E+04	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00	
=SC=	SC-0 Vol	001,	FLUID VELOC v-atms (m/s)	ITIES AT TIME v-pool (m/s)	: 5.00000E+0 v-bubb (m/s)	1 (s)	
Left : Right:	001 002		1.12097E-04 0.00000E+00	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00		
=SC=	SC-0 Gas No.	001, Gas Id.	FLUID COMPOS LEFT MASS FRACTION	SITION AT TIME SURFACE VOLUME FRACTION	: 5.00000E+ RIGHT MASS FRACTION	01 (s) SURFACE VOLUME FRACTION	

\_\_\_\_\_

atms 3 H2O 8.50851E-01 8.99092E-01 8.61549E-01 9.07416E-01 4 N2 1.16011E-01 8.07261E-02 1.07689E-01 7.40670E-02 5 O2 3.31379E-02 2.01815E-02 3.07617E-02 1.85168E-02 atms atms \_\_\_\_\_ atms droplets 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool bubbles 1.00000E+00 1.00000E+00 0.00000E+00 8.00380E-05 =SC= SC-001, CONDENSATION PARAMETERS AT TIME : 5.00000E+01 (s) Mass flux Liq.enth. Vap.enth. Cond.film f(NC) f(SH) (Ŵ/m2) (Ŵ/m2) (m) Vo1 (kq/m2/s) (-) (-) \_\_\_\_\_ \_\_\_\_\_ \_\_\_\_\_ \_\_\_ Left: 1 8.4675E-03 4.1159E+03 2.2874E+04 2.6777E-05 2.897E-01 1.000E+00 =SC= SC-001, BOILING PARAMETERS AT TIME : 5.00000E+01 (s) Mass fluxLiq.enth.Vap.enth.TsatqCHF(kg/m2/s)(W/m2)(W/m2)(K)(W/m2) Vol \_\_\_\_ Right: 2 1.2673E-02 5.1427E+03 3.3915E+04 3.7343E+02 1.4619E+06 =SC= SC-001, LEFT SURFACE, FIN/SPINE DATA AT TIME : 5.00000E+01 (s) ATMOSPHERE: Fin/Spine Efficiency (-) : Eff = 3.62893E-02 Fin/Spine Enhancement (-) : E = 1.53304E+00Heat/Mass Transfer TRUE EFFECTIVE Heat tr. coeff. (W/m2/K) : h = 7.59350E+03 1.16412E+04 Heat flux (W/m2): q = -1.22357E+04 -1.87579E+04 Mass tr. flux (kg/m2/s): m = 5.52330E-03 8.46747E-03 Liquid enth. flux (W/m2): Hliq= 2.68477E+03 4.11588E+03 Gas enth. flux (W/m2): Hgas= 1.49205E+04 2.28738E+04 =SC= SC-001, RIGHT SURFACE, FIN/SPINE DATA AT TIME : 5.00000E+01 (s) ATMOSPHERE: Fin/Spine Efficiency (-) : Eff = 6.43304E-01 Fin/Spine Enhancement (-) : E = 6.13217E+00TRUE EFFECTIVE Heat/Mass Transfer Heat tr. coeff. (W/m2/K) : h = 9.29753E+00 5.70140E+01 Heat flux (W/m2) : q = 7.87148E+01 4.82693E+02 POOL: Fin/Spine Efficiency (-) : Eff = 3.85625E-02 Fin/Spine Enhancement (-) : E = 1.27004E+00Heat/Mass Transfer TRUE EFFECTIVE Heat tr. coeff. (W/m2/K): h = 3.36232E+03 4.27029E+03 Heat flux (W/m2): q = 2.93319E+04 3.72528E+04 Mass tr. flux (kg/m2/s): m = 9.97843E-03 1.26730E-02 Liquid enth. flux (W/m2) : Hliq= 4.04924E+03 5.14270E+03 Gas enth. flux (W/m2) : Hgas= 2.67038E+04 3.39149E+04

The first block contains the printout of the <u>node temperatures</u> for all nodes of the given Conductor. The first node is located on the left surface of the Conductor. The last node is located on the right surface of the conductor. The location of each node is printed in the input diagnostics printout.

The second block contains <u>boundary conditions</u> for the left and right surfaces. Three values are printed: for atmosphere ("atms"), pool ("pool"), and representative ("repr"). The representative values are used as boundary conditions for the Solid Conductor transient conduction equation. The heat transfer mode identifiers, which may be printed in this block are: NC-LAM - natural convection, laminar flow, NC-TUR - natural convection, turbulent flow, FC-LAM - forced convection, laminar flow, FC-TRN - forced convection, transition flow, FC-TUR - forced convection, turbulent flow, NUC-B - nucleate boiling, TRAN-B - transition boiling, FILM-B - film boiling, CONDEN - condensation, INSUL - insulation, TAB-F. - heat transfer coefficient specified by a Tabular Function, CON-F. - heat transfer coefficient specified by a Control Function.

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It is important to note that the heat transfer coefficient printed in this block is always related to the heat flux by the following equation:

$$q = h \left( T_{wall} - T_{fluid} \right)$$

Which means that the heat transfer coefficient is equal to:

$$h = \frac{|q|}{\left|T_{wall} - T_{fluid}\right|}$$

In case of condensation the usual definition of the condensation heat transfer coefficient is:

$$h = \frac{|q|}{\Delta T_{sat}} = \frac{|q|}{(T_{sat} - T_{wall})}$$

Therefore the condensation heat transfer coefficient can be obtained as follows:

$$h_{cond} = h \frac{T_{fluid} - T_{wall}}{T_{sat} - T_{wall}}$$

For pure steam or nearly pure steam mixtures  $h \approx h_{cond}$ . However if the gas contains a large amount of noncondensables, the gas temperature  $(T_{fluid})$  may be significantly different from saturation temperature  $(T_{sat})$ . In such cases to obtain the true value of the condensation heat transfer coefficient the above formula must be used. For example, let's try to obtain the condensation heat transfer coefficient for SC-001 in the example shown above. The value of h is  $7.59350 \times 10^3 \text{ W/m}^2/\text{K}$ . (Note that if fins or spines are present then the "true" heat transfer coefficient must be used, and not the "effective" h.t.c. - see description of fin/spine data below). The fluid temperature is  $3.89768 \times 10^2 \text{ K}$ . The wall surface temperature is  $3.88156 \times 10^2 \text{ K}$ . The saturation temperature is found in the CV output as the "Sat. temp." for the "atms-gas" component. In the present example the saturation temperature is very close to the fluid temperature:  $3.89811 \times 10^{+2} \text{ K}$ . Therefore:

$$h_{cond} = 7.59350 \times 10^{+3} \times (3.89768 \times 10^{+2} - 3.88156 \times 10^{+2}) / (3.89811 \times 10^{+2} - 3.88156 \times 10^{+2}) = 7.47879 \times 10^{+3} \text{ W/m}^2/\text{K}.$$

The third block contains convective and radiative <u>boundary heat fluxes</u> for the left and right surfaces. Convective heat fluxes are given again for the atmosphere, pool, and as the representative values. In case of radiative heat fluxes there is only atmosphere flux; the value of the representative flux is always equal to the atmosphere flux. Note that the radiative fluxes are non-zero not only in case when the thermal radiation model is active, but also in case when a user prescribed heat flux, defined by a Tabular or a Control Function, is used (input parameters IQRLSC, IQRRSC, sections 2.3.11, 2.3.12).

The fourth block contains <u>fluid velocities</u> at the left and right surfaces. Both atmosphere and pool velocities are given.

The fifth block contains <u>fluid composition</u> at the left and right surfaces. First the volume and mass fractions of the atmosphere gases are printed. The values are appropriate for the center point of this part of the surface, which is above the pool surface.

Next the volume and mass fractions of the droplets and bubbles are printed. The droplet fractions are appropriate for the center point of this part of the surface, which is above the pool surface. The bubble fractions are appropriate for the center point of this part of the surface, which is below the pool surface.

The next block contains <u>condensation parameters</u>, including film thickness, non-condensable degradation factor, condensation mass flux, and the enthalpy fluxes associated with the appearing water and the disappearing steam. This block is printed only if condensation occurs on either of the Conductor surfaces.

The next block contains <u>boiling parameters</u>, including boiling mass flux, and the enthalpy fluxes associated with the disappearing water and the appearing steam. This block is printed only if boiling occurs on either of the Conductor surfaces.

The next blocks contain <u>extended surface data</u>. Extended surface (fin/spine) data is printed only if fins/spines are present at the surface. If the surface is exposed to a single environment (i.e. either atmosphere or pool) then this printout consists of only a single block - left surface in the example case. If, on the other hand, the surface is partly covered by pool (as it is on the right surface), then two blocks are printed. The first block gives data for the part of the SC surface above the pool. The second block gives the data for the part below the pool surface.

The printout gives the following information:

- Fin/spine efficiency, defined as the ratio of heat transferred over the total fin/spine area to that which would be transferred if the fins/spines were isothermal (see [14], section 3.B.2.b, page 3-115). The efficiency is always smaller than one and it is close to 1.0 if the heat transfer coefficient is small.
- Fin/spine enhancement, defined as the ratio of average heat transferred through the wall surface (at the base of fins/spines) to that which would be transferred through the same surface if the were no fins/spines. Thus the enhancement is calculated as:

$$E = \frac{A_{base, no fin} + A_{fin} \eta}{A_{base}} = \left(\frac{A_{base, no fin}}{A_{base}}\right) + \left(\frac{A_{fin}}{A_{base, fin}}\right) \cdot \left(\frac{A_{base, fin}}{A_{base}}\right) \cdot \eta$$

where:

 $A_{base}$ surface area at the fin/spine base (equal to the sum:<br/> $A_{base, no fin} + A_{base, fin}$ ), (m²). $A_{fin}$ area of heat/mass transfer of the fin/spine, (m²). $\eta$ efficiency of fin, (-). $A_{base, no fin}$ this part of the surface area at the fin/spine base, which is not<br/>covered by fin/spine, (m²), (Figure 3-1). $A_{base, fin}$ this part of the surface area at the fin/spine base, which is covered<br/>by fin/spine, (m²), (Figure 3-1).



Figure 3-1 Fins and spines

• True and effective values of heat transfer coefficients, heat and mass fluxes. The true values are those calculated by the Heat Transfer Package, using appropriate correlation (convection, boiling, condensation). The effective values are obtained by multiplying the true values by the fin/spine enhancement factor, E. Note that the effective values are those, which are used as Solid Conductor boundary conditions by the 1-D Solid Conductor Package. Thus for example the values of heat transfer coefficient, printed in the second (Boundary Conditions) block are the same as the effective heat transfer coefficients printed in the fin/spine output.

At the bottom of the SC output the summed quantities (data summed for all 1-D Solid Conductors) are printed. An example printout is shown below.

\_\_\_\_\_ =SC= DATA SUMMED FOR ALL 1-D SOLID CONDUCTORS AT TIME : 0.00000E+00 (s) The heat fluxes and integrated heat fluxes printed below are summed over those surfaces which transfer heat to normal Control Volumes (those CVs for which conditions are not held constant). Integrated Heat Flux Heat Flux W J 0.00000E+00 0.00000E+00 Convective : -5.40977E+04 Radiative : 0.00000E+00 : -5.40977E+04 Total 0.00000E+00

This output gives heat fluxes (W), and integrated heat fluxes (J), summed over all 1-D Solid Conductors. Three values are given:

• Convective heat fluxes.

- Radiative heat fluxes.
- Total (convective + radiative) heat fluxes. Note that the total integrated heat flux (J) should be equal to the value of the total energy "Current Initial M&E sources", printed at the bottom of the CV output.

#### 3.1.5 2-D Solid Heat Conductor Output

The 2-D Solid Heat Conductor outputs may be easily found in the output file by searching for the string: =**TC**=. The first TC printout brings the input data printout. An example of the input printout for a 2-D Solid Heat Conductor is shown below. The example consists of the structure shown in Figure 3-2.

The printout below mainly reflects the data entered in the input file and is quite self-explanatory.



Figure 3-2 Example of a 2-D Solid Heat Conductor

```
=TC= ======TC-100====== Steady_state_with_heat_sourc_-_rectangular,_2-D__
GEOMETRY TYPE : RECTANGULAR
CONDUCTOR SIZE : 1.00000E+00
LEFT COORDINATE : 0.00000E+00
ELEVATION (m) : 0.00000E+00
VERTICAL ORIENT.: VERTICAL
POWER SOURCE : 1.00000E+03
NO.OF CONDUCTORS: 1.0000E+00
INITIAL TEMP. : INPUT VALUES
TRANSIENT TEMP. : CONDUCTION EQUATION
=TC= TC-100, X, Y MESH CELL SIZES OF THE 2-D SOLID HEAT CONDUCTOR
X-COORDINATE : 3 MESH CELLS
Y-COORDINATE : 3 MESH CELLS
```

X-COORDINATE CELL DATA Cell No. Cell half width Cell center 
 (m)
 X-coord.(m)

 1.00000E-02
 1.00000E-02

 1.00000E-02
 3.00000E-02

 1.00000E-02
 5.00000E-02
 (K) 1 2 3 Y-COORDINATE CELL DATA Cell No. Cell half width Cell center Y-coord.(m) 0.00000E+00 2.00000E-02 4.00000E-02 (L) (m) 1.00000E-02 1 1.00000E-02 2 1.00000E-02 3 =TC= TC-100, CELL TYPE MAP OF THE 2-D SOLID HEAT CONDUCTOR \K: 1 2 3 L\-----1 |XX|XX|XX| X X XXX \_\_\_\_\_ 2 |X | X|XX| |XX|X | X| 3 |XX|X | X| | XX | XX | XX | MATERIAL MAP OF THE 2-D SOLID HEAT CONDUCTOR =TC= TC-100. \K: 1 2 3 L \ --- ---1 001 001 001 2 001 001 001 3 001 001 001 =TC= TC-100, TOTAL NUMBER OF ACTIVE CELLS IS: 9 =TC= TC-100, CELL NUMBERING MAP \K: 1 2 3 L \ ---- ----1 001 002 003 2 004 005 006 3 007 008 009 =TC= TC-100, TOTAL NUMBER OF BOUNDARY CELLS IS: 7 =TC= TC-100, BOUNDARY CELL NUMBERING MAP \ K: 1 2 3 L \ ---- ----1 001 002 000 2 003 004 005 3 000 006 007 =TC= TC-100, INVERSE CELL NUMBERING MAP I = CONSECUTIVE CELL NO. K = X COORDINATE CELL NO. L = Y-COORDINATE CELL NO. (I K L) 002 02 01 007 01 03 (I K L) (I K L) 003 03 01 004 01 02 008 02 03 009 03 03 (I K L) (I K L) 005 02 02 001 01 01 006 03 02 =TC= TC-100, CELL DATA TC-100, Cell No.: 1, K = 1, L = 1 \_\_\_\_\_ Volume of cell, m3 : 3.00000E-04 Cell center X-coord. m : 1.00000E-02 Cell center Y-coord. m : 0.00000E+00

Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation, Control Volume No. Tabular Heat Transfe Tabular Temperature	- K 1 m2 m m m r C	: : : : : : : : : : : : : : : : : : : :	1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -1.00000E+00 None TF-001 TF-001
Non-conv. Heat Flux		:	None
TC-100, Cell No.:	2,	к	= 2, L = 1
Volume of cell,	mЗ	:	3.00000E-04
Cell center X-coord.	m	:	3.00000E-02
Cell center Y-coord.	m	:	0.00000E+00
Power fraction,	-	:	1.0/143E-01
POINDARY CELL No .	к 2	:	3.00000E+02
Heat transfer area	∠ m2		2 000000-02
Height of surface.	m	:	1 00000E 02
Bottom elevation,	m		-1.00000E-02
Top elevation,	m	:	0.00000E+00
Control Volume No.		:	None
Tabular Heat Transfe	r C	. :	TF-001
Tabular Temperature		:	TF-002
Non-conv. Heat Flux		:	None
TC-100, Cell No.:	з,	K	= 3, L = 1
Volume of cell	 m3		4 00000F-04
Cell center X-coord.	m	;	5.00000E-02
Cell center Y-coord.	m		0.00000E+00
Power fraction,	_	:	1.42857E-01
Input temperature	v		
input temperature,	17	:	3.00000E+02
Internal cell - no b	ound	: dau	3.00000E+02 ry conditions
Internal cell - no b	ound	: dai	3.00000E+02 ry conditions
TC-100, Cell No.:	ouno 4,	daı K	3.00000E+02 ry conditions = 1, L = 2
TC-100, Cell No.: Volume of cell,	ouno 4, 	: dai K 	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04
TC-100, Cell No.: Volume of cell, Cell center X-coord.	ouno 4, m3 m	: dai K 	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02
TC-100, Cell No.: 	ouno 4, m3 m m	: K 	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02
TC-100, Cell No.: 	0uno 4, m3 m m -	: K 	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01
TC-100, Cell No.: 	0 uno 4, m3 m m - K	dan K 	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02
TC-100, Cell No.: TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.:	ound 4, m3 m 	daı K : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02
TC-100, Cell No.: TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area,	0 uno 4, m3 m - K 3 m2	: dai K : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02
TC-100, Cell No.: TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation	0 uno 4, m3 m m - K 3 m2 m m	: dai K : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 2.00000E-02
TC-100, Cell No.: TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation.	0uno 4, m3 m m - K 3 m2 m m m m	: dai K : : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02
Input temperature, Internal cell - no b TC-100, Cell No.: 	4, m3 m  K 3 m2 m m m m	: da1 K : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K 3 m m m m m m m m m	E C C C C C C C C C C C C C C C C C C C	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K 3 m2 m m m r C	: da1 K : : : : : : : : : : : : : : : : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-002
Internal cell - no b TC-100, Cell No.: 	4,  m3 m m - K 3 m2 m m m m r C	E da 1 K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-002 None
Internal cell - no b TC-100, Cell No.: 	Mound 4, m3 m m K 3 m2 m m m r C 5,	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-002 None = 2, L = 2
Internal cell - no b TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation, Control Volume No. Tabular Heat Transfe Tabular Temperature Non-conv. Heat Flux TC-100, Cell No.:	4, m3 m m K 3 m2 m m m m r C	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-002 None = 2, L = 2
Internal cell - no b TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation, Control Volume No. Tabular Heat Transfe Tabular Temperature Non-conv. Heat Flux TC-100, Cell No.: Volume of cell,	4, m3 m - K 3 m2 m m m r C 5,  m3	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 2.00000E-02 1.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-002 None = 2, L = 2 2.00000E-04
Internal cell - no b TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation, Control Volume No. Tabular Heat Transfe Tabular Temperature Non-conv. Heat Flux TC-100, Cell No.: 	4, 	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02
Internal cell - no b TC-100, Cell No.: Volume of cell, Cell center X-coord. Cell center Y-coord. Power fraction, Input temperature, BOUNDARY CELL No.: Heat transfer area, Height of surface, Bottom elevation, Top elevation, Control Volume No. Tabular Heat Transfe Tabular Temperature Non-conv. Heat Flux TC-100, Cell No.: 	4,  m3 m m - K 3 m2 m m m r C 5,  m3 m m	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.0000E-02 2.00000E-02 -1.000
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K 3 m m m m m m m m m m m m m	K K ::::::::::::::::::::::::::::::::::	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 1.00000E-02 -2.00000E-02 -2.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 7.14286E-02 2.00000E+02
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K 3 m m m m m m m m m m m m m	K K K K K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -2.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.00000E-02 2.00000E-02 3.00000E-02 -1.00000E-02 -1.000E-02 -1.0000E-02 -1.000E-02 -1.00
Internal cell - no b TC-100, Cell No.: 	4, m3 m K 3 m K 3 m m K 3 m m K 3 m m K 3 m m K 3 m m K 3 m M M M K 3 m M M M M M M M M M M M M M	: dan K : : : : : : : : : : : : : : : : : : :	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 1.00000E-02 -2.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-02 2.00000E-02 3.00000E-02 2.00000E-02 3.00000E+02 2.00000E+02
Internal cell - no b TC-100, Cell No.: 	4, m3 m K3 m2 m m K3 m2 m m K3 M3 M3 M3 M3 M3 M3 M3 M M3 M3 M M3 M3 M3 M3 M M3 M3 M3 M3 M3 M3 M3 M3 M3	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.0000E+02 -2.00000E-02 0.0000E+00
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K3 m - K3 m - K3 m - K3 m - K4 m3 m - K4 m3 m - K3 m - K3 m - K3 m - K3 m - K3 - - - - - - - - - - - - -	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.0000E+02 -2.00000E-02 1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.00000E+00 0.00000E+00
Internal cell - no b TC-100, Cell No.: 	4, m3 m - K3 m - K3 m - K4 m - K4 m - K4 m - K4 m - - - - - - - - - - - - -	K K K K K K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.00000E+02 -2.00000E+00 0.00000E+00
Internal cell - no b TC-100, Cell No.: 	4, 	K K K K K K K K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.00000E+02 0.00000E+00 0.0000E+00 None
Internal cell - no b TC-100, Cell No.: 	4, 	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E-02 2.00000E-02 3.00000E+02 0.00000E+00 0.0000E+00 None TF-001
Internal cell - no b TC-100, Cell No.: 	4, m3 m K3 m2 m m m C 5,  m3 m m K 4 m m r C 5,  m3 m m r C m3 m r C m3 m r C m3 m r C m3 m r C m3 m r C m3 m r C m3 m r C m3 m r C m3 m r C C m3 m r C C m3 m r C C C C C C C C C C C C C	K	3.00000E+02 ry conditions = 1, L = 2 3.00000E-04 1.00000E-02 2.00000E-02 1.07143E-01 3.00000E+02 -2.00000E-02 -1.00000E-02 -1.00000E-02 -1.00000E-02 None TF-001 TF-002 None = 2, L = 2 2.00000E-04 3.00000E+02 3.00000E+00 0.00000E+00 None TF-001 TF-001 TF-002

TC-100,	Cell	No.	:	6,	K	=		3,	Ι	_	=	2
Volume of	f celi	 1.		 m3	•		3	00	200	00	 E	0.4
Cell cent	ter X-	-, -coo	rd.	m	÷		5	. 00	000	0	— Е-	02
Cell cent	ter Y-	-coo	rd.	m	:		2.	. 0 (	000	)0	— Е-	02
Power fra	actior	n,		-	:		1.	. 0	714	13	Е-	01
Input ter	nperat	ture	,	K	:		З.	. 00	000	0	E+	02
BOUNDARY	CELL	No.	:	5		-						
Heat tran	nsfer	are	a,	m2	:		2.	. 00	000	0	E-	02
Height of	f surf	face	,	m	:		1.	. 00	000	0	Е-	02
Bottom e	levat	ion,		m	:	-	-3.	. 0 (	000	)0	E-	02
Top el	levat	ion,		m	:	-	-2.	. 0 (	000	)0	E-	02
Control V	/olume	e No	•		:						Nc	ne
Tabular H	leat 1	Fran	sfe	er C.	. :				I	'F	-0	01
Tabular 1	lember	ratu	re		:				I	'F	-0	02
Non-conv.	. Heat	t Fl	ux		:						Nc	ne
TC-100,	Cell	No.	:	7,	K	=	1	,	Ι	_	=	3
												0.4
Coll cont	- cel.	L, - 200	rd	m	:		4.	00		) () ) ()	만- 도-	.02
Cell cent	or V-	-000	rd.	m	:		1.	00. 01		) () ) ()	с- г-	.02
Power fr:	ction	-000	IU.	-	:		1	. 00	285	57	E-	.02
Input ter	nperat	<i>1</i>		ĸ	:		3	00	200	ົ່າດ	二 王+	-02
Internal	cell	- n	, o r		Iai	~~~	с.	. o . . n .		- i	on	15
Incornar	COII		0 1	/0 u110		- 1	00	/110			011	
TC-100,	Cell	No.	:	8,	K	=	2	2,	I		=	3
Volume of	f cel'	۱.		m3	:		3.	. 00	00	0	E-	04
Cell cent	ter X-	-, -coo	rd.	m	:		3	. 00	000	0	- E-	02
Cell cent	ter Y-	-coo	rd.	m	:		4.	. 0 (	000	00	– E–	02
Power fra	action	n,		-	:		1.	. 01	714	13	Е-	01
Input ter	nperat	ture	,	K	:		З.	. 00	000	0	E+	02
BOUNDARY	CELL	No.	:	6		-						
Heat tran	nsfer	are	a,	m2	:		2.	. 00	000	0	E-	02
Height of	f surf	face	,	m	:		1.	. 00	000	0	E-	02
Bottom e	levat	ion,		m	:	-	-4.	.00	000	)0	Е-	02
Top el	levat	ion,		m	:	-	-3.	. 0 (	000	)0	E-	02
Control V	Volume	e No	•		:						Nc	ne
Tabular H	leat 1	Iran	sfe	er C.	. :				Г	'F	-0	01
Tabular 1	lemper	ratu	re		:				Г	'F	-0	02
Non-conv.	. Heat	t Fl	ux		:						Nc	ne
тс-100,	Cell	No.	:	9,	K	=	3	<sup>3</sup> ,	I		=	3
Volume of	f cell	l,		m3	:		3.	. 00	000	00	E-	04
Cell cent	ter X-	-coo	rd.	m	:		5.	. 00	000	0	Е-	02
Cell cent	cer Y-	-coo	rd.	m	:		4.	. 00	000	0	Е-	02
Power fra	actior	n,		-	:		1.	. 01	714	13	Е-	01
Input ter	nperat	ture	,	Κ	:		З.	. 00	000	0	E+	02
BOUNDARY	CELL	No.	:	7		-						
Heat tran	nsfer	are	a,	m2	:		2.	. 00	000	0	E-	02
Height of	E suri	face	,	m	:		1.	. 00	000	0	Е-	02
Bottom el	levati	ion,		m	:	-	-4.	. 0 (	000	)0	Е-	02
Top e	levat	ion,		m	:	-	-3.	. 0 (	000	)0	E-	02
Control V	Volume	e No	•		:						Nc	ne
Tabular H	leat ?	Iran	sfe	er C.	. :				Г	'F	-0	01
Tabular 1	lempe:	ratu	re		:				Г	'F	-0	02
Non-conv.	. Heat	t Fl	ux		:						Nc	ne

At the bottom of the 2-D Solid Conductor data printout, the data valid for all 2-D heat conductors is printed. Next the TC reference data is printed for all Control Volumes, which are used as boundary conditions for TC (not present in the current example because no CV were used). Finally, the internal numbering scheme is printed.

=TC= ALL 2-D SOLID HEAT CONDUCTORS ------

CHF AND MINIMUM FILM BOILING PARAMETERS: - MINIMUM VALUE OF T(CHF)-T(MFB): TFMNTC = 5.00000E+00 - MAXIMUM VALUE OF T(CHF)-T(MFB): TFMXTC = 1.00000E+03 - MAXIMUM VALUE OF SLIP FOR CHF : SMAXTC = 1.00000E+02 =TC= 2-D SOLID HEAT CONDUCTOR INTERNAL NUMBERING SCHEME Int. Ref. No. No. --- ------1 TC-100 =TC= END OF 2-D SOLID HEAT CONDUCTOR DATA

An example of the transient printout for a Solid Conductor is shown below. The output consists of the node temperature printout, followed by the printouts for all boundary cells. The printout for the boundary cells is very similar to the printout of left and right surface for 1-D heat conductors.

=TC= =====TC-100====== Steady state with heat sourc - rectangular, 2-D =TC= TC-100, NODE TEMPERATURES AT TIME : 1.00000E+03 (s)  $\setminus$  K: 1 2 3 L \ -----329. 340. 409. 1 340. 315. 340. 409. 340. 329. 2 3 =TC= TC-100, BOUNDARY CONDITIONS AT TIME : 1.00000E+03 (s) BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ \_\_\_\_\_ TC-100, Boundary Cell: IBC = 1, Cell: I = 1 (K,L) = (01,01) \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h H.T. Vol Fractions (K) (K) (W/m2/K) Mode 000 atms 0.00000E+00 3.29330E+02 0.00000E+00 0.00000E+00 pool 0.00000E+00 3.29330E+02 0.00000E+00 0.00000E+00 repr 1.00000E+00 3.29330E+02 3.00000E+02 2.00000E+02 TAB-F. Heat fluxes at the boundary surface  $\begin{array}{cc} q(conv) & Q(conv) & q(rad) & Q(rad) \\ (W/m2) & (W) & (W/m2) & (W) \end{array}$ Vol (W) 000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 5.86603E+03 1.17321E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface Vol comp (~ ' (m/s) ---- -----000 atms 0.00000E+00 000 pool 0.00000E+00 000 bubb 0.00000E+00 Gas composition at the boundary surface Gas Gas MASS VOLUME No. Id. FRACTION FRACTION ---- -- --- ------ -------

\_\_\_\_\_ \_\_\_\_\_ atms droplets 0.00000E+00 0.00000E+00 pool bubbles 0.00000E+00 0.00000E+00 BOUNDARY DATA AT TIME : 1.00000E+03 (s) TC-100, Boundary Cell: IBC = 2, Cell: I = 2 (K,L) = (02,01) \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h Fractions (K) (K) (W/m2/K) H.T. Vol Mode 
 Vol
 Fractions
 (K)
 (K)
 (W/M2/K)
 Mode

 000 atms
 0.00000E+00
 3.39665E+02
 0.00000E+00
 0.00000E+00
 pool
 0.00000E+00
 0.00000E+00
 0.00000E+00
 pool
 0.00000E+00
 0.00000E+00
 0.00000E+00
 pool
 0.00000E+00
 0.00000E+00
 0.00000E+00
 0.00000E+00
 pool
 0.00000E+00
 0.00000E+00
 0.00000E+00
 TAB-F.
 Heat fluxes at the boundary surface q(conv) Q(conv) (W/m2) (W) q(rad) (W/m2) Q(rad) Vol 
 ...
 (W/HLZ)
 (W)
 (W/m2)
 (W)

 000 atms
 0.00000E+00
 0.00000E+00
 0.00000E+00
 0.00000E+00

 pool
 0.00000E+00
 0.00000E+00
 0.00000E+00
 0.00000E+00
 repr 7.93303E+03 1.58661E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface (m/s) Vol comp \_\_\_\_ \_\_\_\_ \_\_\_\_\_ 000 atms 0.00000E+00 000 pool 0.00000E+00 000 bubb 0.00000E+00 Gas composition at the boundary surface Cas Gas MASS TA FRACTION MASS VOID \_\_\_\_\_ ----atms droplets 0.00000E+00 0.00000E+00 pool bubbles 0.00000E+00 0.00000E+00 BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ \_\_\_\_\_ TC-100, Boundary Cell: IBC = 3, Cell: I = 4 (K,L) = (01,02) \_\_\_\_\_ \_\_\_\_\_ \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h H.T. Fractions (K) (K) (W/m2/K) Mode Vol 000 atms 0.00000E+00 3.39665E+02 0.00000E+00 0.00000E+00 pool 0.00000E+00 3.39665E+02 0.00000E+00 0.00000E+00 repr 1.00000E+00 3.39665E+02 3.00000E+02 2.00000E+02 TAB-F. Heat fluxes at the boundary surface q(conv) Q(conv) q(rad) Q(rad) (W/m2) (W) (W/m2) (W) Vol 000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 7.93303E+03 1.58661E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface v (m/s) Vol comp \_\_\_\_ \_\_\_\_ 000 atms 0.00000E+00 000 pool 0.00000E+00 000 bubb 0.00000E+00 Gas composition at the boundary surface Gas Gas MASS VOLUME

No. Id. FRACTION FRACTION ---- ---\_\_\_\_\_ ----\_\_\_\_\_ \_\_\_\_\_ 0.00000E+00 0.00000E+00 atms droplets pool bubbles 0.00000E+00 0.00000E+00 BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ \_\_\_\_\_ TC-100, Boundary Cell: IBC = 4, Cell: I = 5 (K,L) = (02,02) \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface Н.Т. H.T.Area Twall Tfluid h Vol Fractions (K) (K) (W/m2/K) Mode --- ---- -------\_\_\_\_ 000 atms 0.00000E+00 3.15067E+02 0.00000E+00 0.00000E+00 pool 0.00000E+00 3.15067E+02 0.00000E+00 0.00000E+00 repr 1.00000E+00 3.15067E+02 3.00000E+02 2.00000E+02 TAB-F. Heat fluxes at the boundary surface q(conv) Q(conv) q(rad) Q(rad) (W/m2) (W) (W/m2) (W) Vol \_\_\_\_ \_\_\_\_ 000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 3.01344E+03 6.02687E+01 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface 77 Vol comp (m/s) --- ---- ------000 atms 0.00000E+00 000 pool 0.00000E+00 000 bubb 0.00000E+00 Gas composition at the boundary surface Gas Gas MASS VOLUME No. Id. FRACTION FRACTION No. Id. ---- --------\_\_\_\_ \_\_\_\_\_ atms droplets 0.00000E+00 0.00000E+00 pool bubbles 0.00000E+00 0.00000E+00 BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ TC-100, Boundary Cell: IBC = 5, Cell: I = 6 (K,L) = (03,02) \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h Fractions (V) (V) (V) н.т. 
 Vol
 Fractions
 (K)
 (K)
 (W/m2/K)
 Mode

 000 atms
 0.00000E+00
 3.39665E+02
 0.00000E+00
 0.00000E+00
 pol
 0.00000E+00
 0.00000E+00
 0.00000E+00
 pol
 0.00000E+00
 0.00000E+00
 pol
 0.00000E+00
 0.00000E+00
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 0.00000E+00
 pol
 0.00000E+00
 pol
 0.00000E+00
 pol
 0.00000E+00
 pol
 0.00000E+00
 pol
 pol</ Vol Heat fluxes at the boundary surface 
 q(conv)
 Q(conv)
 q(rad)
 Q(rad)

 Vol
 (W/m2)
 (W)
 (W/m2)
 (W)
 000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 7.93303E+03 1.58661E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface Vol comp (m/s) --- ---- ------000 atms 0.00000E+00

000 pool 0.00000E+00 000 bubb 0.00000E+00

Gas composition at the boundary surface Gas Gas MASS Td. FRACTION MASS VOLUME FRACTION FRACTION No. Id. FRACTION FRACTION ---- -atms droplets 0.00000E+00 0.00000E+00 pool bubbles 0.00000E+00 0.00000E+00 BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ TC-100, Boundary Cell: IBC = 6, Cell: I = 8 (K,L) = (02,03) \_\_\_\_\_ \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h Fractions (K) (K) (W/m2/K) Н.Т. Vol Mode \_\_\_\_ \_\_\_\_ 000 atms 0.00000E+00 3.39665E+02 0.00000E+00 0.00000E+00 pool 0.00000E+00 3.39665E+02 0.00000E+00 0.00000E+00 repr 1.00000E+00 3.39665E+02 3.00000E+02 2.00000E+02 TAB-F. Heat fluxes at the boundary surface q(conv) Q(conv) q(rad) Vol (W/m2) (W) (W/m2) Q(rad) (W) \_\_\_\_\_\_ 000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 7.93303E+03 1.58661E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface v (m/s) Vol comp ---- -----000 atms 0.00000E+00 000 pool 0.00000E+00 000 bubb 0.00000E+00 Gas composition at the boundary surface Gas Gas MASS VOLUME VOLUME FRACTION No. Id. -- --- -----\_\_\_\_ atms droplets 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool bubbles BOUNDARY DATA AT TIME : 1.00000E+03 (s) \_\_\_\_\_ ------TC-100, Boundary Cell: IBC = 7, Cell: I = 9 (K,L) = (03,03) \_\_\_\_\_ Temperatures and heat transfer coefficients at the boundary surface H.T.Area Twall Tfluid h H.T. Fractions (K) (K) (W/m2/K) Mode Vol ----000 atms 0.00000E+00 3.29330E+02 0.00000E+00 0.00000E+00 pool 0.00000E+00 3.29330E+02 0.00000E+00 0.00000E+00 repr 1.00000E+00 3.29330E+02 3.00000E+02 2.00000E+02 TAB-F. Heat fluxes at the boundary surface 
 q(conv)
 Q(conv)
 q(rad)
 Q(rad)

 Vol
 (W/m2)
 (W)
 (W/m2)
 (W)
 (W) --- ---- ------------000 atms 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 pool 0.00000E+00 0.00000E+00 repr 5.86603E+03 1.17321E+02 0.00000E+00 0.00000E+00 Fluid velocities at the boundary surface (m/s) Vol comp --- ---- (11/3) 000 atms 0.00000E+00 000 pool 0.00000E+00

000 bubb 0.00000E+00

Gas	compos	composition			boundar	У	/ surface		
	Gas	Gas		MASS			VOLUME		
	No.	Id.	H	FRACTION			FRACTION		
atms	s drop	lets	0.0	000	00E+00	Ο.	00000E+00		
pool	bubb	bubbles		000	00E+00	Ο.	00000E+00		

At the bottom of the TC output the summed quantities (data summed for all 2-D Solid Conductors) are printed. An example printout is shown below.

The heat fluxes and integrated heat fluxes printed below are summed over those surfaces which transfer heat to normal Control Volumes (those CVs for which conditions are not held constant). Integrated Heat Flux Heat Flux W J Convective : 0.0000E+00 0.0000E+00 Radiative : 0.00000E+00 0.00000E+00 Total : 0.0000E+00 0.00000E+00

#### 3.1.6 Thermal Radiation Output

The Thermal Radiation outputs may be easily found in the output file by searching for the string: =TR=. The first TR printout brings the input data printout. An example of the thermal radiation input printout is shown below.

=TR=	INPUT C	ATA FOR 1 RAI	DIATING SYST	EMS	
=TR=	SYSTEM No.: 1 Example problem - thermal radiation				
=TR= MODEL: Grey Enclosure with Participating Gas					
-IK- INFUL DAIA FOR 4 RADIALING SURFACES					
i	TR	SC/TC	Emissivity	Pool option	
1	TR-101	SC-001 Left	TF-007	No	
2	TR-102	SC-002 Right	TF-007	No	
3	TR-103	SC-003 Right	TF-007	No	
4	TR-104	SC-004 Right	TF-007	Yes	
=TR=	View Fa	ctors, (-),	₹ (i->j)		
λj	1	2		3	4
i \ -----\_\_\_\_\_ \_\_\_\_\_ 1.171565E-019.248080E-023.951813E-013.951813E-012.774424E-010.000000E+003.612788E-013.612788E-012.963860E-019.031970E-020.000000E+006.132943E-01 1 2 3 2.963860E-01 9.031970E-02 6.132943E-01 0.000000E+00 4 Sum { F(i->j) j=1..N } Ι 1.0000000E+00 1 2 1.0000000E+00 1.0000000E+00 3 1.0000000E+00 4 =TR= Beam Lengths, (m), L (i->j) \j i \ 1 2 3 4 =TR= Radiation Beams Passing Through Multiple CV-s: 
 Beam
 :
 TR-101 ->
 TR-102

 CV-s on the Beam:
 CV-001
 CV-002

 Beam Lengths
 :
 6.50E+00
 6.50E+00
 Beam Lengths : Beam : TR-102 -> TR-101 CV-s on the Beam: CV-001 CV-002 Beam Lengths : 6.50E+00 6.50E+00 Beam : TR-102 -> TR-103 CV-s on the Beam: CV-002 CV-001 Beam Lengths : 3.65E+00 3.65E+00 : TR-102 -> TR-104 Beam CV-s on the Beam: CV-002 CV-001 Beam Lengths : 3.65E+00 3.65E+00 : TR-103 -> TR-102 Beam CV-s on the Beam: CV-002 CV-001 Beam Lengths : 3.65E+00 3.65E+00 Beam : TR-104 -> TR-102 CV-s on the Beam: CV-002 CV-001 Beam Lengths : 3.65E+00 3.65E+00 =TR= RADIATION PROPERTIES OF 6 GASES \_\_\_\_\_ =TR= EMISSIVITY Emissivity Correlation Gas 1 No absorption/emission 2 No absorption/emission 3 Kostowski Correlation for H2O 4 No absorption/emission No absorption/emission 5 6 Kostowski Correlation for CO2 =TR= ABSORPTIVITY Gas Absorptivity Correlation \_\_\_ \_\_\_\_\_ No absorption/emission 1 2 No absorption/emission A = E ( Tw, pL(Tw/Tg) ) ( Tg/Tw )\*\* 4.500E-01 3 4 No absorption/emission 5 No absorption/emission A = E (Tw, pL(Tw/Tg)) (Tg/Tw)\*\* 6.500E-01 6

=TR= RADIATING SURFACE INTERNAL NUMBERING SCHEME =TR= RADIATING SYSTEM No.: 1 Example\_problem\_-\_thermal\_radiation\_\_\_\_\_\_ Int. Ref. Int. Ref. Int. Ref. Int. Ref. No. No. No. No. No. No. No. 1 TR-101 2 TR-102 3 TR-103 4 TR-104 =TR= END OF THERMAL RADIATION DATA

The radiation model applied is printed at the top of this printout. Then the following blocks are printed:

The first block contains associations of radiating surfaces with the Solid Conductor surfaces (left or right). It also prints the indication of how the surface emissivity is defined, and whether the pool option is used.

The second block contains all view factors,  $F_{i \rightarrow j}$ , and the sums:

$$S_i = \sum_j F_{j \to i}$$

All values of  $S_i$  must be equal to one; otherwise an input error is signaled.

The following blocks are printed only if the radiation model with participating gas is chosen. The first block contains all mean beam lengths,  $L_{i\rightarrow j}$ . Also the Control Volumes, through which the beam passes, are given. If the beam passes through a sequence of several Control Volumes, then the letters "Seq" are printed instead of the volume number. In such case the beams passing multiple Control Volumes are listed next, including the lengths the beam passes in each Control Volume.

The next part of the printout contains enclosure data. This data is printed only to give the user a qualitative verification of his beam length data. This block is printed only if there are no beams passing through multiple Control Volumes (only then the logic identifying enclosures is used). Since in the example case above beams pass multiple Control Volumes, the enclosure data printout is not included there. A printout from another example is included below.

=TR=	Enclosure(	s) descri	ption	
=TR=	Enclosure No.	Fluid Volume	Radiating Surfaces	Pool option
	01	CV-001	TR-101 TR-102 TR-103 TR-104	NO NO NO Yes
=TR=	AVERAGED C Enclosure Engineerin	VER ENCLO average b g beam le	SURES VALUES OF eam l.= average ngth = 4*V/A	GEOMETRIC MEAN BEAM LENGTHS L(i->j), weighted by: A(i)*F(i->j) V - gas volume of enclosure A - total surface area
	Enclosure No.	Fluid Volume	Average Beam L. (m)	Engineering Beam L. (m)

01 CV-001 7.60 6.67

For each identified enclosure an average value of mean beam length is calculated, from the formula:

$$L_{ave} = \frac{\sum_{i=1}^{N} \sum_{j=1}^{N} A_i F_{i \to j} L_{i \to j}}{\sum_{i=1}^{N} \sum_{j=1}^{N} A_i F_{i \to j}}$$

where:  $A_i$  - area of surface i, (m<sup>2</sup>),

 $F_{i \rightarrow j}$  - view factor between surface i and j, (-),

 $L_{i \rightarrow j}$  - mean beam length between surface i and j, (m),

*N* - number of radiating surfaces in given enclosure.

The average value is compared with an "engineering estimation" of mean beam length in an enclosure, which is ([14] page 15-65):

$$L_{ave} = \frac{4V}{A}$$

where: V - total volume of the enclosure, (m<sup>3</sup>), (equal to the volume above the pool for the Control Volume associated with the enclosure),

A - total surface area of the enclosure,  $(m^2)$ , (equal to the sum of surface areas of all radiating surfaces associated with the enclosure,  $\Sigma A_i$ ).

An example of the Thermal Radiation transient printout is shown below.

=TR=	OUTPUT DATA FO	R 1 RADIATING	SYSTEMS AT TIM	E: 1.00000E+03	
=TR=	SYSTEM No.: 1	Example_	_problemther	mal_radiation_	
=TR=	Surface data				
Surfa	ce SC	- (K)	Emis.	q (M(m2)	Q (INI)
mp 10	1 CC 001 Toft	- (V)	(-) 0 50000 01	(W/IIIZ)	(W) 2 20607EL02
TR-10	2 SC=001 Leit	+ 3 58096F+02	9.50000E-01 9.50000E-01	-4.89334E+00	=2.3009/E+03
TR-10	2 SC 002 Righ 3 SC-003 Righ	+ 3 58046E+02	9 50000E 01	-4 66802E+00	-2 93300E+03
TR-10	4 SC-004 Righ	t 3.57988E+02	9.60000E-01	-5.43003E+00	-3.41179E+03
=TR=	Gas Emissivity	, (CV)			
\ ]	1	2	3	4	
l \	CV	CV	CV	CV	
Ţ	7.30E-01 001	9.08E-01 Seq	7.11E-01 001	7.11E-01 001	
2	9.08E-01 Seq	0.00E+00 000	8.5/E-U1 Seq	8.5/E-U1 Seq	
3	7.11E-01 001 7.11E-01 001	8.5/E-01 Seq 8.57E-01 Seq	0.00E+00 000	0.96E-01 001	
7	7.11E 01/001	0.57E 01 5eq	0.905 011001	0.0011001000	
=TR=	Gas Absorptivi	ty, (CV)			
\ j	1	2	3	4	
i \	CV	CV	CV	CV	
1	7.30E-01 001	9.08E-01 Seq	7.11E-01 001	7.11E-01 001	
2	9.08E-01 Seq	0.00E+00 000	8.58E-01 Seq	8.58E-01 Seq	
3	7.11E-01/001	8.58E-01 Seq	0.00E+00 000	6.96E-01 001	
4	/.11E-01 001	8.38E-NT Sed	0.90E-011001	U.UUE+UU 000	
=TR=	Gas Temperatur	e, (CV)			
λj	1	2	3	4	

i \ CV CV 1 3.59E+02 001 3.60E+02 Seq 2 3.60E+02 Seq 0.00E+00 000 3 3.59E+02 001 3.60E+02 Seq 4 3.59E+02 001 3.60E+02 Seq	CV CV 3.59E+02 001 3.59E+02 001 3.60E+02 Seq 3.60E+02 Seq 0.00E+00 000 3.59E+02 001 3.59E+02 001 0.00E+00 000
=TR= Gas Heat Absorp., (CV) $\langle j 1 2 \rangle$	3 4
$1 = -2.39E \pm 0.21001 = 6.11E \pm 0.218ec$	$-7.47 \pm +021001$ $-7.47 \pm +021001$
2 -5.75E+02 Seg 0.00E+001000	-7.03E+02 Seg = -7.03E+02 Seg
3 -7.48E+02 001 -7.47E+02 Seq	0.00E+00 000 -1.52E+03 001
4 -8.23E+02 001 -7.76E+02 Seq	-1.67E+03 001 0.00E+00 000
=TR= Data for Radiation Beams Pass	ing Through Multiple CV-s:
Beam : TR-101 ->	TR-102
CV-s on the Beam: CV-001	CV-002
Gas Emissivity : 6.96E-01	6.96E-01
Gas Absorptivity: 6.96E-01	6.98E-01
Gas Temperature : 3.59E+02	3.61E+02
Beam : TR-102 ->	TR-101
CV-s on the Beam: CV-001	CV-002
Gas Emissivity : 6.96E-01	6.96E-01
Gas Absorptivity: 6.96E-01	6.98E-01
Gas Temperature : 3.59E+02	3.61E+02
Beam : TR-102 ->	TR-103
CV-s on the Beam: CV-002	CV-001
Gas Emissivity : 6.22E-01	6.22E-01
Gas Absorptivity: 6.23E-01	6.22E-01
Gas Temperature : 3.61E+02	3.59E+02
Beam : TR-102 ->	TR-104
CV-s on the Beam: CV-002	CV-001
Gas Emissivity : 6.22E-01	6.22E-01
Gas Absorptivity: 6.23E-01	6.22E-01
Gas Temperature : 3.61E+02	3.59E+02
Beam : TR-103 ->	TR-102
CV-s on the Beam: CV-002	CV-001
Gas Emissivity : 6.22E-01	6.22E-01
Gas Absorptivity: 6.23E-01	6.22E-01
Gas Temperature : 3.61E+02	3.59E+02
Beam : TR-104 ->	TR-102
CV-s on the Beam: CV-002	CV-001
Gas Emissivity : 6.22E-01	6.22E-01
Gas Absorptivity: 6.23E-01	6.22E-01
Gas Temperature : 3.61E+02	3.59E+02

The thermal radiation transient printout consists of the following blocks.

The first block contains printout of the <u>surface data</u>, including temperature, emissivity, heat flux, as well as heat power emitted from all radiating surfaces. If the radiation model with non-absorbing/non-emitting gas is chosen, then this is the only printout from the thermal radiation model.

The next blocks are printed if the radiation model with participating gas is chosen. The first block here contains the <u>gas emissivities</u> for all radiation paths. It also gives the number of a Control Volume, if the beam passes through a single Control Volume, or the letters "Seq", if the beam passes through

several Control Volumes. If the beam passes through single Control Volume, then this is the emissivity calculated for the gas composition and temperature in this CV:

$$\varepsilon_{i \to j} = f(pL_{i \to j})$$

where  $(pL_{i\rightarrow j})$  is the optical length in the CV. If the beam passes through multiple Control Volumes, then the average emissivity is obtained from:

$$\varepsilon_{i\to j} = 1 - \prod_m (1 - \varepsilon_m)$$

where  $\varepsilon_m$  is the individual emissivity in the *m*-th CV, where the beam optical length is  $pL_m$ ,  $\varepsilon_m = \varepsilon_m(pL_m)$ . The multiplication is performed over all Control Volumes on the beam length. The total beam length between surfaces *i* and *j* must of course be equal to the sum of individual lengths, so the following relation is always true (if not, this is flagged as an input error):

$$L_{i \to j} = \sum_m L_m$$

The symbols  $\varepsilon_m$ ,  $L_m$  should be, strictly speaking,  $\varepsilon_{m, i \to j}$ ,  $L_{m, i \to j}$ , but for the sake of clarity the indexes *i*, *j* were skipped.

The next block contains the <u>gas absorptivities</u> for all radiation paths. It also gives the number of a Control Volume, if the beam passes a single Control Volume, or the letters "Seq", if the beam passes several Control Volumes. The average absorptivity of the beam passing through multiple Control Volumes is calculated, similarly as in case of emissivity, from:

$$a_{i \to j} = 1 - \prod_{m} \left( 1 - a_m \right)$$

This means, the overall transmittance is equal to the product of individual transmittances. Again, individual absorptivities  $a_m$  depend on the individual optical lengths,  $pL_m$ ,  $a_m = a_m(pL_m)$ .

Next the gas temperatures are printed. If the beam passes a single Control Volume, then the value printed here is of course identical to the CV atmosphere temperature. For example, the printout for i=1, j=1: **3.59E+02|001**, means the gas temperature is 359 K and it is equal to the atmosphere temperature in CV-001. If the beam passes several Control Volumes, then this is the averaged temperature. For example, the printout for i=1, j=2: **3.60E+02|Seq**, means the gas average temperature is 360 K, and it is averaged over the full sequence of Control Volumes through which the beam passes. The temperature averaging is performed as follows:

$$T_{i \to j} = \left(\frac{\sum_{m} (\varepsilon_m \cdot T_m^4)}{\sum_{m} \varepsilon_m}\right)^{1/4}$$

where  $L_m$  is the beam length in the *m*-th CV and the summation is performed over all Control Volumes on the beam length.

Finally the heat absorbed (emitted) by the gas is printed. If the beam passes a single Control Volume, then the absorbed (emitted) heat (calculated by the Thermal Radiation Package) is of course deposited in (removed from) this Control Volume. If the beam passes several Control Volumes, then the net heat transfer to gas, obtained from the Thermal Radiation Package, is partitioned among all Control Volumes using the following formula.

$$Q_m = Q_{i \to j} \cdot \left(\frac{\varepsilon_m}{\sum_m \varepsilon_m}\right) - A_i F_{i \to j} \sigma \varepsilon_m \left(T_m^4 - T_{i \to j}^4\right)$$

Where  $Q_{i \rightarrow j}$  is the total heat exchanged with gas on the radiation beam  $i \rightarrow j$ . Again the subscript *m* should be, strictly speaking, replaced by *m*,  $i \rightarrow j$ , since all values are those for the radiation beam from the surface *i* to the surface *j*. The extra subscripts were skipped for clarity. Note that the above formulation fulfils the following important relations.

• If the gas emissivity in given CV is zero, then the part of total heat assigned to that volume is zero:

$$Q_m = 0.0$$
 if  $\varepsilon_m = 0.0$ 

This can easily be proved by substituting zero for  $\varepsilon_m$  in the above formula.

• The sum of all heats is equal to the total heat:

$$\sum_{m} Q_{m} = Q_{i \to j}$$

This can be proved by performing the summation and substituting the formula for the average temperature,  $T_{i \rightarrow j}$ :

$$\begin{split} \sum_{m} Q_{m} &= Q_{i \to j} \cdot \left( \frac{\sum_{m} \varepsilon_{m}}{\sum_{m} \varepsilon_{m}} \right) - A_{i} F_{i \to j} \sigma \sum_{m} \varepsilon_{m} \left( T_{m}^{4} - T_{i \to j}^{4} \right) = \\ &= Q_{i \to j} - A_{i} F_{i \to j} \sigma \left( \sum_{m} \varepsilon_{m} T_{m}^{4} - T_{i \to j}^{4} \sum_{m} \varepsilon_{m} \right) = \\ &= Q_{i \to j} - A_{i} F_{i \to j} \sigma \left( \sum_{m} \varepsilon_{m} T_{m}^{4} - \frac{\sum_{m} \varepsilon_{m} T_{m}^{4}}{\sum_{m} \varepsilon_{m}} \sum_{m} \varepsilon_{m} \right) = \\ &= Q_{i \to j} - A_{i} F_{i \to j} \sigma \left( \sum_{m} \varepsilon_{m} T_{m}^{4} - \sum_{m} \varepsilon_{m} T_{m}^{4} \right) = \\ &= Q_{i \to j} - A_{i} F_{i \to j} \sigma \left( \sum_{m} \varepsilon_{m} T_{m}^{4} - \sum_{m} \varepsilon_{m} T_{m}^{4} \right) = \\ &= Q_{i \to j} \end{split}$$

#### 3.1.7 Tabular Function Output

The Tabular Function outputs may be easily found in the output file by searching for the string: =TF=. The first TF printout brings the input data printout. An example of a Tabular Function input printout is shown below.

=TF= =====TF-001===== Example 1 of Tabular Function 1.) TABULAR FUNCTION DEFINITION AND LIMITS: Addit.const. Multiplier Interpolation 0.00000E+00 1.00000E+00 Linear (1-st order) Limits Minimum Maximum \_\_\_\_\_ TF(t)-1.00000E+991.00000E+99dTF(t)/dt-1.00000E+991.00000E+99TF(t)-1.00000E+991.00000E+99 MESSAGE TF(t) MESSAGE dTF(t)/dt -1.00000E+99 1.00000E+99 2.) INTERACTIVE TABULAR FUNCTION At any time of calculations the TF value may be modified in the \*.TFD file If there is no data in the file, then the tabulated points are used. Reset option not used. To get back to tabulated points, the TF definition must be removed from  $\star.\text{TFD}$  file manually or by an external program 3.) TF DATA VALUES 7 TOTAL NUMBER OF DATA POINTS: Ν Х Y \_\_\_\_\_ \_\_\_\_ \_\_\_\_\_ 
 5.00000E+00
 1.00000E-01

 1.00000E+01
 1.10000E+00

 1.50000E+01
 1.10000E+00

 2.50000E+01
 2.00000E-01

 3.0000E+01
 2.50000E+00

 3.50000E+01
 1.00000E+00

 4.50000E+01
 1.00000E+00
 1 2 3 4 5 6 7 \_\_\_\_\_ At the bottom of the TF data the internal numbering scheme is printed: \_\_\_\_\_ =TF= TABULAR FUNCTION INTERNAL NUMBERING SCHEME \_\_\_\_\_ Int. Ref. Int. Ref. No. No. No. No. 1 TF-001 2 TF-002

An example of the Tabular Function transient printout is shown below.

=TF= OUTPUT DATA FOR 2 TABULAR FUNCTIONS, AT TIME : 5.00000E+01 (s)

Function Value Name

 TF-001
 1.00000E+00
 Example\_1\_of\_Tabular\_Function\_\_\_\_\_

 TF-002
 3.00000E+00
 Example\_2\_of\_Tabular\_Function\_\_\_\_\_

\_\_\_\_\_

#### 3.1.8 Control Function Output

The Control Function outputs may be easily found in the output file by searching for the string: =CF=. The first CF printout brings the input data printout. An example of a Control Function input printout is shown below.

```
=CF= =====CF-100====== 2-D General Tabular Function
   A.) CONTROL FUNCTION DEFINITION AND LIMITS:
                                  : TABULAR FUNCTION
           CF TYPE
           Initial value : to be calculated
           Addit.const. Multiplier CF Type
           0.00000E+00 1.00000E+00 TABULAR FUNCTION
                          Minimum Maximum
           Limits
           _____
                                 _____
                                                        _____
             CF(t) -1.00000E+99 1.00000E+99
            dCF(t)/dt -1.00000E+99 1.00000E+99
CF(t) -1.00000E+99 1.00000E+99
MESSAGE CF(t)
MESSAGE dCF(t)/dt -1.00000E+99 1.00000E+99
   B.) CF ARGUMENTS DESCRIPTION:

        No.
        Addit.const.
        Multiplier
        Variable
        Comment

        1.
        0.00000E+00
        1.00000E+00
        JN-500-PVFl-pool-m3/s
        X (1-ST INDEPENDENT VAR.)

        2.
        0.00000E+00
        1.00000E+00
        TF-101-Valu-0000-
        TF VALUE FOR THE ARGUMENT

        3.
        0.00000E+00
        1.00000E+00
        TF-102-Valu-0000-
        TF VALUE FOR THE ARGUMENT

        4.
        0.0000E+00
        1.00000E+00
        TF-103-Valu-0000-
        TF VALUE FOR THE ARGUMENT

        5.
        0.00000E+00
        1.00000E+00
        JN-500-PSpd-pool-1/s
        Y (2-ND INDEPENDENT VAR.)

 No. Addit.const. Multiplier
                                                                                                X (1-ST INDEPENDENT VAR.)
TF VALUE FOR THE ARGUMENT X
                                                                                                TF VALUE FOR THE ARGUMENT X
TF VALUE FOR THE ARGUMENT X
 2-D INTERPOLATION IS PERFORMED, CF IS DEFINED AS:
                    CF(t) = f(x, y)
 where: x - first argument, defined as: x = JN-500-PVFl-pool-m3/s y - second argument, defined as: y = JN-500-PSpd-pool-1/s
 x-interpolation is performed for all tabular functions -> TF(x)
 y-interpolation is performed using the following data points:
       1
   3
           Argument values : implicit
```

At the bottom of the CF data printout the method of calculating all Control Functions is printed. In the present example the functions are included in the implicit solution scheme. This means iteration will be continued until the required convergence is reached for all parameters, including values of all Control Functions. The other option, "CF not included" means that the values of CF will be updated by the solver in the main iteration, along with all other solution parameters, but the convergence criterion will not be checked for the CF. If all other parameters converge, the solver will complete the

advancement and proceed to the next one, independently of the convergence of the CF. Finally, the internal numbering scheme is printed.

An example of the Control Function transient printout is shown below.

====== =CF=	OUTPUT DA	======================== IA FOR 4 CO	NTROL FUNCTIONS, AT TIME : 5.00000E+01 (s)
	Function =CF-001 =CF-002 =CF-003 =CF-004	Value 3.80000E+02 3.42000E+02 6.50000E+01 3.80000E+02	Name Maximum_temperature_of_SC-001 Average_temperature_of_SC-001 Constant_value_of_15.0 Tmax_for_t_<_15_s, Tave_for_t_>_15_s

#### 3.1.9 Reactor Kinetics Output

The Reactor Kinetics outputs may be easily found in the output file by searching for the string:  $=\mathbf{RK}=$ . The first RK printout brings the input data printout. An example of a Reactor Kinetics (including the Isotope Transformation) input printout is shown below.

```
=RK= INPUT DATA FOR THE REACTOR KINETICS MODEL
                                                           _____
             _____
=RK= POWER CALCULATED BY THE REACTOR KINETICS MODEL
      IS AVAILABLE AS CONTROL FUNCTION: CF-001
      IN CASE OF SOLID FUEL (IFTORK=1) THE POWER INCLUDES:
      - FISSION POWER (RT-000-Qfis-000)
       - DECAY
                POWER (RT-000-Qdec-000)
      IN CASE OF LIQUID FUEL (IFTORK=2) THE POWER INCLUDES:
       - FISSION POWER (RT-000-Qfis-000)
      THE DECAY POWER IS IN SUCH CASE CALCULATED BY
      THE RT PACKAGE AND ADDED AUTOMATICALLY TO THE CV POOL
=RK= NODE-INDEPENDENT DATA:
      NO. OF NEUTRONS PER FISSION[-]: XNPFRK = 2.50000E+00HEAT RELEASE PER FISSION[J]: QFISRK = 3.09026E-11THERMAL NEUTRON VELOCITY[m/s]: CTHNRK = 2.56000E+03FAST FISSION FACTOR[-]: EPSRK = 1.02000E+00
      INSTITUSTION FACTOR[-]: EPSRK = 1.02000E+03RESONANCE ESCAPE PROBABILITY[-]: PRESRK = 8.70000E-01FAST NONLEAKAGE PROBABILITY[-]: T-SRE
      FAST NONLEAKAGE PROBABILITY[-]: PFNLRK = 8.80000E-01THERMAL NONLEAKAGE PROBABILITY[-]: PTNLRK = 8.80000E-01
                                            [-] :
      K-INF
                                                             1.29132E+00
      MULTIPLIER ON DECAY HEAT
                                             [-] : QDMLRK = 1.00000E+00
      MINIMUM MACROSCOPIC FISSION CS.[1/m] : SIGMRK = 1.00000E-06
      DO NOT INCLUDE P*EPS IN THE REACTIVITY EFFECT CALCULATION, (IPERRK=1)
=RK= NODE-DEPENDENT DATA:
      NODE
                PNGTRK
       No.
                [s]
       ____
        1
              6.00000E-04
                             RVOLRK PINIRK IINIRK
[m3] [W] [-]
                SIGFRK
                                                                   RINIRK
      NODE
              [1/m] [m3] [W] [-]
                                                                   [$]
       ____
         1
               8.40000E-01 5.15000E+00 3.75000E+07
                                                            1 0.00000E+00
      POINT KINETICS INITIALIZATION : INONRK = 0
      PLOT REQUEST, REACTIVITY VS. K: IRPLRK = 1
=RK= DELAYED NEUTRON PRECURSOR DATA
      YieldDecayHalf-lifeGroup AbsoluteRelativeConstantT(1/2)No.[1/fis][-1][1/c1]
       No.
                                             [1/s]
               [1/fis]
                                [-]
                                                                [s]
             2.20000E-04 3.38462E-02 1.24000E-02 5.58990E+01
1.42000E-03 2.18462E-01 3.05000E-02 2.27261E+01
         1
         2
            1.27000E-03 1.95385E-01 1.11000E-01 6.24457E+00
2.57000E-03 3.95385E-01 3.01000E-01 2.30281E+00
         3
         4
             7.50000E-04 1.15385E-01
                                            1.14000E+00
         5
                                                              6.08024E-01
            2.70000E-04 4.15385E-02 3.01000E+00 2.30281E-01
         6
                 _____
     Sum: 6.50000E-03 1.00000E+00
```

=RK= EXTERNAL NEUTRON SOURCES

NODE SOURCE [1/s]

1 NO EXTERNAL SOURCE =RK= EXTERNAL REACTIVITY DATA NODE REACTIVITY [\$] 1 NO EXTERNAL REACTIVITY =RK= REACTIVITY FEEDBACK DATA Fuel Temper. Reactivity No. [K] [\$] [K] [\$] 0.00000E+00 0.00000E+00 1 1.00000E+04 -1.00000E+02 2 Moderator T. Reactivity No. [K] [\$] 0.00000E+00 0.00000E+00 1.00000E+04 1.50000E+01 1 2 Void Fraction Reactivity No. [-] [\$] 0.00000E+00 0.00000E+00 1 1.00000E+00 0.00000E+00 2 =RK= FULL REACTIVITY FEEDBACK DATA FOR 2 x 2 x 2 DATA POINTS ----- Void Fraction = 0.000E+00 \Tfuel 0.000E+00 1.000E+04 Tmod. 0.000E+00 -1.000E+02 1.500E+01 -8.500E+01 0.000E+00 1.000E+04 ----- Void Fraction = 1.000E+00 \Tfuel 0.000E+00 1.000E+04 Tmod.∖ 0.000E+00 0.000E+00 -1.000E+02 1.000E+04 1.500E+01 -8.500E+01 =RK= WEIGHTING FACTOR DATA FOR 1 NODES ---- NODE No.: 1 -Tf- Fuel Temperature Weighting Factors No. Component number and variable description Weighting factor --\_\_\_\_\_ \_\_\_\_\_ 1 SC-001 Temperature of Nodes: 1 - 5 1.00000E+00 \_\_\_ \_\_\_\_\_ 1.00000E+00 Total The average fuel temperature is obtained from: Tfuel = SUM( Wi \* Ti ) / SUM ( Wi ) Normalization is performed because all factors are positive =RK= SOURCE DENSITY DATA FOR CIRCULATING FUEL (USED ONLY FOR IFTORK = 2) -Qf- Fraction of isotopes generated in core regions No. Location Power factor \_\_\_\_\_ \_\_\_ \_\_\_\_\_ 1 CV-001 Pool volume 1.00000E+00 \_\_\_\_\_ \_\_\_ \_\_\_\_\_ Total 1.00000E+00 Normalization is performed

-Tm- Moderator Temperature Weighting Factors

No. Compon	ent number an	d variable description	Weighting factor
1 SC-001	Temperature	of Nodes: 1 - 6	1.00000E+00
 Total			1.00000E+00
The av	erage moderat	or temperature is obtained	d from:
Tmod =	SUM( Wi * Ti	) / SUM ( Wi )	
Normal	ization is pe	rformed because all factor	rs are positive
Vf- Void f	raction Weigh	ting Factors	
No. Compon	ent number an	d variable description	Weighting factor
1 SC-001	Local bubbl	e fraction at right surface	ce 1.00000E+00
 Total			1.00000E+00
The av	erage void fr	action is obtained from.	
VOID -	SIIM ( Wi + V/	TDi ) / SIM ( Wi )	
VULU -	Som with wo	IDI / / OUT ( WI /	
Normal	ization is pe	riormed because all factor	rs are positive
RK= REACTO OR DUR - CONS - CONS	R CONTROL WHE ING INITIALIZ TANT IN THE F TANT IN THE I	N CV/JN/H2 PACKAGES ARE D ATION OF THE NODAL POINT F ROPORTIONAL CONTROLLER: CF NTEGRATING CONTROLLER: C1	ISABLED XINETICS (INONRK=1) : PCVRK = 1.00000E+00 ICVRK = 1.00000E+00
RK= REACTI	VITY EFFECT C	F ISOTOPE CONCENTRATION CH	HANGES: YES (IREIRK=1)
RK= FUEL T	YPE: SOLID FU	EL (IFTORK = 1)	
ISOTOP	E MAPPING TO	RT : NOT REQUESTED (IMAPRE	<pre>K = 0)</pre>
KK= ISOTOP =======	E TRANSFORMAT	ION MODEL	
:RK= ΤΝΤͲΤΔ	I ISOTOPE CON	CENTRATIONS:	
EQUILI	BRIUM CONCENI	RATIONS OF NON-FISSILE ISC	DTOPES
ARE CA	LCULATED IF N	O VALUE IS SPECIFIED IN IN	NP0.1.
RK= INITIA	l data for 3	4 ISOTOPES	
	Input Initial	Multiplier	
	Concentr.	Reactivity	
L Isotope	[1/m3]	[-]	
)1 TH-232 )2 Th-233	0.00000E+00	1.00000E+00	
)3 Th-234	0.00000E+00	1.00000E+00	
)4 Pa-233	0.00000E+00	1.00000E+00	
)5 Pa-234	0.00000E+00	1.00000E+00	
0 U-233	U.UUUUUE+00	1.00000E+00	
)8 U-234	1.66337E+25	1.00000E+00	
)1 U-238	1.49703E+26	1.00000E+00	
)2 U-239	0.00000E+00	1.00000E+00	
)3 U-240	0.00000E+00	1.00000E+00	
04 Np-239	U.00000E+00	1.00000E+00	
15 Np-240	0.00000E+00	1.00000E+00 1.00000E+00	
07 Pu-240	0.00000E+00	1.00000E+00	
08 Pu-241	0.00000E+00	1.00000E+00	
01 I-135	0.00000E+00	1.00000E+00	
02 Xe-135	0.00000E+00	1.00000E+00	
JI Nd-149 02 Pm-149	U.UUUUUE+00	1.00000E+00	
03 Sm-149	0 00000E+00	1 00000E+00	

501	Eu-157	0.00000E+00	1.00000E+00
502	Gd-157	0.00000E+00	1.00000E+00
601	DHG-01	0.00000E+00	1.00000E+00
602	DHG-02	0.00000E+00	1.00000E+00
603	DHG-03	0.00000E+00	1.00000E+00
604	DHG-04	0.00000E+00	1.00000E+00
605	DHG-05	0.00000E+00	1.00000E+00
606	DHG-06	0.00000E+00	1.00000E+00
607	DHG-07	0.00000E+00	1.00000E+00
608	DHG-08	0.00000E+00	1.00000E+00
609	DHG-09	0.00000E+00	1.00000E+00
610	DHG-10	0.00000E+00	1.00000E+00
611	DHG-11	0.00000E+00	1.00000E+00

=RK= DECAY DATA FOR 34 ISOTOPES

Decay Decay Yield Fraction							
		Decay	Heat	Constant			
i	Isotope	[J/decay]	[MeV/decay]	[1/s]	Isotope	Yield [-]	
101	Th-232	0.00000E+00	0.00000E+00	0.00000E+00			
102	Th-233	1.99000E-13	1.24220E+00	5.23000E-04	Pa-233	1.00000E+00	
103	Th-234	4.37000E-14	2.72784E-01	3.33000E-07	Pa-234	1.00000E+00	
104	Pa-233	9.15000E-14	5.71161E-01	2.93000E-07	U-233	1.00000E+00	
105	Pa-234	3.52000E-13	2.19725E+00	2.87000E-05	U-234	1.00000E+00	
106	U-233	0.00000E+00	0.00000E+00	0.00000E+00			
107	U-234	0.00000E+00	0.00000E+00	0.00000E+00			
108	U-235	0.00000E+00	0.00000E+00	0.00000E+00			
201	U-238	0.00000E+00	0.00000E+00	0.00000E+00			
202	U-239	2.03000E-13	1.26717E+00	5.02000E-04	Np-239	1.00000E+00	
203	U-240	6.22000E-14	3.88265E-01	1.38000E-05	Np-240	1.00000E+00	
204	Np-239	1.16000E-13	7.24095E-01	3.44000E-06	Pu-239	1.00000E+00	
205	Np-240	3.52000E-13	2.19725E+00	1.93000E-04	Pu-240	1.00000E+00	
206	Pu-239	0.00000E+00	0.00000E+00	0.00000E+00			
207	Pu-240	0.00000E+00	0.00000E+00	0.00000E+00			
208	Pu-241	3.36000E-15	2.09738E-02	1.67000E-09			
301	I-135	4.24000E-13	2.64669E+00	2.93000E-05	Xe-135	1.00000E+00	
302	Xe-135	1.84000E-13	1.14856E+00	2.10700E-05			
401	Nd-149	2.71000E-13	1.69164E+00	9.63000E-05	Pm-149	1.00000E+00	
402	Pm-149	1.71000E-13	1.06742E+00	3.57000E-06	Sm-149	1.00000E+00	
403	Sm-149	0.00000E+00	0.00000E+00	0.00000E+00			
501	Eu-157	2.18000E-13	1.36080E+00	1.27000E-05	Gd-157	1.00000E+00	
502	Gd-157	0.00000E+00	0.00000E+00	0.00000E+00			
601	DHG-01	3.84000E-13	2.39700E+00	1.77000E+00	DHG-02	1.00000E+00	
602	DHG-02	3.84000E-13	2.39700E+00	5.77000E-01	DHG-03	1.00000E+00	
603	DHG-03	3.84000E-13	2.39700E+00	6.74000E-02	DHG-04	1.00000E+00	
604	DHG-04	3.84000E-13	2.39700E+00	6.21000E-03	DHG-05	6.02000E-01	
605	DHG-05	3.84000E-13	2.39700E+00	4.74000E-04	DHG-06	5.54000E-01	
606	DHG-06	3.84000E-13	2.39700E+00	4.81000E-05	DHG-07	3.58000E-01	
607	DHG-07	3.84000E-13	2.39700E+00	5.34000E-06	DHG-08	7.10000E-01	
608	DHG-08	3.84000E-13	2.39700E+00	5.73000E-07	DHG-09	7.00000E-01	
609	DHG-09	3.84000E-13	2.39700E+00	1.04000E-07	DHG-10	5.06000E-01	
610	DHG-10	3.84000E-13	2.39700E+00	2.96000E-08	DHG-11	1.00000E-01	
611	DHG-11	3.84000E-13	2.39700E+00	7.59000E-10			

=RK= NEUTRON CAPTURE DATA FOR 34 ISOTOPES

		N. Capture	N. Capture	N. Captu	re Yield Fraction(s)
		cross sec.	cross sec.		
i	Isotope	[barn]	[m2]	Isotope	Yield [-]
101	Th-232	6.54100E+00	6.54100E-28	Th-233	1.00000E+00
102	Th-233	1.40000E+03	1.40000E-25	Th-234	1.00000E+00
103	Th-234	0.00000E+00	0.00000E+00		
104	Pa-233	3.60600E+01	3.60600E-27	Pa-234	1.00000E+00
105	Pa-234	0.00000E+00	0.00000E+00		
106	U-233	4.18400E+01	4.18400E-27	U-234	1.00000E+00
107	U-234	9.06100E+01	9.06100E-27	U-235	1.00000E+00
108	U-235	8.64400E+01	8.64400E-27		
201	U-238	1.87867E+01	1.87867E-27	U-239	1.00000E+00
202	U-239	2.20000E+01	2.20000E-27	U-240	1.00000E+00
203	U-240	0.00000E+00	0.00000E+00		
204	Np-239	3.28600E+01	3.28600E-27	Np-240	1.00000E+00
205	Np-240	0.00000E+00	0.00000E+00	-	

206 Pu-239 207 Pu-240 208 Pu-241 301 I-135 302 Xe-135 401 Nd-149 402 Pm-149 403 Sm-149 501 Eu-157 502 Gd-157 601 DHG-01 602 DHG-02 603 DHG-03 604 DHG-04 605 DHG-05 606 DHG-06 607 DHG-07 608 DHG-08 609 DHG-09 610 DHG-10 611 DHG-11	2.74800E+02 2.63000E+02 3.28200E+02 0.0000E+00 2.72200E+06 0.00000E+00 1.24300E+03 6.15300E+04 1.68600E+02 1.91600E+05 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	2.74800E-26 2.63000E-26 3.28200E-26 0.0000E+00 2.72200E-22 0.0000E+00 1.24300E-25 6.15300E-24 1.68600E-26 1.91600E-23 0.00000E+00 0.00000E+00 0.0000E+00 0.0000E+00 0.000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+00 0.0000E+	Pu-240 Pu-241	1.00000E+00 1.00000E+00
-rv- 11221(	DAIA EUK 3	T ISUIUPES	Disclar	Vield Deschier ( )
i Isotope 101 Th-232 102 Th-233 103 Th-234 104 Pa-233	Fission cross sec. [barn] 0.00000E+00 0.00000E+00 0.00000E+00	Fission cross sec. [m2] 0.00000E+00 0.00000E+00 0.00000E+00	Fission Isotope	Yield Fraction(s) Yield [-]
105 Pa-234 106 U-233	0.00000E+00 4.64700E+02	0.00000E+00 4.64700E-26	I-135 Xe-135 Nd-149 Eu-157 Gd-157 DHG-01 DHG-02 DHG-03 DHG-04  Total:	4.41000E-02 1.47000E-02 7.60000E-03 6.70000E-05 7.20000E-08 2.39200E-01 4.20800E-01 5.80000E-01 3.08000E-01  1.61447E+00
107 U-234 108 U-235	0.00000E+00 5.05000E+02	0.00000E+00 5.05000E-26	I-135 Xe-135 Nd-149 Eu-157 Gd-157 DHG-01 DHG-02 DHG-03 DHG-04  Total:	6.32000E-02 2.60000E-03 1.05000E-02 6.30000E-05 2.20000E-09 2.39200E-01 4.20800E-01 5.80000E-01 3.08000E-01 
201 U-238 202 U-239	0.00000E+00 1.40000E+01	0.00000E+00 1.40000E-27	I-135 Xe-135 Nd-149 Eu-157 Gd-157 DHG-01 DHG-02 DHG-03 DHG-04  Total:	6.32000E-02 2.60000E-03 1.05000E-02 6.30000E-05 2.20000E-09 2.39200E-01 4.20800E-01 5.80000E-01 3.08000E-01 
203 U-240 204 Np-239	0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00		
-				

205 Np-240 206 Pu-239	0.00000E+00 6.98900E+02	0.00000E+00 6.98900E-26	I-135 Xe-135 Nd-149 Eu-157 Gd-157 DHG-01 DHG-02 DHG-03 DHG-04  Total:	6.19000E-02 1.04000E-02 1.25000E-02 7.50000E-04 3.00000E-07 1.60000E-01 3.00000E-01 5.80000E-01 3.08000E-01 			
207 Pu-240 208 Pu-241	0.00000E+00 9.46100E+02	0.00000E+00 9.46100E-26	I-135 Xe-135 Nd-149 Eu-157 Gd-157 DHG-01 DHG-02 DHG-03 DHG-04  Total:	7.07000E-02 2.10000E-03 1.46000E-02 2.70000E-03 4.30000E-08 1.60000E-01 3.00000E-01 3.08000E-01 3.08000E-01 			
301 I-135 302 Xe-135 401 Nd-149 402 Pm-149 403 Sm-149 501 Eu-157 502 Gd-157 601 DHG-01 602 DHG-02 603 DHG-03 604 DHG-04 605 DHG-06 607 DHG-07 608 DHG-08 609 DHG-09 610 DHG-10 611 DHG-11	0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00	0.00000E+00 0.0000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00					
=RK= NO FU	JEL ELEMENT REM	OVAL					
=RK= FUEL	LOADING FUNCTI	ONS					
NODE No. 1	LOADING FUNCT 1 CF-002	ION No.					
=RK= INIT:	IAL FUEL COMPOS	ITION DATA					
Initial Mass Initial Nuclide Fraction Concentration i Isotope [-] [1/m3] 106 U-233 0.00000E+00 0.00000E+00 108 U-235 1.00000E+00 1.66337E+25 202 U-239 0.00000E+00 0.00000E+00 206 Pu-239 0.00000E+00 0.00000E+00 208 Pu-241 0.00000E+00 0.00000E+00							
=RK= LOAD	ING FUNCTION NO	.: 1	1 10112				
Concentrat	ion of Isotops	in					
Assemblies	Concentration	uring Transie	nt				

====: =RK:	16 IT 21 IT 26 IT 31 IT ====================================	'-208 '-403 '-603 '-608 ========	22 27 32 =====	IT-301 IT-501 IT-604 IT-609	23 28 33	IT-502 IT-502 IT-605 IT-610	24 29 34	IT-601 IT-606 IT-611	20 25 30	IT-602 IT-607
	16 IT 21 IT 26 IT 31 IT	2-208 2-403 2-603 2-608	17 22 27 32	IT-501 IT-501 IT-604 IT-609	23 28 33	IT-502 IT-605 IT-610	24 29 34	IT-601 IT-606 IT-611	20 25 30	IT-602 IT-607
	16 II 21 II 26 II 31 II	2-208 2-403 2-603 2-608	17 22 27 32	IT-501 IT-501 IT-604 IT-609	23 28 33	IT-502 IT-502 IT-605 IT-610	24 29 34	IT-601 IT-606 IT-611	20 25 30	IT-602 IT-607
	16 IT 21 IT 26 TT	-208 -403 -603	17 22 27	IT-501 IT-501 IT-604	23	IT-502 IT-502	24 29	IT-601	20 25 30	IT-602 IT-602
	16 IT	-208	1/	IT-301	10	TT 502	19	TT 101	20	TT (02
			17	· m ·)∩1	10	LLL-303	10	rm=401	20	iπ_402
	11 IT	-203	12	IT-204	13	IT-205	14	IT-206	15	IT-207
	6 IT	-106	7	IT-107	8	IT-108	9	IT-201	10	IT-202
	1 IT	-101	2	IT-102	3	IT-103	4	IT-104	5	IT-105
	Int. R No.	No.	Int. No.	Ref. No.	Int. No.	Ref. No.	Int. No.	Ref. No.	Int. No.	Ref. No.
=====										
===== =RK:	======================================	E INTERN	NAL NU	JMBERING	SCHEME					
208	Pu-239 Pu-241	0.00000	0E+00	0.00000	)E+00					
202	U-239 P11-230	0.00000	0E+00	0.00000	)ビ+00 )E+00					
108	U-235	2.00000	0E+00	3.32673	BE+25					
106	U-233	0.00000	0E+00	0.00000	)E+00					
i	Isotope	[-]	]	[1/m3	8]					
		Mass Fract	s ion	Concentr	ation					
		M	~	Maren 1.4						
Fue	l Composi	tion in	Asser	nblies Be	ing Lo	aded Dur	ing Tra	nsient		
θII	DHG-11	0.0000	UE+00							
610	DHG-10	0.00000	0E+00							
609	DHG-09	0.0000	0E+00							
608	DHG-08	0.00000	0E+00							
605 607	DHG-06 DHG-07	0.00000	05+00 05+00							
605	DHG-05	0.00000	0E+00							
604	DHG-04	0.0000	0E+00							
603	DHG-03	0.00000	0E+00							
601 602	DHG-01	0.00000	0E+00							
502	Gd-157	0.0000	0E+00							
501	Eu-157	0.0000	0E+00							
403	Sm-149	0.00000	0E+00							
401	Nd-149 Pm-149	0.00000	UE+00							
302	Xe-135	0.00000	0E+00							
301	I-135	0.0000	0E+00							
208	Pu-241	0.00000	0E+00							
200 207	Pu-239 Pu-240	0.00000	0E+00							
205 206	NP-240 Pu-239	0.00000	05+00 05+00							
204	Np-239	0.00000	UE+00							
203	U-240	0.00000	0E+00							
202	U-239	0.0000	0E+00							
201	U-238	1.33069	9E+26							
108	U-235	3.32673	3E+25							
107	U-234	0.00000	0E+00							
105	II-233	0.00000	DE+00							
104	Pa=233 Pa=234	0.00000	0E+00							
103	Th-234	0.00000	0E+00							
102	Th-233	0.00000	0E+00							
101	Th-232	0.0000	0E+00							
i	Isotope	[1/r	m3]							

An example of the Reactor Kinetics transient printout is shown below. The letter f, in the isotope printout, signifies a fissile isotope.

=RK= OUTPUT DATA FOR POINT REACTOR KINETICS MODEL, AT TIME : -8.64000E+04 [s] =RK= NEUTRON POWER (FISSION POWER) DATA Neutron Neutron Neutron External Neutron Flux Neutron Source Power Node Density Velocity [1/m3] [m/s] [1/m2/s] [1/s] [W] No. 1.09575E+14 2.56000E+03 2.80511E+17 0.00000E+00 3.75000E+07 1 =RK= REACTOR AVERAGE PARAMETERS Fuel Moderator Void Temperature Fraction Node Temperature No. [K] [K] [-] 1 1.37339E+03 1.34908E+03 1.00000E+00 =RK= REACTIVITY DATA Current Control Rod Temp.&Void Isotope Change Bias Node Reactivity Reactivity Feedback Feedback Reactivity No. [\$] [\$] [\$] [\$] [\$] 0.00000E+00 0.00000E+00 -1.17103E+01 2.92344E+01 -1.75241E+01 1 =RK= MULTIPLICATION FACTOR DATA K-eff Node [-] No. 1.00000E+00 1 =RK= MACROSCOPIC FISSION CROSS SECTION DATA Node SigmaF (1/m) No. [-] 1 8.40000E-01 =RK= DATA FOR 6 DELAYED NEUTRON PRECURSORS Node No.: 1 Group Concentration No. [1/m3] 3.24011E+15 1 2 8.50251E+15 3 2.08949E+15 1.55928E+15 4 5 1.20148E+14 6 1.63816E+13 =RK= DATA FOR 34 ISOTOPES AT TIME : -8.64000E+04 [s] Node No.: 1 Nuclide Reactivity Reactivity Decav Heat Density Change [1/m3] [W/m3] i Isotope [\$] [\$] 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 101 Th-232 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 102 Th-233 Th-234 103 104 Pa-233 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 Pa-234 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 105 106 f U-233 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 107 U-234 108 f U-235 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 1.66337E+25 0.00000E+00 6.07781E+01 0.00000E+00 U-238 1.49703E+26 0.00000E+00 -2.66063E+01 0.00000E+00 201 202 f U-239 203 U-240 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 204 Np-239 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 205 Np-240 0.00000E+00 0.00000E+00 0.00000E+00 0.00000E+00 206 f Pu-239 0.00000E+00 207 Pu-240 208 f Pu-241 301 I-135 5.08252E+20 6.31411E+03 0.00000E+00 0.00000E+00 Xe-135 1.59142E+20 6.16974E+02 -4.09802E+00 0.00000E+00 302 2.56917E+19 6.70483E+02 0.00000E+00 0.00000E+00 401 Nd-149 Pm-149 6.86324E+20 4.18980E+02 -8.07054E-03 0.00000E+00 402

102	0	1 410500.01	0 0000000000000000000000000000000000000	0 0 0 0 0 0 1	0 00000000000
403	SIN-149	1.419585+21	0.000008+00	-0.20322E-UI	0.000005+00
501	Eu-157	1.16843E+18	3.23493E+00	-1.86365E-06	0.00000E+00
502	Gd-157	2.76107E+18	0.00000E+00	-5.00467E-03	0.00000E+00
601	DHG-01	3.18432E+16	2.16432E+04	0.00000E+00	0.00000E+00
602	DHG-02	2.69524E+17	5.97179E+04	0.00000E+00	0.00000E+00
603	DHG-03	4.33502E+18	1.12197E+05	0.00000E+00	0.00000E+00
604	DHG-04	5.87366E+19	1.40066E+05	0.00000E+00	0.00000E+00
605	DHG-05	4.63253E+20	8.43195E+04	0.00000E+00	0.00000E+00
606	DHG-06	2.52907E+21	4.67130E+04	0.00000E+00	0.00000E+00
607	DHG-07	8.15546E+21	1.67233E+04	0.00000E+00	0.00000E+00
608	DHG-08	5.39626E+22	1.18735E+04	0.00000E+00	0.00000E+00
609	DHG-09	2.08119E+23	8.31146E+03	0.00000E+00	0.00000E+00
610	DHG-10	3.70003E+23	4.20560E+03	0.00000E+00	0.00000E+00
611	DHG-11	1 44296E+24	4 20560E+02	0 00000E+00	0 00000E+00
011	DIIG II				
		1.68426E+26	5.14215E+05	2.92344E+01	0.00000E+00
=RK=	MISCELLA	NEOUS DATA			
	Fissi	on Fissi	ion De	ecav I	otal
Node	Cross-	sec. Powe	er Po	ower F	ower
No.	[1/m]	ן שו		[W]	[W]
1	8.400001	E-01 3.75000	)E+07 2.648	B21E+06 4.01	482E+07
-	0.100000		2.01		1022.07
=RK=	FUEL LOAD	DING FUNCTIONS	3		
Node	Reload :	rates [1/s] fo	r. 1 funct:	ions	
No	1	14000 [1/0] 10	JI. I LUNCE	10115	
1		F+00			
1	0.00000				

#### 3.1.10 Material Property Output

An example of a Material Property data printout is shown below.

\_\_\_\_\_

#### 3.1.11 Transient Solution (SOLVER) Data

An example of a the SOLVER input data printout is shown below.

=SL= SOLVER INPUT DATA FOR 1 TIME STEP DOMAINS \_\_\_\_\_ =SL= TIME STEP DOMAIN NO.: 1 MAXIMUM TIME STEP FOR THIS DOMAIN: 1.00000E-01 (S) MINIMUM TIME STEP FOR THIS DOMAIN: 1.00000E-04 (S) PRINT FREQUENCY FOR THIS DOMAIN: 5.00000E+00 (S)PLOT FREQUENCY FOR THIS DOMAIN: 1.00000E+00 (S)END TIME FOR THIS DOMAIN: 5.00000E+00 (S) END TIME FOR THIS DOMAIN \_\_\_\_\_ =SL= SOLVER INPUT DATA \_\_\_\_\_ \_\_\_\_\_ =SL= START TIME: -8.64000E+04 =SL= SCREEN MESSAGE FREQUENCY: 1.00000E+00 =SL= ADVANCEMENT MESSAGE FREQUENCY: 10 =SL= EXTENDED DIAGNOSTICS NOT REQUESTED =SL= DEBUG PRINTOUT NOT REQUESTED =SL= MESSAGES WRITTED TO \*.MES FILE =SL= TTERATION DATA MAX.NO.OF ITER. TO CUT TIME STEP BY DTREDN, MAXITR = 50 MIN.NO.OF ITER. TO INCREASE TIME STEP BY DTINC, MINITR = 20 MINIMUM NO.OF ITER. TO ACCEPT THE SOLUTION, ITMNSL = TIME STEP REDUCTION FACTOR IN CASE OF NONCONV. DTREDN = 4.00000E+00 TIME STEP REDUCTION FACTOR IN CASE OF FAILURE, DTREDF = 8.00000E+00 DTINC = 1.30278E+00 TIME STEP INCREASE FACTOR IF ITER < MINITR, ACTION ON FAILURE DURING TRANSIENT : TERMINATE THE RUN ACTION ON FAILURE DURING INITIAL STATE: TERMINATE THE RUN MAIN CONVERGENCE CRITERIA : - CALCULATED-ASSUMED : CCCASL = 1.00000E-03 - ASSUMED-ASSUMED : CCAASL = 1.00000E-04 - RK MULT. CAL.-ASS. : CMCASL = 1.00000E+00 - RK MULT. ASS.-ASS. : CMAASL = 1.00000E+00 - ABSOLUTE LIMIT : ABSLSL = 1.00000E-10 - INITIAL DISTURBANCE: DISTIN = 1.00000E-02 - ABSOLUTE LIMIT FISSION PRODUCT CONVERGENCE CRITERIA : CALCULATED-ASSUMED : FCCASL = 1.00000E+01
 ASSUMED-ASSUMED : FCAASL = 1.00000E+00
 ABSOLUTE LIMIT : FABLSL = 1.00000E-30
 MAX. ITERATIONS : ITMXSL = 15 - MAX. ITERATIONS : ITMXSL = 15 - MASS ERROR TREATM. : IFPESL = -1 (MASS ERROR ALLOWED) =SL= IDIAFL = 0 : WARNING AND ERROR MESSAGES ARE WRITTEN TO THE DIAGNOSTICS FILE DURING THE CALCULATIONS =SL= ITSNSL = 1 : TIME STEP IS NOT ADJUSTED AT THE END OF EACH TIME STEP DOMAIN =SL= SIMULATOR OPTION : INACTIVE (ISIMUL<=0) =SL= SCRAMBLING OF INPUT: NOT NEEDED (ISCRMB<=0) =SL= MODEL EXPORTING : NOT NEEDED (IEXPSL=0) =SL= INITIAL CONDITIONS ARE READ FROM THE INITIAL CONDITION FILE: ./SS-CP.ICF

An example of the SOLVER transient output is shown below.

=SL= SOLVER OUTPUI	AT TIME: 5.10000E+0	0, ADVANCEMENT NUM	BER: 51
=SL= MAIN ITERATIC	N PARAMETERS		
PACKAGE	VARIABLE	ITERATIONS TO CONV	ERGE
Control Volume Control Volume Control Volume Control Volume Control Volume Control Volume Control Volume Control Volume Control Volume Control Volume CV Junction CV Junction 1-D H. Conductor	Atms mass, kg, Bubble mass, kg, Droplet mass, kg, Pool mass, kg, Energy, J/kg, No.of bubb, No.of drops, -, Bubb.posit. m, Droplet pos. m, Pressure Pa, Velocity, m/s, Pressure, Pa, T(left), K,	4 5 4 3 6 4 3 3 3 3 1 1 1 1 2	
1-D H. Conductor 2-D H. Conductor Control Function Reactor Kinetics Reactor Kinetics	T(right), K, T(boundary), K, CF value, Neutron concent. Precur. concent.	3 1 1 1 1	

\_\_\_\_\_

At the end of the calculations SOLVER prints the run statistics. An example of this printout is shown below.

=SL= RUN STATISTICS Analyzed model time (s) : 5.10 ( 0.142E-02 (hrs) ) CPU time (s) : 0.734 ( 0.204E-03 (hrs) ) Warp factor (model/CPU) : 6.94 Minimum time step (s) : 0.100 Maximum time step (s) : 0.100 Average time step (s) : 0.100 No. of advancements 51 CPU per advancement (s) : 0.144E-01

#### 3.2 Description of the Diagnostics File (\*.DIA)

An example of the diagnostics file is shown below. The diagnostics file contains all warning and error messages produced during:

- input processing,
- transient calculations.
- All error messages are preceded by "\*\*\*\*\*". All warning messages are preceded by "\* \* \*".

Furthermore, the diagnostics file contains information about every time step advancement, including:

- advancement number,
- time at the start of the advancement, (s),
- time at the end of the advancement, (s),
- time step, (s),
- number of iterations required to complete the advancement,
- CPU time and run time (s).

When the run is terminated, the run statistics is written to the diagnostics file.

```
_____
SPECTRA - Sophisticated Plant Evaluation Code for
                  Thermalhydraulic Response Assessment
                 Version 2.00 (c) MSt, October 2003
                                                _____
_____
Input data diagnostics
                                               _____
 * * * = IN= WARNING: TOO MANY ENTRIES IN RECORD: 302001
                        EXCESSIVE ITEMS ( 2 - 2) OMITTED
                        **** NOTE !
                        THIS WARNING INDICATES THAT THERE MIGHT BE AN ERROR
                        IN THIS RECORD. CHECK CAREFULLY THE ENTIRE INPUT RECORD.
SPECTRA - Sophisticated Plant Evaluation Code for
                 Thermalhydraulic Response Assessment
                 Version 2.00 (c) MSt, October 2003
Transient diagnostics for the problem:
CV example
               _____

      0
      T (beg) = 0.000E+00
      T (end) = 0.000E+00
      dT = 1.000E+99
      Iter:
      4
      CPU= 0.000E+00

      1
      T (beg) = 0.000E+00
      T (end) = 1.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.125E-01

      2
      T (beg) = 1.000E-01
      T (end) = 2.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.281E-01

      3
      T (beg) = 2.000E-01
      T (end) = 3.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.281E-01

      4
      T (beg) = 3.000E-01
      T (end) = 4.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.281E-01

      5
      T (beg) = 4.000E-01
      T (end) = 5.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.438E-01

      6
      T (beg) = 5.000E-01
      T (end) = 6.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.438E-01

      7
      T (beg) = 6.000E-01
      T (end) = 7.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.438E-01

      8
      T (beg) = 7.000E-01
      T (end) = 7.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.594E-01

      8
      T (beg) = 8.000E-01
      T (end) = 9.000E-01
      dT = 1.000E-01
      Iter:
      7
      CPU= 3.594E-01

Adv:
 Adv:
 Adv:
Adv:
Adv:
Adv:
Adv:
Adv:
 Adv.
 Adv:
Adv:
 * * * = CV= WARNING IN EQM6CV, CALCULATING CV TABULAR MASS SOURCES:
                        CV-001, MASS SOURCE: 1
POSITIVE MASS SOURCE, Wtotal = 5.00000E-02
                        SOURCE PRESSURE BELOW CV PRESSURE
                        P(Source) = 1.00000E+05
P(CV) = 1.05000E+05
                        WARNING FOR : Control Volume No.:
                                                                                             1
  _____
                                                     _____
 * * * =CV= WARNING IN EQM6CV, CALCULATING CV TABULAR MASS SOURCES:
                        CV-001, MASS SOURCE: 2
POSITIVE MASS SOURCE; Wtotal = 5.00000E-02
                        SOURCE PRESSURE BELOW CV PRESSURE
                        P(Source) = 1.00000E+05
P(CV) = 1.05000E+05
```

1

```
K6223/24.277594 MSt-2402
```

WARNING FOR : Control Volume No.:

Adv:       11       T(beg) = 1.000E+00       T(end) = 1.100E+00       dT = 1.000E-01       Iter:       14       CPU= 3.         Adv:       12       T(beg) = 1.100E+00       T(end) = 1.200E+00       dT = 1.000E-01       Iter:       15       CPU= 4.         Adv:       13       T(beg) = 1.200E+00       T(end) = 1.300E+00       dT = 1.000E-01       Iter:       12       CPU= 4.	906E-01 062E-01
Adv:         12         T(beg) = 1.100E+00         T(end) = 1.200E+00         dT = 1.000E-01         Iter:         15         CPU= 4.           Adv:         13         T(beg) = 1.200E+00         T(end) = 1.300E+00         dT = 1.000E-01         Iter:         12         CPU= 4.	062E-01
Adv: 13 T(beg) = 1.200E+00 T(end) = 1.300E+00 dT= 1.000E-01 Iter: 12 CPU= 4.	0628-01
	0028 01
Adv: 14 $T(beg) = 1.300E+00$ $T(end) = 1.400E+00$ dT = 1.000E-01 Iter: 10 CPU= 4.	219E-01
Adv: 15 T(beg) = 1.400E+00 T(end) = 1.500E+00 dT= 1.000E-01 Iter: 9 CPU= 4.	219E-01
Adv: 16 T(beg) = 1.500E+00 T(end) = 1.600E+00 dT= 1.000E-01 Iter: 9 CPU= 4.	375E-01
Adv: 17 T(beg) = 1.600E+00 T(end) = 1.700E+00 dT= 1.000E-01 Iter: 11 CPU= 4.	531E-01
Adv: 18 T(beg) = 1.700E+00 T(end) = 1.800E+00 dT= 1.000E-01 Iter: 11 CPU= 4.	531E-01
Adv: 19 T(beg) = 1.800E+00 T(end) = 1.900E+00 dT= 1.000E-01 Iter: 11 CPU= 4.	688E-01
Adv: 20 T(beg) = 1.900E+00 T(end) = 2.000E+00 dT= 1.000E-01 Iter: 11 CPU= 4.	844E-01
Adv: 21 T(beg) = 2.000E+00 T(end) = 2.100E+00 dT= 1.000E-01 Iter: 8 CPU= 4.	844E-01
Adv: 22 T(beg) = 2.100E+00 T(end) = 2.200E+00 dT= 1.000E-01 Iter: 9 CPU= 5.	000E-01
Adv: 23 T(beg) = 2.200E+00 T(end) = 2.300E+00 dT= 1.000E-01 Iter: 8 CPU= 5.	000E-01
Adv: 24 T(beg) = 2.300E+00 T(end) = 2.400E+00 dT= 1.000E-01 Iter: 8 CPU= 5.	156E-01
Adv: $25 \text{ T}(\text{beg}) = 2.400\text{ F}(-00 \text{ T}(\text{end}) = 2.500\text{ F}(-00 \text{ d}) = 1.000\text{ F}(-01 \text{ T}(\text{end}) = 2.500\text{ F}(-00 \text{ d}) = 1.000\text{ F}(-01 \text{ T}(\text{end}) = 2.500\text{ F}(-00 \text{ d}) = 1.000\text{ F}(-01 \text{ d}) = 1.000$	156E-01
Adv: 26 $T(beg) = 2.500F+00$ $T(end) = 2.600F+00$ dT= 1.000F-01 Iter: 8 CPU= 5	312E-01
Adv: $27 \text{ T}(\text{beg}) = 2.600\text{ F}(00 \text{ T}(\text{end}) = 2.700\text{ F}(00 \text{ dT} = 1.000\text{ F}(01 \text{ T}(\text{end}) = 2.700\text{ F}(01 \text{ dT} = 1.000\text{ F}(01 \text{ dT} = 1.000\text{ dT} = 1$	312E-01
Adv: 28 $T(beg) = 2.700F+00$ $T(end) = 2.800F+00$ dT= 1.000F=01 Iter: 10 CPU=5	469E-01
Adv. 20 $T(\text{beg}) = 2.800\text{F}(0) T(\text{eng}) = 2.800\text{F}(0) dT = 1.000\text{F}(0) T(\text{eng}) = 2.800\text{F}(0) dT = 1.000\text{F}(0) T(\text{eng}) = 2.800\text{F}(0) dT = 1.000\text{F}(0) dT = 1.000$	469E-01
Adv. 25 $\Gamma(\text{beg}) = 2.000 \text{ From } 0.000 \text{ from } 0.000 \text{ from } 0.0000 \text{ from } 0.0000 \text{ from } 0.0000000000000000000000000000000000$	625E-01
Adv. $50 \text{ (beg)} = 2.900 \text{ (bid)} = 3.0000 \text{ (d} = 1.0000 \text{ -01 lter.} 0 \text{ CFU} = 5.0000 \text{ -01 lter.} 0 \text{ -01 lter.} $	625E 01
Adv. $S1 = (beg) = 5.00 E + 00 = 1(E + d) = 5.100 E + 00 d = 1.00 E - 01 = 1 + 0.00 E + 0.00$	7010 01
Adv: $32 \text{ (Deg)} = 3.100 \text{ ETO} \text{ (ella)} = 3.200 \text{ ETO} \text{ all } 1.000 \text{ EOI} \text{ Iter:} \text{ o CPU} = 3.200 \text{ ETO} \text{ all } 1.000 \text{ EOI} \text{ Iter:} \text{ o CPU} = 3.200 \text{ ETO} \text{ all } 1.000 \text{ EOI} $	7010 01
Adv: $35 \text{ i}(\text{Beg}) = 5.200\text{ET00} \text{ i}(\text{ell}) = 2.300\text{ET00} \text{ dl} = 1.000\text{E-01} \text{ i}(\text{ell}) = 0.000\text{ s}$	020E 01
Adv: $34 \ (\text{Deg}) = 3.300 \text{ETO} \ 1 \ (\text{elg}) = 3.400 \text{ETO} \ d= 1.000 \text{ETO} \ 1 \ \text{terr}; \ 0 \ \text{CPU} = 3.$	020E-01
Adv: $35 \text{ [(beg)]} = 3.400 \text{ EVO} \text{ [(end)]} = 3.500 \text{ EVO} \text{ dim} \text{ [1,000 E-01] [ter: 8 CPU= 5.}$	938E-UI
Adv: $36 \text{ f}(\text{Deg}) = 3.500\text{E}+00 \text{ f}(\text{end}) = 3.500\text{E}+00 \text{ d} = 1.000\text{E}+01 \text{ iter: } 8 \text{ CPU= } 6.$	094E-01
Adv: $37 + (beg) = 3.800E+00 + (eng) = 3.700E+00 + d1 = 1.000E-01 + ter: 8 CPU = 6.$	094E-01
Adv: 38 $T(beg) = 3.700E+00$ $T(eng) = 3.800E+00$ $dT = 1.000E-01$ Iter: 8 CPU= 6.	250E-01
Adv: $39 \text{ T}(\text{beg}) = 3.800\text{E}+00 \text{ T}(\text{eng}) = 3.900\text{E}+00 \text{ dr} = 1.000\text{E}-01 \text{ tter: } 8 \text{ CPU= 6.}$	250E-01
Adv: 40 $T(beg) = 3.900E+00$ $T(eng) = 4.000E+00$ $dT = 1.000E-01$ Iter: 8 CPU= 6.	406E-01
Adv: 41 $T(beg) = 4.000E+00$ $T(eng) = 4.100E+00$ $dT = 1.000E-01$ Iter: 8 CPU= 6.	406E-01
Adv: $42 \text{ T}(beg) = 4.100 \text{ E}(b) \text{ T}(ena) = 4.200 \text{ E}(b) \text{ are } 1.000 \text{ E}(c) \text{ T}(ena) = 4.200 \text{ E}(c) \text{ are } 1.000 \text{ e}(c) \text{ are }$	562E-UI
Adv: 43 $T(beg) = 4.200E+00$ $T(end) = 4.300E+00$ $dT = 1.000E-01$ Iter: 8 CPU= 6.	562E-01
Adv: 44 T(beg) = 4.300E+00 T(end) = 4.400E+00 dT = 1.000E-01 Iter: 8 CPU= 6.	/19E-01
Adv: 45 T(beg) = 4.400E+00 T(end) = 4.500E+00 dT = 1.000E-01 Iter: 8 CPU= 6.	/19E-01
Adv: 46 $T(beg) = 4.500E+00$ $T(end) = 4.600E+00$ dT = 1.000E-01 Iter: 8 CPU= 6.	875E-01
Adv: $47 \text{ T}(beg) = 4.600\text{ E}+00 \text{ T}(end) = 4.700\text{ E}+00 \text{ dT} = 1.000\text{ E}-01 \text{ Iter: } 8 \text{ CPU= 6.}$	875E-01
Adv: 48 $T(beg) = 4.700E+00$ $T(end) = 4.800E+00$ $dT = 1.000E-01$ Iter: 7 CPU= 7.	031E-01
Adv: 49 $T(beg) = 4.800E+00$ $T(end) = 4.900E+00$ dT = 1.000E-01 Iter: 7 CPU= 7.	031E-01
Adv: 50 $T(beg) = 4.900E+00$ $T(end) = 5.000E+00$ dT = 1.000E-01 Iter: 7 CPU= 7.	188E-01
Adv: 51 T(beg) = 5.000E+00 T(end) = 5.100E+00 dT= 1.000E-01 Iter: 7 CPU= 7.	344E-01
-> END OF CALCULATIONS.	
-> RUN STATISTICS	
Analyzed model time (s) : 5.10 ( 0.142E-02 (hrs) )	
CPU time (s) : 0.734 (0.204E-03 (hrs))	
Warp factor (model/CPU) : 6.94	
Minimum time step (s) : 0.100	
Maximum time step (s) : 0.100	
Average time step (s) : 0.100	
No. of advancements 51	

In case when the debug printout is requested, the diagnostics file contains also the debug printout. It may be used in case of numerical problems, to find out how the iterations proceed. Debug printout is written to the diagnostics file every iteration. Thus an enormous amount of printout may be generated in a very short time. Therefore debug printout should be activated shortly before the time when the numerical problems are occurring.

An example of the debug printout is shown below. Debug printout gives four values for each variable controlled by the SOLVER: the assumed and obtained values, for the last two iterations.

Each variable that has not yet converged is distinguished in the output by the exclamation sign (!) in front of the variable name.

=SL= SOLVER DEBUG PRINTOUT ADV.: 51 T(beg)= 5.000E+00 T(end)= 5.100E+00 DT= 1.000E-01 ITER: 2

CPU per advancement (s) : 0.144E-01

		ASSUMED LAST ITER. ITER-1		LAST ITER. ITER-1			
Atms mass, kg, Atms mass, kg, !Atms mass, kg, !Atms mass, kg, !Atms mass, kg, Atms mass, kg,	CV-001 H2 CV-001 He CV-001 H20 CV-001 N2 CV-001 O2 CV-001 CO2	0.00000E+00 0.00000E+00 1.44343E-01 4.21229E+00 1.24880E+00 0.00000E+00	-1.00000E-04 -1.00000E-04 1.44251E-01 4.21162E+00 1.24991E+00 -1.00000E-04	0.00000E+00 0.00000E+00 1.44353E-01 4.21244E+00 1.24889E+00 0.00000E+00	0.00000E+00 0.0000E+00 1.44350E-01 4.21230E+00 1.24889E+00 0.00000E+00		
		ASSU LAST ITER.	IMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
Bubble mass, kg, Bubble mass, kg, !Bubble mass, kg, !Bubble mass, kg, Bubble mass, kg, Bubble mass, kg,	CV-001 H2 CV-001 He CV-001 H20 CV-001 N2 CV-001 O2 CV-001 CO2	0.00000E+00 0.00000E+00 7.40714E-03 2.98931E-01 0.00000E+00 0.00000E+00	-1.00000E-04 -1.00000E-04 7.35254E-03 2.96938E-01 -1.00000E-04 -1.00000E-04	0.00000E+00 0.00000E+00 7.55781E-03 3.02737E-01 0.00000E+00 0.00000E+00	0.00000E+00 0.00000E+00 7.55875E-03 3.02877E-01 0.00000E+00 0.00000E+00		
		ASSU LAST ITER.	JMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!Droplet mass,kg,	CV-001 drop	4.38730E-02	4.39026E-02	4.38985E-02	4.38749E-02		
		ASSU LAST ITER.	JMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!Pool mass, kg,	CV-001 pool	4.95749E+03	4.95699E+03	4.95750E+03	4.95750E+03		
		ASSU LAST ITER.	ITER-1	CALCU LAST ITER.	LATED ITER-1		
<pre>!Energy, J/kg, !Energy, J/kg, !Energy, J/kg, !Energy, J/kg,</pre>	CV-001 atms CV-001 drop CV-001 pool CV-001 bubb	2.94696E+05 3.07601E+05 1.75345E+05 2.99227E+05	2.94631E+05 3.07555E+05 1.75326E+05 2.98155E+05	2.94752E+05 3.07600E+05 1.75347E+05 2.69266E+05	2.94697E+05 3.07601E+05 1.75345E+05 2.99819E+05		
		ASSU LAST ITER.	JMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!No.of bubb,	CV-001	1.10401E+05	1.09680E+05	1.11749E+05	1.11749E+05		
		ASSU LAST ITER.	JMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!No.of drops, -,	CV-001	8.59410E+01	8.59639E+01	8.59416E+01	8.59416E+01		
		ASSU LAST ITER.	IMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!Bubb.posit. m,	CV-001	4.19171E+00	4.18809E+00	4.19205E+00	4.19205E+00		
		ASSU LAST ITER.	JMED ITER-1	CALCU LAST ITER.	LATED ITER-1		
!Droplet pos. m,	CV-001	3.33171E+00 P (Pa)	3.33472E+00 T (K)	3.33196E+00	3.33196E+00		
Thermodynamics,	CV-001 atms	1.10030E+05	3.19146E+02				
		Atms. Velc LAST VALUE	pcity, (m/s) PREV. VALUE	Pool Veloc LAST VALUE	ity, (m/s) PREV. VALUE		
Velocities,	JN-001	4.25023E-01	4.25139E-01	0.00000E+00	0.00000E+00		
		Atms. Pres LAST VALUE	sure, (Pa) PREV. VALUE	Pool Press LAST VALUE	ure, (Pa) PREV. VALUE		
Pressures,	CV-001	1.10030E+05 ASSU	1.09990E+05 JMED	1.10030E+05 CALCU	1.09990E+05 LATED		

			LAST	ITER.	ITER-1	L	AST ITEF	ι.	ITER-1	L
T(left),	к,	SC-001	3.15	002E+02	3.14971E+	02 3	.15002E+	02	3.15002E	S+02
T(left),	K,	SC-002	3.15	002E+02	3.14971E+	02 3	.15002E+	02	3.15002E	E+02
				ASSU	MED		CA	LCUL	ATED	
			LAST	ITER.	ITER-1	L	AST ITER	ι.	ITER-1	L
T(right),	к,	SC-001	3.15	 002E+02	3.14970E+	02 3	.15002E+	02	 3.15002E	 _+02
T(right),	к,	SC-002	3.15	002E+02	3.14970E+	02 3	.15002E+	02	3.15002E	E+02
				ASSU	MED		CA	LCUL	ATED	
			LAST	ITER.	ITER-1	L	AST ITER	ι.	ITER-1	L
Neutron conce	nt.	NC-000	0.00	D00E+00	0.00000E+	00 0	.00000E+	00	0.00000	2+00
						=====		====		

#### 3.3 Description of the Plot File (\*.PLT)

The SPECTRA plot file is written in a readable, ASCII format. The structure of the file is shown below. A simple post processing program: S-GRAPH, is provided for quick extract of plot data and arranging the in columns for plotting (with EXCEL or other plotting program). Use of S-GRAPH is described in section 3.3.1. A convenient visualization tool, program VISOR, is available for graphical presentation of SPECTRA results. Use of VISOR is illustrated in section 3.3.2.

An example of the plot file is shown below. The first record of the plot file contains information on how many plot variables are present in the file. In the present example the number of plot variables (NPLT) is equal to 26. The value of NPLT is written to the plot file using the format: ('NPLT =',I7) and can be read using for example the format: (8X,I7) (8 characters, integer number 7 fields wide).

NPLT	=	26								
	1.	SL-000-Time-	0000-s							
	2.	CV-100-Pres-	atms-Pa							
	3.	CV-200-Pres-	atms-Pa							
	4.	CV-300-Pres-	atms-Pa							
	5.	CV-400-Pres-	atms-Pa							
	6.	CV-500-Pres-	atms-Pa							
	7.	CV-100-Temp-	atms-K							
	8.	CV-200-Temp-	atms-K							
	9.	CV-300-Temp-	atms-K							
	10.	CV-400-Temp-	atms-K							
	11.	CV-500-Temp-	atms-K							
	12.	CV-100-Temp-	drop-K							
	13.	CV-200-Temp-	drop-K							
	14.	CV-300-Temp-	drop-K							
	15.	CV-400-Temp-	drop-K							
	16.	CV-500-Temp-	drop-K							
	17.	CV-100-Temp-	pool-K							
	18.	CV-200-Temp-	pool-K							
	19.	CV-300-Temp-	pool-K							
	20.	CV-400-Temp-	pool-K							
	21.	CV-500-Temp-	pool-K							
	22.	CV-100-Temp-	bubb-K							
	23.	CV-200-Temp-	bubb-K							
	24.	CV-300-Temp-	bubb-K							
	25.	CV-400-Temp-	bubb-K							
	26.	CV-500-Temp-	oubb-K							
0.000	00E+0(	) 1.05000E+05	1.05000E+05	1.05000E+05	1.05000E+05	1.05000E+05	3.15000E+02	3.15000E+02	3.15000E+02	3.15000E+02
3.150	00E+02	2 0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	3.15000E+02	3.15000E+02	3.15000E+02	3.15000E+02
3.150	00E+02	2 0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00				
2.000	00E-01	l 1.05001E+05	1.05001E+05	1.05001E+05	1.05001E+05	1.05001E+05	3.15001E+02	3.15001E+02	3.15001E+02	3.15001E+02
3.150	01E+02	2 0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	3.15000E+02	3.15000E+02	3.15000E+02	3.15000E+02
3.150	00E+02	2 0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00				
4.000	00E-01	L 1.05001E+05	1.05001E+05	1.05003E+05	1.05003E+05	1.05003E+05	3.15001E+02	3.15001E+02	3.15003E+02	3.15003E+02
3.150	03E+02	2 0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	3.15000E+02	3.15000E+02	3.15000E+02	3.15000E+02
3.150	UOE+03	2 U.UUUU00E+00	0.00000E+00	0.00000E+00	U.UUUU0E+00	U.UUUU0E+00				
E 000	000 00	1 1 050010.05	1 050010/05	1 0500000.05	1 050030.05	1 0500000.05	3 150010.00	2 150010:00	2 150020.00	2 150028/00
2.000	005-0.	L I.USUUIE+US	1.03001E+05	1.03003E+05	1.USUU3E+U5	1.USUU3E+U5	3.15001E+02	3.15001E+UZ	3.15003E+UZ	3.15003E+U2
3.150	005-02	2 0.00000000000000000000000000000000000	0.00000E+00	0.00000E+00	0.00000E+00	0.00000E+00	3.13000E+02	3.13000E+02	3.13000E+02	3.13000E+02
3.130	005+0	2 0.00000E+00	0.000008+00	0.000008+00	0.00000E+00	0.00000E+00				

The following NPLT records are occupied by the alphanumeric identifiers of variables, one identifier in a single record. The identifiers are written using the format: (**19**,**'. ',A25**), and can be read using for example the format (**12X,A25**) (12 characters, alpha-numeric string 25 characters).

Each variable identifier is a 25 (or less) character string. For example, the identifier of the atmosphere pressure in the Control Volume No. 100, is:

#### CV-100-Pres-atms-Pa

Each identifier consists of the following parts:

- 2 char. Package identifier. For example 'CV' is the Control Volume Package.
- 1 char. dash (-)
- 3 char. Component number, written using three digits. If for example the package identifier is 'CV' then this is the Control Volume number.
- 1 char. dash (-)
- 4 char. Variable identifier. For example '**Pres**' means pressure.
- 1 char. dash (-)
- 4 char. Additional variable identifier. For example '**atms**' means atmosphere. If for a given variable the additional identifier is not used, then this part contains four zeroes.
- 1 char. dash (-)
- 8 char Units of the variable. This is a string of up to 8 characters. If it is shorter than 8 characters the remaining characters are left blank. If the variable is dimensionless then the string is empty.

The next part of the plot file, below the variable identifiers, contains the plot edits. Each plot edit is preceded by a single empty line. Each plot edit consists of NPLT numbers, giving the current values of the NPLT plot variables. The values of the plot variables are written using the format: (10(ES12.5)) (ten real numbers, each 12 fields wide with 5 decimal places after the decimal point). The same format must be used to read the plot variables.

The full list of identifiers used by the SPECTRA plot file is presented in tables Table 2-23 through Table 2-32.

#### 3.3.1 Using S-GRAPH to Make Plots

Convenient plot programs (a "mouse-click" type) are able to perform all necessary operations: extract the requested data from the plot file, display it on the screen, and finally make a hard-copy using a printer. Such program, called VISOR, is available for SPECTRA post-processing. Examples are shown in the next section. VISOR is a first choice tool make making graphs and presenting SPECTRA results. VISOR however is limited to a certain operating platform (i.e. Windows environment). For systems such as UNIX or LINUX or for Users who do not wish to use VISOR, a simple, but generally applicable program is provided, which helps to make graphs from SPECTRA results. The program name is S-GRAPH and is described below.

The program S-GRAPH extracts one, or several variables from the SPECTRA plot file, and writes those variables in a form of several columns of numbers. When the data is available in the form of columns than a general plot program, available on given computer system, may be used to make a graph.

The process is illustrated in Figure 3-3. When SPECTRA run is finished the plottable variables are available in the plot file (\*.PLT). The program S-GRAPH reads the SPECTRA plot file and a so-called plot request file (\*.PLR). The structure of the plot request file is described below. The plot request file tells S-GRAPH which variable (or variables) need to be extracted from the plot file, and stored in the form of data columns.



Figure 3-3 Use of the program S-GRAPH.

When S-GRAPH is finished the requested variable(s) are available in the S-GRAPH output file (\*.ASC). Those data columns may be easily plotted using a general-purpose plot program available for a given system. Such programs (for example: GNUPLOT, XMGR, EXCEL, etc.) are easy to obtain for any particular system.

#### HOW TO USE S-GRAPH

The following steps, described below, need to be made to produce a graph with the help of the program S-GRAPH:

- Prepare requests for plot variable (or variables).
- Extract the variable data from the plot file using S-GRAPH.
- Make a graph using a plot program or a spreadsheet (EXCEL, GNUPLOT, COPLOT).

#### A) Prepare the plot request file (\*.PLR)

The plot request file tells S-GRAPH which variables need to be extracted from the SPECTRA plot file, and written as the columns of data. The first variable to be extracted is always time (s). It will be written in the first column. There is no need to request the time specifically in the \*.PLR file.

The \*.PLR file consists of one or more records (maximum is 99). Each record is a request for a single variable. There are three different formats, which can be used to request a variable:

#### Format 1:

The number of the variable in the plot file can be used. For example, in case of the plot file shown above, to request the CV-100 pressure one needs to write simply:

#### 2

#### Format 2:

The "pointers" can be used. A set of pointers consists of four numbers. The first pointer is the package identifier. For example the CV Package has number 1. The second pointer is the component number within package. If for example the first pointer is equal to one, then the second pointer is the CV number. The third and fourth pointers indicate the variable. The values of those pointers are shown in Table 2-23 through Table 2-32. For example, in case of the CV Package the third pointer equal to 13 means pressure and the fourth pointer equal to one means atmosphere (Table 2-23). Thus, to request the same variable as above - the atmosphere pressure in CV-001, one needs to write:

#### 1 100 13 1

Format 3:

The name of the variable can be used. To request the same variable as above one needs to write:

#### CV-100-Pres-atms-Pa

The units need not to be included, thus the same request may also look like:

#### CV-100-Pres-atms

Both strings shown above will extract the same variable from the plot file.

Any of the three formats shown above may be used. If the \*.PLR file consists of a single record then it will produce two columns: time and the requested variable. If it consists of N records it will produce N+1 columns: time and the requested variables, in the same order in which they are requested, as shown in the examples shown below.

Example 1: The file 'PRES.PLR' contains the following lines:

```
CV-100-Pres-atms
CV-300-Pres-atms
CV-200-Pres-atms
```

It will produce four columns of data. The first column will contain time. The next three columns will contain atmosphere pressures in Control Volumes 100, 300 and 200 respectively. The data will be stored in the file 'PRES.ASC'

Example 2: The file 'TEMP.PLR' contains the following lines:

```
CV-100-Temp-atms
1 100 14 2
CV-100-Temp-pool
1 100 14 4
```

It will produce five columns of data: time and four temperatures: atmosphere, droplets, pool and bubbles, in CV-001. The data will be stored in the file 'TEMP.ASC'.

Example 3: The file 'X.PLR' contains the following lines:

```
CV-100-Temp-atms
4
```

It will produce three columns of data: time, atmosphere temperature in CV-001, and the variable that is stored with the number four in the plot file. The data will be stored in the file 'X.ASC'

#### B) Run S-GRAPH to extract the requested variables

Execute S-GRAPH in a directory in which the SPECTRA plot file (\*.PLT) and a plot request file (\*.PLR) exist.

If the directory contains only one file with the extension 'PLT', then S-GRAPH will automatically use this file as the plot file. If there are more plot files, it will display the list of all plot files present in the current directory, and ask the user to enter the file name (the extension need not be entered).

If the directory contains only one file with the extension 'PLR', then S-GRAPH will automatically use this file as the request file. If there are more request files it will display the list of all request files present in the current directory, and ask the user to enter the file name (the extension need not be entered).

S-GRAPH checks whether the requested variables are present in the plot file. If they are not it writes an appropriate error message and stops.

If the requests are valid it extracts the requested variables and stores them in the output file. The name of the S-GRAPH output file has always the extension 'ASC'. The first part of the name is the same as the name of the request file. Thus, if the name of the request file is for example: 'PRES.PLR', then the results will be written to the file 'PRES.ASC'.

The results are written in the ASCII format, in the following manner. The first line contains names of all variables (25 character strings) separated by spaces. The next records contain the values of all plot variables, separated by spaces. Some plot programs (COPLOT) need the variable names to be written in the first record of the data file. Some other programs can only read columns of data and thus it may be necessary to delete the first record.

#### C) Make the graph using the file produced by S-GRAPH

In the last step a graph is made, using one of available general plot programs or spreadsheets, like EXCEL, GNUPLOT, COPLOT, etc. If the plot program cannot read alphanumeric headers then the first record in the \*.ASC file must be deleted before making a graph.

#### 3.3.2 Using VISOR as a Post-Processor

VISOR is an excellent tool to visualise results of SPECTRA or other codes (currently VISOR may be used for RELAP, MELCOR, MAAP, as well as for data arranged in columns). Use of VISOR is described in the VISOR Manual, however the program is so user friendly and simple that may be used practically without any training. A beginner may simply start from working examples and modify them for his needs.

Some simple example pictures, made with VISOR are shown below in Figure 3-4 through Figure 3-7.



Figure 3-4 Example test case - REFLOOD.



Figure 3-5 Example test case - HEX.





Figure 3-6 BWR-1000 simulator, reactor vessel, emergency systems, and containment.



Figure 3-7 BWR-1000 simulator, turbine.

#### 3.4 Restart File (\*.RST)

The restart option is provided to allow continuing calculations, which have been terminated, either by normal termination, by stop file, or by failure. The restart file (\*.RST) is a binary file, which contains values of all variables in all SPECTRA Common Blocks. When a job is restarted the values of all variables are read from the \*.RST file and the calculations are continued. An example illustrating the restarting procedure is presented below.

#### Example

An example is provided in \Z-INPUTS\SL\Restarting\. The following input files are present:

- "Run12" Input file Run12.SPE a "full-time" run, analysis time 0.0 2200 s.
- "Run1" Input file Run1.SPE the same input, but the run time is 0 1100 s
- "Run2" Input file Run2.SPE restart input only time steps are provided
  - end time = 2200 s,
  - start time is determined interactively on restart, as shown below.

It is important to note that the input file for restarting should contain minimum input (as all input will be read from the restart file. In the present case, the input file Run2.SPE contains the following inputs:

*						*			
*	DTMAX	DTMIN	DTPRT	DTPLT	TEND	*	Time	step	data
900001	0.1	1.0E-6	100.0	10.0	2200.0	*			
*									

The run script, provided in the test run location  $Z-INPUTSSL\$  estarting, the file "Run-all.bat" contains the following commands:

call C:\SPECTRA\Z-EXE\SPECTRA.EXE Run12.SPE call C:\SPECTRA\Z-EXE\SPECTRA.EXE Run1.SPE copy Run1.RST Run2.RST copy Run1.OUT Run2.OUT copy Run1.PLT Run2.PLT copy Run1.MES Run2.MES copy Run1.DIA Run2.DIA call C:\SPECTRA\Z-EXE\SPECTRA.EXE Run2.SPE

The run script performs the following operations:

- First, it executes the full run, Run12.SPE (2200 s), which serves as reference run.
- Next, it executes the run Run1.SPE, which covers the first half of the transient (1100 s)
- Next it copies the results of the output files from run "Run1" to "Run2"
- Finally, it executes the Run2.SPE. When this one is executed, SPECTRA detects the presence of the restart file and starts the interactive restarting process, which is shown below.

🔤 C:\Windows\System32\cmd.exe	_	$\times$
=SPE= SPECTRA Version 22-04, Apr. 2022, Windows		^
Sophisticated Plant Evaluation Code for Thermal-hydraulic Response Assessment		ľ
Validity: 12/2025, Applicability: AppC = 0000		
> INPUT DATA FILE :\> Run2.SPE		
> RESTART FILE EXISTS. ENTER "R" TO RESTART, OTHER TO START :\> r		
<pre>-&gt; READING RESTART FILE &gt; CURRENT TIME: 5.00000E+02 [s], RESTART FROM THIS POINT (Y/N) :\&gt; n &gt; CURRENT TIME: 1.10000E+03 [s], RESTART FROM THIS POINT (Y/N) :\&gt; y</pre>		
<pre>-&gt; CURRENT TIME STEP DOMAIN NUMBER: 1 -&gt; TIME STEPS AND END TIME &gt; MAXIMUM DT ( 1.00000E-01 [s] ), NEW:\&gt; 0 &gt; MINIMUM DT ( 1.00000E-06 [s] ), NEW:\&gt; 0 &gt; PRINT DT ( 1.00000E+02 [s] ), NEW:\&gt; 0 &gt; PLOT DT ( 1.00000E+01 [s] ), NEW:\&gt; 0 &gt; END TIME ( 2.20000E+03 [s] ), NEW:\&gt; 0</pre>		
-> TRANSIENT CALCULATIONS RESTARTED		
t = 1.38E+03 ( 64%) dt = 1.00E-01 CPU = 2.34E-01 RUN = 1.00E+00 Iter: 4		
-> END OF CALCULATIONS.		
-> RUN STATISTICS		
Analyzed model time [s]: 0.230E+04 (0.639 [hrs]) 100% Processor time (CPU) [s]: 0.781 (0.217E-03 [hrs]) Clock time (RUN) [s]: 1.55 (0.430E-03 [hrs]) Warp factor (model/CPU): 0.294E+04 (1 / 0.340E-03) Run ratio (RUN/model): 0.673E-03 (1 / 0.149E+04) Minimum time step [s]: 0.100E+00 Maximum time step [s]: 0.100E+00 Average time step [s]: 0.100E+00 No. of advancements 23001 No. of iter. per advanc.: 4.20 CPU per advancement [s]: 0.340E-04 Run time per advanc. [s]: 0.673E-04		
-> =SPE= SPECTRA Version 22-04, Apr. 2022, Windows FILES CLOSED ON : 20/10/2022, 18:29:21.68		

When Run2.SPE is started, SPECTRA detects that the restart file exists for the requested job ("Run2.RST"). It therefore asks whether the user wishes to restart the job, or to start a new run. In this case the user wants to restart, therefore "r" (or "R") is entered.

Next, the program reads the restart file, prints the times of the restart points, and asks the user to restart the job. In this case the user wants to restart from the second point, at t = 1100 s.

Next, the program asks for the new time steps, print and plot intervals, and the end time for this time step domain. The values read from the restart file are the default values, and they are printed in brackets. For the present example the user does not wish to change the time steps; therefore, zeroes are entered.

The output file and the diagnostics file are appended, so the information from the first run is not lost.

Note 1:

If the output/plot files are not copied, then the results of the Run2.SPE will contain only the data for times between 1100 s and 2200 s. The plot file will still be readable; in the case when no previous plot file is provided, SPECTRA will start the new plot file by writing variable names/ headers, so the plot file will be readable by the usual plotting programs.

Note 2:

During the restart the input file (in this case Run2.SPE), if exists, should contain only the Solver (time step) data and eventually the Tabular Function data that should replace the data in the restart file (see section 2.20). An example of the input file (Run2-TF.SPE) that may be used on restart to redefine an existing Tabular Function, TF-100, is presented below.

Compared to the original TF-100, the last value has been redefined from 0.1E+5 to 1.0E+5. The run Run2-TF may be executed in the same way as Run-2, i.e.

- The output files from "Run-1" should be copied to "Run-2-TF"
- The Run-2-TF.SPE should be executed and restarted from the second restart point.

In this case Run2-TF will be the same as Run2 until 1200 s. After that the results will be different as the values of TF-100 are different.

Summarizing, it should be noted that:

- The data that must always be entered interactively includes:
  - $\circ$  the restarting time point,
  - the time step data for the current time step domain (zeros may be entered to keep the old value).
- The data that may be entered in the SPECTRA input file (\*.SPE) includes:
  - Solver data,
  - o TF data.

Currently, only the Solver data and the TF data may be re-defined in the SPECTRA input file upon restart (see section 2.20).

#### 3.5 The Initial Condition File (\*.ICF)

At the end of each calculations SPECTRA writes all current parameters (pressures, temperatures, fluid velocities, etc., into the \*.ICF file. In contrast to the restart file, the ICF file is a text file, so it is easy for the user to manipulate. An example of an ICF file is shown below.

=CV=	INITIAL CONDIT	ION DATA FOR 5	CONTROL VOLUME	S		
CV 001 002 003 004 005	DSP 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	TSP 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	PSP 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00			
CV 001 002 003 004 005	ATMS-PRES 1.10120002E+05 1.10191625E+05 1.05034461E+05 1.05034460E+05 1.05034461E+05	ATMS-TEMP 3.19267493E+02 3.19314069E+02 3.15032406E+02 3.15032405E+02 3.15032407E+02	POOL-LEVEL 5.24442099E+00 5.00000195E+00 4.99999897E+00 4.99999837E+00 4.99999897E+00	POOL-TEMP 3.15027081E+02 3.14999980E+02 3.14999904E+02 3.14999904E+02 3.14999904E+02		
CV 001 002 003 004 005	ATMS GAS COMPO 0.00000000000000000000000000000000000	SITION 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	4.31708948E-01 4.14391333E-01 2.88037881E-03 2.88038628E-03 2.88036870E-03	7.62233365E-01 7.59650039E-01 9.99774778E-01 9.99774778E-01 9.99774779E-01	1.97758053E-01 2.01874765E-01 0.0000000E+00 0.0000000E+00 0.0000000E+00	0.00000000E+00 0.00000000E+00 0.00000000E+00 0.00000000E+00 0.00000000E+00
CV 001 002 003 004 005	DROP.FRACTION 9.45904198E-06 0.00000000E+00 0.00000000E+00 0.0000000E+00 0.0000000E+00	TEMPERATURE 3.46641497E+02 0.00000000E+00 0.00000000E+00 0.0000000E+00 0.0000000E+00	DIAMETER 1.0000000E-02 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	POSITION 3.33195737E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00		
CV 001 002 003 004 005	BUBB.FRACTION 4.65286629E-02 0.00000000E+00 0.00000000E+00 0.00000000E+00 0.00000000E+00	TEMPERATURE 3.14969153E+02 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	DIAMETER 1.6000000E-02 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	POSITION 4.19204872E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00		
CV 001 002 003 004 005	BUBB GAS COMPO 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.00000000E+00	SITION 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.00000000E+00	5.41465292E-01 0.00000000E+00 0.0000000E+00 0.00000000E+00 0.00000000E+00	9.63177081E-01 0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00	0.00000000E+00 0.00000000E+00 0.0000000E+00 0.00000000E+00 0.00000000E+00	0.00000000E+00 0.00000000E+00 0.00000000E+00 0.00000000E+00 0.00000000E+00
=JN=	INITIAL CONDIT	ION DATA FOR 1	JUNCTIONS			
JN 001	ATMS-VELOCITY 4.25095714E-01	POOL-VELOCITY 0.00000000E+00				
JN 001	VALVE OPEN FR. 1.00000000E+00	K-FORWARD 1.00000000E+00	K-REVERSE 1.00000000E+00			
JN 001	ATMS-PUMP-SPEE 0.00000000E+00	D POOL-PUMP-SPEE	D ATMS-PUMP-FLOW 0.00000000E+00	POOL-PUMP-FLOW 0.00000000E+00		
=SC=	INITIAL CONDIT	ION DATA FOR 12	1-D SOLID HEAT	CONDUCTORS		
SC 001 SC	CELL TEMPER N K/L 0 2 00 3.15002 N K/L 0	ATURES 1 02 253E+02 3.15001 1 02	2 0 981E+02 2 0	3 0 3 0	4 0 4 0	5
002 SC	2 00 3.15002 N K/L 0	253E+02 3.150019 1 02	981E+02 2 0	3 0	4 0	5
003 SC	2 00 3.15002 N K/L 0	253E+02 3.15001 1 02	981E+02 2 0	3 0	4 0	5
004 SC	2 00 3.15002 N K/L 0	253E+02 3.150019 1 02	981E+02 2 0	3 0	4 0	5
005 SC	2 00 3.15002 N K/L 0	253E+02 3.150019 1 02	981E+02 2 0	3 0	4 0	5
006 SC	2 00 3.15002 N K/L 0	252E+02 3.150019 1 02	980E+02 2 0	3 0	4 0	5
```
2 00 3.15002251E+02 3.15001979E+02
007
                                       ----- 0.3 ----- 0.4 ----- 0.5 -----
SC N K/L ----- 01 ----- 02 -----
     2 00 3.15002258E+02 3.15001982E+02
008
                                       ----- 03 ----- 04 ----- 05 -----
SC
    N K/L ----- 01 -----
                         ---- 02
      2 00 3.15002262E+02 3.15001983E+02
009
                             -- 02 ----- 03 ----- 04 ----- 05 -----
    N K/L ----- 01 -----
      2 00 3.15002964E+02 3.15002529E+02
010
                                       ----- 03 ----- 04 ----- 05 -----
SC
    N K/L ----- 01 ----- 02 -----
     2 00 2.77516768E+02 2.77324570E+02
011
                                       ----- 03 ----- 04 ----- 05 -----
    N K/L ----- 01 -----
                         ----- 02 -----
SC
      2 00 2.77516768E+02 2.77324570E+02
012
SC OXIDATION DATA, METAL AND OXIDE THICKNESSES IN BOUNDARY CELLS
SC
     LEFT METAL
                   LEFT OXIDE
                                  RIGHT METAL
                                                RIGHT OXIDE
     0.00000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
001
002
     0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
     0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
003
     0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
004
005
     0.0000000E+00 0.0000000E+00 0.0000000E+00
                                               0.0000000E+00
    0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
006
007
     0.0000000E+00 0.0000000E+00 0.0000000E+00
                                                0.0000000E+00
008
     0.0000000E+00 0.0000000E+00
                                 0.0000000E+00
                                                0.0000000E+00
009
     0.0000000E+00
                   0.0000000E+00 0.0000000E+00
                                                0.0000000E+00
     0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
010
011
     0.0000000E+00 0.0000000E+00 0.0000000E+00 0.0000000E+00
     0.0000000E+00 0.000000E+00 0.000000E+00 0.000000E+00
012
=TC= INITIAL CONDITION DATA FOR 0 2-D SOLID HEAT CONDUCTORS
=CF= INITIAL CONDITION DATA FOR 0 CONTROL FUNCTIONS
=RK= REACTOR KINETICS CF NO.:
                            0 (CF-000)
```

This file may be used to provide initial conditions for another calculations. This is done in record 905000 (see section 2.16.3). When the ICF file is requested in record 905000, then all conditions that are present in the input deck are replaced by the values read from the ICF file. Therefore, **If the ICF file is used and the user wishes to change some parameter in the system, he cannot do it in the input deck! the parameter must be modified in the ICF file.** This is easily done, since the ICF is an ASCII file.

For example, the user needs to run a full power stationary state using the reactor kinetics model. The initial temperatures of fluid and structures, entered in the input deck, are usually not very accurate. Consequently the temperatures will change before steady state operation is reached. If the user starts the run directly with the reactor kinetics model, then the thermal feedback would cause large reactivity changes and would make it very difficult to keep the reactor at the desired power. To avoid this one can apply a two-step procedure:

- 1. Run the model with a constant reactor power (defined by a Tabular Function) for a time sufficiently long to obtain stable parameters in the analysed system. This Constant Power (CP) run will produce the file CP.ICF.
- 2. Start the reactor kinetics run (RK) using the initial conditions calculated in the CP run, by requesting the file CP.ICF in record 905000.

## 3.6 The Tabular Function Data File (\*.TFD)

The TFD file may be used to change the value of any Tabular Function that is defined as interactive (see section 2.7.5). The interactive functions are used to run SPECTRA as a background code for a simulator.

In order to change the value of any function, one has simply to type the function number and the value. For example, the following record in the TFD file:

500 -2.37

will change the value of function TF-500 to -2.37. Note that the change will be restricted by the limits imposed on the function (see section 2.7.3).

If several definitions are present in the TFD file, then the last one is used. For example, if the following records are present in the TFD file:

500 -2.37 500 +1.23 500 0.0 500 1000.0

then the value of TF-500 will be set to 1000.0.

In order to switch back to the TF data tabulated in the input deck, one must remove all definitions of given TF from the TFD file. This can be done automatically using the automatic reset option - record 611XXX.

### 3.7 Message File (\*.MES)

The message file contains messages about certain events. The following events are written to the message file:

- change of burn status within CV, change of burn propagation status,
- change of valve status (opening/closing),
- change of pump/turbine status (starting up/stopping),
- reaching user defined limits (min/max, rates of change) for TF/CF,
- EDF data transfers (optionally, if requested by the user),
- TF value read from the \*.TFD file (timing and value read).

#### 3.8 Stop File (\*.STP)

Calculations can be terminated at any time using a SPECTRA Stop File. To do this user has to put a file, with the name "**\***.**STP**", in the directory where the run is performed.

When the program encounters the presence of the stop file it asks the user for confirmation (see the example printout below). If the termination is confirmed, the program writes the final edit in the output and plot files, writes the restart file, deletes the stop file (to avoid unintended stopping in the future), and terminates the calculations. Below, an example of the screen output is shown.

t = 5.13E+04 ( 0%) dt = 1.00E+01 CPU = 1.00E+01 RUN = 1.00E+01 Iter: 6
t = 7.15E+04 ( 0%) dt = 1.00E+01 CPU = 1.10E+01 RUN = 1.10E+01 Iter: 6
-> STOP SIGNAL ENCOUNTERED

```
> ENTER "Y" TO CONFIRM TERMINATION OF THE RUN
    ENTER "N" TO CONTINUE AFTER INTERACTIVE MENU
     ENTER "F" TO REDIRECT INTERACTIVE MENU TO STOP FILE
 >
 >
     v
 > RUN TERMINATED BY THE STOP FILE
-> RUN STATISTICS
                        _____
     Analyzed model time (s): 0.733E+05 ( 20.4 (hrs) )

Processor time (CPU) (s): 10.1 ( 0.281E-02 (hrs) )

Clock time (RUN) (s): 10.1 ( 0.281E-02 (hrs) )

Warp factor (model/CPU) : 0.724E+04 ( 1 / 0.138E-03 )

Run ratio (RUN/model) : 0.138E-03 ( 1 / 0.725E+04 )

Minimum time step (s): 1.000

Maximum time step (s): 10.00

Average time step (s): 4.49
                                                                                                    08
     Average time step (s): 4.49
No. of advancements 16347
     No. of iter. per advanc.: 6.13
     CPU per advancement (s): 0.619E-03
Run time per advanc. (s): 0.619E-03
                                                       _____
      _____
                   _____
```

-> =SPE= SPECTRA Version 3.61, February 2016 FILES CLOSED ON : 22/02/2016, 22:04:59.26

The "stop file" may also be used to change time steps, activate the extended diagnostics or debug printout (section 2.16.2, 2.16.4). To change time steps or activate the extended diagnostics or debug printout, the user has to answer "N" or "n" when asked to confirm termination of the run (see the example output below). In this case the program will ask the user for the time steps, print and plot intervals, as well as the end time for this time step domain. If zeroes are entered then the current values are used (unchanged). Next, the program will ask whether the extended diagnostics or debug printout should be activated. If the transient diagnostics is suppressed (see section 2.16.7), then the program will ask whether the user is yes, it will ask whether the user wishes to activate the extended diagnostics and the debug printout.

Finally, the program will ask whether to write a restart and the ICF data at the current time. Thus the STOP file may be used to obtain an extra restart point or ICF data (apart from the restarts that are being written in the restart frequency of DTRST - see section 2.16.2 and the ICF file which is always written at the termination of the run). Below, an example of the screen output is shown.

```
t = 7.25E+04 ( 0%) dt = 1.00E+01 CPU = 1.00E+01 RUN = 1.00E+01 Iter: 6 t = 8.33E+04 ( 0%) dt = 1.00E+01 CPU = 1.10E+01 RUN = 1.10E+01 Iter: 6
-> STOP SIGNAL ENCOUNTERED
     ENTER "Y" TO CONFIRM TERMINATION OF THE RUN
 >
     ENTER "N" TO CONTINUE AFTER INTERACTIVE MENU
 >
     ENTER "F" TO REDIRECT INTERACTIVE MENU TO STOP FILE
 >
     Ν
    RUN WILL BE CONTINUED
 >
    CURRENT TIME: 8.50324E+04 (s), CURRENT DOMAIN No.: 3
 >
    MAXIMUM DT ( 1.00000E+01 (s) ), NEW:> 0
MINIMUM DT ( 1.00000E-05 (s) ), NEW:> 0
 >

        MINIMUM D1
        (1.00000E 03 (s) ), NEW:\> 0

        PRINT DT
        (9.00000E+03 (s) ), NEW:\> 0

        PLOT DT
        (5.00000E+02 (s) ), NEW:\> 0

        END TIME
        (1.00000E+05 (s) ), NEW:\> 0

 >
 >
     DO YOU WANT EXTENDED DIAGNOSTICS IN THE NEXT PART OF THE RUN (Y/N) :> N
 >
     DO YOU WANT DEBUG PRINTOUT IN THE NEXT PART OF THE RUN (Y/N) : > N
 >
     DO YOU WANT TO WRITE A RESTART AT THE CURRENT TIME POINT (Y/N)
 >
                                                                                                    :\> N
     DO YOU WANT TO WRITE AN ICF AT THE CURRENT TIME POINT (Y/N)
 >
                                                                                                    :\> N
```

```
-> TRANSIENT CALCULATIONS CONTINUED
```

t = 8.50E+04 ( 0%) dt = 1.00E+01 CPU = 1.11E+01 RUN = 3.23E+01 Iter: 6 t = 1.17E+05 ( 1%) dt = 1.00E+02 CPU = 1.21E+01 RUN = 3.33E+01 Iter: 6

In some cases it is convenient to redirect the interactive menu into the content of the\*.STP file. This can be done by pressing "F" or "f". The content of the \*.STP file should look like:

Ν	*	DON'T STOP
0	*	MAX DT
0	*	MIN DT
0	*	PRINT DT
0	*	PLOT DT
0	*	END TIME
Ν	*	EXTENDED DIAGNOSTICS
Ν	*	DEBUG PRINTOUT
Ν	*	WRITE RESTART POINT
Ν	*	WRITE ICF

Below, an example of the screen output is shown for the above \*.STP file.

t =  $5.30\pm04$  ( 0%) dt =  $1.00\pm01$  CPU =  $8.99\pm00$  RUN =  $9.00\pm00$  Iter: 6 t =  $6.97\pm04$  ( 0%) dt =  $1.00\pm01$  CPU =  $9.98\pm00$  RUN =  $1.00\pm01$  Iter: 6 -> STOP SIGNAL ENCOUNTERED ENTER "Y" TO CONFIRM TERMINATION OF THE RUN ENTER "N" TO CONTINUE AFTER INTERACTIVE MENU > > > ENTER "F" TO REDIRECT INTERACTIVE MENU TO STOP FILE > F > RUN WILL BE CONTINUED > CURRENT TIME: 7.78024E+04 (s), CURRENT DOMAIN No.: 3 > DO YOU WANT EXTENDED DIAGNOSTICS IN THE NEXT PART OF THE RUN (Y/N) : > N :\> N DO YOU WANT DEBUG PRINTOUT IN THE NEXT PART OF THE RUN (Y/N) >  $>\,$  DO YOU WANT TO WRITE A RESTART AT THE CURRENT TIME POINT (Y/N) :\> N > DO YOU WANT TO WRITE AN ICF AT THE CURRENT TIME POINT (Y/N) :\> Ν -> TRANSIENT CALCULATIONS CONTINUED

t = 7.78E+04 ( 0%) dt = 1.00E+01 CPU = 1.05E+01 RUN = 1.59E+01 Iter: 6 t = 9.44E+04 ( 0%) dt = 1.00E+01 CPU = 1.15E+01 RUN = 1.69E+01 Iter: 6

# 4 SPECTRA Installation Guide

This chapter describes installation and verification of the SPECTRA code. Hardware requirements are given in section 4.1. Installation is discussed in section 4.2. Installation of the program should be followed by verification, which consists of rerunning the supplied test case with the newly installed program and comparing the obtained results with the supplied reference results. A short guide how to execute the program is provided in section 4.3. The reference results of the test case for verification of the installed code are described in section 4.4. Section 4.5 discusses the automatic verification. Section 4.6 discusses other possible verification runs.

## 4.1 Hardware and Software Requirements

SPECTRA may be run under Windows or Linux operating systems. Both Windows and Linux versions are delivered.

## 4.2 Installation of the SPECTRA Code

The SPECTRA distribution consists of the following parts:

- SPECTRA code
- Code manuals
- Utilities (inputs for V&V and test input files)

Installation procedure for SPECTRA:

- SPECTRA executable should be copied to a preferred location, for example:
  - Windows:
    - C:\SPECTRA\SPECTRA.EXE
  - o Linux
    - ~/SPECTRA/SPECTRA.X
- In Windows an appropriate link should be set, to be able to start SPECTRA calculations by simply double-clicking on a SPECTRA input file \*.SPE. This may be done as follows:
  - Right-click on any SPECTRA input file, \*.SPE
  - Select "open with"
  - Select "browse" (or "Look for another app on this PC", depending on Windows version)
  - Select the SPECTRA code executable, located as selected in the previous step.

The post-processor/visualization tool for SPECTRA (also applicable for other codes, MELCOR, RELAP5, etc.), VISOR, is distributed together with the SPECTRA code. The distribution consists of the following parts:

- VISOR code
- User's manual

Installation procedure for VISOR:

- VISOR can only be executed under Windows. It can read plot files created on both Windows and Linux machines. Visor should be copied to a preferred location, for example: C:\SPECTRA\VISOR.EXE
- An appropriate link should be set, to be able to start VISOR by simply double-clicking on a VISOR input file \*.VSD. This may be done as follows:
  - Right-click on any Visor input file, \*.VSD
  - Select "open with"
  - Select "browse" (or "Look for another app on this PC", depending on Windows version)
  - Select the VISOR code executable, located as selected in the previous step.

## 4.3 Execution of the Code

If the links described in the previous section are set then:

- SPECTRA can be started by simply double-clicking on a SPECTRA input file \*.SPE
- VISOR can be started by simply double-clicking on a VISOR visualization file \*.VSD

Alternatively, these programs can be started by double clicking on the executable files, followed by typing the SPECTRA input file name:



or by selecting "File" - "Open" in Visor:

1	🚸 Visor	¥2.2.	3			. 🗆 🗵
Ī	File Edit	Run	Mode	Window		
	🗋 New			Ctrl+N	» • • • • • • • • • • • • • • • • • • •	
	📂 Open			Ctrl+O		
	📙 Save			Ctrl+S		
۱	Export Data to Excel Export Data to ASCII file		( file			
ļ	Exit			Ctrl+Q		

Alternatively, a script may be written to start specific SPECTRA jobs. This method is more convenient if multiple jobs need to be started. For example, suppose we define a Windows script (e.g. as a file: Run-123.bat) as follows:

#### start C:\SPECTRA\SPECTRA.EXE JOB1.SPE start C:\SPECTRA\SPECTRA.EXE JOB2.SPE call C:\SPECTRA\SPECTRA.EXE JOB3.SPE

This will start simultaneously three calculations, with inputs defined as JOB1, JOB2, and JOB3. If we want to start runs subsequently, this can be done using the following script:

```
call C:\SPECTRA\SPECTRA.EXE Test1.SPE
call C:\SPECTRA\SPECTRA.EXE Test2.SPE
call C:\SPECTRA\SPECTRA.EXE Test3.SPE
```

The calculations will be performed in sequence, i.e. Test 2 will be started when Test 1 is finished, etc.

Similar ways are available in Linux. The code can be started by typing the full path to the code and then typing the input file name at the command prompt:



Linux jobs can be started in the background, using the nohup command. For example, suppose we define a script (e.g. as an executable file: Run-123.x) as follows:

nohup ~/SPECTRA/SPECTRA.X JOB1.SPE > JOB1.SCN & nohup ~/SPECTRA/SPECTRA.X JOB2.SPE > JOB2.SCN & nohup ~/SPECTRA/SPECTRA.X JOB3.SPE > JOB3.SCN &

This will start simultaneously three calculations, with inputs defined as JOB1, JOB2, and JOB3. The output that is normally sent to the screen, will be send to the prescribed file, in this case \*.SCN. The screen output is a short summary of an advancement, including the current time, the percentage advancement, the time step used, CPU Time and run (clock) time elapsed, and the number of iterations needed. An example of the screen output is shown below:

```
 t = -9.90E+00 (0\%) dt = 1.00E-01 CPU = 3.63E+00 RUN = 3.62E+00 Iter: 20 \\ t = -9.89E+00 (0\%) dt = 4.71E-03 CPU = 4.84E+00 RUN = 4.83E+00 Iter: 5 \\ t = -9.85E+00 (0\%) dt = 8.57E-03 CPU = 5.92E+00 RUN = 5.91E+00 Iter: 11 \\ t = -9.80E+00 (0\%) dt = 8.56E-03 CPU = 7.16E+00 RUN = 7.15E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = 8.56E-03 CPU = 8.26E+00 RUN = 8.25E+00 Iter: 5 \\ t = -9.76E+00 (0\%) dt = -9.76E+00 RUN = -9.76E+00 RUN
```

The jobs can also be started in the foreground, in which case they will be executed subsequently. For example, suppose we define a script (e.g. as an executable file: Run-123.x) as follows:

~/SPECTRA/SPECTRA.X Test1.SPE ~/SPECTRA/SPECTRA.X Test2.SPE ~/SPECTRA/SPECTRA.X Test3.SPE

The calculations will be performed in sequence, i.e. Test 2 will be started when Test 1 is finished, etc. It should be noted that Linux system is case-sensitive, so Test1.SPE is not the same as, for example, test1.spe. In Windows system the file names are not case sensitive.

During the calculations SPECTRA creates output files, described in Chapter 3. The output files are located in the same directory where the input file exist, and have the same name as the input file but with different extensions (see section 3).

## 4.4 Manual Verification

The manual verification test is provided in the directory: \Z-INPUTS\Qualification-tests-EFP\

The full test "establishment of flow problem" (EFP) is described in detail in Volume 3. The verification test discussed here consists of the first 60 seconds of EFP Case A. Results of SPECTRA are compared to the results of MELCOR. The visualization picture for this test is provided in EFP-SPE.VSD. The end state (t = 60 s) is shown in Figure 4-1. In order to perform verification of calculated results the following steps should be taken.

- Run the file: EFP-A.SPE using the Windows or Linux version of SPECTRA.
- Compare the output file: EFP-A.OUT, with the source file delivered in: \Z-INPUTS\Qualification-tests-EFP\Source\EFP-A.OUT (Windows version) \Z-INPUTS\Qualification-tests-EFP\Source-Linux\EFP-A.OUT (Linux version)



Figure 4-1 Test "establishment of flow" - visualization screen from EFP-SPE.VSD



Figure 4-2 Test "establishment of flow" - export of data from EFP-Graphs-SPE.VSD



Figure 4-3 Test "establishment of flow" - import of to data into EFP-Graphs-Case-A.xls

**(b)** 

**(a)** 





Figure 4-4 Reference test result - steam line flow versus time

The obtained results should be identical as the appropriate source results. Furthermore, it is recommended to compare the SPECTRA results with the reference (MELCOR) results for this case. This is done as follows:

- Open the file EFP-Graphs-SPE.VSD (double-click on this file).
- Check the end value, by clicking on "Go to a specific time" button Figure 4-2 (a) and specifying 60.0 seconds The velocity should read 27.23 m/s.
- Export the data to excel by pressing the button "Export Data to Excel" Figure 4-2 (b). This will open a new excel file (with a default name, e.g. "Sheet1")
- Open the file EFP-Graphs-Case-A.xls and copy the data from "Sheet1" into EFP-Graphs-Case-A, tab "SPE" Figure 4-3 (a).
- View the graph provided in EFP-Graphs-Case-A, tab "Graph" Figure 4-3 (b).

The SPECTRA results should be in good agreement with the MELCOR results (these are provided in EFP-Graphs-Case-A, tab "MEL". The final graph is provided in Figure 4-4.

## 4.5 Automatic Verification

The base set of automatic verification tests is provided in the directory: \Z-INPUTS\Qualification-tests\

The automatic verification is made based on the following property of the SPECTRA output file: The \*.OUT file starts with an echo of input file, which is followed by an end-of-input marker (a period in the first column) and then followed by the output. If \*.OUT from an earlier calculation is renamed to \*.SPE and executed, then the code reads the input file, ignores everything which follows the end-of-input marker and performs calculations. If the calculations proceed in exactly the same way as the earlier calculation, the new \*.OUT is exactly the same then the original \*.OUT file. This procedure is illustrated in Figure 4-5. In short, the \*.OUT file renamed into \*.SPE and executed, should duplicate itself. If an Initial Condition File is used, then it must also be provided together with the renamed \*.OUT file.



Automated verification using the SPECTRA output file

Figure 4-5 Automatic verification using the \*.OUT file

The main directories contain subdirectories \Source, with output files from all test calculations. In order to activate the automatic testing one must activate the script:

#### Test-all.bat

This script performs the following actions:

- Extracts the original \*.OUT and \*.ICF files from the \Source subdirectory
- Renames \*.OUT into \*.SPE
- Executes all \*.SPE files (Note: path to the source code may need to be redefined by the user. The current path is C:\SPECTRA\Z-EXE\SPECTRA.EXE)
- Compares the obtained results with the results stored in the \Source directory
- Writes the outcome of such comparison to the file "Results.txt"

When the test script is terminated, the user must check the file "Results.txt" If the test is successful there is no difference in all cases. The contents of the Results.txt file should be as shown below:

SPECTRA AUTOMATIC TEST SCRIPT EXECUTED ON:

USERNAME=STEMPNIEWICZ COMPUTERNAME=P6014

Tue 11/24/2020 04:35 PM

THE TEST IS SUCCESSFUL IF THERE ARE NO DIFFERENCES IN ALL CASES

Comparing files Butterfly-Valve.OUT and .\SOURCE\BUTTERFLY-VALVE.OUT FC: no differences encountered

Comparing files CF.OUT and .\SOURCE\CF.OUT FC: no differences encountered

Comparing files ED-RW.OUT and .\SOURCE\ED-RW.OUT FC: no differences encountered

... etc.

Linux version of the same set of automatic verification tests is provided in the directory:  $\Text{Z-INPUTS}\Qualification-tests-Linux}$ 

The testing procedure is the same as described above for the Windows verification tests.

The automatic verification tests specific to HTRs is provided in the directory: \Z-INPUTS\Qualification-tests-HTR\ The testing procedure is the same as described above for the base verification tests.

## 4.6 Other Verification Runs

Apart from the verification run, described above, the user may perform additional verification using any test cases described in the Volume 3 of the SPECTRA Code Manuals: "Verification & Validation". The SPECTRA Manuals are available in the subdirectory \Z-MANUALS\, which is supplied together with the SPECTRA code.

Almost all test cases that are described in Volume 3 are available in the subdirectory  $\langle Z-INPUTS \rangle$ , which is supplied together with the SPECTRA code. In order to perform additional verification runs the user must perform the following steps:

- Select a test case in Volume 3. The user may find it important to perform additional verification of a selected part of the code, for example the 2-D conduction, the Radioactive Particle Transport, etc. In such case the user should select a test case from the appropriate chapter of Volume 3.
- The location of the input file is mentioned for each test described in Volume 3. In order to make it easier for the user to find the files, the file locations are always given in bold characters, for example the "CV" test case may be found in \Z-INPUTS\CV\CV.SPE. Thus, once the user selects the test, it should not be a problem to locate the appropriate input deck in the subdirectory \Z-INPUTS\.
- Once the input deck is located, calculations should be performed according to the instructions for code execution, mentioned in section 4.3.
- When the calculations are finished the results may be viewed using the provided visualization picture (Visor picture), for example \Z-INPUTS\CV\CV.VSD. Using Visor one can compare snapshots at given time points to corresponding snapshots presented in Volume 3, but also make time-dependent graphs for comparison with similar graphs provided in Volume 3.

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# appendix A Pump/Compressor Maps

Two models are available for pumps/compressors in SPECTRA. The first model (Type 1) simply sets the flow in junction based on the pressure difference across the junction and the user-defined maps. The second model (Type 2) calculates the pressure head based on the user-defined maps and then uses the general momentum equation to calculate the flow. Type 1 is seldom used. This was the first pump model applied in an early version of SPECTRA, and it is preserved in the code to keep compatibility with earlier input decks. Type 2 is generally recommended, because it is physically correct, while Type 1 is only an approximation valid for quasi-stationary conditions. Moreover Type 2 offers several additional capabilities, like:

- More flexible map generation (there are more map defining parameters that can be specified by the user exponents *a*, *b*, *c*).
- Internal power calculation. When Type 1 is used, the user must define Control Functions to define power entering the fluid. A set of recommended functions had been provided in the manual to an early SPECTRA version. When Type 2 is used, the power that enters the fluid is calculated internally by the code, using efficiency tables.
- Speed can be calculated using a rotor inertia equation.

The discussion below explains how a pump/compressor map is defined using relatively few input parameters. The pump maps are discussed basically for the Type 2 pumps/compressors. The Type 1 has the same maps, except that the exponents a, b, c have fixed values, and cannot be affected by the user.

## A.1 Approach

The basic approach in the SPECTRA code is quite different than in codes such as RELAP, TRAC, etc. These codes require the user to provide data tables specifying maps for all possible conditions (four quadrant curves - see (Dimenna, 1988)). Alternatively, they offer built-in curves for typical pumps (Bingham Westinghouse pump curves are available in RELAP).

In general, it is quite difficult to find sufficient data to determine the four quadrant curves; specifically the data for reverse speed and reverse flow are typically not available from the manufacturer. The required input data is extensive; the user must provide a sufficient amount of data to cover all possible conditions, even if some conditions are never expected to occur. Consequently users of RELAP or TRAC typically prefer to use the built-in maps. Thus the modelling is either tedious or not flexible.

The pump/compressor model in SPECTRA was designed to provide flexible modelling, while simultaneously limiting the amount of effort in input data preparation. The pump/compressor maps are approximated by a standard equation, which is built into the code. The coefficients in this equation are defined by the user. The user has therefore to define only a few input parameters that will provide the full pump/compressor map.

Pump/compressor map is approximated in SPECTRA by a parabolic equation. The shape of map depends on the user-defined parameters, such as  $V_{0}$ ,  $C_{RS}$ ,  $C_{RF}$ ,  $C_{DS}$ ,  $C_{VS}$  and exponents *a*, *b*, *c*. The user-defined parameters and their effect on the pressure head are illustrated in Figure 4-6.



Figure 4-6 Influence of input parameters: CP, CRS, CDS, CVS, on the pump map.

Note that in the previous code versions  $C_P$  was the pump/compressor input parameter, instead of  $V_0$ . This was changed in order to make the pump/compressor input parameters the same as the turbine input parameters. There is a simple relation between  $C_P$  and  $V_0$ . The relation is shown in the section describing the input parameters (section 2.2.8), so the user can easily convert his old input decks.

The user must in each case check his maps. This is done quite simply. A test run is set up, with a pump being between two volumes with time dependent conditions. The conditions should be selected in such way as to force the pump to operate in the range that needs to be plotted to create a full map. Several identical pumps may be set, each operating with different speed. The resulting flow and pressure head (or pressure ratio) of each pump are then plotted. Instead of plotting them against time (V=f(t),  $\Delta P=f(t)$ ), they are plotted against each other ( $\Delta P=f(V)$ ). In this way maps with curves for several different pump/compressor speeds are obtained. Such maps are discussed in sections A.2.2 and A.2.3. Examples of input files for creating such maps are given in Volume 3.

### A.2 Pump/Compressor Maps

Section A.2.1 shows definitions of reduced (dimensionless) parameters, which are being used with the pump/compressor maps. The discussion of the pump/compressor maps is provided in two parts. In the first part (section A.2.2) an "ideal" map is described, that is a map based on parabolic equation, in which surge does not appear (surge degradation factor,  $C_{DS} = 1.0$ ). The second part (section A.2.3) describes how the surge is modelled.

### A.2.1 Reduced Parameters

The reduced (dimensionless) parameters, which are being used with the pump/compressor maps, are:

- Reduced speed,  $\omega_R$ ,
- Reduced flow,  $V_R$ .
- Reduced pressure head  $P_R$ , or reduced pressure ratio,  $\Pi_R$ .

The user has several options as to how these parameters are defined. The available definitions are discussed below.

#### Reduced speed, $\omega_R$

The reduced speed  $\omega_R$ , is calculated based on the user defined nominal speed,  $\omega_N$ , (s<sup>-1</sup>), and eventually the nominal temperature  $T_N$ , (K). If the nominal temperature,  $T_N$ , is not specified, then the reduced speed is defined as:

$$\omega_R = \left(\frac{\omega}{\omega_N}\right) \tag{1}$$

If a positive nominal temperature,  $T_N$ , is specified, then the reduced speed is defined as:

$$\omega_{R} = \frac{\left(\frac{\omega}{\omega_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}}$$
(2)

In the above definitions  $\omega$  is the pump speed and T is the temperature at the inlet to the pump/compressor. The first definition is appropriate for typical pumps (see for example (Featherstone, 1982)), while the second is appropriate for typical gas compressors (see for example (Logan, 1995)).

#### Reduced flow, $V_R$

The reduced flow  $V_R$ , is calculated based on the user defined nominal volumetric flow,  $V_N$ , (m<sup>3</sup>/s) and eventually the nominal temperature  $T_N$ , the nominal fluid velocity,  $v_N$ , the nominal gas constant,  $R_N$ . If only the nominal flow,  $V_N$ , is entered, then the reduced flow is defined as:

$$V_R = \left(\frac{V}{V_N}\right) \tag{3}$$

If a positive nominal temperature,  $T_N$ , is specified, then the reduced flow is defined as:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \tag{4}$$

If a positive nominal fluid velocity,  $v_N$ , is specified, then the reduced flow is defined as:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$
(5)

Finally, if a positive nominal gas constant,  $R_N$ , is specified, then the reduced flow is defined as:

$$V_{R} = \frac{\left(\frac{V}{V_{N}}\right)}{\left(\frac{R}{R_{N}}\right)\sqrt{\frac{T}{T_{N}}}} \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$
(6)

In the above definitions V is the pump volumetric flow, T is the gas temperature at the inlet to the pump, v is the fluid velocity in the pump/compressor. R and  $c_p$  are the perfect gas constant and the specific heat at constant pressure for the gas mixture flowing through the pump/compressor.

The first definition (equation (3)) is appropriate for typical pumps (see for example (Featherstone, 1982)). The last definition (equation (6)) is appropriate for typical gas compressors, as will be shown below. The intermediate definitions are approximations of the exact formula for compressors.

In case of gas compressors, the maps are frequently defined using so called, "corrected flow",  $W_{corr}$ , defined as (see for example (Logan, 1995)):

$$W_{corr} = W \frac{\sqrt{T_{tot}}}{p_{tot}} \tag{7}$$

Where *W* is the mass flow,  $T_{tot}$  is the total temperature (based on the enthalpy,  $h=c_p T$ , and the kinetic energy,  $v^2/2$ ), and  $p_{tot}$  is the total pressure (static, *p*, and dynamic,  $\rho v^2/2$ ). The above formula can be transformed as follows:

$$W \frac{\sqrt{T_{tot}}}{p_{tot}} = W \frac{\sqrt{T + v^2 / 2c_p}}{p + \rho v^2 / 2} = W \frac{\sqrt{T}}{p} \frac{\sqrt{1 + v^2 / 2c_p T}}{1 + \rho v^2 / 2p} =$$

$$= \rho V \frac{\sqrt{T}}{p} \frac{\sqrt{1 + v^2 / 2c_p T}}{1 + \rho v^2 / 2p} = \frac{V}{R\sqrt{T}} \frac{\sqrt{1 + v^2 / 2c_p T}}{1 + v^2 / 2RT}$$
(8)

In the above transformation use was made of the perfect gas law:  $p = \rho RT$ , and the relation  $W = \rho V$ . The above formula is written in SPECTRA in a dimensionless form, by replacing each dimensional parameter by the ratio of the parameter and it's nominal value. The result is:

$$\frac{\left(\frac{V}{V_{N}}\right)}{\left(\frac{R}{R_{N}}\right)\sqrt{\frac{T}{T_{N}}}} \quad \frac{\sqrt{\frac{1+v^{2}/2c_{p}T}{1+v_{N}^{2}/2c_{p}T_{N}}}}{\left(\frac{1+v^{2}/2RT}{1+v_{N}^{2}/2RT_{N}}\right)}$$
(9)

The above formula is identical to the last formula for  $V_R$ , (equation (6) shown above). Therefore the equation (6) gives a dimensionless form of the corrected flow,  $W_{corr}$ .

If the gas composition does not change during calculations, then the gas constant R is always equal to the  $R_N$ , and the gas constant ratio can be removed from the formula. Therefore equation (5) is exact as long as the gas composition does not change. If additionally the dynamic terms can be neglected compared to the static terms, then the terms with velocity squared disappear from the formula (9), and it becomes identical with the equation (4). Summarising, the following options may be used to calculate the reduced flow:

- 1. Equation (3), appropriate for pumps,
- 2. Equation (4), appropriate for compressors with no gas composition changes and dynamic terms neglected.
- 3. Equation (5), appropriate for compressors with no gas composition changes.
- 4. Equation (6), appropriate for compressors without any restrictions and simplifications.

#### Reduced pressure head $P_R$ , or reduced pressure ratio, $\Pi_R$

The user can define either the nominal pressure head (Pa), or the nominal pressure ratio, (-). If the nominal pressure head,  $\Delta P_N$ , is specified, then the pump/compressor map uses the reduced pressure head,  $\Delta P_R$ , defined as:

$$\Delta P_R = \left(\frac{\Delta P}{\Delta P_N}\right) \tag{10}$$

If the nominal pressure ratio,  $\Pi_N$  is specified, then the pump/compressor map uses the reduced pressure ratio,  $\Pi_R$ , defined as:

$$\Pi_R = \left(\frac{\Pi}{\Pi_N}\right) \tag{11}$$

In the above definitions  $\Delta P$  and  $\Pi$  are the pressure head and the pressure ratio respectively. If the pressure ratio is used, then the reduced pressure head,  $\Delta P_R$ , is replaced by  $(\Pi - 1)/(\Pi_R - 1)$ .

#### A.2.2 Pump/Compressor Maps - Ideal Map with no Surge

Definitions and detailed descriptions of all parameters are provided in the User's Guide section 2.2.8. Below a short description is provided how each parameter affects the shape of the pump/compressor pressure head.

The pump/compressor model is based on the map, which is approximated by the following equation:

$$\Delta P_R = C_{RS} C_P \ \omega_R^a \mp C_{RF} (C_P - 1) \omega_R^b V_R^c \tag{12}$$

- where:  $\Delta P_R$  Reduced pressure head, (-). If the nominal pressure ratio,  $\Pi_N$ , is specified, the pressure head is equal to:  $\Delta P_N(t) = (\Pi_N - 1) \cdot P_0(t)$ , where  $P_0(t)$  is the current pressure upstream the pump. In this case the reduced pressure head,  $\Delta P_R$ , in the above formula is replaced by  $(\Pi - 1)/(\Pi_N - 1)$ , where  $\Pi = (\Delta P/P_0 + 1)$ ,  $\Delta P$  is the actual pressure head in (Pa), and  $\Pi_N$  is the nominal pressure ratio (input parameter) that is related to the nominal pressure head,  $\Delta P_N(t)$  (time-dependent) by  $\Pi_N = \Delta P_N(t)/P_0(t) + 1$ .
  - $V_R$  Reduced pump flow, (-).
  - $\omega_R$  Reduced pump speed, (-).
  - $C_P$  Constant defining the shape of pressure head in pump map, (-),  $C_P > 1.0$ . The value of  $C_P$  is related to the input parameters  $V_N$  (VFNPJN), and  $V_0$  (VF0PJN), as:  $C_P = (V_0/V_N)^c / ((V_0/V_N)^c 1)$
  - $C_{RS}$  Degradation factor for reverse speed, (-),  $\omega > 0.0$ :  $C_{RS} = 1.0$  $\omega < 0.0$ :  $C_{RS}$  is given by the user-defined parameters CRSPJN.
  - $C_{RF}$  Degradation factor for reverse flow, (-),<br/>V > 0.0:  $C_{RF} = 1.0$ <br/>V < 0.0:  $C_{RF}$  is given by the user-defined parameters CRFPJN.a First exponent (default value of 2.0).b Second exponent (default value of 1.0).
  - c Third exponent (default value of 2.0).

In the above equation the sign is – in case of positive flow, and + in case of negative flow. The parameters  $V_{0}$ ,  $C_{RS}$ ,  $C_{RF}$ , a, b, c, are user-defined. The influence of these parameters on the shape of pump map is discussed below.

Influence of  $C_P(V_0/V_N)$  on the pump map is shown in Figure 4-7. The following nominal parameters were assumed to make the plot.

$\Delta P_N$	$= 1.0 \times 10^5 \text{ Pa},$
$V_N$	$= 1.0 \text{ m}^{3/\text{s}},$
$\omega_N$	$= 50.0 \text{ s}^{-1}$ .

Figure 4-7 shows pressure heads made for values of  $V_0/V_N$  between 10.0 (corresponding  $C_P$  of 1.01) and 1.01 (corresponding  $C_P$  of 50.8). The corresponding values of  $C_P$ , calculated for the default value of the exponent *c* (*c*=2.0) are shown below:

$V_0/V_N = 10.0$	$C_P = 1.01$	
$V_0/V_N = 3.3$	$C_P = 1.10$	
$V_0/V_N = 2.0$	$C_P = 1.33$	(typical water pump)
$V_0/V_N = 1.2$	$C_P = 3.27$	(typical gas compressor)
$V_0/V_N = 1.01$	$C_P = 50.8$	(piston pump)



Figure 4-7 Influence of the parameter  $V_0$ , on the pump maps.  $V_0/V_N$  between 10.0 ( $C_P = 1.01$ ) and 1.01 ( $C_P = 50.8$ ).

It is seen that when  $V_0/V_N$  is very small ( $V_0/V_N=1.01$ ) then the pressure head makes a nearly vertical line. This means that the pump flow is nearly constant, independently of the pressure head. This shape is typical for the piston pumps. When  $V_0/V_N$  is very large, the pressure head line becomes flat. (If the Type 1 pump is used, then very large values of  $V_0/V_N$  may also cause numerical solution problems - the flow is quite sensitive to any pressure changes.).

<u>The influence of the degradation factor for reverse flow,  $C_{RF}$ , on the pump map is illustrated in Figure</u> 4-8. The value of  $C_{RF}$  affects the pump map only in the reverse flow range. If the default value is used ( $C_{RF} = 1.0$ ) then the pressure head lines in the negative flow range are symmetrical to the lines in the positive flow range. If  $C_{RF} < 1.0$  then the pressure head lines in the negative flow are flatter than in the positive flow. If  $C_{RF} > 1.0$  then the pressure head lines in the negative flow are steeper than in the positive flow. Comparison with the pump map from RELAP-5 (Dimenna, 1988), shown in Volume 3, shows that the latter value is appropriate to represent the pump map from RELAP-5.

The influence of the degradation factor for reverse speed,  $C_{RS}$ , on the pump map is illustrated in Figure 4-9 through Figure 4-12. The figures show pump maps on the  $\omega$ -V diagram for several different pressure heads, ranging from -1.0 bar to +1.0 bar. The pump nominal values assumed to plot the maps shown in these figures are:

$$\Delta P_N = 1.0 \times 10^5 \text{ Pa},$$
  
 $V_N = 1.0 \text{ m}^{3/\text{s}},$   
 $\omega_N = 50.0 \text{ s}^{-1}.$ 



Figure 4-9 shows the pump map for  $C_{RS} = 0.1$ . This is the map of a typical centrifugal pump (such as built-in RELAP code - compare (Dimenna, 1988), figure 8-1, constant head lines). It is seen that when the pump speed is reversed the lines bend to the right, which means the flow tends to be in the positive direction, although it is smaller than in case of the positive pump speed.

To illustrate the influence of  $C_{RS}$ , the pump map for  $C_{RS} = 1.0$  is shown in Figure 4-10. The lines are symmetrical with respect to the horizontal axis, which means the pump behaves exactly the same when it turns forward or reverse. Such pumps do not exist in practice. Theoretically one could build such a pump if the blades were made flat, and several outlet collectors were placed symmetrically around the pump. The pump would have to look something like the one shown in Figure 4-10. Such a pump would of course be very inefficient, and the example is shown here only to illustrate the influence of  $C_{RS}$  on the shape of the pump map.

The above two examples show that for the centrifugal machines (pumps, centrifugal compressors or centrifugal fans) an appropriate value of  $C_{RS}$  is positive and less than 1.0:

centrifugal pumps: 
$$0.0 < C_{RS} < 1.0$$

It is observed that with decreasing  $C_{RS}$  the lines of the pump map become more vertical in the negative pump speed range.

Figure 4-11 shows the pump map for  $C_{RS} = -0.1$ . This is a map of an axial pump/compressor. When the pump speed is reversed, the flow also reverses.

Figure 4-12 shows the pump map for  $C_{RS} = -1.0$ . For this value the lines are symmetrical with respect to the coordinate center. That means when the pump speed is reversed the behavior is the same as if it

was placed in the opposite direction and running forward. An example of such pump is a simple, low efficiency axial fan, with flat blades.

The above two examples show that for the axial machines (typical compressors, fans) an appropriate value of  $C_{RS}$  is negative, and not smaller than -1.0:

axial pumps: 
$$-1.0 < C_{RS} < 0.0$$

It is observed that with decreasing absolute value of  $C_{RS}$  the lines of the pump map become more vertical in the negative pump speed range.

The maps discussed above were produced using the value of exponents: a=2.0, b=0.0 (default settings for the Type 1 pump). Comparisons with typical pump and compressors maps show that a better value for the exponent *b* is 0.5 - 1.0. Below, Figure 4-13 and Figure 4-14 show two maps for a=2.0, b=0.5. The first map (Figure 4-13) is a "centrifugal pump" map, with  $C_{RS} = +0.1$ . The second map (Figure 4-14) is an "axial pump" map, with  $C_{RS} = -0.1$ . The value of b=0.5 is a default setting for the Type 2 pump (the pump type recommended for general use). When b > 0.0 the pressure head is equal to zero when the pump/compressor speed is zero. This is more realistic than having a non-zero head with zero speed, which is the case when b = 0.0.

The <u>influence of the exponents a, b, c, on the pump maps</u> is shown in Figure 4-15 through Figure 4-20. The Type 1 pump settings (a=2.0, b=0.0) are shown in Figure 4-15. With these values of exponents the pressure head lines run approximately parallel, and never cross. See also the turbine map with the same a, b, appendix B, Figure 4-32. Note that compared to the pump/compressor maps, the turbine maps are "upside-down" because of different definition of the turbine pressure ratio (inverse).

Figure 4-16 shows the pressure head lines for (a=2.0, b=1.0). The lines cross each other in negative head range, which is not visible here, but will be clearly visible in the turbine maps - see appendix B, Figure 4-33. Note that compared to the pump/compressor maps, the turbine maps are "upside-down".

Figure 4-17 shows the pressure head lines for (a=2.0, b=2.0). The lines cross each other in the same point, at the value of pressure head equal to zero. This is not visible here, but will be clearly visible in the turbine maps (see appendix B, Figure 4-34 - note that compared to the pump/compressor maps, the turbine maps are "upside-down").

Figure 4-18 shows the pressure head lines for (a=3.0, b=1.0). Comparison of Figure 4-16 and Figure 4-18 shows that increasing the value of a one obtains a pump that is more sensitive to the speed changes, i.e. a certain (say 10%) change of speed running at nominal conditions results in larger change of the pressure head.

The influence of the exponent c on the pump/compressor map is shown in Figure 4-19 and Figure 4-20. These figures show the maps obtained with the exponent c equal to 3.0 (default value is 2.0), and all other parameters being the same as shown in Figure 4-15 and Figure 4-16. Thus the influence of the exponent c is seen by comparing Figure 4-19 with Figure 4-15, and Figure 4-20 with Figure 4-16.



Pump/Compressor Model

Figure 4-9 Influence of the parameter  $C_{RS}$  on the pump maps.  $C_{RS} = 0.1$  (typical centrifugal pump).









Pump/Compressor Model

Figure 4-11 Influence of the parameter  $C_{RS}$ , on the pump maps.  $C_{RS} = -0.1$  (typical axial pump).



Figure 4-12 Influence of the parameter  $C_{RS}$ , on the pump maps.  $C_{RS} = -1.0$  (theoretical axial "pump").



Pump/Compressor Model

Figure 4-13 Influence of the parameter  $C_{RS}$ , on the pump maps.  $C_{RS} = 0.1 \ (a=2.0, b=0.5, c=2.0).$ 



Figure 4-14 Influence of the parameter  $C_{RS}$ , on the pump maps.  $C_{RS} = -0.1$  (*a*=2.0, *b*=0.5, *c*=2.0).















Figure 4-18 Influence of exponents on map, *a*=3.0, *b*=1.0, *c*=2.0.







Figure 4-20 Influence of exponents on map, a=2.0, b=1.0, c=3.0 (compare Figure 4-16).

Negative values of the exponent *b*, although generally not recommended, was found useful for matching some compressor map data. If b < 0.0, then the term with  $\omega_R^{b}$  is becoming large when the speed is small, giving unrealistically large pump head or compressor pressure ratio for a slowly turning machine. To prevent this a limit is imposed on  $\omega_R^{b}$ :  $\omega_R^{b} < \omega_{lim}^{b}$ . For lower speeds the term is linearly interpolated to give zero for zero speed (see Figure 4-21). Default value of  $\omega_{lim}^{b}$  is equal to 10.0 (input parameter BLMPJN, Word 27, records 231XXX and 233XXX). The data in Figure 4-21 is shown for the limit equal to 2.0. The pump/compressor map for the parameter *b* equal to -1.0 is shown in Figure 4-22. Comparison with Figure 4-20 shows how the map changes when the value of *b* is changed from +1.0 to -1.0.





Figure 4-21 Influence of the limit B-LIM in case of negative *b*.



Figure 4-22 Influence of exponents on map, *a*=2.0, *b*=–1.0, *c*=3.0 (compare Figure 4-20).

## A.2.3 Pump/Compressor Maps - Degradation of Head (Surge Model)

In the low flow range the machines such as compressors typically lose their capability to provide head. This is called "surge". In case of pumps the maps are close to the ideal maps, shown above. However, even in case of pumps a small decrease of head in low flow range is typically observed - see Volume 3 - comparison with pump model from RELAP-5.

In SPECTRA three input parameters are introduced in order to model the pump/compressor behavior in the low flow range. These are:

- $C_{VS}$  relative volumetric flow at which degradation begins, defined as a ratio of the flow at which surge starts to the flow at zero pressure head at nominal speed (see Figure 4-6).
- $C_{DS}$  degradation factor, defined as the ratio of the degraded pressure head at zero flow to the undegraded pressure head at zero flow (resulting from the un-degraded pump/compressor model equation - see Figure 4-6).
- *s* exponent in surge region interpolation.

The low flow region (the surge region) is defined as a region where the volumetric flow is:

$$V < V_{surge} = C_{VS} \cdot V_0(\omega) = C_{VS} \cdot V_N \cdot \left(\frac{C_P}{C_P - 1}\right)^{1/c} \cdot \left(\frac{\omega_R^a}{\omega_R^b}\right)^{1/c}$$

In the low flow range the pump head is decreased by introducing an effective speed,  $\omega'$ , defined as:

$$\omega' = \omega \cdot [C_{DS}^{1/a} + (1 - C_{DS}^{1/a}) \cdot (V/V_{surge})^{1/s}]$$

Substituting the above formula into the pump/compressor model equation, shown in section A.2.2, one obtains the formula applied in the low flow (surge) region:

$$\Delta P_{R} = C_{P} \cdot \omega_{R}^{a} \cdot [C_{DS}^{1/a} + (1 - C_{DS}^{1/a}) \cdot (V / V_{surge})^{1/s}]^{a} \mp$$
  
$$\mp (C_{P} - 1) \cdot \omega_{R}^{b} \cdot [C_{DS}^{1/a} + (1 - C_{DS}^{1/a}) \cdot (V / V_{surge})^{1/s}]^{b} \cdot V_{R}^{c}$$

The influence of the surge parameters  $C_{VS}$  and  $C_{DS}$ . is discussed first for a typical compressor. Next, examples of a typical pump are shown and the influence of the exponent *s* on the stability of the pump is discussed.

For the next case a very small degradation factor was assumed:

relative flow:	$C_{VS}$	= 0.7,
degradation factor	$C_{DS}$	= 0.01.

Such a small value of  $C_{DS}$  is appropriate for gas compressors. The value of the constant  $C_P$  has been chosen as 3.0 (typical compressor). With this value of  $C_P$  the lines are relatively steep ( $C_P \sim 1.3$  for typical pump maps - see discussion below), and the relative flow for surge,  $C_{VS}$ , is large (0.7) compared to a typical pump (~0.3 - see discussion below). The resulting pressure head map is shown in Figure 4-23.



Figure 4-23 Influence of surge parameters on map,  $C_{DS}$ =0.01,  $C_{VS}$ =0.7 ( $V_0/V_N$ =1.2 - typical compressor).



 $(V_0/V_N=1.2 - typical compressor).$
The equation determining the pump/compressor map implies that at the nominal speed ( $\omega_R$ =1.0),  $V_N$ , is related to  $V_0$  by (see Figure 4-6):

$$\frac{V_N}{V_0} = \left(\frac{C_P - 1}{C_P}\right)^{1/c}$$

The relative flow for surge is typically smaller than the nominal flow, thus:

C -	V <sub>surge</sub>	$V_{N}$	$\left( C_P - 1 \right)^{1/2}$	' c
$C_{VS}$ -	$V_0$	$\overline{V_0}$	$-\left(\begin{array}{c} \hline C_P \end{array}\right)$	

Therefore:	for $C_P = 1.3$ ,	$C_{VS} < 0.480,$
	for $C_P = 3.0$ ,	$C_{VS} < 0.816.$

If  $C_{VS}$  is greater than the limit defined by the above formula, the code issues a warning message.

The next example is presented to illustrate the ability of the user to specify a variable surge limit:  $C_{VS} = f(\omega)$ . All the parameters are the same as above, except for the  $C_{VS}$ . In the present case the value is tabulated, as shown in the table below.

Table 4-1 Example of volumetric flow limit for surge as a function of speed.

$\omega/\omega_N$	0.20	0.40	0.60	0.80	1.00
$C_{VS}$	0.55	0.60	0.65	0.70	0.75

The results are shown in Figure 4-24. The pressure head lines are very similar to those observed in Figure 4-27. The only difference is the location of the surge limit. In Figure 4-24 the surge limit varies from 0.55 to 0.75, depending on the speed, while in Figure 4-23 it is constant and equal to 0.7.

The next examples show maps with low values of the degradation factor. Such maps are appropriate for typical water pumps. Before the pump examples are shown, a short discussion is presented on the stability of pump characteristics. The pump map has locally unstable characteristics if there is a region where the pressure head decreases with decreasing fluid flow. In this region stable operation of the pump is impossible; the fluid flow will oscillate between the two points bounding the unstable part of the map.

In order to obtain conditions for stable pump characteristics, it is important to find out what is the pressure head at zero flow, compared to the pressure head at the surge point. The pump/compressor pressure head at zero flow is equal to:

$$\Delta P_R\Big|_{V=0.0} = C_P \cdot \omega_R^a \cdot C_{DS}$$

The surge point flow is equal to:

$$\frac{V_{surge}}{V_0} = C_{VS}$$

Using the relation between  $V_N$  and  $V_0$ :

$$\frac{V_0}{V_N} = \left(\frac{C_P}{C_P - 1}\right)^{1/c} \cdot \left(\frac{\omega_R^a}{\omega_R^b}\right)^{1/c}$$

the relative flow at surge can be expressed as:

$$\left(\frac{V_{surge}}{V_N}\right) = \left(\frac{V_{surge}}{V_0}\right) \cdot \left(\frac{V_0}{V_N}\right) = C_{VS} \cdot \left(\frac{\omega_R^a}{\omega_R^b}\right)^{1/c} \cdot \left(\frac{C_P}{C_P-1}\right)^{1/c}$$

The pressure head at the surge point is therefore equal to:

$$\Delta P_R \Big|_{V=surge} = C_P \cdot \omega_R^a - (C_P - 1) \cdot \omega_R^b \cdot \left(\frac{\omega^a}{\omega^b}\right) \cdot \left(\frac{C_P}{C_P - 1}\right) \cdot C_{VS}^c$$
$$\Delta P_R \Big|_{V=surge} = C_P \cdot \omega_R^a \cdot (1 - C_{VS}^c)$$

The pressure head at zero flow is equal to the pressure head at the surge point if:

$$C_P \cdot \omega_R^a \cdot C_{DS} = C_P \cdot \omega_R^a \cdot (1 - C_{VS}^c)$$

or:

or:

 $C_{DS} = 1 - C_{VS}^c$ 

If the head at zero flow is smaller than the pressure head at the surge point, then there will certainly be an unstable region in the pump map. The necessary condition to obtain a stable pump is therefore:  $C_{DS} \ge 1 - C_{VS}^{c}$ . As will be shown below, this condition is not sufficient to obtain a stable pump. A proper value of the exponent *s* is needed to ensure a fully stable pump map.

The example cases presented below were calculated using the default value of  $V_0/V_N = 2.0$  (typical centrifugal pump). In the first case the value of  $C_{VS}$  was set to 0.3 (This value is still somewhat too high compared to a typical pump - see Volume 3 - but it gives a more clearly visible unstable region.)

*relative flow:* 
$$C_{VS} = 0.3$$

To obtain a stable map, the value of  $C_{DS}$  must be greater than or equal to  $1 - 0.3^2 = 0.91$ . The first example was run with this value:

degradation factor 
$$C_{DS} = 0.91$$
.

The resulting pressure head map is shown in Figure 4-25. It is seen that although the pressure head at the surge point and at the zero flow are the same, there is an unstable region in the pump map. The unstable region is marked in the figure.



Pump/Compressor Model - Test MAP091

Figure 4-25 Influence of surge parameters on map,  $C_{DS}$ =0.91,  $C_{VS}$ =0.3, s=1.0 ( $V_0/V_N$ =2.0 - typical pump).



Figure 4-26 Influence of surge parameters on map,  $C_{DS}$ =0.95,  $C_{VS}$ =0.3, s=1.0 ( $V_0/V_N$ =2.0 - typical pump).



Pump/Compressor Model - Test MAP091S

Figure 4-27 Influence of surge parameters on map,  $C_{DS}$ =0.91,  $C_{VS}$ =0.3, s=0.5 ( $V_0/V_N$ =2.0 - typical pump).



Figure 4-28 Influence of surge parameters on map,  $C_{DS}$ =0.95,  $C_{VS}$ =0.3, s=0.5 ( $V_0/V_N$ =2.0 - typical pump).

In the next example the degradation factor was set to a higher value:

degradation factor  $C_{DS} = 0.95$ .

The resulting pressure head map is shown in Figure 4-26. It is seen that the unstable region still exists, although it is smaller than in the previous case.

The next two cases were run with the same degradation factors, namely 0.91 and 0.95 respectively, but with the exponent *s* decreased from 1.0 (the default value) to 0.5. The results are shown in Figure 4-27 and Figure 4-28. It is seen that there is no unstable region in both maps.

It is interesting to note that the map shown in Figure 4-27 is similar to the pump map applied in the MELCOR code (see (Summers, 1997), Reference Manual, CVH/FL Package). MELCOR however does not take into account a change of the pressure head with the pump speed; the pump is simply on (nominal speed) or off (zero pressure head). Moreover in MELCOR the pump head does not change in negative speed range, so the MELCOR model and the model shown in Figure 4-27 are identical provided that a check valve is present, prohibiting backflow through the pump.

The above examples show that in order to obtain a stable map the exponent *s* should be set to 0.5. The default value of *s* (1.0) was selected because this is most appropriate for gas compressors, and the surge model is of primary importance for gas compressors. If s = 0.5 is used for the example shown in Figure 4-23, then the pressure head will become negative in the low flow range - see the example case shown in Figure 4-29.



Figure 4-29 Influence of surge parameters on map,  $C_{DS}$ =0.01,  $C_{VS}$ =0.7, s=0.5 ( $V_0/V_N$ =2.0 - typical compressor).

Use of the exponent *s* in order to provide a stable map may be important in analyses involving typical pumps. For example, the pump model applied in RELAP-5 (Dimenna, 1988) is best approximated using a stable map, with s = 0.5 - see Volume 3.

#### **References of Appendix A**

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#### **Turbine Maps** appendix B

The turbine model is based on the same approach as the turbine Type 2 model (see appendix A). In fact the turbine model uses exactly the same subroutine as the Type 2 turbine/compressor. Only the input procedures are slightly different. All input parameters are the same as in case of the Type 2 pump. The turbine nominal parameters, such as nominal flow and pressure ratio or head, are internally converted by the code into nominal parameters of an "equivalent pump", as shown in Figure 4-30. The equivalent pump is defined as a pump/compressor that has exactly the same map as the turbine, if the map is plotted in terms of the pump pressure ratio (outlet divided by inlet pressure) rather than the turbine pressure ratio (inlet divided by outlet pressure).

The "equivalent pump" approach allows to perform calculations using the same subroutines that are calculating pumps/compressors. The equation defining turbine behavior is therefore exactly the same as the equation defining the pump/compressor map (see appendix A), and is therefore not discussed here. Only the conversion to the "Equivalent Pump" is shown below.

Using the equation defining the pump map (appendix A), it may be shown that nominal parameters of the equivalent pump are related to the turbine parameters as follows:

nominal volumetric flow:

$$V_{E.P.} = V_0 \cdot \left[ (C_P - 1) / C_P \right]^{(1/c)}$$

nominal pressure ratio (if the pressure ratio is entered):

$$\Pi_{E.P.} = 1 + \frac{1 - 1/\Pi_N}{(C_P - 1) (V_N / V_{E.P.})^c - C_P}$$

nominal pressure head (if the pressure head is entered):

$$\Delta P_{E.P.} = \frac{\Delta P_{N}}{(C_{P} - 1) (V_{N} / V_{E.P.})^{c} - C_{P}}$$

where:	$\Pi_N$	-	nominal turbine pressure ratio, (-), (user defined),
	$\Delta P_N$	-	nominal turbine pressure head, (Pa), (alternatively user defined),
	$V_N$	-	nominal turbine flow, (m <sup>3</sup> /s), (user defined),
	$V_0$	-	flow at zero-head $\Delta P = 0.0$ (or $\Pi = 1.0$ ), (m <sup>3</sup> /s), (user defined),
	$\Pi_{E.P.}$	-	nominal pressure ratio of the "equivalent pump", (-),
	$\Delta P_{E.P.}$	-	nominal pressure head of the "equivalent pump", (Pa),
	$C_P$	-	constant in pump map (see appendix A). Note that the value of this constant
			affects the nominal parameters of the "equivalent pump", but does not
			influence the turbine map, which is fully defined by $V_N$ , $V_0$ , and $\Pi_N$ or $\Delta P_N$ .
	С	-	third exponent in turbine map definition, (-) (user defined).

The conversion to the "equivalent pump" is done automatically within the code; it is "transparent" for the user, i.e. the user works only with the turbine parameters  $(V_N, V_0, \Pi_N \text{ or } \Delta P_N)$  while internally calculations are performed using the equivalent pump parameters ( $V_{E.P.}$ ,  $\Pi_{E.P.}$  or  $\Delta P_{E.P.}$ ).



Figure 4-30 Turbine map - conversion of the turbine parameters into the "Equivalent Pump" parameters, performed internally by the code.

The parameters available to tune the turbine map are:  $V_0$ , the exponents *a*, *b*, *c*, and the constant  $C_{RS}$ , determining the turbine behavior in case of negative speed. The influence of these parameters on the turbine map is discussed below.

The <u>influence of the parameter  $V_0$  on the turbine maps</u> is quite obvious from the definition of the parameter. It is illustrated below, in Figure 4-31. The lines shown in this figure were obtained for a turbine with  $\Pi_N = 1.5$ ,  $V_N = 1.0$  m<sup>3</sup>/s,  $\omega_N = 50.0$  s<sup>-1</sup>, a = 2.0, b = 1.0, c = 1.0, running at nominal speed.

The <u>influence of the exponents a, b, c, on the turbine maps</u> is shown in Figure 4-32 through Figure 4-37. The following values were used to produce maps shown in these figures:

$\Pi_N$	= 1.5,
$V_N$	$= 1.0 \text{ m}^{3/\text{s}},$
$V_0$	$= 0.5 \text{ m}^{3}/\text{s},$
$\omega_N$	$= 50.0 \text{ s}^{-1}.$



Figure 4-31 Influence of  $V_0$  on turbine map (a=2.0, b=1.0, c=2.0),

The map obtained for (a=2.0, b=0.0, c=2.0) is shown in Figure 4-32. With these values of the exponents the pressure ratio lines run approximately parallel, and never cross. See also the pump/compressor map with the same a, b, c, - appendix A, Figure 4-15. Note that compared to the turbine maps, the pump/compressor maps are "upside-down" because of a different definition of the pressure ratio (inverse).

Figure 4-33 shows the pressure ratio lines for (a=2.0, b=1.0, c=2.0). The lines cross each other at flow  $V>V_0$ . (See also the pump/compressor maps with the same *a*, *b*, *c*, - appendix A, Figure 4-16. Note that compared to the turbine maps, the pump/compressor maps are "upside-down".)

Figure 4-34 shows the pressure ratio lines for (a=2.0, b=2.0, c=2.0). The lines cross each other in the same point; the point where the pressure head is equal to zero (or the pressure ratio equal to one, or the volumetric flow equal to:  $V=V_0$ ). With this set of constants the turbine becomes more sensitive to changes of speed; the pressure ratio is small for small turbine velocity and large for large velocity. (See also the pump/compressor map with the same *a*, *b*, *c*, - see appendix A, Figure 4-17. Note that compared to the turbine maps, the pump/compressor maps are "upside-down").

Figure 4-35 shows the pressure ratio lines for (a=3.0, b=1.0, c=2.0). Comparison of Figure 4-33 and Figure 4-35 shows that increasing the value of a, the lines cross at higher value of flow. (See also the pump/compressor map with the same a, b, c, - see appendix A, Figure 4-18. Note that compared to the turbine maps, the pump/compressor maps are "upside-down").

Note that in the case of a turbine, a machine more sensitive to speed changes is obtained by increasing the exponent b, while in case of pumps/compressors the same is achieved by increasing the exponent a.



Figure 4-32 Influence of exponents on turbine map, *a*=2.0, *b*=0.0, *c*=2.0.







Turbine Model - Test MAP22















The influence of the third exponent, c, is illustrated in Figure 4-36 and Figure 4-37. The maps shown in these figures should be compared to the map shown in Figure 4-33, to see how the map changes when c is increased from the default value of 2.0 (Figure 4-33) to 3.0 (Figure 4-36), and decreased to 1.5 (Figure 4-37).

<u>The influence of the reverse speed degradation factor,  $C_{RS}$ , on the turbine maps is shown in Figure 4-38, Figure 4-39 and Figure 4-40. The following values were used to produce maps shown in these figures:</u>

 $\begin{aligned} \Pi_N &= 1.5, \\ V_N &= 1.0 \text{ m}^3\text{/s}, \\ V_0 &= 0.5 \text{ m}^3\text{/s}, \\ \omega_N &= 50.0 \text{ s}^{-1}, \\ a &= 2.0, \\ b &= 1.0, \\ c &= 2.0. \end{aligned}$ 

Figure 4-38 shows turbine maps for  $C_{RS} = 0.1$  for the turbine speed,  $\omega$ , between +100% and -100%. It is seen that in case of negative (reverse) speed the pressure ratio is larger than for a corresponding positive speed. The difference is small for small  $|\omega|$ , and increases with increasing  $|\omega|$ .

Figure 4-39 shows turbine maps for  $C_{RS} = 2.0$  for the turbine speed,  $\omega$ , between +100% and -100%. In contrast to the previous case, the negative (reverse) speed gives smaller pressure ratio than that for a corresponding positive speed. Again, the difference is small for small  $|\omega|$ , and increases with increasing  $|\omega|$ .

Generally, it may be observed that for  $C_{RS} < 1.0$  the lines at reverse speed are above those at the corresponding normal speed, while for  $C_{RS} > 1.0$  the lines at reverse speed are below those at the corresponding normal speed.

Finally, Figure 4-40 shows turbine maps for  $C_{RS} = -1.0$  for the turbine speed,  $\omega$ , between +100% and -100%. With decreasing the value of  $C_{RS}$ , the pressure lines are higher in negative (reverse) speed range.

The influence of the parameter  $C_{RS}$  may be shortly described by looking at the maps for the (nearly) zero fluid flow and  $\omega = +100\%$  and  $\omega = -100\%$ . If  $C_{RS}$  is positive, then at nearly zero flow the turbine acts as compressor, i.e. it provides pressure head in the normal flow direction, for both forward and reverse speeds. On the other hand, if  $C_{RS}$  is negative, then at zero flow and  $\omega = +100\%$  the turbine acts as compressor, proving (a small) pressure head in the normal flow direction, while at zero flow and  $\omega = -100\%$  it acts as a compressor providing (a small) head in the reversed flow direction. It should be noted that for large fluid flows and  $\omega = -100\%$  it acts as a compressor providing a large pressure head in the reversed flow direction.

The default value of  $C_{RS}$  is -1.5. The value was chosen based on comparisons with four-quadrant turbine data, shown in (Bemmert, 1980). In the previous SPECTRA versions the default value of  $C_{RS}$  was equal to 0.1.









Influence of  $C_{RS}$  on turbine map,  $C_{RS}=2.0$ .



Turbine Model - Test MAP1

Figure 4-40 Influence of  $C_{RS}$  on turbine map,  $C_{RS}$ =-1.0.

The influence of the reverse flow degradation factor,  $C_{RF}$ , on the turbine maps is shown in Figure 4-41 and Figure 4-42. The following values were used to produce the maps shown in these figures:

$$\begin{array}{ll} \Pi_N & = 1.5, \\ V_N & = 1.0 \ {\rm m}^3/{\rm s}, \\ V_0 & = 0.5 \ {\rm m}^3/{\rm s}, \\ \omega_N & = 50.0 \ {\rm s}^{-1}, \\ a & = 2.0, \\ b & = 1.0, \\ c & = 2.0, \\ C_{RS} & = -1.5. \end{array}$$

The default value of value of  $C_{RS}$  was used in both figures. Comparison of Figure 4-41 and Figure 4-42 gives an indication of the influence of the reverse flow degradation factor,  $C_{RF}$ . The default value of  $C_{RF}$  is 0.05. The value was chosen based on comparisons with four-quadrant turbine data, shown in (Bemmert, 1980). In the previous SPECTRA versions the reverse speed factor was not used, which means that  $C_{RF}$  was by definition equal to 1.0.

Comparison of the maps obtained with different values of  $C_{RS}$  and  $C_{RF}$  with measurement data from (Bemmert, 1980), is shown in Figure 4-43 and Figure 4-44. The turbine nominal data were assumed following the data in (Bemmert, 1980):

$$\Pi_N = 3.91, V_N = 3.0 \text{ m}^3/\text{s}, \omega_N = 116.7 \text{ s}^{-1}, (7000 \text{ rev/min}).$$



Turbine Model - Test MAP4





Figure 4-42 Influence of  $C_{RF}$  on turbine map,  $C_{RF}$ =1.0,  $C_{RS}$ =-1.5.

The values of  $V_0$  and the exponents, suitable to represent reasonably well the turbine behavior in the normal operating conditions (positive speed, positive flow) were selected in a few trials as:

$$V_0 = 1.0 \text{ m}^3/\text{s}, a = 2.0, b = 0.5, c = 2.0.$$

The parameters determining the turbine behavior in the reverse speed and reverse flow conditions were selected to be:

$$C_{RS} = -1.5,$$
  
 $C_{RF} = 0.05.$ 

Figure 4-43 shows the measured power for positive (normal) and negative (reversed) flows and speeds. The positive speed values are plotted using solid lines and empty markers, while the negative speed values are plotted using dashed lines and filled markers.

Figure 4-44 shows the calculated values. The positive speed values are plotted using grey lines and empty markers, while the negative speed values are plotted using dark lines and filled markers. The left graph in Figure 4-44 shows values obtained with a constant efficiency of 1.0. In case of reversed speed and normal (positive) flow the fluid decompression is very similar to the decompression occurring in normal speed. Therefore the power calculated with the efficiency of 1.0 is negative (meaning the power is obtained from the machine – watch the scale in Figure 4-44). Based on the measured data it is clear that the power should be positive (the power is consumed by the turbine turning on backwards). This may be best explained using a h-s (enthalpy-entropy) graph, shown in Figure 4-45.

In case of an ideal isentropic expansion from a given pressure  $p_1$  to another pressure  $p_2$ , one obtains maximum power – this is the line 1-2a. This is an ideal process and it does not occur in practice. A practical process in a turbine at its normal operating conditions is shown by the line 1-2b. In such case some energy is dissipated as heat and the energy that is obtained from the turbine is smaller. The isentropic efficiency is in this case equal to:

$$\eta = \frac{\Delta h_1}{\Delta h_0}$$

A typical turbine has the efficiency of 0.7 - 0.9 in the typical operating conditions. The case of turbine turning on reverse (Figure 4-43 dashed lines), the fluid decompression is shown by the line 1-2c in Figure 4-45. The amount of energy dissipated as heat is so large that the exit enthalpy is higher than the inlet enthalpy. Consequently one has to put energy into the turbine to keep it running. In this case the turbine efficiency is negative, as shown in Figure 4-45.



Figure 4-43 Power – reference (Bemmert, 1980).



Figure 4-44 Turbine power  $C_{RS}$ =-1.5  $C_{RF}$ =0.05 (default in V. 2.10) left: only positive efficiency, right: negative efficiency in reverse speed.





Looking at Figure 4-43 it is clear that the efficiency is negative in all cases with reverse speed (except maybe the lowest negative speed case, in the negative flow range). For the calculations shown in the right graph in Figure 4-44 the following efficiencies were used:

Negative (reverse) flow
$\eta = +0.6$
$\eta = +0.4$
$\eta = +0.2$
$\eta = -0.1$
$\eta = -0.3$
$\eta = -3.0$

The values of efficiencies were obtained in few trials, in order to provide a reasonably good match to the measured data, shown in Figure 4-43. For simplicity a constant efficiency was defined for each speed, thus the efficiency was in fact only a function of speed:  $\eta = \eta(N)$ . The efficiency could be made as a function of both flow and speed,  $\eta = \eta(V, N)$  and in this way a better match could be obtained.

# **References of Appendix B**

Bemmert 1980 K. Bemmert, P. Zehner, "Measurements of the Four-Quadrant Characteristics on a Multi-Stage Turbine", *Journal of Engineering for Power, Transactions of ASME*, Vol. 102, pp. 316-321, April 1980.

## appendix C Pressure Loss Coefficients for Valves

In general the pressure loss coefficient of a valve changes with the valve open fraction. Sometimes the change is so significant that it is important to include a variable loss coefficient in the computational model.

• The following expression may be used to calculate the loss factors (forward and reverse):

$$K_{V} = K_{0} \cdot \left[ C_{V} + \left( 1 - C_{V} \right) \frac{A_{V}}{A_{0}} \right]$$

• Tabular Function may be used. The TF value is calculated by the program using the open fraction as an argument. The loss factors (forward and reverse) are calculated from:

$$K_V = K_0 \cdot TF(A_V / A_0)$$

These two methods are described in the following subsections.

#### C.1 Pressure Loss Coefficient Given by an Analytical Expression

SPECTRA uses two values to define valve characteristics:  $K_0$  and  $C_V$ . The actual loss coefficient is calculated from:

$$K_{V} = K_{0} \left[ C_{V} + (1 - C_{V}) \frac{A_{V}}{A_{0}} \right]$$

- $K_V$  current valve loss coefficient, (-)
- $K_0$  loss coefficient for fully open valve, (-) (FLCFJN or FLCRJN, record 210XXX)
- $C_V$  valve resistance increase coefficient, (-) (CVVLJN, record 220XXX)
- $A_V$  current valve open area, (m<sup>2</sup>)
- $A_0$  area for fully open valve, (m<sup>2</sup>) (AMAXJN, record 200XXX)

The values of  $K_0$  and  $C_V$  may be estimated, using the following relations:

$$C_{V} = \frac{K_{V} / K_{0} - A_{V} / A_{0}}{1 - A_{V} / A_{0}}$$

$$K_{V} \rightarrow K_{0} \qquad \text{when} \quad A_{V} \rightarrow A_{0}$$

$$K_{V} \rightarrow K_{0} \cdot C_{V} \qquad \text{when} \quad A_{V} \rightarrow 0.0$$

Data can easily be obtained from appropriate handbooks. Below a calculation procedure is shown, to obtain the coefficients for two valve types: a butterfly valve and a rectangular gate valve.

Butterfly Valve

Reference (Idel, 1986) gives loss coefficients for a butterfly valve in a tube of a circular cross section (Diagram 9-16 in (Idel, 1986)). In case of a thin plane disk (Curve 2 in Diagram 9-16) the values are:

θ°	0	10	20	30	40	50	60	70
K <sub>Idel</sub>	0.30	0.52	1.54	4.50	11.0	29.0	108.0	625.0

It must be remembered that the loss factors given in (Idel, 1986),  $K_{Idel}$ , are related to the velocity in a fully open channel. To obtain values related to the actual valve flow area one must multiply these values by the area ratio squared:  $(A/A_0)^2$ . For a given angle,  $\theta$ , the open area is given by:  $A=A_0 \cdot (1-\sin\theta)$ . Therefore the loss factors related to the actual flow area are equal to:  $K=K_{Idel} \times (1-\sin\theta)^2$ . The values of *K*, as well as  $K_{Idel}$ , are shown in Figure 4-46.

The value of  $K_0$ , needed for SPECTRA input, is equal to the loss factor for the fully open valve, thus 0.30. It has been found using a trial and error procedure, that a value of  $C_V=7.0$  represents well the *K* values in Figure 4-46. Thus, for the butterfly valve considered here the appropriate values are:

$$K_0 = 0.30,$$
  
 $C_V = 7.0.$ 



Figure 4-46

Loss factors, butterfly valve.

• Gate Valve

For a rectangular, single disk, gate valve the loss coefficients are given as a function of the ratio of the disk position (h), to the channel width (a) ((Idel, 1986), Diagram 9-5). The values are:

h/a	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
KIdel	193	44.5	17.8	8.12	4.02	2.08	0.95	0.39	0.09

Again the values of  $K_{Idel}$  are related to the velocity in a fully open channel. The values are therefore multiplied by the area ratio squared:  $(A/A_0)^2$ . For a rectangular value  $(A/A_0)^2$  is simply equal to  $(h/a)^2$ . The values of K, as well as  $K_{Idel}$ , are shown in Figure 4-47.

The value of  $K_0$ , needed for SPECTRA input, is equal to the loss factor for the fully open valve, thus 0.09. It has been found using a trial and error procedure, that a value of  $C_{v}=25.0$  represents well the K values in Figure 4-47. Thus, for the rectangular gate valve considered here the appropriate values are:

$$K_0 = 0.09,$$
  
 $C_V = 25.0.$ 



Figure 4-47 Loss factors, gate valve.

## C.2 Pressure Loss Coefficient Given by a Table

With this option the pressure loss factors (forward and reverse) are calculated from:

$$K_V = K_0 \cdot TF(A_V / A_0)$$

- $K_0$  constant multiplier on the pressure loss coefficient (forward and reverse)
- *TF* Tabular Function evaluated for the current valve open fraction,  $A_V/A_0$ , (-) (the TF number is indicated by negative value of CVVLJN, record 220XXX)

For example, in case of a butterfly valve the values are:

θ°	0	10	20	30	40	50	60	70
$A/A_0$	1.00	0.826	0.658	0.500	0.357	0.234	0.134	0.0603
$K_{Idel}$	0.30	0.52	1.54	4.50	11.0	29.0	108.0	625.0
K	0.30	0.355	0.667	1.13	1.40	1.59	1.94	2.27

The input deck defining such valve is discussed in Volume 3.

# **References of Appendix C**

Idel, 1986 I.E. Idelchik, "Handbook of Hydraulic Resistance", Second Edition, ISBN 3-540-15962-2, Hemisphere Publishing Corporation, 1986.